

# CHEMICAL PROCESS CALCULATIONS

**(Chemical Reaction Stoichiometry)**

Lecture # 12: October 05, 2023

# Stoichiometry

- Proportion of chemical species that combine with one another
- Relative number of molecules/moles of reactants and products in a reaction
- Number of atoms of any atomic species on both sides of a reaction must be same
- Stoichiometric coefficients
- Stoichiometric ratio

# Limiting & Excess Reactant

- Limiting reactant
- Excess reactant
- Fractional excess
- Percentage excess
- Fractional conversion

# Limiting & Excess Reactant



20 kmol acetylene		After some time
50 kmol hydrogen		30 kmol hydrogen
50 kmol ethane		reacted

$$n_{H_2} = (n_{H_2})_0 - 2\xi$$

$$n_{C_2H_2} = (n_{C_2H_2})_0 - \xi$$

$$n_{C_2H_6} = (n_{C_2H_6})_0 + \xi$$

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$$v_{C_2H_2} = -1$$

$$v_{H_2} = -2$$

$$v_{C_2H_6} = +1$$

# Limiting & Excess Reactant

$$n_{H_2} = (n_{H_2})_0 - 2\xi$$

$$n_{C_2H_2} = (n_{C_2H_2})_0 - \xi$$

$$n_{C_2H_6} = (n_{C_2H_6})_0 + \xi$$

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$$v_{C_2H_2} = -1$$

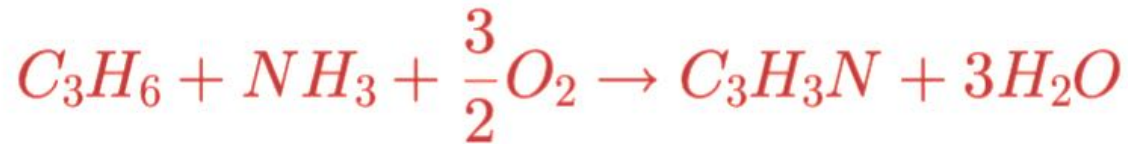
$$v_{H_2} = -2$$

$$v_{C_2H_6} = +1$$

$$n_i = n_{i0} + v_i \xi$$

$\xi$  = Extent of reaction

# Limiting & Excess Reactant



Mole composition:

