

Optativa 4rt curs de Biotecnologia

Modelització i simulació de biosistemes

Sistemes en estat estacionari. MFB

Joan Albiol

Departament d'Enginyeria Química Escola d'Enginyeria Universitat Autònoma de Barcelona







Anàlisi per balanceig de fluxos (Flux Balance Analisis)

Una forma d'estudiar les capacitats del metabolisme o l'efecte d'una modificació consisteix en optimitzar una determinada funció que sigui combinació lineal de fluxos.

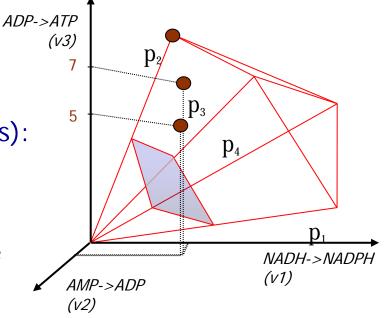
Per exemple:

$$F(v) = \overset{\circ}{\mathbf{a}} \; \mathbf{a}_i v_i$$

S'ha de complir al mateix temps (restriccions):

$$0 = \frac{dx}{dt} = S \times V \qquad v_i \stackrel{3}{=} 0, \quad v_j < b$$

Es tractaria de trobar la combinació de fluxos que faci que la funció F arribi a un màxim (mètodes d'optimització. Programació lineal)



Per exemple quina distribució de fluxos donaria la màxima producció d'ATP o la biomassa màxima?

En general l'òptim possible es troba en un vèrtex del con de flux.

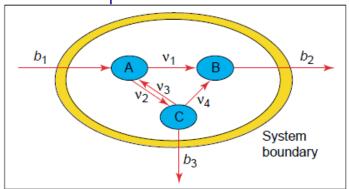
Quan es compara una soca salvatge amb una modificada es sol trobar un punt proper a l'òptim trobat



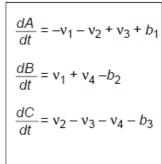


Esquema bàsic del procediment (exemple I)

(a) Xarxa a optimitzar

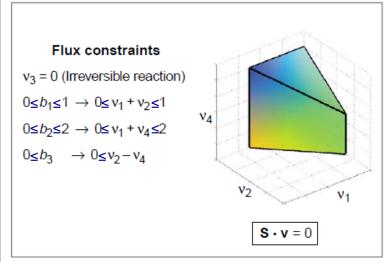


(b) Equacions diferencials i matrius que la representen

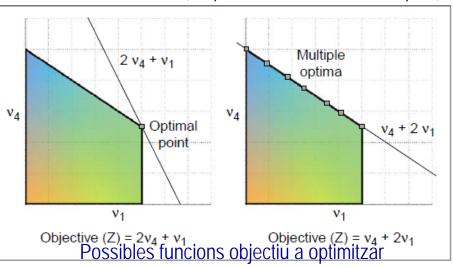


$$\begin{bmatrix} \frac{dA}{dt} \\ \frac{dB}{dt} \\ \frac{dC}{dt} \end{bmatrix} = \begin{bmatrix} -1 & -1 & 1 & 0 & 1 & 0 & 0 \\ 1 & 0 & 0 & 1 & 0 & -1 & 0 \\ 0 & 1 & -1 & -1 & 0 & 0 & -1 \\ \hline & & & & & & & & & & \end{bmatrix} \begin{bmatrix} v_1 \\ v_2 \\ v_3 \\ v_4 \\ b_1 \\ b_2 \\ b_3 \end{bmatrix}$$

(c) Restriccions a aplicar



(d) Possibles solucions (esquerra: única, dreta: múltiples)



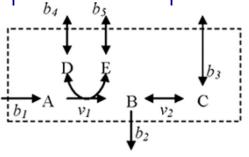
Current Opinion in Biotechnology







Esquema bàsic del procediment (exemple II)

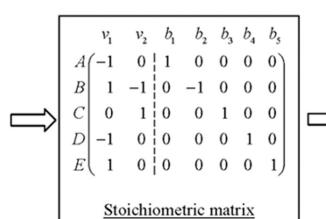


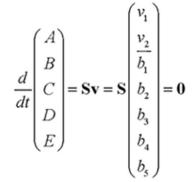
System Reconstruction

 v_1 : A + D \rightarrow E + B v_2 : B \leftrightarrow C

 b_1, b_2, \dots, b_5 : Exchange

reactions for A-E

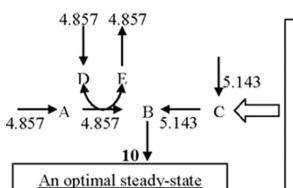




Steady State Mass balance

FLUX BALANCE ANALYSIS





flux distribution

Objective: maximise production of B (b_2)

