Basic Equations in Integral Form for a Control Volume

Fox and McDonald Ch - 4 N = Arbitrary extensive property of a system

$$N|_{SYSEM} = \int_{Mass(System)} \eta \, dm = \int_{V-(System)} \eta \rho \, dV$$

 η = Corresponding intensive property

Basic Equations in Integral Form for a CV

Conservation of Mass

Conservation of Momentum

Relation of System Derivatives to the Control Volume Formulation

$$\left. \frac{\partial N}{\partial t} \right|_{SYSEM} = \left. \frac{\partial}{\partial t} \int_{CV} \eta \rho d\Psi + \int_{CS} \eta \rho \vec{V} . d\vec{A} \right. \qquad \overrightarrow{V} \text{ is measured relative to the CV}$$

$$\frac{\partial N}{\partial t}\Big|_{\text{SYSEM}}$$
 = Total rate of change of any arbitrary extensive property of the system

$$\frac{\partial}{\partial t} \int_{CV} \eta \rho dV$$
 = Time rate of change of the arbitrary extensive property within the CV

$$\int_{CS} \eta \rho \vec{V} \cdot d\vec{A} = \text{Net rate of efflux of the extensive property, N, through the control surface}$$

Conservation of Mass N = Mass, $\eta = 1$

$$\left. \frac{\partial N}{\partial t} \right|_{SYSEM} = \left. \frac{\partial}{\partial t} \int_{CV} \eta \rho dV + \int_{CS} \eta \rho \vec{V} . d\vec{A} \right.$$

$$0 = \frac{\partial}{\partial t} \int_{CV} \rho dV + \int_{CS} \rho \vec{V} \cdot d\vec{A}$$

Incompressible Fluid

$$0 = \int_{CS} \rho \vec{V} . d\vec{A}$$

The size of the CV is fixed

$$\int_{CS} \rho \overrightarrow{V} \cdot d\overrightarrow{A} = \pm \left| \rho_n V_n A_n \right|$$

When uniform flow at section n is assumed

Momentum Equation for Inertial CV, N = Momentum, $\eta = Velocity$

$$\left. \frac{\partial N}{\partial t} \right|_{SYSEM} = \left. \frac{\partial}{\partial t} \int_{CV} \eta \rho dV + \int_{CS} \eta \rho \vec{V} \cdot d\vec{A} \right.$$

$$\vec{F} = \vec{F}_S + \vec{F}_B = \frac{\partial}{\partial t} \int_{CV} \vec{V} \rho dV + \int_{CS} \vec{V} \rho \vec{V} \cdot d\vec{A}$$

$$\vec{F}_B = \int_{CV} \vec{B} \rho dV \qquad \vec{F}_S = \int_A - p \, d\vec{A}$$

Scalar Component

$$F_{x} = F_{Sx} + F_{Bx} = \frac{\partial}{\partial t} \int_{CV} u \rho \, dV + \int_{CS} u \rho \, \overrightarrow{V} . \, d\overrightarrow{A}$$

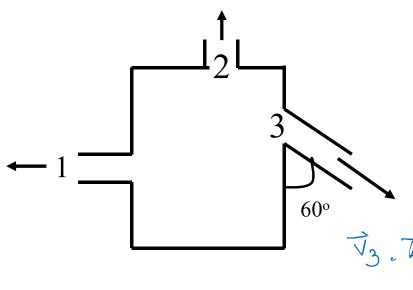
1. To determine the sign of

$$\rho \vec{V} \cdot d\vec{A} = \pm |\rho V dA \cos \alpha|$$

2. To determine the sign of each velocity component

$$u \rho \overrightarrow{V} \cdot d\overrightarrow{A} = u \{ \pm |\rho V dA \cos \alpha | \}$$

