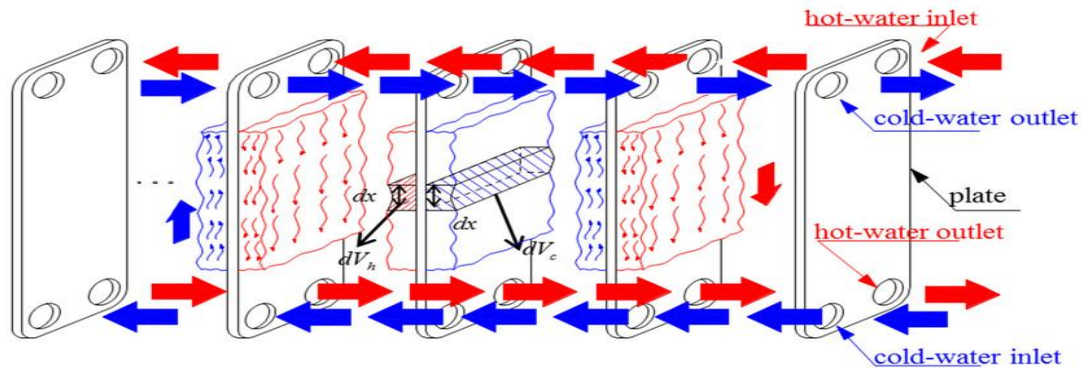


Characterization of a Plate Heat Exchanger



https://www.researchgate.net/figure/Heat-transfer-process-of-the-plate-heat-exchanger-PHE_fig1_319695150

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<https://wcruk.com/what-is-a-plate-heat-exchanger/>

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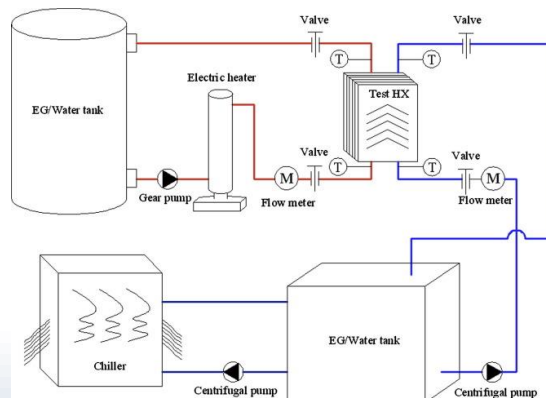
This presentation focuses on characterizing a plate heat exchanger and comparing it to theory

$$Nu = C_1 Re^{C_2} Pr^{\frac{1}{3}} \quad U_{meas} = \frac{Q}{A_{proj} \Delta T_{LMTD}}$$

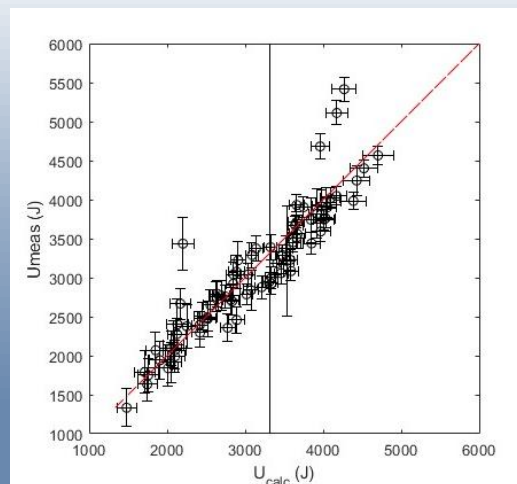
$$Q = \frac{m_h c_h (T_{h,i} - T_{h,o}) - m_c c_c (T_{c,i} - T_{c,o})}{2}$$

$$\frac{1}{A_{proj} h_h} = \frac{1}{A_{proj} U_{calc}} - \frac{t}{A_{proj} k_w} - \frac{1}{A_{proj} h_c}$$

