

1.723 HW5

Sachith Dunatunga

April 2, 2015

1 Problem 1

1.1 Part 1

The steady-state flow equation is given by

$$\nabla \cdot \mathbf{u} = 0 \quad (1)$$

where

$$\mathbf{u} = -\lambda(x, y) \nabla p. \quad (2)$$

For a single cell with center at (i, j) , we want to integrate

$$\int_{\Omega_{i,j}} \nabla \cdot \mathbf{u} \, dV = 0 \quad (3)$$

This is converted to a flux from all the surfaces $(i + 1/2, j)$, $(i - 1/2, j)$, $(i, j + 1/2)$, and $(i, j - 1/2)$ via the divergence theorem, yielding

$$\int_{\Gamma_{i+1/2,j}} \mathbf{u} \cdot \mathbf{n} \, dS + \int_{\Gamma_{i-1/2,j}} \mathbf{u} \cdot \mathbf{n} \, dS + \int_{\Gamma_{i,j+1/2}} \mathbf{u} \cdot \mathbf{n} \, dS + \int_{\Gamma_{i,j-1/2}} \mathbf{u} \cdot \mathbf{n} \, dS = 0, \quad (4)$$

which can be expanded to

$$\int_{\Gamma_{i+1/2,j}} u_{i+1/2,j}^x(1) \, dS + \int_{\Gamma_{i-1/2,j}} u_{i-1/2,j}^x(-1) \, dS + \int_{\Gamma_{i,j+1/2}} u_{i,j+1/2}^y(1) \, dS + \int_{\Gamma_{i,j-1/2}} u_{i,j-1/2}^y(-1) \, dS = 0. \quad (5)$$

Define the transmissibilities as

$$T_{i+1/2,j}^x = \bar{\lambda}_{i+1/2,j} \frac{\delta y}{\delta x} \quad (6)$$

$$T_{i-1/2,j}^x = \bar{\lambda}_{i-1/2,j} \frac{\delta y}{\delta x} \quad (7)$$

$$T_{i,j+1/2}^y = \bar{\lambda}_{i,j+1/2} \frac{\delta x}{\delta y} \quad (8)$$

$$T_{i,j-1/2}^y = \bar{\lambda}_{i,j-1/2} \frac{\delta x}{\delta y} \quad (9)$$

where

$$\bar{\lambda}_{i+1/2,j} = 2 (\lambda_{i,j}^{-1} + \lambda_{i+1,j}^{-1})^{-1} \quad (10)$$

$$\bar{\lambda}_{i-1/2,j} = 2 (\lambda_{i,j}^{-1} + \lambda_{i-1,j}^{-1})^{-1} \quad (11)$$

$$\bar{\lambda}_{i,j+1/2} = 2 (\lambda_{i,j}^{-1} + \lambda_{i,j+1}^{-1})^{-1} \quad (12)$$

$$\bar{\lambda}_{i,j-1/2} = 2 (\lambda_{i,j}^{-1} + \lambda_{i,j-1}^{-1})^{-1}. \quad (13)$$

Using the two point flux approximation, we can write the surface integrals as

$$\int_{\Gamma_{i+1/2,j}} u_{i+1/2,j}^x(1) \, dS = T_{i+1/2,j}^x(p_{i,j} - p_{i+1,j}) \quad (14)$$

$$\int_{\Gamma_{i-1/2,j}} u_{i-1/2,j}^x(-1) \, dS = T_{i-1/2,j}^x(p_{i,j} - p_{i-1,j}) \quad (15)$$

$$\int_{\Gamma_{i,j+1/2}} u_{i,j+1/2}^y(1) \, dS = T_{i,j+1/2}^y(p_{i,j} - p_{i,j+1}) \quad (16)$$

$$\int_{\Gamma_{i,j-1/2}} u_{i,j-1/2}^y(-1) \, dS = T_{i,j-1/2}^y(p_{i,j} - p_{i,j-1}), \quad (17)$$

which allows us to write the sum of fluxes as

$$\begin{aligned} & -T_{i+1/2,j}^x p_{i+1,j} \\ & -T_{i-1/2,j}^x p_{i-1,j} \\ & (T_{i+1/2,j}^x + T_{i-1/2,j}^x + T_{i,j+1/2}^y + T_{i,j-1/2}^y) p_{i,j} \\ & -T_{i,j+1/2}^y p_{i,j+1} \\ & -T_{i,j-1/2}^y p_{i,j-1} = 0. \end{aligned}$$

