

Large Eddy Simulation: Practical issues

Filtering, modelling, and errors
wall-modeling
turbulence injection

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Large eddy simulations: Practical issues

LES: A brief reminder

NS equation and turbulence

LES, filtering and models

Numerics, errors and LES

Implicit LES

Wall treatment

Wall-bounded turbulence

The logarithmic law-of-the-wall

Wall-modeled LES: analytical, TBLE

Detached-Eddy Simulations

Log-layer mismatch and applications

Turbulence injection

Synthetic methods (Fourier / POD)

Precursor method

Wall-bounded turbulent injection



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NS equations and turbulence

Compressible NS equations:

$$\frac{\partial \rho}{\partial t} + \frac{\partial \rho u_i}{\partial x_i} = 0$$

$$\frac{\partial \rho u_i}{\partial t} + \frac{\partial \rho u_i u_j}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \frac{\partial \tau_{ij}}{\partial x_j}$$

$$\frac{\partial \rho E}{\partial t} + \frac{\partial \rho E u_j}{\partial x_j} = \frac{\partial u_i \tau_{ij}}{\partial x_j} - \frac{\partial q_j}{\partial x_j}$$

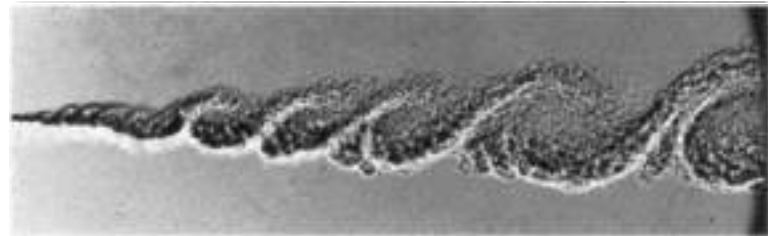
Viscous stress tensor

$$\tau_{ij} = -p\delta_{ij} + \mu\left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i}\right) - \frac{2}{3}\mu\frac{\partial u_k}{\partial x_k}\delta_{ij}$$

Heat flux

$$q_j = -\lambda \frac{\partial T}{\partial x_j}$$

Navier Stokes equations: **Non linearity** leads to **turbulence**!



Determinist: For 1 initial condition => 1 unique solution

Hardly-predictible: An initial perturbation amplifies on a **large range** of scale.



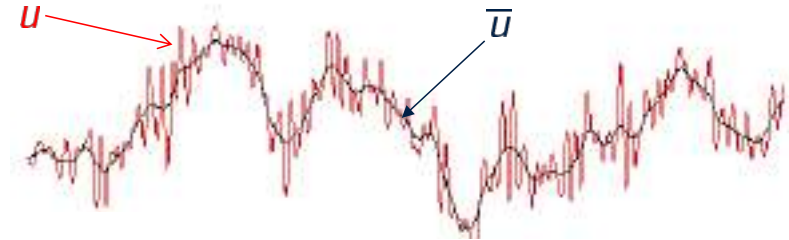
Turbulence

Reynolds Averaging and fluctuation

Reynolds decomposition:

$$u = \bar{u} + u'$$

RANS decomposition



For **compressible** flows:

Favre averaging (mass-weighted averaging)

$$\tilde{u} = \frac{\overline{\rho u}}{\bar{\rho}}$$

Fluctuation:

$$u'' = u - \tilde{u}$$

Accounts for coupled density / velocity fluctuations

Favre **averaged** NS equations:

$$\frac{\partial \bar{\rho}}{\partial t} + \frac{\partial \bar{\rho} \tilde{u}_i}{\partial x_i} = 0$$

$$\frac{\partial \bar{\rho} \tilde{u}_i}{\partial t} + \frac{\partial \bar{\rho} \tilde{u}_i \tilde{u}_j}{\partial x_j} = -\frac{\partial \bar{p}}{\partial x_i} + \frac{\partial \bar{\tau}_{ij}}{\partial x_j} - \frac{\partial R_{ij}}{\partial x_j}$$

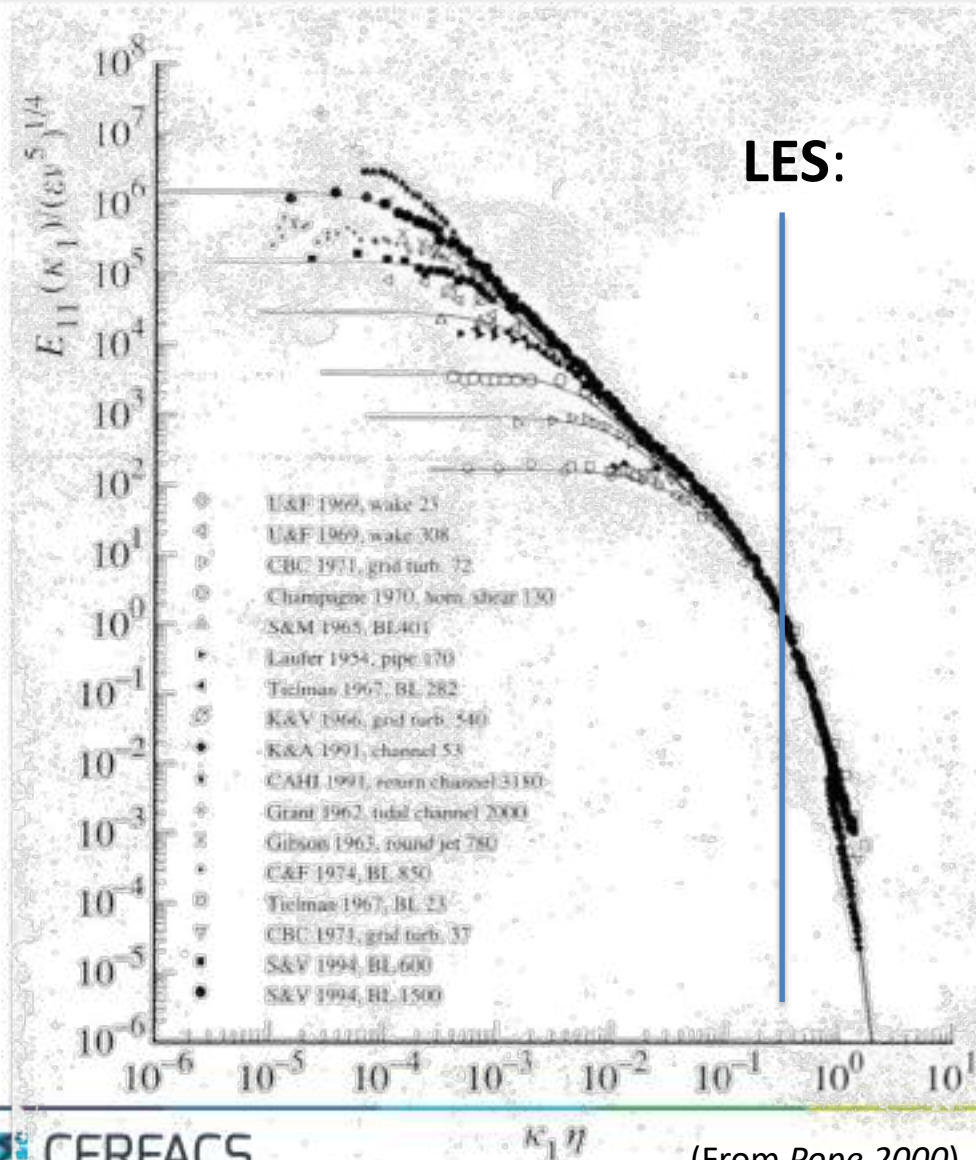
Turbulent stress tensor:

$$R_{ij} = -\overline{\rho u_i'' u_j''}$$

$$\frac{\partial \bar{\rho} \tilde{E}}{\partial t} + \frac{\partial \bar{\rho} \tilde{u}_j \tilde{E}}{\partial x_j} = -\frac{\partial}{\partial x_j} \left(\overline{\rho u_j'' E''} \right) + \frac{\partial \bar{\tau}_{ij} \tilde{u}_i}{\partial x_j} + \frac{\partial}{\partial x_j} \left(\lambda \frac{\partial \bar{T}}{\partial x_j} \right)$$

$$\tilde{E} = \frac{\tilde{u}_i \tilde{u}_i}{2} + c_v \tilde{T} + \frac{1}{2} \overline{u_i'' u_i''}$$

Turbulence cascade

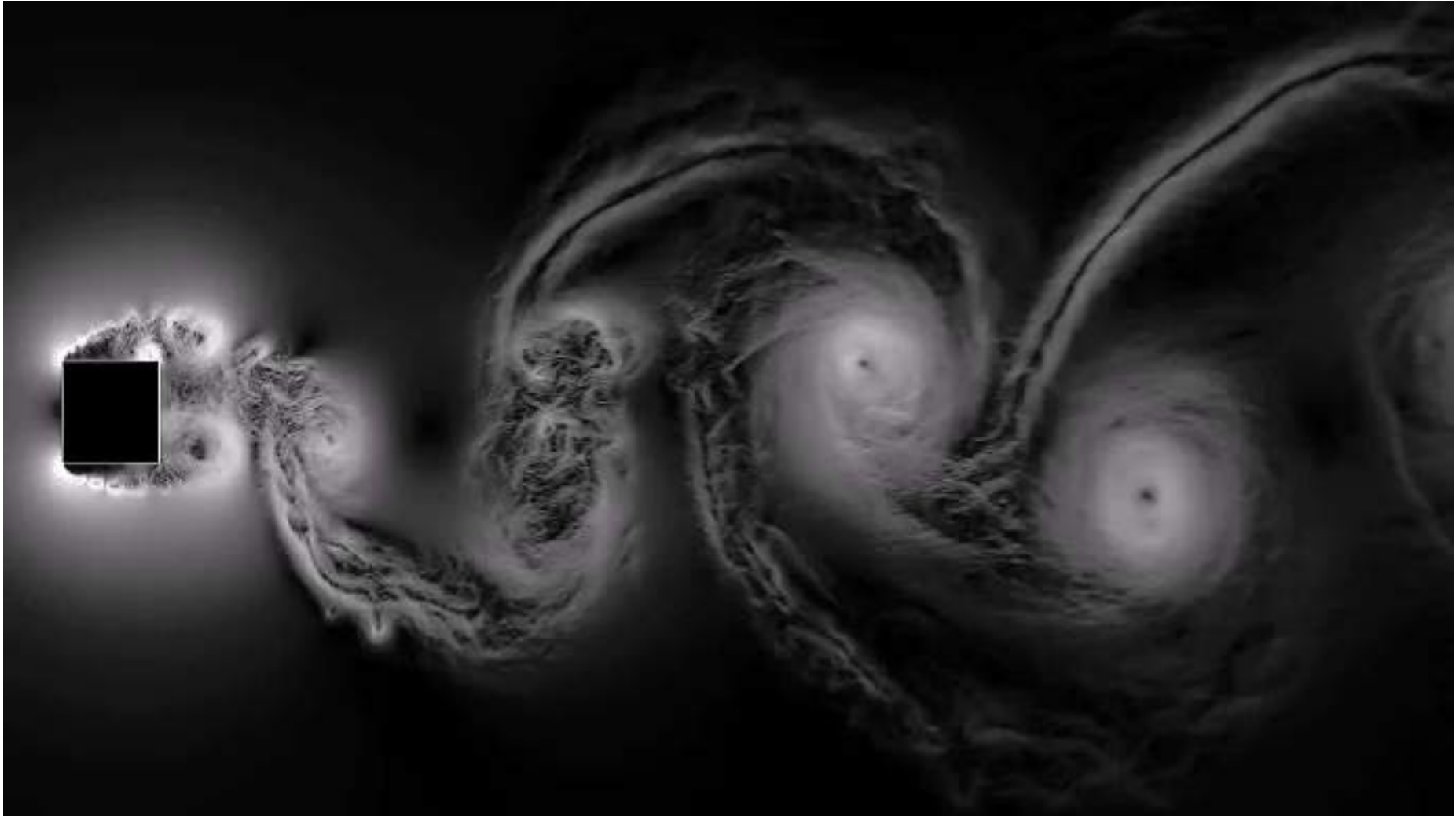


Compilation of numerous experiments (pipe, grids, jets, wake, BL...)

LES: Let's **filter** the high frequencies



Turbulence, auto-similarity





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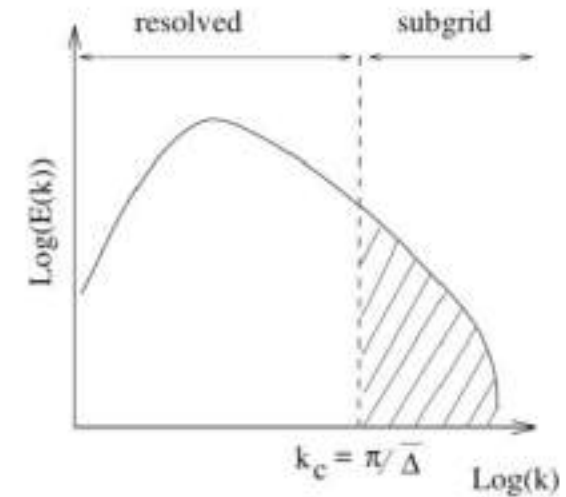
Wall-bounded turbulent injection

The LES concepts

4 conceptual steps in LES:

- Define a **filtering operation** : $Q = \bar{Q} + Q'$
- **Filter** NS equations => residual stress tensor
- Define a **Closure** to **model** the residual stress tensor
- Filtered equations are **numerically** solved.

⇒ Provide an approximation of the large scales motion, for 1 realization of turbulent flow.



Filtering and **modeling** are **independent of the numerical method**, in particular of the grid.

Numerical method is supposed to provide an accurate **solution** to the **filtered equations**.

LES: about filtering

Filtering operation: convolution (Leonard, 1974)

$$\bar{Q}(\mathbf{x}) = \int Q(\mathbf{x}^*) F(\mathbf{x} - \mathbf{x}^*) d\mathbf{x}^*$$

↑
Filtered quantity

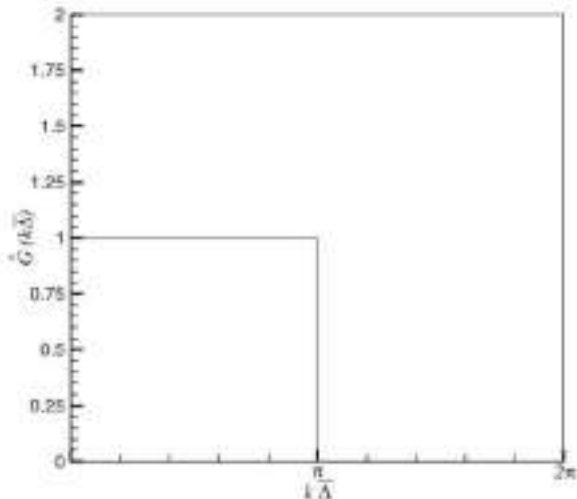
↑
filter

with $\int_{-\infty}^{\infty} F(\mathbf{x}) d\mathbf{x} = 1$
(normalization)

Filters exempla

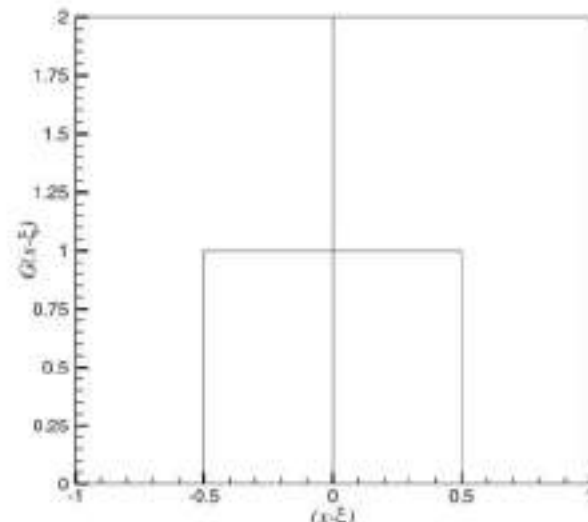
Cut-off filter (spectral space)

$$\bar{F}(k) = \begin{cases} 1 & \text{if } k \leq \pi/\Delta \\ 0 & \text{otherwise} \end{cases}$$



Box filter (physical space)

$$F(\mathbf{x}) = F(x_1, x_2, x_3) = \begin{cases} 1/\Delta^3 & \text{if } |x_i| \leq \Delta/2, i = 1, 2, 3 \\ 0 & \text{otherwise} \end{cases}$$





LES: about filtering

Similar to Favre **averaging**, one can define Favre **filtering**:

$$\bar{\rho} \tilde{Q}(x) = \int \rho Q(x^*) F(x - x^*) dx^*$$

Averaging \neq Filtering !

- Reynolds decomposition:
$$u = \overline{u} + u'$$

 ↑ ↑
 average fluctuation

$$\underline{\overline{u'}} = 0$$
- Filtering:
$$Q = \bar{Q} + Q'$$

 ↑ ↑
 resolved modeled

$$\underline{\overline{Q'}} \neq 0$$

See Veynante – Vervisch, PECS 2002

In practice, the **filter width** is usually given by the **local mesh size**. $\Delta = \sqrt[3]{\Delta x \Delta y \Delta z}$
=> **Numerical** and **modeling errors** can hardly be separated.

NS filtered equations

Similar to Favre **averaged** equations, one can define Favre **filtered** NS equations:

$$\begin{cases} \frac{\partial \bar{\rho}}{\partial t} + \frac{\partial}{\partial x_i} (\bar{\rho} \tilde{u}_i) = 0 \\ \frac{\partial \bar{\rho} \tilde{u}_i}{\partial t} + \frac{\partial}{\partial x_i} (\bar{\rho} \tilde{u}_i \tilde{u}_j) = -\frac{\partial \bar{p}}{\partial x_i} + \frac{\partial}{\partial x_j} \tilde{\sigma}_{ij} - \frac{\partial}{\partial x_j} \tau_{ij} \end{cases}$$

Viscous stress tensor

$$\tilde{\sigma}_{ij} = \bar{\mu} \left(\frac{\partial \tilde{u}_i}{\partial x_j} + \frac{\partial \tilde{u}_j}{\partial x_i} - \frac{2}{3} \delta_{ij} \frac{\partial \tilde{u}_k}{\partial x_k} \right)$$

Subgrid (residual) stress tensor

$$\tau_{ij} = \rho (\widetilde{u_i u_j} - \tilde{u}_i \tilde{u}_j)$$

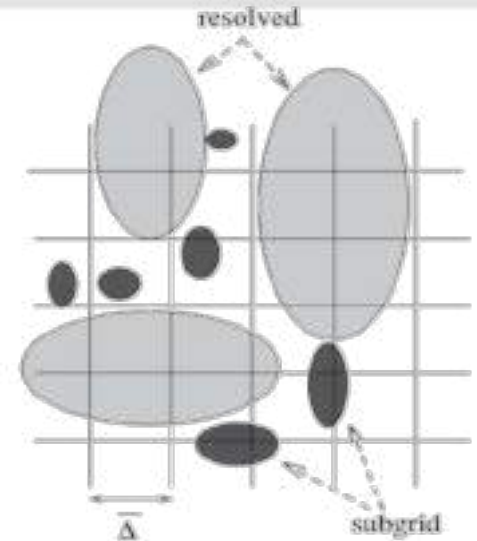
⇒ Need to be modeled

Eddy viscosity assumption:

$$\tau_{ij} = -2\nu_t S_{ij}$$

with $S_{ij} = \frac{1}{2} \left(\frac{\partial \tilde{u}_i}{\partial x_j} + \frac{\partial \tilde{u}_j}{\partial x_i} \right)$

Turbulent viscosity, provided by a SGS model





A few LES models

Reminder:

- Residual stress tensor: $\tau_{ij} = \rho (\widetilde{u_i u_j} - \widetilde{u}_i \widetilde{u}_j)$
- Assumption: $\tau_{ij} = -2\nu_t S_{ij}$

Smagorinsky model (1963):

$$\nu_t = (C_s \Delta)^2 \sqrt{2 \widetilde{S_{ij}} \widetilde{S_{ij}}} = (C_s \Delta)^2 |S|$$

$$C_s \in [0.1, 0.18]$$

Shear flows,
wall-bounded

HIT

Filter size (in practise, grid size)



A few LES models

Dynamic Smagorinsky model (Germano, 1992):

- Introduction of a **2nd filter** (test filter)
- Based on test filtered equations, **dynamic determination** of C_s

- **Grid filter** $\tilde{\Delta}$
 - **Test filter** $\hat{\Delta} = 2\tilde{\Delta}$
- Filter NS \rightarrow
- $$\tau_{ij} = \widetilde{u_i u_j} - \tilde{u}_i \tilde{u}_j$$
- $$T_{ij} = \widehat{\widetilde{u_i u_j}} - \widehat{\tilde{u}_i \tilde{u}_j}$$

Germano identity :

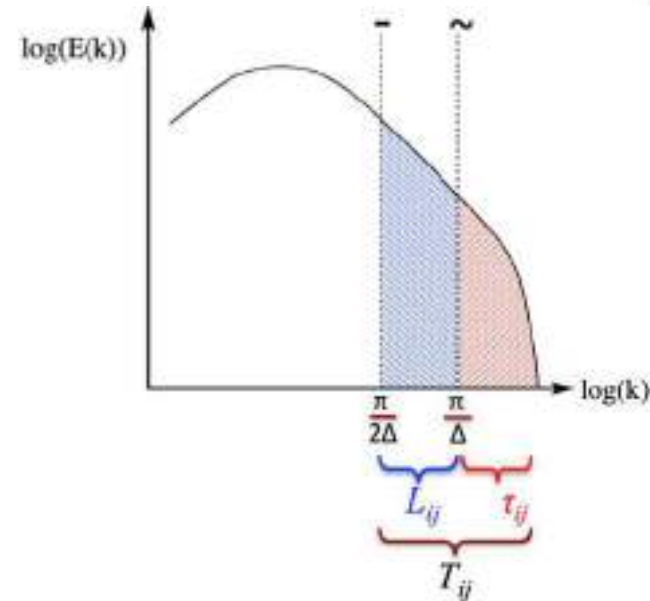
$$\widehat{\widetilde{u_i u_j}} - \widehat{\tilde{u}_i \tilde{u}_j} = T_{ij} - \widehat{\tau_{ij}}$$

Can be computed on the grid

Must be modeled

- Smagorinsky for τ_{ij} and T_{ij} :
- $$T_{ij} = 2C_s \hat{\Delta}^2 |\widehat{\tilde{S}}| \widehat{\tilde{S}_{ij}}$$
- $$\tau_{ij} = 2C_s \tilde{\Delta}^2 |\tilde{S}| \tilde{S}_{ij}$$

=> Substitute into Germano identity



A few LES models

Dynamic Smagorinsky model (Germano, 1992):

- Substitute into Germano identity

$$\widehat{\widetilde{u_i u_j}} - \widehat{\widetilde{u_i}} \widehat{\widetilde{u_j}} = 2C_s \left(\widehat{\widetilde{\Delta^2 |\widetilde{S}| \widetilde{S_{ij}}}} - \widetilde{\widehat{\Delta^2 |\widetilde{S}| \widetilde{S_{ij}}}} \right)$$

Can be computed on the grid

- Finally
$$C_s = \frac{1}{2} \frac{\widehat{\widetilde{u_i u_j}} - \widehat{\widetilde{u_i}} \widehat{\widetilde{u_j}}}{\widehat{\widetilde{\Delta^2 |\widetilde{S}| \widetilde{S_{ij}}}} - \widetilde{\widehat{\Delta^2 |\widetilde{S}| \widetilde{S_{ij}}}}}$$
 Formulation later improved (Lilly 1992)

Main ideas:

- Introduction of a **test filter**
- Germano identity
- **Relying on resolved scales to model unresolved scales**



A few LES models

WALE model (Nicoud, Ducros, 1999):

Wall Adapting Local Eddy Viscosity

- Intended for **wall bounded flows** (*without law-of-the-wall...*).
- Turbulent viscosity must vanish according to $\nu_t \propto (y^+)^3$ close to a wall.

$$\nu_t = (C_\omega \Delta)^2 \frac{(s_{ij}^d s_{ij}^d)^{3/2}}{(\tilde{S}_{ij} \tilde{S}_{ij})^{5/2} + (s_{ij}^d s_{ij}^d)^{5/4}}$$

$C_\omega = 0,4929$

$$s_{ij}^d = \frac{1}{2}(\tilde{g}_{ij}^2 - \tilde{g}_{ij}^2) - \frac{1}{3}\tilde{g}_{kk}^2 \delta_{ij}$$
$$\tilde{g}_{ij} = \partial \tilde{u}_i / \partial x_j$$



A few LES models

Sigma model (Nicoud et al., 2011):

- Intended for **wall bounded flows** (*without wall-law...*).
- Turbulent viscosity must vanish according to $\nu_t \propto (y^+)^3$ close to a wall.
- **WALE improvement for pure shear or solid rotation cases**

$$\nu_t = (C_\sigma \Delta)^2 \frac{\sigma_3(\sigma_1 - \sigma_2)(\sigma_2 - \sigma_3)}{\sigma_1^2}$$

$C_\sigma = 1.5$

$\sigma_1 \geq \sigma_2 \geq \sigma_3 \geq 0$

Singular values of the velocity gradient tensor



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Reminder:

- Incompressible momentum equation

$$\frac{\partial u_i}{\partial t} + \frac{\partial u_i u_j}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \frac{\partial \tau_{ij}}{\partial x_j}$$

- Filtered quantity:

$$\bar{f}(\vec{x}, t) = \int f(\vec{y}, t) \bar{G}_{\Delta x}(\vec{x} - \vec{y}) d\vec{y}$$

Filtered momentum equation:

$$\bullet \quad \overline{\frac{\partial u_i}{\partial t} + \frac{\partial u_i u_j}{\partial x_j} + \frac{\partial p}{\partial x_i} - \frac{\partial \tau_{ij}}{\partial x_j}} = 0$$

$$\bullet \quad \frac{\partial \bar{u}_i}{\partial t} + \frac{\partial \bar{u}_i u_j}{\partial x_j} + \frac{\partial \bar{p}}{\partial x_i} - \frac{\partial \bar{\tau}_{ij}}{\partial x_j} = 0$$

For non-uniform grids:

$$\bullet \quad \frac{\partial \bar{u}_i}{\partial t} + \frac{\partial \bar{u}_i u_j}{\partial x_j} + \frac{\partial \bar{p}}{\partial x_i} - \frac{\partial \bar{\tau}_{ij}}{\partial x_j} = \mathbf{m}$$

Commutation error

$$m = \frac{\partial \bar{u}_i u_j}{\partial x_j} - \frac{\partial \bar{u}_i \bar{u}_j}{\partial x_j} \quad [1,2]$$

$$\bullet \quad \frac{\partial \bar{u}_i}{\partial t} + \frac{\partial \bar{u}_i \bar{u}_j}{\partial x_j} + \frac{\partial \bar{p}}{\partial x_i} - \frac{\partial \bar{\tau}_{ij}}{\partial x_j} = \mathbf{m} + \frac{\partial \bar{\tau}_{ij}^t}{\partial x_j}$$

Modeling induces resolution error



Numerics, errors and LES

Filtered quantity:

$$\bar{f}(\vec{x}, t) = \int f(\vec{y}, t) \bar{G}_{\Delta x}(\vec{x} - \vec{y}) d\vec{y}$$

Commutation and resolution errors

- On **regular** meshes, **commutation** with temporal and spatial derivatives
- For variable $\Delta x \Rightarrow$ **variable width** for the filter.
- We **no longer have commutation** with spatial derivative. Induces “**Commutation error**”.
- Subgrid scale **modelling** induces **resolution error**.



