

Technical Team

Nature of Invention: Process Flow Diagram and Mass Balance.

Applicant: GreenovateX

Inventors: Sumit Chouhan, Sanjeeta Singh

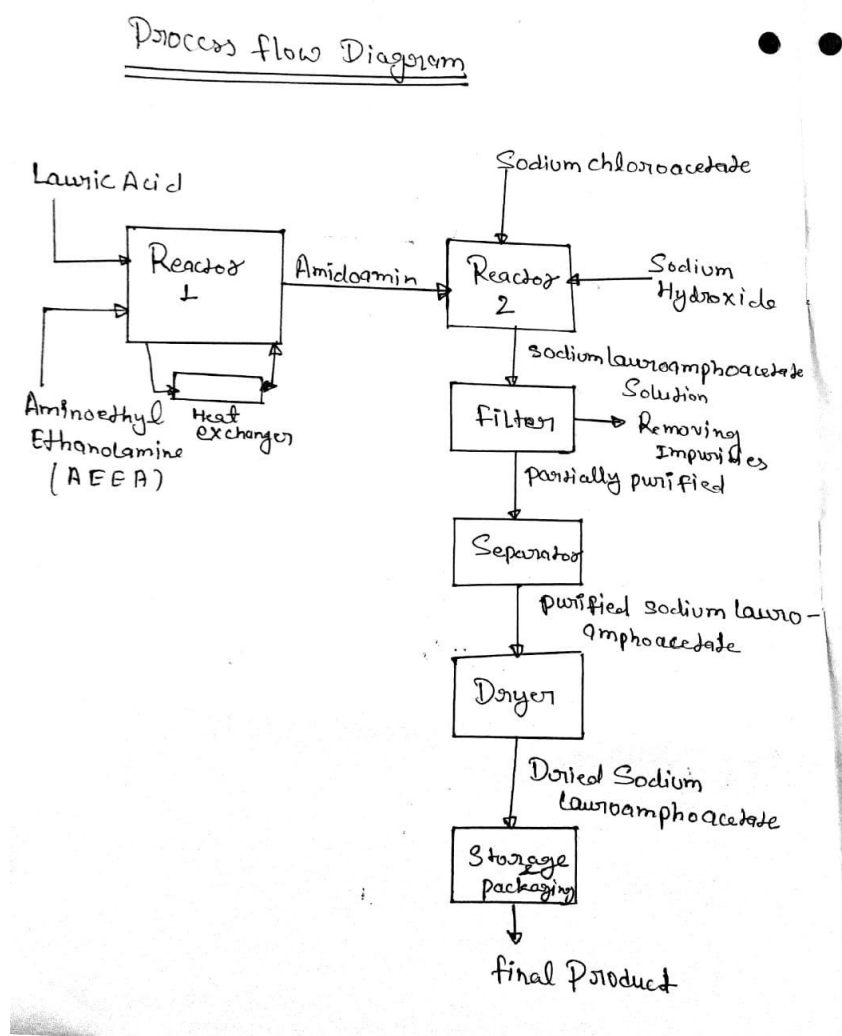
Chemical Formula: $C_{18}H_{35}N_2NaO_4$

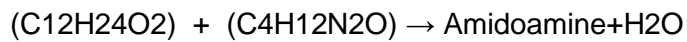
Chemical Name: Sodium Lauroamphoacetate

Process Title: Production of Sodium Lauroamphoacetate from Lauric Acid

Raw materials and chemicals Required: Lauric Acid, Sodium Chloroacetate, Ammonia, Coconut Oil and Water and pH Adjusters.

Process Description (Block diagram):



Step 1: Amidation Reaction (Formation of Amidoamine Intermediate)**Lauric Acid + AEEA \rightarrow Amidoamine + H₂O****Step 2: Carboxymethylation Reaction (Formation of Sodium Lauroamphoacetate)**Amidoamine + Sodium Monochloroacetate \rightarrow Sodium Lauroamphoacetate + NaCl**Material Balance:**

1. Reaction Equations for Production

Step: 1

Amidation Reaction (formation of Amidoamine Intermediate)

Lauric Acid + AEEA \rightarrow Amidoamine + H₂O

$C_{12}H_{24}O_2 + C_4H_{12}N_2O \rightarrow \text{Amidoamine} + H_2O$

Step: 2

Carboxymethylation Reaction (formation of Sodium Lauroamphoacetate)

Amidoamine + Sodium Monochloroacetate \rightarrow SL + NaCl

2. Data Provided

Total feed: 1000 kg/day

Reaction yield: 30%

Molecular Weights (MW):

