

# SPE Symposium: Decarbonisation Initiative: CO<sub>2</sub> Sequestration Opportunities in Global Energy Transition

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# Estimating Storable Quantities for CCS Projects

Shane Hattingh  
Gaffney, Cline & Associates



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## Introduction, Objectives and Content

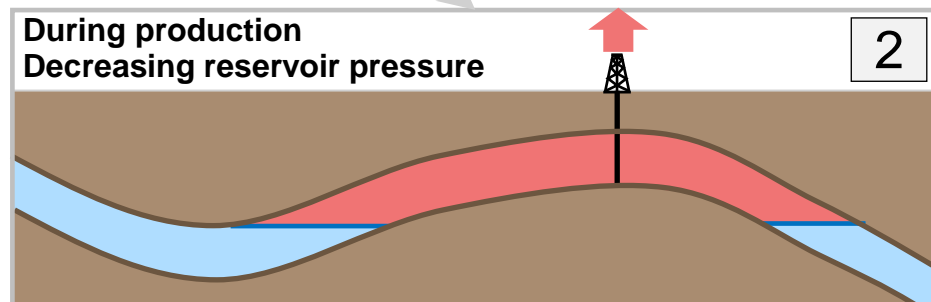
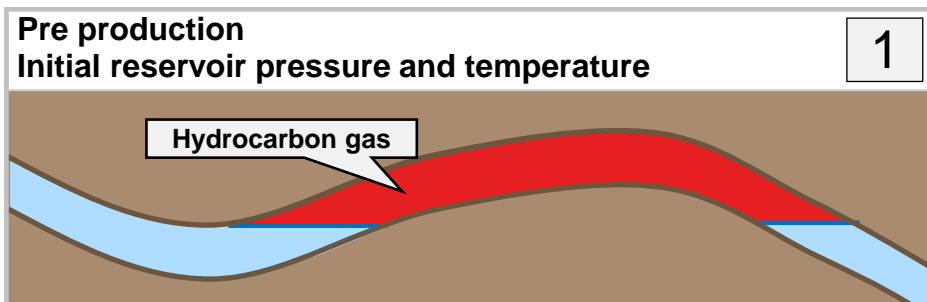
**The objective of this presentation is to describe a pragmatic approach for estimating storable quantities of CO<sub>2</sub> from experience gained on a variety of CCS projects in different parts of the world.**

(A matter of terminology: The author uses “storable quantities” to describe technical volumes and/or mass.  
“Capacity” is a defined term under SPE SRMS.)

### **Contents:**

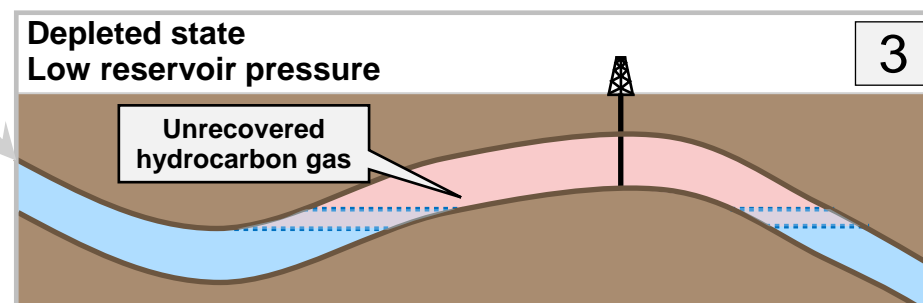
1. Depleted gas reservoirs.
2. Aquifers.
3. Concluding remarks.