Note relevant heat transfer equations



Record steady state data



Compare real characteristics to theoretical

The Nusselt number characterizes heat transfer of the system

experimentally found (same for hot and cold fluid)

$$Nu = C_1 Re^{C_2} Pr^{\frac{1}{3}}$$

$$\frac{\text{convective heat transfer}}{\text{conductive heat transfer}} = \frac{hL}{k}$$

$$\frac{\text{Momentum Diffusivity}}{\text{Heat Diffusivity}} = \frac{C_p \mu}{k}$$

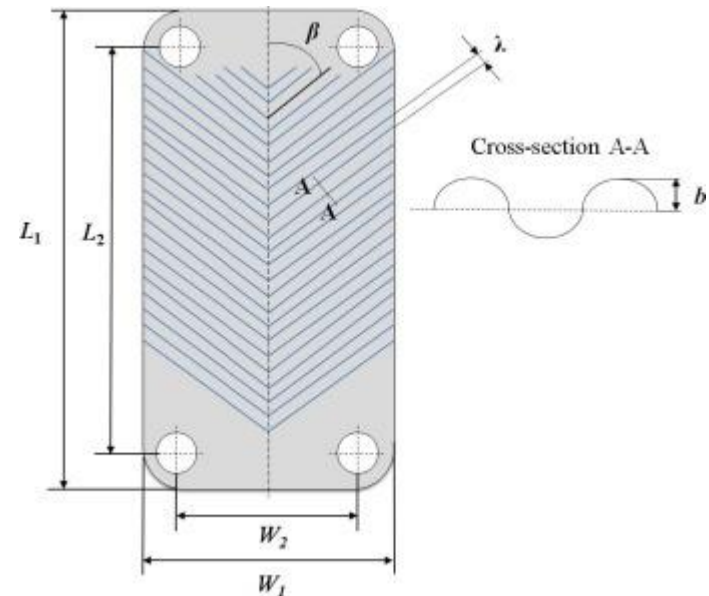
$$\frac{\text{inertial forces}}{\text{viscous forces}} = \frac{\rho v L}{\mu}$$

Theoretical and measured overall heat transfer coefficients can be found and compared

Theoretical

$$\frac{1}{A_{proj} h_h} = \frac{1}{A_{proj} U_{calc}} - \frac{t}{A_{proj} k_w} - \frac{1}{A_{proj} h_c}$$

