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SUMMARY

Turbomachinery
MECA-H-402

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Appel à contribution

Synthèse Open Source



Ce document est grandement inspiré de l'excellent cours donné par Patrick HENDRICK à l'EPB (École Polytechnique de Bruxelles), faculté de l'ULB (Université Libre de Bruxelles). Il est écrit par les auteurs susnommés avec l'aide de tous les autres étudiants et votre aide est la bienvenue ! En effet, il y a toujours moyen de

l'améliorer surtout que si le cours change, la synthèse doit être changée en conséquence. On peut retrouver le code source à l'adresse suivante

<https://github.com/nenglebert/Syntheses>

Pour contribuer à cette synthèse, il vous suffira de créer un compte sur *Github.com*. De légères modifications (petites coquilles, orthographe, ...) peuvent directement être faites sur le site ! Vous avez vu une petite faute ? Si oui, la corriger de cette façon ne prendra que quelques secondes, une bonne raison de le faire !

Pour de plus longues modifications, il est intéressant de disposer des fichiers : il vous faudra pour cela installer L^AT_EX, mais aussi *git*. Si cela pose problème, nous sommes évidemment ouverts à des contributeurs envoyant leur changement par mail ou n'importe quel autre moyen.

Le lien donné ci-dessus contient aussi un README contenant de plus amples informations, vous êtes invités à le lire si vous voulez faire avancer ce projet !

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Merci !

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Chapter 1

Fundamental equations of turbomachinery

1.1 Basics and principles

1.1.1 Introduction

About the exam, he likes the drawings and likes to give a sentence and asks if it is the reality or not. The questions are about the **lectures** and not the notes. This summary is thus mainly based on the lectures.

The course is organized as:

1. **Turbopumps** and the system involved: a pump is something applying pressure to a fluid $\Delta p > 0$, which will first be a liquid $\rho = cst$.
2. **Turbines**: in this case the fluid involves a pressure loss $\Delta p < 0$, so expansion (a valve, simple releaser). We will see the gas turbines and the hydraulic turbines. Some machines can be used in the two ways, both roles, same mechanical component is acting as a pump and as a turbine in the other direction (reversible).
3. **Volumetric compressors**: as in other courses we have polytropic or isentropic efficiency, we can define volumetric compressors.
4. **Compressors $\rho \neq cst$** : we need to consider the axial and centrifugal systems separately because they are very different and complicated.

1.1.2 Classification of turbomachines

If the role of the machine is to extract energy from the fluid to the shaft we speak about **turboproducers** or **turbomotors** (ex: hydraulic turbines), and in the other case **turboabsorbers** or **turbogenerators**.

1.1.3 General organization of turbomachines

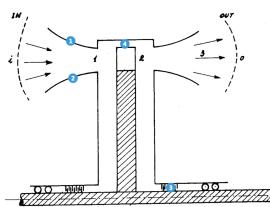


Figure 1.1

We always have a **shaft**, and on the shaft we have a **disk** or a **rotor** where the energy transformation takes place, and on this we put a **blade** (white rectangle on Figure 1.1), an element with a given geometry. The blade is situated at a distance r_H from the shaft and implies high tangential velocities. The device is closed by a **carter** and we have to be careful at the top of the blade since there can be

leakage, this is why the clearance is very small (μm). We can also have active clearance control by blowing fluid on the carter. Remark that there is an **external carter** (blue 1) and an **internal carter** (blue 2) that can constitute a convergent distributor and a divergent diffuser. These can contain non rotating parts called **vane**, we speak of **vaned convergent**, **vaned divergent** or **vaneless** nozzles. The internal carter plays the role of support and is connected to the shaft via **bearings** and **seals** (to avoid air preferring this way to reach atmospheric pressure).

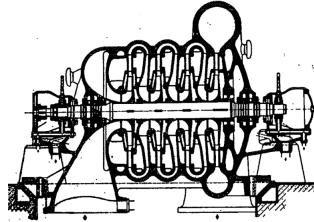


Figure 1.2

The major types of machine have an axial configuration so that the particles flows parallel to the shaft, radial configuration where flows enters horizontal and leaves vertical also exists. Most turbines or compressors are axial turbines. Turbopumps are most of the time radial, centrifugal. Several disks can be mounted on a same shaft (or several shafts), with fixed components changing the direction of the flow (multistage pump on Figure 1.2).

1.1.4 Notations

On Figure 1.1, 0 is the inlet of the distributor, 1 the inlet of the rotor, 2 outlet of the rotor, 3 outlet of the diffuser and o/s the upstream/downstream plenum. There are 3 velocity components: the absolute velocity \bar{v} , the frame tangential velocity \bar{u} and the relative velocity \bar{w} due to the rotation of fluid particles.

1.1.5 Velocity triangle

The absolute velocity respects:

$$\bar{v} = \bar{u} + \bar{w}. \quad (1.1)$$

By defining α and β the angle between \bar{u} and respectively \bar{v} and \bar{w} , we can write:

$$v \cos \alpha = u + \cos \beta \quad w^2 = u^2 + v^2 + 2uv \cos \alpha \quad (1.2)$$

The velocity triangle is the keypoint of a turbomachine, we have to play with the velocities by means of the mass flow rate \dot{m} and the machine rpm N . It is important to see that these parameters are linked to the velocity triangle, for the mass flow for example $\dot{m} = \rho u A$.

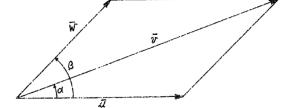


Figure 1.3

1.2 Fundamental equations of the flow

1.2.1 Equations of the flow in a fixed frame

For all developments, only **steady state** regime is considered, so that $\omega = cst$ and the flow properties are not time dependent. Moreover, boundary layers are neglected and the flow propagates in parallel slices.

Energy equation

Let's consider sections A_0 and A_1 denoting the input and output of a non interrupted flow section, for instance 0 to 1 in previous figure. The total energy equation is:

$$q = h_1 - h_0 + \frac{v_1^2 - v_0^2}{2} + g(z_1 - z_0) \quad (1.3)$$

where q is the heat exchanged with the outside [J/kg], v is the absolute velocity [m/s] and h is the enthalpy [J/kg]. In adiabatic systems $q = 0$. We see that if there is thermal, kinetic or potential energy loss, it will create heat. Be careful that this equation is not applicable around the blade.

Equation of kinetic energy

We know that kinetic and potential energy can be transformed into work in a machine. We have:

$$\frac{v_1^2 - v_0^2}{2} + g(z_1 - z_0) = - \int_{p_0}^{p_1} \nu dp - w'_f \quad (1.4)$$

where $\nu = 1/\rho$ is the specific volume [m^3/kg] and w'_f the work resulting from all friction effects [J/kg]. We see that if velocity increases/decreases, pressure decreases/increases and the friction is a loss, so "-" signs.

Global thermodynamic equation

By considering (1.4) in (1.3):

$$q + w'_f = h_1 - h_0 - \int_{p_0}^{p_1} \nu dp \quad (1.5)$$

The physical content is different, we see that in fact the losses corresponds to pressure and temperature losses.

Mass flow rate equation

The mass flow is constant over a tube:

$$\dot{m} = \rho v A = \rho_0 v_0 A_0 = \rho_1 v_1 A_1 = \frac{v_1 A_1}{\nu_1} \quad (1.6)$$

where \dot{m} [kg/s].

1.2.2 Equations of the flow in a moving frame

Now we can consider the indices 1 and 2 referring to the blade space.

Equation of kinetic energy in a relative space

He skipped the long demo page 8. The equations are the same as before, the only difference is that we replace the absolute velocity by the relative one and an additional kinetic energy term due to the rotation of the frame:

$$\frac{w_2^2 - w_1^2}{2} + g(z_2 - z_1) = - \int_{p_1}^{p_2} \nu dp - w''_f + \frac{u_2 - u_1}{2} \quad (1.7)$$

Remark that this term can play a huge role because in a centrifugal system the term is non zero while zero in axial system.

Global thermodynamic equation

The equation is exactly the same as before, except w'_f that becomes w''_f .

$$q + w''_f = h_2 - h_1 - \int_{p_1}^{p_2} \nu dp \quad (1.8)$$

Energy equation

If we combine the two previous equation we get:

$$q + \frac{u_2 - u_1}{2} = h_2 - h_1 + \frac{w_2^2 - w_1^2}{2} + g(z_2 - z_1) \quad (1.9)$$

Mass flow equation rate equation

For a section normal to the relative velocity:

$$\dot{m} = \rho w A = \rho_1 w_1 A_1 = \rho_2 w_2 A_2 \quad (1.10)$$

1.3 Fundamental equations of turbomachinery

1.3.1 Compressors

Internal losses

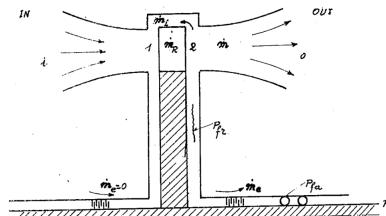


Figure 1.4

Several kind of losses are present in a compressor. First of all, friction in the distributor gives birth to losses noted w'_f . Then, the fluid go through the interblade channel where its energy increases, but a loss due to friction is present w''_f . In addition, the clearance between the blade tip and the carter is non zero and leads to back-flow leakage \dot{m}_i as the pressure upstream is lower. If we denote the mass flow rate through the blades \dot{m}_R , we have:

$$\dot{m}_R = \dot{m} + \dot{m}_i \quad (1.11)$$

Big part of the flow goes then through the diffuser, but a small part escapes from the seal to the outside \dot{m}_e . The small gap between the rotor and the internal carter is filled with part of the fluid. Even if this fluid does not contribute to the energy exchanges (stagnation), part of the power supplied to the shaft will dissipate due to fluid friction P_{fr} .