Optimise (LP): $\max \langle \mathbf{c} \cdot \mathbf{v} \rangle$ s. t. $\mathbf{S}\mathbf{v} = \mathbf{0}$

 $\mathbf{c} = \begin{bmatrix} 0 & 0 & 0 & 1 & 0 & 0 & 0 \end{bmatrix}^{\mathrm{T}}$

Objective function for optimisation

 $\max_{\mathbf{v}} \mathbf{c}^T \mathbf{v} \quad \text{s. t. } \mathbf{S} \cdot \mathbf{v} = 0$

$$\begin{aligned} 0 &\leq v_1 \leq 10 \\ -10 &\leq v_2 \leq 10 \\ 0 &\leq b_1, b_2 \leq 10 \\ -10 &\leq b_3, b_4, b_5 \leq 10 \end{aligned}$$

Addition of Constraints

(Raman 2009)

Anàlisi per balanceig de fluxos Esquema bàsic del procediment (exemple IIII)



 R_1 R_2

 R_3

 R_{Δ} R_5

 R_6

 R_7

 \mathbf{R}_8

 R_9

 R_{10}

 V_{m}

 A_{xt}

 \mathbf{D}_{xt}

 \mathbf{F}_{xt}

 \mathbf{H}_{xt}

V

 $V_{ ext{growth}}$

0

0

0

0

0

0

0

0

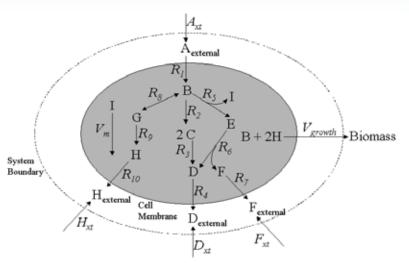
0

0

0

0

=



	R_1	R_2	R_3	R_4	R_5	R_6	R_7	R_8	R_9	R_{10}	V_m	V_{growth}	Axt	$D_{\mathbf{x}t}$	F_{nt}	H_{xt}
A	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
В	1	-1	0	0	-1	0	0	-1	0	0	0	-1	0	0	0	0
С	0	2	-1	0	0	0	0	0	0	0	0	0	0	0	0	0
D	0	0	1	-1	0	1	0	0	0	0	0	0	0	0	0	0
E	0	0	0	0	1	-1	0	0	0	0	0	0	0	0	0	0
F	0	0	0	0	0	1	-1	0	0	0	0	0	0	0	0	0
G	0	0	0	0	0	0	0	1	-1	0	0	0	0	0	0	0
Н	0	0	0	0	0	0	0	0	1	-1	0	-2	0	0	0	0
I	0	0	0	0	1	0	0	0	0	0	-1	0	0	0	0	0
$\mathbf{A}_{external}$	-1	0	0	0	0	0	0	0	0	0	0	0	1	0	0	0
$\mathbf{D}_{external}$	0	0	0	1	0	0	0	0	0	0	0	0	0	1	0	0
F _{external}	0	0	0	0	0	0	1	0	0	0	0	0	0	0	1	0
$\mathbf{H}_{external}$	0	0	0	0	0	0	0	0	0	1	0	0	0	0	0	1
'	_							C			•					
							1	3								

Figure 2b: Hypothetical metabolic network

Mass Balances	Flux Constraints					
$\mathbf{B}: R_{1} - R_{2} - R_{5} - R_{8} - V_{\text{excepts}} = 0$	$0 \le R_1 \le \infty$					
	$0 \le R_q \le \infty$					
$C: 2R_2 - R_3 = 0$	0 ≤ R, ≤ ∞					
$\mathbf{D}: R_3 + R_6 - R_4 = 0$	0≤R,≤∞					
$\mathbf{E}: R_s - R_e = 0$	0 ≤ R, ≤∞					
$\mathbf{F}: R_{\varepsilon} - R_{2} = 0$	0≤R,≤∞					
	0 ≤ R _y ≤ ∞					
$G: R_8 - R_9 = 0$	-∞≤R ₆ ≤∞					
$\mathbf{H}: R_9 - R_{10} - 2V_{growth} = 0$	0≤R, ≤∞ 0≤R, ≤∞					
$I: R_s - V_m = 0$	K S V_ S K					
$\mathbf{A}_{enemal}: A_{st} - R_1 = 0$	0 ≤ V _{prod} ≤ ∞					
$\mathbf{D}_{coronal}$: $D_{cr} + R_{s} = 0$	$Y_2 \le A_{\omega_p} \le Y_2$					
\mathbf{F}_{extend} : $F_{ex} + R_2 = 0$	-∞≤D≤0					
months of 1	$-\infty \le F_{\omega_r} \le 0$					
$\mathbf{H}_{external}$: $H_{sp} + R_{10} = 0$	$-\omega \le H_{sp} \le 0$					
Objective Function						
$Z=V_{growth}$						