$$A_{proj} = L_2 \times W_1$$



<https://doi.org/10.1016/j.applthermaleng.2016.10.147>

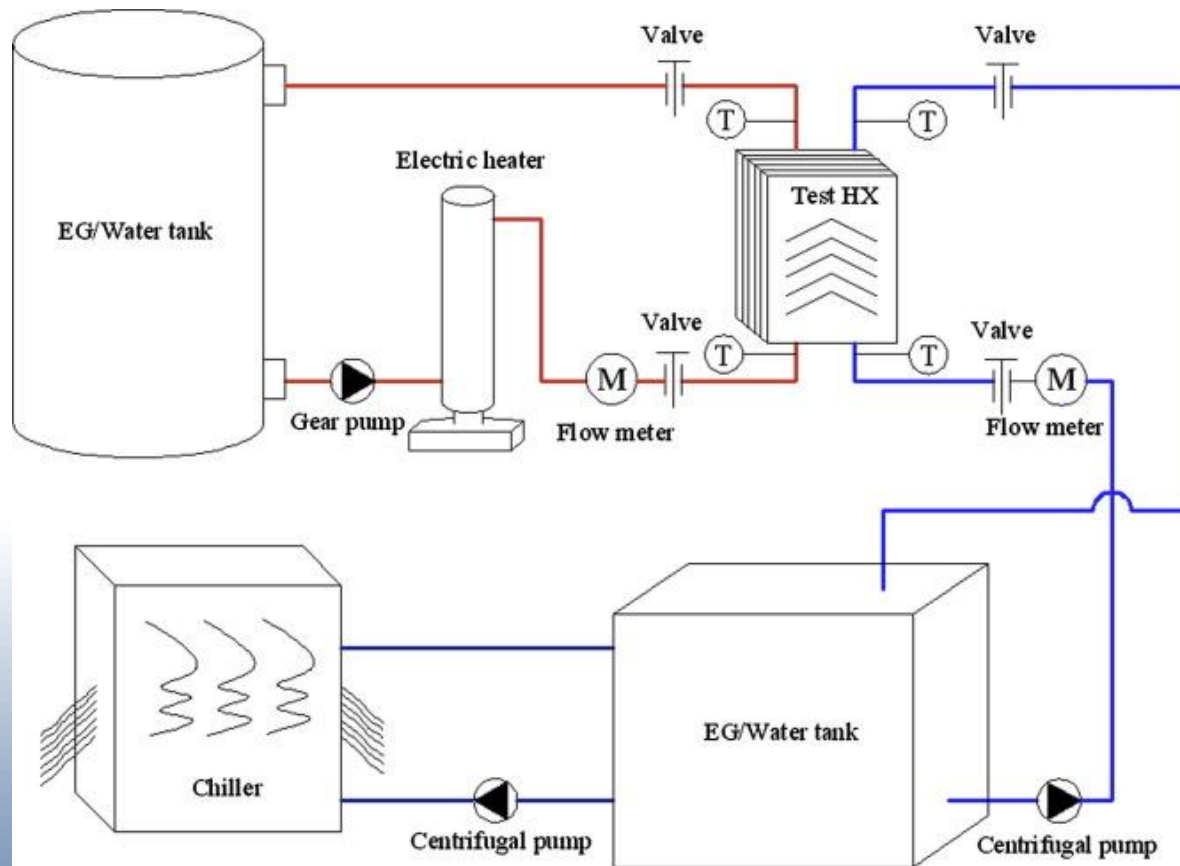
Measured

$$U_{meas} = \frac{Q}{A_{proj} \Delta T_{LMTD}}$$

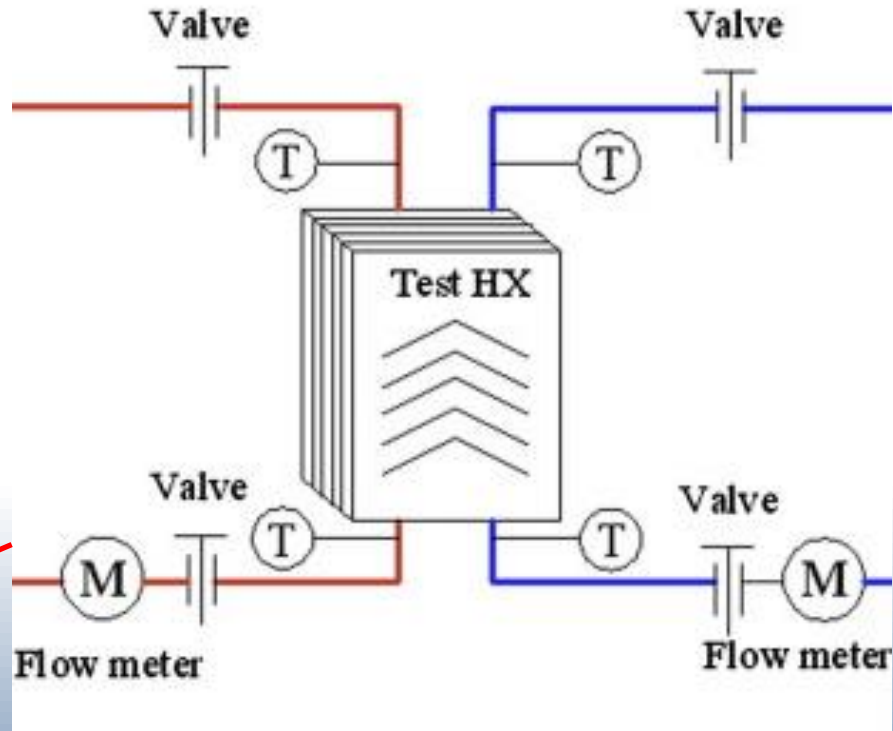
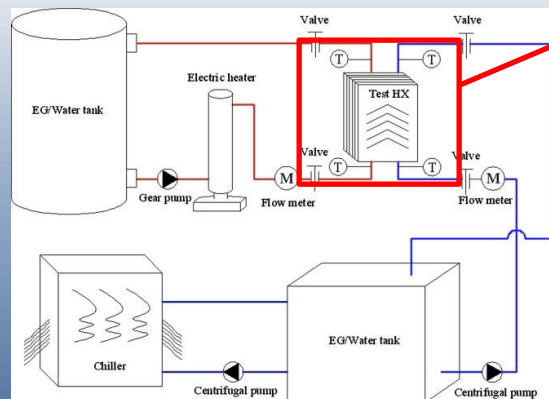
$$Q = \frac{m_h c_h (T_{h,i} - T_{h,o}) - m_c c_c (T_{c,i} - T_{c,o})}{2}$$