External losses

As discussed, part of the flow escapes through the seals. The upstream one is not a problem since the pressure is close to the atmospheric one, but for the downstream $\dot{m}_e \neq 0$ since the pressure is higher. This will be neglected in the study. The last losses are due to bearings and other mechanical components such as the fuel pump that we all denote in a single absorbed power P_{fa} .

Energy equation

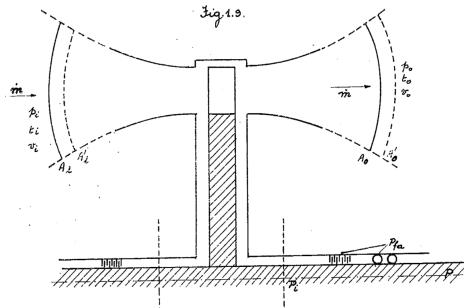


Figure 1.5

Before going through all the losses appearing in the engine, let's have a global view limiting the study region as on the figure. The total energy equation between input and output is:

$$q + W_{e \rightarrow s} = u_o - u_i + \frac{v_o^2 - v_i^2}{2} + g(z_o - z_i) \quad (1.12)$$

where we have the heat exchanged with the outside, the work from external forces to the system due to

fluid pressure $p_i\nu_i - p_o\nu_o$ and work applied on the shaft $\frac{P - P_{fa}}{\dot{m}} = \frac{P_i}{\dot{m}}$ equal to the variation of internal energy, kinetic energy and potential energy. Heat exchanges and the height difference in such engine is negligible, by introducing the enthalpy instead of internal energy and fluid pressure, we have:

$$P_i = P - P_{fa} = \dot{m} \left(h_o - h_i + \frac{v_o^2 - v_i^2}{2} \right) = \dot{m}(h_{t_o} - h_{t_i}) = \dot{m}c_p(T_{t_o} - T_{t_i}) \quad (1.13)$$

where the index t denotes the total or stagnation quantities. We conclude that the work transferred through the shaft increases the total energy of the fluid.

Equation of kinetic energy

This adapted to the work $\frac{P_i}{\dot{m}}$ gives:

$$P_i = \dot{m} \underbrace{\left(\frac{v_o^2 - v_i^2}{2} + \int_i^o \nu dp + g(z_o - z_i) \right)}_e + P_f = \dot{m}e + P_f \quad (1.14)$$

P_f is the internal friction loss with the active as well as the non-active fluid and e is the energy transferred to the fluid.

A first distribution of the power - efficiencies

The figure summarizes all the above equations, for the efficiency we have $\dot{m}e$ at the end and we inject P so:

$$\eta_g = \frac{\dot{m}e}{P} = \frac{\dot{m}e}{P_i P} = \eta_i \eta_m \quad (1.15)$$

that we rewrite as internal efficiency and external mechanical efficiency.

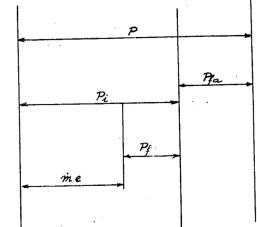


Figure 1.6

Energy transfer to the rotor

The only new equation we have is the **Euler-Rateau equation**. The energy given to the flow in a pump is linked to the energy provided to the shaft. We have to consider the kinetic moment (moment of the quantity of movement) related to the shaft:

$$\frac{d}{dt} \sum M_{axe}(m\bar{v}) = \sum M_{axe}\bar{F}_e \quad (1.16)$$

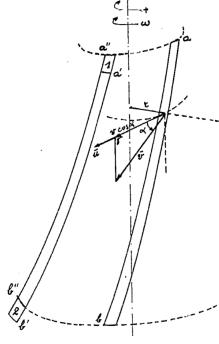


Figure 1.7

The variation of the kinetic moment of the rotor is zero since the rotation speed is constant. For a fluid element with mass m and at a distance r of the shaft, the velocity \bar{v} is composed of a component // to the shaft, radial component and tangential component on the rotor. Only the tangential component delivers a moment:

$$M_{axe}(m\bar{v}) = mrv \cos \alpha \quad (1.17)$$

and since the flow is permanent, after a time dt very small, if the mass flow is constant:

Figure 1.7

$$\sum_{b'b''} mrv \cos \alpha - \sum_{a'a''} mrv \cos \alpha = m'(r_2 v_2 \cos \alpha_2 - r_1 v_1 \cos \alpha_1) = m'(r_2 v_{2u} - r_1 v_{1u}) \quad (1.18)$$

Accepting $r_2 v_{2u} - r_1 v_{1u} = cst$ for all channels we get:

$$\frac{d}{dt} \sum M_{axe}(m\bar{v}) = \frac{d}{dt} [(r_2 v_{2u} - r_1 v_{1u}) \sum m'] = \dot{m}_R(r_2 v_{2u} - r_1 v_{1u}) \quad (1.19)$$

For the right hand side of (1.16), the weight of the wheel, the weight of the fluid, the pressure at inlet, at outlet and at side walls are null due to symmetry. Only the **driving torque** applied on the shaft M_i and the **resistive torque** $-M_{fr}$ due to friction between the wheel and the non-active fluid are present, so that we finally get:

$$\dot{m}_R(r_2 v_{2u} - r_1 v_{1u}) = M_i - M_{fr} \quad (1.20)$$

And if we multiply by ω :

Equation of Euler-Rateau

$$P_i - P_{fr} = P - P_{fa} - P_{fr} = P_R = \dot{m}_R(u_2 v_{2u} - u_1 v_{1u}) = \dot{m}_R \Delta(uv_u) \quad (1.21)$$

This equation tells that in order to be transferred to the mass flow rate \dot{m}_R , the power at the rotor shaft P_R must show an increase of the quantity uv_u which is directly related to the velocity triangle.

As $w^2 = v^2 + u^2 - 2uv_u$, one can also write:

$$P_R = \dot{m}_R \left(\frac{v_2^2 - v_1^2}{2} + \frac{u_2^2 - u_1^2}{2} - \frac{w_2^2 - w_1^2}{2} \right) \quad (1.22)$$

Energy generated by the rotor

Remember (1.7) and replace this in (1.22), we get:

$$P_R = \dot{m}_R \underbrace{\left(\frac{v_2^2 - v_1^2}{2} + \int_{p_1}^{p_2} \nu dp + g(z_2 - z_1) \right)}_{e_R} + \dot{m}_R w_f'' \quad (1.23)$$

where e_R is the energy transferred to the fluid through the channels on the rotor between section 1 and 2 on the common figure. $\dot{m}_R w_f'' = P_f''$ being the power absorbed by friction effects, we get:

$$P_R = \dot{m}_R e_R + P_f'' \quad (\text{and } P_R = \dot{m}(h_{t_2} - h_{t_1})) \quad (1.24)$$

And we get thus 4 different expression for P_R , where the last expression was given in lecture.

1.3.2 Detailed power distribution

The different losses can be depicted thanks to the previous equation:

$$P_i = P - P_{fa} \quad P_R = P_i - P_{fr} \quad \dot{m}_R e_R = P_R - P_f'' \quad \dot{m}_R = \dot{m} + \dot{m}_i \quad (1.25)$$

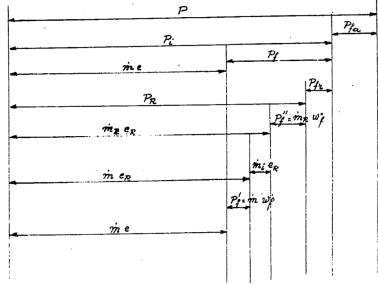


Figure 1.8

where we clearly see the mechanical losses, the loss due to stationary fluid, the loss at the rotor and the back flow. To this we have to add the loss at the diffuser and distributor which we wrote as:

$$P_f' = \dot{m} w_f' \quad (1.26)$$

On the figure, we first see the loss due to mechanical components giving P_i , then the fluid losses composed of stationary fluid losses giving P_R , then rotor channels loss giving $\dot{m}_R e_R$, but we have the back flow loss $\dot{m}_i e_R$ giving $\dot{m}_i e_R$ and the last venturi losses that gives the output power $\dot{m}e$ plus all the losses.

1.4 Turbines

Description

The equations are in fact the same except that we have to adapt the signs and indexes to the working principle since the energy is flowing from the fluid to the shaft. As before, there is a clearance flow \dot{m}_i such that:

$$\dot{m} = \dot{m}_R + \dot{m}_i \quad (1.27)$$

The losses due to mechanical components P_{fa} and the leakage flows \dot{m}_e (negligible), the energy losses in non rotating (w_f') and rotating (w_f'') frame and the loss due to non-active fluid P_{fr} are present. The useful power P_u replaces the P we had before.