10% propylene, 12% ammonia, 78% air

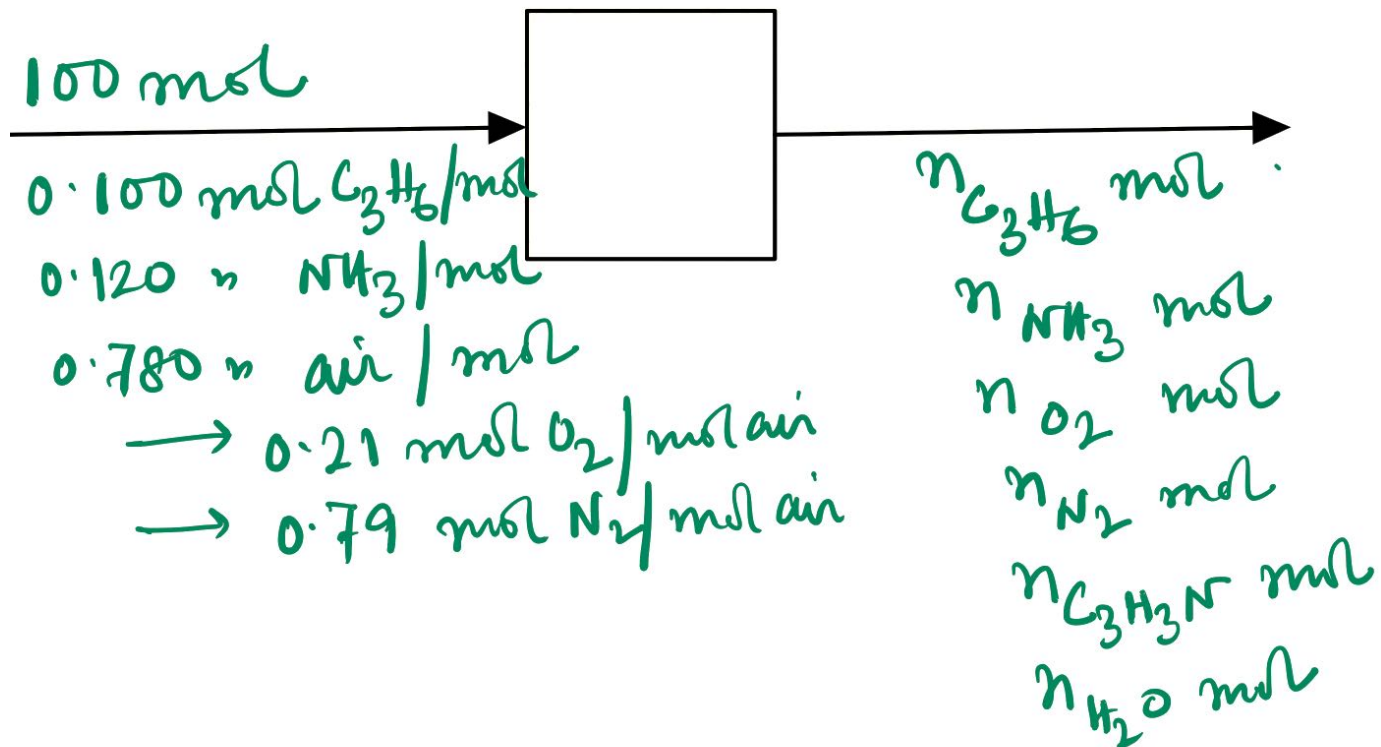
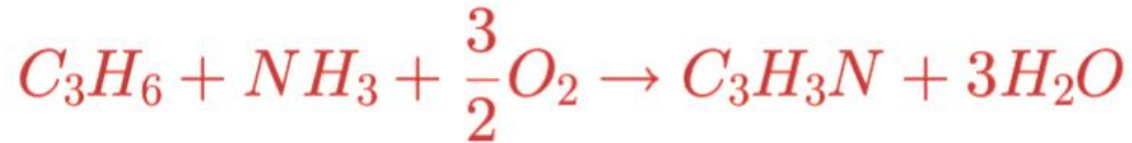
Fractional conversion:

30% of the limiting reactant

% excess of other reactants

Molar composition of product gas

# Limiting & Excess Reactant



100 mol

0.100 mol  $C_3H_6$  / mol

0.120 "  $NH_3$  / mol

0.780 " air / mol

→ 0.21 mol  $O_2$  / mol air

→ 0.79 mol  $N_2$  / mol air

$n_{C_3H_6}$  mol

$n_{NH_3}$  mol

$n_{O_2}$  mol

$n_{N_2}$  mol

$n_{C_3H_3N}$  mol

$n_{H_2O}$  mol

$$(n_{C_3H_6})_0 = 10.0 \text{ mol}$$

$$(n_{NH_3})_0 = 12.0 \text{ mol}$$

$$(n_{O_2})_0 = 78.0 \times 0.210 = 16.4 \text{ mol}$$

$$(n_{NH_3} / n_{C_3H_6})_0 = \frac{12.0}{10.0} = 1.20$$

$$(n_{NH_3} / n_{C_3H_6})_{St} = 1/1 = 1$$

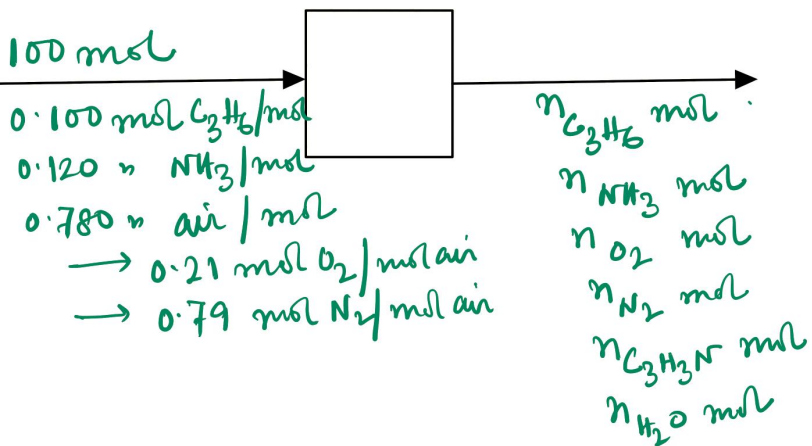
⇒  $NH_3$  is in excess.