$$\Delta T_{LMTD} = \frac{\Delta T_{in} - \Delta T_{out}}{\ln \frac{\Delta T_{in}}{\Delta T_{out}}}$$

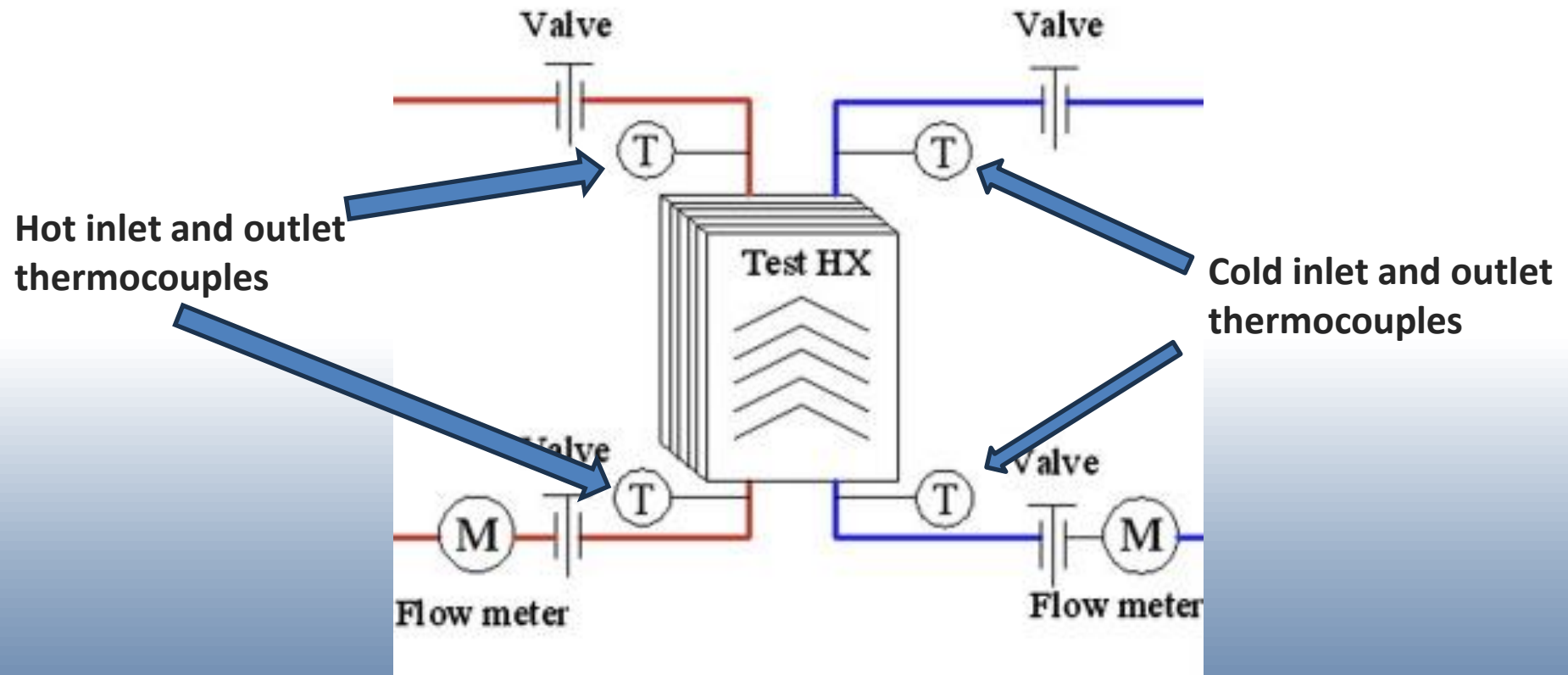
Temperature and flow rates should be collected and plugged into the previous equation