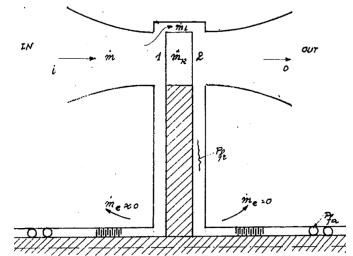


Figure 1.9

Energy equation

It is the same as before except that the indexes are inverted and the useful power is $P_u = P_i - P_{fa}$:

$$P_i = P_u + P_{fa} = \dot{m}(h_{t_i} - h_{t_o}) \quad (1.28)$$

Equation of kinetic energy

$$P_i = \dot{m} \underbrace{\left(\frac{v_i^2 - v_o^2}{2} + \int_{p_o}^{p_i} \nu dp + g(z_i - z_o) \right)}_e - P_f = \dot{m}e - P_f \quad (1.29)$$

First distribution of the power

The efficiencies are inverted:

$$\eta_g = \frac{P_u}{\dot{m}e} = \frac{P_u}{P_i} \frac{P_i}{\dot{m}e} = \eta_m \eta_i \quad (1.30)$$

On Figure 1.10 is represented a first plot of the different powers, remark that it is similar to what we had, only the fluid losses comes before the mechanical losses. The fluid losses are the same as before.

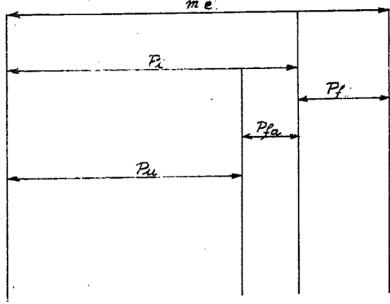


Figure 1.10

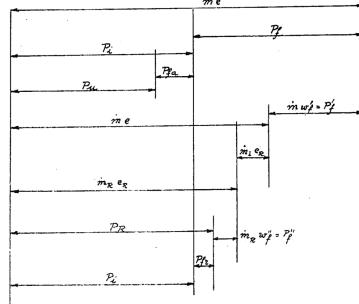


Figure 1.11

Equation of Euler-Rateau

We can rewrite P_R as the power transferred to the rotor from the fluid \dot{m}_R :

$$P_R = P_i + P_{fr} = \dot{m}_R(u_1 v_1 \cos \alpha_1 - u_2 v_2 \cos \alpha_2) \quad (1.31)$$

Energy absorbed by the rotor

As before, combining the above equation and the equation for rotating frame we get:

$$P_R = \dot{m}_R e_R - P_f'' \quad (1.32)$$

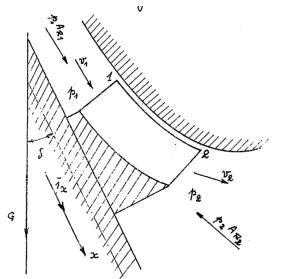
1.5 Axial thrust and disc friction

1.5.1 Definition

Since the turbomachinery is used to increase the energy of the fluid or extract energy, the pressure at the two sides of the rotor is different. This leads to an axial force and we need **thrust bearings** to avoid the shaft to slip.

1.5.2 Equation of the axial thrust

We apply the equation of quantity of movements to the wheel and fluid without the shaft between section 1 and 2:



$$\sum \frac{d}{dt}(m\bar{v}) = \sum \bar{F}_e \quad (1.33)$$

We will make a projection along x-axis. The external forces in presence are: the pressure forces $p_1 A_{R1}$ and $p_2 A_{R2}$, the weight of the rotor and the fluid projected is $G \cos \delta$ and the reaction force of the shaft on the

Figure 1.12

rotor with projection F_{ax} so $-F_{ax}$ as seen by the rotor (projection of moments is null). The equation of quantity of movement becomes:

$$\begin{aligned} \dot{m}_R (v_{2ax} - v_{1ax}) &= p_1 A_{R1} - p_2 A_{R2} + F_{ax} + G \cos \delta \\ \Leftrightarrow F_{ax} &= \dot{m}_R dt(v_{2ax} - v_{1ax}) + P_2 A_{R2} - P_1 A_{R1} - G \cos \delta \end{aligned} \quad (1.34)$$

1.5.3 Friction of the disc

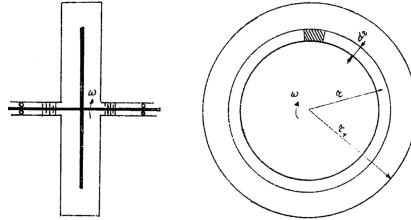


Figure 1.13

As mentioned before, there is friction between the disc and the non-active fluid. It is obvious that the friction torque will increase with the radius (more surface), the rpm (u) and the volumetric mass of the fluid. Considering an elementary surface $2\pi r dr$, we find experimentally for the elementary friction force and torque:

$$dF_{fr} = K\rho u^2 2\pi r dr \quad dC_{fr} = 2K\rho 2\pi r^2 dr u^2 \quad (1.35)$$

the 2 appears by considering the 2 sides of the disc. We integrate from internal radius r to the external one r_1 and multiply by ω to have powers (neglect r^5 compared to r_1^5):

$$C_{fr} = K\rho\omega^2 r_1^5 \quad \Rightarrow P_{fr} = K\rho\omega^3 r_1^5 \quad (1.36)$$

Remark that one could think that we will have enormous values for ω^3 , but be aware that if ω increases, the mechanical stresses on the device increases and force to reduce the r_1 . This is why the friction is finite. If the side walls are very smooth, the coefficient K is related to the Reynolds number:

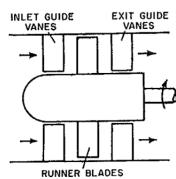
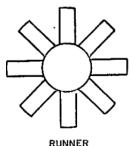
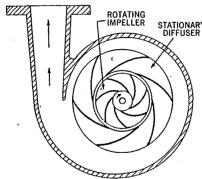
$$Re = \frac{\rho\omega r_1^2}{\mu} \quad (1.37)$$

Chapter 2

Centrifugal pumps

2.1 Generalities

2.1.1 Description - Type of turbopump



The task of the turbopump is to transfer

Figure 2.1

Figure 2.2

energy to a liquid. Above we can see a centrifugal and an axial turbopump. Between these two extremes, we can have a variety of types depending on the requirements. Each turbopump is composed of one or several wheels that can be mounted in parallel (increase mass flow rate) or in series (higher energy transfer), see Figure 1.2.

2.1.2 Installation of a turbopump

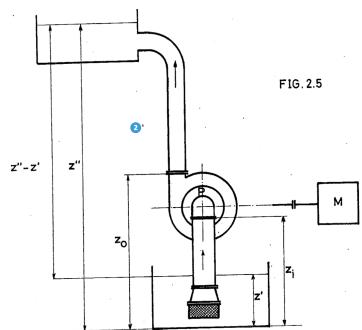
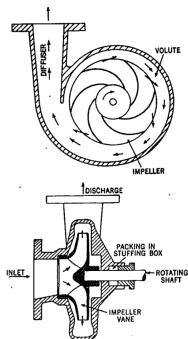


Figure 2.3

Figure 2.4

that the flow enters at the middle in the rotating blade and is projected into the volute. This last has a growing section from the beginning to the end as the mass flow increases. The turbopump is commonly used to transfer liquid from a downstream reservoir to an upstream reservoir situated higher. We have to be careful to avoid cavitation (evaporation of the fluid due to too low pressures) and we also have a control valve at the suction section to always have a contact blade-fluid.

2.1.3 Energy developed by the turbopump - flow rate

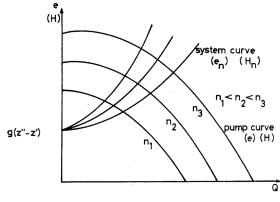


Figure 2.5

$$e = \frac{v_o^2 - v_i^2}{2} + \int_{p_i}^{p_o} \nu dp + g(h_o - h_i) = \frac{v_o^2 - v_i^2}{2} + \frac{p_o - p_i}{\rho} + g(h_o - h_i) \quad (2.1)$$

The velocity is low in order to limit the head losses and thus the pressure term is the highest (height change in a compressor is low too). The energy delivered by the pump to the fluid can be rewritten in terms of the volumetric flow rate Q [m^3/s]:

$$e_p = \frac{p_a - p_i}{\rho} - \frac{p_a - p_o}{\rho} + \frac{A_i^2 - A_o^2}{2A_i A_o} Q^2 + g(z_o - z_i) \quad (2.2)$$

2.1.4 Useful power or hydraulic power

The power transferred from the input of the pump until the exit and the global efficiency of the pump are:

$$P_h = \dot{m}e = \rho Q e \quad [W] \quad \eta = \frac{\rho Q e}{P_m} \quad (2.3)$$

where P_m is the mechanical power to drive the pump.

2.1.5 Working point of a turbopump

Consider Figure 2.4 and let's apply Bernouilli equation (kinetic energy equation) between z' and z_i then z_o and z'' :

$$\frac{v_i^2 - v'^2}{2} + g(z_i - z') = -\frac{p_i - p'}{\rho} - w'_{fa} \frac{v''^2 - v_o^2}{2} + g(z'' - z_o) = -\frac{p'' - p_o}{\rho} - w'_{fr} \quad (2.4)$$

One can make the sum of the two expression and regroup the terms of the reservoirs in a new **energy requested by the circuit e_n** . If we consider large reservoirs $v'' \approx v'$ and $p'' \approx p' \approx p_a$, we have:

$$e_n = g(z'' - z') + \underbrace{w'_{fa} + w'_{fr}}_{w'_f} \Rightarrow e_p = e_n \quad (2.5)$$

This is always valid in **steady state**.