Using a global numbering $I = f(i, j)$, e.g. $I = N_x i + j$, we can write this as a system of equations for unknown p_I .

Note that the above equation only applies in the interior of the domain. On the boundaries, we must rederive the equations. Setting the transmissibilities to zero suffices to set no-flow boundary conditions. On boundaries where the pressure is known, we must double the interior cell transmissibility; e.g. on the top right corner of the quarter five point, we set

$$T_{N_x+1/2,N_y}^x = 2\lambda_{N_x,N_y} \frac{\delta y}{\delta x} \quad (18)$$

$$T_{N_x,N_y+1/2}^y = 2\lambda_{N_x,N_y} \frac{\delta x}{\delta y} \quad (19)$$

and the boundary term is added in the load vector

$$b_{N_x N_y} = T_{N_x+1/2,N_y}^x \bar{p} + T_{N_x,N_y+1/2}^y \bar{p}. \quad (20)$$

On the inflow boundary (the bottom left cell), we already know the integrated flux entering the system, so we simply replace those integrals in the sum for that cell.

$$\int_{\Gamma_{i+1/2,j}} u_{i+1/2,j}^x(1) \, dS = T_{i+1/2,j}^x(p_{i,j} - p_{i+1,j}) \quad (21)$$

$$\int_{\Gamma_{i-1/2,j}} u_{i-1/2,j}^x(-1) \, dS = -Q/2 \quad (22)$$

$$\int_{\Gamma_{i,j+1/2}} u_{i,j+1/2}^y(1) \, dS = T_{i,j+1/2}^y(p_{i,j} - p_{i,j+1}) \quad (23)$$

$$\int_{\Gamma_{i,j-1/2}} u_{i,j-1/2}^y(-1) \, dS = -Q/2, \quad (24)$$

which becomes

$$\begin{aligned} & -T_{i+1/2,j}^x p_{i+1,j} \\ & (T_{i+1/2,j}^x + T_{i,j+1/2}^y) p_{i,j} \\ & -T_{i,j+1/2}^y p_{i,j+1} = Q. \end{aligned}$$

We can achieve this by setting the transmissibilities to zero and adding into the load vector

$$b_1 = Q. \quad (25)$$

For the tracer transport we have

$$\frac{\partial c}{\partial t} + \nabla \cdot (\mathbf{u}c - \frac{1}{\text{Pe}} \nabla c) = 0 \quad (26)$$

Using the solution from the pressure equation, we can obtain the velocity via

$$u_{i+1/2,j}^x = T_{i+1/2,j}^x * (p_{i,j} - p_{i+1,j}) \quad (27)$$

$$u_{i-1/2,j}^x = T_{i-1/2,j}^x * (p_{i,j} - p_{i-1,j}) \quad (28)$$

$$u_{i,j+1/2}^y = T_{i,j+1/2}^y * (p_{i,j} - p_{i,j+1}) \quad (29)$$

$$u_{i,j-1/2}^y = T_{i,j-1/2}^y * (p_{i,j} - p_{i,j-1}) \quad (30)$$

For upwinding, we look at the signs of u_x and u_y . If the sign of u_x is positive, we take $F_{i+1/2,j}^x$ as $u_{i+1/2,j}^x c_{i,j}$, otherwise we use $u_{i+1/2,j}^x c_{i+1,j}$, and similarly for the y component. For the diffusive flux, we use the two point flux approximation, meaning we take $F_{i+1/2,j}^x = \frac{1}{\text{Pe}}(c_{i,j} - c_{i+1,j}) \frac{\delta y}{\delta x}$, and similarly for the y component.