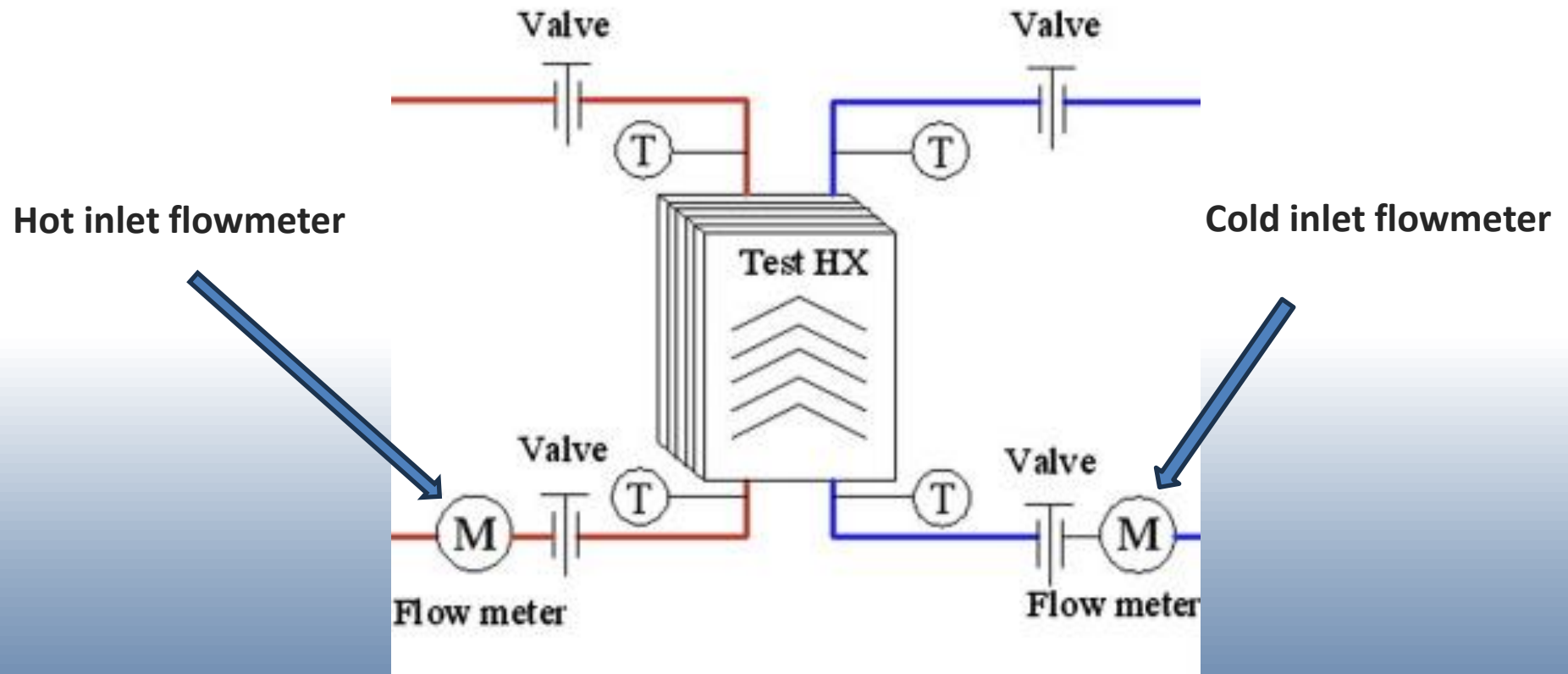
Temperature and flow rates should be collected and plugged into the previous equation