2.1.6 Characteristic of the hydraulic circuit

The system curves on Figure 2.5 plot e_n which depends on the height difference and the mass flow rate (because $w'_f \propto v^2$ of the flow) and depends thus on the square of the volumetric mass flow rate. This is why we have a parabolic shape, the slope depends on the head loss coefficient K . If we have a valve, the closer the valve, the higher the slope.

2.1.7 Performance curve of a pump

Similar curves can be established for the e, Q relations at different rpm. With a control valve at the exit, and by fixing the rpm of the engine, we can find them and are plotted on Figure 2.5.

2.1.8 Working regimes

Practical analysis shows that if two of the three parameters e, Q, n are fixed, the working point too: $f(e, Q, n) = 0$

2.1.9 Practical units

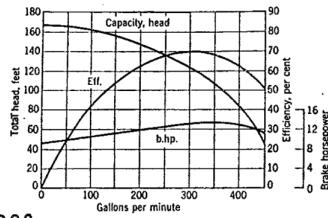


FIG.2.8.

Figure 2.6

Here we express the energy in J/kg but we know that it is also $g\Delta z$ in [m]. Thus we will use instead of e , $H = e/g$ [m]. The energy transferred to the fluid is often called the **height** of the **head**. For example $H = 10$ m means that we transfer energy such that we increase z of 10 m. As last remark, be aware that efficiency curves are provided by the manufacturer and the pump has to be chosen specifically to the circuit where it should operate to get the maximum efficiency.

2.2 The centrifugal pump

2.2.1 Organization of a centrifugal pump

We have an inlet distributor D charged of guiding the fluid towards the entrance 1 of the rotor R or also called **impeller**. The rotor is made of one or two disks on which are mounted the blades beginning at a certain external radius r_1 and finishing at r_2 . A fixed diffuser d composed of 2 parallel discs surrounding the rotor, connected with vanes surrounds the exit of the blades, sometimes it is not used. A **volute** or **collector** c with increasing volume directs the flow to the exit section of the machine.

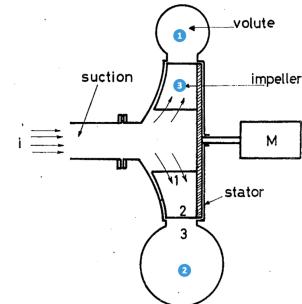


Figure 2.7

2.2.2 The distributor

If there is no vane in the distributor, the flow penetrates in the rotor axially since we assume no fluid particle to rotate before entering in the rotor, and becomes radial symmetrically at entrance 1. If there is vane, the direction of the flow is imposed by the vanes but we take the first case here. The equation of kinetic energy applied between i and 1 when neglecting the height difference is:

$$\frac{v_i^2 - v_1^2}{2} + \frac{p_i - p_1}{\rho} = w'_{fD} \quad (2.6)$$

where w'_{fD} represents the pressure losses in the distributor, proportional to the square of Q and thus to v_1^2 : $w'_{fD} = K_D \frac{v_1^2}{2}$ where $K_D \approx 5.10^{-3}$

2.2.3 The rotor

The impeller starts at r_1 and finish at r_2 , the section of the rotor at these levels are:

$$A_1 = 2\pi r_1 b_1 e_1 \quad A_1 = 2\pi r_2 b_2 e_2 \quad (2.7)$$

where e_1, e_2 are blockage coefficients taking into account the decrease in area due to the thickness of the impeller.

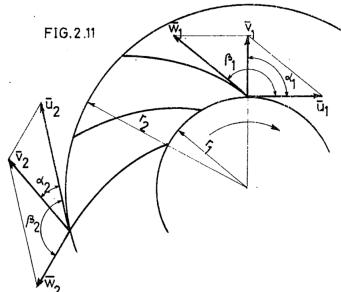


Figure 2.8

The rotor and impeller velocity triangles are represented on the figure. v_1 is known by the previous discussion and is purely radial and u_1 can be computed:

$$v_1 = \frac{Q_R}{2\pi r_1 b_1 e_1} \quad u_1 = r_1 \omega_1 = \frac{2\pi n}{60} r_1 \quad \alpha_1 = 90^\circ \quad (2.8)$$

The missing components of the velocity triangles are w_1 and β_1 and can be retrieved by construction. In addition we make an assumption for β_1 (fluid angle) which must be equal to $\bar{\beta}_1$ (solid angle), this is imposed by the design to avoid collision or separation. Indeed, the pump is designed to work with a certain Q_R and a certain n , if this changes, shocks and separation can occur, leading to losses. Same considered for β_2 , $u_2 = r_2 \omega$ and this time the radial velocity is the projection of w_2 :

$$u_2 = r_2 \omega_2 \quad w_2 \sin \beta_2 = \frac{Q_R}{2\pi r_2 b_2 e_2} \quad (2.9)$$

β_2 is chosen larger than 90° in order to make v_2 small and thus limit the diffuser size (limit the losses, β_2 between 145° and 165°). We are now able to retrieve v_2 and w_2 .

2.2.4 Number and shape of the blades

The number of blades determine the volume available to the flow and the guidance. The more we have blades, the more the fluid is guided but the more we have pressure losses. The designer must make a trade-off, generally there are 6 to 12 blades. The profile of the blades must be so that the angles $\beta_1 = \bar{\beta}_1$ and $\beta_2 = \bar{\beta}_2$ are respected.

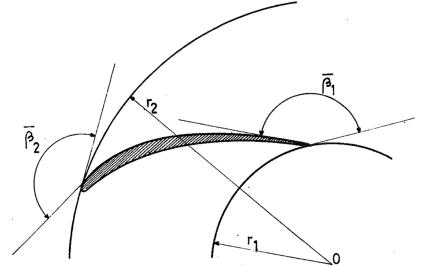


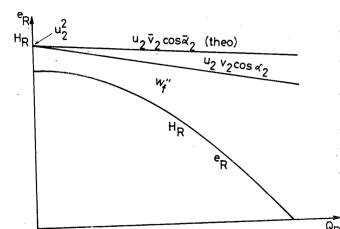
Figure 2.9

If the blades are made of two surfaces, one active and one non-active as represented on the figure, if the two surfaces makes an angle too large at the entrance, it is impossible that β_1 is tangent to both and lead to shocks. At the exit, since there is a pressure gradient between active and non active sides, the β_2 is "sucked" by the non-active part where the pressure is lower.

2.2.5 Head of Euler of the rotor

Using Euler-Rateau and power distribution, we have:

$$P_R = \dot{m}_R (u_2 v_{2u} - u_1 v_{1u}) = \dot{m}_R e_R + \dot{m}_R w_f'' \Rightarrow e_R = u_2 v_{2u} - u_1 v_{1u} - w_f'' \quad (2.10)$$



as we have seen, $\alpha_1 = 90^\circ \Rightarrow v_{1u} = 0$ and $e_R = u_2 v_{2u} - w_f''$. The term $u_2 v_{2u}$ is called the **energy of Euler** and is the theoretical energy that the rotor transfers to the fluid. The **head of Euler** is $\frac{u_2 v_{2u}}{g}$. Lets show that this energy is function of $Q_R, N, \bar{\beta}_1$ and $\bar{\beta}_2$ using the velocity triangle relation:

Figure 2.10

$$\mathbf{u}_2 v_2 \cos \alpha 2 = \mathbf{u}_2 (u_2 + w_2 \cos \bar{\beta}_2) \Rightarrow e_r = u_2^2 + \frac{Q_R}{2\pi r_2 e_2 b_2 \tan \bar{\beta}_2} \quad (2.11)$$

where we used (2.9). We see that as $\bar{\beta}_2 > 90^\circ$ in practice, we have a linearly decreasing function. We still don't have the characteristics since we are underestimating the angles deviation, the number of blades and the fluid losses.

2.2.6 Losses in the rotor due to friction

He skipped the previous section. The term w_f'' regroups the different losses that occurs in the rotor and can be separated in:

- the losses due to the development of the boundary layer in the channel sidewalls and $\propto Q_R^2$:

$$k_1 Q_R^2 = K_R \frac{w_1^2}{2} \quad K_R \approx 0.025 \quad (2.12)$$

- a second loss due to the shocks and separation of the boundary layer each time w_2 is not tangent to the blade. Looking to the situation on Figure 2.11, we find experimentally that these losses are $\propto (\Delta w)^2$ that is $\propto v_1$ that is $\propto Q_R - Q_{RD}$ where Q_{RD} is the flow rate in design conditions $\beta_1 = \bar{\beta}_1$:

$$Q_R = 2\pi r_1 b_1 e_1 v_1 \quad Q_{RD} = 2\pi r_1 b_1 e_1 v_{1D} \quad (2.13)$$

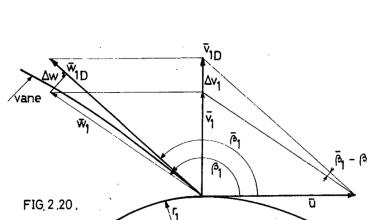


Figure 2.11

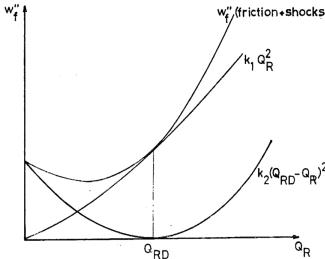


Figure 2.12

The sum is represented on Figure 2.12 and we see that even at low Q_R w_f'' is high, this is due to the second loss.