## Conversion of a Depleted Gas Reservoir to CO<sub>2</sub> Storage

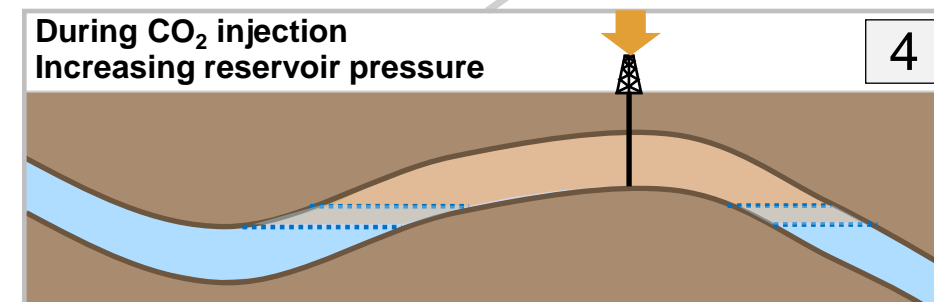
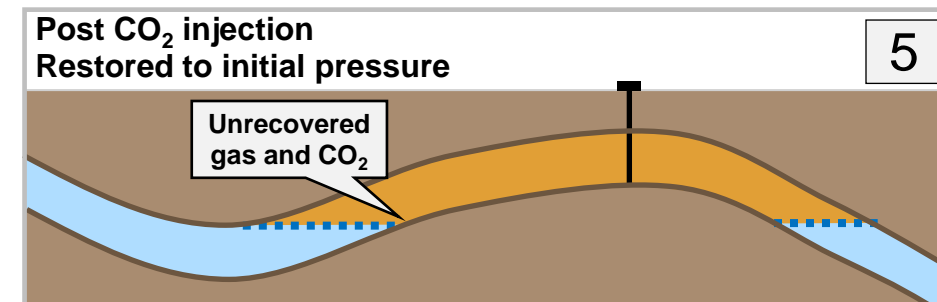


Two options:

1. Conventional geoscience estimation of pore volume.
2. Material balance.



CO<sub>2</sub> is injected into a depleted gas reservoir to restore pressure to its original level.



*We know how much came out so we should know how much can go back.*

Diagram modified from: CCUS deployment challenges and opportunities for the GCC. January 2022.  
A report prepared for the Oil and Gas Climate Initiative by AFRY & GaffneyCline.

## Depleted Gas Reservoirs- Material Balance

The storable quantity of CO<sub>2</sub> in a depleted gas reservoir is:

$$CO2Mi = \frac{Gp}{Ei} * \rho CO2i$$

Where:

*CO2Mi* mass of storable CO<sub>2</sub> if the reservoir is returned to its original pressure [metric tonnes].  
*Gp* volume of HC gas that has been produced at surface temperature and pressure [m<sup>3</sup>].  
*Ei* initial HC gas expansion factor [sm<sup>3</sup>/rm<sup>3</sup>].  
*ρCO2i* density of CO<sub>2</sub> at the original reservoir pressure [tonnes/m<sup>3</sup>].

Data requirements:

- Produced HC gas volume.
- HC gas PVT.
- Initial reservoir pressure.
- Initial reservoir temperature.

If storage pressure does not equal initial reservoir pressure then:

$$CO2Msto = \left( (GRV * NTG * \phi * (1 - Swir)) * \left( 1 - \frac{Ei}{Esto} \right) + \frac{Gp}{Esto} \right) * \rho CO2sto$$

Where:

*CO2Msto* mass of storable CO<sub>2</sub> if the reservoir is returned to any pressure [metric tonnes].  
*GRV, NTG, φ, Swir* gross rock volume [m<sup>3</sup>], net-to-gross ratio [fraction], porosity [fraction] and irreducible water saturation [fraction].  
*Esto* HC gas expansion factor at storage pressure [sm<sup>3</sup>/rm<sup>3</sup>].  
*ρCO2sto* density of CO<sub>2</sub> at storage pressure [tonnes/m<sup>3</sup>].

## Limitations of Material Balance

The material balance equations shown above do not account for:

**Decreases** ❖ Aquifer influx – *can be very large*.

- Heterogeneity – *can be large*.

❖ Condensate drop out – *can be large in some cases*.

❖ Impurities in injectant.

❖ Hysteresis in pore volume compressibility – *expected to be small*.

❖ To some extent could be accounted for by expanding material balance.

**Increases** • Utilisation of aquifer surrounding pool – *potentially large*.

❖ Dissolution in connate water – *small*.

**Other**

- Thermal effects.
- Mixing with remaining HC gas (mixing, banking, segregation).
- Vaporization of connate water (with salt precipitation).

Dynamic simulation can be used to address most of these points.