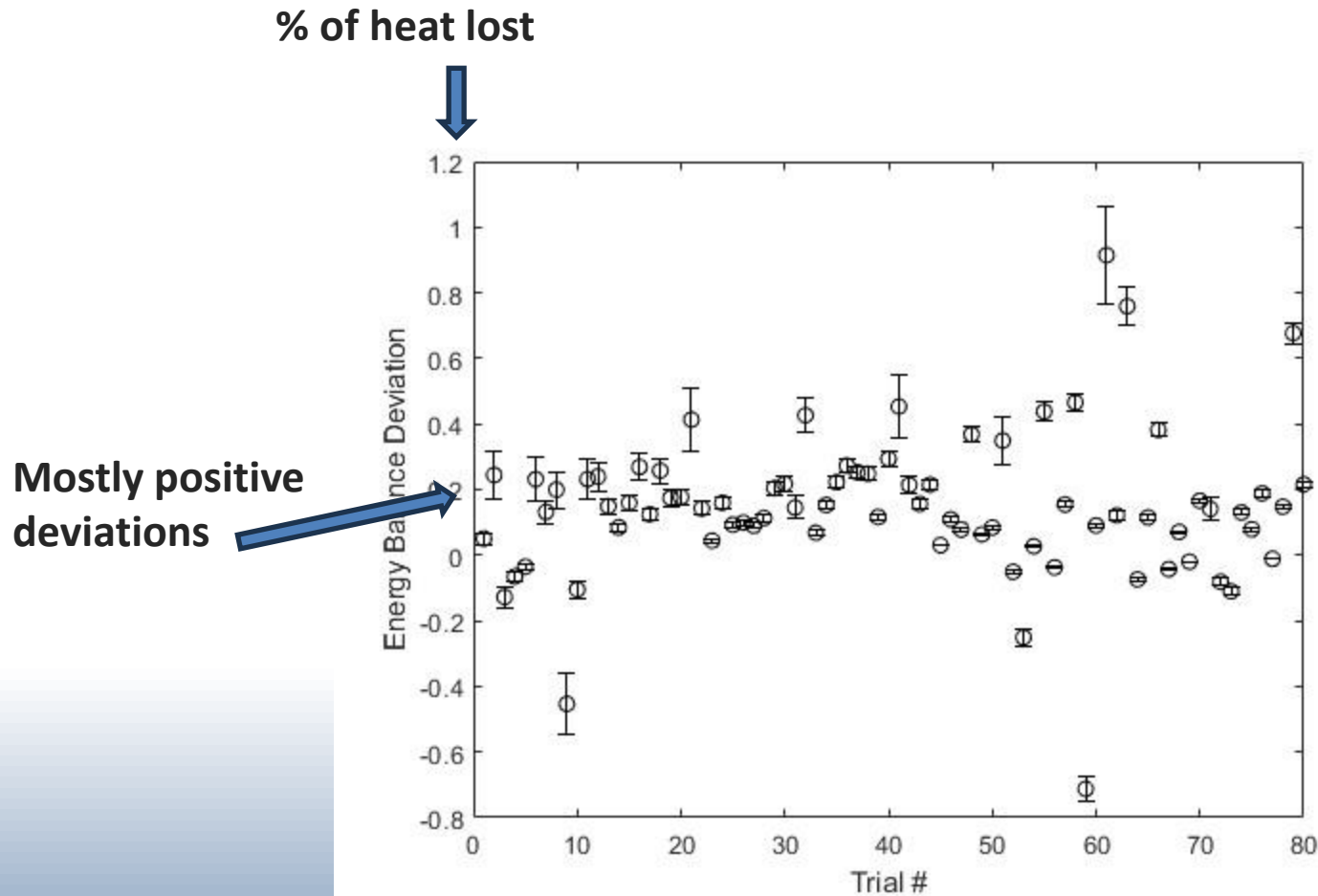
Temperature and flow rates should be collected and plugged into the previous equation