2.2.7 Loss due to the internal leak flow

We already know what it is, it goes from 1 for large pumps to 10% of \dot{m}_R for small pumps. This is due to the fact that the clearance cannot be reduced under an absolute size and the seals in large machines cannot be more efficient than in small machines. The power loss is:

$$\dot{m}_i e_R = (0.01 \text{ to } 0.1) \dot{m}_R e_R \quad [W] \quad (2.14)$$

2.2.8 Friction of the disc on the non-active fluid

Per side of the disc, it can be estimated as:

$$P_{fr} = 1.21 \cdot 10^{-3} u_2^3 D_2^2 \quad [ch] \quad (2.15)$$

2.2.9 The diffuser

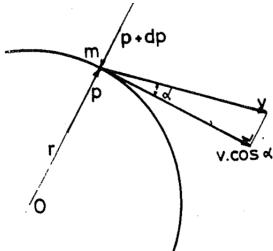
Energy transformation in the diffuser

The velocity v_2 at the exit of the pump is generally too high for some applications, the diffuser converts part of the kinetic energy into pressure energy. There exists 4 types of diffuser: straight parallel sidewalls or inclined, and for each we can have vaneless or vaneless. The kinetic energy equation in a fixed frame with $z_3 - z_2 = 0$ is:

$$\frac{p_3 - p_2}{\rho} = -\frac{v_3^2 - v_2^2}{2} - w'_{fd} \quad (2.16)$$

where $w'_{fd} \approx 0.02 - 0.03v_2^2/2$ [J/kg]. We see that kinetic energy gives pressure and loss.

The vaneless diffuser with flanges



The common architecture of the diffuser is composed of two circular flanges put around and in the continuity of the exhaust of the rotor. Let's apply the equation of the kinetic moment to a fluid element of mass m and at a radius r :

$$\frac{d}{dt} M_{axis}(m\bar{v}) = M_{axis} \bar{F}_e \quad (2.17)$$

The situation is represented on Figure 2.13, the flow in the diffuser is axisymmetric. If one neglects the weight of the particles, the external forces moment is null since the pressure is radial. All particles are facing the same pressure for symmetrical reasons and have thus the same trajectory. We have:

$$\frac{d}{dt}(mvr \cos \alpha) = 0 \quad \Leftrightarrow mvr \cos \alpha = rv_u = cst \quad (2.18)$$

This is valid for a non-rotational flow. On the other hand we have the mass flow rate:

$$2\pi rb \sin \alpha = cst \quad \Rightarrow b \tan \alpha = cst \quad (2.19)$$

If the flanges are parallel $b = cst$ and thus $\alpha = cst$, this gives a logarithmic spiral for the particles trajectory. The only way to make v_3 decrease is to have larger r_3 :

$$2\pi r_2 b_2 v_2 \sin \alpha_2 = 2\pi r_3 b_3 v_3 \sin \alpha_3 \quad \Rightarrow v_3 = v_2 \frac{r_2}{r_3} \quad (2.20)$$

Another way is to have variable b . In (2.19) this would mean that α decreases. We have thus:

$$2\pi r_2 b_2 v_2 \sin \alpha_2 = 2\pi r_3 b_3 v_3 \sin \alpha_3 \quad \Rightarrow v_3 = v_2 \frac{r_2 b_2 \sin \alpha_2}{r_3 b_3 \sin \alpha_3} = v_2 \frac{r_2 \cos \alpha_2}{r_3 \cos \alpha_3} \quad (2.21)$$

Since $\cos \alpha_3 > \cos \alpha_2$, v_3 will be lower. The divergence angle is limited to 6-7° because of separation (have to look for another method).

The diffuser with blades

With the previous discussion, if v_2 increases we still have to increase r_3 . Another method to avoid this, is the use of vanes between the flanges. Their job is to guide the fluid particle so that α increases:

$$2\pi r_2 b_2 v_2 \sin \alpha_2 = e_3 2\pi r_3 b_3 v_3 \sin \alpha_3 \quad \Rightarrow \frac{r_3}{r_2} = \frac{1}{e_3} \frac{v_2 \sin \alpha_2}{v_3 \sin \alpha_3} \quad (2.22)$$

where e_3 is the filling coefficient taking into account the presence of the vanes. We see that for higher α_3 , we can take lower r_3 . But blade means friction and thus shock.

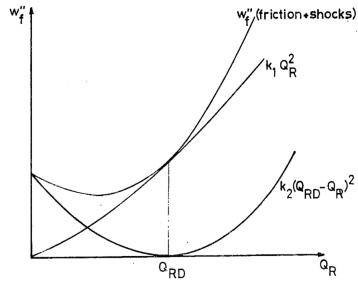


Figure 2.14 preferable to use the vaneless involving Q^2 losses.

To avoid this the entrance of the diffuser should be 1 or 2 mm larger and the vanes should be tangent to the flow, depending on Q and N . The design is thus made in order to be tangent for a certain couple N_D, Q_D called design conditions. In off-design conditions, shocks and separation occur. There is a small gap between vanes and the rotor blades to limit the noise produced by turbulences. Due to the shocks and separation, w'' is never equal to zero and rather large for small Q . In conclusion, the vaned diffuser gives smaller dimensions, but lead to considerable losses when far from the working point and it is maybe

2.2.10 The volute or collector

Its job is to collect the flow coming out of the diffuser or the rotor, its section increases from the beginning to the end, the flow in radial section is non uniform and respects:

$$v_u r = v_{u3} r_3 = cst \quad (2.23)$$

and the losses in the diffuser and volute are estimated to (0.02 and 0.03) $\frac{v^2}{2}$ [J/kg].

2.2.11 Characteristic curves of a centrifugal pump

We are now able to understand the shape of the characteristic curve on Figure 2.10 since the losses w_f'' have a parabolic shape. To deduce the curve in function of the flow Q , we still have to consider the internal leak flow $Q = Q_R - Q_i$ and the w'_{fD} and w'_{fd} that are function of Q^2 and $(Q - Q_D)^2$ when the diffuser is vaned. We can make these curves for different rpm it goes up and right, we will see how to plot them without experiment, we only have to measure for one rpm.

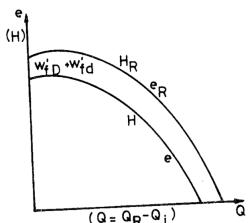


Figure 2.15

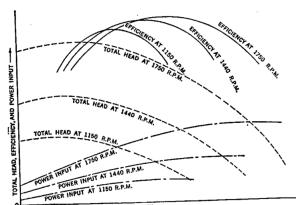


Figure 2.16

2.3 Performance curves of centrifugal pumps non-dimensional analysis

2.3.1 Theory of Vachy-Buckingham

Consider a machine characterized by some physical variables containing q fundamental parameters. It is possible to choose p independent variables and to build $p - q$ independent non-dimensional variables. Any other dimensionless combination of these variables will be function of the independent reduced variables.

2.3.2 Application to turbopumps

The variables differentiating geometrically equivalent pumps working points are: r [L], n [T^{-1}], \dot{m} [MT^{-1}], ρ [ML^{-3}] and μ [$ML^{-1}T^{-1}$]. We can limit the physical variables to 4 parameters by noticing that $u = r \frac{2\pi n}{60}$ and that μ is in Re number already non-dimensional and 3 fundamental variables. The non-dimensional variable can be found as follows:

$$\begin{aligned}\pi &= r^x u^y \dot{m}^z \rho^w \Rightarrow \pi = (L)^x (LT^{-1})^y (MT^{-1})^z (ML^{-3})^w = M^0 L^0 T^0 \\ x + y - 3w &= 0 \quad -y - z = 0 \quad z + w = 0\end{aligned}\quad (2.24)$$

We have a system of 3 equations with 4 variables, we will fix $z = 1$ to have \dot{m} in the expression, that gives $y = -1, w = -1, x = -2$, and the reduced variable is:

$$\frac{\dot{m}}{\rho u r^2} = \frac{Q}{u r^2} \Rightarrow \frac{Q}{u r^2} \cdot \frac{\dot{e}}{u^2} \cdot \eta_g \cdot \frac{\dot{P}}{\rho u^3 r^2} \quad (2.25)$$

2.3.3 Performance curves of a type of pumps

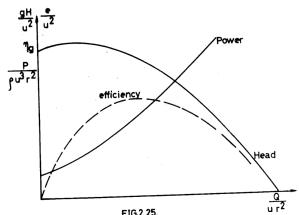


Figure 2.17

For a family of pumps with same r, ρ and u we can plot the non-dimensional $\frac{gH}{u^2}, \eta_g, \frac{P}{\rho u^3 r^2}$ in function of the non dimensional $\frac{Q}{\rho u r^2}$. If two of the parameters are known, the third is known since:

$$\frac{P}{\rho u^3 r^2} = \frac{P}{\dot{m} e} \frac{\dot{m}}{\rho u r^2} \frac{e}{u^2} = \frac{1}{\eta_g} \frac{Q}{u r^2} \frac{gH}{u^2} \quad (2.26)$$

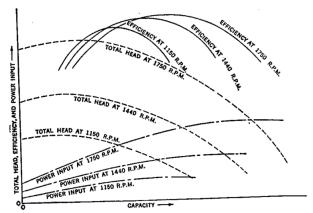


Figure 2.18

2.3.5 Stability of a turbopump

Stability of the motor + pump assembly

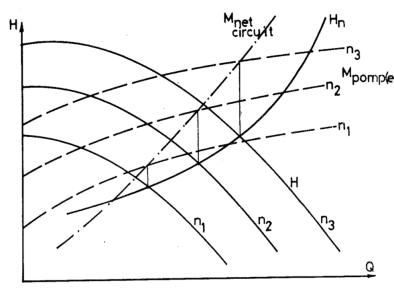


Figure 2.19

This is based on the driving torque of the motor and resistive torque of the pump. These can be found considering the characteristic curve of a pump in a fixed network. For what concerns the torque curve of the pump, one just has to divide the H curve by the rpm and will get a torque curve for every rpm. For the resistive torque, determine the intersection of $H_{network}$ and H_{pump} and make the projection on the pump torque for every rpm. We find a positive slope curve.

