

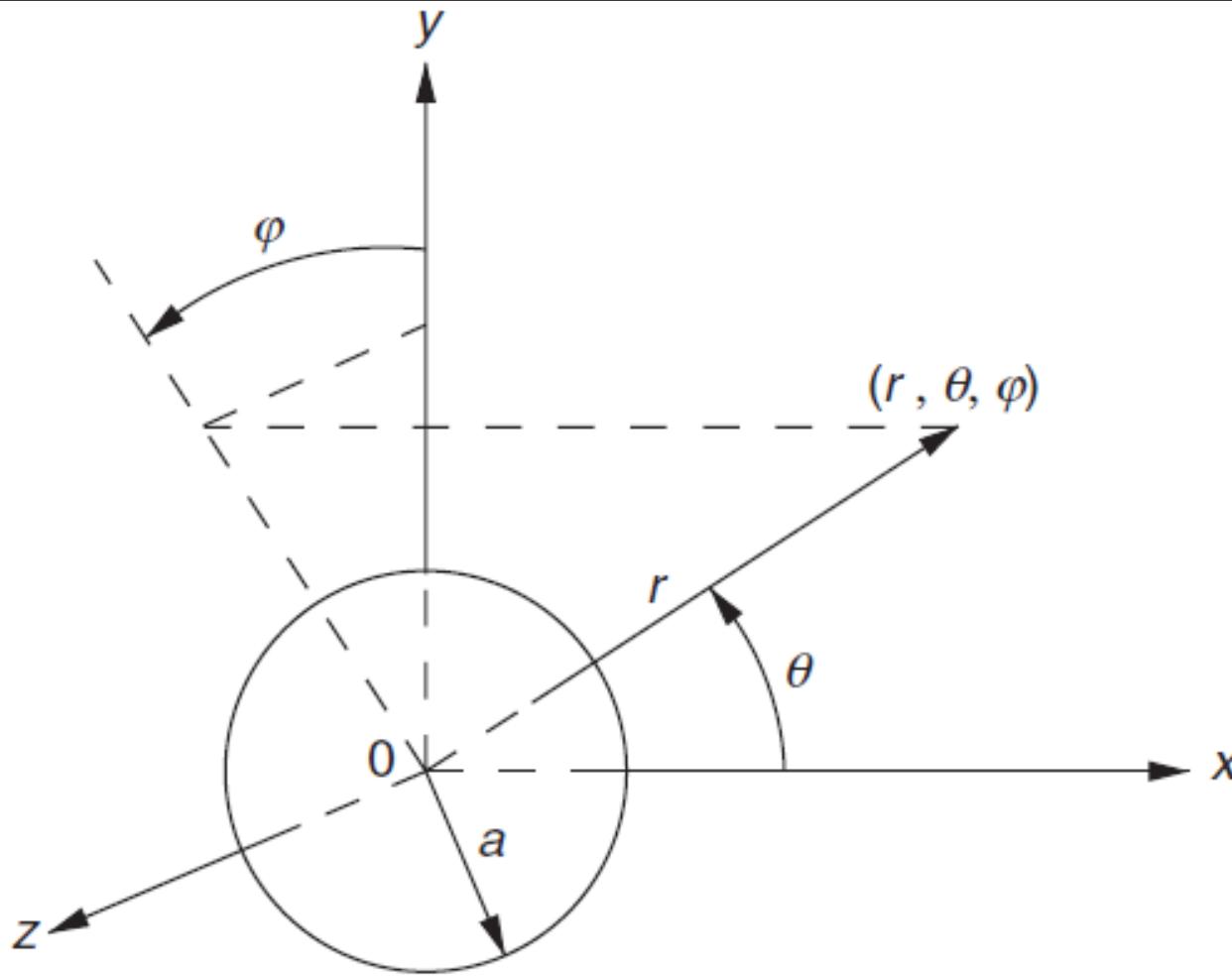
Numerical Solution of the Incompressible Navier-Stokes Equation

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Flow around A Sphere

- Consider an incompressible flow past a sphere.



- "Far away from the sphere the flow is of a constant speed U along the x axis."
- Due to the axisymmetry, the flow field is independent of the azimuthal coordinate φ .

Flow around A Sphere

- The velocity components u_r and u_θ can be written in term of the stream function ψ as follows.

$$u_r = \frac{1}{r^2 \sin \theta} \frac{\partial \psi}{\partial \theta}, \quad u_\theta = -\frac{1}{r \sin \theta} \frac{\partial \psi}{\partial r}$$

- The Navier-Stokes equation in the general form is given by

$$\rho \left[\frac{\partial \mathbf{v}}{\partial t} - \mathbf{v} \times (\nabla \times \mathbf{v}) \right] = -\nabla \left(p + \frac{1}{2} \rho v^2 \right) - \mu \nabla \times \nabla \times \mathbf{v}, \quad v = |\mathbf{v}|$$

- Taking the curl of the last equation and using the steady-flow assumption, we obtain

$$\frac{1}{r^2 \sin \theta} \left(\frac{\partial \psi}{\partial \theta} \frac{\partial}{\partial r} - \frac{\partial \psi}{\partial r} \frac{\partial}{\partial \theta} + 2 \cot \theta \frac{\partial \psi}{\partial r} - \frac{2}{r} \frac{\partial \psi}{\partial \theta} \right) D^2 \psi = \frac{2}{Re} D^4 \psi$$

Flow around A Sphere

- The Reynolds number $\text{Re} = 2\rho U a / \mu$ is based on the sphere diameter a .
- The stream function ψ and radial coordinate r are nondimensionalized by reference to Ua^2 and a , respectively.
- The operator D^2 is defined as

$$D^2 \equiv \frac{\partial^2}{\partial r^2} + \frac{\sin \theta}{r^2} \frac{\partial}{\partial \theta} \left(\frac{1}{\sin \theta} \frac{\partial}{\partial \theta} \right)$$

- The non-slip boundary condition on the sphere surface leads to

$$\psi(1, \theta) = 0, \quad \frac{\partial \psi}{\partial r}(1, \theta) = 0$$

- Far away from the sphere the flow is uniform, i.e.,

$$\psi(r, \theta) = \frac{1}{2} r^2 \sin^2 \theta \quad \text{as } r \rightarrow \infty$$

Flow around A Sphere

- In term of $\zeta = \cos\theta$, the equation

$$\frac{1}{r^2 \sin \theta} \left(\frac{\partial \psi}{\partial \theta} \frac{\partial}{\partial r} - \frac{\partial \psi}{\partial r} \frac{\partial}{\partial \theta} + 2 \cot \theta \frac{\partial \psi}{\partial r} - \frac{2}{r} \frac{\partial \psi}{\partial \theta} \right) D^2 \psi = \frac{2}{Re} D^4 \psi$$

can be written as

$$\frac{2}{Re} D^4 \psi + \frac{1}{r^2} \left(\frac{\partial \psi}{\partial \zeta} \frac{\partial}{\partial r} - \frac{\partial \psi}{\partial r} \frac{\partial}{\partial \zeta} - \frac{2\zeta}{1-\zeta^2} \frac{\partial \psi}{\partial r} - \frac{2}{r} \frac{\partial \psi}{\partial \zeta} \right) D^2 \psi = 0$$

where $D^2 \equiv \frac{\partial^2}{\partial r^2} + \frac{1-\zeta^2}{r^2} \frac{\partial^2}{\partial \zeta^2}$

- The boundary condition at points far away from the sphere becomes

$$\psi(r, \zeta) = \frac{1}{2} r^2 (1 - \zeta^2) \quad \text{as } r \rightarrow \infty$$

Flow around A Sphere

- Using the Galerkin method, the trial solution is written as a linear combination of basis functions Φ_i : $\psi = \sum_{i=1}^n \Phi_i(r, \zeta)$
- The basis functions Φ_i must be linear independent and differentiable.
- For this problem the basis functions are chosen to be

$$\Phi_i(r, \zeta) = f_i(r) [P_{i-1}(\zeta) - P_{i+1}(\zeta)], \quad i = 1, 2, \dots$$

where $P_m(\zeta)$ are the Legendre polynomials defined by the Rodrigues' formula

$$P_m(\zeta) = \frac{1}{2^m m!} \frac{d^m}{d\zeta^m} (\zeta^2 - 1)^m$$

with the orthogonality $\int_{-1}^1 P_m(\zeta) P_n(\zeta) d\zeta = \frac{2}{2n+1} \delta_{mn}$

Flow around A Sphere

- Using $n = 2$ and $f_i(r)$ is chosen such that

$$\psi = \Phi_1(r, \zeta) + \Phi_2(r, \zeta)$$

where

$$\Phi_1(r, \zeta) = \left(\frac{1}{2}r^2 + \frac{A_1}{r} + \frac{A_2}{r^2} + \frac{A_3}{r^3} + \frac{A_4}{r^4} \right) (1 - \zeta^2)$$

$$\Phi_2(r, \zeta) = \left(\frac{B_1}{r} + \frac{B_2}{r^2} + \frac{B_3}{r^3} + \frac{B_4}{r^4} \right) \zeta (1 - \zeta^2)$$

- To determine the 8 coefficients, A_i and B_i , we need 8 equations.
- The derivation of these equations are given in the reference below.

Rayleigh-Benard Instability

- When a layer of fluid is heated from below, the hotter fluid at the bottom has a lower density than the cooler fluid at the top.
- The buoyant force pushes the hotter fluid from the bottom to the top while the viscous force opposes the buoyant force.
- The dimensionless number called Rayleigh number Ra is the ratio between the buoyant force and the viscous force:

$$\text{Ra} = \frac{g\alpha}{\nu\kappa} (T_{\text{bottom}} - T_{\text{top}}) H^3$$

where α = thermal expansion coefficient of the fluid

κ = thermal diffusivity of the fluid

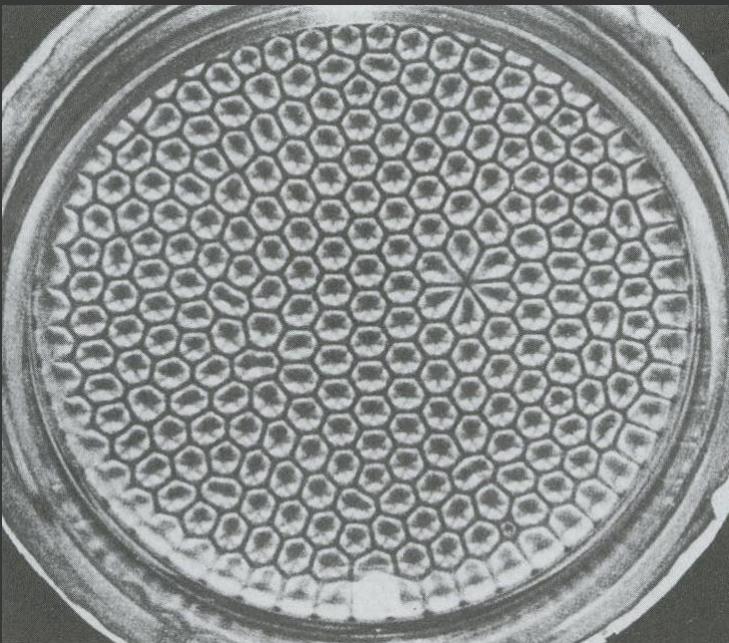
ν = kinematic viscosity of the fluid

H = height of fluid layer

$T_{\text{bottom}}, T_{\text{top}}$ are temperatures at the bottom and top of the fluid

Rayleigh-Benard Instability

- At a large Rayleigh number, the buoyant force is dominant.
- At a critical Rayleigh number, the fluid flow becomes unstable and this instability leads to the formation of Benard cells.
- The onset of Rayleigh-Benard instability can be predicted by a linearized theory presented in Section 3.8 of Biringen and Chow (2011).
 - Once the flow becomes unstable, the fluid motion is governed by the nonlinear Navier-Stokes equation.