Steady Incompressible Flow



Fluid with $\rho = 1050$ kg/m3 is flowing through the box, $A_1 = 0.05$ m², $A_2 = 0.01$ m², $A_3 = 0.06$ m²

$$\vec{V}_1 = 4 \hat{\imath} \ m/s \quad \vec{V}_2 = -8 \hat{\jmath} \ m/s \quad \text{Find V3}$$

$$\vec{\nabla}_3 \cdot \vec{A}_3 = -\vec{\nabla}_1 \cdot \vec{A}_1 - \vec{\nabla}_2 \cdot \vec{A}_2$$

$$=-4^{\circ}.0.05(-^{\circ})-(-8^{\circ}).0.01^{\circ}$$

$$\nabla_3 \cdot \overline{A}_3 = 0.28 \, \text{m}^3/\text{s} \cdot 5 \cdot \text{nce} \, \nabla_3 \, \overline{A}_3 > 0, \text{ flow at}$$
Section 3 is out of $CV \cdot V_3 = \frac{1}{A_3} \times 0.28 \, \text{m}^3/\text{s} = 4.67 \, \text{m/s}$
From geometry $\nabla_3 = V_3 \sin \theta \hat{\iota} - V_3 \cos \theta \hat{\delta} = 4.04 \hat{\iota} - 2.34 \hat{\delta}$

Find the net rate of efflux of momentum through the CV

The net rate of momentum efflux is given by

$$= \sqrt{1 + \sqrt{1 + \sqrt{2}}} \sqrt{1 + \sqrt{2}} \sqrt{1 + \sqrt{2}} \sqrt{1 + \sqrt{3}} \sqrt{1 +$$

Water exits a pipe from a series of 109 holes drilled into the side as shown in the figure, along with the coordinate systems. The pressure at the inlet section is 35 kPa. Calculate the forces required to hold the spray pipe in place. The pipe and the water ($\rho = 10^3 \text{ kg/m}^3$) it contains weighs 5 kg.

$$F_{x} = F_{Sx} + F_{Bx} = \frac{\partial}{\partial t} \int_{CV} u \rho \, dV + \int_{CS} u \rho \, \vec{V} \cdot d\vec{A} \qquad F_{y} = F_{Sy} + F_{By} = \frac{\partial}{\partial t} \int_{CV} v \rho \, dV + \int_{CS} v \rho \, \vec{V} \cdot d\vec{A}$$

$$F_{y} = F_{Sy} + F_{By} = \frac{\partial}{\partial t} \int_{CV} v \rho \, dV + \int_{CS} v \rho \, \overrightarrow{V} \cdot d\overrightarrow{A}$$

$$A_{1m} = \frac{\pi}{4} (0.175)^{2} = 2.404 \times 10^{2} m^{2}$$

$$A_{0uT} / hole = \frac{\pi}{4} (0.015)^{2} = 1.766 \times 10^{-4} m^{2}$$

$$V_{1m} = 8 m / h$$

$$A_{0uT} (Total) = 109 \times 1.766 \times 10^{-4} m^{2}$$

$$= 1.925 \times 10^{-2} m^{2}$$

$$= 1.925 \times 10^{-2} m^{2}$$

$$V_{0uT} = 9.98 m / s$$

$$V_{0uT} = 9.98$$

$$R_{x} = -1000 \times 1092 \times 10^{-1} \times 8 - 35 \times 10^{3} \times 2.404 \times 10^{-2}$$

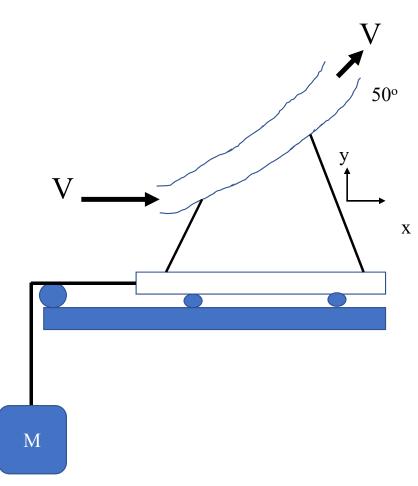
$$R_{x} = -2377 \text{ N}$$
FOR Y directⁿ

