

Lecture 14 - Newtonian Fluids

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schedule

- 3 Nov - Newtonian Fluids
- 5 Nov - Experimental Rheology
- 10 Nov - Energy, Rotation, Vorticity
- 12 Nov - Compressible Flow, HW8 Due
- 17 Nov - Non-Newtonian Fluids

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- newtonian fluids
- flow conditions

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fluids in rigid motion

- We define a fluid as a material which is unable to resist shear stress at rest
- For a fluid in rigid body motion, the stress vector on any plane will be normal to that plane

$$T_{ij}n_j = \lambda n_i$$

- The symmetry of the stress tensor leads us to find that

$$T_{ij} = -p\delta_{ij}$$

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fluid compressibility

- Most liquids can be treated as incompressible in many fluid problems
- Their change in density is negligible under a wide range of pressures
- Most gases, however, must be treated as compressible
- Recall the conservation of mass

$$\frac{D}{Dt}\rho + \rho \frac{\partial v_k}{\partial x_k} = 0$$

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fluid compressibility

- Which for an incompressible material becomes

$$\frac{\partial v_k}{\partial x_k} = 0$$

- Density of an incompressible material can vary in space, as long as it does not vary in time

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- If we substitute $T_{ij} = -p\delta_{ij}$ into the equilibrium equations, we find

$$\frac{\partial p}{\partial x_i} = \rho B_i$$

- If gravity is the only body force and acts in x_3 , then pressure will only be a function of x_3 (for static fluid)
- If the fluid is in rigid body motion then we have

$$-\frac{\partial p}{\partial x_i} + \rho B_i = \rho a_i$$

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example

- You are planning to load your fish tank into your friend's car for transportation
- Your friend brags that he can accelerate from 0 to 60 in 5 seconds
- Assuming this is true, and your tank is 2'x4' and 2' deep, how deep can you fill the tank without allowing any spilling due to acceleration?

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- For a fluid in general motion, we de-compose the stress tensor into two portions

$$T_{ij} = -p\delta_{ij} + T'_{ij}$$

- Where T'_{ij} depends only on the rate of deformation and p is a scalar which does not depend on the rate of deformation

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newtonian fluids

- For a fluid to be Newtonian, we make two assumptions
- First, we assume that T'_{ij} is linearly dependent on D_{ij} and nothing else
- Second, we assume the fluid is isotropic
- This gives

$$T'_{ij} = \lambda D_{kk}\delta_{ij} + 2\mu D_{ij}$$

- If we consider a shear flow given by the velocity field

$$v_1 = f(x_2) \quad v_2 = v_3 = 0$$

- We have a rate of deformation tensor with

$$D_{12} = \frac{1}{2} \frac{dv_1}{dx_2}$$

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- With all other $D_{ij} = 0$
- Thus we find $T_{12} = \mu \frac{dv_1}{dx_2}$
- μ relates shear stress to the rate of change of the angle, is known as viscosity

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- For a general velocity field, if we take $1/3$ of the contraction of the viscous stress tensor, we find

$$\frac{1}{3} T'_{ii} = \left(\lambda + \frac{2\mu}{3} \right) D_{ii}$$

- The quantity $(\lambda + \frac{2\mu}{3})$ relates the mean viscous normal stress to the change in volume
- It is often referred to as the bulk viscosity

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incompressible fluid

- If a fluid is considered to be incompressible, then $D_{ii} = 0$
- This gives the constitutive equation

$$T_{ij} = -p\delta_{ij} + 2\mu D_{ij}$$

- It is convenient to write it in terms of the velocity vector

$$T_{ij} = -p\delta_{ij} + \mu(v_{i,j} + v_{j,i})$$

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- If we recall Navier-Stokes equations of motion

$$\rho \left(\frac{\partial v_i}{\partial t} + v_j \frac{\partial v_i}{\partial x_j} \right) = \frac{\partial T_{ij}}{\partial x_j} + \rho B_i$$

- We can substitute the constitutive equation for newtonian fluids to find

$$\rho \left(\frac{\partial v_i}{\partial t} + v_j \frac{\partial v_i}{\partial x_j} \right) = \rho B_i - \frac{\partial p}{\partial x_i} + \mu \frac{\partial^2 v_i}{\partial x_j \partial x_j}$$

