

**Part-B answer**

4. In the conical region of silo, inclined solids wall offers significant wall stress/resistance stress on the particles during the flow of particles. It dominates very high as the cross sectional area converges. This resistance stress causes the consolidation of particles. Hence, depends upon the outlet diameter, arch may be formed in the conical region of the silo. These effects are not at all observed in the cylindrical region of the silo.

$$5. \sigma^1 (2\pi r) dl \sin\theta = \rho_b (\pi r^2) dz g$$

6. Sudden raise in the energy (pressure) losses at minimum fluidization velocity is to overcome the static friction between particles.

7. Draw Geldart chart. Fluidization – Type A and B. dense phase pneumatic transport – Type A and D.

8. If abrasive particles are stored in silo, funnel flow is recommended to avoid the erosion of silo walls.

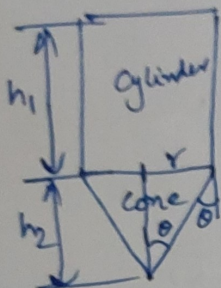
Please turn to next page for the solutions of Q 9 and Q10.

9

$$\text{mass} = 1000 \text{ tons}$$

$$\text{density} = 3 \text{ g/cc} = 3000 \text{ kg/m}^3$$

$$\text{Volume of powder to be stored} = \frac{10^5}{3000} = \frac{1}{3} \times 10^2 = 33.33 \text{ m}^3$$



$$\text{Volume of Silo} = 33.33 \text{ m}^3$$

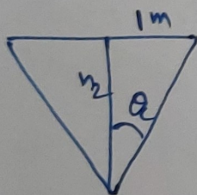
$$V_{\text{cylinder}} + V_{\text{cone}} = 33.33 \text{ m}^3$$

$$\pi r^2 h_1 + \frac{1}{3} \pi r^2 h_2 = 33.33$$

$$\text{dia} = 2 \text{ m}$$

$$r = 1 \text{ m}$$

$$\pi h_1 + \frac{1}{3} \pi h_2 = 33.33 \quad \text{--- (1)}$$



$\theta_c \rightarrow$  cone angle

$$\phi_2 = 12^\circ$$

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$$\tan \phi_e = \frac{\text{shear stress}}{\text{normal stress}}$$

$$= \frac{6.92}{4}$$

$$\phi_e = 60^\circ$$

from mass

$$\theta_c = 33^\circ - 3^\circ = 30^\circ$$

$$\tan \theta_c = r/h_2$$

$$h_2 = \frac{1}{\tan 30^\circ} = \sqrt{3} \text{ m}$$

$$\text{from eq (1)} \quad \pi h_1 + \frac{1}{3} \pi \times \sqrt{3} = 33.33$$

$$\Rightarrow h_1 = 10.03 \text{ m}$$

$$\text{Silo Height} = h_1 + h_2$$

$$= 10.03 + \sqrt{3} = 11.76 \text{ m}$$



10) Sol<sup>n</sup>:-

Pipe =

$$L = 50 \text{ m}$$

$$D = 4 \text{ inch} = 0.1016 \text{ m}$$

$$U_s V_A = 15 \text{ ms}^{-1}$$

$$\Delta P = ?$$

$$K.E \ll P.E \quad \therefore 0.5 \times 200 \times 0.0211 + 20 \times 0.0211 = 0.422$$

$$\text{Mass flow, } M_p = 200 \text{ kg/min.}$$

$$\rho_p = 2000 \text{ kg/m}^3, \quad \epsilon = 0.98.$$

$$\theta = 90^\circ.$$

for press<sup>r</sup> drop,

$$\Delta P = f_{fw} L + f_{pw} L + f_f L \epsilon g \sin \theta + f_p L (1 - \epsilon) g \sin \theta. \quad \rightarrow \textcircled{1}$$

Now,

$$f_{pw} L = 0.057 G L \sqrt{g/D}.$$

$$G = \frac{M_p}{A} = \frac{200 \text{ kg/min}}{\frac{\pi}{4} (0.1016)^2} = \frac{200 \times 4}{\pi (0.1016) \times 60 \text{ sec}}$$

$$= 411.15$$

$$\therefore f_{pw} L = 0.057 \times 411.15 \times 50 \sqrt{\frac{9.8}{0.1016}} = 11508.304$$

$$f_{fw} L = \frac{2 f_g f_f U_s^2 L}{D}, \quad \text{where, } f_g = \text{fanning factor.}$$

$$Re = \frac{\rho v d}{\mu}$$

$$\mu = 10^{-3} \text{ CP} = 10^{-6} \frac{\text{g}}{\text{m.s}}$$

$$= \frac{1 \times 15 \times 0.1016}{10^{-6}}$$

$$= 1.5 \times 10^6$$

$\therefore$  from diagram,  $f_g$  is found to be 0.011.

$$\therefore f_{fw} L = \frac{2 \times 0.011 \times 1 \times (15)^2 \times 50}{0.1016} = 2436.02$$



Now,

$$\int_0^L \epsilon g \sin \theta = 1 \times 50 \times 0.98 \times 9.8 = 480.2$$

$$\int_0^L (1-\epsilon) g \sin \theta = 2000 \times 50 \times 0.02 \times 9.8 = 19600$$

Substituting in eq<sup>n</sup> (1), we get.

$$\Delta P = 2436.02 + 11508.304 + 480.2 + 19600$$

$$= 34024.524 \text{ Pa.}$$

$$= 34.024 \text{ kPa}$$

$$\Delta P = 34.024 \text{ kPa}$$