$$(n_{O_2} / n_{C_3H_6})_0 = 16.4 / 10.0 = 1.64$$

$$(n_{O_2} / n_{C_3H_6})_{St} = 1.5/1 = 1.5$$

⇒  $O_2$  is in excess.





$$\% \text{ excess } NH_3 = \frac{(n_{NH_3})_0 - (n_{NH_3})_{St}}{(n_{NH_3})_{St}} \times 100\%$$

$$= \frac{12.0 - 10.0}{10.0} \times 100\% = 20\%$$

$$\% \text{ excess } O_2 = \frac{16.4 - 15.0}{15.0} \times 100\% = 9.33\%$$

$$(n_{NH_3})_{St} = 10.0 \text{ mol } C_3H_6 \times \frac{1 \text{ mol } NH_3}{1 \text{ mol } C_3H_6}$$

$$= 10.0 \text{ mol } NH_3$$

$$(n_{O_2})_{St} = 10.0 \text{ mol } C_3H_6 \times \frac{1.5 \text{ mol } O_2}{1 \text{ mol } C_3H_6}$$

$$= 15.0 \text{ mol } O_2$$

100 mol

0.100 mol  $C_3H_6$  / mol

0.120 "  $NH_3$  / mol

0.780 " air / mol

→ 0.21 mol  $O_2$  / mol air

→ 0.79 mol  $N_2$  / mol air

$n_{C_3H_6}$  mol

$n_{NH_3}$  mol

$n_{O_2}$  mol

$n_{N_2}$  mol

$n_{C_3H_3N}$  mol

$n_{H_2O}$  mol

$$(n_{C_3H_6})_{out} = 0.700 \times (n_{C_3H_6})_0 = 7.0 \text{ mol}$$