Figure 3: Constraints on the metabolic network. The constraints on the metabolic network consist of mass balance constraints and flux constraints (reversibility constraints). Linear programming can be used to determine the optimal use of the metabolic network subject to the imposed constraints.

Maximitzar el producte:

$$\max(v) = \begin{cases} \hat{\mathbf{e}}_{0} & \hat{\mathbf{u}} & \hat{\mathbf{e}}_{R_{5}} & \hat{\mathbf{u}} \\ \hat{\mathbf{e}}_{0} & \hat{\mathbf{u}} & \hat{\mathbf{e}}_{R_{6}} & \hat{\mathbf{u}} \\ \hat{\mathbf{e}}_{0} & \hat{\mathbf{u}} & \hat{\mathbf{e}}_{R_{6}} & \hat{\mathbf{u}} \\ \hat{\mathbf{e}}_{0} & \hat{\mathbf{u}} & \hat{\mathbf{e}}_{R_{7}} & \hat{\mathbf{u}} \\ \hat{\mathbf{e}}_{0} & \hat{\mathbf{u}} & \hat{\mathbf{e}}_{R_{8}} & \hat{\mathbf{u}} \\ \hat{\mathbf{e}}_{0} & \hat{\mathbf{u}} & \hat{\mathbf{e}}_{R_{9}} & \hat{\mathbf{u}} \\ \hat{\mathbf{e}}_{0} & \hat{\mathbf{u}} & \hat{\mathbf{e}}_{R_{9}} & \hat{\mathbf{u}} \\ \hat{\mathbf{e}}_{0} & \hat{\mathbf{u}} & \hat{\mathbf{e}}_{R_{10}} & \hat{\mathbf{e}}_{R_{10}} & \hat{\mathbf{u}} \\ \hat{\mathbf{e}}_{0} & \hat{\mathbf{u}} & \hat{\mathbf{e}}_{R_{10}} & \hat{\mathbf{u}} \\ \hat{\mathbf{e}}_{$$

 $\stackrel{\cdot}{\mathbf{e}} R_1 \stackrel{\cdot}{\mathbf{u}}$ $\stackrel{\cdot}{\mathbf{e}} R_2 \stackrel{\cdot}{\mathbf{u}}$ $\stackrel{\cdot}{\mathbf{e}} R_3 \stackrel{\cdot}{\mathbf{u}}$ $\stackrel{\cdot}{\mathbf{e}} R_4 \stackrel{\cdot}{\mathbf{u}}$

Subjecte a les restriccions:

$$0 = S \times V$$

 $v_i^{3} 0, v_j < b$







Avantatges i desavantatges

Avantatges

- Només es necessita informació de les reaccions del metabolisme i la seva estequiometria
- No es necessita obtenir paràmetres cinètics (molt difícils de determinar amb precisió)

Desavantatges

- No té en compte informació de regulació (per tant s'ha de considerar com un òptim però no necessariament l'organisme hi ha d'arribar)
- Les discrepàncies amb dades experimentals impliquen que s'ha d'obtenir informació de la regulació.
- No dóna informació del comportament dinàmic (es sap l'òptim al que pot arribar però no a la velocitat que hi arribarà si hi arriba)