Rayleigh-Benard Instability

The governing equations in the case are

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{v}) = 0$$

$$\rho \frac{D\mathbf{v}}{Dt} = -\nabla p - \mu \nabla^2 \mathbf{v} + \Delta \rho \mathbf{g}$$

$$\rho \frac{Dh}{Dt} = \frac{Dp}{Dt} + \nabla \cdot (k \nabla T) + \Phi$$

$$\rho = \rho_0 [1 - \alpha (T - T_0)]$$

where T_0 is the temperature at which the fluid density is ρ_0 .

Rayleigh-Benard Instability

- For ordinary liquids, α is of order 10^{-4} .
- So the Boussinesq approximation can be used, i.e., density can be considered constant everywhere except in the buoyant force term.
- The continuity equation and the Navier-Stokes equation become

$$\nabla \cdot \mathbf{v} = 0, \quad \rho_0 \frac{D\mathbf{v}}{Dt} = -\nabla p - \mu \nabla^2 \mathbf{v} - (\rho - \rho_0) g \mathbf{j}$$

where \mathbf{j} is the unit vector along the y-axis opposite to the gravity.

- It can be shown that the energy equation reduces to

$$\frac{DT}{Dt} = \kappa \nabla^2 T$$

Rayleigh-Benard Instability in 2D

- Consider a 2D flow in the x - y plane.
- Let the height of the fluid layer be H .
- Initially, the fluid has a uniform temperature of T_0 .
- The fluid is then heated from below such that the temperature of the fluid at bottom is fixed at T_1 .
- Any fluid rotation is in the x - y plane. So, the vorticity is in the z direction.
- Let the magnitude of vorticity at any location be denoted by ζ .
- For this problem, the reference length is H , reference velocity is $\mu/\rho_0 H$, and the reference temperature difference is $T_1 - T_0$.

Rayleigh-Benard Instability in 2D

- Dimensionless variables are defined as follows.

$$X = \frac{x}{H}, \quad Y = \frac{y}{H}, \quad T = \frac{t}{\rho_0 H^2 / \mu}, \quad U = \frac{u}{\mu / \rho_0 H}, \quad V = \frac{v}{\mu / \rho_0 H}$$

$$\Psi = \frac{\psi}{\mu / \rho_0}, \quad \Omega = \frac{\zeta}{\mu / \rho_0 H^2}, \quad \theta = \frac{T - T_0}{T_1 - T_0}$$

- From now on T is the dimensionless time.

Rayleigh-Benard Instability in 2D

In terms of the dimensionless variables the governing equations are

$$U = \frac{\partial \Psi}{\partial Y}, \quad V = -\frac{\partial \Psi}{\partial X}, \quad \Omega = -\left(\frac{\partial^2}{\partial X^2} + \frac{\partial^2}{\partial Y^2} \right) \Psi$$

$$\frac{\partial \Omega}{\partial T} + \frac{\partial(U\Omega)}{\partial X} + \frac{\partial(V\Omega)}{\partial Y} = \text{Gr} \frac{\partial \theta}{\partial X} + \left(\frac{\partial^2}{\partial X^2} + \frac{\partial^2}{\partial Y^2} \right) \Omega$$

$$\frac{\partial \theta}{\partial T} + \frac{\partial(U\theta)}{\partial X} + \frac{\partial(V\theta)}{\partial Y} = \text{Pr}^{-1} \left(\frac{\partial^2}{\partial X^2} + \frac{\partial^2}{\partial Y^2} \right) \theta$$

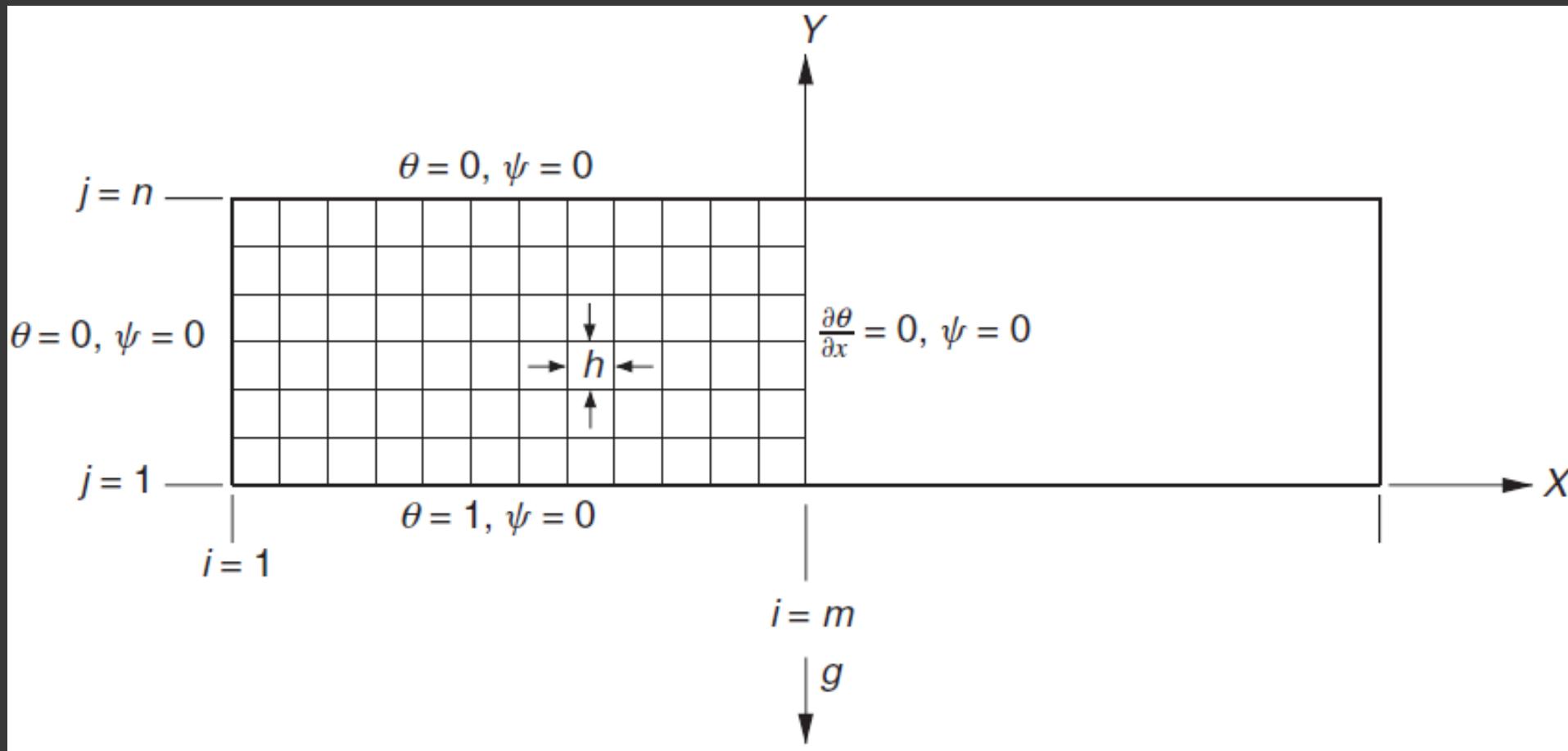
where $\text{Gr} = \alpha g H^3 (T_1 - T_0) / v^2$ is the Grashof number

$\text{Pr} = \nu/\kappa$ is the Prandtl number.

The Rayleigh number is $\text{Ra} = \text{Gr} \times \text{Pr}$.

Rayleigh-Benard Instability in 2D

Let the fluid be water ($\text{Pr} = 6.75$) enclosed by a rectangular box shown below. Due to the symmetry about the Y axis, only the left half needs to be computed.



Rayleigh-Benard Instability in 2D

- At time $T = 0$, the temperature distribution is $\theta = 0$ everywhere, except at the bottom where $\theta = 1$.
- The boundary condition for temperature θ is shown in the previous figure.
- Along the Y axis $d\theta/dX = 0$ due to the symmetry.
- The governing equations are approximated by FD approximations as follows.

$$U = \frac{\partial \Psi}{\partial Y} \quad \rightarrow U_{i,j} = \frac{\Psi_{i,j+1} - \Psi_{i,j-1}}{2h}$$

$$V = -\frac{\partial \Psi}{\partial X} \quad \rightarrow V_{i,j} = -\frac{\Psi_{i+1,j} - \Psi_{i-1,j}}{2h}$$

Rayleigh-Benard Instability in 2D

- The FD and SOR method can be used to solve the Poisson equation

$$\left(\frac{\partial^2}{\partial X^2} + \frac{\partial^2}{\partial Y^2} \right) \Psi = -\Omega$$

- The boundary conditions for Ψ are $\Psi = 0$ on the three solid walls since there is no net flow across these boundaries.
- In addition, $\Psi = 0$ along the Y -axis to make the fluid motion to its right the mirror image of that to its left.

Rayleigh-Benard Instability in 2D

- The symmetric distribution of θ and the antisymmetric distribution of Ψ about the Y axis result in the following boundary conditions for all values of j .

$$\theta_{m+1,j} = \theta_{m-1,j}$$

$$\Psi_{m,j} = 0$$

$$\Psi_{m+1,j} = -\Psi_{m-1,j}$$

$$U_{m+1,j} = -U_{m-1,j}$$

$$U_{m,j} = 0$$

$$V_{m,j} = \Psi_{m-1,j} / h$$

$$\Omega_{m,j} = 0$$

Rayleigh-Benard Instability in 2D

- To solve these equations

$$\frac{\partial \Omega}{\partial T} + \frac{\partial(U\Omega)}{\partial X} + \frac{\partial(V\Omega)}{\partial Y} = \text{Gr} \frac{\partial \theta}{\partial X} + \left(\frac{\partial^2}{\partial X^2} + \frac{\partial^2}{\partial Y^2} \right) \Omega$$

$$\frac{\partial \theta}{\partial T} + \frac{\partial(U\theta)}{\partial X} + \frac{\partial(V\theta)}{\partial Y} = \text{Pr}^{-1} \left(\frac{\partial^2}{\partial X^2} + \frac{\partial^2}{\partial Y^2} \right) \theta$$

the upwind FD scheme is used to approximate the nonlinear convection terms.

- We can write a program to solve the generic equation

$$\frac{\partial P}{\partial T} = - \frac{\partial(UP)}{\partial X} - \frac{\partial(VP)}{\partial Y} + A \frac{\partial Q}{\partial X} + B \left(\frac{\partial^2 P}{\partial X^2} + \frac{\partial^2 P}{\partial Y^2} \right)$$

Rayleigh-Benard Instability in 2D

- Let's define U_f and U_b as the average x -directional velocities evaluated at half a grid point forward and backward from the point (X_i, Y_j)

$$U_f = \frac{1}{2}(U_{i+1,j} + U_{i,j}), \quad U_b = \frac{1}{2}(U_{i,j} + U_{i-1,j})$$

- Similarly, V_f and V_b are defined as

$$V_f = \frac{1}{2}(V_{i,j+1} + V_{i,j}), \quad V_b = \frac{1}{2}(V_{i,j} + V_{i,j-1})$$

Rayleigh-Benard Instability in 2D

- For the convection terms, the upwind FD scheme is used to define

$$P1 = \left(U_f - |U_f| \right) P_{i+1,j} + \left(U_f + |U_f| - U_b + |U_b| \right) P_{i,j} - \left(U_b + |U_b| \right) P_{i-1,j}$$

$$P2 = \left(V_f - |V_f| \right) P_{i,j+1} + \left(V_f + |V_f| - V_b + |V_b| \right) P_{i,j} - \left(V_b + |V_b| \right) P_{i,j-1}$$

- The terms multiplied by A and B are approximated by central FD schemes:

$$P3 = Q_{i+1,j} - Q_{i-1,j}$$

$$P4 = P_{i+1,j} + P_{i-1,j} + P_{i,j+1} + P_{i,j-1} - 4P_{i,j}$$

- The time derivative is approximated by the forward FD scheme:

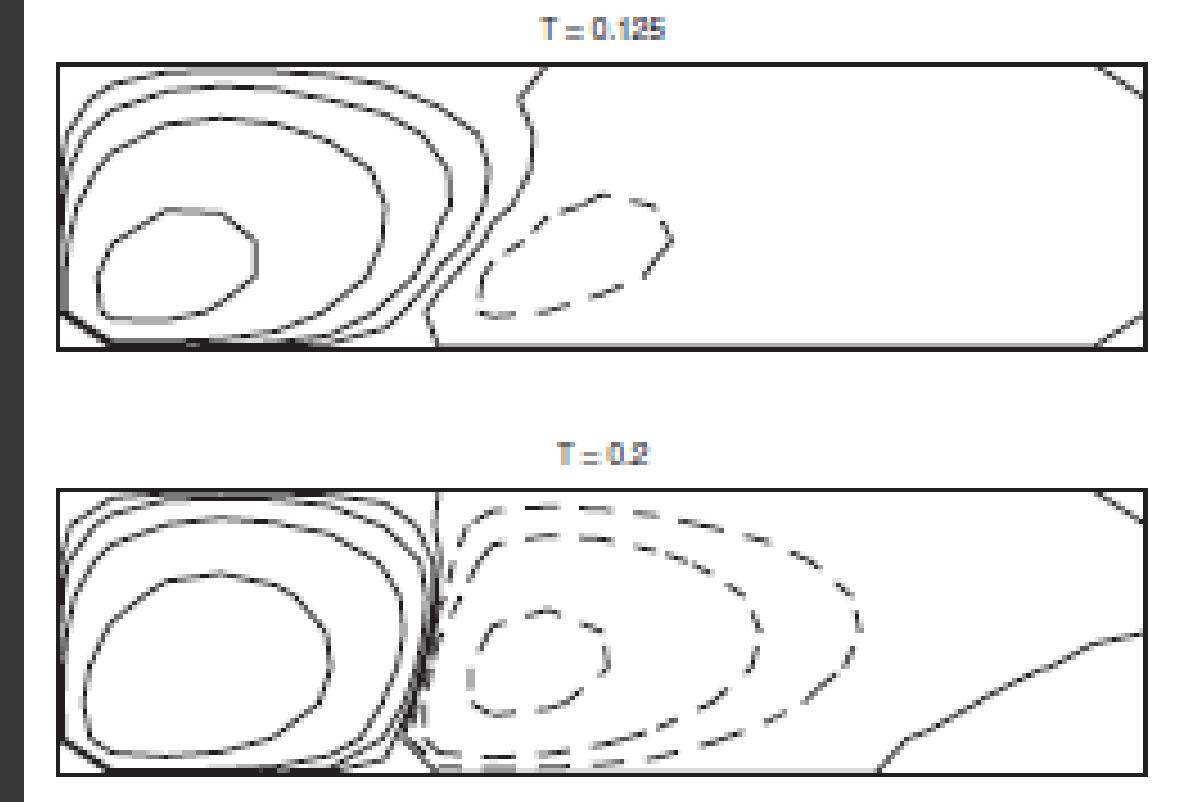
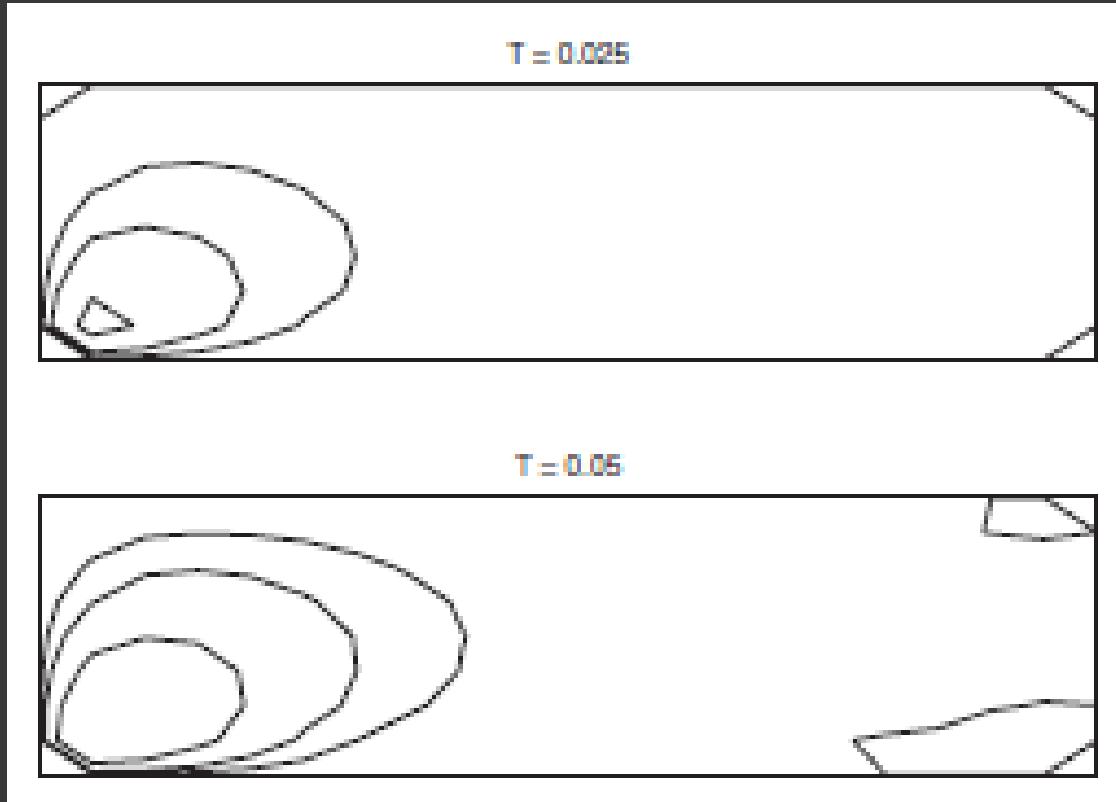
$$\left(\frac{\partial P}{\partial T} \right)_{i,j} = \frac{P'_{i,j} - P_{i,j}}{\Delta T}$$

Rayleigh-Benard Instability in 2D

- Here P' denote the value of P evaluated at time $T + \Delta T$.

$$P'_{i,j} = P_{i,j} + \frac{\Delta T}{2h} \left(-P1 - P2 + A \cdot P3 + 2B \frac{P4}{h} \right)$$

Rayleigh-Benard Instability in 2D



Incompressible Navier-Stokes Eq.

- 2D incompressible Navier-Stokes equations are given as

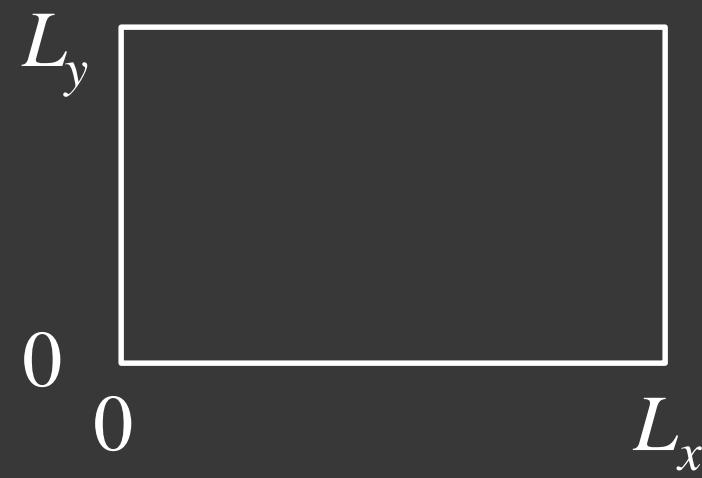
$$u_t + p_x = -\left(u^2\right)_x - \left(uv\right)_y + \frac{1}{\text{Re}} \left(u_{xx} + u_{yy}\right)$$

$$v_t + p_y = -\left(uv\right)_x - \left(v^2\right)_y + \frac{1}{\text{Re}} \left(v_{xx} + v_{yy}\right)$$

$$u_x + v_y = 0$$

incompressibility condition $\nabla \cdot \mathbf{v} = 0$

where Re is the Reynolds number.



No-Slip Boundary Conditions

- Consider the case in which all boundary conditions are no-slip.

$$u(x, L_y) = u_N(x)$$

$$v(x, L_y) = 0$$

$$u(x, 0) = u_S(x)$$

$$v(x, 0) = 0$$

$$u(0, y) = 0$$

$$v(0, y) = v_W(y)$$

$$u(L_x, y) = 0$$

$$v(L_x, y) = v_E(y)$$

Numerical Solution of N-V eq

- Using a splitting method, we can separately treat the advection terms, the diffusion terms, and the pressure gradient.
- The nonlinear advection is solved using an explicit scheme

$$\frac{u^* - u^n}{\Delta t} = - \left[(u^n)^2 \right]_x - \left[u^n v^n \right]_y$$

$$\frac{v^* - v^n}{\Delta t} = - \left[u^n v^n \right]_x - \left[(u^n)^2 \right]_y$$

- The diffusion equation is solved using an implicit (backward Euler) scheme

$$\frac{u^{**} - u^*}{\Delta t} = (u_{xx}^{**} + u_{yy}^{**}) / \text{Re}$$

$$\frac{v^{**} - v^*}{\Delta t} = (v_{xx}^{**} + v_{yy}^{**}) / \text{Re}$$

Pressure Correction

- The pressure is the Lagrange multiplier used to enforce the incompressibility condition.

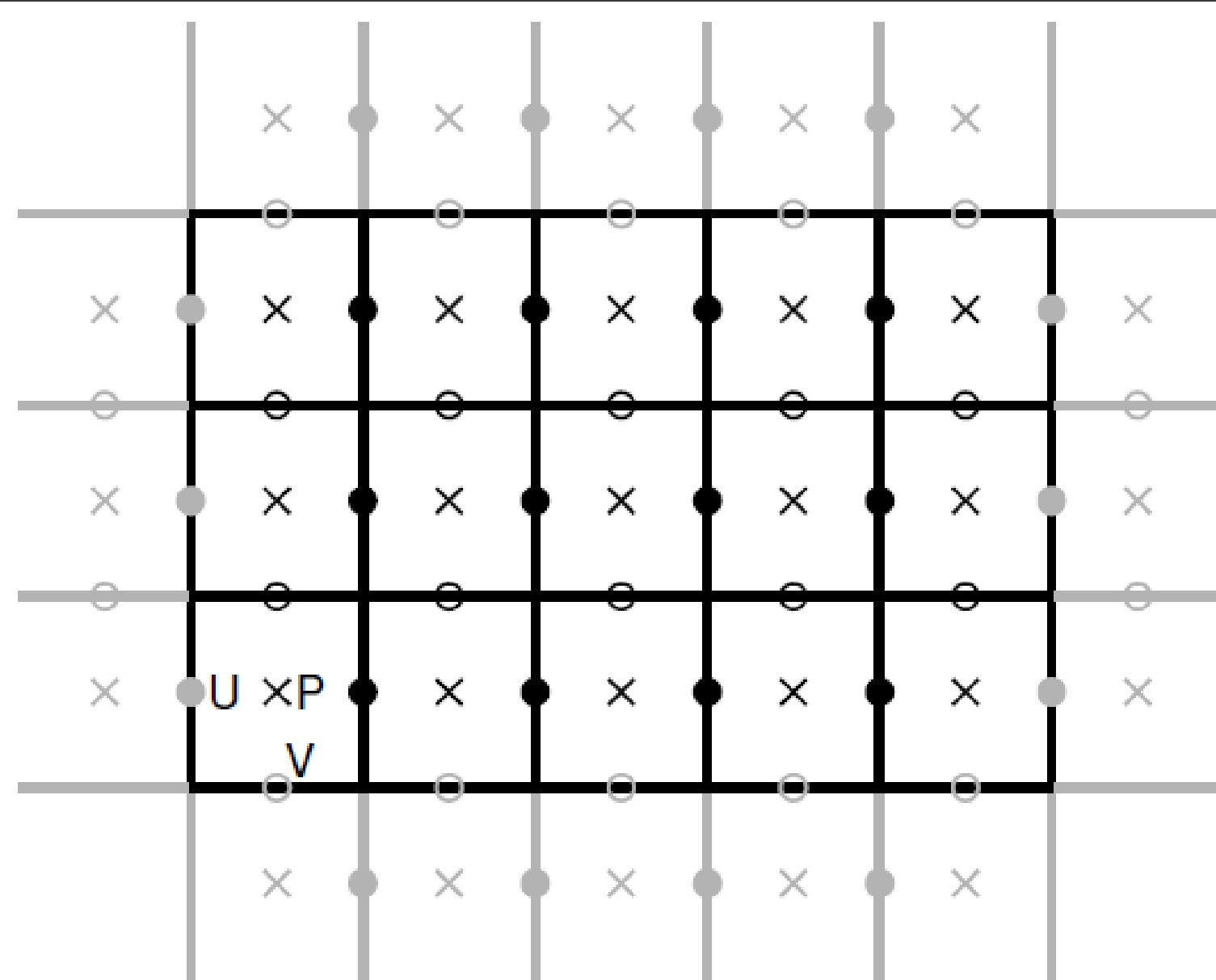
$$\frac{u^{n+1} - u^{**}}{\Delta t} = - \left(p^{n+1} \right)_x \quad \rightarrow \quad \frac{1}{\Delta t} (\mathbf{v}^{n+1} - \mathbf{v}^{**}) = - \nabla p^{n+1}$$
$$\frac{v^{n+1} - v^{**}}{\Delta t} = - \left(p^{n+1} \right)_y$$