Discretization (Truncation) error

Transport equation:

$$\frac{\partial U}{\partial t} + \nabla \cdot F(U) = 0$$



Discretization



Equation satisfied by the **numerical solution** (“Modified Equation”)

$$\frac{\partial U^N}{\partial t} + \nabla \cdot F(U^N) = \epsilon(U^N)$$



Discretization error

=> Application on Burgers equation...

Ex: truncation error and Burgers equation

Burgers Equation:

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} = \nu \frac{\partial^2 u}{\partial x^2}$$

Finite difference method:

1st order derivative

$$\frac{\partial u}{\partial x} \approx \mathcal{D}_h^- u(x) \equiv \frac{u(x) - u(x-h)}{h}$$

2nd order derivative

$$\frac{\partial^2 u}{\partial x^2} \approx \mathcal{D}_h^2 u(x) \equiv \frac{u(x+h) - 2u(x) + u(x-h)}{h^2}$$

Numerically solved equation:

$$\frac{\partial u}{\partial t} + u \mathcal{D}_h^- u = \nu \mathcal{D}_h^2 u$$

Equivalent to (**modified equation**):

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} = (\nu + \nu_{num}) \frac{\partial^2 u}{\partial x^2} + \mathcal{O}(h^2)$$

$$\nu_{num} = \frac{1}{2} u h$$

- **1-order accurate** numerical scheme
- **Non-linear** error
- New **source terme** is the equation **actually solved**



Numerics, errors and LES

Finally: Incompressible momentum equation:

$$\frac{\partial u_i}{\partial t} + \frac{\partial u_i u_j}{\partial x_j} = -\frac{1}{\rho} \frac{\partial p}{\partial x_i} + \nu \frac{\partial^2 u_i}{\partial x_j^2} + \frac{\partial}{\partial x_i} (\tau_{ij}^t + \tau_{ij}^h) + m$$

Explicit SGS model
contribution

Truncation error
contribution

Commutation error
for non-uniform grids

- A good LES requires:

$$\frac{\partial}{\partial x_j} (\tau_{ij}^h) + m \ll \frac{\partial}{\partial x_j} (\tau_{ij}^t)$$

=> Need for accurate numerical scheme, and uniform grids

- Ghosal 1996: “Models” and “errors” are comparable in typical LES...

=> Investigation of high-order schemes, + “non-conventional” SGS modeling



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Implicit LES

- Assimilate the **discretization** to a **low-pass filter**.
- A SGS model is no longer needed: “**No-model**” LES.
- Scheme **must be accurate**: τ^h_{ij} (truncation error) must be small.

$$\frac{\partial u_i}{\partial t} + \frac{\partial u_i u_j}{\partial x_j} = -\frac{1}{\rho} \frac{\partial p}{\partial x_i} + \nu \frac{\partial^2 u_i}{\partial x_j^2} + \frac{\partial}{\partial x_i} (\tau^t_{ij} + \tau^h_{ij}) + m$$

Explicit SGS model
contribution

Truncation error
contribution

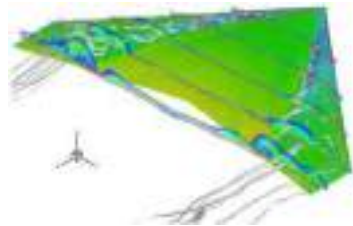
Commutation error
for non-uniform grids

- **No all implicit SGS will work !**
Truncation error must satisfies **SGS properties**
- No SGS model is used=> **modeling** and **numerics** are **inseparably coupled**.

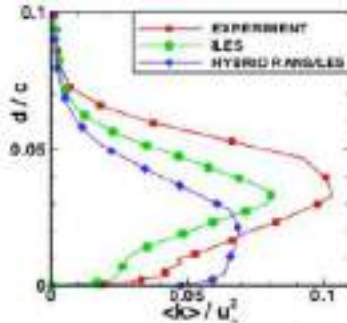
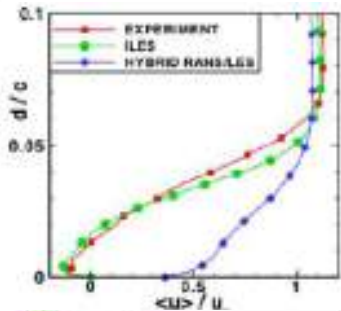
Implicit LES

ILES has advocates and detractors...

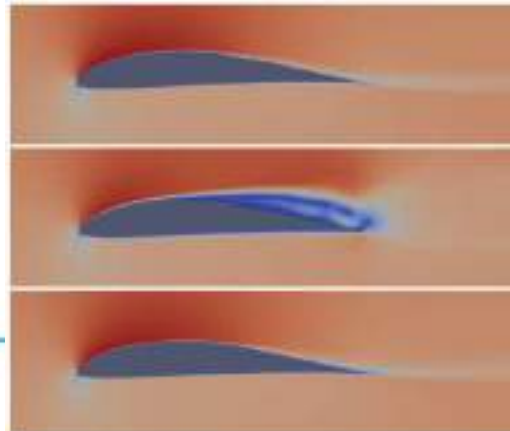
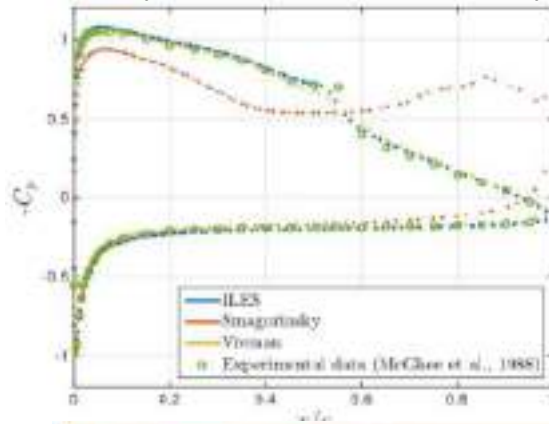
Despite controversies, **ILES** has proven to be **reliable** when used with adequate **high-order numerical schemes**.



Drikakis et al., 2009



Transitional flow
(*Fernandez et al., 2017*)



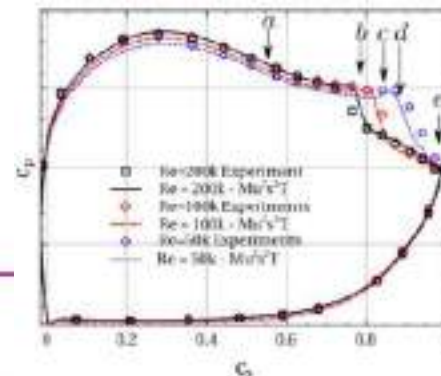
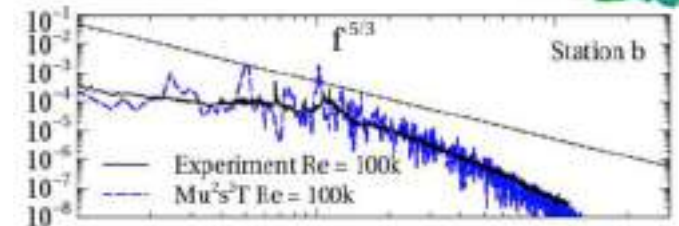
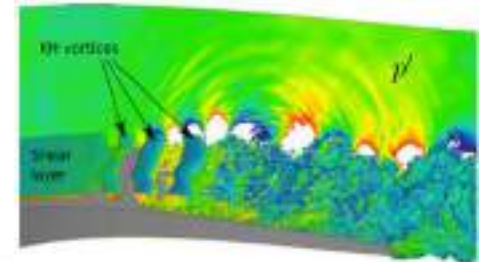
ILES:
High-Order
Discontinuous
Galerkin
scheme

ILES

Smago

Vreman

Bolinches Gisbert et al. 2019



ILES:
High-Order Flux
Reconstruction
scheme



LES: about modeling

Explicit LES approach:

A **model** is introduced to account for the filtered subgrid scales:

Among others: (Dynamic) Smagorinsky *(See Sagaut (2001))*
WALE/Sigma
Vreman, lagrangian averaging...

Implicit LES:

- **No SGS model.** The **numerical method** is chosen such that **numerical error** and **resolution error** cancel each other.

A “good LES”:

- Filter and grid are sufficiently fine to **resolve 80% of the energy** (Pope, 2000)



A few conclusion

- **Averaging \neq Filtering**

- **“Real life” :**
modeling + spatio-temporal discretization \rightarrow **errors**
modeling (resolution), **commutation**, **truncation** errors

- **Numerics and modeling can be inseparably coupled**



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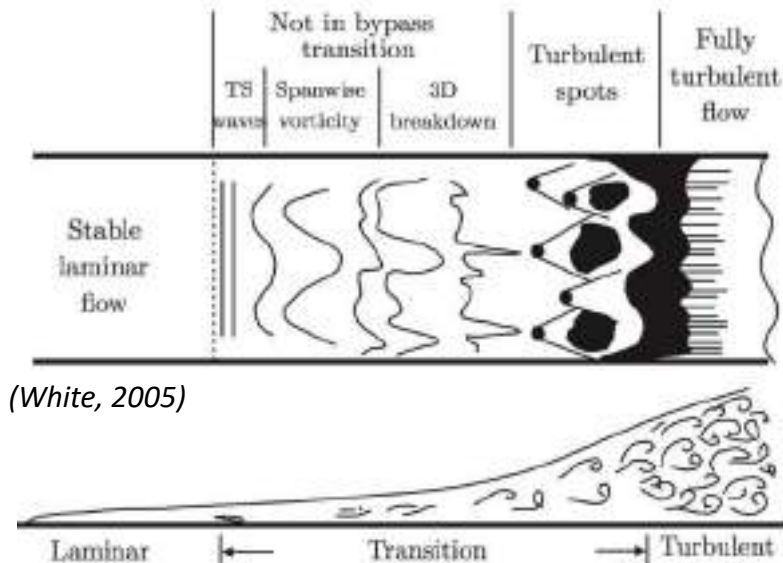
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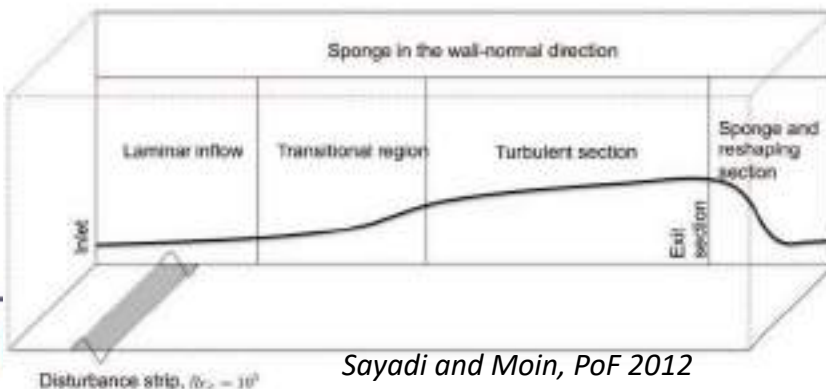
Wall-bounded turbulent injection

Boundary layer

Wall bounded flows: Development of a boundary layer
Convection + diffusion of vorticity

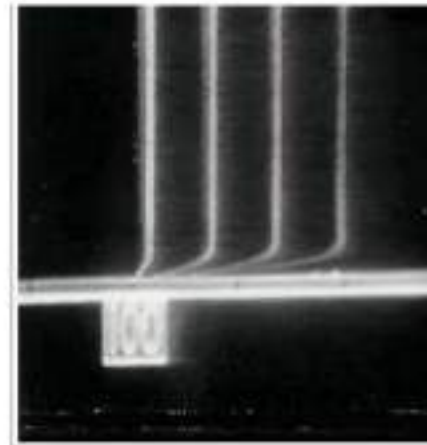


(White, 2005)

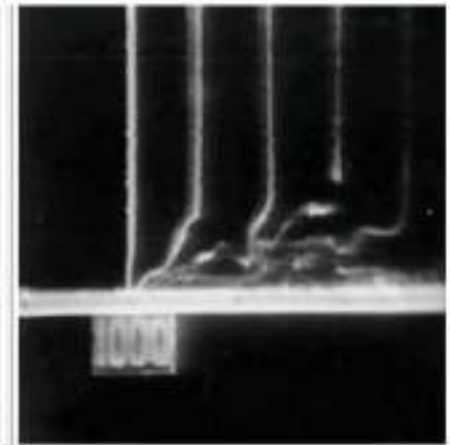


Sayadi and Moin, PoF 2012

laminar



turbulent



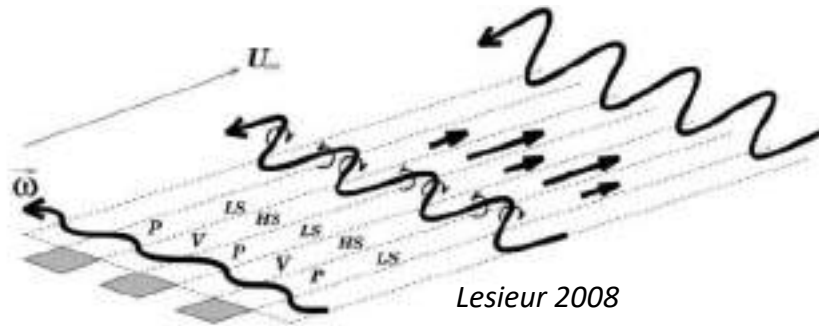
University of Iowa

3 main regimes:

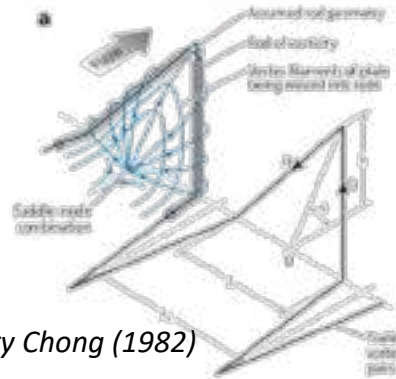
- **Laminar** boundary layer
- **Transition** laminar \rightarrow turbulence
- **Turbulent** boundary layer

(Natural) transition to turbulence

Vorticity evolution



Lesieur 2008

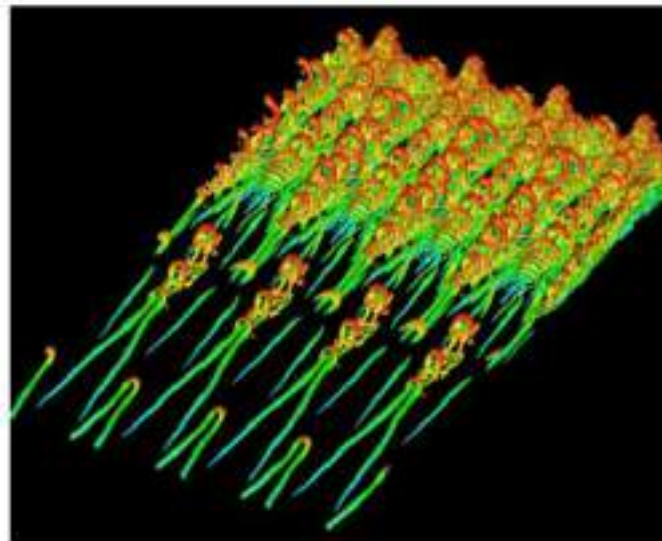


Perry Chong (1982)

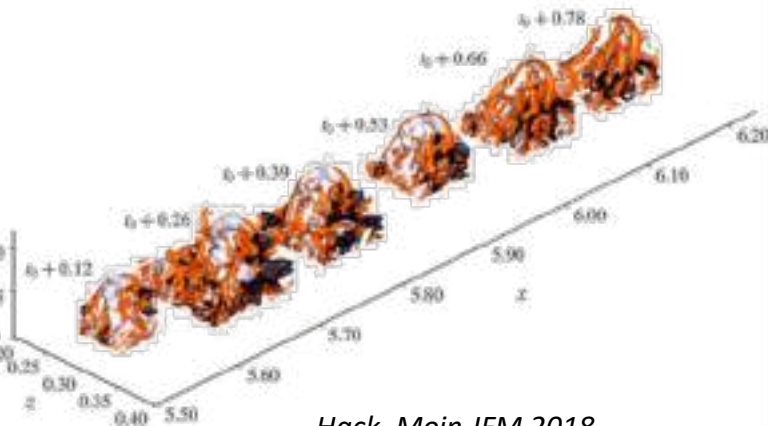
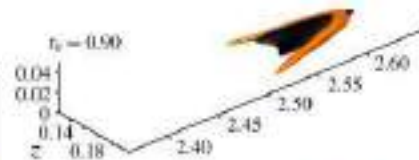


Perry et al. (1981)

Hairpin formation



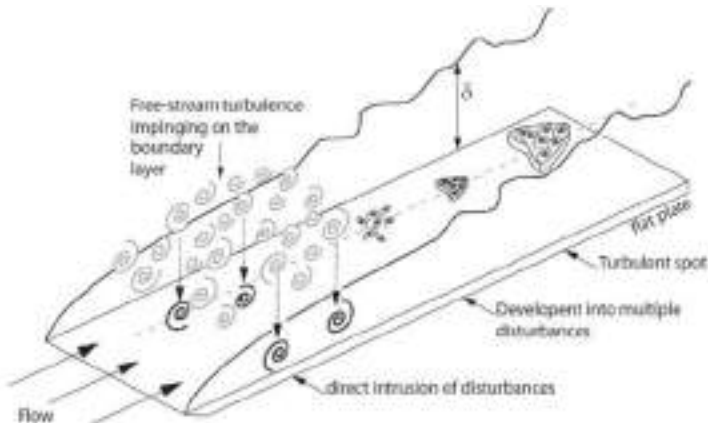
Sayadi 2012



Hack, Moin JFM 2018

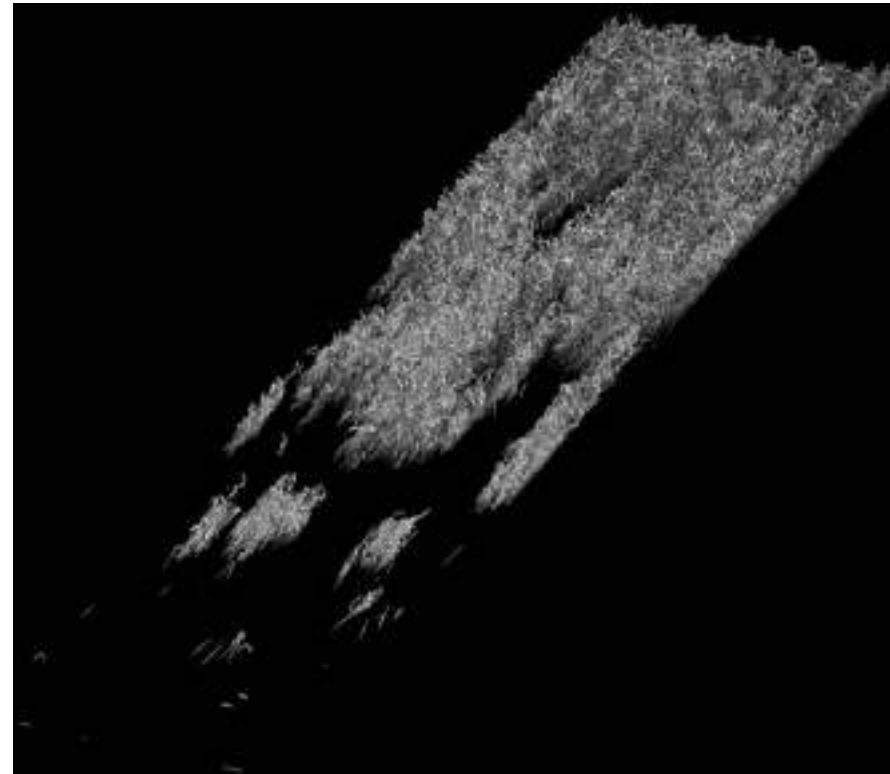
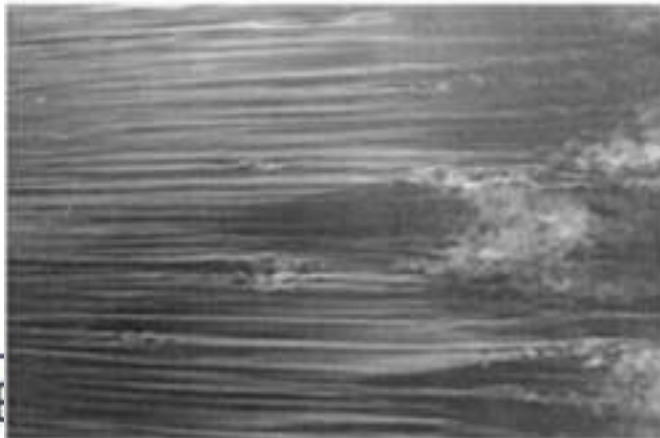
(Bypass) transition to turbulence

- Bypass transition: Non-natural transition to turbulence
- Transition **under freestream turbulence, noise**



Ghasemi et al., JHMT 2014

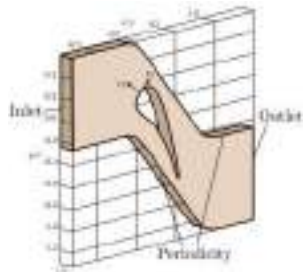
Turbulent spot



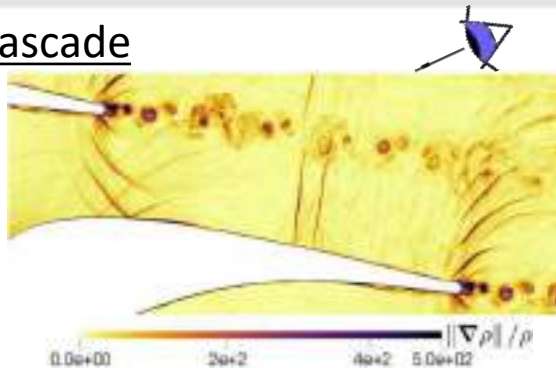
Wu et al., POF2014, PNAS 2017

Bypass transition

LS89 VKI turbine cascade

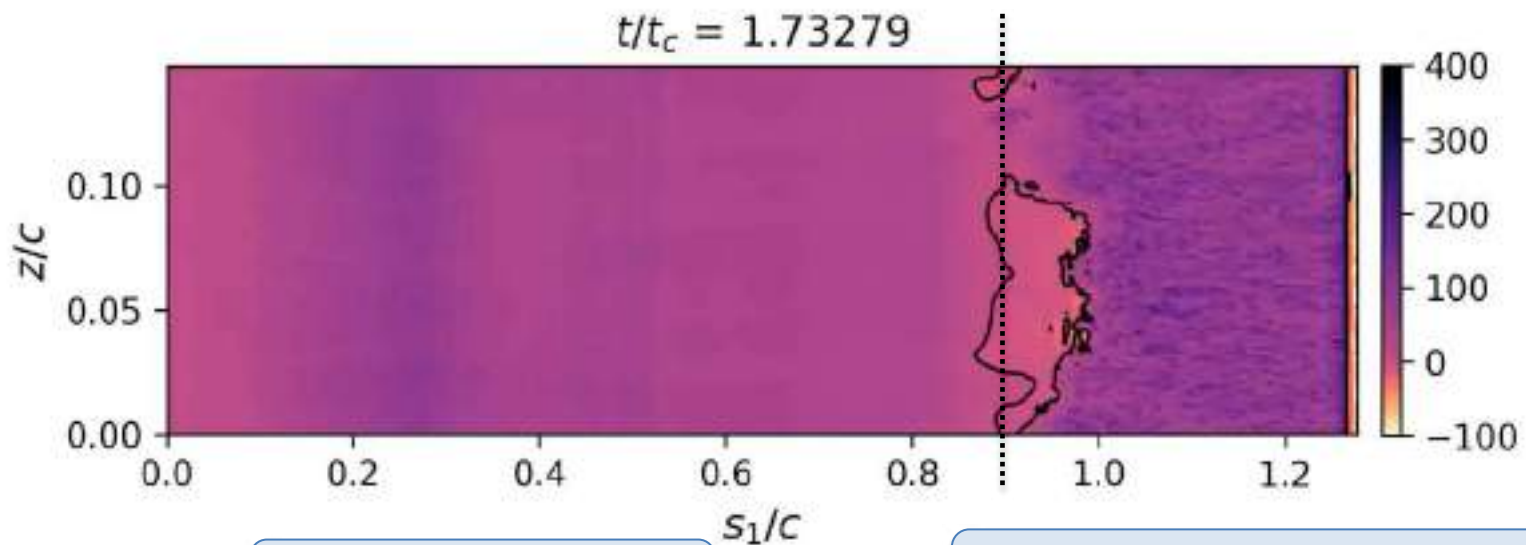


Dupuy et al., PoF2020



⇒ **Critical** phenomena for **heat transfer** prediction

Shock



- Streaks
- Bypass transition
- Turbulent spots

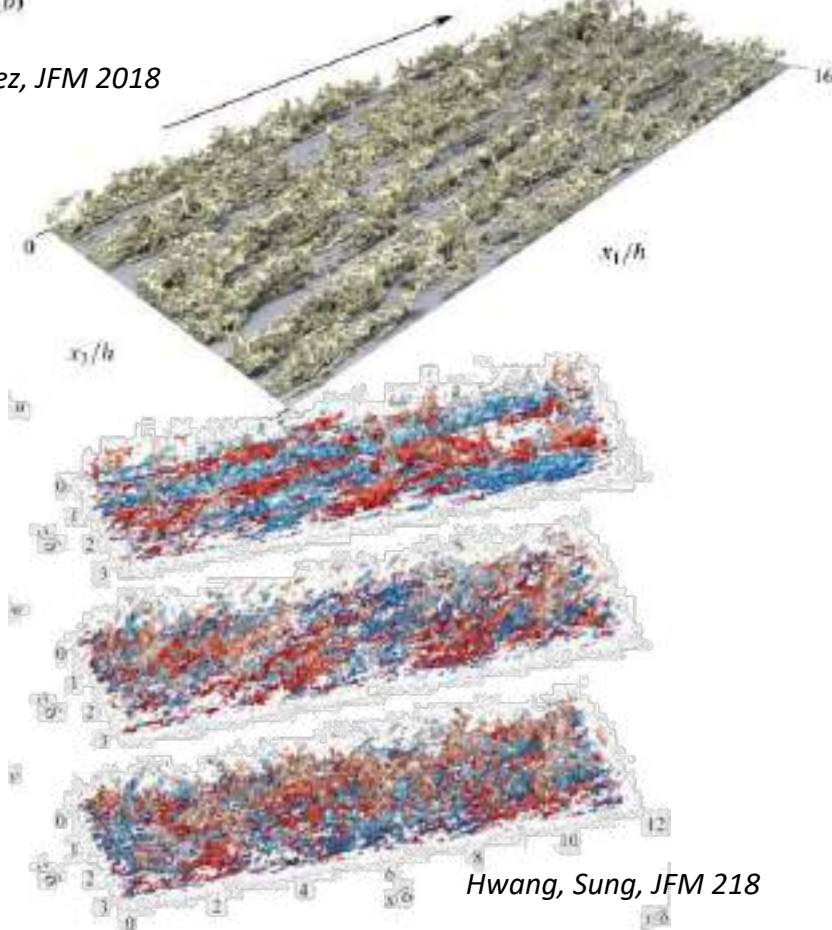
- Bypass transition
- Turbulent BL
- Intermittent relaminarisation