$$R_{y} # P_{2} g \text{ Aout} - Pg V = -PQ V_{1} + PQ V_{2} \gamma$$

$$= 0$$

$$R_{y} = PQ V_{2} + Pg V$$

$$R_{y} = -1867 \text{ N}$$



Vane on a frictionless platform with a block of mass, M, attached to it

$$V = 15 \text{ m/s}, A = 0.05 \text{ m}^2, \theta = 50^{\circ}$$

Find the mass, M, Needed to hold the cart stationary

$$F_{x} = F_{Sx} + F_{Bx} = \frac{\partial}{\partial t} \int_{CV} u \rho \, dV + \int_{CS} u \rho \, \overrightarrow{V} . \, d\overrightarrow{A}$$

$$F_{x} = F_{Sx} + F_{Bx} = \frac{\partial}{\partial t} \int_{CV} u \rho \, d\Psi + \int_{CS} u \rho \, \overrightarrow{V} . \, d\overrightarrow{A}$$

$$-Mg = u_1 \left\{ -\left| \rho_1 V_1 A_1 \right| \right\} + u_2 \left\{ +\left| \rho_2 V_2 A_2 \right| \right\}$$
$$u_1 = V \qquad u_2 = V \cos \theta$$

$$M = \rho V^2 A (1 - \cos \theta) / g$$

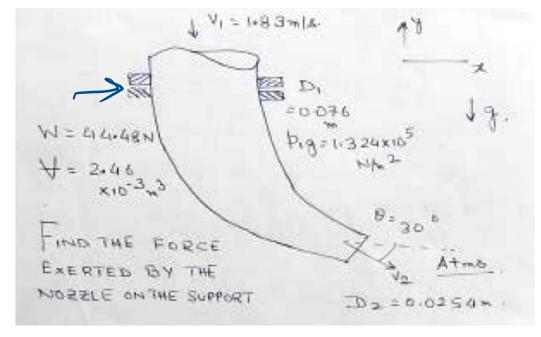
Curved nozzle Assembly, discharging water to the atmosphere, as shown in the figure

Given:

$$W = 44.48N$$
, $p_{1g} = 1.324x10^5 N/m^2$, $V = 2.46x10^{-3}m^3$, $V_1 = 1.83 m/s$, $D_1 = 0.076 m$, $D_2 = 0.0254 m$

The angle at the exit is 30° with the horizontal.

Calculate the reaction force exerted by the nozzle on the coupling of the inlet pipe.



$$F_{x} = F_{Sx} + F_{Bx} = \frac{\partial}{\partial t} \int_{CV} u \rho \, dV + \int_{CS} u \rho \, \overrightarrow{V} . \, d\overrightarrow{A}$$

$$R_{\chi} = \chi_1 \left[- | P v_1 A_1 | \right] + \chi_2 \left[+ | P v_2 A_2 | \right]$$

$$= 0$$

$$| R_{x} = P V_2 A_2 COS \Theta | = 117.03 N$$

$$Ry - P_{1}gA_{1} - W - PgH = V_{1}S - |PV_{1}A_{1}||_{1}V_{2}S_{1}$$

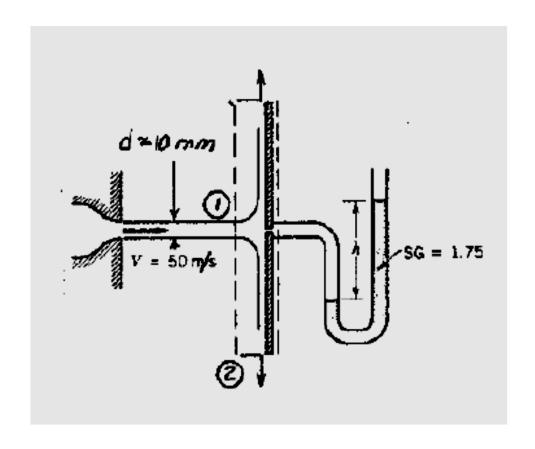
+ $|PV_{2}A_{2}||_{1}$
- $|=616N|$ $V_{1}=-V_{1}$, $V_{2}=-V_{2}S_{1}M_{2}$