Stability of the pump on the circuit

The second stability problem is the problem of the pump in the circuit. Consider the figure illustrating a water tower without losses inducing a horizontal network characteristic, (b) has a small design mass flow rate and the other (c) large. The small one has in fact the same curve as the second but the maximum is shifted on the y-axis.

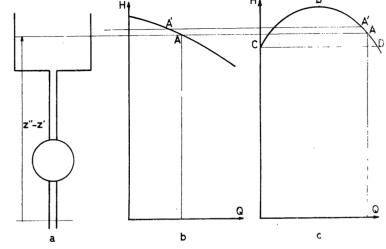


Figure 2.20

Now, imagine a town to supply with a water tower. At a given moment we have a certain amount of users, and we are at point A. If now there are using less and less of water, the level of water is increasing so that more power is requested from the pump. The two configuration are good in the sense where the increase of the level makes the flow reduce. If now the level goes higher and higher until reaching the maximum of the curve, the pump stops, there is no intersection on the curve. The configuration (b) is ok because the level drops the pump is used normally.

But for configuration (c), when the pump stops, we go directly to point C and when the level drops, the pump will be functional only when the level reaches C and has a jump to point D. The problem is that the flow is maximal and the level goes rapidly up such that we have a cycle ABCD. This is called **surge mode**. This is a low frequency loop because it requires time to go from D to B ($\approx 1 \text{ Hz}$). In conclusion, the (b) is very good for stability but not for performance and the contrary for the other. So we want to combine the two. We put a c pump on the network that is always used and we have in parallel another pump b that will be used at high levels.

2.3.6 Pump cavitation

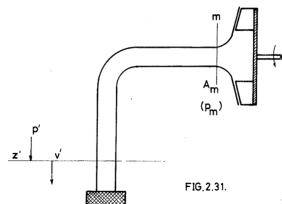


Figure 2.21

When the pump is placed above the free fluid level, the intrance pressure should be less than the atmospheric pressure to allow suction. We can define the minimum section as the end of the distributor. When Q increases this will be the place of high velocities and thus low pressures. When the pressure is lower than the saturation pressure, gas bubbles or vapor pockets will be formed. There are problems due to the gas dissolved in the fluid:

- reduction of the flow rate due to narrowing of the fluid section;
- noise characteristic of the phenomenon and changing with the intensity of the cavitation;
- degradation of the blades due to the interaction with bubbles, they produce a locally concentrated stress, erosion and corrosion of the metal of the blades.

The pressure at the minimum section can be found by using the kinetic energy equation between free level and minimum section, expressing the losses as kQ^2 and replacing the velocity by $v_m = Q/A_m$:

$$\frac{v_m^2 - 0}{2} + g(z_m - z') + \frac{p_m - p_a}{\rho} = -kQ^2 \quad \Rightarrow p_m = p_a - g\rho(z_m - z') - \rho \left(k + \frac{1}{2A_m^2} \right) Q^2 \quad (2.27)$$

Using this formula we can see that increase of Q makes p_m smaller, same for decrease of A_m , increase of k and higher level differences. The gas to liquid ratio is also important (ability to liberate gas into the liquid). The saturation pressure is changing with temperature. What we

can do to avoid cavitation is to place the pump at the same level as the free level or below, and avoid all the friction before the entrance such as additional valves or pipe turns,

We can conclude by stating that a modification in the circuit can have important consequences on the efficiency of a pump, always check!

NSPH

In order to make rise a column of fluid, underpressure is needed for suction. If this underpressure is lower than the saturation pressure of the fluid, cavitation will take place. If the water head to be sucked is too important to be elevated without cavitation, one has to use several pumps. The maximum possible underpressure before cavitation is called the available NPSH (Net Positive Suction Head). This is related to the water head aspiration, there is also one related to the pump flow rate since we need an extra underpressure to give a certain more or less high flow rate called requested NPSH:

$$NPSH_{avail} = H_e - \frac{p_s}{\rho g} \quad NPSH_{avail} > NPSH_{req} \text{ to avoid cavitation} \quad (2.28)$$

2.4 The network and its characteristic curve

2.4.1 Simple circuit

By simple circuit we mean the one composed by two reservoirs the pipes and one turbopump. If we apply the kinetic energy equation between ' and i and between o and " we can combine them and get:

$$\frac{v''^2 - v'^2}{2g} + \frac{p'' - p'}{\rho g} + (z'' - z') + \frac{\sum w_f}{g} = \frac{v_o^2 - v_i^2}{2g} + \frac{p_o - p_i}{\rho g} + (z_o - z_i) \quad H_n = H \quad (2.29)$$

H_n is the characteristic of the circuit. In a simple configuration as in Figure 2.4 we have $v'' = v' \approx 0$ and $p'' = p' = p_a$ such that:

$$H_n = (z'' - z') + \frac{\sum w_f}{g} \quad (2.30)$$

but in some applications we cannot neglect these terms so that we have 2 terms independent of Q^2 and two dependent and thus the actual characteristic $H_n(Q)$ is the increasing part of a parabol beginning at ordinate $z'' - z' + \frac{p'' - p'}{\rho g}$.

2.4.2 Calculation of the characteristic curve of a circuit

Losses in the circuit

We consider non incrusted circular pipes for turbulent pipes:

$$Re = \frac{vD}{\nu} > 2500 \quad (2.31)$$

where ν is the kinematic viscosity. There will be losses in straight pipes, accessories and shape modifications.

Regular pressure losses (in straight pipes)

They are $\propto L, Q(\nu), \nu$ and inversely $\propto D^2$.

Singular losses (in all accessories)

They can be replaced by equivalent straight pipe losses thanks to coefficients listed in a table that one must multiply by the diameter in cm to get m. Each accessory has its own coefficient.

Losses due to abrupt shape modifications

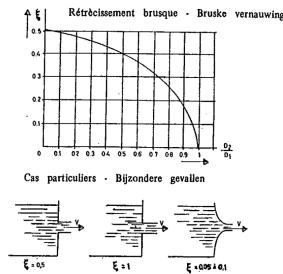


Figure 2.22

They are computed in meter using the formula:

$$\zeta \frac{v^2}{2g} \quad (2.32)$$

where v is the downward velocity in case of an opening of the section and backward in the case of a restriction. In the case of a section increase:

$$\zeta = \left(\frac{D_{aval}^2}{D_{amont}^2} - 1 \right) \quad (2.33)$$

In the case of a restriction the value is computed using the graph. An example of computation is made at page 56, a remark: in case of rough pipes more rigorous computations must be made.

Complex circuits

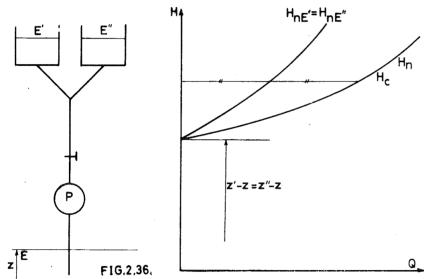


Figure 2.23

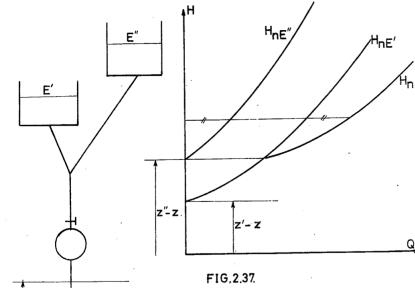


Figure 2.24

In the case of complex circuits like the two above, one has just to consider the two characteristics, which are superimposed in the first case since the water head is the same and where they are different in the second case because of the height difference (start on y-axis). In the first case, once the pump is able to deliver to one of the reservoir it is also able to deliver to the other and thus we need a larger flow rate. This manifests by doubling the x-axis. In the second case, when the height is between z' and z'' only the lower one is filled, and once we arrive at z'' the combination is made as the first case.

2.5 Selection of a pump of a pump type

2.5.1 Users of pumps

We take the point of view of the process engineer and not the designer, so we select an existing pump fitting at best the need in H and Q . The speed is normally fixed by the driving motor, variable speed could be useful to select the region of maximum efficiency for a working region

but is more expensive. A high rotation speed makes the device more compact and cheaper. We need thus to fix the circuit on which the pump will be used, the desired Q_D , the nature of the fluid ρ and the rpm N .