- Applying the divergence yields $-\nabla^2 p^{n+1} = \frac{1}{\Delta t} (\nabla \cdot \mathbf{v}^{n+1} - \nabla \cdot \mathbf{v}^n) = - \frac{1}{\Delta t} \nabla \cdot \mathbf{v}^n$
- Solve the Poisson equation for p^{n+1} and then update the velocity field by

$$\mathbf{v}^{n+1} = \mathbf{v}^{**} - \Delta t \nabla p^{n+1}$$

- This is called the pressure projection method.

Staggered Grid



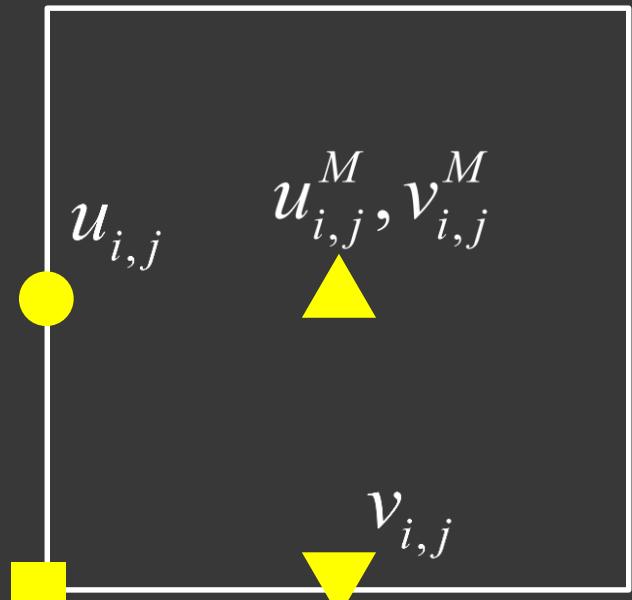
The stream function q used for visualizing streamlines is also computed by solving the Poisson equation

$$\nabla^2 q^n = -\nabla \times \mathbf{v}^n$$

where q^n are defined on the cell corners.

Nonlinear Advection: Revisited

Let $u_{i,j}^M = \frac{u_{i,j} + u_{i+1,j}}{2}$, $v_{i,j}^M = \frac{v_{i,j+1} + v_{i,j}}{2}$, $u_{i,j}^C = \frac{u_{i,j-1} + u_{i,j}}{2}$, $v_{i,j}^C = \frac{v_{i-1,j} + v_{i,j}}{2}$



$$\frac{u_{i,j}^* - u_{i,j}^n}{\Delta t} = - \frac{\left(u_{i,j}^M\right)^2 - \left(u_{i-1,j}^M\right)^2}{\Delta x} - \frac{u_{i,j+1}^C v_{i,j+1}^C - u_{i,j}^C v_{i,j}^C}{\Delta y}$$

$$\frac{v_{i,j}^* - v_{i,j}^n}{\Delta t} = - \frac{u_{i+1,j}^C v_{i+1,j}^C - u_{i,j}^C v_{i,j}^C}{\Delta x} - \frac{\left(v_{i,j}^M\right)^2 - \left(v_{i-1,j}^M\right)^2}{\Delta y}$$

An upwind scheme should be used in this case.
See Seibold (2008) for more details.

Boundary Conditions in 2D Flow

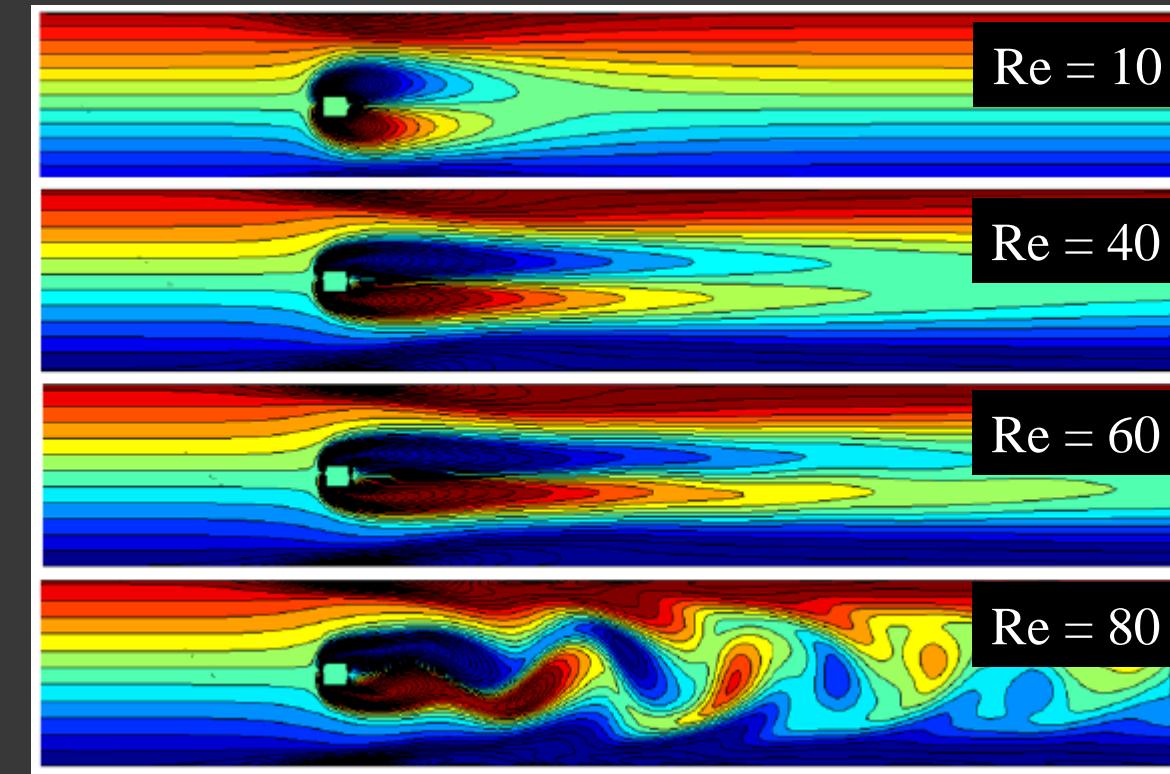
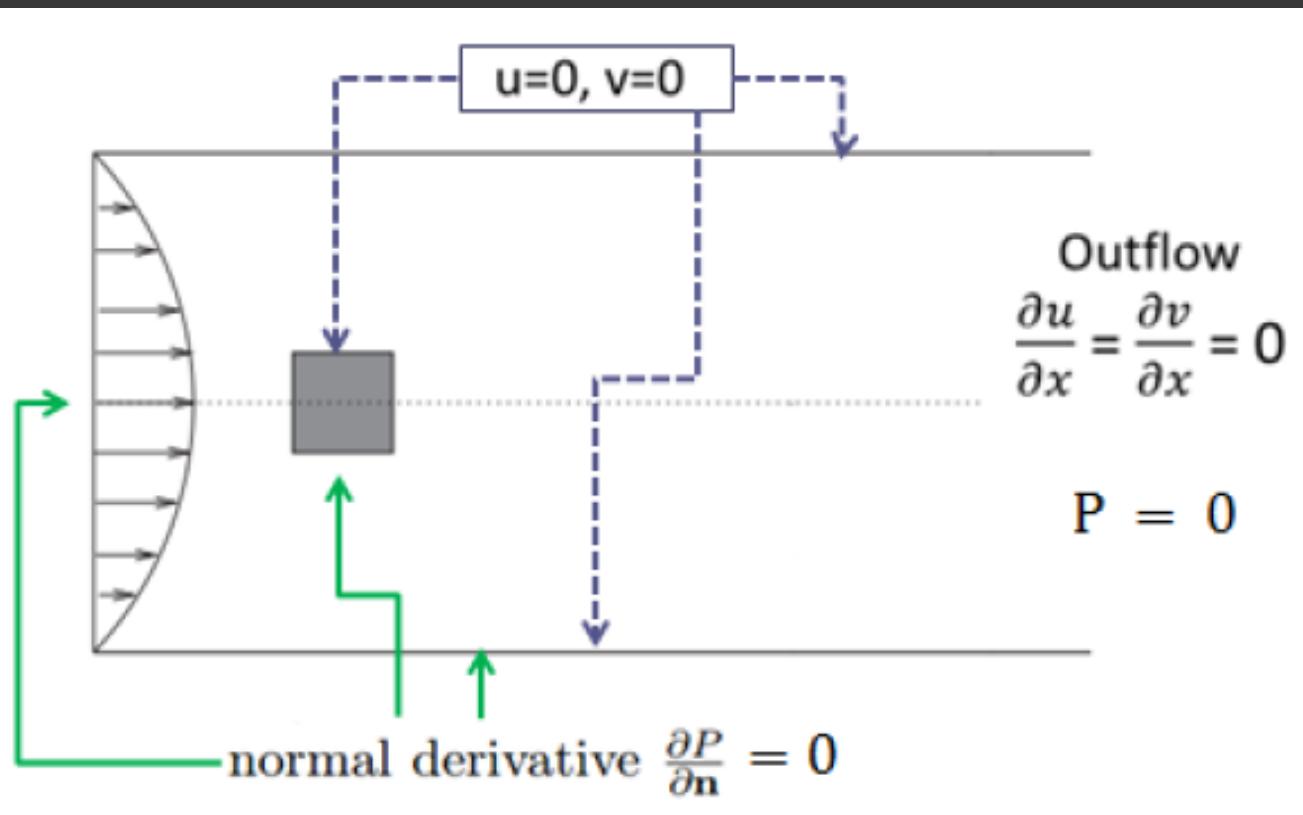
- Suppose that the velocity inlet boundary condition is at the left boundary and the pressure outlet boundary condition is at the right boundary.
- At the **velocity inlet** BC, we have $u = u_0$ and $v = v_0$.
- At the **pressure outlet** BC, we have

$$\frac{1}{\text{Re}} \frac{\partial u}{\partial x} - p = 0 \quad \text{and} \quad \frac{\partial v}{\partial x} = 0$$

- In a channel flow, no fluid crosses the top and bottom boundaries.
- If the **no-slip** condition is used, then $u = v = 0$.

Flow Past a Square Cylinder

- A flow past a square cylinder can be simulated by solving the 2D incompressible Navier-Stokes equation given previously using the boundary conditions given the below figure.