$$(n_{C_3H_6})_{out} = 10.0 - \xi$$

$$\Rightarrow \xi = 3.0 \text{ mol}$$

$$n_{NH_3} = 12.0 - \xi$$

$$n_{C_3H_3N} = \xi$$

$$n_{O_2} = 16.4 - 1.5 \xi$$

$$n_{H_2O} = 3\xi$$

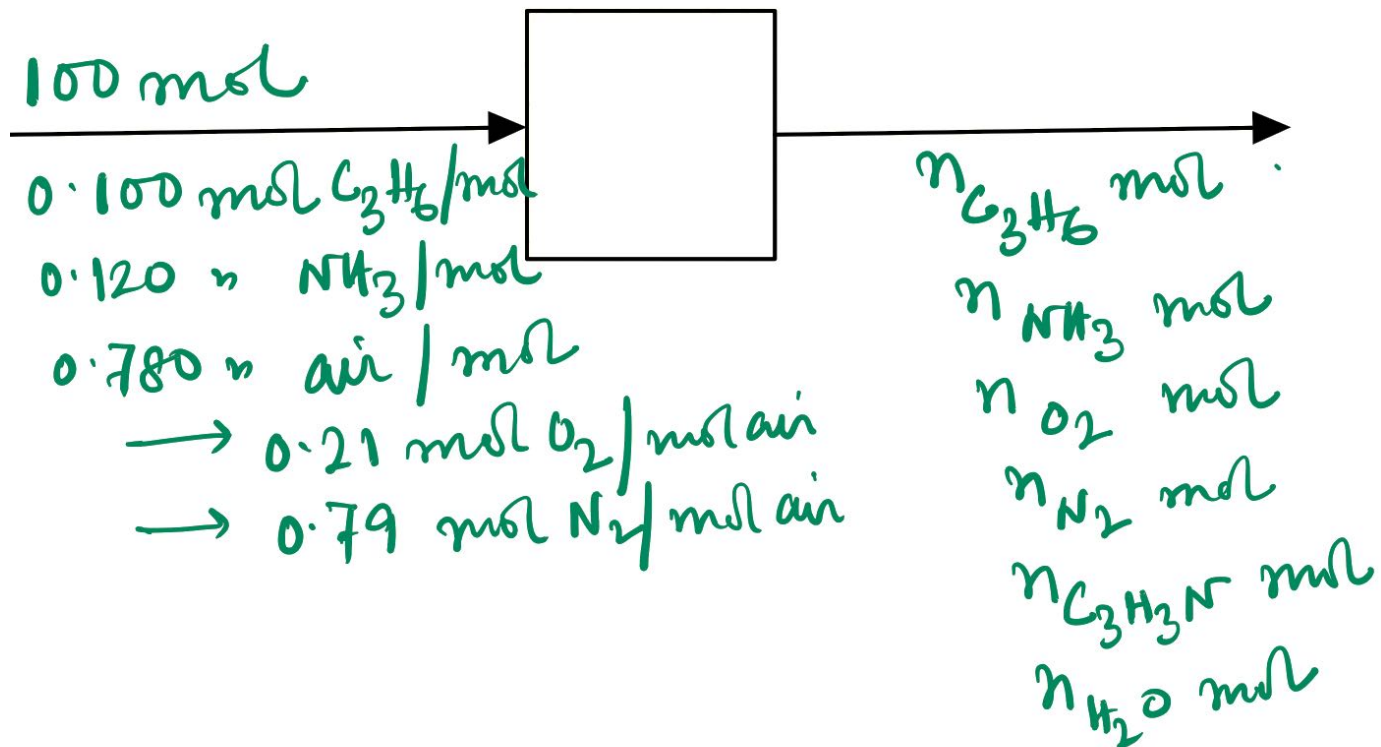
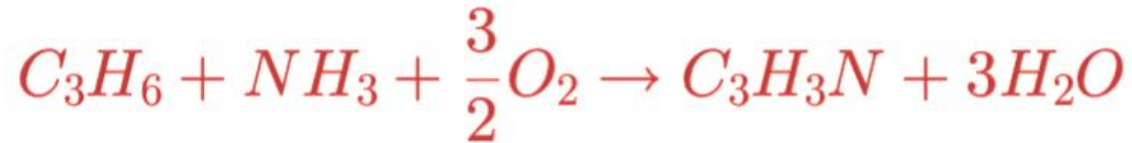
$$n_{N_2} = (n_{N_2})_0$$

# CHEMICAL PROCESS CALCULATIONS

**(Chemical Reaction Stoichiometry)**

Lecture # 13: October 09, 2023

# Limiting & Excess Reactant



100 mol

0.100 mol  $C_3H_6$  / mol

0.120 "  $NH_3$  / mol

0.780 " air / mol

→ 0.21 mol  $O_2$  / mol air

→ 0.79 mol  $N_2$  / mol air

$n_{C_3H_6}$  mol

$n_{NH_3}$  mol

$n_{O_2}$  mol

$n_{N_2}$  mol

$n_{C_3H_3N}$  mol

$n_{H_2O}$  mol

$$(n_{C_3H_6})_0 = 10.0 \text{ mol}$$

$$(n_{NH_3})_0 = 12.0 \text{ mol}$$

$$(n_{O_2})_0 = 78.0 \times 0.210 = 16.4 \text{ mol}$$

$$(n_{NH_3} / n_{C_3H_6})_0 = \frac{12.0}{10.0} = 1.20$$

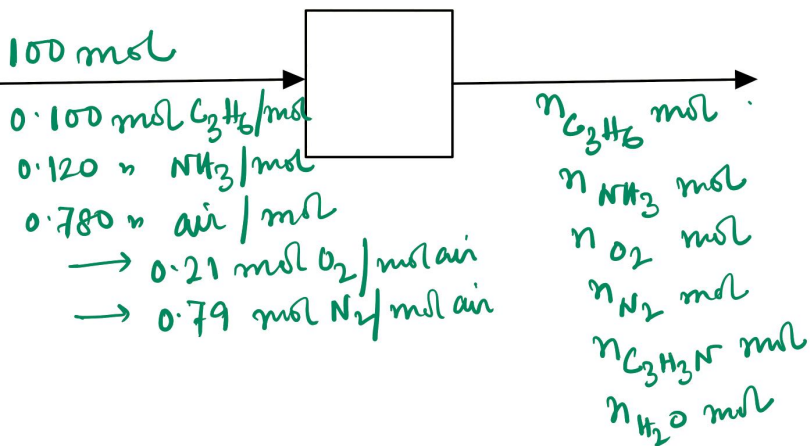
$$(n_{NH_3} / n_{C_3H_6})_{St} = 1/1 = 1$$