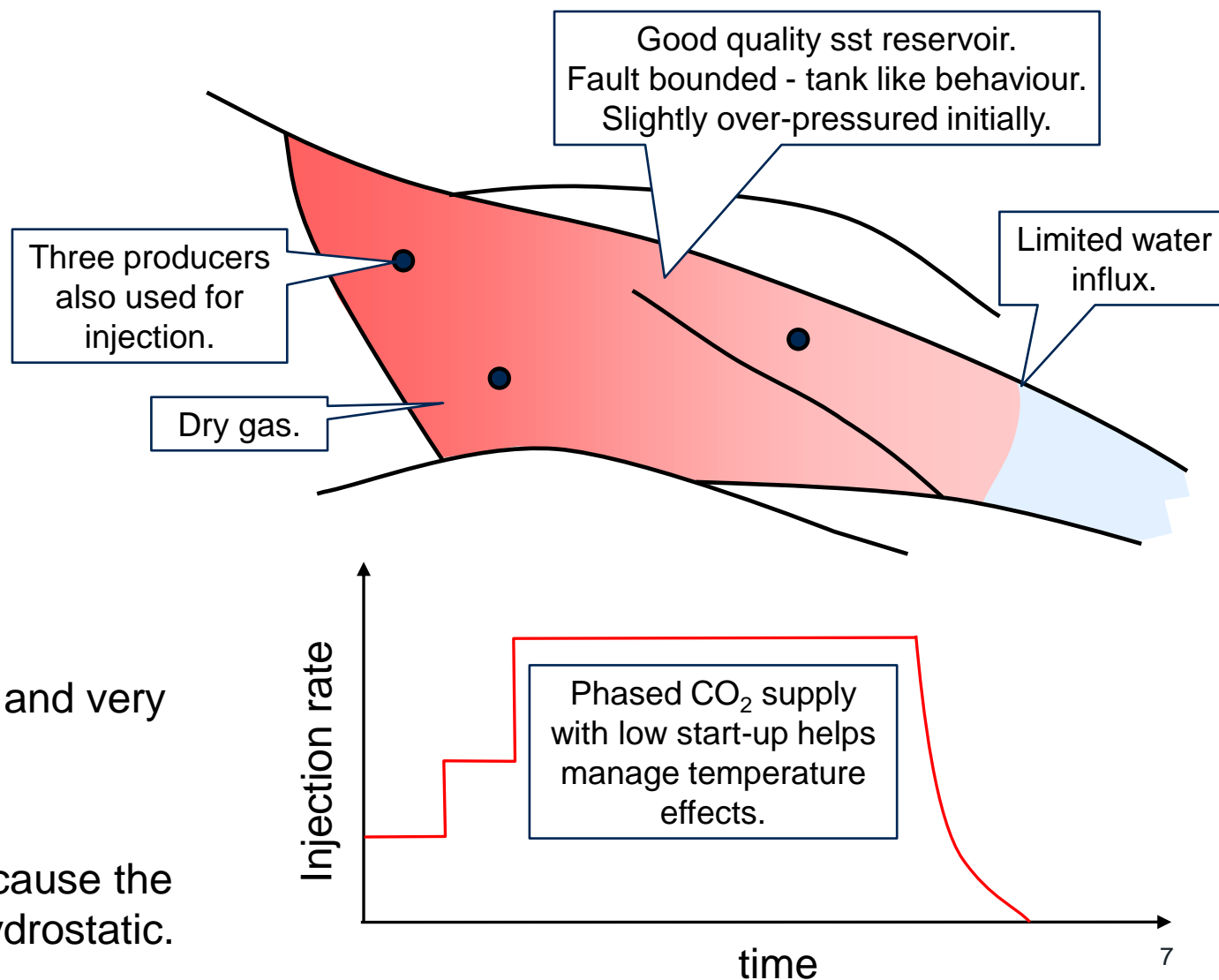


## Depleted Gas Reservoirs- Example 1

Item	Quantity
CO <sub>2</sub> density at initial P&T (t/m <sup>3</sup> )	<b>0.65</b>
Material balance CO <sub>2</sub> quantity (Mt)	<b>39.0</b>
Simulation CO <sub>2</sub> quantity (Mt)	<b>36.1</b>
Difference (%)	<b>-7%</b>

- Some water influx.
- Minor impurities in injectant.
- Some mixing with remaining HC gas.
- Tiny hysteresis effect.
- Good CCS storage candidate, but very deep and very depleted.