1.2 Part 2

Here we show three different permeability fields generated using the same parameters as we are to use for the rest of the problem. They look mostly the same, but the scale is different.

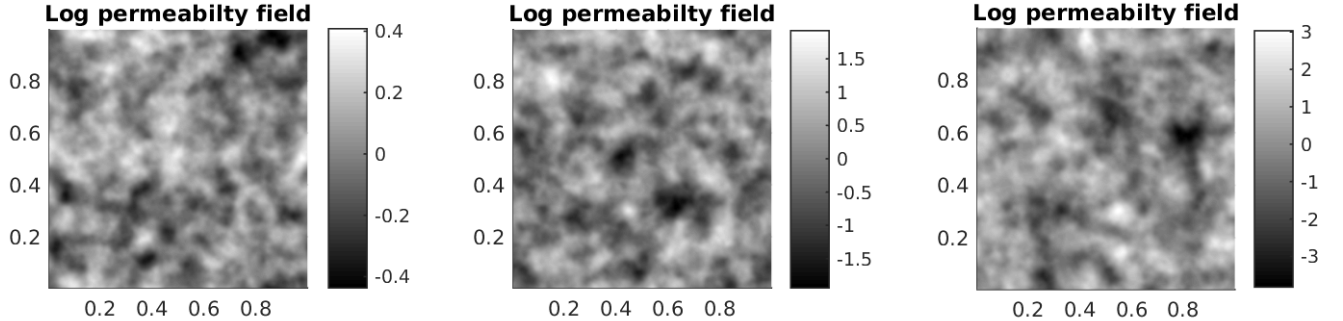


Table 1: Here the variance in log of k varies from 0.1 to 2 to 5 (left to right). The correlation lengths are both $5dx$, where $dx = 1/200$.

Increasing the correlation length in these next images makes larger blocks of similar values.

1.3 Part 3

The code is provided in the zip file, but the main integration routine is reproduced below.

```
function [ cm, ta, p ] = integrate_scalar_tracer_equation_2d( Nx, Ny, var_lnk, Pe, dt, tf )
%INTEGRATE_SCALAR_TRACER_EQUATION_2D Solves 2D linear scalar transport equation
%using finite volumes.
% Nx - number of grid cells in x
% Ny - number of grid cells in y
% Pe - Peclet number
% dt - time step size
% tf - max time
```