⇒  $NH_3$  is in excess.

$$(n_{O_2} / n_{C_3H_6})_0 = 16.4 / 10.0 = 1.64$$

$$(n_{O_2} / n_{C_3H_6})_{St} = 1.5/1 = 1.5$$

⇒  $O_2$  is in excess.



$$\% \text{ excess } NH_3 = \frac{(n_{NH_3})_0 - (n_{NH_3})_{St}}{(n_{NH_3})_{St}} \times 100\%$$

$$= \frac{12.0 - 10.0}{10.0} \times 100\% = 20\%$$

$$\% \text{ excess } O_2 = \frac{16.4 - 15.0}{15.0} \times 100\% = 9.33\%$$

$$(n_{NH_3})_{St} = 10.0 \text{ mol } C_3H_6 \times \frac{1 \text{ mol } NH_3}{1 \text{ mol } C_3H_6}$$

$$= 10.0 \text{ mol } NH_3$$

$$(n_{O_2})_{St} = 10.0 \text{ mol } C_3H_6 \times \frac{1.5 \text{ mol } O_2}{1 \text{ mol } C_3H_6}$$

$$= 15.0 \text{ mol } O_2$$

100 mol

0.100 mol  $C_3H_6$  / mol

0.120 "  $NH_3$  / mol

0.780 " air / mol

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$n_{C_3H_6}$  mol

$n_{NH_3}$  mol

$n_{O_2}$  mol

$n_{N_2}$  mol

$n_{C_3H_3N}$  mol

$n_{H_2O}$  mol

$$(n_{C_3H_6})_{out} = 0.700 \times (n_{C_3H_6})_0 = 7.0 \text{ mol}$$

$$(n_{C_3H_6})_{out} = 10.0 - \xi$$

$$\Rightarrow \xi = 3.0 \text{ mol}$$

$$n_{NH_3} = 12.0 - \xi$$

$$n_{C_3H_3N} = \xi$$

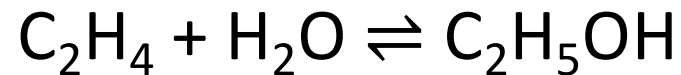
$$n_{O_2} = 16.4 - 1.5 \xi$$

$$n_{H_2O} = 3\xi$$

$$n_{N_2} = (n_{N_2})_0$$

# Chemical Equilibrium

- Equilibrium composition of the reaction mixture
- Time to reach the onset of equilibrium
- Irreversible reaction
- Reversible reaction





# Chemical Equilibrium



$$\frac{y_{\text{CO}_2} y_{\text{H}_2}}{y_{\text{CO}} y_{\text{H}_2\text{O}}} = K(T)$$

At $T = 1105 \text{ K}$ $K = 1.00$
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Feed:  $\begin{cases} 1 \text{ mol CO} \\ 2 \text{ mol H}_2\text{O} \end{cases}$

Fractional conversion

Calculate  
equilibrium  
composition.

# Chemical Equilibrium

$$n_{\text{CO}} = 1.00 - \xi_e$$

$$n_{\text{H}_2\text{O}} = 2.00 - \xi_e$$

$$n_{\text{CO}_2} = \xi_e$$

$$n_{\text{H}_2} = \xi_e$$

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$$n_t = 3.00$$

$$y_{\text{CO}} = (1.00 - \xi_e) / 3.00$$

$$y_{\text{H}_2\text{O}} = (2.00 - \xi_e) / 3.00$$

$$y_{\text{CO}_2} = \xi_e / 3.00$$

$$y_{\text{H}_2} = \xi_e / 3.00$$

# Chemical Equilibrium

$$\frac{y_{\text{CO}_2} y_{\text{H}_2}}{y_{\text{CO}} y_{\text{H}_2\text{O}}} = \frac{\xi_e^2}{(1.00 - \xi_e)(2.00 - \xi_e)} = 1.00$$

$$\Rightarrow \xi = 0.667$$

$$y_{\text{CO}} = 0.111$$

$$y_{\text{H}_2\text{O}} = 0.444$$

$$y_{\text{CO}_2} = 0.222$$

$$y_{\text{H}_2} = 0.222$$

||

# Chemical Equilibrium

$$n_{\text{CO}} = (1.00 - 0.667) \text{ mol} = 0.333 \text{ mol}$$

$$f_{\text{CO}} = \frac{(1.00 - 0.333) \text{ CO reacted}}{1.00 \text{ mol CO fed}} = \underline{\underline{0.667}}$$