In reality: The storable quantity will be lower because the final pressure will not be permitted to exceed hydrostatic.

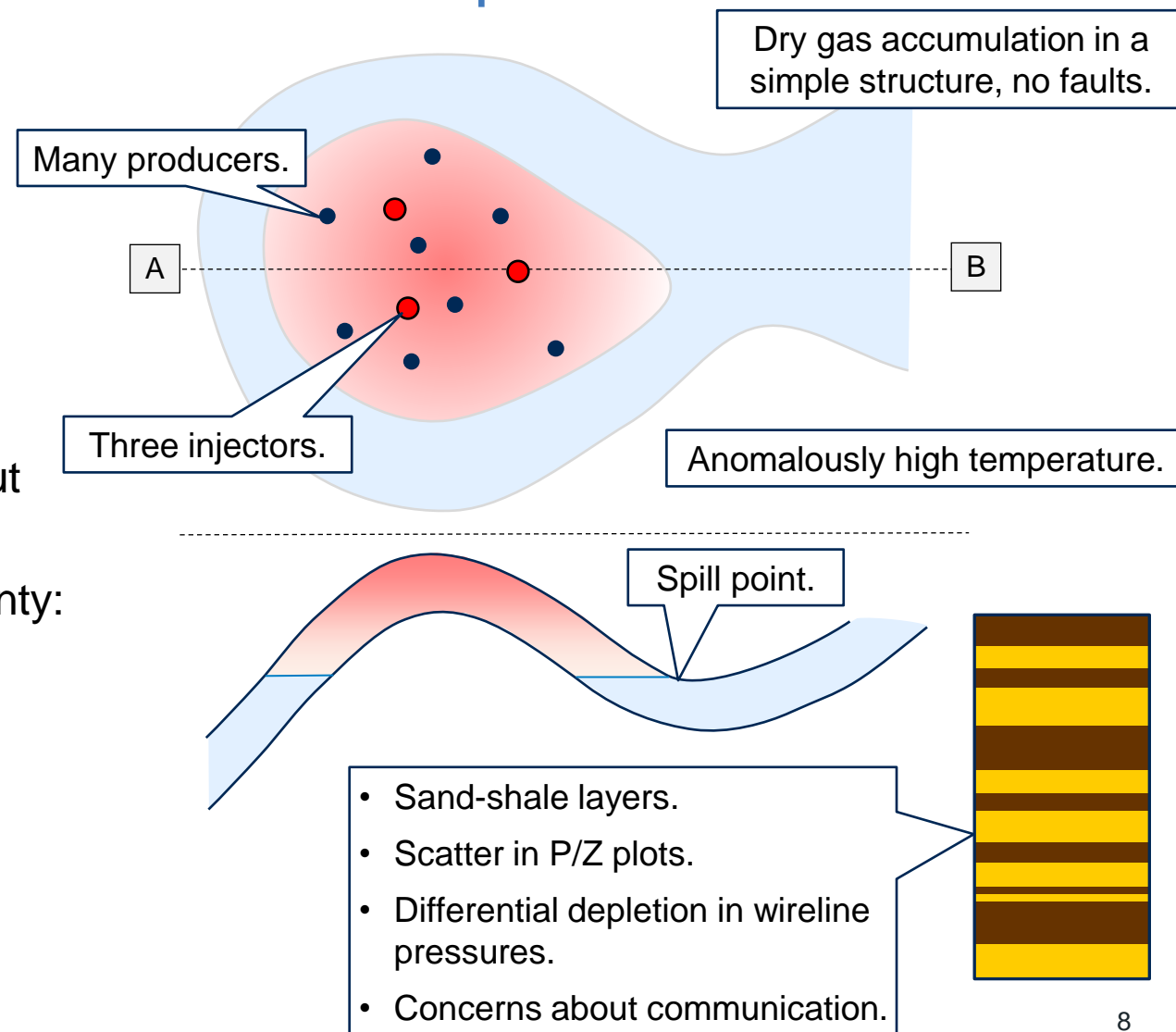


## Depleted Gas Reservoirs- Example 2

Item	Quantity
CO <sub>2</sub> density at initial P&T (t/m <sup>3</sup> )	<b>0.33</b>
Material balance CO <sub>2</sub> quantity (Mt)	<b>17.4</b>
Simulation CO <sub>2</sub> quantity (Mt)	<b>14.8</b>
Difference (%)	<b>-15%</b>

- History match for gas production is reasonable, but heterogeneity is a concern for CCS.
- Simulation sensitivities to define range of uncertainty:  
11.4 - 14.8 - 17.0 Mt (low, mid, high).