2D Smoke Simulation

- A 2D simulation of smoke can be performed by solving the system

$$\mathbf{u}_t + (\mathbf{u} \cdot \nabla) \mathbf{u} = -\nabla p / \rho_0 + \nu \nabla^2 \mathbf{u} + (\alpha s - \beta(T - T_{\text{amb}})) g$$

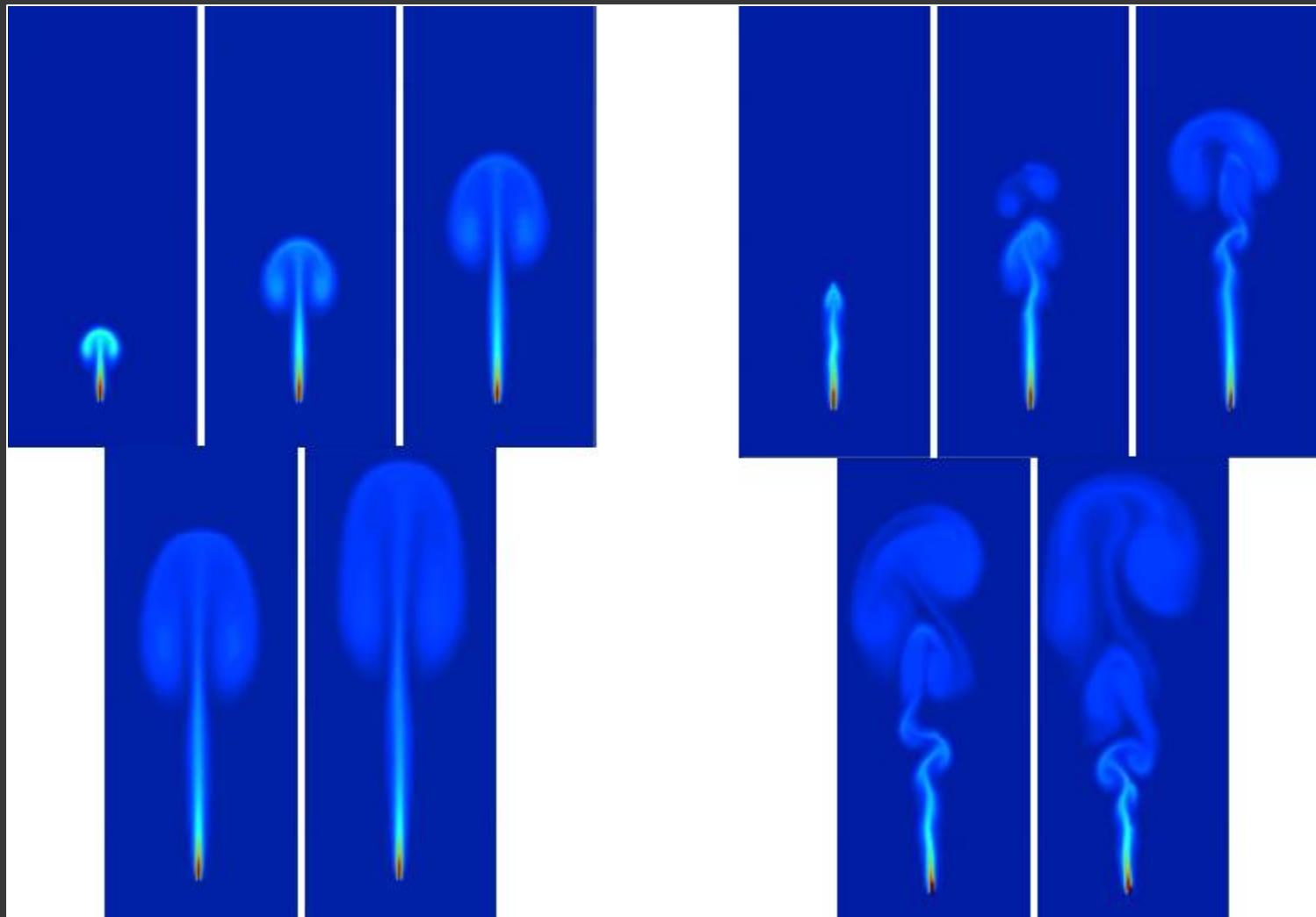
$$\nabla \cdot \mathbf{u} = 0$$

$$T_t + (\mathbf{u} \cdot \nabla) T = D_T \nabla^2 T + r_T (T_{\text{source}} - T)$$

$$s_t + (\mathbf{u} \cdot \nabla) s = D_s \nabla^2 s + r_s$$

where \mathbf{u} is fluid velocity, p pressure, T temperature, T_{source} temperature at the source point, T_{amb} the ambient temperature, s smoke concentration, ρ_0 the smoke-free air density at ambient temperature, g gravity, D_T diffusion coefficient of temperature, D_s diffusion coefficient of smoke concentration, r_T the rate of heat release, r_s the rate of smoke release.

2D Smoke Simulation



$$\nu = 10^{-3}$$

$$\nu = 10^{-5}$$

Exercise: 1D Diffusion

Solve the 1D diffusion equation

$$\frac{\partial u}{\partial t} = D \frac{\partial^2 u}{\partial x^2}$$

using an implicit FD scheme

$$\frac{u_i^n - u_i^{n-1}}{\Delta t} = D \left(\frac{u_{i-1}^n - 2u_i^n + u_{i+1}^n}{h^2} \right)$$

$$u_i^n - \frac{D\Delta t}{h^2} (u_{i-1}^n - 2u_i^n + u_{i+1}^n) = u_i^{n-1}$$

$$\alpha u_{i-1}^n + \beta u_i^n + \alpha u_{i+1}^n = u_i^{n-1}$$

$$\alpha = -\frac{D\Delta t}{h^2}, \beta = 1 + \frac{2D\Delta t}{h^2}$$

Exercise: 2D Diffusion

Solve the 2D diffusion equation

$$\frac{\partial u}{\partial t} = D \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right)$$

using an implicit FD scheme

$$\frac{u_{i,j}^n - u_{i,j}^{n-1}}{\Delta t} = D \left(\frac{u_{i-1,j}^n - 2u_{i,j}^n + u_{i+1,j}^n}{h^2} + \frac{u_{i,j-1}^n - 2u_{i,j}^n + u_{i,j+1}^n}{h^2} \right)$$

$$u_{i,j}^n - \frac{D\Delta t}{h^2} (u_{i-1,j}^n + u_{i+1,j}^n + u_{i,j-1}^n + u_{i,j+1}^n - 4u_i^n) = u_i^{n-1}$$

$$\alpha u_{i-1,j}^n + \alpha u_{i+1,j}^n + \alpha u_{i,j-1}^n + \alpha u_{i,j+1}^n + \beta u_{i,j}^n = u_i^{n-1}$$

$$\alpha = -\frac{D\Delta t}{h^2}, \beta = 1 + \frac{4D\Delta t}{h^2}$$

Inviscid Burgers' Equation

- The inviscid Burgers' equation governing a nonlinear convection is

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} = 0$$

where u is the fluid velocity.

- Consider the Taylor series expansion

$$u_i^{n+1} = u_i^n + (u_t)_i^n \Delta t + (u_{tt})_i^n \frac{\Delta t^2}{2} + O(\Delta t^3)$$

where $u_t = \frac{\partial u}{\partial t}$, $u_{tt} = \frac{\partial^2 u}{\partial t^2}$

- Let's approximate u_{tt} as $(u_{tt})_i^n = \frac{(u_t)_i^n - (u_t)_i^{n-1}}{\Delta t} + O(\Delta t)$

Inviscid Burgers' Equation

- The Taylor series expansion can then be written as

$$u_i^{n+1} = u_i^n + (u_t)_i^n \Delta t + \left[(u_t)_i^n - (u_t)_i^{n-1} \right] \frac{\Delta t}{2} + O(\Delta t^3)$$

- According to the inviscid Burgers' equation,

$$\frac{\partial u}{\partial t} = -u \frac{\partial u}{\partial x}$$

- We then obtain an Adams-Bashforth scheme

$$\frac{u_i^{n+1} - u_i^n}{\Delta t} = \frac{3}{2} \left(-u \frac{\partial u}{\partial x} \right)_i^n - \frac{1}{2} \left(-u \frac{\partial u}{\partial x} \right)_i^{n-1} + O(\Delta t^2)$$

- The spatial derivatives can be approximated using the second-order centered FD approximation.

Inviscid Burgers' Equation

- We then obtain an explicit second-order numerical scheme

$$\frac{u_i^{n+1} - u_i^n}{\Delta t} = \frac{3}{2} \left[-u_i^n \left(\frac{u_{i+1}^n - u_{i-1}^n}{2\Delta x} \right) \right] - \frac{1}{2} \left[-u_i^{n-1} \left(\frac{u_{i+1}^{n-1} - u_{i-1}^{n-1}}{2\Delta x} \right) \right] + O(\Delta x^2, \Delta t^2)$$

- This scheme is unconditionally unstable but the instability remains bounded if the Courant number satisfies the condition

$$C \equiv \frac{u_{\max} \Delta t}{\Delta x} \leq 1 \quad \leftrightarrow \quad \Delta t \leq \frac{\Delta x}{u_{\max}}$$

- This scheme requires initial velocity field at two time steps.
- We can use the explicit Euler method to obtain the field at the second step as

$$u_i^1 = u_i^0 - \Delta t \left[u_i^0 \left(\frac{u_{i+1}^0 - u_{i-1}^0}{2\Delta x} \right) \right] + O(\Delta x^2, \Delta t^2)$$

Viscous Burgers' Equation

- The viscous Burgers' equation is a nonlinear convection-diffusion equation

$$\frac{\partial u}{\partial t} = -u \frac{\partial u}{\partial x} + \nu \frac{\partial^2 u}{\partial x^2} \equiv H$$

- The corresponding Adams-Bashforth scheme with central FD in space for this case is

$$\frac{u_i^{n+1} - u_i^n}{\Delta t} = \frac{3}{2} H_i^n - \frac{1}{2} H_i^{n-1} + O(\Delta x^2, \Delta t^2)$$

- Using von Neumann analysis, the convective and diffusive stability conditions are

$$\frac{u_{\max} \Delta t}{\Delta x} \leq 1, \quad \frac{\nu \Delta t}{\Delta x^2} \leq \frac{1}{2}$$

- As a result, the time step must satisfy $\Delta t \leq \min\left(\frac{\Delta x}{u_{\max}}, \frac{\Delta x^2}{2\nu}\right)$

Exercise: Inviscid Burger's Eq.

Solve the initial value problem

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} = 0, \quad x \in [0, 1]$$

$$u(x, 0) = 0.1 + 0.1e^{-1000(x-0.2)^2}$$

using the numerical scheme

$$u_i^{n+1} = u_i^n - \frac{\Delta t}{4\Delta x} \left[3u_i^n (u_{i+1}^n - u_{i-1}^n) - u_i^{n-1} (u_{i+1}^{n-1} - u_{i-1}^{n-1}) \right]$$

$$u_i^1 = u_i^0 - \Delta t \left[u_i^0 \left(\frac{u_{i+1}^0 - u_{i-1}^0}{2\Delta x} \right) \right]$$

$$\Delta t \leq \Delta x / u_{\max}$$

Exercise: Viscous Burger's Eq.