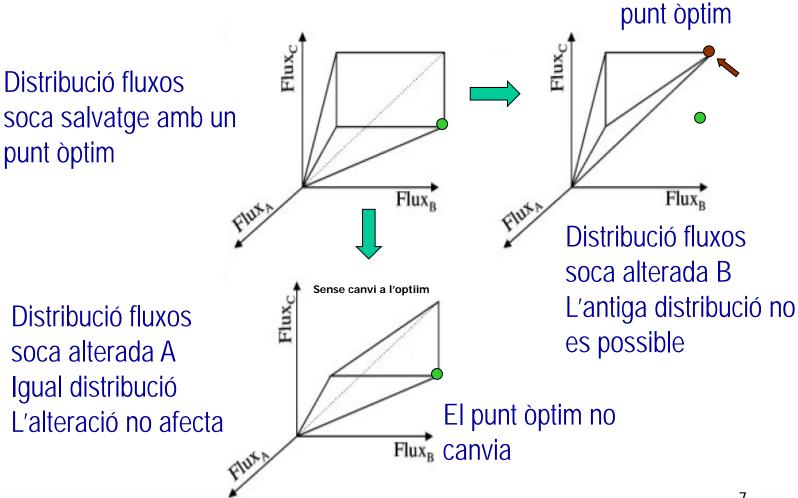




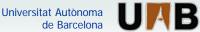
Apareix un nou

L'efecte d'una eliminació d'un pas és eliminar una via extrema i l'espai de fluxos possible queda restringit a un espai menor

Exemple de dos canvis diferents:







In silico predictions of Escherichia coli metabolic capabilities are consistent with experimental data

Jeremy S. Edwards^{1,2}, Rafael U. Ibarra¹, and Bernhard O. Palsson^{1*}

Department of Bioengineering, University of California, San Diego, 9500 Gilman Drive, La Jolla, CA 92093-0412. Current address: Department of Chemical Engineering, University of Delaware, Newark, DE 19716. *Corresponding author (palsson@ucsd.edu).

Received 19 September 2000; accepted 9 November 2000

A significant goal in the post-genome era is to relate the annotated genome sequence to the physiological functions of a cell. Working from the annotated genome sequence, as well as biochemical and physiological information, it is possible to reconstruct complete metabolic networks. Furthermore, computational methods have been developed to interpret and predict the optimal performance of a metabolic network under a range of growth conditions. We have tested the hypothesis that *Escherichia coli* uses its metabolism to grow at a maximal rate using the *E. coli* MG1655 metabolic reconstruction. Based on this hypothesis, we formulated experiments that describe the quantitative relationship between a primary carbon source (acetate or succinate) uptake rate, oxygen uptake rate, and maximal cellular growth rate. We found that the experimental data were consistent with the stated hypothesis, namely that the *E. coli* metabolic network is optimized to maximize growth under the experimental conditions considered. This study thus demonstrates how the combination of *in silico* and experimental biology can be used to obtain a quantitative genotype-phenotype relationship for metabolism in bacterial cells.

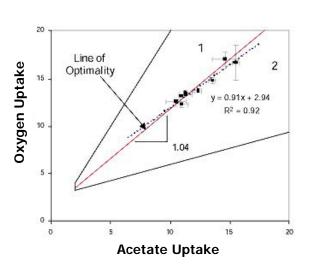


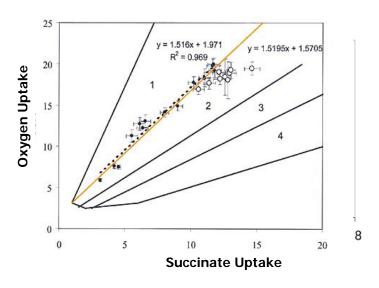


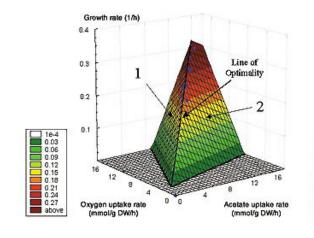
Comprovació de la predicció 'in silico' amb dades experimentals

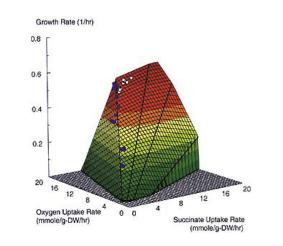
E.colia) Predicció:Relació entre

- -Velocitat de creixement
- -Consum d'oxigen
- -Consum d'acetat o succinat
- b) Comparació amb dades experimentals









0.42

Universitat Autònoma de Barcelona

Vol. 60, No. 10

APPLIED AND ENVIRONMENTAL MICROBIOLOGY, Oct. 1994, p. 3724–3731 0099-2240/94/\$04.00+0 Copyright © 1994, American Society for Microbiology

Stoichiometric Flux Balance Models Quantitatively Predict Growth and Metabolic By-Product Secretion in Wild-Type Escherichia coli W3110

AMIT VARMA AND BERNHARD O. PALSSON*

Department of Chemical Engineering, University of Michigan, Ann Arbor, Michigan 48109