1 VI = 1+83m	to a
5253	D,
M= 44.48N / p	19:1324×105
X10-3,13	8:30 6
EXERTED BY THE	No Atmo
NOZZLE ON THE SUPPORT	ID 2 = 0.02 50 x

A horizontal, axi-symmetric jet of air ($\rho = 1.23$ Kg/m³) with a diameter of 10 mm strikes the centre of a vertical disk of 200 mm diameter. The jet speed is 50 m/s at the nozzle exit.

There is a small hole at the centre of the disk, where the air jet strikes and a manometer with a manometric liquid of specific gravity equal to 1.75.

Calculate (i) the deflection, h, of the manometer and (ii) the force exerted by the jet on the disk.



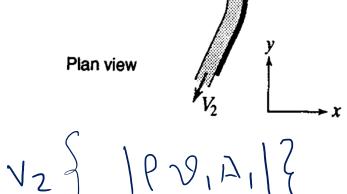
Pitot Tube

$$F_{x} = F_{Sx} + F_{Bx} = \frac{\partial}{\partial t} \int_{CV} u \rho \, dV + \int_{CS} u \rho \, \overrightarrow{V} . \, d\overrightarrow{A}$$

$$R_{x} = U_{1} \left\{ \begin{array}{l} - P \vee A \\ = \end{array} \right\} + \left\{ \begin{array}{l} + \sqrt{2} + P \vee A \\ = \end{array} \right\}$$

$$R_{x} = -P \mathcal{I}^{2} A = -00024 N$$

Refer to the given figure where a water jet is forced to change its direction because of the presence of a blade in its path. Assume that friction is negligible, that $\theta = 115^{\circ}$, and that the water jet has a velocity of 25 m/s and a diameter of 40 mm. Find (a) the component of the force acting on the blade (the portion shown by the dark line atthe bend) in the direction of the jet; (b) the force component normal to the jet; and (c) the magnitude and direction of the resultant force exerted on the blade.



Rx = u, {- 180, A, 1} + u2 } + 18v, A, 16 $U_{1}=25m/8$, $U_{2}=25cos115$ => Rx= - 1117N Ry= 9, 5-1PV, A, 13+ V2 3+ 1PV2 A2/ $v_1 = 0$, $v_2 = -v_2 \sin 15$ Ry= -712N FORCEONTHE BLADE +1117N & +712N

Control Volume Moving with Constant Velocity

The previous equations (e.g., momentum) are valid for inertial control volumes. A control volume moving with constant velocity is also inertial, since it has no acceleration with respect o the inertial reference frame XYZ.

$$\left. \frac{\partial N}{\partial t} \right|_{SYSEM} = \left. \frac{\partial}{\partial t} \int_{CV} \eta \rho dV + \int_{CS} \eta \rho \vec{V} \cdot d\vec{A} \right.$$

The above equation is valid for any constant velocity motion of coordinate system XYZ, fixed to the control volume if

- 1. All velocities are measured relative to the control volume
- 2. All time derivatives are measured relative to the control volume

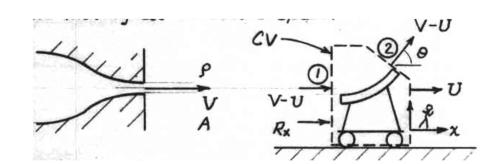
$$F_{x} = F_{Sx} + F_{Bx} = \frac{\partial}{\partial t} \int_{CV} u_{xyz} \rho \, dV + \int_{CS} u_{xyz} \rho \, \overrightarrow{V}_{xyz} \cdot d\overrightarrow{A}$$

The subscript xyz indicates that all velocities are measured relative to the control volume. Velocities are those that would be seen by an observer moving at constant speed with the control volume.