2.5.2 General case

For a same family of pumps, it is possible to reduce the performance curves in a single one as seen previously with non-dimensional numbers at certain rpm:

$$\frac{W_m}{\rho u^3 r^2}, \frac{e}{u^2}, \frac{gH}{u^2} \quad \eta_g \quad \text{in } f\left(\frac{Q}{ur^2}\right) \quad (2.34)$$

2.5.3 Choice of the pump type

We can plot $\left(\frac{e}{u^2}\right)^{\frac{3}{2}}$ in function of $\frac{Q}{ur^2}$ we can plot the performance curve of each family on the same graph and can target the maximum efficiency region on each curve. Let's define the angle:

$$\tan \psi = \frac{\left(\frac{e}{u^2}\right)^{\frac{3}{2}}}{\frac{Q}{ur^2}} = \frac{(gH)^{3/2} r^2}{Qu^2} = \left(\frac{60}{2\pi}\right)^2 \frac{(gH)^{3/2}}{Qn^2} \quad (2.35)$$

where we used the relation $u = \frac{2\pi n}{60}r$ for the last expression. By replacing n, Q, H by the desired ones, we can find a ψ_D that one draws on the figure and select the pump that intersects the nearest to the maximum efficiency region (here 1).

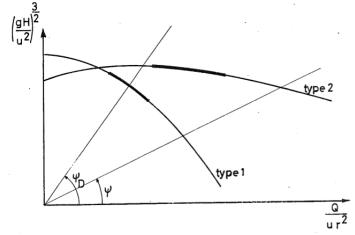


Figure 2.25

2.5.4 Choice of the pump

Once the previous point has been done, one knows the value of $\frac{Q}{ur^2}$ and can compute r_D as follows:

$$\frac{Q}{ur^2} = \frac{60}{2\pi} \frac{Q}{nr^3} \quad (2.36)$$

and replacing by the design values. It is not always possible to have exact values of radius disponible for every families and one has sometimes to make compromises and thus we have to compute the final values of:

$$u_D = \frac{2\pi n_D r_D}{60} \quad \frac{Q_D}{u_D r_D^2} \quad P_m = \frac{\rho g Q_D H_D}{\eta_g} \quad (2.37)$$

where η_g is read on the curve. The rotation speed of the rotor is determined via $u_D = r\omega$.

2.5.5 Groups of pumps

Problem

For low Q and high H or high Q and low H it is possible that the desired line with ψ_D does not intersect any performance curve with an admissible efficiency. This problem can be solved using several pumps in parallel or series.

Serial grouping of pumps

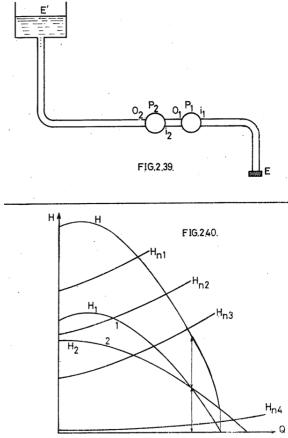


Figure 2.26

the increase in Q . For cases where high Q and low H are required, the series are limited by the maximum Q of one of the pump and thus on the figure we see that pump2 single could deliver while the combination not. In conclusion, this type is reserved for high head and low Q .

Grouping of pumps in parallel

For this case we have:

$$H = H_1 = H_2 \quad Q_1 + Q_2 = Q \quad (2.39)$$

and the graph is just obtained by the summation of the two in the Q direction. We can observe that the combination shows its interest only after a certain flow rate since for H_{n1} for example the pump1 can work alone and pumps2 is useless. In this case an anti-return valve is to be foreseen. For higher flow rates, one can observe that both pumps can deliver flow but at a lower rate. In conclusion, we see that this configuration is reserved for high flow rate applications.

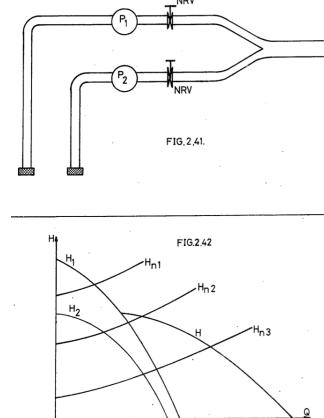


Figure 2.27

Chapter 3

Axial turbines

3.1 Stages of axial turbines

3.1.1 Organization of a stage - 2D flow

A turbine is composed of 2 main stages, the distributor with fixed vanes and the rotor (also called receptor) with rotating blades. The aim is to find the best shape for the vanes and blades in order to have the minimum flow losses. We limit ourselves to the flow through the mean cylinder (flow intersecting the blades and vanes at the mid span).

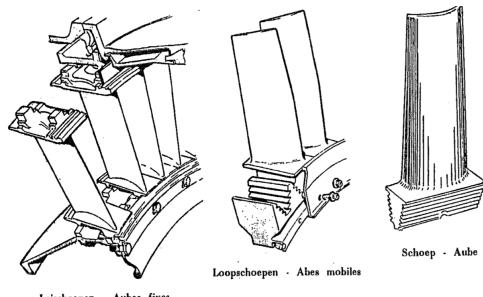
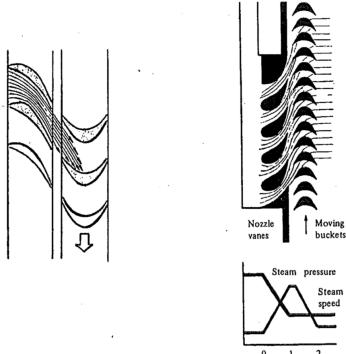


Figure 3.1

Figure 3.2

The 3D turbine will be simplified in a 2D study by considering the distributor and the receptor as a grid of blades with constant distance called **pitch** or **spacing** and a constant span h (while not in 3D) and we consider the flow identical over the span. We can end up with the first figure where we have a limited and non constant span of the blades, no presence of carter and swirling effect on the rotor not considered.

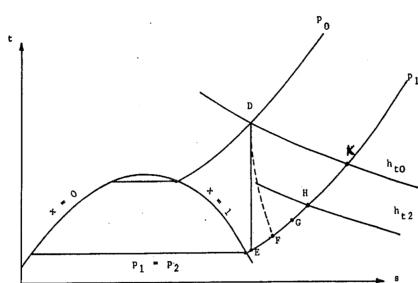


Figure 3.3
can find the total enthalpy variation through the machine.

If we look to the evolution on a T-S diagram, we know the inlet and outlet pressures, so if we define the initial state as D with p_0, t_0, v_0 , we can first consider the isentropic expansion through the stator (E). But isentropic doesn't exist so we consider the losses to arrive at F. Then we go to G through the blades since the only kinetic energy is converted into mechanical energy and not pressure. At the outlet, some kinetic energy remains and this is a loss, so we have to deduce it and arrive at point H to compute the useful energy. By drawing two iso-enthalpic curves we

3.1.2 Impulse stage with one velocity drop

Definition of the stage

The principle of this type of turbine is to first extend the ONLY flow through the vanes of the stator and then to transform kinetic energy into mechanical energy through the rotor. Since no expansion is made on rotor, the rotor blades should have the same inlet and outlet sections as shown on Figure 3.1. One can observe the velocity evolution on the same figure, where only one velocity drop happens, giving the name to the turbine.

Evolution of the gas/steam - Velocity triangles

Computation of the flow velocity v_1 at the outlet of the stator vanes

The expansion in the stator is the stage D to E on Figure 3.3, since the total enthalpy is conserved:

$$h_{t0} = h_{t1} \quad \Rightarrow h_0 + \frac{v_0^2}{2} = h_1 + \frac{v_1^2}{2} \quad \Rightarrow v_1 = \sqrt{v_0^2 + 2(h_0 - h_1)} \quad (3.1)$$

In fact this is not true since losses occur in reality. Let's define the reheat coefficient:

$$\xi = \frac{h_1 - h_{1i}}{h_0 - h_{1i}} \quad (3.2)$$

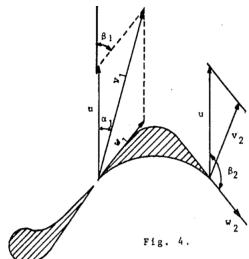
where h_{1i} is the isentropic enthalpy that can be computed by laws and h_1 the real one. This is kind of efficiency factor. We have then that by making appear the equal total enthalpies (considering v_0 negligible):

$$\xi = \frac{\frac{v_{1i}^2}{2} - \frac{v_1^2}{2}}{\frac{v_{1i}^2}{2} - \frac{v_0^2}{2}} = 1 - \left(\frac{v_1}{v_{1i}} \right)^2 = 1 - \varphi^2 \quad \Rightarrow \varphi = \sqrt{1 - \xi} \quad (3.3)$$

where we define the **speed reduction coefficient φ** . The velocity v_1 can thus be expressed in term of h_{1i} replacing in (3.1):

$$v_1 = \sqrt{v_0^2 + 2(1 - \xi)(h_0 - h_{1i})} \approx \varphi \sqrt{2(h_{t0} - h_{1i})} \quad (3.4)$$

where we considered v_0 negligible so that $h_0 = h_{t0}$.