Received 10 March 1994/Accepted 4 August 1994

Flux balance models of metabolism use stoichiometry of metabolic pathways, metabolic demands of growth, and optimality principles to predict metabolic flux distribution and cellular growth under specified environmental conditions. These models have provided a mechanistic interpretation of systemic metabolic physiology, and they are also useful as a quantitative tool for metabolic pathway design. Quantitative predictions of cell growth and metabolic by-product secretion that are experimentally testable can be obtained from these models. In the present report, we used independent measurements to determine the model parameters for the wild-type Escherichia coli strain W3110. We experimentally determined the maximum oxygen utilization rate (15 mmol of O2 per g [dry weight] per h), the maximum aerobic glucose utilization rate (10.5 mmol of Glc per g [dry weight] per h), the maximum anaerobic glucose utilization rate (18.5 mmol of Glc per g [dry weight] per h), the non-growth-associated maintenance requirements (7.6 mmol of ATP per g [dry weight] per h), and the growth-associated maintenance requirements (13 mmol of ATP per g of biomass). The flux balance model specified by these parameters was found to quantitatively predict glucose and oxygen uptake rates as well as acetate secretion rates observed in chemostat experiments. We have formulated a predictive algorithm in order to apply the flux balance model to describe unsteady-state growth and by-product secretion in aerobic batch, fed-batch, and anaerobic batch cultures. In aerobic experiments we observed acetate secretion, accumulation in the culture medium, and reutilization from the culture medium. In fed-batch cultures acetate is cometabolized with glucose during the later part of the culture period. Anaerobic batch culture is observed to primarily secrete the by-products acetate, ethanol, and formate. The flux balance model was found to quantitatively predict the time profiles of cell density and glucose and by-product concentrations in the above-described experiments. Taken together, the experimental data and model predictions presented show that observed growth and by-product secretion of wild-type E. coli are consistent with stoichiometrically optimal pathway utilization. Flux balance models can thus be used to describe prokaryotic metabolic physiology, and they can be applied to bioprocess design and control.





Comprovació de la predicció 'in silico' amb dades experimentals II

a) Predicció:

Fixar una determinada velocitat de consum de

substrat Calcular:

- -Velocitat de creixement
- -Consum d'oxigen
- -Producció d'acetat
- b) Comparació amb dades experimentals

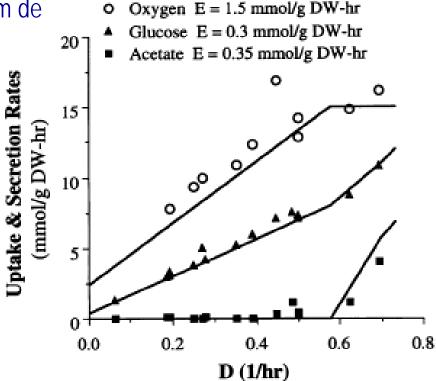
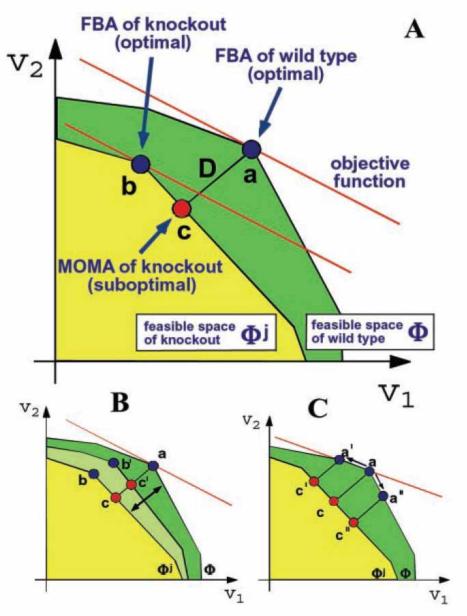


FIG. 6. Analysis of aerobic chemostat culture showing the glucose and oxygen uptake rates and the acetate secretion rate as functions of the dilution or growth rate. The chemostat was not limited for minerals. The solid lines represent the flux balance model simulations. E, average deviation between predictions of the model and experimental measurements; DW, dry weight.



A partir de l'èxit aconseguit amb els mètodes FBA s'estudien nous mètodes que busquen millorar les prediccions

El MOMA és un exemple d'aquests mètodes.

Intenta predir una distribució de fluxos d'un organisme al que se l'hi ha eliminat un pas metabòlic.

Postula que el sistema metabòlic es reajusta de manera que es minimitza la 'distància' entre la distribució de fluxos que pot assolir i el òptim on arribaria la soca salvatge.