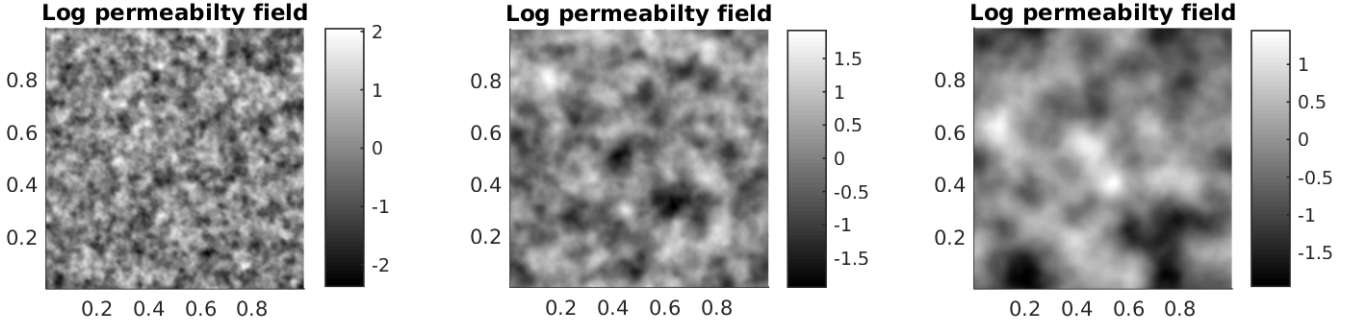


Table 2: Here the variance in log of k is constant at 2. The correlation lengths are equal to each other, but vary from $2dx$, to $5dx$, to $20dx$ from left to right (again $dx = 1/200$).

```
%
% Returns Nx x Ny x (# times) matrix xm containing cell point locations,
% 1 x (# times) matrix cm containing top right cell concentrations at different times,
% 1 x (# times) matrix ta containing actual times data is saved at.
% Nx x Ny matrix containing pressure field.

Lx = 1;
Ly = 1;
hx = Lx / Nx;
hy = Ly / Ny;
x = linspace(0+hx/2.0, Lx-hx/2.0, Nx);
y = linspace(0+hy/2.0, Ly-hy/2.0, Ny);
[X,Y] = meshgrid(x,y);
X = X';
Y = Y';

corr_lenx = 4*hx;
corr_leny = 4*hy;

[perm,var_lnk_actual]= random_perm(var_lnk,corr_lenx,corr_leny,Nx,Ny,Lx,Ly);
perm = perm';
kinv = 1./perm;

lambda_bar_x = zeros(Nx+1,Ny);
lambda_bar_x(2:end-1,:) = (hy / hx) * 2 ./ (kinv(2:Nx,:) + kinv(1:Nx-1,:));
lambda_bar_y = zeros(Nx,Ny+1);
lambda_bar_y(:,2:end-1) = (hx / hy) * 2 ./ (kinv(:,2:Ny) + kinv(:,1:Ny-1));

% Set BCs (default is no-flow)
b = zeros(Nx,Ny);
b(1,1) = 1;

lambda_bar_x(end,end) = (hy / hx) * 2 * perm(end,end);
lambda_bar_y(end,end) = (hx / hy) * 2 * perm(end,end);

% make diagonals
T_x_left = reshape(lambda_bar_x(1:end-1, :)', [], 1);
T_x_right = reshape(lambda_bar_x(2:end, :)', [], 1);
T_y_bottom = reshape(lambda_bar_y(:, 1:end-1)', [], 1);
T_y_top = reshape(lambda_bar_y(:, 2:end)', [], 1);

sumT = T_x_right + T_x_left + T_y_bottom + T_y_top;
diags = [-T_x_left, -T_y_bottom, sumT, -T_y_top, -T_x_right];

% assemble matrix
A = spdiags(diags, [Ny;1;0;-1;-Ny], Nx*Ny, Nx*Ny)';
bv = reshape(b, [], 1);

% solve for pressure
pv = A \ bv;
p = reshape(pv, Nx, Ny);
```

```

% show plots and save pressure
% figure; surf(X,Y,log(perm),'edgecolor','none'); view([0, 0, 1]);
% figure; surf(X,Y,p,'edgecolor','none'); view([0, 0, 1]);
% h = figure; plot(x, diag(p) - p(end/2,end/2));
% set(h, 'units', 'inches', 'position', [1 1 3 3])
% set(h, 'PaperUnits','centimeters');
% set(h, 'Units','centimeters');
% pos=get(h,'Position');