Turbulent BL

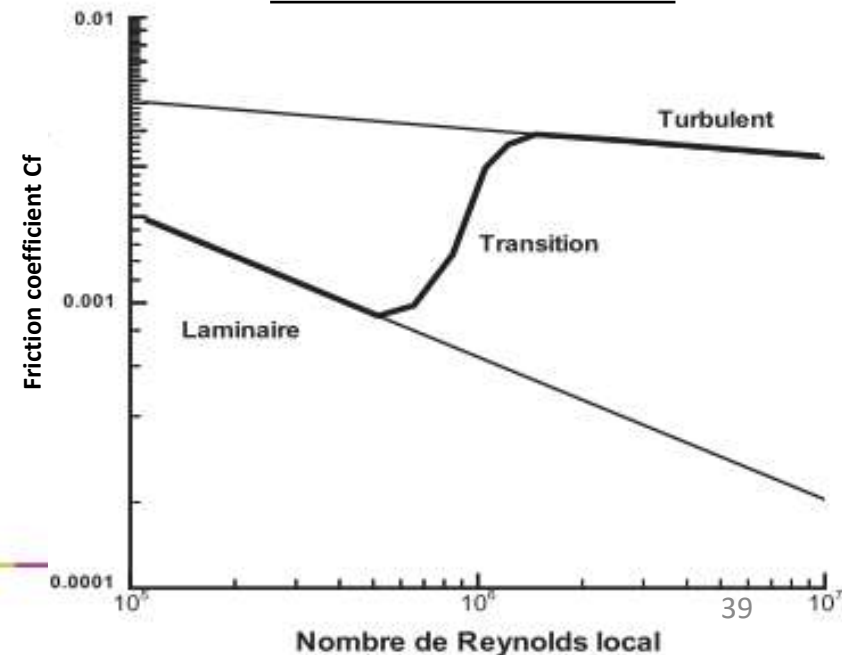
Coherent structures in a **turbulent** BL:

Jimenez, JFM 2018



Falco 1974

Friction coefficient

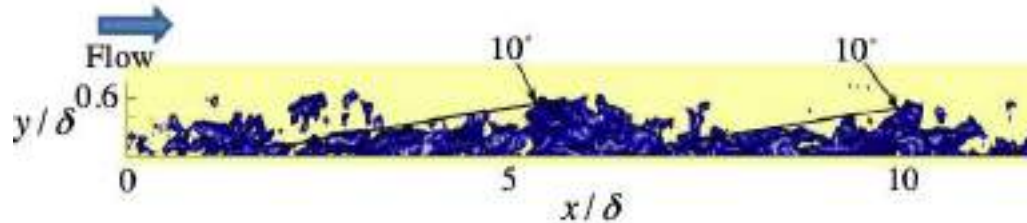


Once BL becomes turbulent: **Friction significantly increases!!!**

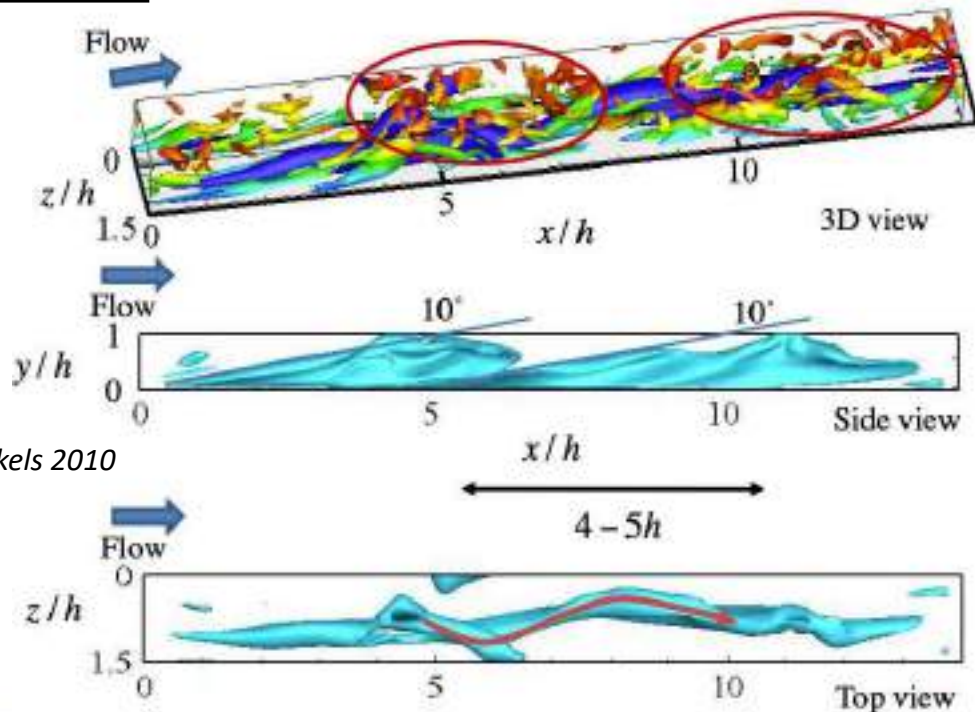


Coherence in turbulent BL

PIV measurement



Simulation



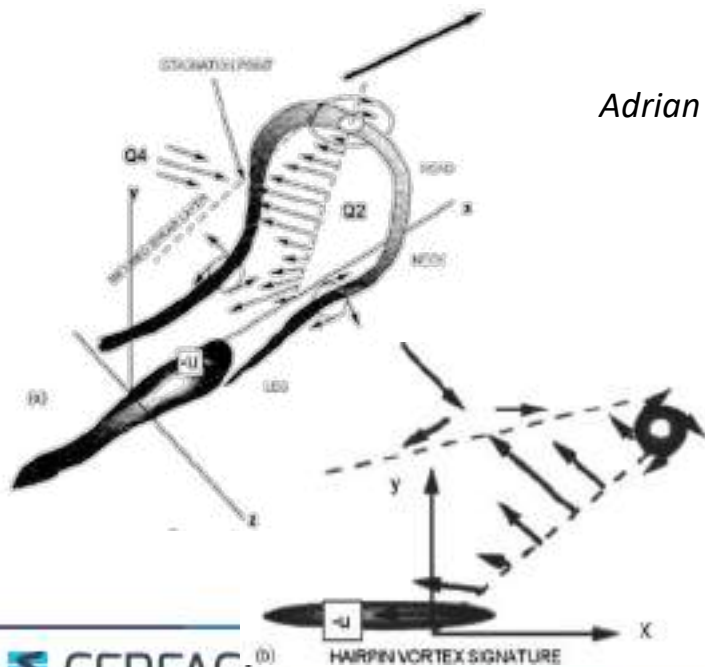
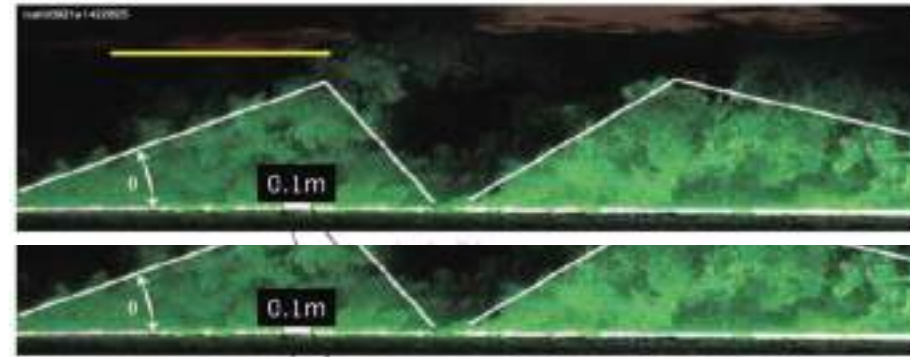
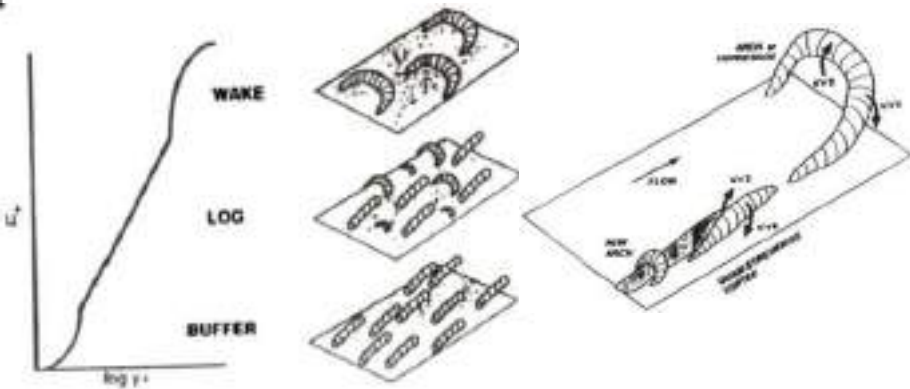
Coherence in turbulent boundary layer:
 \Rightarrow **Streaks**

Elongated, anisotropic structures

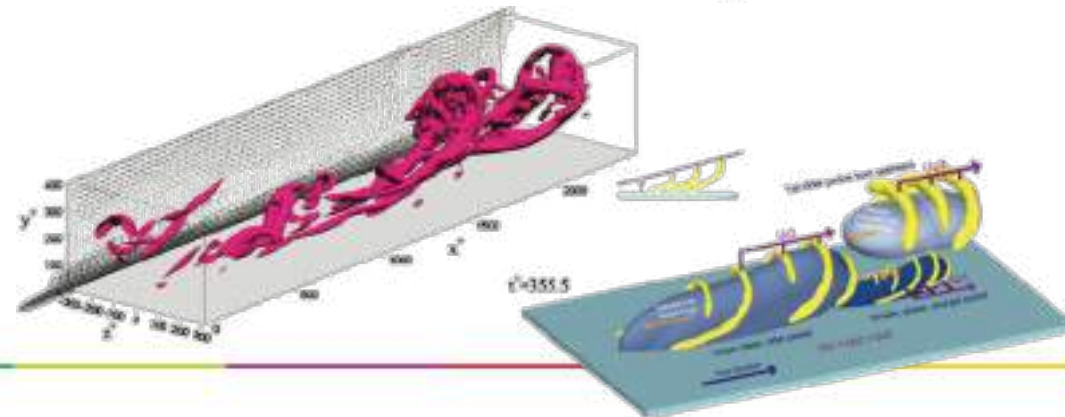
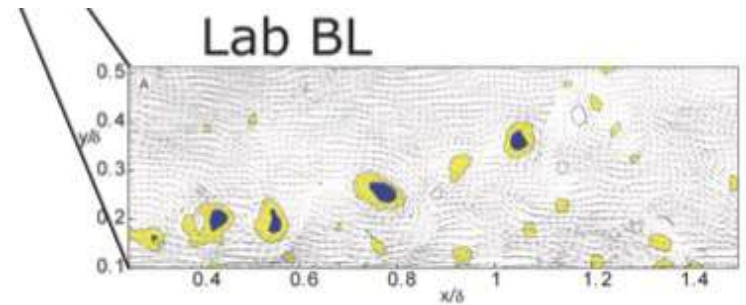
Nickels 2010

Streaks and hairpins packets

Large Scale Motions (LSM)



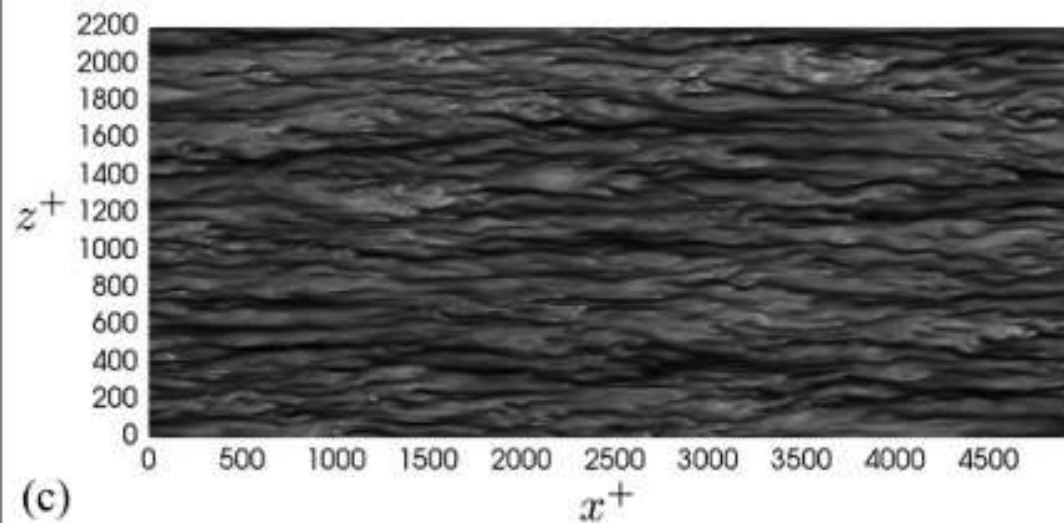
Adrian POF 2007



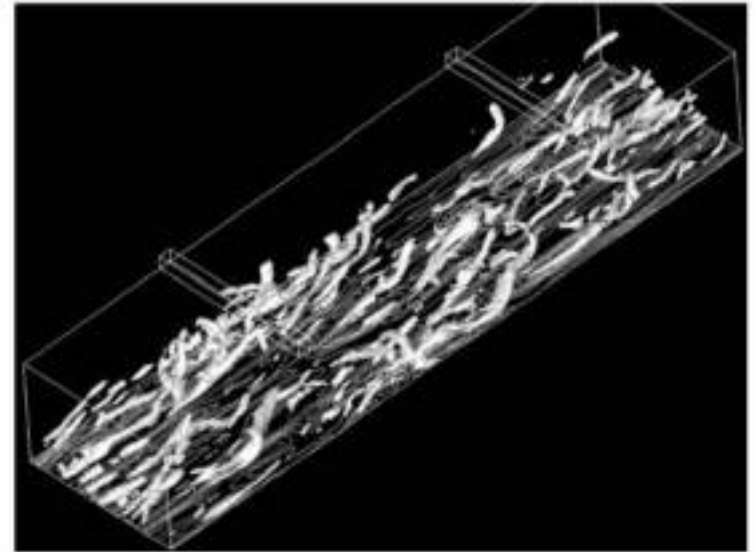


Close to the wall: “Streaks”

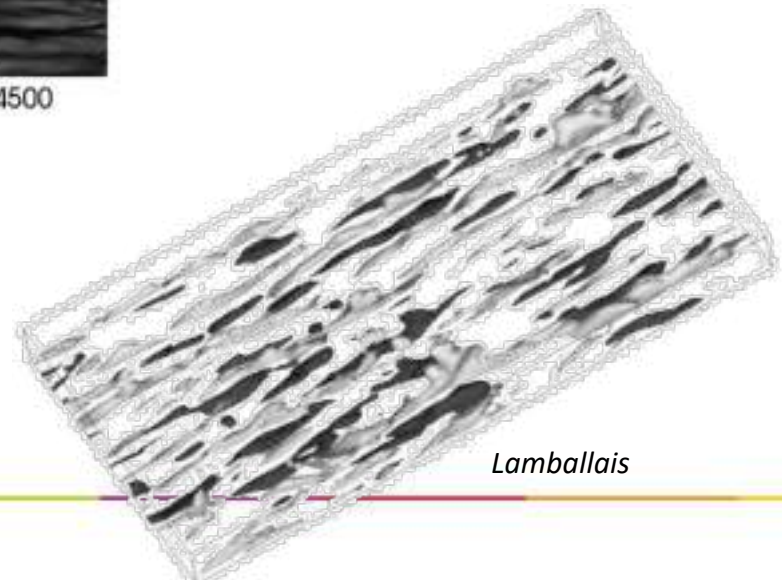
Anisotropic structures: “Streaks”



(c) *Rezaeiravesh Liefvendahl, PoF2018*



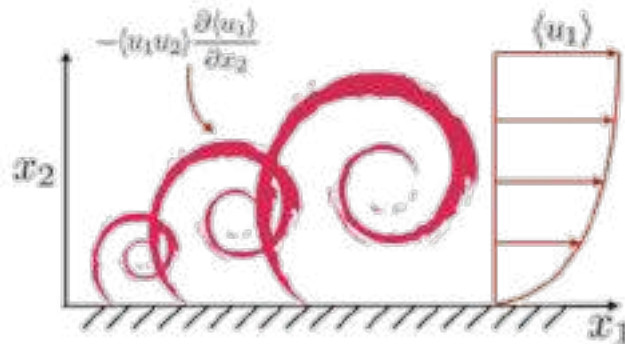
Dubief



Lamballais

Wall-attached eddies

Townsend 1976: Structural model: attached eddies to the wall

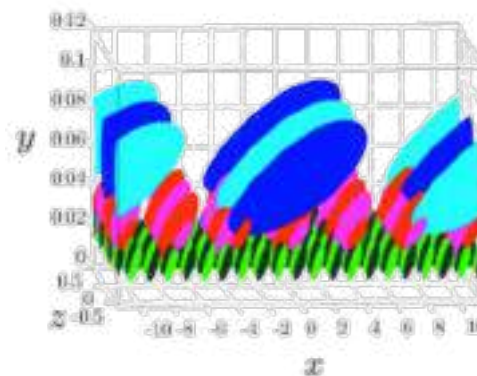


$$u^* \sim \sqrt{-\langle u_1 u_2 \rangle}$$

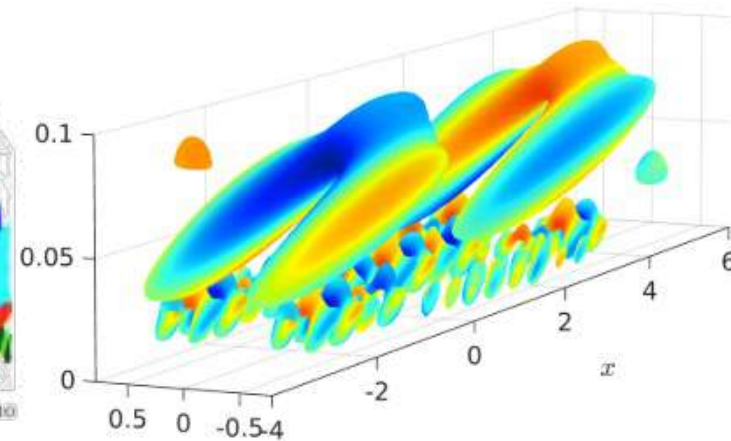
$$l^* \sim \frac{\partial \langle u_1 \rangle}{\partial x_2}^{-1}$$

$$l^* \sim u^* \cdot t^*$$

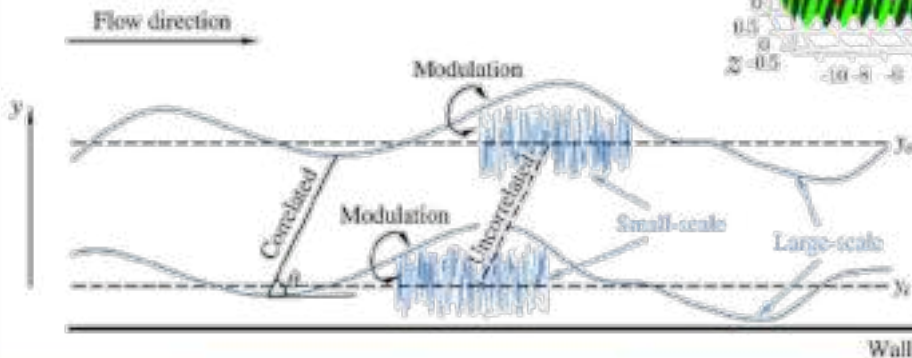
Lozano Duran, Bae 2019



Self similar modes in turbulent BL:



Sharma et al., 2017

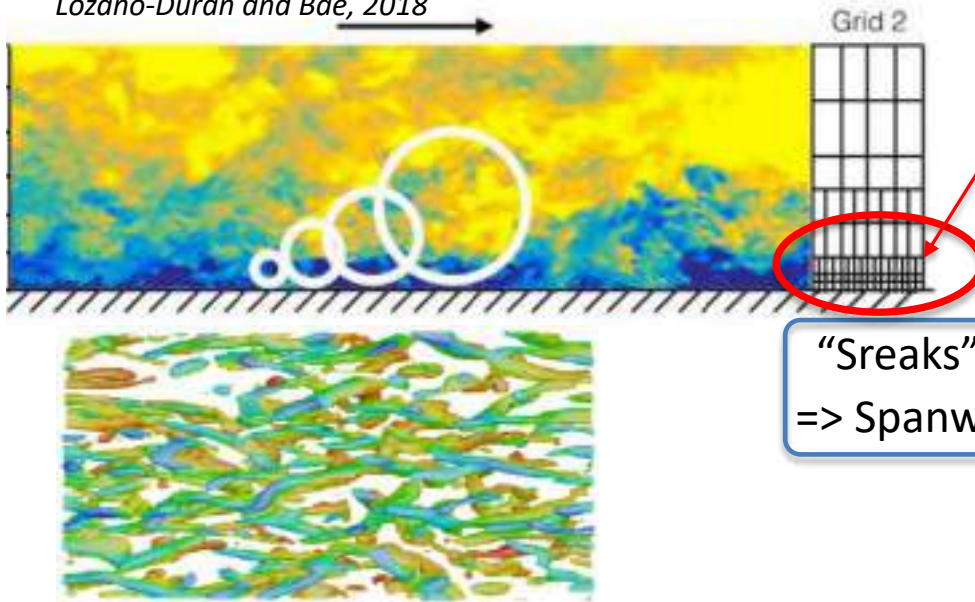


=> Order in chaos...

See book by Bergé, Pomeau,
Vidal...

Turbulent BL and numerical simulations

Lozano-Duran and Bae, 2018



A fine grid is mandatory to resolve all structures!

“Sreaks”: Anisotropic wall turbulent structures:
=> Spanwise and streamwise **constraints**:

$$\Delta y_1^+ < 2$$

$$\Delta x^+ \sim 50 - 150$$

$$\Delta z^+ \sim 15 - 40$$

Chapman (1979), Choi & Moin (2012):

Outer Layer (LES)

- Spatial resolution : $N_x N_y N_z \sim \text{Re}^{0.4}$
- Total cost : $N_x N_y N_z \times N_t \sim \text{Re}^{0.6}$

Inner Layer (LES)

- Stretched, nested grids : $N_x N_y N_z \propto \text{Re}^{1.8}$
- Total cost : $N_x N_y N_z \times N_t \sim \text{Re}^{2.3} \text{ to } \text{Re}^{3.6}$

Resolving the inner layer is CPU demanding!!

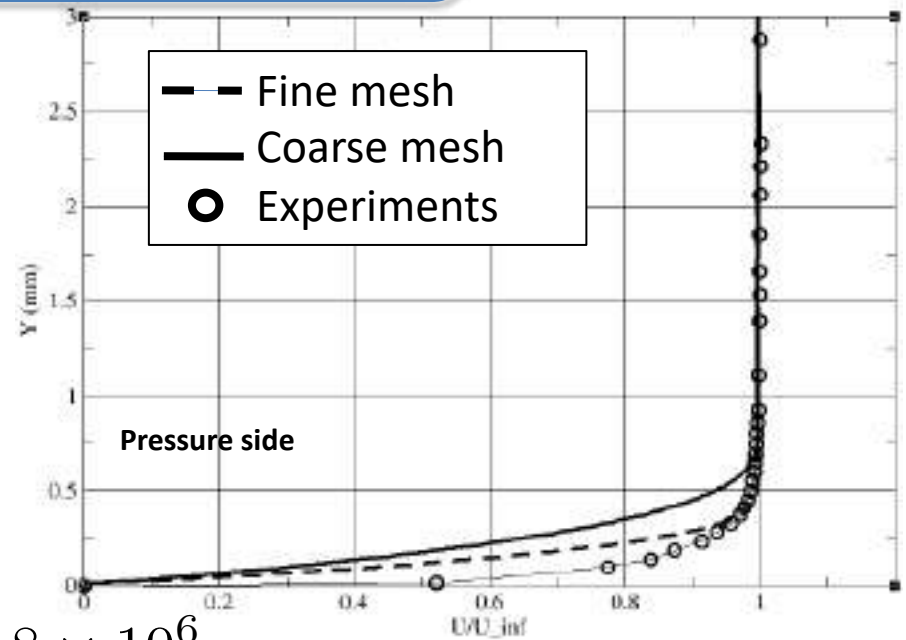
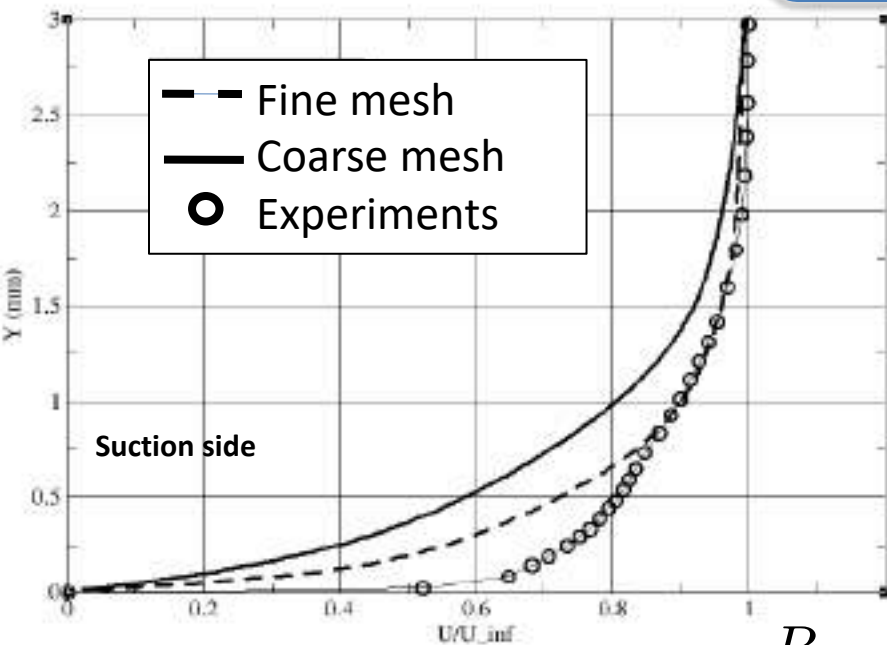
Wall resolved simulations

Even with such constraints, friction prediction remains a challenge at High Reynolds

“Fine mesh”:

$$\Delta y^+ \simeq 2$$
$$\Delta x^+ \simeq 100$$
$$\Delta z^+ \simeq 50$$


Leonard et al., 2010

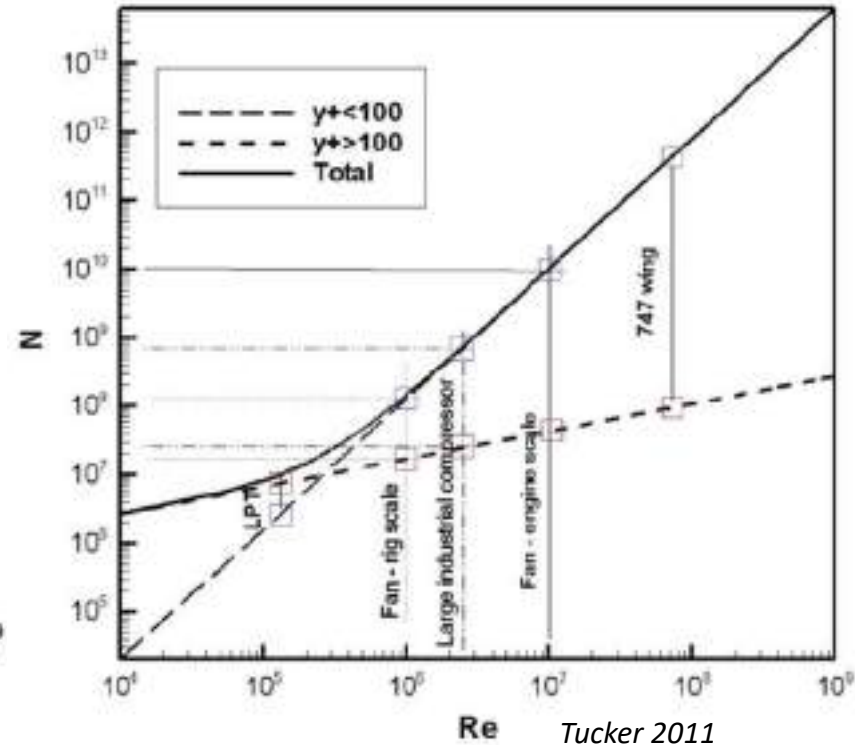
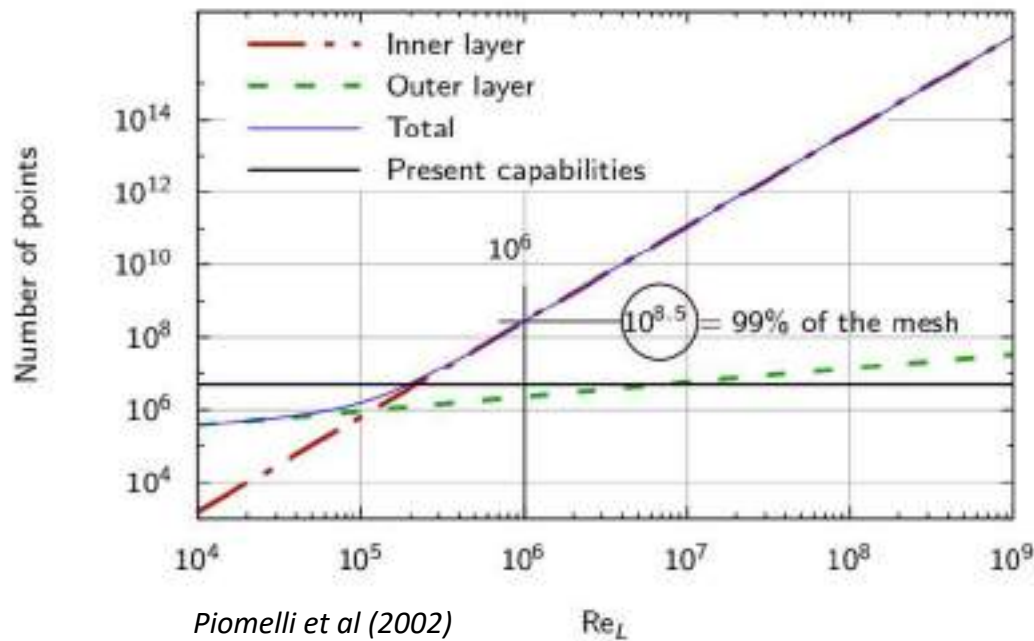


$$Re = 2.8 \times 10^6$$

A need for wall modeling

In any case, **resolving the entire boundary layer is still intractable** for real applications.