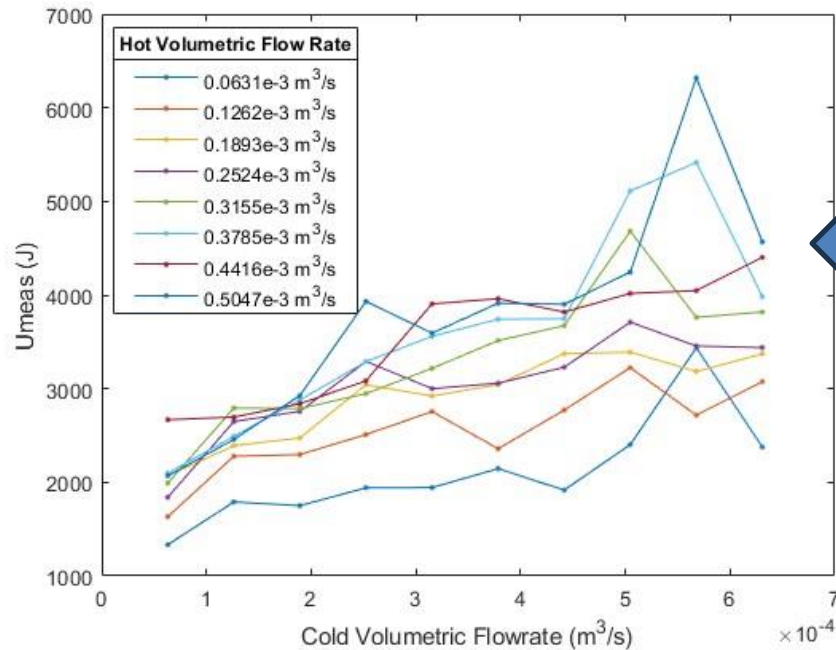
Temperature and flow rates should be collected and plugged into the previous equation