In reality: More wells can be drilled, and storable quantities could be higher if the aquifer can be used.



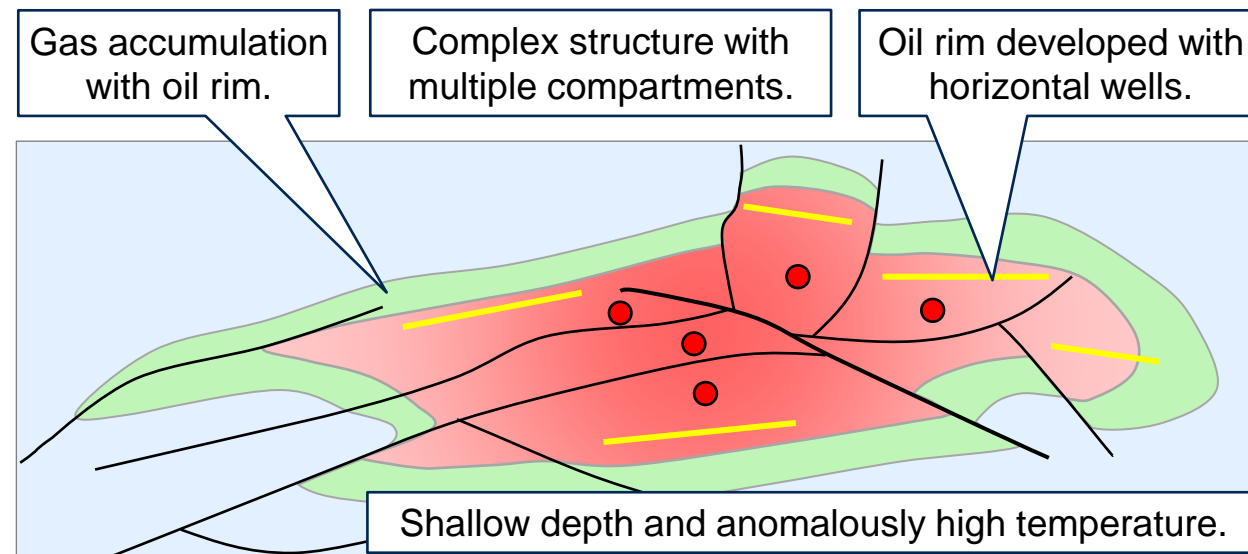


## Depleted Gas Reservoirs- Example 3

Item	Quantity
CO <sub>2</sub> density at initial P&T (t/m <sup>3</sup> )	<b>0.26</b>
Material balance CO <sub>2</sub> quantity (Mt)	<b>12.0</b>
Simulation CO <sub>2</sub> quantity (Mt)	<b>8.4</b>
Difference (%)	<b>-30%</b>

- Aquifer influx.
- Complex geology.
- Complex fluids.
- Very shallow depth and not much scope for increasing BHIP.

In reality: Not an optimal CO<sub>2</sub> storage site!



During production:

- Water encroached into oil.
- Oil encroached into gas.
- Gas blowdown.

Dynamic modelling:

- Good black oil history match of oil, water, gas, pressures.
- Converted to compositional formulation for CCS.

## Aquifers – The Volumetric Equation

The storable quantity of CO<sub>2</sub> in an aquifer “container” can be estimated with the following volumetric equation:

$$CO_2M_{sto} = PV * EF * \rho_{CO_2sto}$$

Where:

$CO_2M_{sto}$  mass of CO<sub>2</sub> that can be stored at the final storage pressure of the container [metric tonnes].

$PV$  pore volume of the storage container [m<sup>3</sup>].

$EF$  efficiency factor - defined here as the ratio of the volume of CO<sub>2</sub> injected into an aquifer, to the pore volume of the aquifer at the final storage pressure. (Think of it as the saturation of CO<sub>2</sub>).