Number of grid points required to resolve a boundary layer²



- Full airplane wall-resolved simulation not expected by 2100.
- **Modeling** the boundary layer is **mandatory** for real applications



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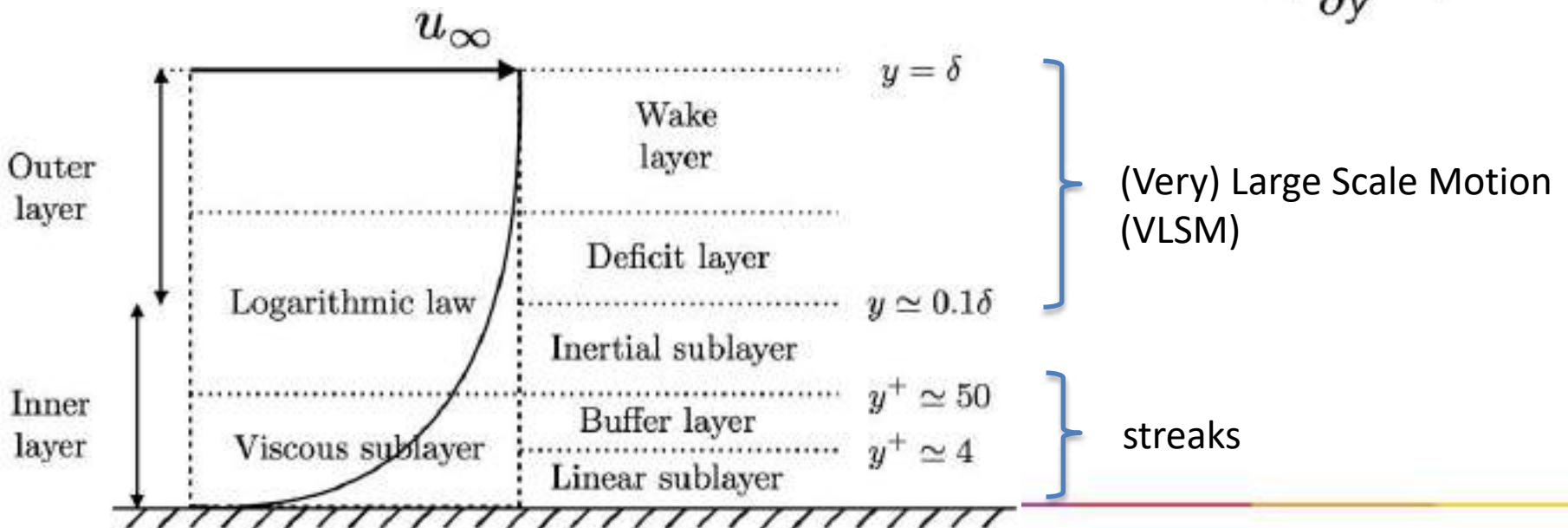
Turbulent boundary layer

- Let's consider an **incompressible 2D flow, zero pressure gradient, steady mean flow**.

⇒ Momentum equation becomes:

$$\underbrace{\bar{u} \frac{\partial \bar{u}}{\partial x} + \bar{v} \frac{\partial \bar{u}}{\partial y}}_{\text{inertial terms}} = \underbrace{\nu \frac{\partial^2 \bar{u}}{\partial y^2}}_{\text{viscous stress}} + \underbrace{\frac{\partial(-\overline{u'v'})}{\partial y}}_{\text{Reynolds shear stress}}$$

- BL is divided in regions, according to the **total shear stress** $\tau = \mu \frac{\partial \bar{u}}{\partial y} - \rho \overline{u'v'}$



Velocity profile in a turbulent BL

$$\underbrace{\bar{u} \frac{\partial \bar{u}}{\partial x} + \bar{v} \frac{\partial \bar{u}}{\partial y}}_{\text{inertial terms}} = \underbrace{\nu \frac{\partial^2 \bar{u}}{\partial y^2}}_{\text{viscous stress}} + \underbrace{\frac{\partial(-\overline{u'v'})}{\partial y}}_{\text{Reynolds shear stress}}$$

In the limit of **infinite Reynolds**: $Re = \frac{UL}{\nu} = \frac{T_{vis}}{T_{in}}$

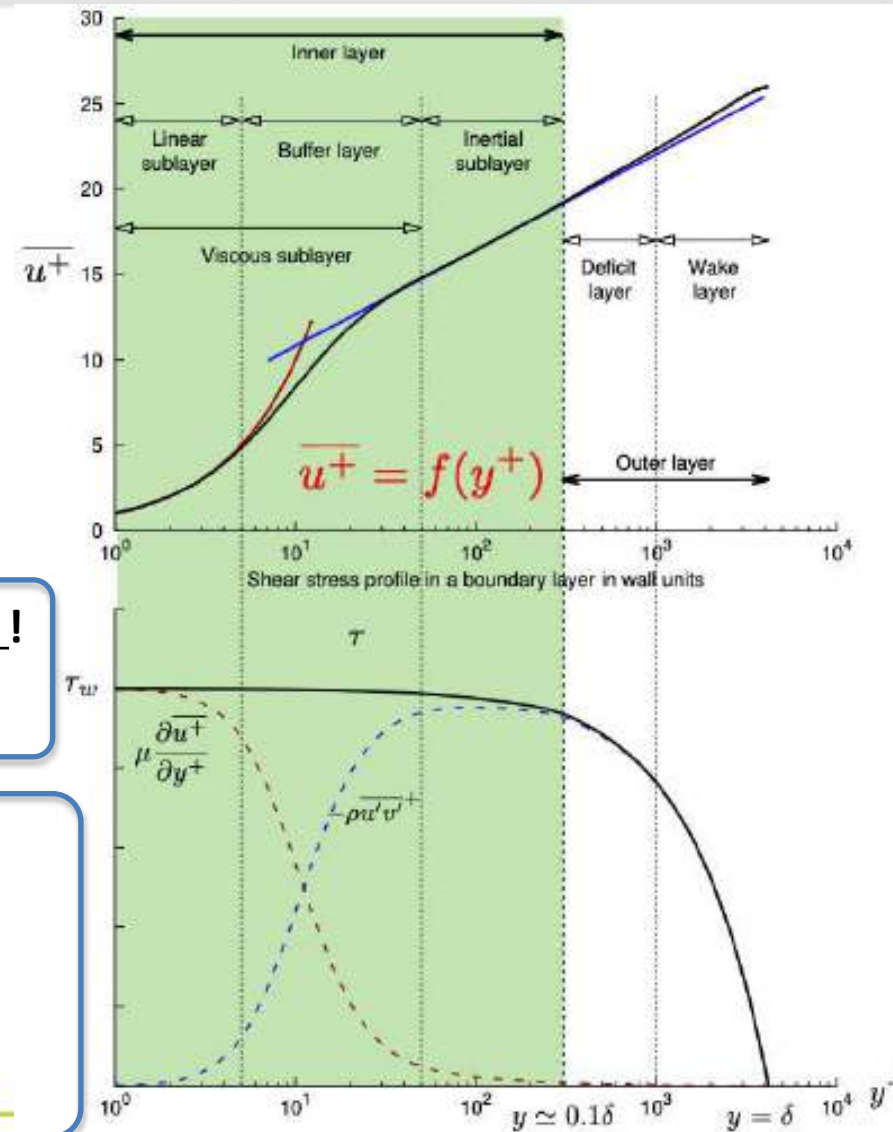
$$0 = \frac{\partial}{\partial y} \left[-\rho \overline{u'v'} + \mu \frac{\partial \bar{u}}{\partial y} \right] = \frac{\partial \tau}{\partial y}$$

=> In the inner layer, **total shear stress = constant !**

$$\tau = \text{cst} = \tau_w$$

Let's define:

- $\bar{u}^+ = \frac{\bar{u}}{u_\tau} = f(y^+)$
- $u_\tau = \sqrt{\frac{\tau_w}{\rho}}$
- $y^+ = \frac{yu_\tau}{\nu}$



$$0 = \underbrace{\nu \frac{\partial^2 \bar{u}}{\partial y^2}}_{\text{viscous stress}} + \underbrace{\frac{\partial (-\overline{u'v'})}{\partial y}}_{\text{Reynolds shear stress}}$$

Velocity profile in a turbulent BL

- Very near the wall:

Reynolds stress
negligible:

$$\mu \frac{\partial^2 \bar{u}}{\partial y^2} = 0$$

- Integration:

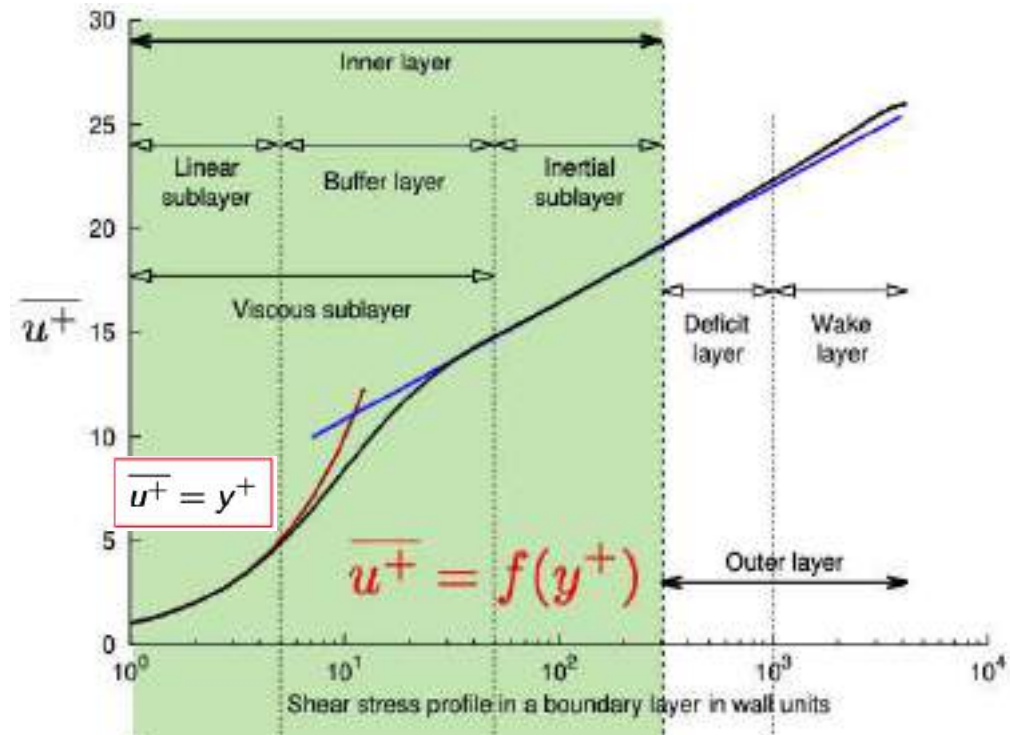
$$u = \text{cst} \times y = \frac{\tau_w}{\mu} y$$

- In inner variables:

$$\bar{u}^+ = y^+$$

Linear layer

$$y^+ \sim 3-5$$



$$\bar{u}^+ = \frac{\bar{u}}{u_\tau} \quad u_\tau = \sqrt{\frac{\tau_w}{\rho}}$$

$$y^+ = \frac{y u_\tau}{\nu}$$

$$0 = \underbrace{\nu \frac{\partial^2 \bar{u}}{\partial y^2}}_{\text{viscous stress}} + \underbrace{\frac{\partial (-\overline{u'v'})}{\partial y}}_{\text{Reynolds shear stress}}$$

Velocity profile in a turbulent BL

- Away from the viscous region: Reynolds stress dominates : $\tau = \cancel{\mu \frac{\partial \bar{u}}{\partial y}} - \rho \overline{u'v'}$

- Boussinesq hypothesis:

$$-\overline{u'v'} = \nu_t \frac{\partial \bar{u}}{\partial y}$$

- Mixing length hypothesis:

$$\nu_t = \kappa u_\tau y$$

Von Karman "constant",
 $\kappa \approx 0.41$

$$\mu_t \frac{\partial \bar{u}}{\partial y} = \tau_w$$

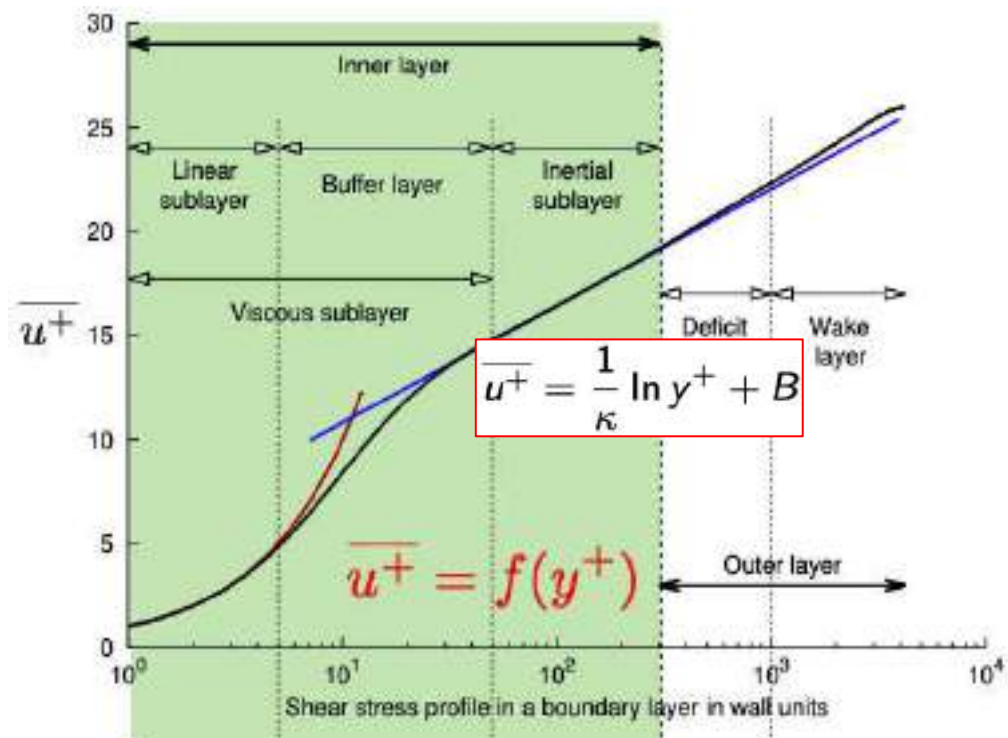
$$\rho \kappa u_\tau y \frac{\partial \bar{u}}{\partial y} = \tau_w = \rho u_\tau^2$$

$$\kappa \frac{\partial \bar{u}}{u_\tau} = \frac{\partial y}{y}$$

$$du^+ = \frac{1}{\kappa} \frac{dy^+}{y^+}$$

$$u^+ = \frac{1}{\kappa} \ln(y^+) + B$$

Logarithmic layer



$$\begin{aligned} u^+ &= \frac{\bar{u}}{u_\tau} & u_\tau &= \sqrt{\frac{\tau_w}{\rho}} \\ y^+ &= \frac{y u_\tau}{\nu} \end{aligned}$$

$$0 = \underbrace{\nu \frac{\partial^2 \bar{u}}{\partial y^2}}_{\text{viscous stress}} + \underbrace{\frac{\partial (-\overline{u'v'})}{\partial y}}_{\text{Reynolds shear stress}}$$

Velocity profile in a turbulent BL

- Very near the wall:

Reynolds stress negligible:

$$\overline{u^+} = y^+$$

Linear layer

$$y^+ \sim 3-5$$

- Away from the viscous region:

Reynolds stress dominates:

$$\overline{u^+} = \frac{1}{\kappa} \ln y^+ + B$$

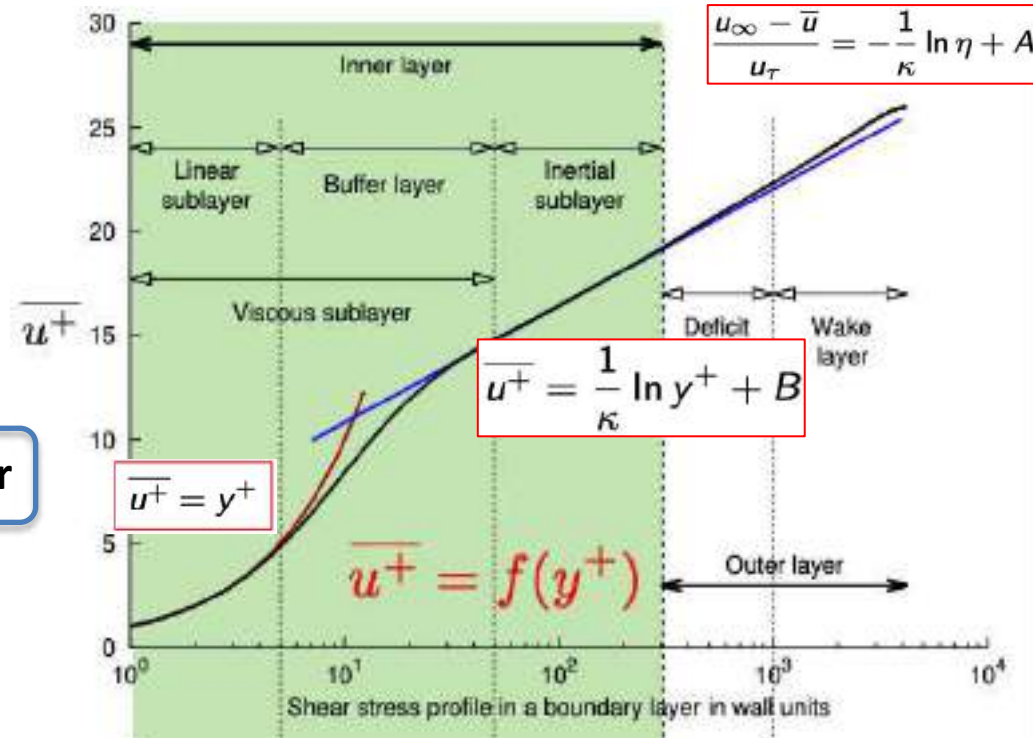
Logarithmic layer

- We can also demonstrate:

Close to $y \simeq \delta$

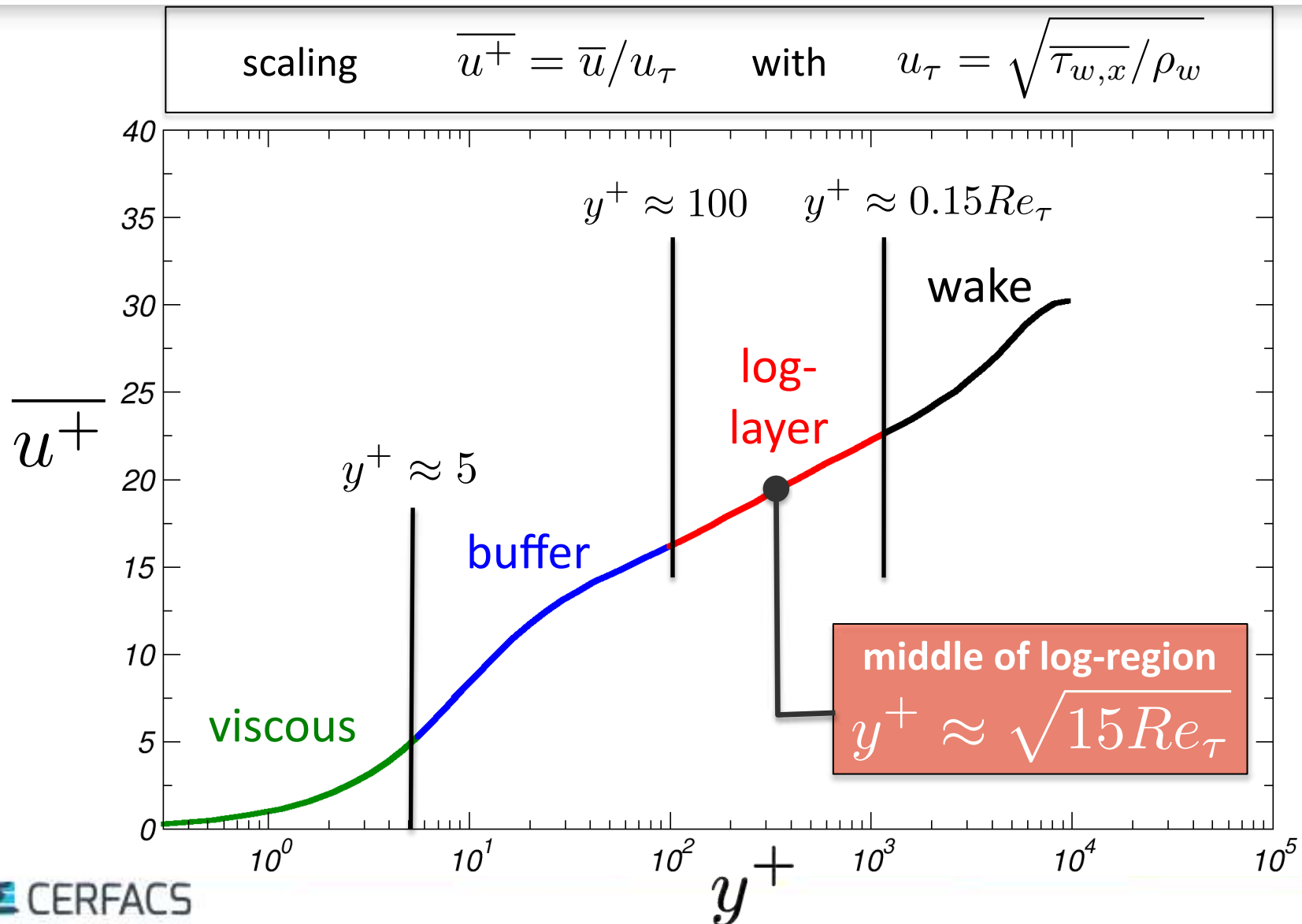
$$\frac{u_\infty - \bar{u}}{u_\tau} = -\frac{1}{\kappa} \ln \eta + A$$

Wake layer
 $\eta = y/\delta$

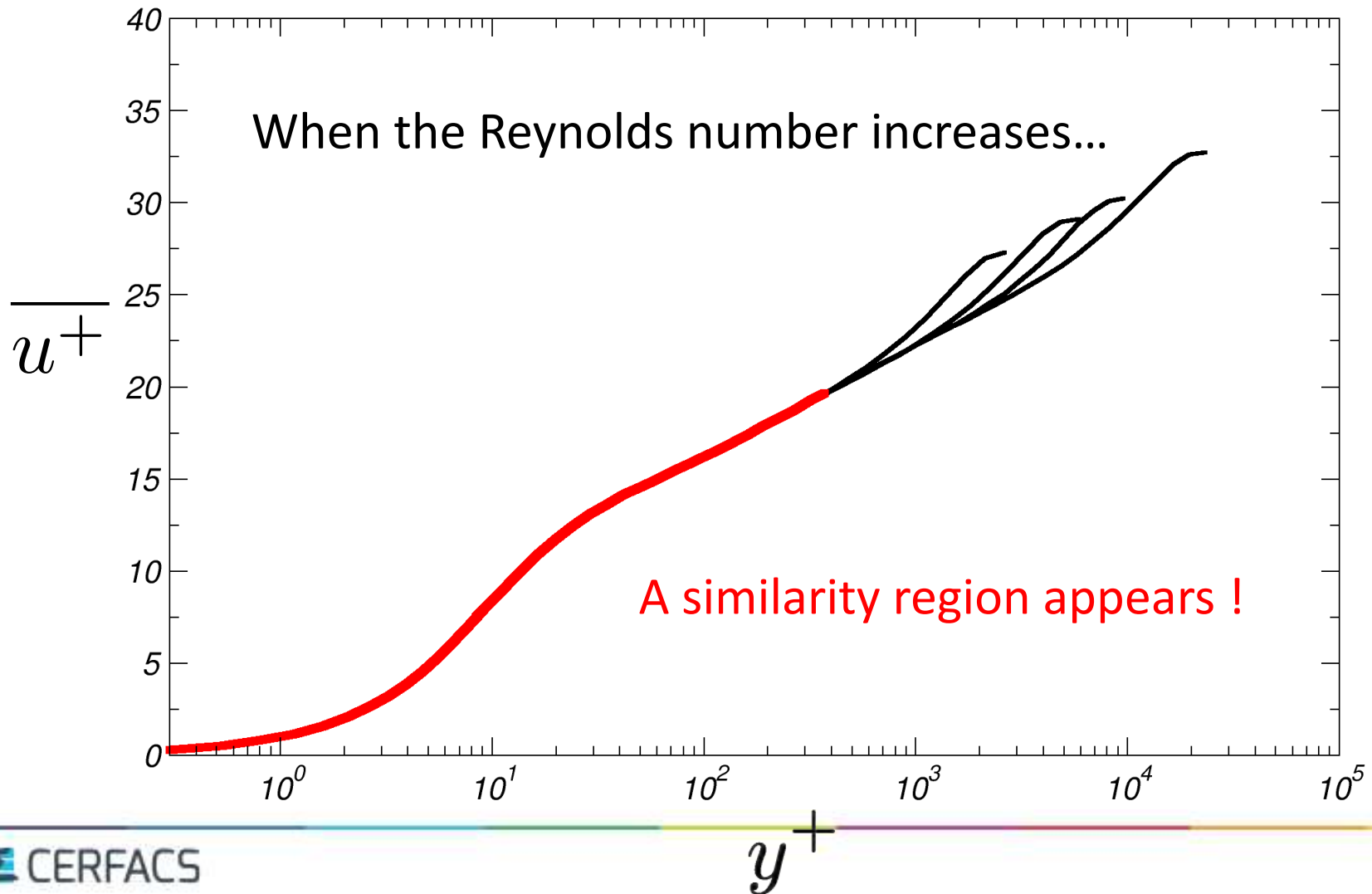


$$\overline{u^+} = \frac{\bar{u}}{u_\tau} \quad y^+ = \frac{y u_\tau}{\nu} \quad u_\tau = \sqrt{\frac{\tau_w}{\rho}}$$