Heat losses seen through deviations in energy balance

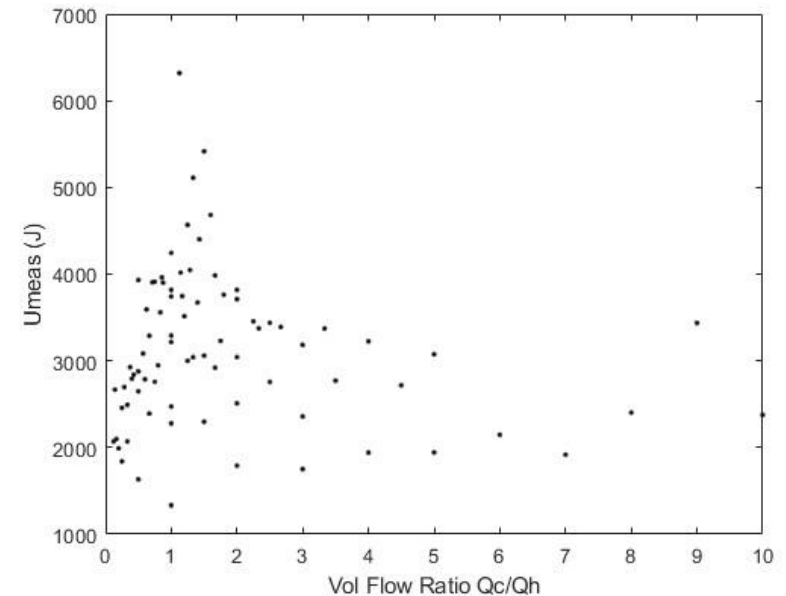


Effects of changing the hot and cold flowrates

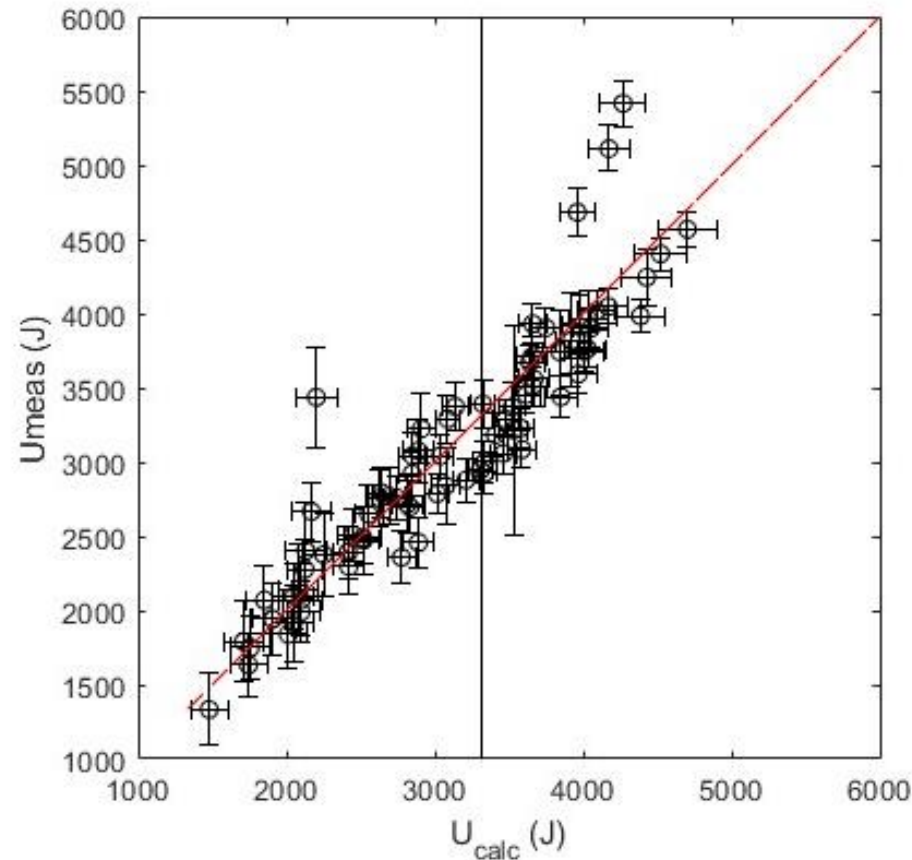


Increasing the flow rates improves heat transfer

Heat transfer is better at 1:1 hot and cold flow rates



Theoretical and measured data confirm accurate data and low inefficiencies



In conclusion, a reliable correlation was drawn between the Nusselt number, Reynolds number, and Prandtl number.

The correlation is as follows:

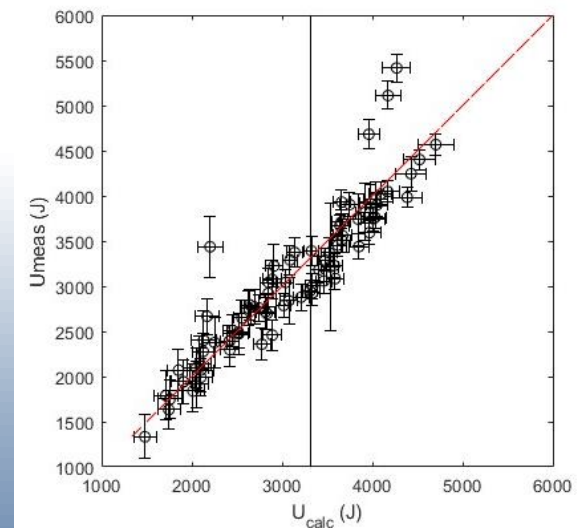
$$Nu = 0.4 Re^{0.60} Pr^{\frac{1}{3}}$$

which is confirmed by the correlation between measured and calculated overall heat coefficients

Coefficients

$$C_1 = 0.4 \pm 0.2$$

$$C_2 = 0.60 \pm 0.06$$



Questions?