The reaction between ethylene and hydrogen bromide to form ethyl bromide is carried out in a continuous reactor. The product stream is analyzed and found to contain 51.7 mole% C<sub>2</sub>H<sub>5</sub>Br and 17.3% HBr. The feed to the reactor contains only ethylene and hydrogen bromide. Calculate the fractional conversion of the limiting reactant and the percentage by which the other reactant is in excess. If the molar flow rate of the feed stream is 165 mol/s, what is the extent of reaction?



# CHEMICAL PROCESS CALCULATIONS

**(Chemical Reaction Stoichiometry)**

Lecture # 14: October 12, 2023

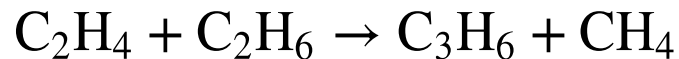
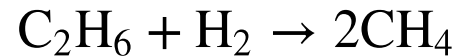
# Multiple Reactions, Yield, and Selectivity

- Desired product yield
- Desired product purity
- Yield and Selectivity

$$\text{Yield} = \frac{\text{moles of desired product formed}}{\text{moles that would be formed if there were no side reactions and the limiting reactant were consumed completely}} \times 100\%$$

$$\text{Selectivity} = \frac{\text{moles of desired product formed}}{\text{moles of undesired product formed}}$$

# Multiple Reactions, Yield, and Selectivity



$$\text{Yield} = \frac{(n_{\text{C}_2\text{H}_4})_{\text{gen}}}{(v_{\text{C}_2\text{H}_4} / v_{\text{C}_2\text{H}_6})(n_{\text{C}_2\text{H}_6})_{\text{input}}} \times 100\%$$

$$\text{Selectivity} = \frac{(n_{\text{C}_2\text{H}_4})_{\text{gen}}}{(n_{\text{CH}_4})_{\text{gen}}}$$

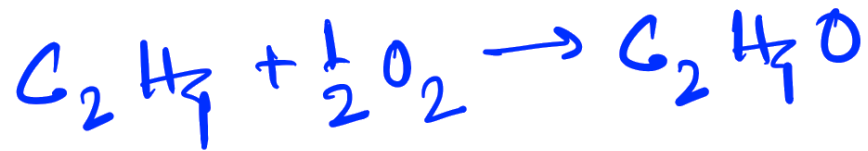
**Yield**  $\Rightarrow$  moles of desired product divided  
by either moles of reactant fed or moles of  
reactant consumed in the reactor



# Multiple Reactions, Yield, and Selectivity

Single reaction:  $n_i = n_{i0} + \nu_i \xi$

Multiple reaction:  $n_i = n_{i0} + \sum_j \nu_{ij} \xi_j$



# Multiple Reactions, Yield, and Selectivity

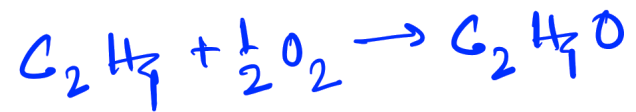
$$(n_{C_2H_2})_{out} = (n_{C_2H_2})_0 - \xi_1 - \xi_2$$