Velocity profile in a turbulent BL

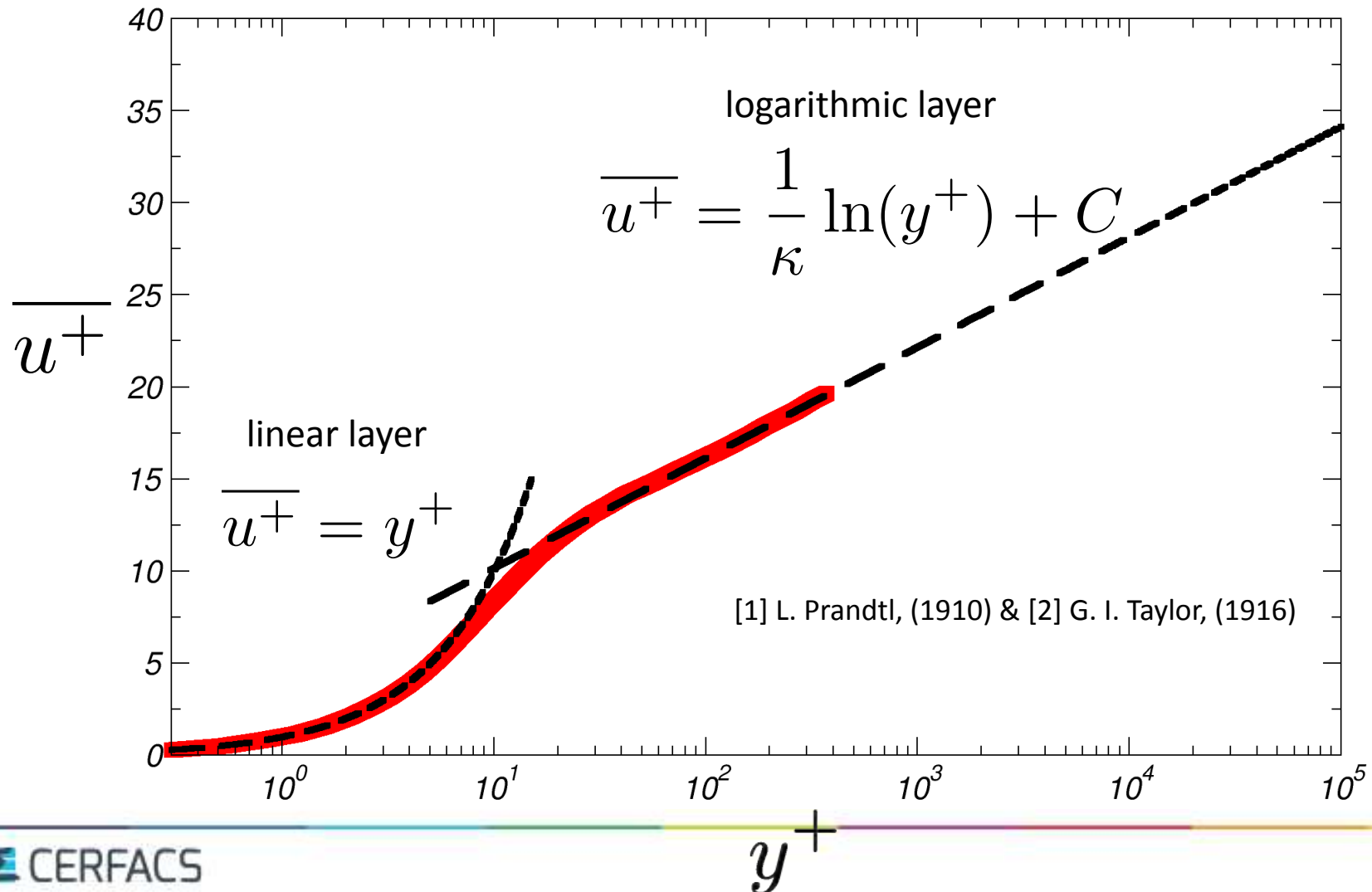


Velocity profile in a turbulent BL



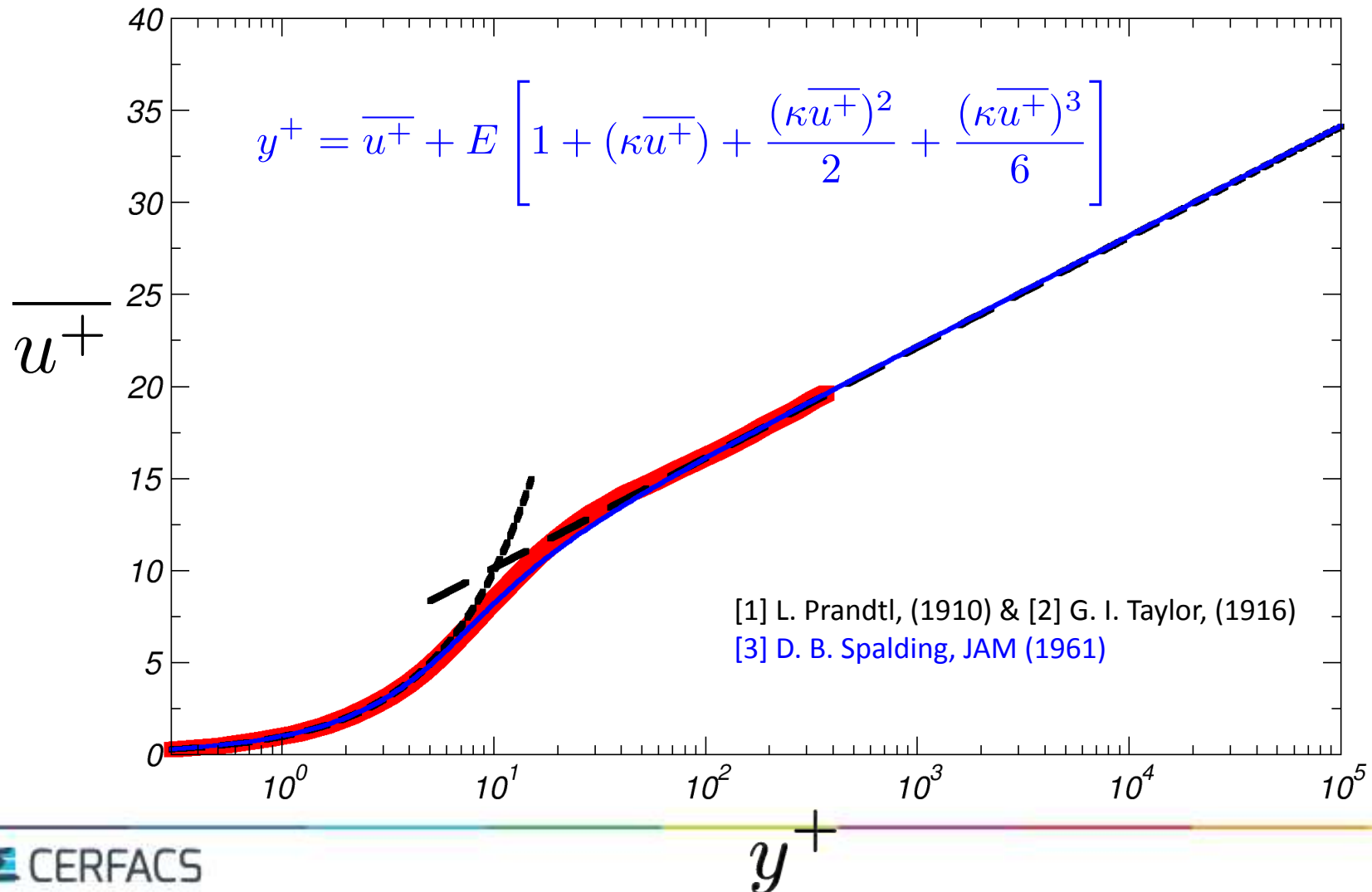
Let's model this velocity profile... The **wall-law**

2-layer approach [1-2]



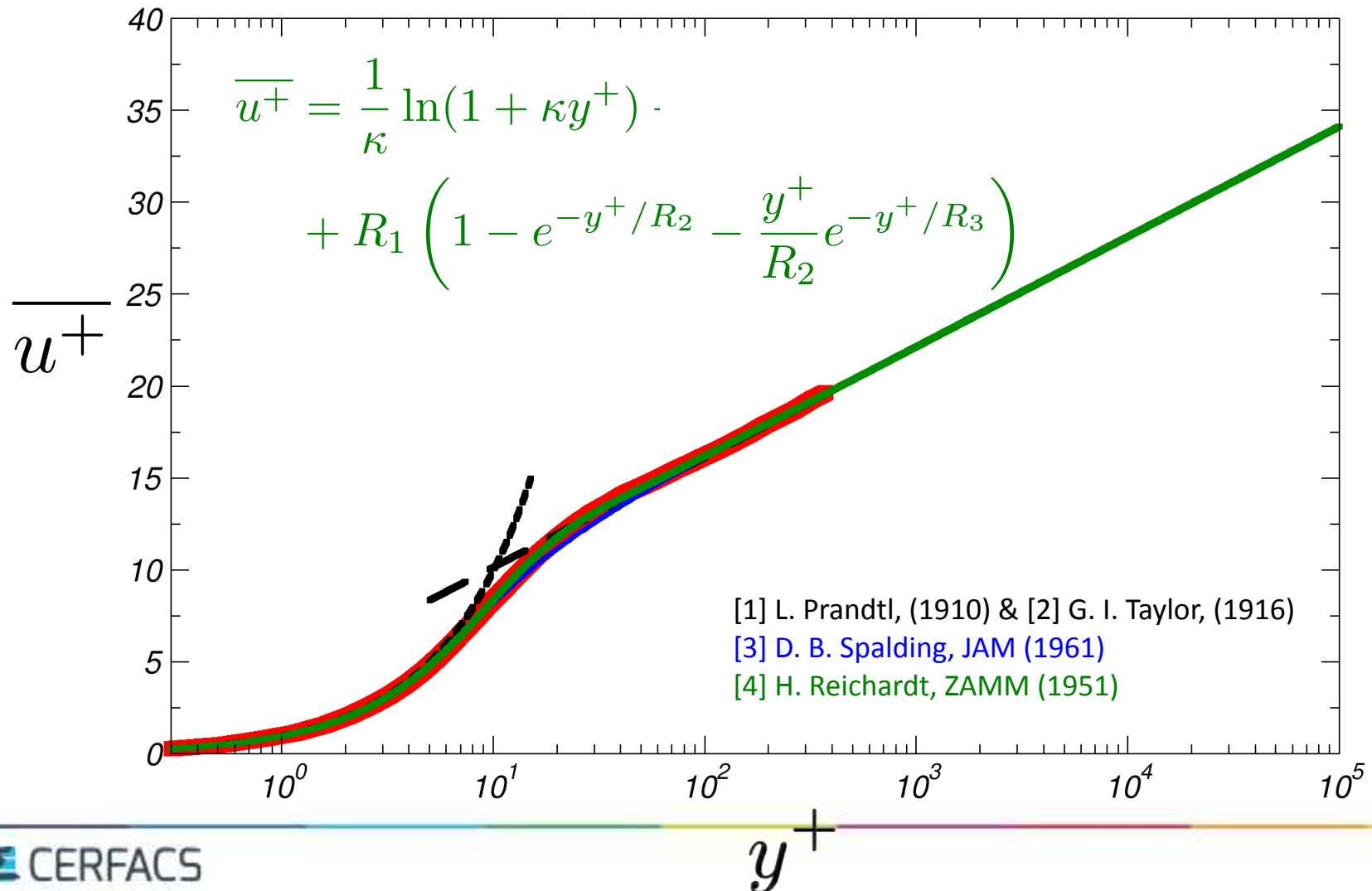
Let's model this velocity profile... The wall-law

Spalding's Law [3]

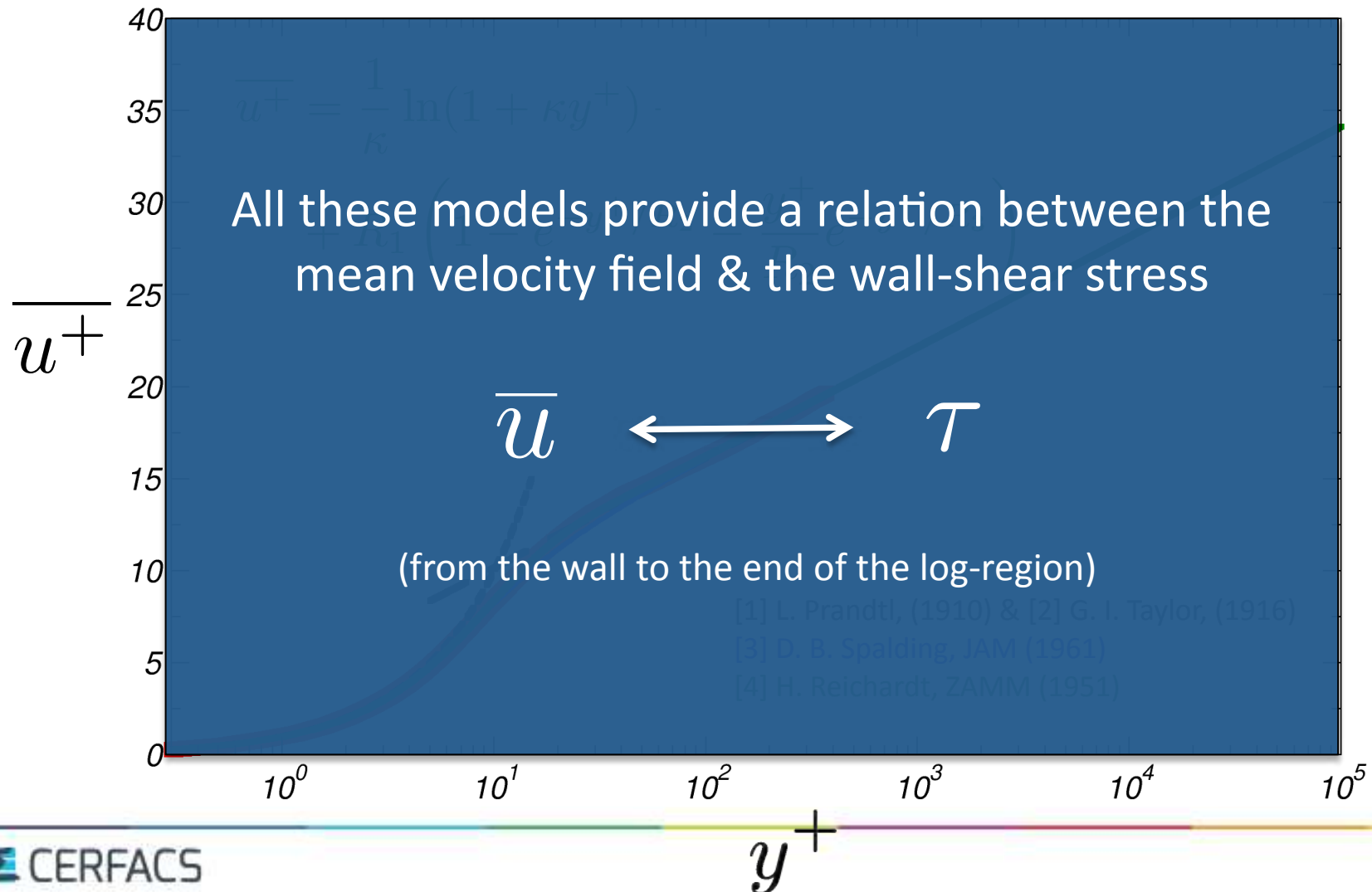


Let's model this velocity profile... The wall-law

Reichardt's Law [4]



Let's model this velocity profile... The wall-law



Let's model this velocity profile... The wall-law

$\overline{u^+} = f(y^+)$ is called the “**wall-law**”, or “**law-of-the-wall**”

The **simplest** wall-law is the **2-layer law**:

- $\overline{u^+} = y^+$ For low y^+
- $\overline{u^+} = \frac{1}{\kappa} \ln y^+ + B$ For $y^+ > 10$

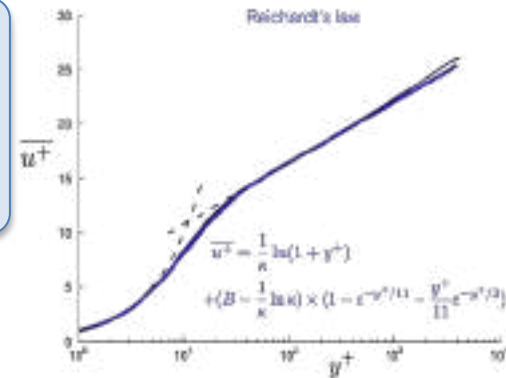
Provide a **relation** between **mean velocity** and mean wall **shear stress**:

$$\overline{u} \longleftrightarrow \tau_w$$

Relies on **assumptions!**

- **Stationary** flow
- No pressure gradient
- Attached flow
- Flat plate
- 2D
- Incompressible
- Fully turbulent

$$\begin{aligned}\overline{u^+} &= \frac{\overline{u}}{u_\tau} \\ y^+ &= \frac{y u_\tau}{\nu} \\ u_\tau &= \sqrt{\frac{\tau_w}{\rho}}\end{aligned}$$





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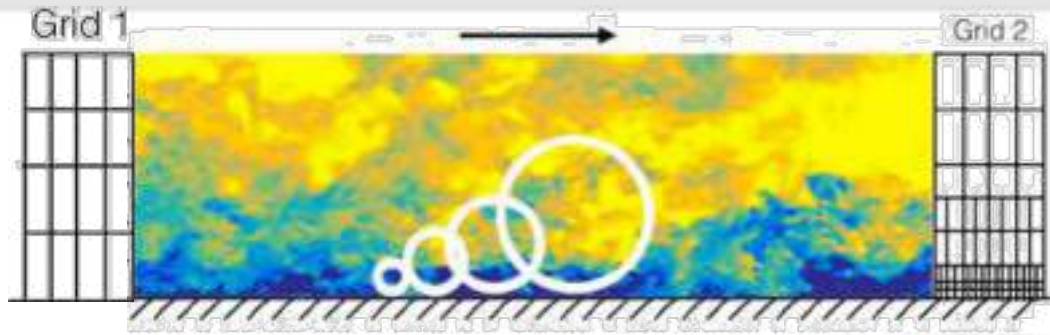
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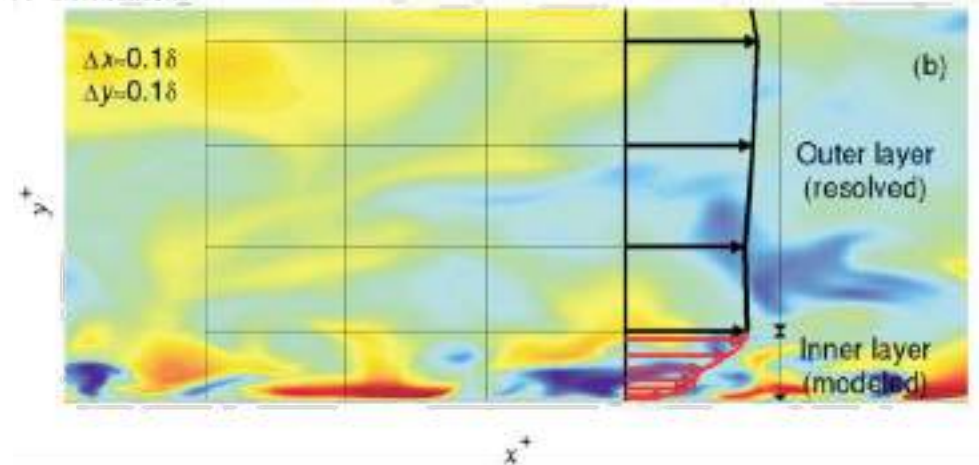
Wall-bounded turbulent injection

Wall-modeled LES: principle



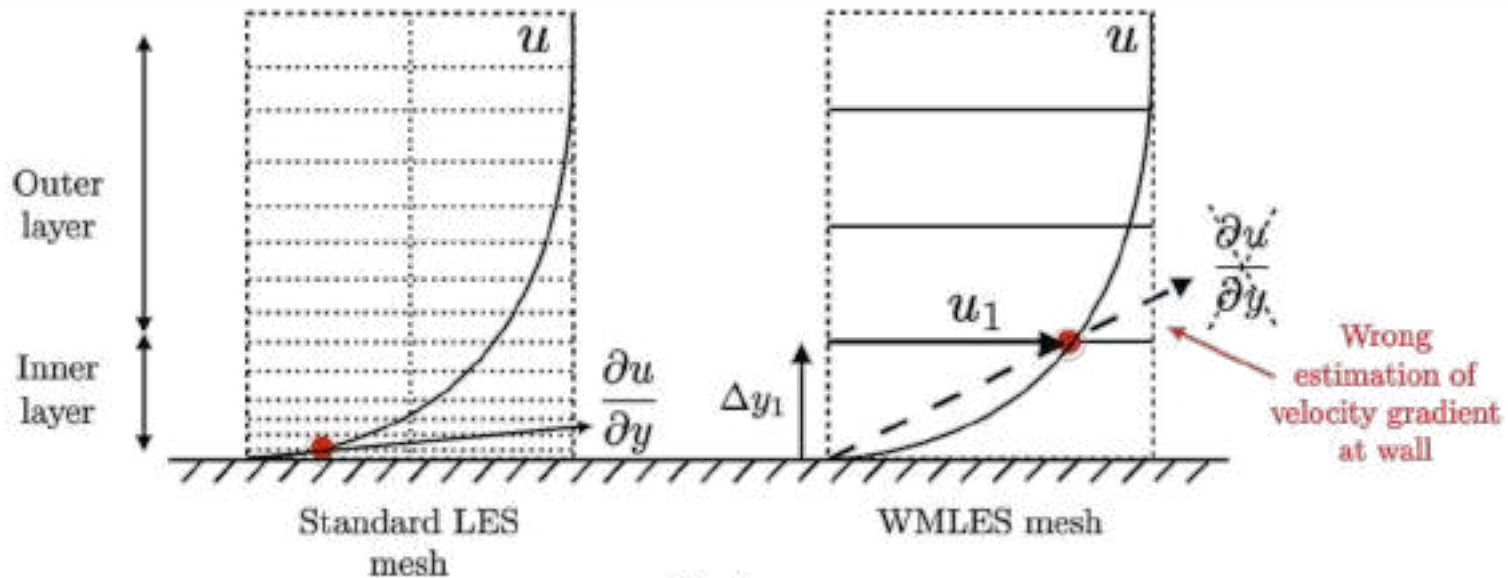
Bae et al. 2018

Piomelli Balaras 2002



- Mesh dedicated to the **outer layer**.
- **Inner layer** not resolved in WMLES => a **model** is needed.
- **SGS model** and **numerical method** likely to induce **non-physical structures...**

Wall-modeled LES: principle



- We need to compute $\tau_w = \mu_w \left. \frac{\partial u}{\partial y} \right|_{y=0}$

- For wall-**resolved** LES:
(fine mesh)

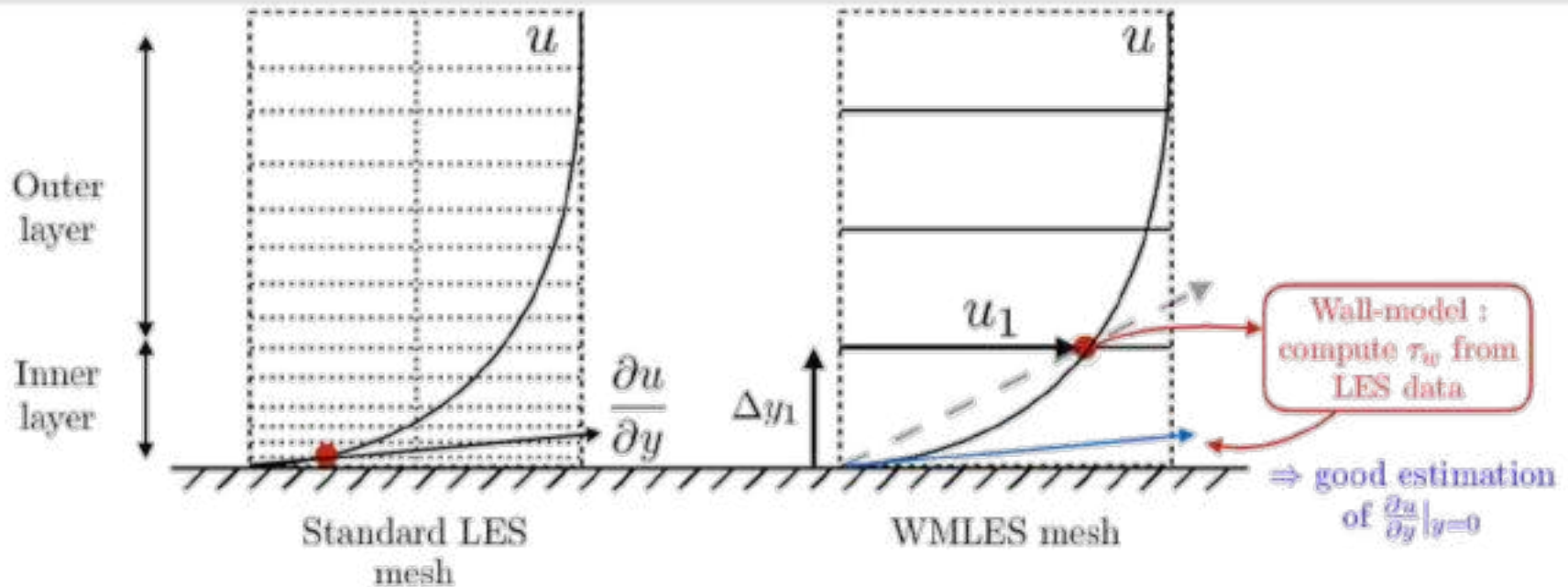
$$\tau_w \simeq \mu_w \frac{u_1}{\Delta y_1}$$

- For wall-**modeled** LES:
(Coarse mesh)

~~$$\tau_w \simeq \mu_w \frac{u_1}{\Delta y_1}$$~~

Using finite-difference, τ_w is **overestimated** on **coarse** meshes.
=> **A model is needed.**

Analytical Wall-modeled LES



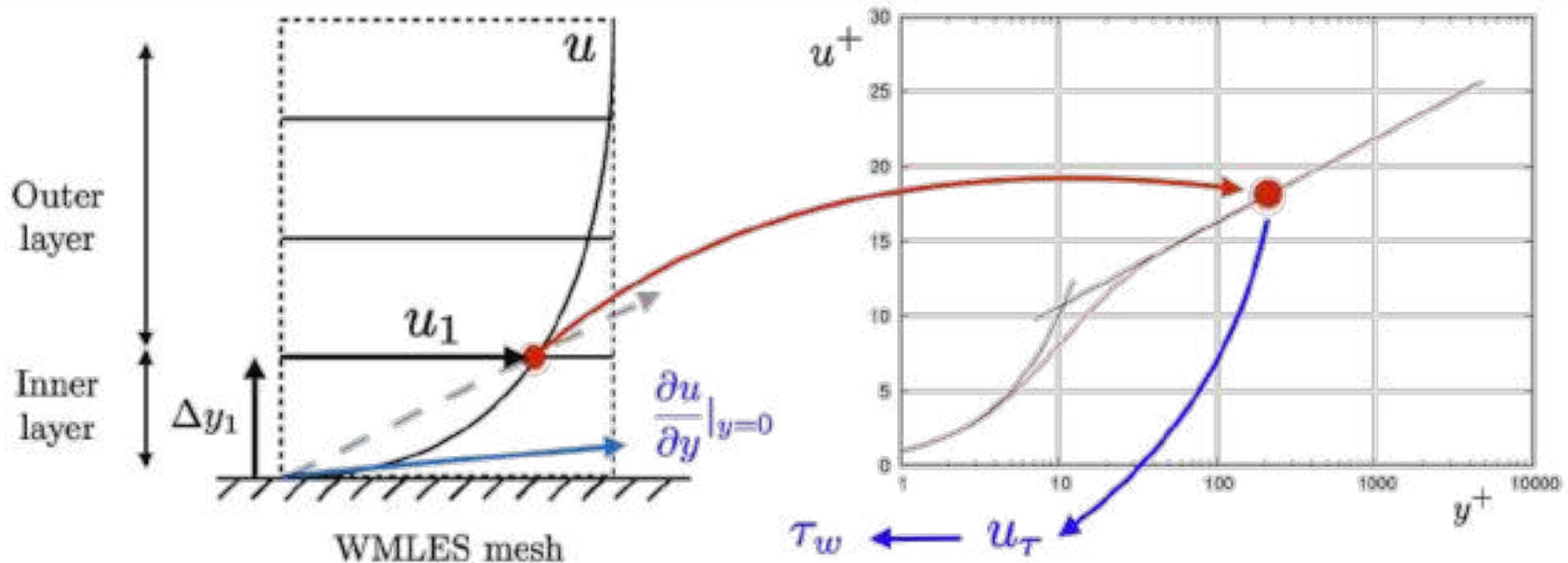
Wall modeling: provide an estimate of the wall –flux τ_w using the LES velocity at the first grid node.