Velocity triangle in section 1 In the figure, for now we only know v_1 . But we can assume to know $u_1 = r_m \omega$ where ω is the rotation speed of the rotor and r_m the mean radius at the entrance of the wheel. To be able to compute all the triangle, we still need the angles. We will consider that in fact α_1 is an angle to fix and thus we are able to compute w_1 but also β_1 the important design angle for the rotor blades:

Figure 3.4

$$w_1^2 = v_1^2 + u_1^2 - 2u_1 v_1 \cos \alpha_1 \quad \cos \beta_1 = \frac{v_1 \cos \alpha_1 - u_1}{w_1} \quad (3.5)$$

Channel in the rotor blades - relative velocity w_2 at the receptor exit We know that the rotor blades should be so that the pressure at inlet and outlet sections should be the same. We can also consider that $u_1 = u_2$ since it depends on the radius and the rotation speed. This applied to the kinetic energy equation we have that:

$$\frac{w_2^2 - w_1^2}{2} = -w_f'' < 0 \quad (3.6)$$

For isentropic flow, so without losses, we should have the same velocity between entrance and outlet. This is not the case in reality since we have losses and following the equation $w_2 < w_1$. Applying energy equation we see that the enthalpy increases:

$$\frac{w_2^2 - w_1^2}{2} = h_1 - h_2 \quad (3.7)$$

This was only qualitative description, to compute these outlet values, we need to know the relative velocity reduction ratio $\psi = \frac{w_2}{w_1}$ that can be known experimentally (around 0.8 - 0.9 in practice) depending on the shape of the receptor blades:

$$w_2 = \psi w_1 \quad h_2 = h_1 + \frac{w_1^2 - w_2^2}{2} = h_1 + (1 - \psi^2) \frac{w_1^2}{2} \quad (3.8)$$

Finally, in order to compute the the inlet and outlet sections, one has to use the mass flow rate equation since the velocities w are known and the density can be determined for a gas using T-S diagram point F (inlet) and G (outlet). Note that for a flow without friction, $w_2 = w_1$ and $h_2 = h_1$ so that $A_2 = A_1$ and F = G.

Shape of the rotor blades As we have seen, in the case of no loss, $w_1 = w_2$ and the flow sections can be chosen identical. This is easily done when we give a symmetric shape to the rotor blades with the complementary solid angles $\bar{\beta}_1, \bar{\beta}_2$ (increased by 90°).

But as we have seen, in reality $w_2 < w_1$ and $\nu_2 > \nu_1$ that forces us to increase the outlet section. This is accomplished with symmetrical blades by increasing the height h of the blades between inlet and outlet.

In a pre-design phase, one will always chose $\bar{\beta}_1 = \beta_1$ the flow angle computed in the velocity triangle in order to avoid shock and separation. If the working conditions are changed further extra losses must be added.

Velocity triangle at the exit of the receptor If we admit that we chose a symmetric blade such that $\bar{\beta}_1 = \beta_1$ and $\bar{\beta}_2 = \pi - \bar{\beta}_1$, as long as the flow in the rotor remains sane, w_2 is tangent to the blade and thus $\beta_2 = \bar{\beta}_2$. Since $u_1 = u_2$ and $w_2 = \psi w_1$, the velocity triangle is computed as:

$$v_2^2 = u_2^2 + w_2^2 - 2u_2 w_2 \cos \beta_2 \quad \cos \alpha_2 = \frac{u_2 + w_2 \cos \beta_2}{v_2} \quad (3.9)$$

Losses in the rotor channel The lost energy corresponds to the area under the curve FG on the TS diagram, or given by the formula:

$$w_f'' = h_2 - h_1 = \frac{w_1^2 - w_2^2}{2} = (1 - \psi^2) \frac{w_1^2}{2} \quad (3.10)$$

Losses at the receptor exit At the exit, the fluid has still kinetic energy corresponding to $\frac{v_2^2}{2}$ which is lost. This energy corresponds to the projection area under GH. A part of this could be recuperated in a second stage.

Power on the wheel shaft (P_R)

The power on the shaft is given by the Euler-Rateau equation:

$$P_R = \dot{m}_R u (v_1 \cos \alpha_1 - v_2 \cos \alpha_2) = \dot{m}_R \left(\frac{v_1^2 - v_2^2}{2} - \frac{w_1^2 - w_2^2}{2} \right) = \dot{m}_R (\underbrace{h_{t1} - h_{t2}}_{h_{t0}}) \quad (3.11)$$

We see from this formula that the power can be computed by the total enthalpy difference. We have also:

$$P_R = \dot{m}_R \left(\frac{v_1^2 - v_2^2}{2} + \int_{p_2}^{p_1} -w_f'' \right) \Rightarrow \dot{m}_R \frac{v_1^2 - v_2^2}{2} = P_R + \dot{m}_R w_f'' \quad (3.12)$$

Where the pressure variation is null through the rotor and we see that we find the same explanations we've made. The torque applied on the blades is:

$$P_R / \omega = \dot{m}_R (v_1 \cos \alpha_1 - v_2 \cos \alpha_2) r_m \quad (3.13)$$

This shows how the variation of v in amplitude and angle gives a torque. The intersection of the iso enthalpy curve h_{t0} with $p_2 = p_1$ (point K) is represented on the same figure. The extracted energy is given by the area under HK:

$$HK = h_{t1} - h_{t2} = P_R / \dot{m}_R \quad (3.14)$$

Degree of reaction

By definition it is the ratio between the power of the fluid in a reactive working and the total power to the rotor:

$$R = \frac{(P_R)_{react}}{P_R} = \frac{\frac{w_2^2 - w_1^2}{2}}{\frac{v_1^2 - v_2^2}{2} + \frac{w_2^2 - w_1^2}{2}} = \frac{\int_{p_2}^{p_1} \nu dp - w_f''}{\frac{v_1^2 - v_2^2}{2} + \int_{p_2}^{p_1} \nu dp - w_f''} \approx 0 \quad (3.15)$$

This is nearly 0 since the difference in v is very small and the pressure constant over the blade. It would be strictly 0 if there was no friction, this is why this kind of blade is an impulse or action stage.

Stage efficiency – Pre-design

Stage efficiency This is by definition the ratio of the power of the stage (delivered to the rotor) and the theoretical available power that is obtained by product of \dot{m}_R with the kinetic energy available after isentropic and complete expansion, and no remaining energy at the exit of the rotor. The theoretical power and the efficiency are:

$$\dot{m}_R \frac{v_{1i}^2}{2} = \dot{m}_R (h_{t0} - h_{1i}) \Rightarrow \eta_E = \frac{\dot{m}_R u (v_1 \cos \alpha_1 - v_2 \cos \alpha_2)}{\dot{m}_R \frac{v_{1i}^2}{2}} = \frac{h_{t0} - h_{t2}}{h_{t0} - h_{1i}} = \eta_D \eta_R \quad (3.16)$$

also the product of distributor and rotor efficiency since $\frac{\dot{m}_R \frac{v_1^2}{2}}{\dot{m}_R \frac{v_{1i}^2}{2}} \frac{\dot{m}_R u(v_1 \cos \alpha_1 - v_2 \cos \alpha_2)}{\dot{m}_R \frac{v_1^2}{2}}$. Previously

we said α_1 and u are chosen, let's see how to choose the most efficient. If $\bar{\beta}_1$ is chosen tangent to w_1 , there is no shock and thus the coefficient of reduction $\psi = \psi_r$ depends on the friction in the rotor. Then, if one consider a symmetric blade, these relations in the velocity triangle can be made:

$$v_2 \cos \alpha_2 = u + w_2 \cos \beta_2 = u - \psi_R w_1 \cos \beta_1 = u - \psi_r (v_1 \cos \alpha_1 - u) \quad (3.17)$$

and after replacing in the definition of $\eta_E = \eta_D \eta_R$:

$$\eta_E = 2\eta_D \frac{u}{v_1} \left[\cos \alpha_1 - \frac{u}{v_1} + \psi_r \left(\cos \alpha_1 - \frac{u}{v_1} \right) \right] = f(\eta_D, \alpha_1, \frac{u}{v_1}, \psi_r) \quad (3.18)$$

where $\eta_D = \frac{v_1^2}{v_{1i}^2} = \varphi^2 = 1 - \xi$ as demonstrated previously. $\xi = \frac{u}{v_1}$ is the **speed coefficient** and thus:

$$\eta_E = 2\eta_D \xi (1 + \psi_r) (\cos \alpha_1 - \xi) \quad (3.19)$$

Optimal values of the elements in the velocity triangles η_D depends on α_1 related to the camber of the distributor blades, on v_1 depending on the pressure drop P_0/P_1 that depends on the shape of the distributor (convergent/divergent). The velocity coefficient ψ is also function of α_1 and v_1 since it depends on the difference $\bar{\beta}_2 - \bar{\beta}_1$. ψ_r depends also on w_1 . Due to lack of information, we can just suppose that since these parameters are limited η_D and ψ are constant and we will try to optimize using ξ and α_1 .

The maximum stage efficiency η_E in function of ξ is obtained for null derivative (do it as exercise it's ok for me):

$$\xi_{opt} = \frac{\cos \alpha_1}{2} \quad \Rightarrow \eta_E = 2\eta_D (1 + \psi_r) \xi_{opt}^2 \quad (3.20)$$

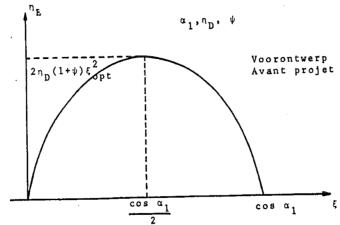


Figure 3.5
between 0.8-0.95 for $\alpha_1 \approx 20^\circ$ and the maximum stage efficiency is around 0.8.

On basis of this, we can see that the maximum efficiency is obtained for maximum $\cos \alpha_1$ and thus minimum α_1 . But small α_1 means smaller axial component, larger vertical component, larger flow section required and thus longer vanes/blades. Moreover, the stator vanes must have higher curvature and larger chord. This is negative effects and the angle is chosen between 15-25° in practice. The evolution of η_E in function of ξ is shown on the figure. The value of η_D is around 0.9-0.96, ψ_r

Selection of a speed coefficient different from the optimum