$$(n_{O_2})_{out} = (n_{O_2})_0 - 0.5\xi_1 - 3\xi_2$$

$$(n_{C_2H_3O})_{out} = (n_{C_2H_3O})_0 + \xi_1$$

$$(n_{CO_2})_{out} = (n_{CO_2})_0 + 2\xi_2$$

$$(n_{H_2O})_{out} = (n_{H_2O})_0 + 2\xi_2$$



# Multiple Reactions, Yield, and Selectivity



Feed: 85.0 mole% ethane and the balance inert

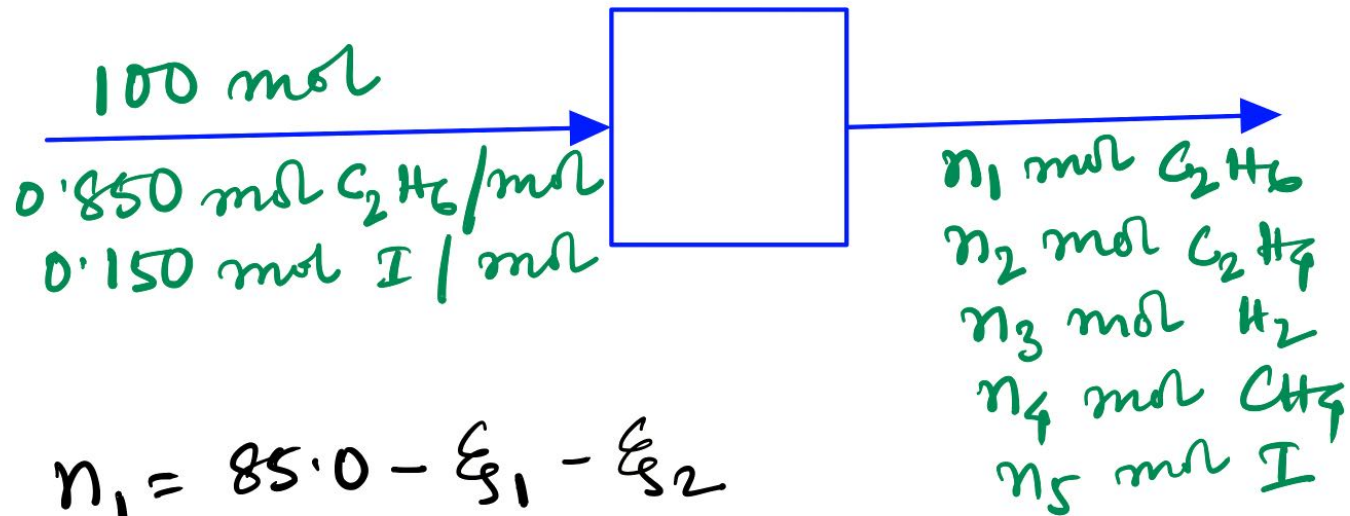
Fractional conversion of ethane = 0.501

Fractional yield of ethylene = 0.471

Calculate

- molar composition of the product gas
- selectivity of ethylene to methane production

# Multiple Reactions, Yield, and Selectivity



$$n_1 = 85.0 - \xi_1 - \xi_2$$

$$n_2 = \xi_1$$

$$n_3 = \xi_1 - \xi_2$$

$$n_4 = 2\xi_2$$

$$n_5 = 15.0$$

# Multiple Reactions, Yield, and Selectivity

C<sub>2</sub>H<sub>6</sub>:

Fractional conversion: 0.501

$$(1 - 0.501) \times 85.0 = n_1$$

$$\Rightarrow n_1 = 42.4 = 85.0 - \xi_1 - \xi_2$$

C<sub>2</sub>H<sub>4</sub>:

Fractional yield: 0.471

$$0.471 \times 85.0 = n_2$$

$$\Rightarrow n_2 = 40.0 = \xi_1$$

$$\Rightarrow \xi_2 = 2.6$$

# Multiple Reactions, Yield, and Selectivity

$$n_3 = \xi_1 - \xi_2 = 37.4$$

$$n_4 = 2\xi_2 = 5.2$$

$$n_5 = 15.0$$

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$$n_1 = 42.4$$

$$n_2 = 40.0$$

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$$n_t = 140.0$$

Product

$$C_2H_6 - 30.3\%$$

$$C_2H_4 - 28.6\%$$

$$H_2 - 26.7\%$$

$$CH_3 - 3.7\%$$

$$I - 10.7\%$$

Selectivity

$$= \frac{40.0 \text{ mol } C_2H_4}{5.2 \text{ mol } CH_3} = 7.69 \text{ mol } C_2H_4 / \text{mol } CH_3$$

# Reactive system balance

- (a) molecular species balances (similar to nonreactive systems)
  - (b) atomic species balances
  - (c) extents of reaction
- 
- independent equations
  - independent species
  - independent chemical reactions