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- This gives three equations with four unknowns, we use the continuity equation to find the fourth unknown

$$\frac{\partial v_i}{\partial x_i} = 0$$

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- Navier-Stokes equations in cylindrical and spherical coordinates are found on p. 364-365 of the text
- There is a typo in 6.8.1, should read

$$\begin{aligned} \frac{\partial v_r}{\partial r} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \left(\frac{\partial v_r}{\partial \theta} - v_\theta \right) + v_z \frac{\partial v_r}{\partial z} = -\frac{1}{\rho} \frac{\partial p}{\partial r} + B_r \\ + \frac{\mu}{\rho} \left[\frac{\partial^2 v_r}{\partial r^2} + \frac{1}{r^2} \frac{\partial^2 v_r}{\partial \theta^2} + \frac{\partial^2 v_r}{\partial z^2} + \frac{1}{r} \frac{\partial v_r}{\partial r} - \frac{2}{r^2} \frac{\partial v_\theta}{\partial \theta} - \frac{v_r}{r^2} \right] \end{aligned}$$

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nonslip

- A common assumption is that of *nonslip* boundaries
- Agrees well with experiments
- Both Newtonian and non-Newtonian fluids
- Fluid moves with boundary, for rigid boundaries the velocity at the boundary is 0

- In general, fluid flow is characterized by a velocity field
- As a vector field, there are different ways in which to visualize the field
- Streamlines, pathlines, streaklines and timelines are common ways we talk about fluids

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steady and unsteady flow

- A flow is called *steady* if it is fixed in time (at a fixed location)
- Otherwise it is called unsteady
- Steady flow does not mean the material derivative is zero ($D\Psi/Dt \neq 0$)
- But it does mean that the partial derivative with respect to time is zero ($\partial\Psi/\partial t = 0$)
- For steady flow, streamlines, streaklines, and pathlines are the same

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- A streamline is a curve which is instantaneously tangent to the velocity vector
- Experimentally, streamlines can be found on the surface of a fluid by sprinkling reflective particles and making a short-time exposure photograph
- Mathematically, streamlines can be found by considering a parametric equation for a curve $x_i = x_i(s)$
- We choose s so that $dx_i/ds = v_i$ and $s = 0$ corresponds to the point x_0 , which is the originating point of our streamline

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streamline example

- Given the velocity field

$$v_i = \left\langle \frac{kx_1}{1 + \alpha t}, kx_2, 0 \right\rangle$$

find the streamline passing through (a_1, a_2, a_3) at time t

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- A pathline is the path traversed by a fluid particle
- Experimentally, pathlines can be found by using one reflective particle and a long-time exposure photograph
- Mathematically, the pathline can be obtained from the velocity field as follows

$$\frac{dx_i}{dt} = v_i(x_i, t)$$
$$x_i(t_0) = X_i$$

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pathline example

- Given the velocity field

$$v_i = \left\langle \frac{kx_1}{1 + \alpha t}, kx_2, 0 \right\rangle$$

find the pathline passing through (a_1, a_2, a_3) at time t

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streakline

- Streaklines are commonly found experimentally, but are difficult to express mathematically
- A streakline is formed when dye is steadily injected into a fluid from a fixed point
- The path that the very first point of dye follows is a pathline
- But the dye following behind is altered by the changing flow field, which makes the streakline left by the continuously injected dye different from a pathline

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timeline

- The final common method for visualizing fluid flows is known as a timeline
- Fluid particles are marked at a given instance of time (often forming a line at t_0)
- After set intervals of time, lines are drawn between these particles
- These lines are called timelines

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laminar flow

- Laminar flow is very orderly
- Fluid particles move in smooth layers (*laminae*)
- Occurs when fluid flow is relatively slow

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reynolds number

- Dimensionless parameter to compare how “fast” or “slow” a fluid is moving
- For experiments under otherwise identical conditions, reynolds number is used to determine whether flow will be laminar
- Ratio of inertial forces to viscous forces

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- In a tube, Reynolds number is

$$N_R = \frac{v_m \rho d}{\mu}$$

- For water in a tube, $N_R < 2100$ gives laminar flow

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turbulent flow

- In laminar flow, small perturbations are quickly overcome
- For turbulent flow, unsteady vortices appear and interact with each other
- Turbulent flows are highly irregular and chaotic
- Turbulence increases diffusivity, causing fluids to mix more quickly
- High Reynolds numbers correspond to turbulence, but how high depends on the specific experiment
- There is often a large transition range between laminar and turbulent flow

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– pp 365-375