Solve the initial value problem

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} = \nu \frac{\partial^2 u}{\partial x^2}, \quad x \in [0, 1], \quad \nu = 10^{-4}$$
$$u(x, 0) = 0.1 + 0.1e^{-1000(x-0.2)^2}$$

using the numerical scheme

$$u_i^{n+1} = u_i^n + \frac{\Delta t}{2} (3H_i^n - H_i^{n-1}), \quad H_i^n = -u_i^n \left(\frac{u_{i+1}^n - u_{i-1}^n}{2\Delta x} \right) + \nu \left(\frac{u_{i+1}^n - 2u_i^n + u_{i-1}^n}{\Delta x^2} \right)$$

$$u_i^1 = u_i^0 + \Delta t \left[-u_i^0 \left(\frac{u_{i+1}^0 - u_{i-1}^0}{2\Delta x} \right) + \nu \left(\frac{u_{i+1}^0 - 2u_i^0 + u_{i-1}^0}{\Delta x^2} \right) \right]$$

$$\Delta t \leq \min \left(\frac{\Delta x}{u_{\max}}, \frac{\Delta x^2}{2\nu} \right)$$

Diffusion Equation

- Consider the diffusion equation

$$\frac{\partial u}{\partial t} = \nu \frac{\partial^2 u}{\partial x^2}$$

- Recall the Taylor series expansion

$$f(t_1) = f(t_2) + f'(t_2)(t_1 - t_2) + f''(t_2) \frac{(t_1 - t_2)^2}{2} + f'''(t_2) \frac{(t_1 - t_2)^3}{6} + \dots$$

- We can then expand u_i^n and u_i^{n+1} as follows.

$$u_i^{n+1} = u_i^n + (u_t)_i^n \Delta t + (u_{tt})_i^n \frac{\Delta t^2}{2} + (u_{ttt})_i^n \frac{\Delta t^3}{6} + \dots$$

$$u_i^n = u_i^{n+1} - (u_t)_i^{n+1} \Delta t + (u_{tt})_i^{n+1} \frac{\Delta t^2}{2} - (u_{ttt})_i^{n+1} \frac{\Delta t^3}{6} + \dots$$

Diffusion Equation

- Subtracting the last two equations yield

$$u_i^{n+1} - u_i^n = u_i^n - u_i^{n+1} + (u_t)_i^n \Delta t + (u_t)_i^{n+1} \Delta t + \\ (u_{tt})_i^n \frac{\Delta t^2}{2} - (u_{tt})_i^{n+1} \frac{\Delta t^2}{2} + (u_{ttt})_i^n \frac{\Delta t^3}{6} + (u_{ttt})_i^{n+1} \frac{\Delta t^3}{6} + \dots$$

- Substituting the expansion

$$(u_{tt})_i^{n+1} = (u_{tt})_i^n + (u_{ttt})_i^n \Delta t + O(\Delta t^2)$$

into the last equation yields

$$2(u_i^{n+1} - u_i^n) = (u_t)_i^n \Delta t + (u_t)_i^{n+1} \Delta t - (u_{ttt})_i^n \frac{\Delta t^3}{6} + \dots$$

Crank-Nicolson Scheme

- Rearranging the last equation yields

$$\frac{u_i^{n+1} - u_i^n}{\Delta t} = \frac{1}{2} (u_t)_i^n + \frac{1}{2} (u_t)_i^{n+1} \Delta t + O(\Delta t^2)$$

- Substituting $u_t = vu_{xx}$ into the last equation yields

$$\frac{u_i^{n+1} - u_i^n}{\Delta t} = \frac{1}{2} (vu_{xx})_i^n + \frac{1}{2} (vu_{xx})_i^{n+1} \Delta t + O(\Delta t^2)$$

- Approximating the spatial derivative by second-order central difference yields the Crank-Nicolson scheme

$$\frac{u_i^{n+1} - u_i^n}{\Delta t} = \frac{\nu}{2\Delta x^2} (u_{i+1}^{n+1} - 2u_i^{n+1} + u_{i-1}^{n+1} + u_{i+1}^n - 2u_i^n + u_{i-1}^n) + O(\Delta x^2, \Delta t^2)$$

Crank-Nicolson Scheme

- Let $\alpha = v\Delta t/\Delta x^2$. The Crank-Nicolson scheme can be written as

$$-\frac{\alpha}{2}u_{i-1}^{n+1} + (1+\alpha)u_i^{n+1} - \frac{\alpha}{2}u_{i+1}^{n+1} = \frac{\alpha}{2}u_{i-1}^n + (1-\alpha)u_i^n + \frac{\alpha}{2}u_{i+1}^n$$

- Let's apply the Crank-Nicolson method to the Burgers equation

$$u_t = -uu_x + vu_{xx}$$

- Substituting the last equation into the Crank-Nicolson scheme yields

$$\frac{u_i^{n+1} - u_i^n}{\Delta t} = \frac{1}{2}(u_t)_i^n + \frac{1}{2}(u_t)_i^{n+1} \Delta t = \frac{1}{2}(-uu_x + vu_{xx})_i^n + \frac{1}{2}(-uu_x + vu_{xx})_i^{n+1} \Delta t$$

- Using the central difference on the convection term

$$(uu_x)_i^{n+1} = u_i^{n+1} \left(\frac{u_{i+1}^{n+1} - u_{i-1}^{n+1}}{2\Delta x} \right)$$

leads to a nonlinear difference equation which is more difficult to solve.

Adams-Bashforth-Crank-Nicolson Scheme

- A more popular numerical scheme for a convection-diffusion equation is a semi-implicit Adams-Bashforth-Crank-Nicolson scheme.
- The explicit Adams-Bashforth scheme is used for the convection term while the Crank-Nicolson scheme is used for the diffusion term.
- The Burgers' equation can be written as $u_t = -\frac{1}{2} \left(u^2 \right)_x + vu_{xx}$
- The explicit Adams-Bashforth scheme for the convection term is

$$\frac{u_i^{n+1} - u_i^n}{\Delta t} = \frac{3}{2} \left(-\frac{1}{2} \frac{\partial}{\partial x} \left(u^2 \right) \right)_i^n - \frac{1}{2} \left(-\frac{1}{2} \frac{\partial}{\partial x} \left(u^2 \right) \right)_i^{n-1} + O(\Delta t^2)$$

- The implicit Crank-Nicolson scheme for the diffusion term is

$$\frac{u_i^{n+1} - u_i^n}{\Delta t} = \frac{1}{2} \left(vu_{xx} \right)_i^n + \frac{1}{2} \left(vu_{xx} \right)_i^{n+1} \Delta t + O(\Delta t^2)$$

Adams-Bashforth-Crank-Nicolson Scheme

- Combining the two schemes yields the semi-implicit second-order scheme

$$\begin{aligned}\frac{u_i^{n+1} - u_i^n}{\Delta t} = & \frac{3}{2} \left(-\frac{1}{2} \frac{\partial}{\partial x} (u^2) \right)_i^n - \frac{1}{2} \left(-\frac{1}{2} \frac{\partial}{\partial x} (u^2) \right)_i^{n-1} \\ & + \frac{1}{2} (v u_{xx})_i^n + \frac{1}{2} (v u_{xx})_i^{n+1} + O(\Delta x^2, \Delta t^2)\end{aligned}$$

where the spatial derivatives are approximated by second-order central FD.

- Rearranging the equation yields

$$u_i^{n+1} - \frac{v \Delta t}{2} (u_{xx})_i^{n+1} = u_i^n - \frac{3 \Delta t}{4} \left((u^2)_x \right)_i^n + \underbrace{\frac{\Delta t}{4} \left((u^2)_x \right)_i^{n-1} + \frac{v \Delta t}{2} (u_{xx})_i^n}_{\text{RHS}_i^n}$$

Adams-Bashforth-Crank-Nicolson Scheme

- The semi-implicit scheme can then be written as

$$-\frac{\alpha}{2}u_{i-1}^{n+1} + (\alpha + 1)u_i^{n+1} - \frac{\alpha}{2}u_{i+1}^{n+1} = \text{RHS}_i^n$$

where $\text{RHS}_i^n = \frac{\alpha}{2}(u_{i-1}^n + u_{i+1}^n) + (1 - \alpha)u_i^n$

$$-3\beta \left[(u_{i+1}^n)^2 - (u_{i-1}^n)^2 \right] + \beta \left[(u_{i+1}^{n-1})^2 - (u_{i-1}^{n-1})^2 \right]$$

$$\alpha = \frac{v\Delta t}{\Delta x^2}, \beta = \frac{\Delta t}{8\Delta x}$$

- This scheme is stable when $\Delta t \leq \Delta x/u_{\max}$.
- The corresponding tridiagonal linear system can be efficiently solved using the Thomas algorithm.

Primitive-Variable Formulation

- Consider the incompressible Navier-Stokes equations

$$\nabla \cdot \mathbf{v} = 0$$

$$\mathbf{v}_t + \mathbf{v} \cdot \nabla \mathbf{v} = -\nabla P + \frac{1}{\text{Re}} \nabla^2 \mathbf{v}$$

- Here, $P = p/\rho$, where p is thermodynamic pressure.
- Nondimensionalization was performed using the characteristic length L and characteristic velocity U .
- The Reynolds number is defined as $\text{Re} = UL/\nu$.
- Here, we will use the projection method to solve the incompressible Navier-Stokes equations.

Projection Method

- Let's define \mathbf{H} as follows.

$$\mathbf{H} = \mathbf{v} \cdot \nabla \mathbf{v} = \nabla \cdot (\mathbf{v}\mathbf{v}) - \mathbf{v} \nabla \cdot \mathbf{v} = \nabla \cdot (\mathbf{v}\mathbf{v}) \quad \text{since } \nabla \cdot \mathbf{v} = 0$$

- The projection method first splits the Navier-Stokes equation into

$$\mathbf{v}_t = -\mathbf{H} + \nabla^2 \mathbf{v} / \text{Re}$$

$$\mathbf{v}_t = -\nabla P$$

- The first equation is solved using the semi-implicit scheme presented previously:

$$\frac{\mathbf{v}^* - \mathbf{v}^n}{\Delta t} = -\frac{3}{2} \mathbf{H}^n + \frac{1}{2} \mathbf{H}^{n-1} + \frac{1}{2 \text{Re}} \nabla^2 (\mathbf{v}^* + \mathbf{v}^n)$$

- Next, the second equation is solved using the implicit scheme

$$\frac{\mathbf{v}^{n+1} - \mathbf{v}^*}{\Delta t} = -\nabla P^{n+1}$$

Projection Method

- Applying divergence to the last equation yields

$$\frac{\nabla \cdot \mathbf{v}^{n+1} - \nabla \cdot \mathbf{v}^*}{\Delta t} = -\nabla \cdot \nabla P^{n+1}$$

- We want \mathbf{v}^{n+1} to satisfy the incompressibility condition, i.e., $\nabla \cdot \mathbf{v}^{n+1} = 0$
- Thus, we obtain the Poisson equation

$$\nabla^2 P^{n+1} = \frac{\nabla \cdot \mathbf{v}^*}{\Delta t}$$

- After solving the Poisson equation for P^{n+1} , the velocity \mathbf{v}^{n+1} is then updated by

$$\mathbf{v}^{n+1} = \mathbf{v}^* - \Delta t \nabla P^{n+1}$$

2D Incompressible Navier-Stokes Eq.

- 2D incompressible Navier-Stokes equations are given as

$$u_x + v_y = 0$$

$$u_t = -\left(u^2\right)_x - \left(uv\right)_y + \frac{1}{\text{Re}} \left(u_{xx} + u_{yy}\right) - P_x$$

$$v_t = -\left(uv\right)_x - \left(v^2\right)_y + \frac{1}{\text{Re}} \left(v_{xx} + v_{yy}\right) - P_y$$

x-Momentum Equation

Terms in the *x*-momentum equation

$$u_t = -\left(u^2\right)_x - \left(uv\right)_y + \frac{1}{\text{Re}} \left(u_{xx} + u_{yy}\right) - P_x$$