Analytical law: $\overline{u^+} = f(y^+)$ (based on the log-law) provides τ_w .

Cost of an analytical law is negligible compared to a LES iteration.

Assumptions: stationary 2D flow, no pressure gradient, attached BL.

Analytical Wall-modeled LES



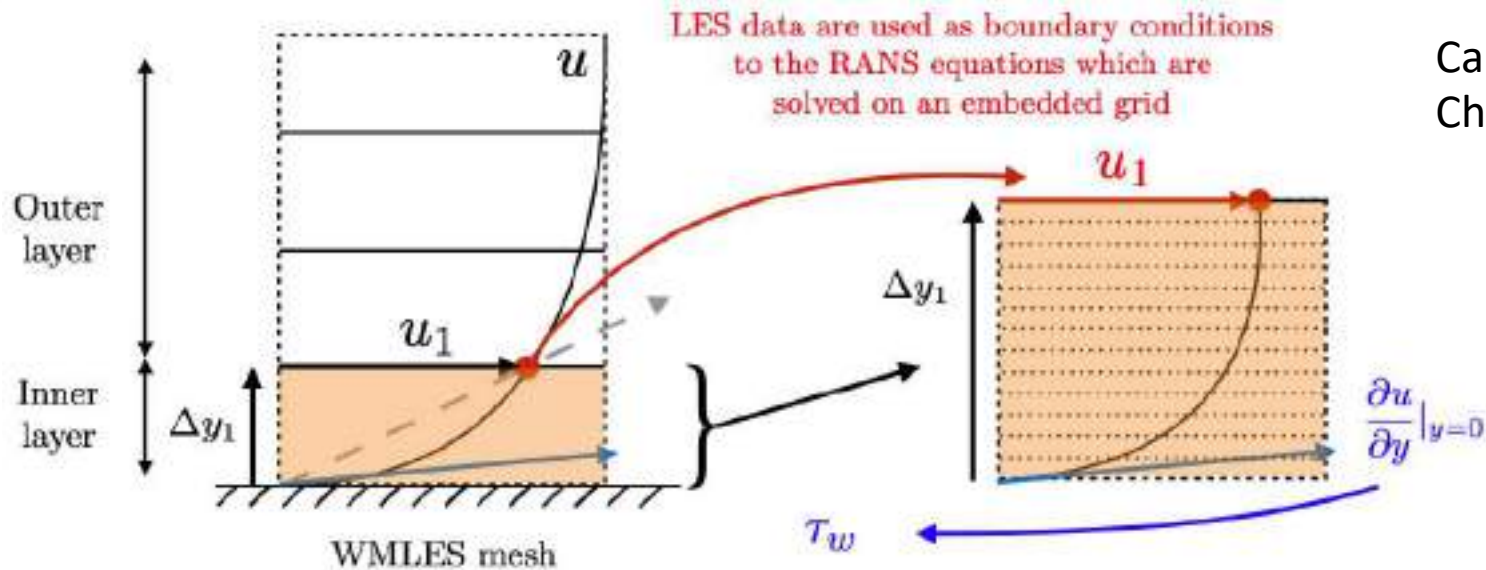
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Assumptions: stationary 2D flow, no pressure gradient, attached BL.

“Numerical” wall modeling: TBLE



Cabot & Moin,
Chen et al.

Instead using analytical law, a **set of differential equations** is solved on an embedded grid (=> **numerical** model).

Thin Boundary Layer Equations:

$$\rho \frac{\partial u}{\partial t} + \rho v_i \frac{\partial u}{\partial x_i} = - \frac{\partial p}{\partial x} + \frac{\partial}{\partial y} [(\mu + \mu^t) \frac{\partial u}{\partial y}]$$

$$\frac{\partial}{\partial y} [(\mu + \mu^t) \frac{\partial u}{\partial y}] = 0$$

2nd order **ordinary** differential equation
(Ex: Thomas Algorithm)



“Numerical” wall modeling: TBLE

$$\cancel{\frac{\partial \tilde{u}_i}{\partial t}} + \cancel{\frac{\partial (\tilde{u}_i \tilde{u}_j)}{\partial x_j}} + \cancel{\frac{\partial P_m}{\partial x_i}} = \frac{\partial}{\partial y} \left[(\nu + \nu_t) \frac{\partial \tilde{u}_i}{\partial y} \right]$$

(Cabot and Moin 2000)

Let's assume

$$\nu_t = \kappa y u_\tau (1 - e^{-y^+/A})^2$$

(Mixing length with Van Driest damping)

$$\rightarrow u_\tau = \sqrt{\frac{\tau_w}{\rho}} \Rightarrow \underline{\text{Provides } \tau_w}$$

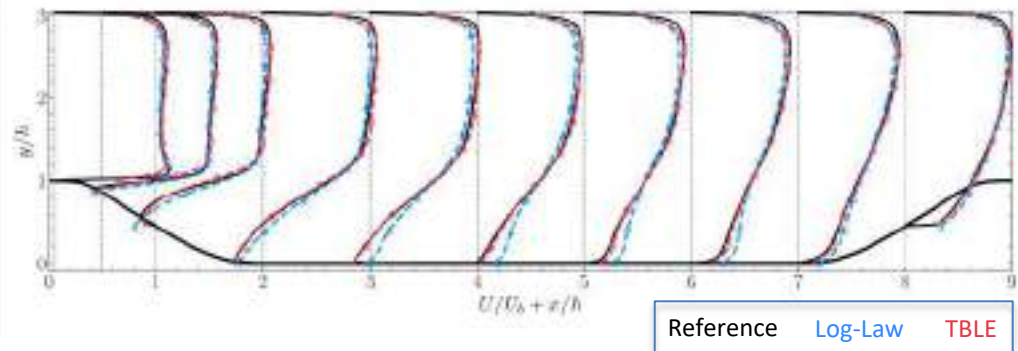
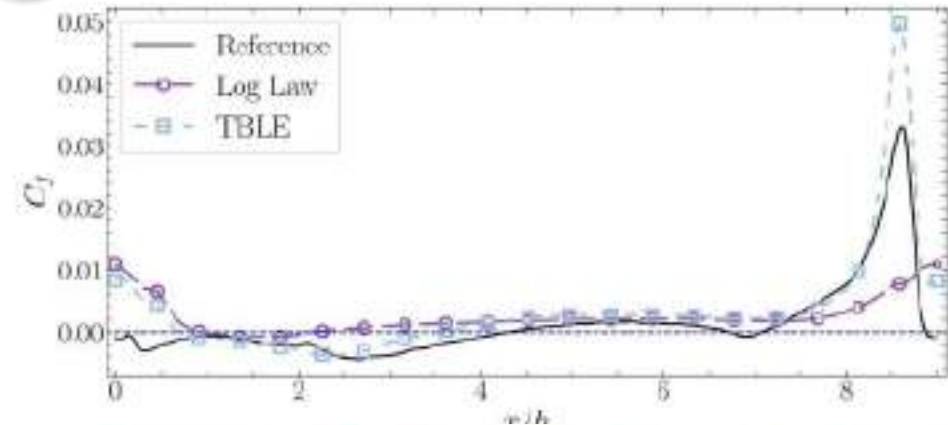
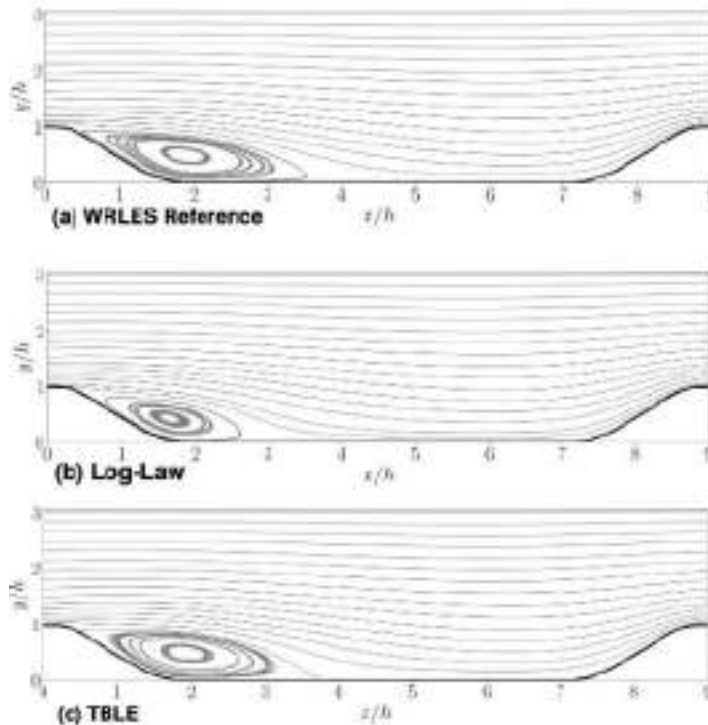
- Computational 10 to 20% more expensive than analytical law (but rather affordable regarding the LES iteration).
- Allow to account for complex effects (Pressure gradient, non-equilibrium, convective terms).

TBLE: Pressure gradient effect

- TBLE and **Pressure gradient** :

$$\frac{1}{\rho} \frac{\partial \bar{P}}{\partial x} = \frac{\partial}{\partial y} \left([\bar{\nu} + \nu_t] \frac{\partial \bar{u}}{\partial y} \right)$$

PhD Cizeron, 2024



- Temperature gradient** can also be accounted for:

$$\rho \bar{u} C_p \frac{\partial \bar{T}}{\partial x} + \frac{\partial}{\partial y} \left[(\lambda + \lambda_t) \frac{\partial \bar{T}}{\partial y} \right] = 0$$

Back to analytical WMLES... Complex physics: Heat Flux

- A logarithmic relation can also be derived for **thermal flux**:

$$\begin{cases} T^+ = \frac{P_{rt}}{\kappa} \ln(y^+) + \beta(P_r) \\ u^+ = \frac{1}{\kappa} \ln(y^+) + C_{vd} \end{cases}$$

Provides q_w

Provides τ_w

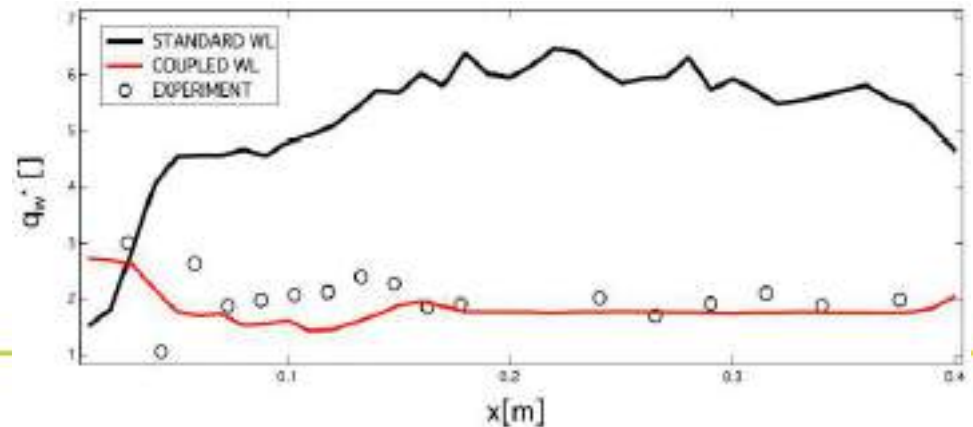
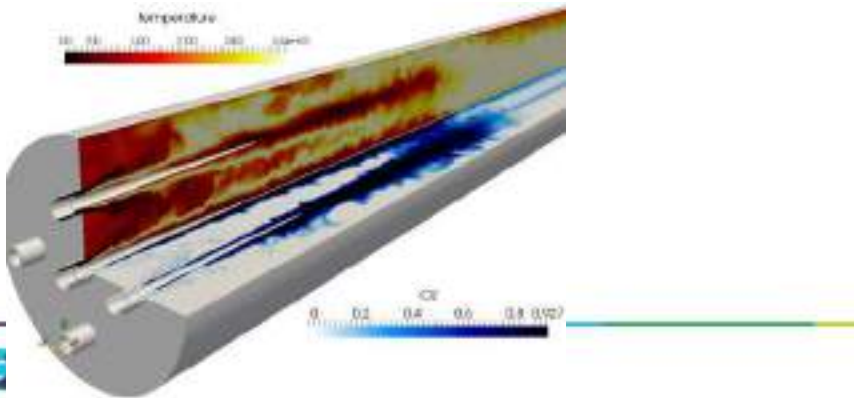
$$T^+ = \frac{\overline{T_w} - \overline{T}}{T_\tau}$$

$$T_\tau = \frac{\overline{q_w}}{\rho_w C_{p,w} u_\tau}$$

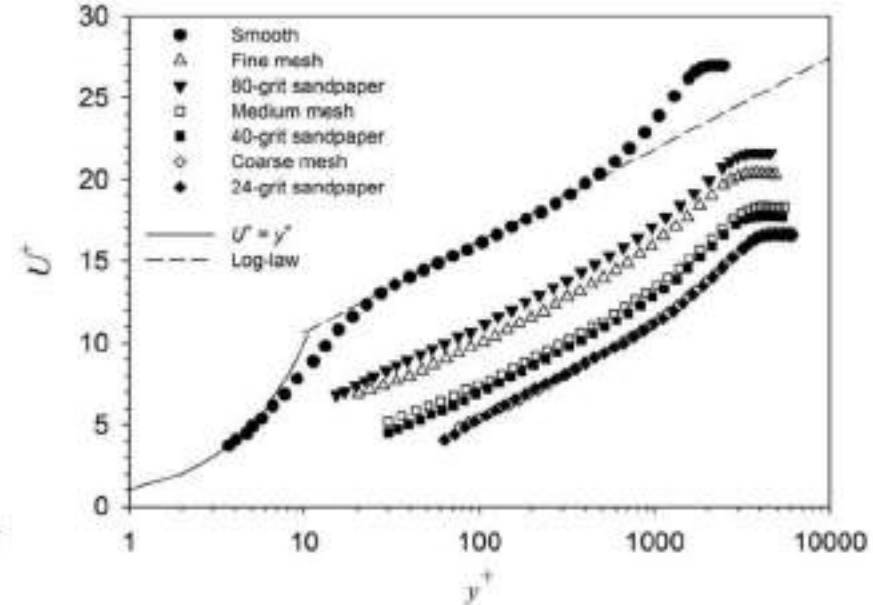
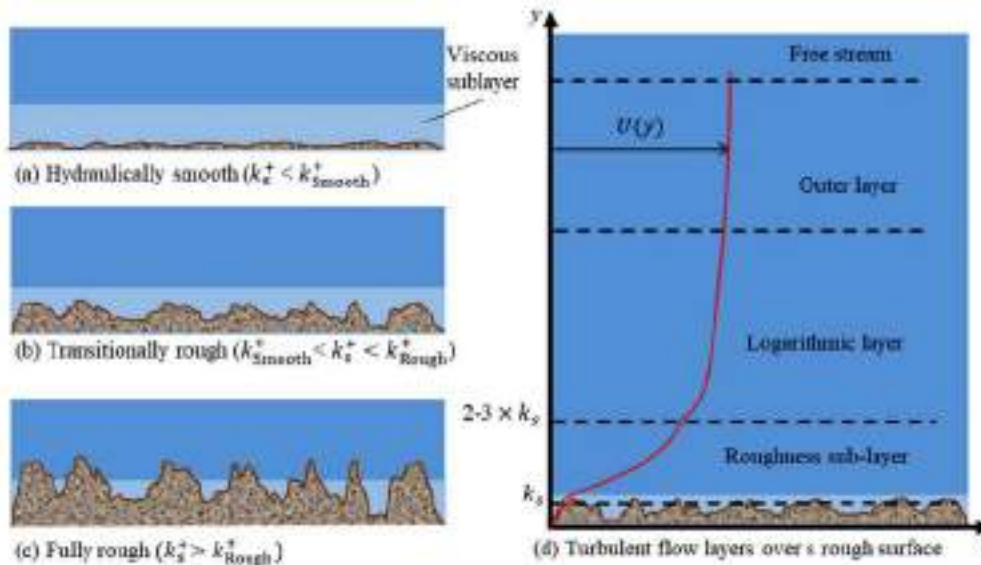
- Cabrit, 2009: **Coupled velocity-temperature** analytical wall model

$$\begin{cases} \frac{2}{P_{rt} B_q} \left(\sqrt{1 - K B_q} - \sqrt{\frac{T}{T_w}} \right) = \frac{1}{\kappa} \ln y^+ + C_{vd} \\ T^+ = P_{rt} u^+ + K \end{cases}$$

Strong improvement for **large temperature gradients** (rocket engines) :



Back to analytical WMLES... Complex physics: Roughness



Roughness modifies the mean velocity profile

Flack et al. POF 2007

Roughness can be accounted for through:

$$u^+ = \frac{1}{\kappa} \ln \left(\frac{y^+}{y_0} \right) + B$$

Reviews in :

Flack et al POF 2014
Kadivar 2021



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Wall-modeled LES: analytical, TBLE

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Turbulence injection

Synthetic methods (Fourier / POD)

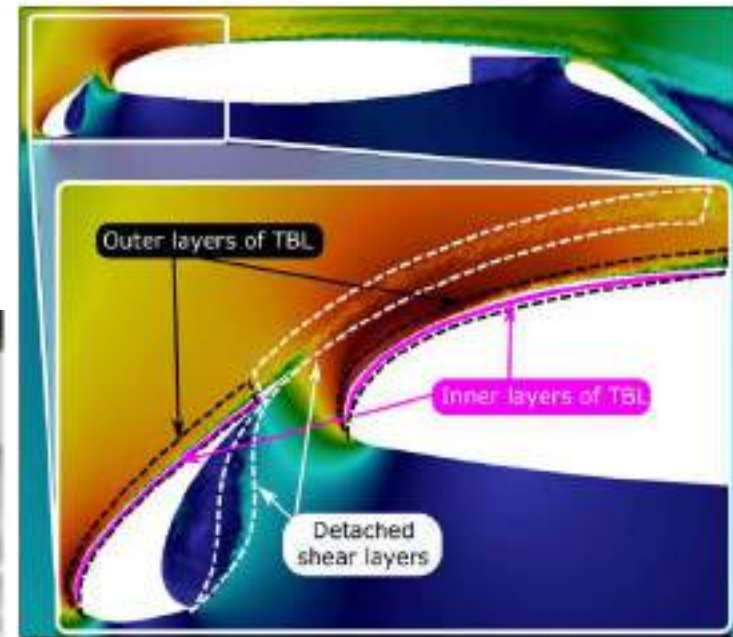
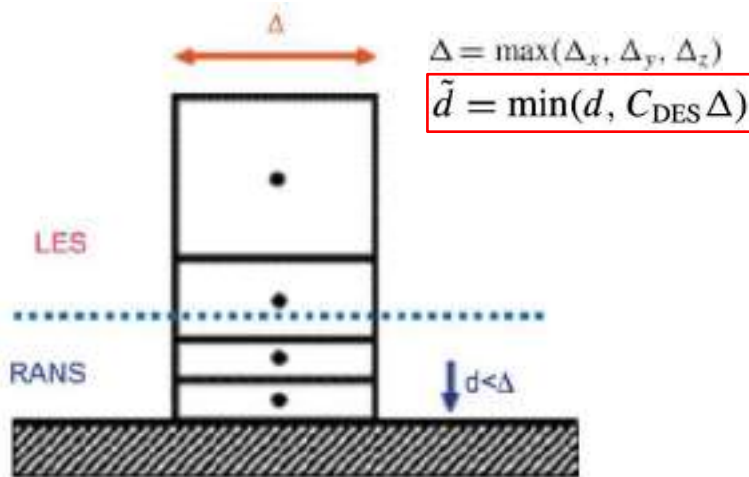
Precursor method

Wall-bounded turbulent injection

Detached-Eddy Simulation

Originally proposed by Spalart (1997): Intended for “detached” flow:

=> **LES** for **detached** flow, **RANS** for **attached BL**.



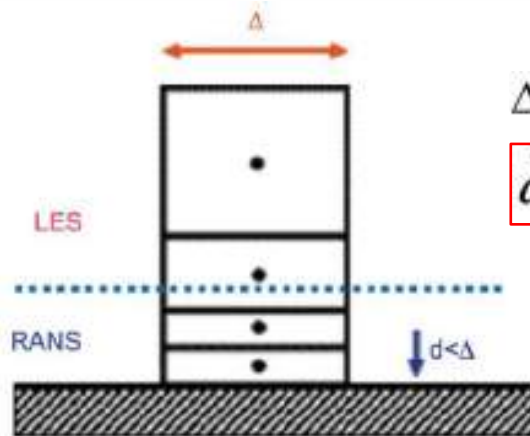
Concept:

Switch from **LES SGS** model to **RANS turbulence model** depending on the wall distance.

- **Close** to the wall: **RANS** modeling
- **Away** from the wall: **LES** modeling

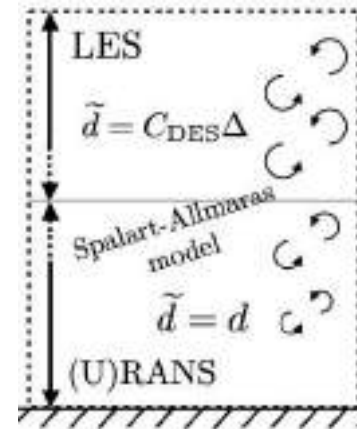
Uses a single grid.

Detached-Eddy Simulation



$$\Delta = \max(\Delta_x, \Delta_y, \Delta_z)$$

$$\tilde{d} = \min(d, C_{DES} \Delta)$$



- Close to the wall: $d_w < C_{DES} \Delta \Rightarrow$ **URANS**

Spalart-Allmaras model:

$$\nu_t = \tilde{\nu} f_{v1}$$

$$\frac{\partial \tilde{\nu}}{\partial t} + u_j \frac{\partial \tilde{\nu}}{\partial x_j} = C_{b1} [1 - f_{t2}] \tilde{S} \tilde{\nu} + \frac{1}{\sigma} \{ \nabla \cdot [(\nu + \tilde{\nu}) \nabla \tilde{\nu}] + C_{b2} |\nabla \tilde{\nu}|^2 \} - \left[C_{w1} f_w - \frac{C_{b1}}{\kappa^2} f_{t2} \right] \left(\frac{\tilde{\nu}}{d} \right)^2 + f_{t1} \Delta U^2$$

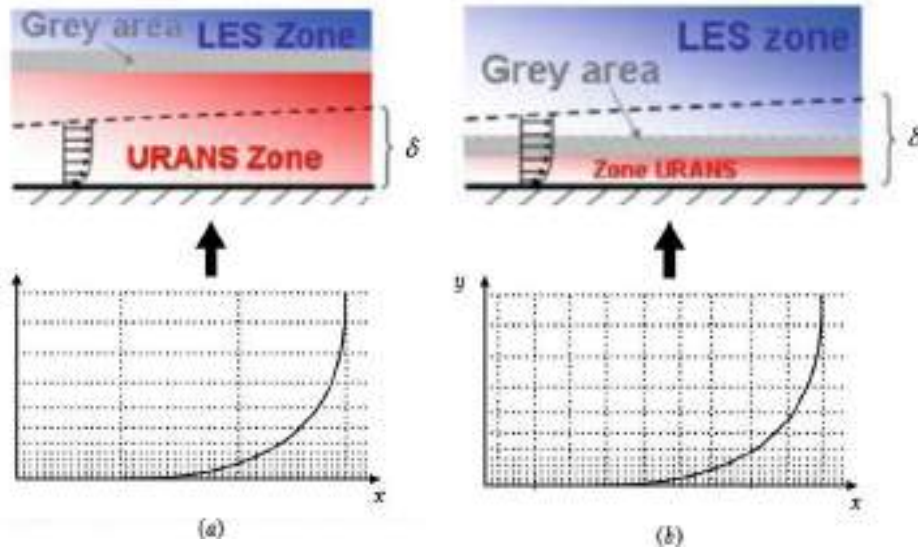
- Away from the wall: $d_w > C_{DES} \Delta \Rightarrow$ **LES**

Smagorinsky model: $\nu_t = (C_s \Delta)^2 \sqrt{2 \bar{S}_{ij} \bar{S}_{ij}}$

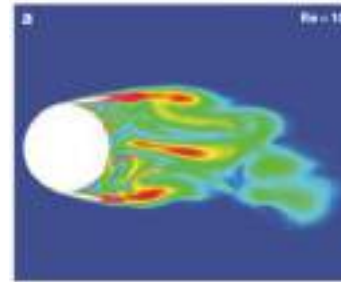


Detached-Eddy Simulation

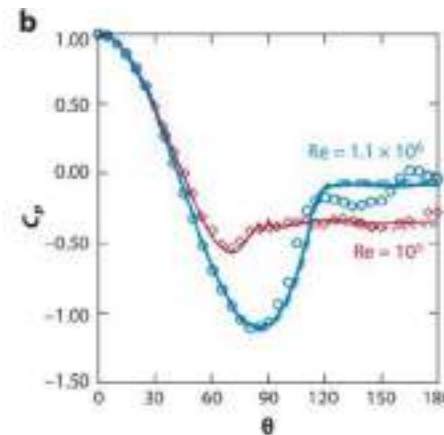
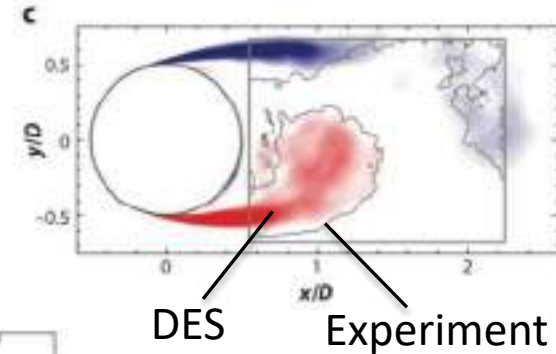
- Very efficient for massively separated flows



instantaneous



Phase averaging



(Mockett et al., 2008)

RANS / LES transition depends on the mesh resolution.