% set(h, 'PaperSize', [pos(3) pos(4)]);
% set(h, 'PaperPositionMode', 'manual');
% set(h, 'PaperPosition',[0 0 pos(3) pos(4)]);
% fname = sprintf('figs/pressure_%d_%d.png', 10*var_lnk, Nx);
% title(sprintf('Pressure along diagonal\n(N = %d)', Nx));
% xlabel('Coordinate');
% ylabel('Pressure');
% print(fname, '-dpng');

% calculate integrated velocities
ux_int = lambda_bar_x(2:end-1, :).*(p(1:end-1, :) - p(2:end, :));
uy_int = lambda_bar_y(:, 2:end-1).*(p(:, 1:end-1) - p(:, 2:end));
zx = zeros(1, size(ux_int, 2));
zy = zeros(size(uy_int, 1), 1);
ux = [zx; ux_int; zx];
uy = [zy; uy_int; zy];
ux(1,1) = 1/2;
uy(1,1) = 1/2;
ux(end,end) = 1/2;
uy(end,end) = 1/2;

% draw approximate velocities on perm field
% scale = 0.1;
% figure; h = surf(X,Y,zeros(size(X)), log(perm),'edgecolor','none'); view([0, 0, 1]);
% axis equal square;
% hold on;
% quiver(X,Y,scale*(ux(1:end-1,:)+ux(2:end, :))/2, scale*(uy(:, 1:end-1) + uy(:, 2:end))/2, '
    Autoscale','off', 'color', [0,0,0]);
% hold off;

t = 0;
i = 1;
c = zeros(Nx, Ny);
while (t < tf)
    t = t + dt;
    ta(i) = t;
    cm(i) = c(end,end);
    c(1,1) = 1;

    Fx_adv = ux_int.*(ux_int > 0).*(c(1:end-1, :) + ux_int.*(ux_int < 0).*(c(2:end, :));
    zFx = zeros(1, size(Fx_adv, 2));
    Fx_adv = [zFx; Fx_adv; zFx];

    Fy_adv = uy_int.*(uy_int > 0).*(c(:, 1:end-1) + uy_int.*(uy_int < 0).*(c(:, 2:end));
    zFy = zeros(size(Fy_adv, 1), 1);
    Fy_adv = [zFy; Fy_adv; zFy];

    Fx_diff = (1 / Pe) * (hy / hx) * (c(1:end-1, :) - c(2:end, :));
    Fx_diff = [zFx; Fx_diff; zFx];

    Fy_diff = (1 / Pe) * (hx / hy) * (c(:, 1:end-1) - c(:, 2:end));
    Fy_diff = [zFy; Fy_diff; zFy];

    Fx = Fx_adv + Fx_diff;
    Fy = Fy_adv + Fy_diff;

    Fx(1,1) = 1/2;
    Fy(1,1) = 1/2;
    Fx(end,end) = c(end,end)*1/2;
    Fy(end,end) = c(end,end)*1/2;

    dc = (dt / (hx * hy)) * (Fx(1:end-1,:) - Fx(2:end, :) + Fy(:, 1:end-1) - Fy(:, 2:end));
    c = c + dc;

    % plot concentration
    % surf(X,Y,c, 'edgecolor', 'none');
    % view([0 0 1]);
    % colormap(hot);
    % drawnow;

    i = i + 1;
end

