



Answer attached

**Answer the following four questions.**

**Pay attention: Problem draft drawings will be considered.**

**Question:1**

**(5 Marks)**

**Calculate** the rate of heat loss through the vertical walls of a boiler furnace of size 4 m by 3 m by 3 m high. The walls are constructed from an inner fire brick wall 25 cm thick of thermal conductivity 0.4 W/ m°K, a layer of ceramic blanket insulation of thermal conductivity 0.2 W/ m°K and 8 cm thick, and a steel protective layer of thermal conductivity 55 W/m°K and 2 mm thick. The inside temperature of the fire brick layer was measured at 600 °C and the temperature of the outside of the insulation 60 °C. Also **find** the interface temperature of layers.

**Question:2**

**(5 Marks)**

Air at 20°C blow over a hot plate 50 x 75 cm and thick 2 cm maintained at 250°C. The convection heat transfer coefficient is 25 W/m<sup>2</sup> °C. **Calculate** the inside plate temperature if it is made of carbon steel and that 300 W is lost from the plate surface by radiation, where thermal conductivity is 43 W/m °C.

**Question:3**

**(5 Marks)**

A steam pipe of 10 cm ID and 11 cm OD is covered with an insulating substance, ( $k = 1$  W/ m°K). The steam temperature is 200 °C and ambient temperature is 20 °C. If the convective heat transfer coefficient between insulating surface and air is ( $h_{air} = 8$  W/m<sup>2</sup>K), find the critical radius of insulation for this case, ( $r_c$ ). **Calculate** the heat loss per m of pipe ( $\frac{Q}{L}$ ), and the outer surface temperature, ( $T_o$ ). Neglect steel pipe thermal resistance.

**Question:4**

**(5 Marks)**

One meter length steel pipe ( $K = 45.0$  W/ m°K), having a 0.05m O.D is covered with a 0.042 m thick layer of magnesia ( $K = 0.07$  W/ m°K) which in turn covered with a 0.024 m layer of fiberglass insulation ( $K = 0.048$  W/ m°K). The pipe wall outside temperature is 370 °K and the outer surface temperature of the fiberglass is 305 °K.? Also, Neglecting steel pipe thermal resistance, **Calculate**:

- The steady state heat transfer.
- The interfacial temperature between the magnesia and fiberglass.
- The overall heat transfer coefficient, considering area of steel outside surface.

With my best wishes,

Dr. Salah Dafea



**Question:1**

**(5 Marks)**

$$A = 4 \times 3 = 12 \text{ m}^2$$

$$\Delta T = 600 - 60 = 540^\circ\text{C}$$

$$R_{th_1} = \frac{L_1}{k_1 A_1} = \frac{0.25}{0.4 \times 12} = 0.052 \text{ } ^\circ\text{K/W}$$

$$R_{th_2} = \frac{L_2}{k_2 A_2} = \frac{0.08}{0.2 \times 12} = 0.033 \text{ } ^\circ\text{K/W}$$

$$R_{th_3} = \frac{0.002}{55 \times 12} = 0.000003 \text{ } ^\circ\text{K/W}$$

$$\Delta T = Q R_{th}$$

$$\therefore Q = \Delta T / \sum R_{th}$$

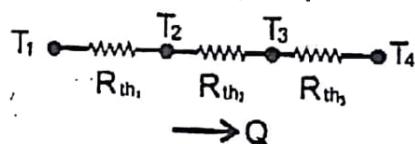
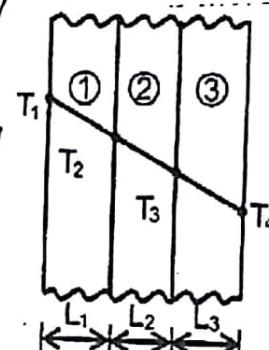
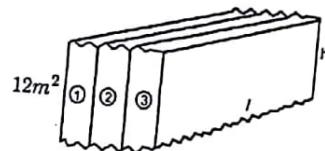
$$= \frac{540}{0.052 + 0.033 + 0.000003} = 6320.96 \text{ W} \quad \text{ans}$$

For steel layer only :

$$Q = \frac{T_{inner} - 60}{R_{th_3}} \implies T_3 - 60 = Q R_{th}$$

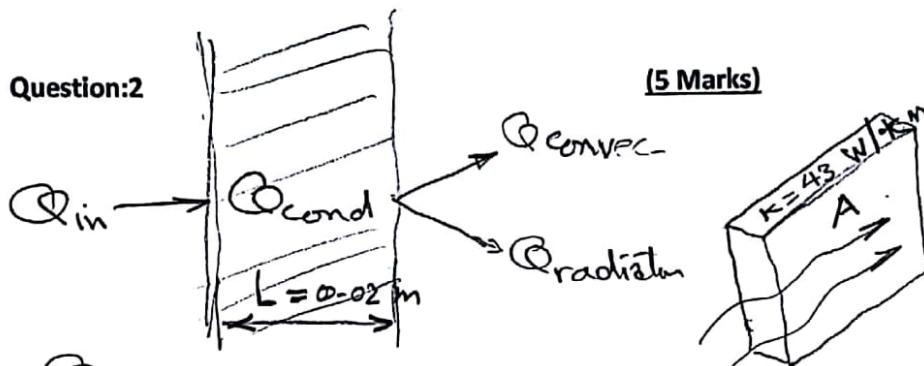
$$\therefore T_3 - 60 = 6320 \times 0.000003 = 0.0196 \text{ } ^\circ\text{K}$$