⇒ Significant solution dependency

Not so efficient for attached turbulent BL.

DES: other approaches

Delayed Detached Eddy Simulations (*Spalart, 2006*)

Add a constraint on d , to enforce URANS/LES transition out of the boundary layer.
Enforce BL resolution with URANS, reduces grid dependency.

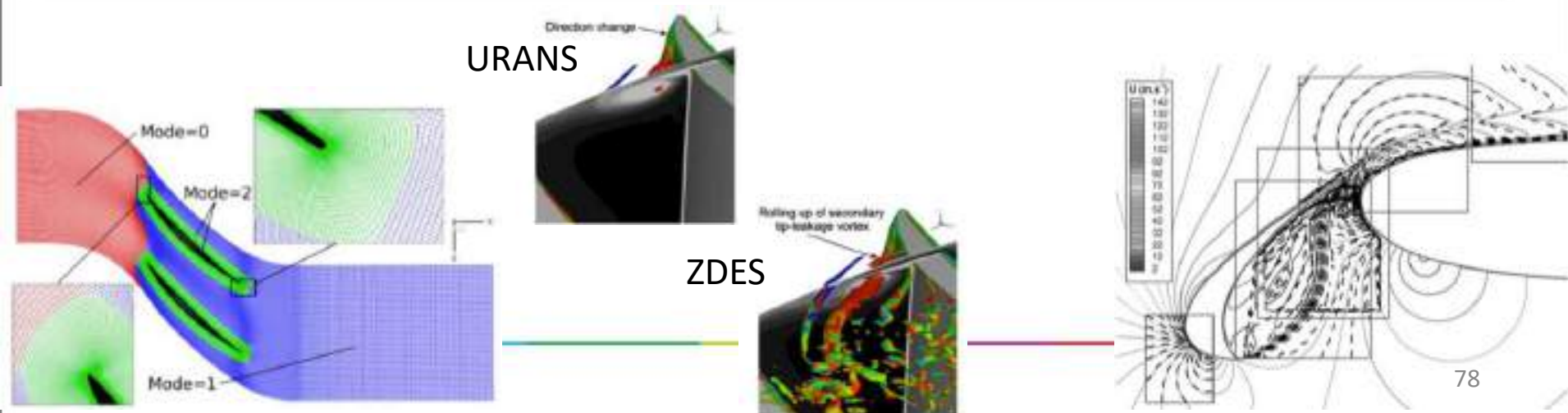
However, solution can depends on initial solution (*Fröhlich and Terzi, 2008*)

Improved Detached Eddy Simulation (*Shur et al., 2008*)

Define Δ as a function of grid size + wall distance: $\Delta = f(h_x, h_y, h_z, d_w)$

Zonal Detached Eddy Simulation (*Deck et al., 2005, 2011*)

Explicit definition of URANS / LES transition





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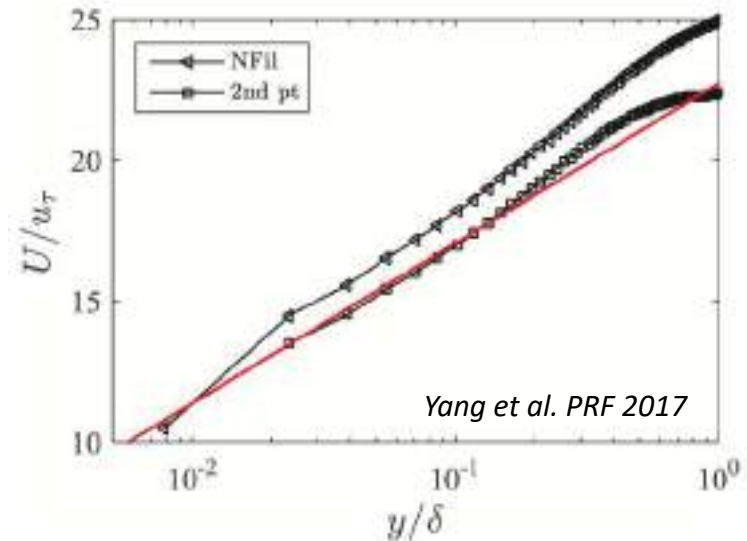
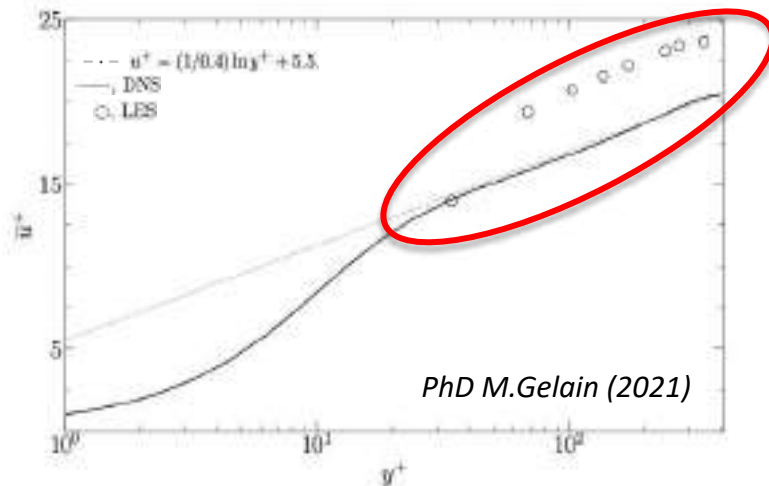
Wall-bounded turbulent injection



Log-layer mismatch

- SGS models: WALE, Sigma, ... developed in a **Wall-resolved** context
- Wall-models: First intended for RANS context, **without SGS** models

When coupling both...: « **Log-layer mismatch** » !



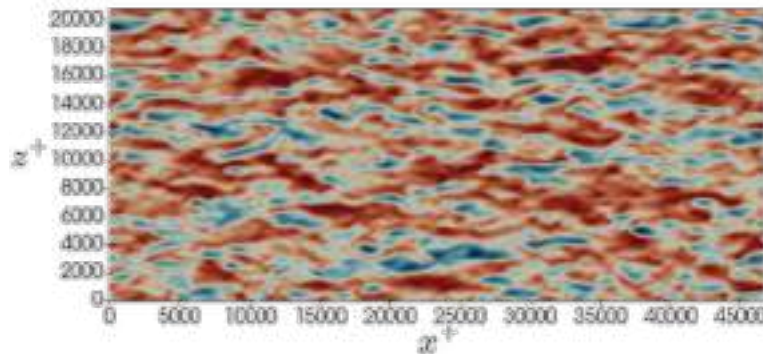
- ⇒ Correction of SGS viscosity
- ⇒ Matching point at 2nd, 3rd off-wall node
- ⇒ Temporal filtering
- ⇒ Stochastic forcing in 1st cell

Still a current topic of interest...

Impact of modeling

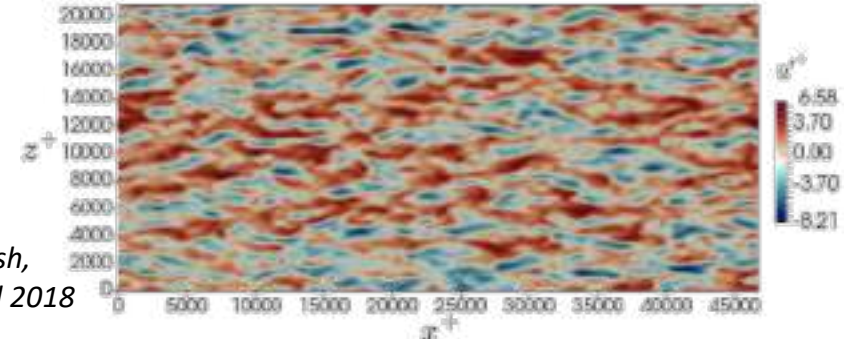
Impact of SGS modeling: flat plate, using an analytical Spalding wall-model

No SGS

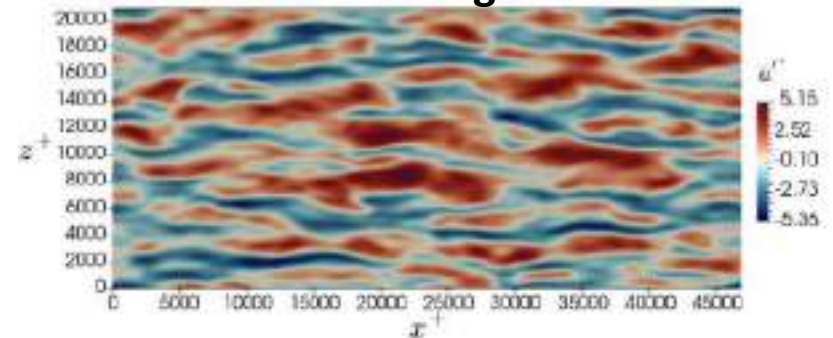


Rezaeiravesh,
Liefvendahl 2018

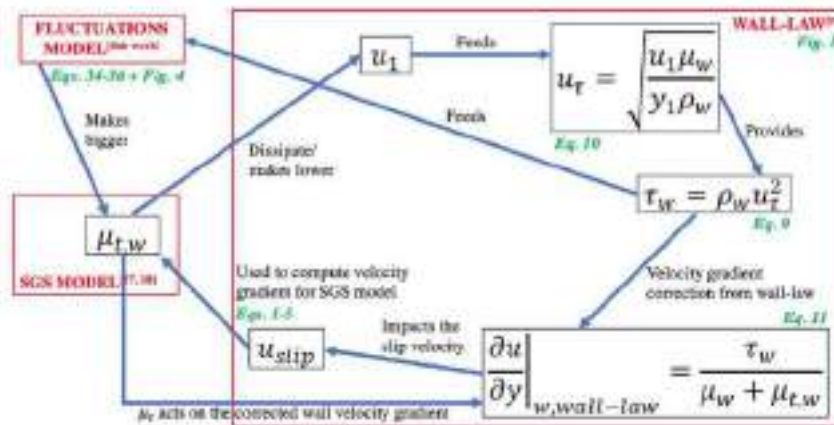
WALE



Smago



Wall law – SGS coupling

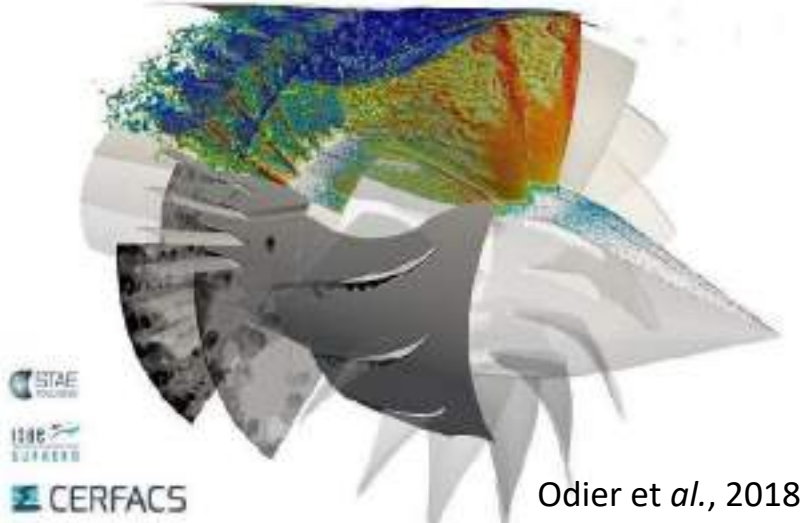


- Wall-modeling and SGS modeling can be **tightly coupled**.
- Result can be highly sensitive to the SGS model.



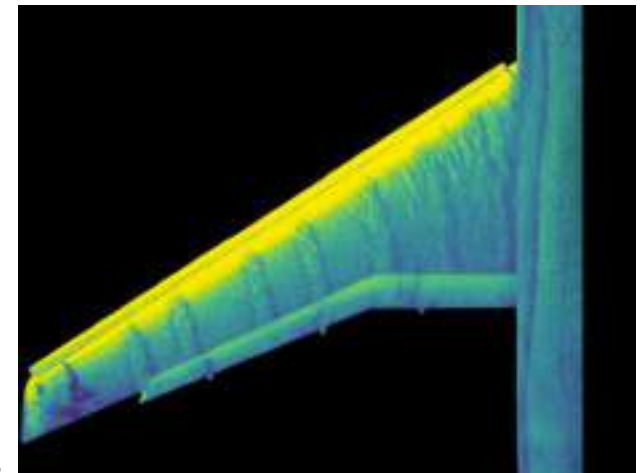
Applications: analytical WMLES

Turbomachinery Aerodynamics



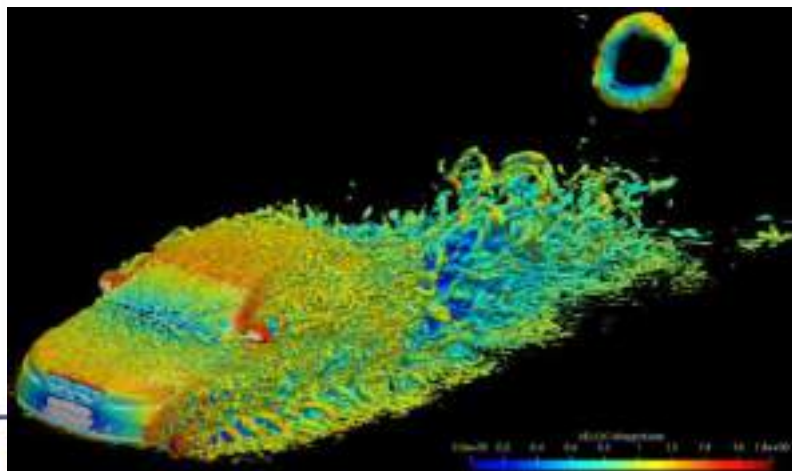
Odier et *al.*, 2018

Aeronautical flows at stall conditions



Lehmkuhl et *al.*, 2018

Automotive aerodynamics



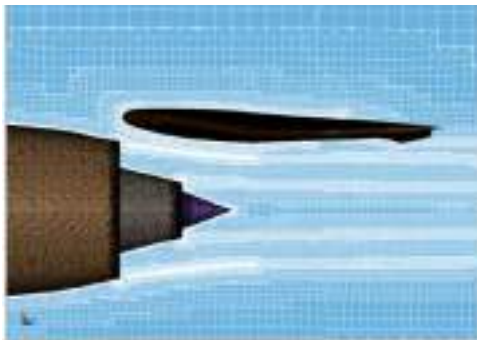
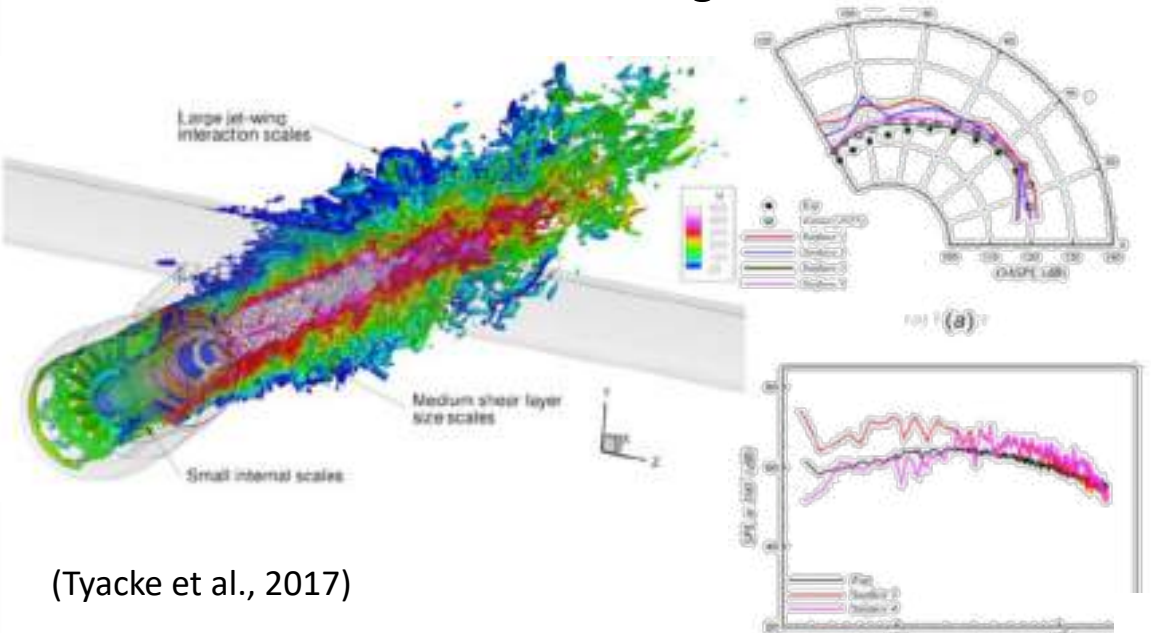
Lehmkuhl et *al.*, 2018



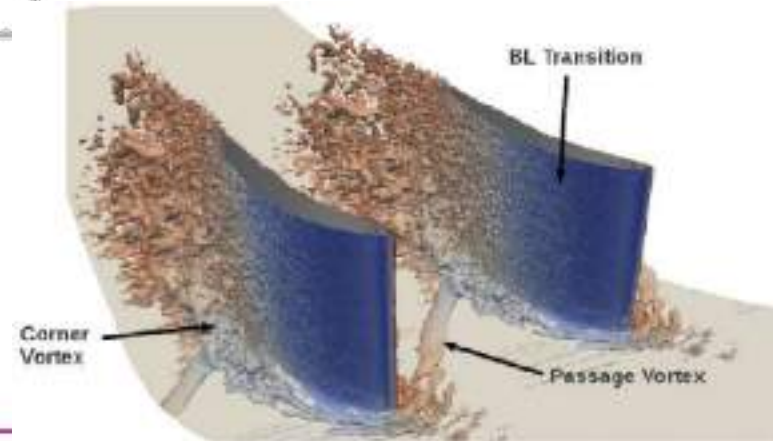


Applications: Hybrid RANS/LES

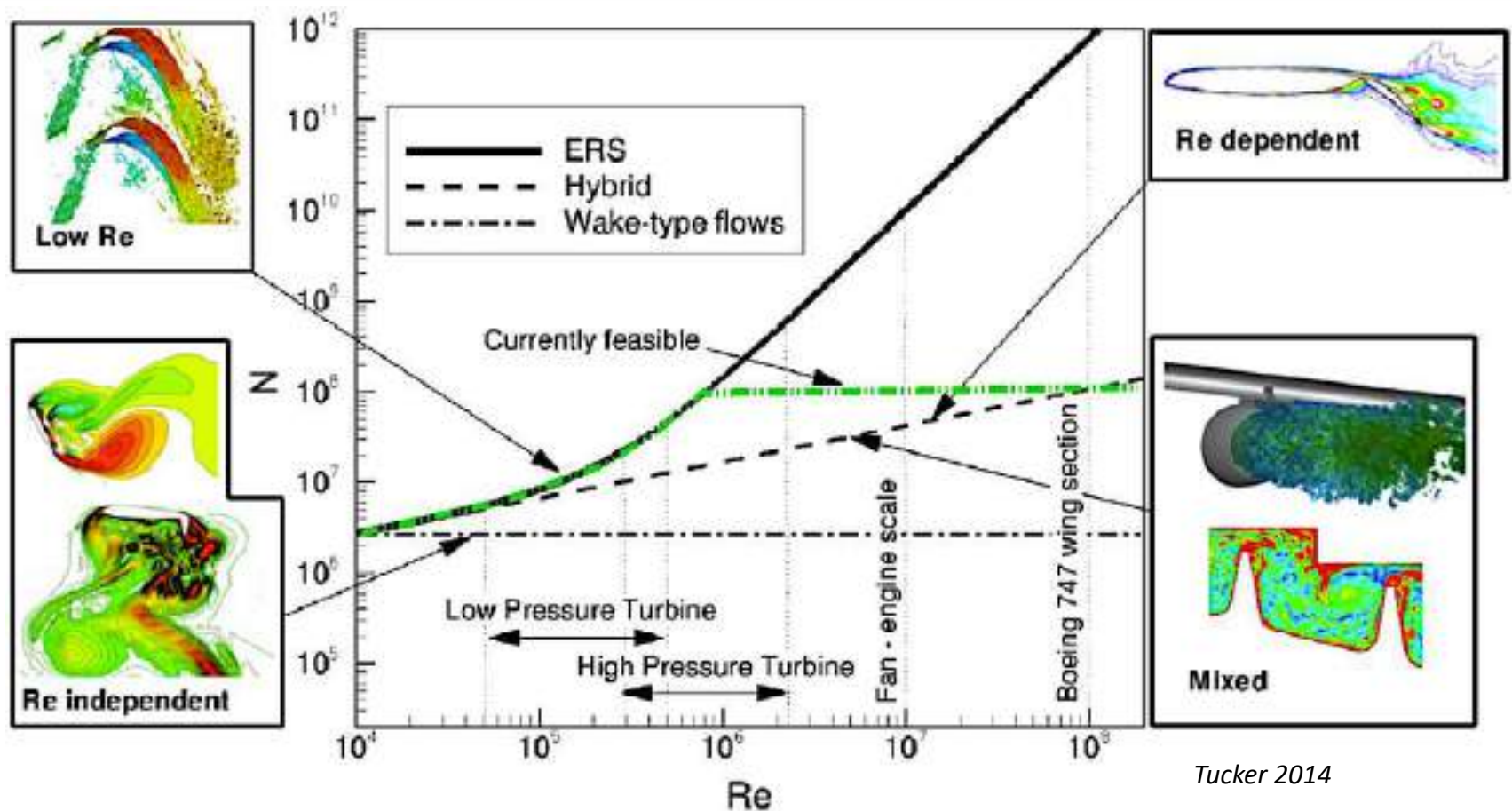
Aeroacoustic of an installed engine



Aerodynamics



Wall-modeling and real applications



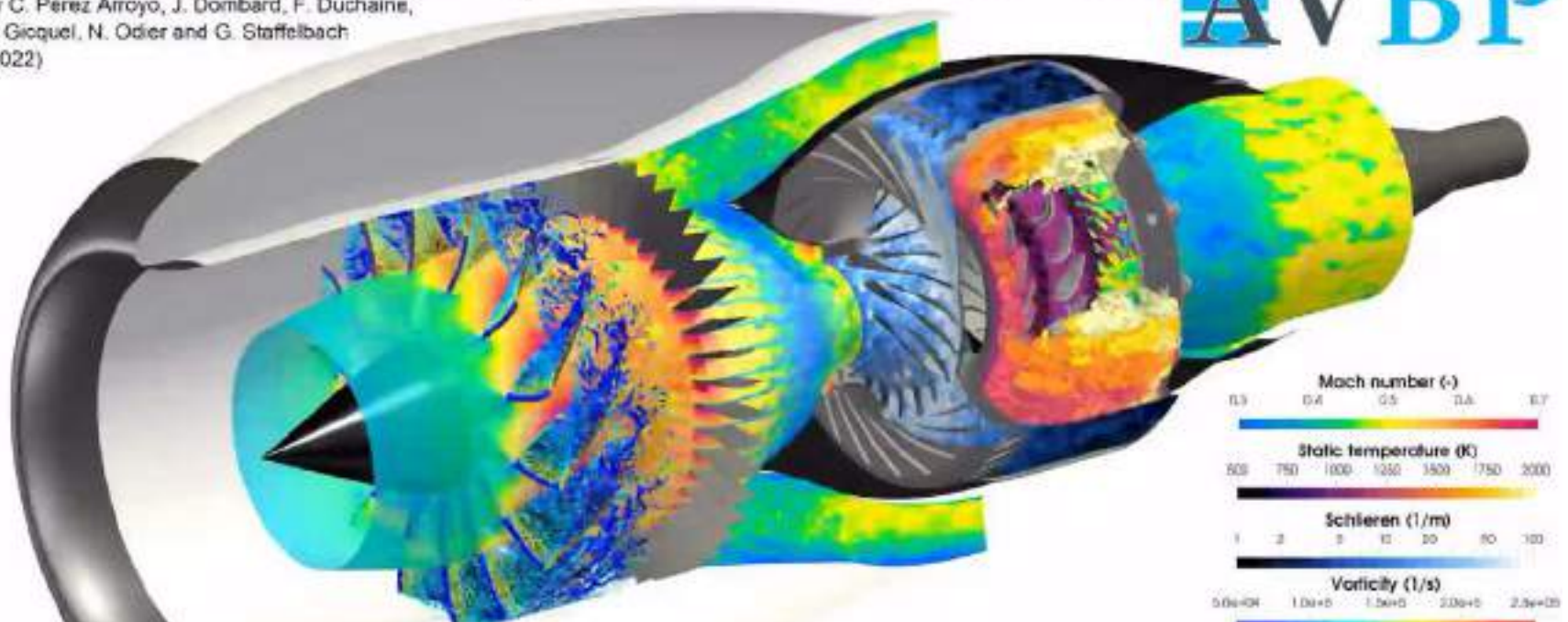
- Eddy-resolved simulation forbids many real applications
- Hybrids / wall-modeled LES are currently computationally affordable

Real application

DGEN-380 engine Large Eddy Simulation at take-off conditions

by C. Pérez Arroyo, J. Dombard, F. Duchaine,
L. Gioquel, N. Odier and G. Staffelbach
(2022)