```

end

Listing 1: integrate_scalar_tracer_equation_2d.m

1.4 Part 4

We plot the pressure along the diagonal over multiple grid spacings. For low variance (0.1), we see that the solution looks like that for a point source and a point sink, as expected. When the variance is larger though we see a lot of inhomogeneity both within the solution and also between solutions (the curves don't look like they will converge to anything, although I'm sure there is a 'distribution average'). The pressures themselves seem to be higher with increasing range in permeabilities.

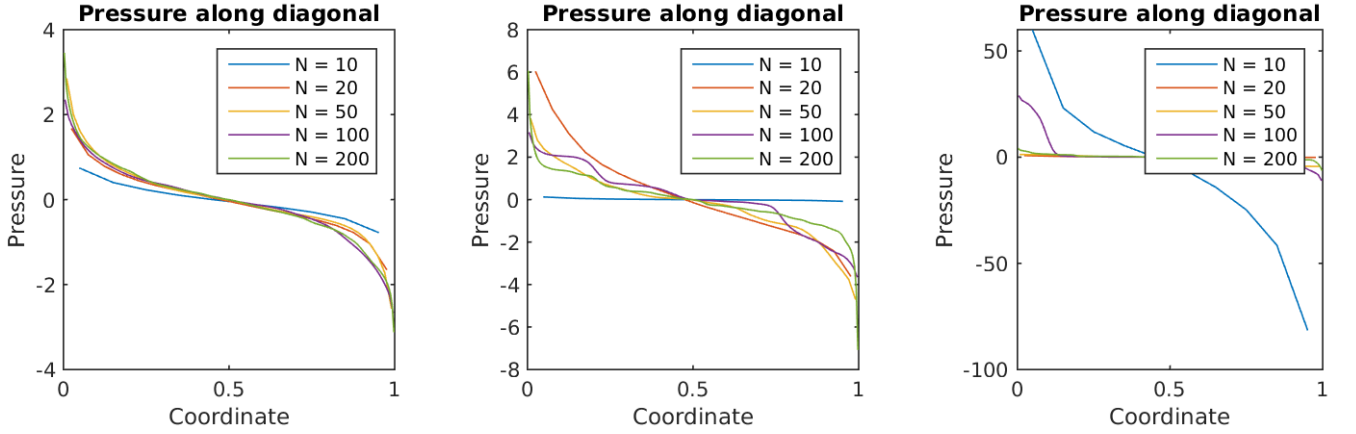


Table 3: The pressure along the diagonal is plotted for multiple grid spacings for various variances in log permeability (0.1, 2, and 5 from left to right).

1.5 Part 5

Although I tried to use $N = 200$, the timestep restrictions were too severe for my patience (my code may be especially inefficient, I'm not sure). The following graphs are done at $N = 40$ instead. We note that first

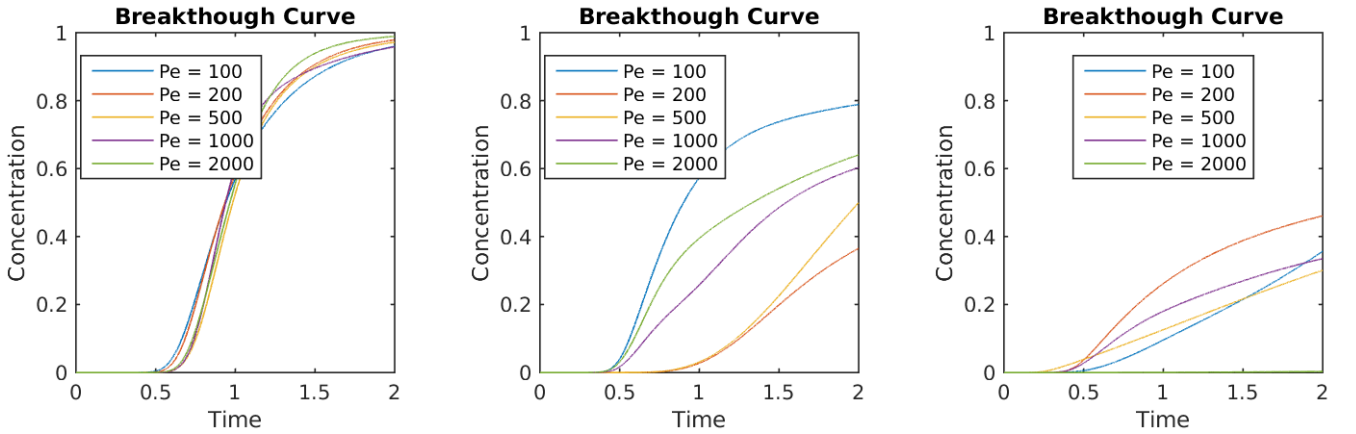


Table 4: The breakthrough curves at varying Peclet number for various variances in log permeability (0.1, 2, and 5 from left to right).

of all, there is significant variation in the curves for larger variation in permeability, which is expected. We

also notice that, in general, with larger variation in permeability, the initial time to nonzero concentration is lessened, but the time to saturation is also increased. A larger Peclet number appears to “sharpen” the curve in the low variance case, which makes sense since it means means diffusion is less significant to the tracer motion compared to advection. I can’t see a general trend with Peclet number in the larger variance cases though, which is surprising to me.