The adjoining figure shows water from a jet (of velocity V) striking a vane of mass M moving with a constant speed (U).

Find expressions for the

- i) forces, R_x and R_y exerted by the vane;
- ii) power produced by the vane;
- iii) deduce a relation between V and U to maximize the power.



You may assume that there is no net pressure force and no change in jet speed.

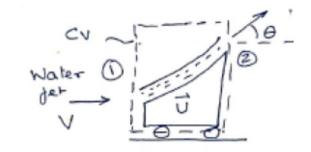
$$F_{x} = F_{Sx} + F_{Bx} = \frac{\partial}{\partial t} \int_{CV} u_{xyz} \rho dV + \int_{CS} u_{xyz} \rho \overrightarrow{V}_{xyz} . d\overrightarrow{A}$$

$$F_{x} = F_{Sx} + F_{Bx} = \frac{\partial}{\partial t} \int_{CV} u_{xyz} \rho \, dV + \int_{CS} u_{xyz} \rho \, \overline{V}_{xyz} \, . \, d\overline{A}$$

Ry =
$$P(V-u)^2(cos\theta-1)$$

 $V_{x} = -R_{x} = P(V-u)^2(1-cos\theta)$
POWER PRODUCED BY THE VANE
 $V_{x} \times (VEL) = P(V-u)^2 U \wedge (I-cos\theta)$
 $V_{x} \times (VEL) = V_{y} = V_{y}$

Since the area of the jet is constant, the velocity of the jet leaving will also be equal to \overrightarrow{V} . The velocity of the CV to the right is \overrightarrow{U}



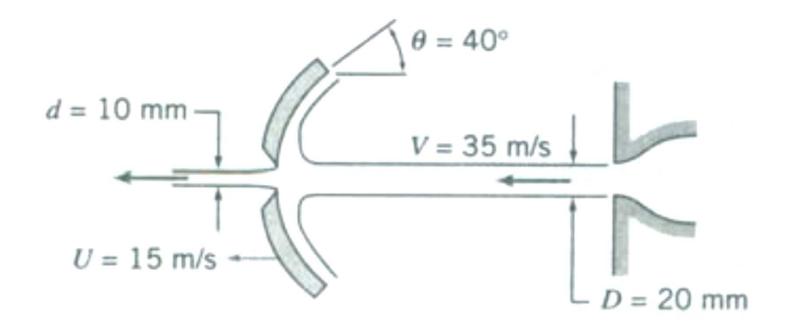
The time derivatives in the governing equations are to be measured relative to the CV. The CV is moving to the right

In order to use the equations (mass and momentum) in the integral form for **an inertial CV**, we may assume that the entire CV may be moving to the left with a velocity \overrightarrow{U} (i.e. the velocity now is $-\overrightarrow{U}$) such that the coordinate system fixed on the CV would appear to be stationery.

The velocity of water entering and leaving the jet in that case would have to be taken as $(\vec{V} - \vec{U})$ at both entry and exit, to be used in the continuity and momentum equations, i.e., $\vec{V}_{xyz} = \vec{V} - \vec{U}$

To use the 2nd tern of the momentum equation, $\int u \rho \vec{V}_{xyz}$. \vec{dA} u is the x component of \vec{V}_{xyz}

Thus u at 1 is $\vec{V}_{xyz} \cos 0^o = V - U$ and u at 2 is $\vec{V}_{xyz} \cos \theta = (V - U) \cos \theta$



The circular dish in the figure has an outside diameter of 0.2 m. A water jet with speed of 35 m/s strikes the dish concentrically. The dish moves to the left at 15 m/s. The jet diameter is 20 mm. The dish has a hole at its centre that allows a stream of water, 10 mm in diameter to pass through without resistance. The remainder of the jet is deflected and flows along the dish. Calculate the force required to maintain the dish motion.

Answer: $R_x = -167N$