$$T_3 = 60.02 \text{ } ^\circ\text{K}$$



Question:2

(5 Marks)



$$h_{\text{air}} = 25 \text{ W/m}^2 \text{K}$$

$$K = 43 \text{ W/mK}$$

$$\begin{aligned} Q_{\text{conv.}} &= h A \Delta T \\ &= 25 \times 0.375 \times (250 - 20) \\ &= 2.156 \text{ kW} \end{aligned}$$

$$\begin{aligned} A &= 0.5 \times 0.75 \\ &= 0.375 \text{ m}^2 \end{aligned}$$

$$\begin{aligned} Q_{\text{rad}} &= 300 \text{ W} = 0.3 \text{ kW} \\ Q_{\text{tot}} &= 0.3 + 2.156 = 2.456 \text{ kW} \end{aligned}$$

$$Q_{\text{tot}} = Q_{\text{in}} = 43 (0.375) \times \frac{T_1 - 250}{0.02} \implies T_1 = 253.05^\circ\text{C}$$

Question:3

(5 Marks)

$$r_c = \frac{k}{h_o} = \frac{1}{8} = 0.125 \text{ m}$$

$$\Delta T = Q \sum R_{\text{th}}$$

$$\sum R_{\text{th}} = \left( \frac{\ln \frac{r_c}{r_o}}{2\pi k L} + \frac{1}{h \cdot r_c} \right)$$

$$= 2\pi L \left( \frac{\ln(r_c/r_o)}{k} + \frac{1}{h \cdot r_c} \right)$$

$$= 2\pi \times 1 \left( \frac{\ln \frac{0.125}{0.5}}{1} + \frac{1}{8 \times 0.125} \right) = 0.289$$

$$\frac{Q}{L} = \frac{\Delta T}{\sum R_{\text{th}}} = \frac{-180}{0.289} = 622 \text{ W/m} \rightarrow \text{ans}$$

For convection heat transfer;

$$Q = \frac{\Delta T}{R_{\text{th}}} = \frac{T_3 - 20}{\frac{1}{8 \times 2\pi \times 0.125 \times 1}}$$

From which

$$T_3 = 118.72^\circ\text{C}$$

Question:4

(5 Marks)

$$\Delta T_{\text{overall}} = 370 - 305 = 65^{\circ}\text{K}$$

$$r_1 = 0.025 \text{ m}$$

$$r_2 = 0.025 + 0.42 \\ = 0.067 \text{ m}$$

$$r_3 = 0.067 + 0.024 \\ = 0.091 \text{ m}$$

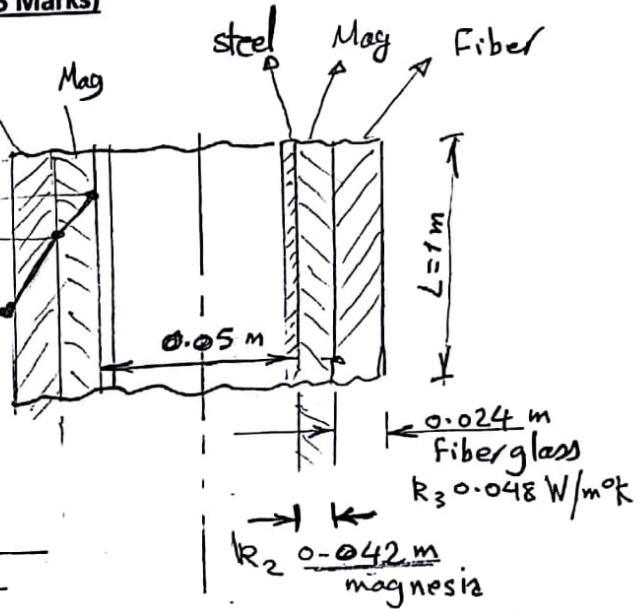
neglecting pipe steel resistance

$$\sum R_{th} = \frac{\ln \frac{r_2}{r_1}}{2\pi k_2 L} + \frac{\ln \frac{r_3}{r_2}}{2\pi k_3 L}$$

$$= \frac{\ln \frac{0.067}{0.025}}{2\pi \times 0.07 \times 1} + \frac{\ln \frac{0.091}{0.067}}{2\pi \times 0.048 \times 1}$$

$$= 2.24 + 1.02$$

$$= 3.26 \text{ } ^{\circ}\text{K/W}$$



$$Q = \frac{\Delta T}{\sum R_{th}} = \frac{65}{3.26} = 19.9 \text{ W} \rightarrow \text{ans (a)}$$

For Magnesia only

$$Q = \frac{\Delta T}{R_{th}}$$

$$19.9 \text{ W} = \frac{(370 - T_2)}{\left( \frac{\ln \frac{0.067}{0.025}}{2\pi \times 0.07 \times 1} \right)} = \frac{370 - T_2}{2.24}$$

$$\therefore T_2 = 19.9 \times 2.24 - 370 = 325.62 \text{ } ^{\circ}\text{K} \rightarrow \text{ans (b)}$$

$$\therefore Q = U A \Delta T = \frac{\Delta T}{R_{th}}$$

$$U = \frac{1}{R_{th} \cdot A} \rightarrow = \frac{1}{3.26 \times 2\pi(0.025) \times 1}$$

$$U = 1.95 \text{ W}/\text{K.m} \rightarrow \text{ans (c)}$$