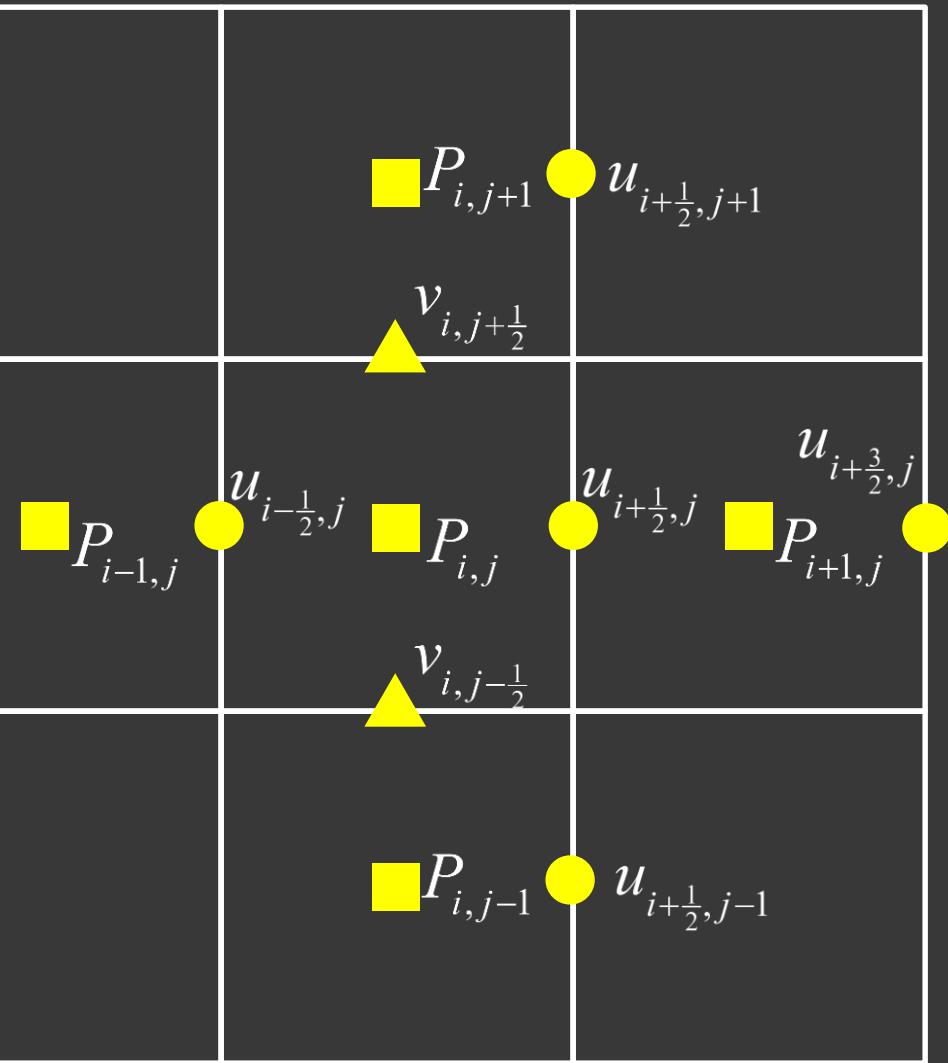
are computed as follows.

$$(u_t)_{i+\frac{1}{2},j}^{n+1} = \left(u_{i+\frac{1}{2},j}^{n+1} - u_{i+\frac{1}{2},j}^n \right) / \Delta t$$

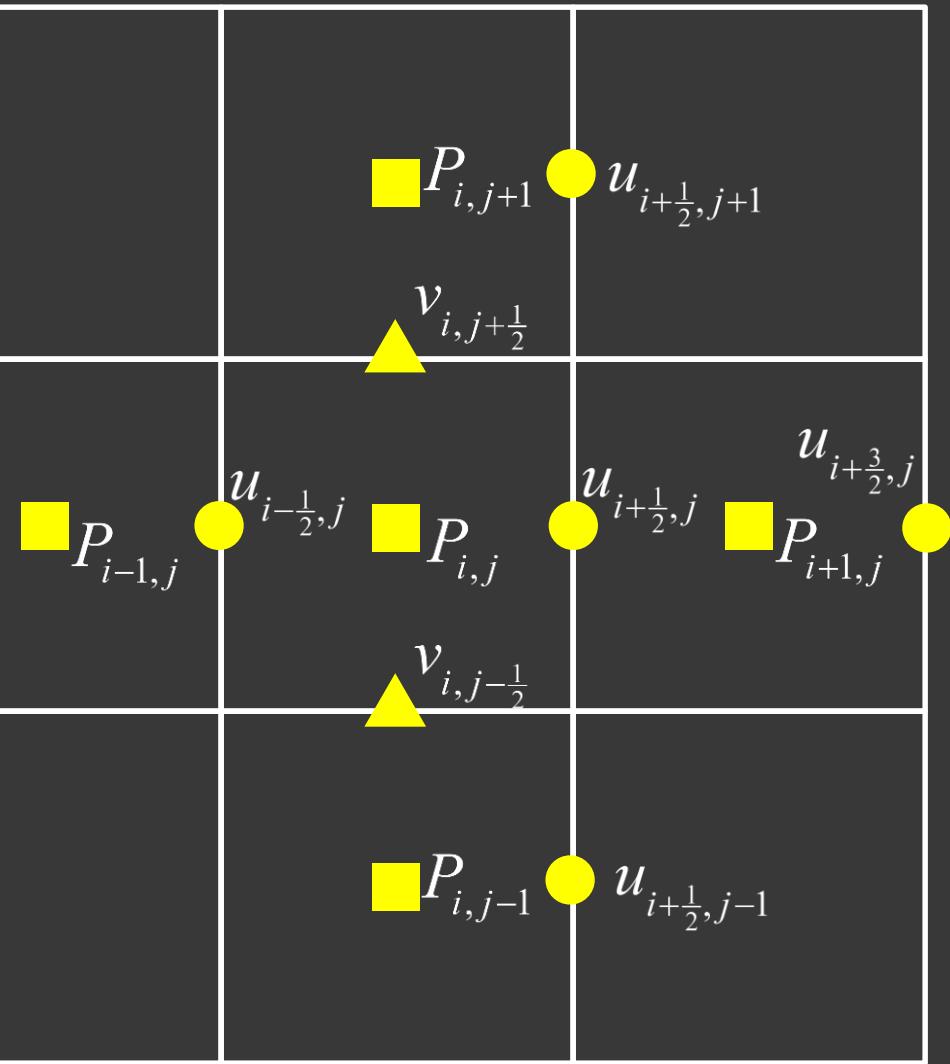
$$(u_{xx})_{i+\frac{1}{2},j}^{n+1} = \left(u_{i-\frac{1}{2},j}^{n+1} - 2u_{i+\frac{1}{2},j}^{n+1} + u_{i+\frac{3}{2},j}^{n+1} \right) / \Delta x^2$$

$$(u_{yy})_{i+\frac{1}{2},j}^{n+1} = \left(u_{i+\frac{1}{2},j-1}^{n+1} - 2u_{i+\frac{1}{2},j}^{n+1} + u_{i+\frac{1}{2},j+1}^{n+1} \right) / \Delta y^2$$

$$(P_x)_{i+\frac{1}{2},j}^{n+1} = \left(P_{i+1,j}^{n+1} - P_{i,j}^{n+1} \right) / \Delta x$$



x -Momentum Equation



$$\left((u^2)_x \right)_{i+\frac{1}{2},j}^n = \left((u_{i+1,j}^n)^2 - (u_{i,j}^n)^2 \right) / \Delta x$$

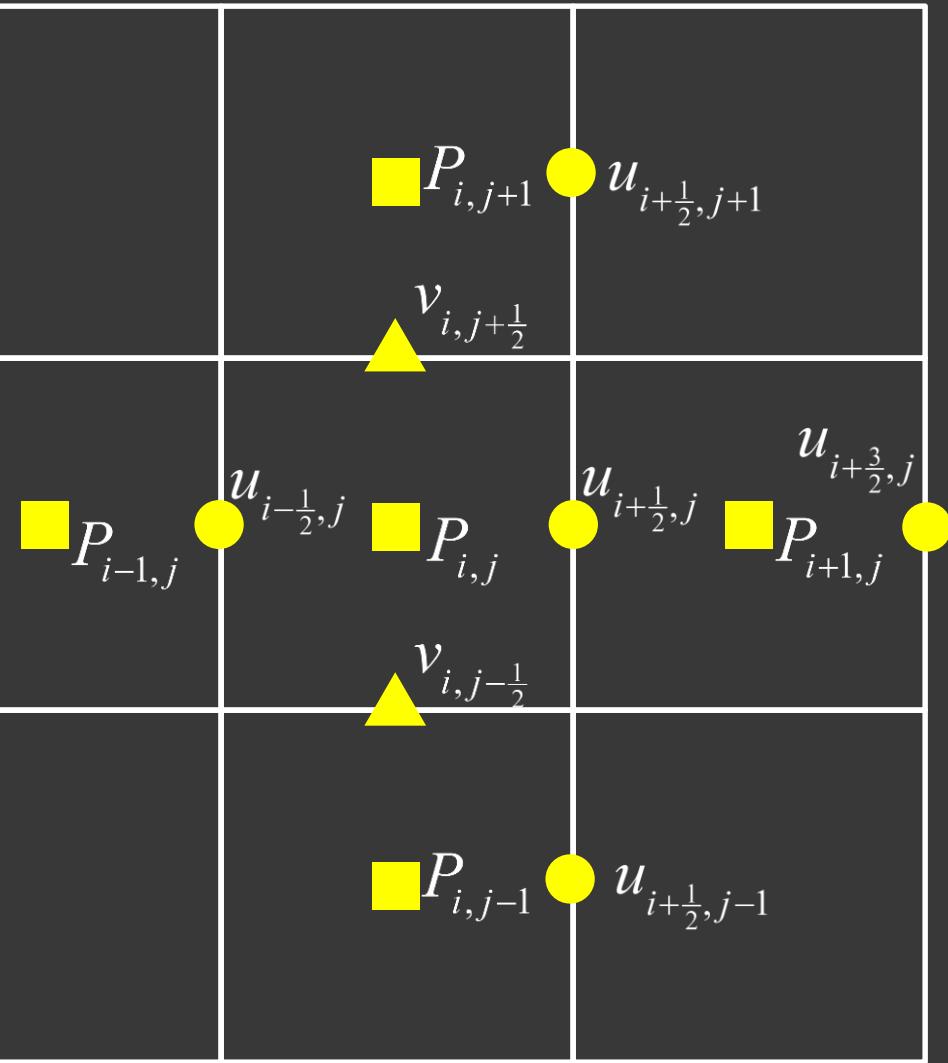
$u_{i+1,j}$ is not defined on a u node. So, it is defined as an average:

$$u_{i+1,j} = \frac{1}{2} (u_{i+1/2,j} + u_{i+3/2,j})$$

The term $(uv)_y$ will be evaluated as the product of averages:

$$\left((uv)_y \right)_{i+\frac{1}{2},j}^n = \left[(uv)_{i+\frac{1}{2},j+\frac{1}{2}} - (uv)_{i+\frac{1}{2},j-\frac{1}{2}} \right] / \Delta y$$

x -Momentum Equation



where

$$(uv)_{i+\frac{1}{2},j+\frac{1}{2}} = u_{i+\frac{1}{2},j+\frac{1}{2}} v_{i+\frac{1}{2},j+\frac{1}{2}}$$

$$(uv)_{i+\frac{1}{2},j-\frac{1}{2}} = u_{i+\frac{1}{2},j-\frac{1}{2}} v_{i+\frac{1}{2},j-\frac{1}{2}}$$

$$u_{i+\frac{1}{2},j+\frac{1}{2}} = \frac{1}{2} \left(u_{i+\frac{1}{2},j} + u_{i+\frac{1}{2},j+1} \right)$$

$$v_{i+\frac{1}{2},j+\frac{1}{2}} = \frac{1}{2} \left(v_{i,j+\frac{1}{2}} + v_{i+1,j+\frac{1}{2}} \right)$$

$$u_{i+\frac{1}{2},j-\frac{1}{2}} = \frac{1}{2} \left(u_{i+\frac{1}{2},j-1} + u_{i+\frac{1}{2},j} \right)$$

$$v_{i+\frac{1}{2},j-\frac{1}{2}} = \frac{1}{2} \left(v_{i,j-\frac{1}{2}} + v_{i+1,j-\frac{1}{2}} \right)$$

Velocity Boundary Conditions

- An explicit boundary condition on the pressure is not needed.
- Suppose we have a boundary condition for u on a horizontal wall as u_Γ .
- The value of u at a fictitious point can be computed from linear extrapolation

