# Some preliminary investigations with a view to preparing acetic anhydride from acetaldehyde.

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Description: -

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Alternatively, the iodide salt may be generated in-situ since under the operating conditions of the reaction system, a wide range of non-iodide salt precursors will react with methyl iodide to generate the corresponding co-promoter iodide salt stabilizer. Also, invention proposes a method for removing organic iodides containing 10-16 carbon atoms from acetic acid or acetic anhydride involving contact of acetic acid or acetic anhydride comprising dodecyl iodide with silver- or mercury-exchange cationic ion-exchange substrate at temperature in the range 50°C - 150°C.

# Recent advances in the methanol carbonylation reaction into acetic acid

Water flow thus return back flow into the column 18 through line 62. You can see that the recommended concentration is then basically the same as for stabilizirovannye, and to increase speed. A method of purifying acetic anhydride or a mixture of acetic anhydride and acetic acid as recited in claim 1, wherein said ozone-treated acetic anhydride or said ozone-treated mixture of acetic anhydride and acetic acid is introduced into a plate column, having a top and a bottom and a middle section, at an introduction site located at said middle section of said plate column or at an upper part of said middle section, wherein said plate column contains 20 to 80 plates, and wherein said plate column is operated at a column top pressure of 100 mmHg to atmospheric pressure, and wherein a low-boiling impurity fraction is partly recovered from said top of said plate column and remaining overhead liquid is returned as a reflux in a reflux ratio of 50 to 500, and wherein purified acetic anhydride or a purified mixture of acetic anhydride and acetic acid is recovered in a vapor form from said 1st to 5th plate from said bottom of said plate column, with a high-boiling impurity fraction being recovered from said bottom of said plate column.

## Method for continuous producing acetic acid (variants) and method for treatment of acetic acid flow

The partial pressure of carbon monoxide in the reaction is suitably in the range 1 to 70 bar, preferably 1 to 35 bar, and most preferably 1 to 15 bar. A method of purifying acetic anhydride or a mixture of acetic anhydride and acetic acid as recited in claim 1, wherein said acetic anhydride or said mixture of acetic anhydride and acetic acid to be purified is contacted with ozone at a temperature of 20° C. Acetic acid containing a high-boiling fraction was continuously withdrawn from the bottom at a rate of 6.

Part of this liquid residue 27 is passed to a first evaporator 22' and then returned to the column to provide the heat required for fractionation, and the remainder is passed to a second fractionating column 24'.

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The resulting standardized solutions had the color number APHA 5, APHA 10, APHA 15, APHA 20 and APHA 25, respectively. As an example, the patent describes UD the other hexylidene of acetic acid at temperatures from about 25° With up to about 45°C.

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For practical purposes, the impeller-equipped stirring vessel type and sparger-equipped bubble column type are preferred.

# Method for continuous producing acetic acid (variants) and method for treatment of acetic acid flow

JP48030615 September, 1973 JP5564545 November, 1978 JP60222439 April, 1984 PURIFICATION OF CRUDE ACETIC ANHYDRIDE JP61002052 January, 1986 AUTOMATIC MOISTURE METER FOR GRAIN JP61056151 March, 1986 PURIFICATION OF ACETIC ACID JP01211548 August, 1989 PURIFICATION OF ACETIC ACID WITH OZONE JP02231448 September, 1990 METHOD FOR TREATING ACETIC ACID WITH HYDROGEN IN THE PRESENCE OF HYDROGENATION CATALYST JPH02231448A 1990-09-13 JPS4830615A 1973-04-23 JPH01211548A 1989-08-24 JPS5564545A 1980-05-15 JPS6156151A 1986-03-20 JPS612052A 1986-01-08 JPS60222439A 1985-11-07 What is claimed is: 1.

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