$\rho_{CO_2sto}$  density of CO<sub>2</sub> at the final storage pressure of the container [tonnes/m<sup>3</sup>].

Two equally important considerations:

1. Mechanism for trapping and immobilization of CO<sub>2</sub>.
2. Nature of the container.

## Aquifers – Types of Storage

$$EF = (1 - S_{wir}) \text{ (max)}$$

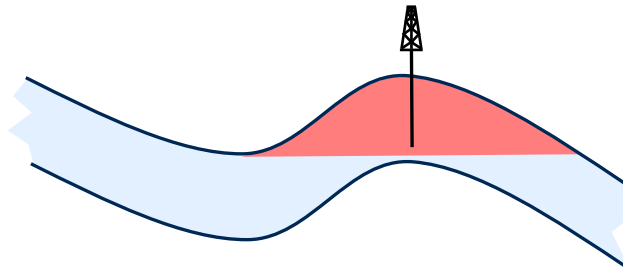
Expect EF ~ **30 to 40%**  
of structure PV.

Increase by spilling out.

Structural trapping

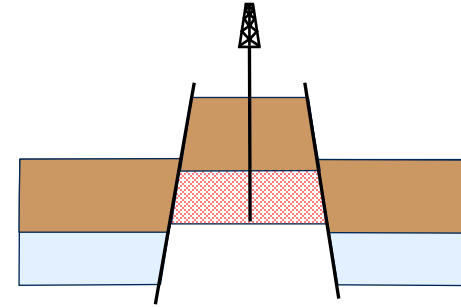
### Open Aquifer

CO<sub>2</sub> displaces water and is  
trapped in mobile state.  
Pressure dissipates.



### Confined Aquifer

CO<sub>2</sub> trapped in mobile state.  
Pressure increases.



Structural trapping

$$EF = C_t * \Delta P$$

Expect EF ~ **0.5%**

Increases with  
dissolution.

Increase with brine  
extraction.

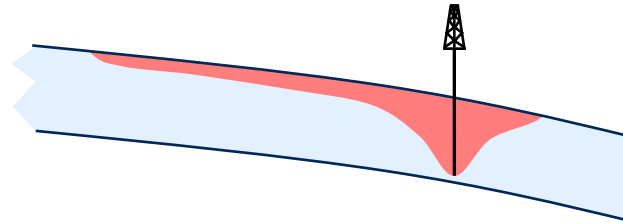
No simple expression  
for EF.

Reported EF ranges  
typically **0.5% to 7%,  
(or more).**

Definition of container  
determined by  
development plan.

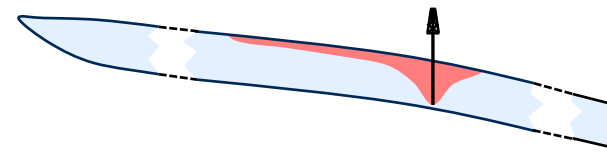
Solubility & residual

CO<sub>2</sub> forms a plume, becoming  
immobilised. Pressure dissipates.



### Open Aquifer

CO<sub>2</sub> forms a plume, becoming  
immobilised. Pressure increases.



### Confined Aquifer

Solubility & residual

Similar to adjacent case  
but pressure increases.

## Concluding Remarks

### Depleted gas reservoirs

- Analytical methods provide a good basis for benchmarking estimates of storable quantities.
- Dynamic model sensitivity analyses can provide insight into different processes.
- Dynamic models calibrated for production don't automatically provide reliable CCS forecasts.
- Storable quantities can be estimated accurately, usually with a relative low range of uncertainty.

### Aquifers

- Analogues are still too sparse to provide a reliable basis for estimating storable quantities.
- Dynamic modelling is usually essential, supported by analytical end-points.
- For large open aquifers in particular storable quantities are determined by the development plan rather than by some “inherent” efficiency factor.

**Depleted gas reservoirs offer relative low risk opportunities, but in the long run aquifers will provide the storage space that we need to make a material difference to CO<sub>2</sub> emissions.**

# Thank you for your attention

Shane Hattingh

[shane.hattingh@gaffneycline.com](mailto:shane.hattingh@gaffneycline.com)

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