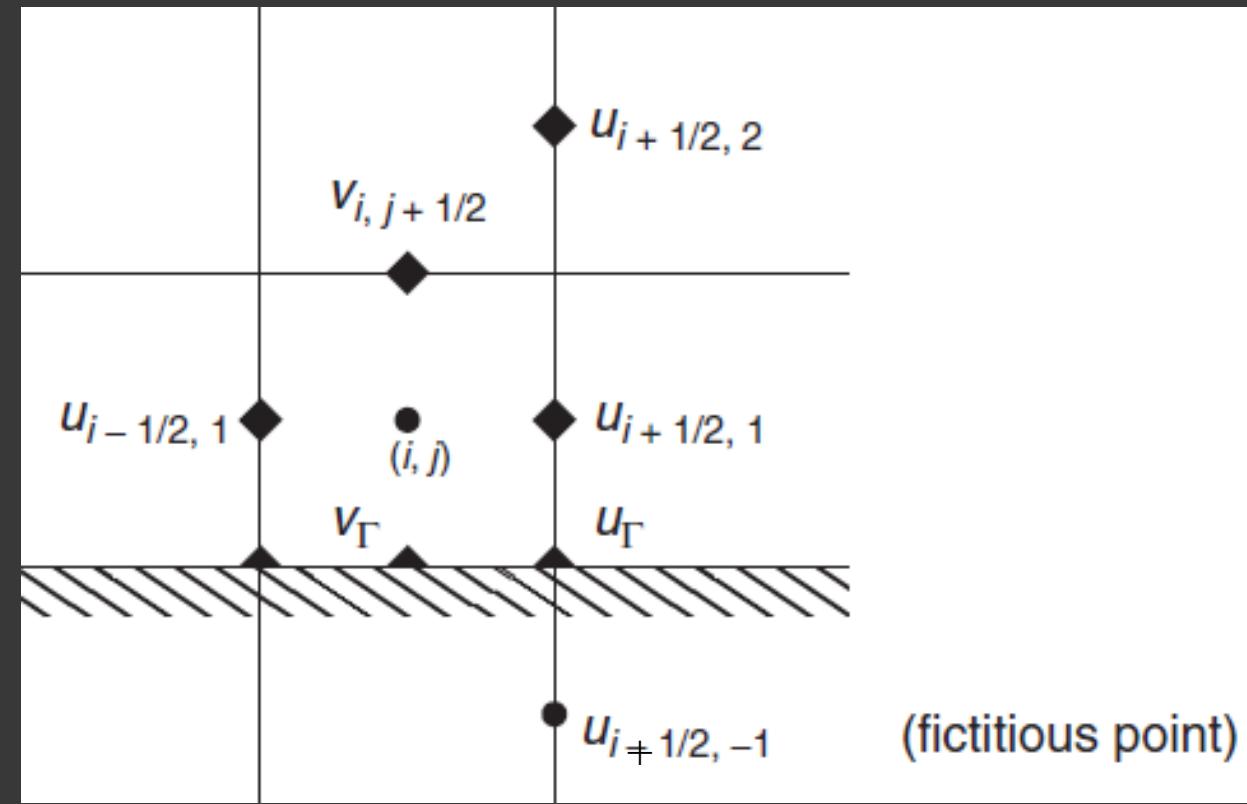
$$u_\Gamma = \frac{1}{2} \left(u_{i+\frac{1}{2},1} + u_{i+\frac{1}{2},-1} \right)$$

$$u_{i+\frac{1}{2},-1} = 2u_\Gamma - u_{i+\frac{1}{2},1}$$

or quadratic extrapolation

$$u_{i+\frac{1}{2},-1} = \frac{1}{3} \left(8u_\Gamma - 6u_{i+\frac{1}{2},1} + u_{i+\frac{1}{2},2} \right)$$

- For a stationary wall, $u_\Gamma = 0$.
- For a vertical wall, extrapolation formulas can be used for v .

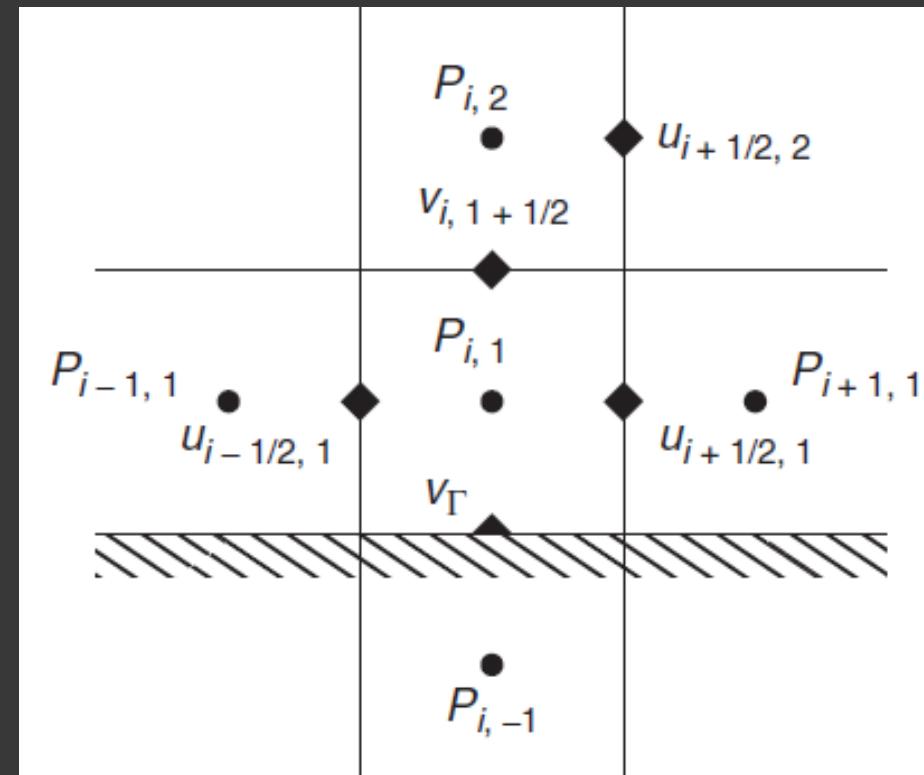


Pressure Boundary Conditions

- At a wall, the boundary condition for the pressure is the Neumann boundary condition $\partial P / \partial n = 0$
- The Poisson equation $\nabla^2 P^{n+1} = \frac{\nabla \cdot \mathbf{v}^*}{\Delta t}$ becomes

$$\frac{P_{i+1,1}^{n+1} - 2P_{i,1}^{n+1} + P_{i-1,1}^{n+1}}{\Delta x^2} + \frac{P_{i,2}^{n+1} - 2P_{i,1}^{n+1} + P_{i,-1}^{n+1}}{\Delta y^2} = \\ \frac{1}{\Delta t} \left[\frac{u_{i+\frac{1}{2},1}^* - u_{i-\frac{1}{2},1}^*}{\Delta x} + \frac{v_{i,1+\frac{1}{2}}^* - v_\Gamma^*}{\Delta y} \right]$$

$$P_{i,-1}^{n+1} = P_{i,1}^{n+1} \text{ from } \partial P / \partial n = 0$$



Vorticity-Stream Function Formulation

- Here we will derive the vorticity-stream function formulation of incompressible flows from the Navier-Stokes equation

$$\frac{\partial \mathbf{v}}{\partial t} + (\mathbf{v} \cdot \nabla) \mathbf{v} = -\nabla \left(\frac{p}{\rho} \right) + \nu \nabla^2 \mathbf{v}$$

- The convection term can be written as

$$(\mathbf{v} \cdot \nabla) \mathbf{v} = \nabla \left(\frac{1}{2} \mathbf{v} \cdot \mathbf{v} \right) - \mathbf{v} \times (\nabla \times \mathbf{v}) = \nabla \left(\frac{1}{2} \mathbf{v} \cdot \mathbf{v} \right) - \mathbf{v} \times \boldsymbol{\omega}$$

where $\boldsymbol{\omega} = \nabla \times \mathbf{v}$ is the vorticity.

- The Navier-Stokes equation can then be written as

$$\frac{\partial \mathbf{v}}{\partial t} + \nabla \left(\frac{1}{2} \mathbf{v} \cdot \mathbf{v} \right) - \mathbf{v} \times \boldsymbol{\omega} = -\nabla \left(\frac{p}{\rho} \right) + \nu \nabla^2 \mathbf{v}$$

Vorticity-Stream Function Formulation

- Taking curl of $\mathbf{v}_t + \nabla\left(\frac{1}{2}\mathbf{v} \cdot \mathbf{v}\right) - \mathbf{v} \times \boldsymbol{\omega} = -\nabla(p/\rho) + \nu\nabla^2\mathbf{v}$, we obtain

$$\boldsymbol{\omega}_t - \nabla \times (\mathbf{v} \times \boldsymbol{\omega}) = \nu \nabla^2 \boldsymbol{\omega}$$

- The gradient terms vanish since $\nabla \times \nabla f = \mathbf{0}$
- Using vector identities, we obtain

$$\nabla \times (\mathbf{v} \times \boldsymbol{\omega}) = \mathbf{v}(\nabla \cdot \boldsymbol{\omega}) - \boldsymbol{\omega}(\nabla \cdot \mathbf{v}) - (\mathbf{v} \cdot \nabla)\boldsymbol{\omega} + (\boldsymbol{\omega} \cdot \nabla)\mathbf{v}$$

$$\nabla \cdot \boldsymbol{\omega} = \nabla \cdot \nabla \times \mathbf{v} = 0 \quad \text{Divergence of curl of a vector is zero}$$

$$\nabla \cdot \mathbf{v} = 0 \quad \text{Incompressibility condition}$$

$$(\boldsymbol{\omega} \cdot \nabla)\mathbf{v} = 0 \quad \text{for 2D flows}$$

- The equation $\boldsymbol{\omega}_t - \nabla \times (\mathbf{v} \times \boldsymbol{\omega}) = \nu \nabla^2 \boldsymbol{\omega}$ then becomes the vorticity transport equation

$$\boldsymbol{\omega}_t + (\mathbf{v} \cdot \nabla)\boldsymbol{\omega} = \nu \nabla^2 \boldsymbol{\omega}$$

Vorticity-Stream Function Formulation

- In 2D flow in the x - y plane, only the z -component of the vorticity, denoted as ω , is nonzero. We then obtain the scalar equation

$$\omega_t + u\omega_x + v\omega_y = \nu(\omega_{xx} + \omega_{yy})$$

- The velocities u and v can be written in terms of the stream function as

$$u = \psi_y, \quad v = -\psi_x$$

- Substituting these into the definition of vorticity $\omega = v_x - u_y$ yields the Poisson equation

$$\nabla^2\psi = \psi_{xx} + \psi_{yy} = -\omega$$

- For the vorticity-stream function formulation, a collocated grid, in which all variables are at the same nodes, can be used.

Driven Cavity Problem

- The Navier-Stokes equation is nondimensionalized by the lid velocity U and the cavity height L .
- So, the Reynolds number is defined as $\text{Re} = UL/\nu$.
- Using the second-order central differencing for spatial derivatives and the Euler method for time integration, the vorticity transport equation becomes the difference equation

$$\frac{\omega_{i,j}^{n+1} - \omega_{i,j}^n}{\Delta t} + u_{i,j}^n \frac{\omega_{i+1,j}^n - \omega_{i-1,j}^n}{2h} + v_{i,j}^n \frac{\omega_{i,j+1}^n - \omega_{i,j-1}^n}{2h} = \frac{1}{h^2 \text{Re}} (\omega_{i+1,j}^n + \omega_{i-1,j}^n + \omega_{i,j+1}^n + \omega_{i,j-1}^n - 4\omega_{i,j}^n)$$

- Here, a square grid is used, i.e., $h = \Delta x = \Delta y$.

Driven Cavity Problem

- The Poisson equation for the stream function is approximated as the difference equation

$$\frac{\psi_{i+1,j}^{n+1} - 2\psi_{i,j}^{n+1} + \psi_{i-1,j}^{n+1}}{h^2} + \frac{\psi_{i,j+1}^{n+1} - 2\psi_{i,j}^{n+1} + \psi_{i,j-1}^{n+1}}{h^2} = -\omega_{i,j}^{n+1}$$

- After solving the discretized Poisson equation for the stream function, the velocity components are then updated using

$$u_{i,j}^{n+1} = \frac{\psi_{i,j+1}^{n+1} - \psi_{i,j-1}^{n+1}}{2h}, \quad v_{i,j}^{n+1} = -\frac{\psi_{i+1,j}^{n+1} - \psi_{i-1,j}^{n+1}}{2h}$$

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