Lauric Acid ($C_{12}H_{24}O_2$) = 200.32 g/mol

AEEA ($C_4H_8N_2O$) = 104.15 g/mol

Amidocamine intermediate = 286.47 g/mol

Sodium Monochloroacetate = 116.48 g/mol

Sodium Lauroamphoacetate = 368.48 g/mol

3. Mass flow Rate Calculation

Step 1

Assuming Lauric Acid makes up to 60% of the feed (600 kg/day)

$$\text{Moles of Lauric Acid} = \frac{600,000 \text{ g}}{200.32 \text{ g/mol}} = 2995 \text{ mol/kg}$$

Since the reaction is 1:1
required AEEA is also 2995 moles

$$\begin{aligned} \text{Mass of AEEA} &= 2995 \times 104.15 = 311,850 \text{ g} \\ &= 311.85 \text{ kg/day} \end{aligned}$$

Mass of Amidoamine Intermediate produced -

$$2995 \times 286.7 = 857,900 \text{ g} = 857.9 \text{ kg/day}$$

Mass of Water (by product) :-

$$2995 \times 18.015 = 53,950 \text{ g} = 53.95 \text{ kg/day}$$

~~Step 2~~ Amidation Reactor (R-101)

Mass processed for batch

$$\text{Lauric Acid (600) kg} + \text{AEEA (312) kg} = 912 \text{ kg}$$

$$\text{Density} \sim 900 \text{ kg/m}^3$$

$$\text{Volume for batch} = V = \frac{912}{900} = 1.01 \text{ m}^3$$

Considering 70% fill factor

$$V_{\text{reactor}} = \frac{1.01}{0.7} = 1.44 \text{ m}^3$$

final reactor Size Selection: 1.5 m³ Glass-lined
CS Reactor

Step 2. Operating Conditions: 80-100°C, atmospheric pressure.

Total mass input ~ 1100 kg

As Amidamine Intermediate reacts 1:1 with SMCA

Moles of SMCA = 2995 moles.

Mass of SMCA

$$= 2995 \times 116.48 = 348,840 \text{ g} = 348.84 \text{ kg/day}$$

Mass of Sodium Laurylsulfate (Final Product)

$$= 2995 \times 368.48 = 1,103,200 \text{ g} = 1103.2 \text{ kg/day}$$

Mass of NaCl (by product)

$$= 2995 \times 58.44 = 175,088 \text{ g} = 175.08 \text{ kg/day}$$

Carboxymethylation Reactor (R-102)

Mass processed for batch

$$\text{Amidamine (857.91g)} + \text{SMCA (348.81g)} = 1206.7\text{g}$$

$$\text{Density} \sim 950 \text{ kg/m}^3$$

Volume required for batch

$$V = \frac{1206.7}{950} = 1.27 \text{ m}^3$$

Total Volume Needed (Considering 70% fill factor)

$$V_{\text{reactor}} = \frac{1.27}{0.7} = 1.81 \text{ m}^3$$

Final reactor Size Selection : 2 m³ Glass-lined C.S Reactor

4. Mole fractions (final ^{product} moles)

$$\text{mole fraction of Sodium Laurylphosphate} = \frac{2995}{2995 + 2995} = 0.5$$

$$\text{mole fraction of NaCl} = \frac{2995}{2995 + 2995} = 0.5$$

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Filtration, Drying & Storage.

Filtration System : Nutsche Filter $\sim 1.5 m^3$
Evaporator for solvent removal $\sim 1.5 m^3$ capacity
Storage tanks $\sim 3 m^3$ for final product.

Capital cost (only for the reactor):

example:

Equipment	Design Capacity (L)	No. of units	Cost/unit (\$ for year 2014)	Total Cost (\$ for year 2014)
Amidation Reactor (Glass-Lined CS, R-101)	1500	1	30,000	30,000
Carboxymethylation Reactor (Glass-Lined CS, R-102)	2000	1	40,000	40,000
Total Estimated Cost	----	----	-----	70,000

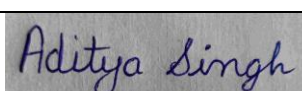
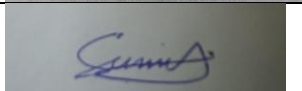
References: Provide reference for a research paper or an actual patent.

1. <http://www.matche.com/equipcost/Reacto.html>

List the contributions of each author:

- Sumit Chouhan : Reactor and equipment costing, Material Balance
- Sanjeeta: Block diagram

Sign the pdf and upload.

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