AVBP



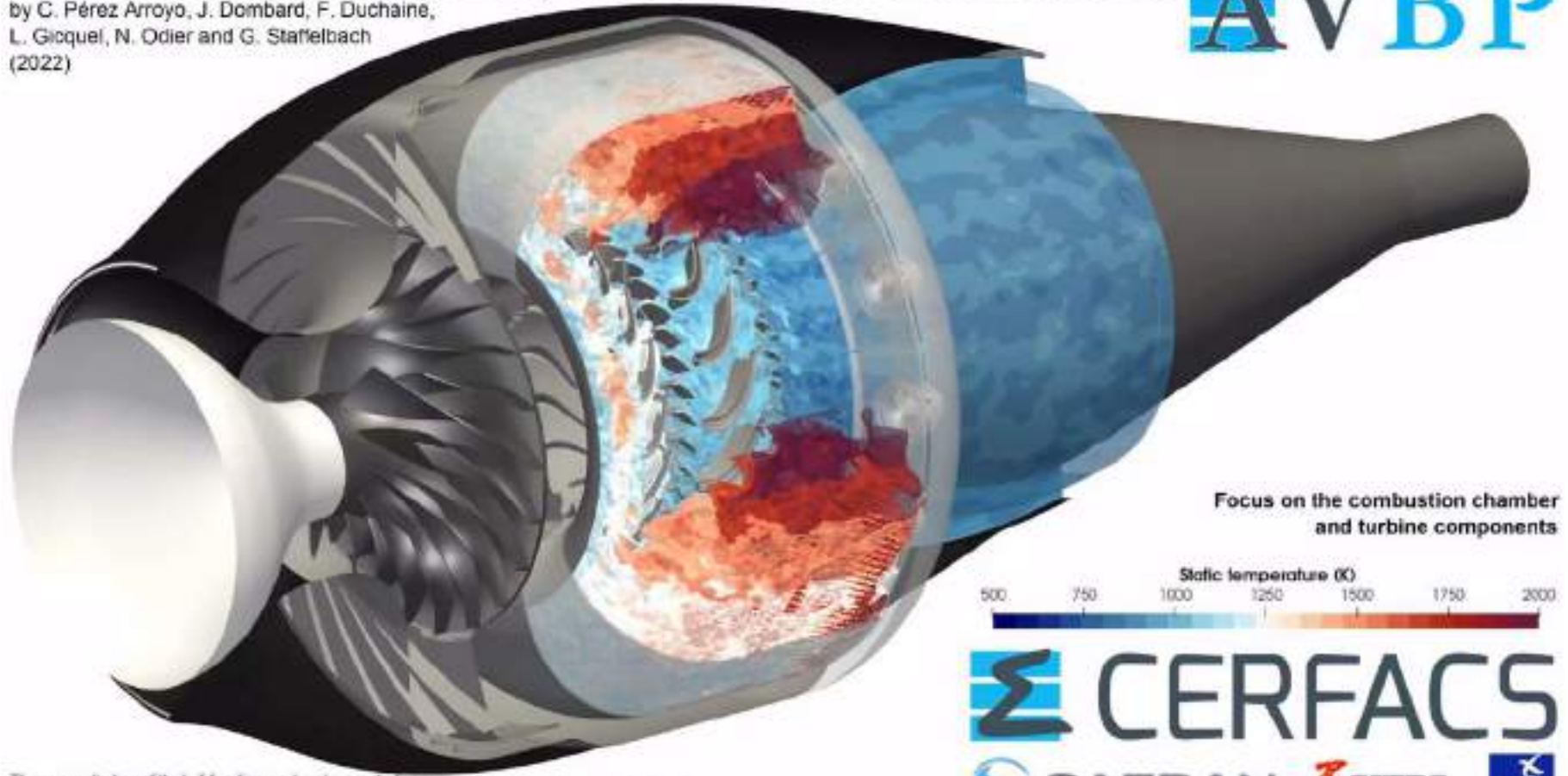
These results benefited of funding or developments from:
project ATOM (DGAC/SafranTech No 2018-39), PRACE (20th Call Project Access FULLEST),
EXCELLERAT (H2020 823601), EPEEC (H2020 801051) and GENCI (A0122A06074)

 CERFACS
 SAFRAN  AIRBUS  dgac

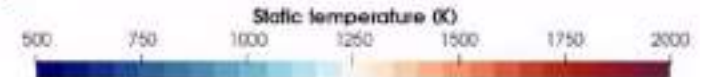
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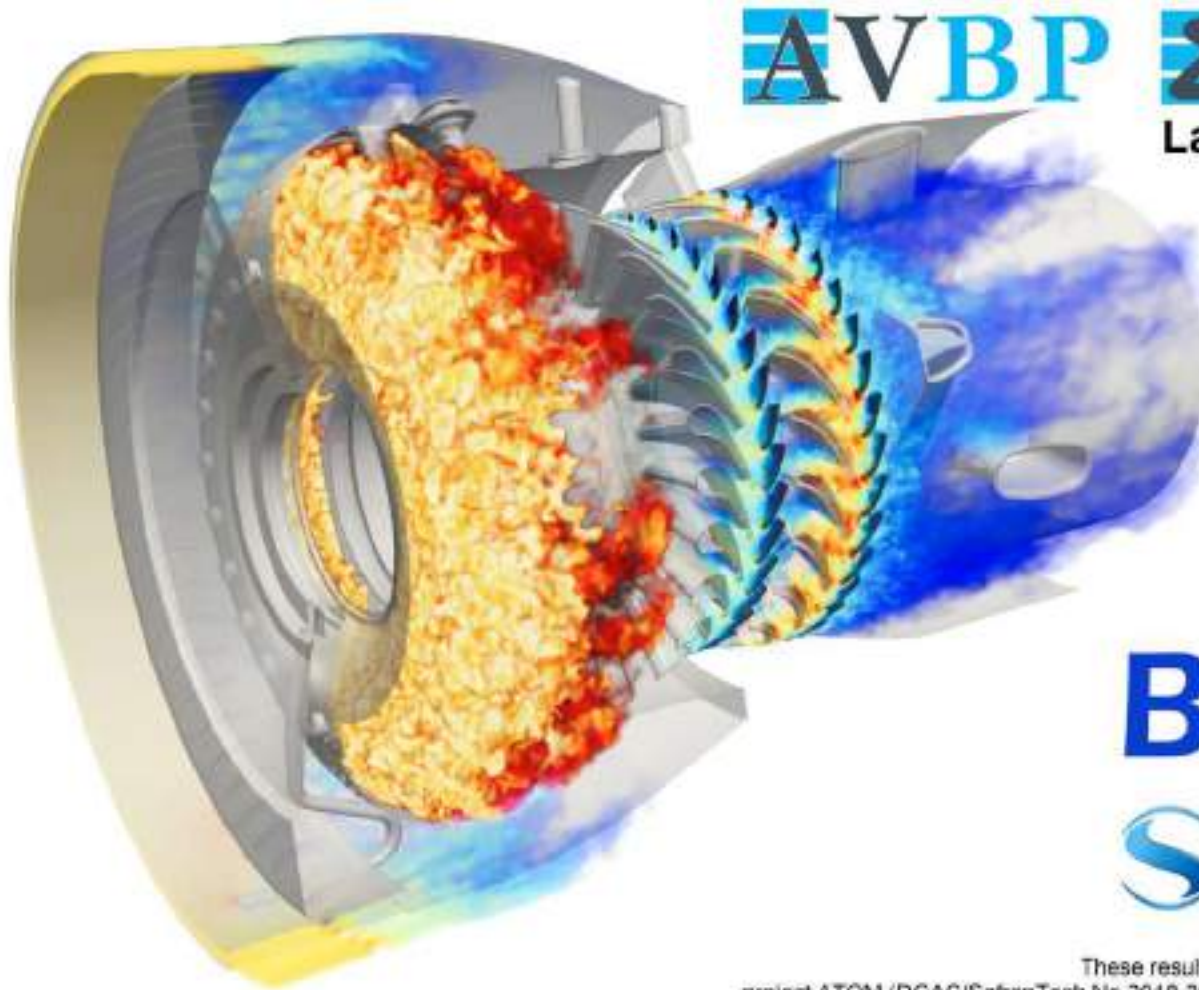


Focus on the combustion chamber
and turbine components



These results benefited of funding or developments from:
project ATOM (DGAC/SafranTech No 2018-39), PRACE (20th Call Project Access FULLST),
EXCELLERAT (H2020 823891), EPEEC (H2020 801051) and GENCI (A0122A08074).

Real application



AVBP

CERFACS

Large Eddy Simulation of the
BEARCAT test bench

by C. Pérez Arroyo et al. (2023)

Static temperature (K)

Mach number (-)

BEARCAT

SAFRAN dgac

These results benefitted of funding, developments or ressources from
project ATOM (DGAC/SafranTech No 2018-39) and GENCI-CINES Grand Challenge (2023-GDA2305).



A few conclusions

Wall-bounded turbulence:

- A **complex physics**: transition to turbulence, streaks, large-scale structures...
- **Self-similar physics**.
- A **universal** velocity profile: the **logarithmic law-of-the-wall**.

- (U)RANS approaches are **not efficient** for complex physics predictions.
- **Large-eddy simulation**: a **wall-modeling** is mandatory for real applications.

- Either **analytical model** (based on log-law), **numerical model** (TBLE) to deal with turbulent boundary layer.
- Other **hybrid RANS/LES** models: Detached Eddy Simulation
- An accurate wall model / SGS model coupling is still a research topic...



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- Log-layer mismatch and applications

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- Synthetic methods (Fourier / POD)
- Precursor method
- Wall-bounded turbulent injection

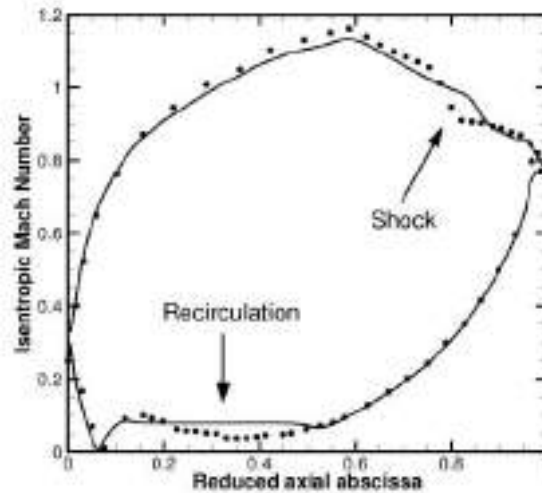


Context

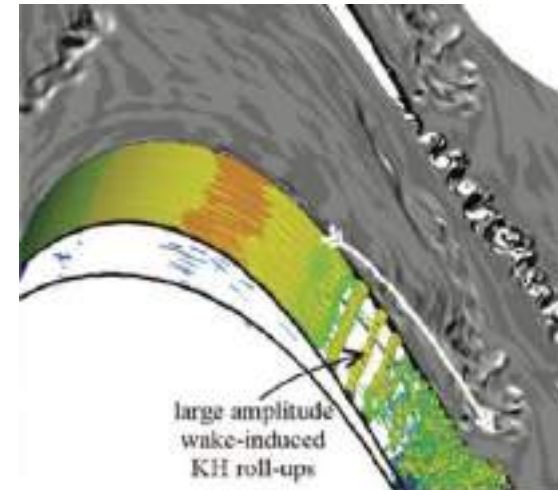
Why do we care about turbulence injection in LES ?



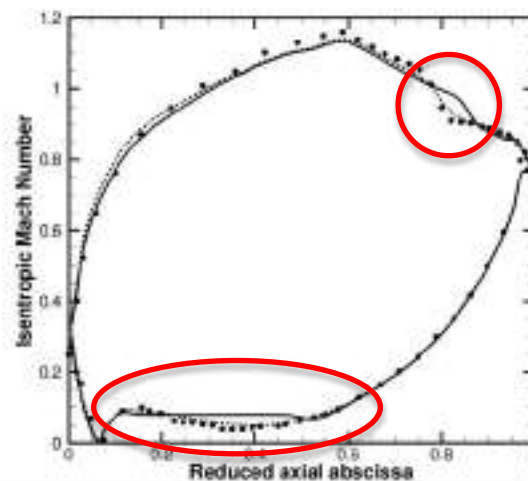
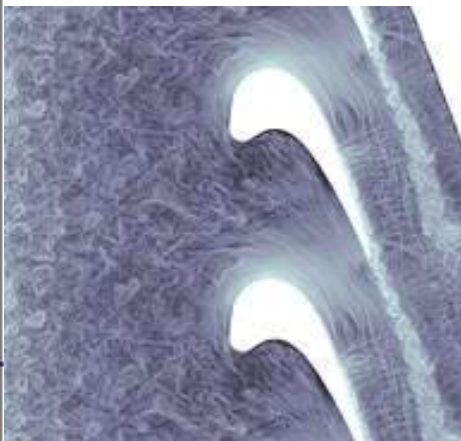
Harnieh et al., 2017



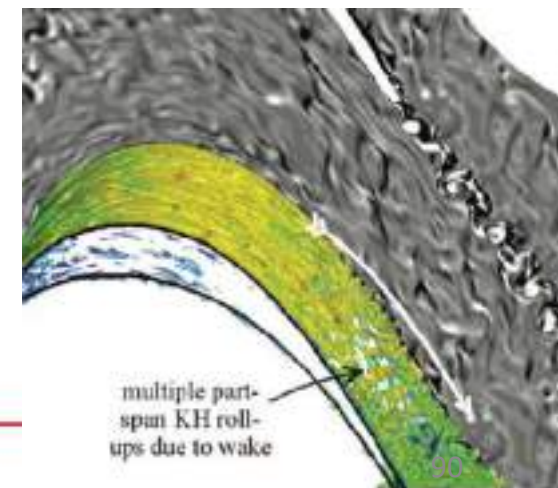
Laminar
inlet



Cui et al. 2015

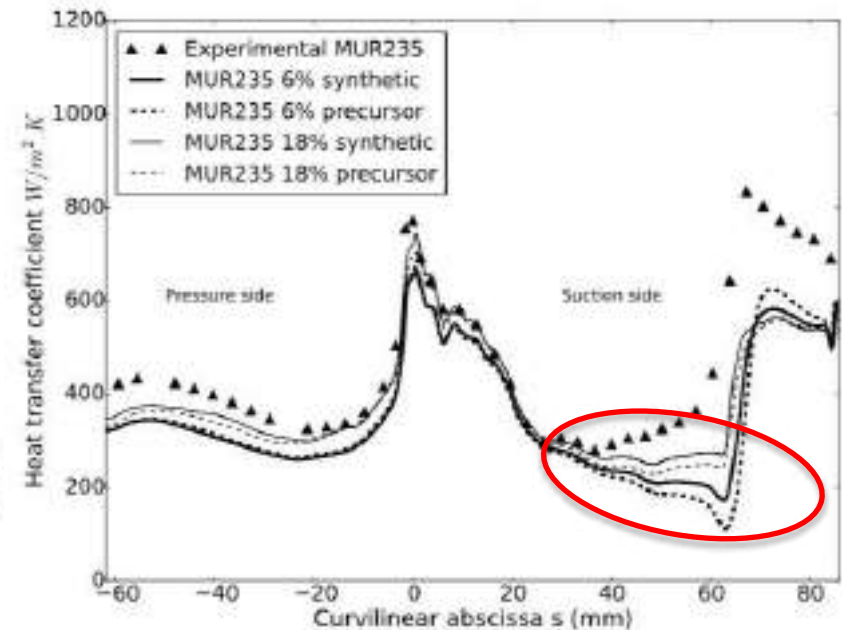
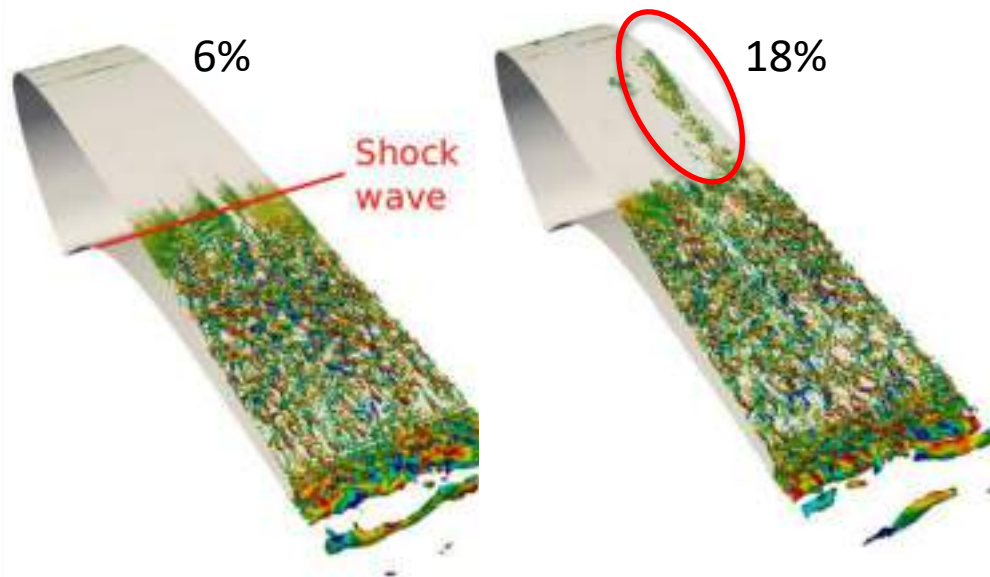


Turbulent
inlet





Why do we care about turbulence injection in LES ?



Inlet turbulence level may modify the boundary layer transition process:

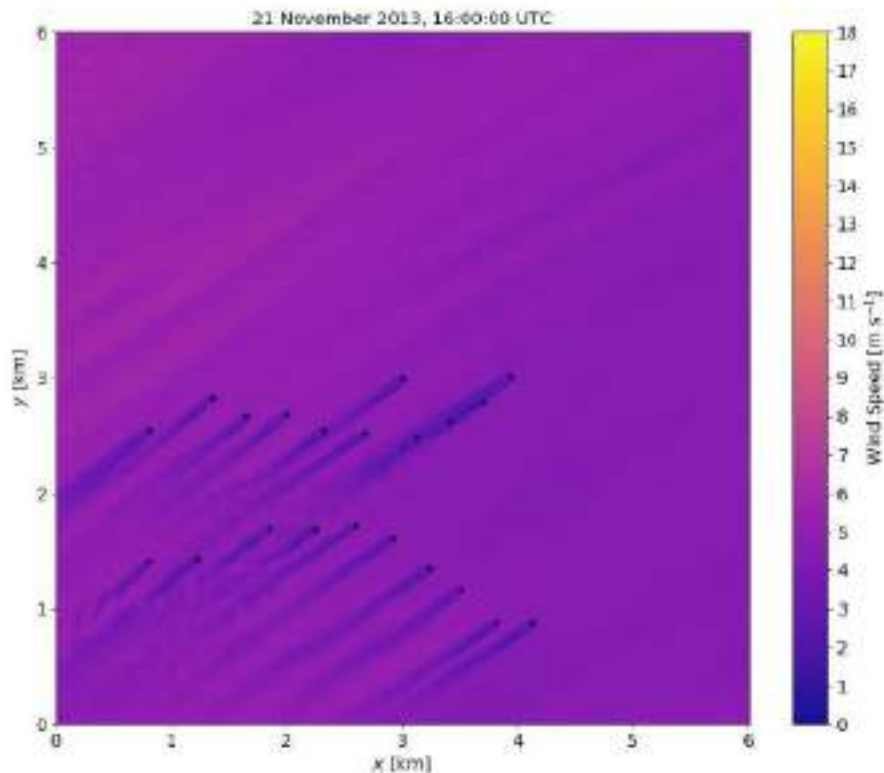
- ⇒ Significant influence on the **average pressure distribution**
- ⇒ Significant impact on **resulting losses**
- ⇒ Significant impact on **heat transfer**



Context

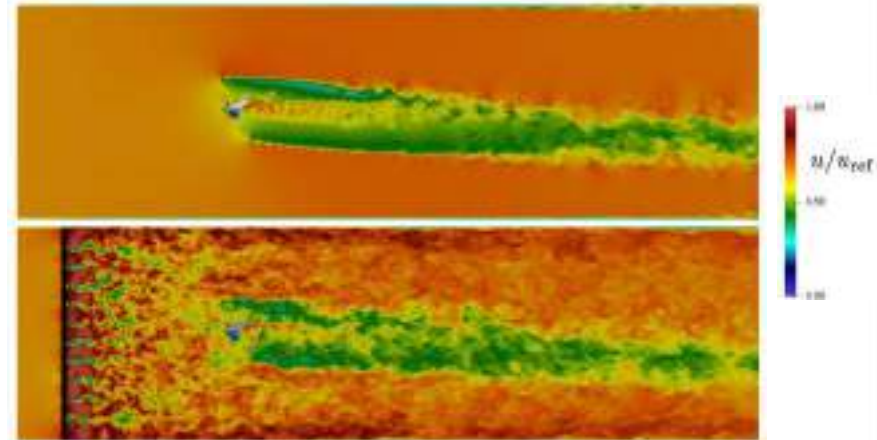
Offshore wind farm

Radar observation

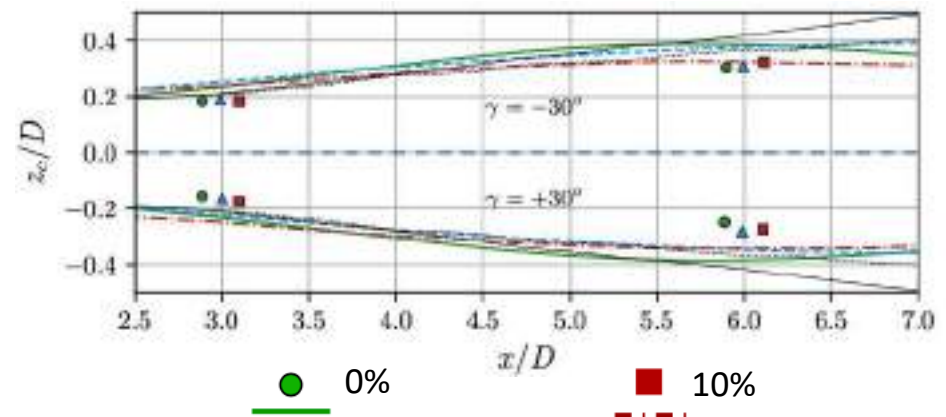


Arthur et al., 2020

Standalone wind turbine



Houtin-Mongrolle et al., 2020



Turbulence modifies wake development



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- Wall modeling: The “wall-law”, TBLE
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- Synthetic methods (Fourier / POD)
- Precursor method
- Wall-bounded turbulent injection

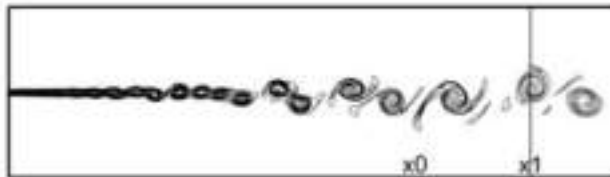


Turbulence injection

Basic principle: Generation of instantaneous realizations statistically equivalent to the freestream flow.

$$\mathbf{u}(\mathbf{x}_0, t) = U_0(x_0) + \mathbf{u}'(x_0, t)$$

???



Reference simulation

Imposed $\mathbf{u}'(x_0, t)$:

Exact solution

White noise with same single point statistics as in ref.

White noise + same two-points temporal statistics

White noise + same two-points spatial statistics

Reconstruction POD

White noise:

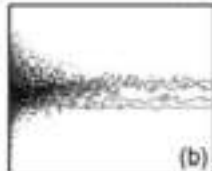
- **Lacks** spatial and temporal **coherence** of turbulence

=> **Other approaches are needed**

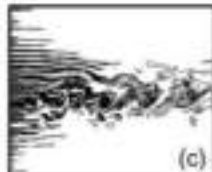
Druault et al., 2004



(a)



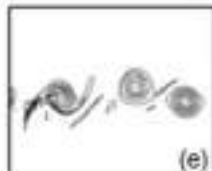
(b)



(c)



(d)



(e)



Synthetic methods: Fourier techniques

Objective: Build velocity fluctuations that behave similarly to turbulent fluctuations.

Kraichnan (1970): Fluctuations can be seen as a **sum of random Fourier modes**:

$$\underline{u}'(\underline{r}, t) = \sum_{n=1}^N \hat{\underline{u}}^n(\underline{k}^n) e^{(j\underline{k}^n \cdot \underline{r} + j\omega^n t)}$$

$$\hat{\underline{u}}^n \cdot \underline{k}^n = 0 \quad \forall n \quad (\text{continuity equation})$$

$$\hat{\underline{u}}^n(\underline{k}^n) = \hat{v}^n(\underline{k}^n) + j\hat{w}^n(\underline{k}^n)$$

Recast as:

$$\underline{u}'(\underline{r}, t) = \sum_{n=1}^N [\hat{v}^n(\underline{k}^n) \cos(\underline{k}^n \cdot \underline{r} + \omega^n t) + \hat{w}^n(\underline{k}^n) \sin(\underline{k}^n \cdot \underline{r} + \omega^n t)]$$

Wave vector

Pulsation

Taken from isotropic **Gaussian distributions** so shaped that **E(k)** is reached in the limit $N \rightarrow \infty$

Velocity fluctuations are finally **added to the mean flow** imposed at the inlet (“Frozen turbulence hypothesis”, Taylor 1938)

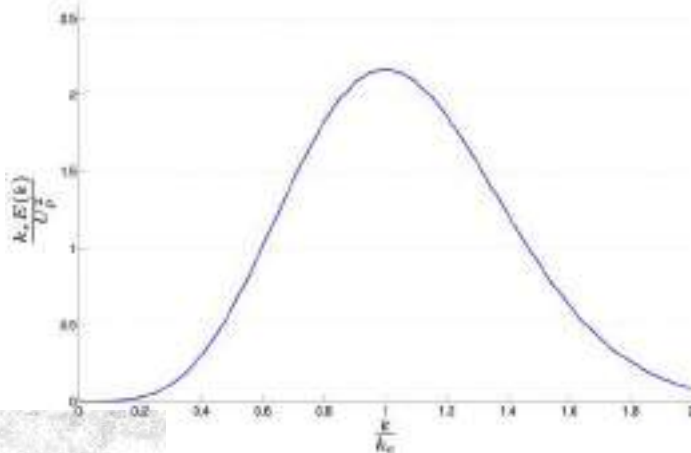
Synthetic methods: Fourier techniques

Passot-Pouquet

$$E(k) = A \left(\frac{k}{k_e} \right)^4 \exp \left(-2 \left(\frac{k}{k_e} \right)^2 \right)$$

with $A = \frac{16U_p^2}{k_e} \sqrt{\frac{2}{\pi}}$

Integration gives : $k \equiv \frac{1}{2} \overline{u'_i u'_i} = \frac{3}{2} U_p^2$

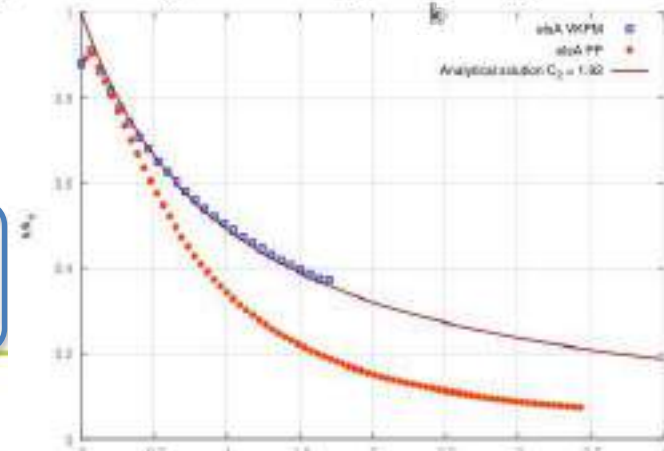
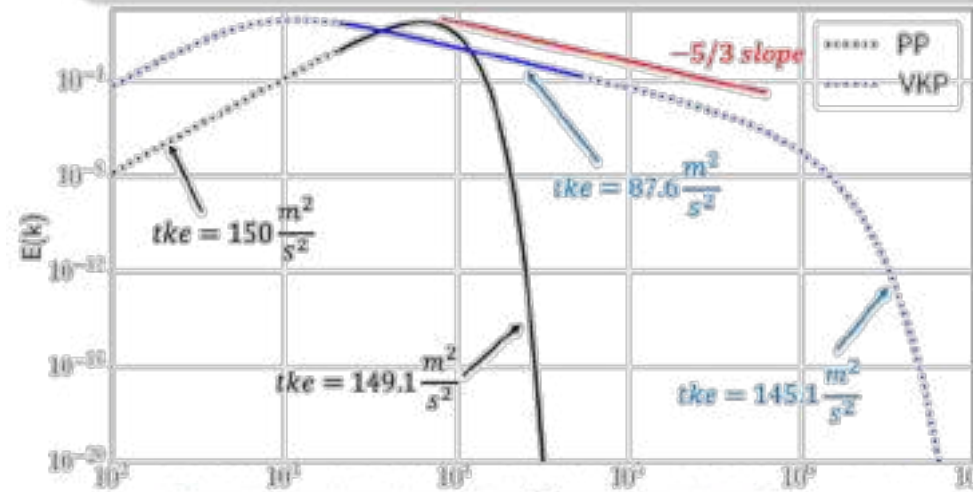


Turbulence decay in a turbulent channel

Spectra example:

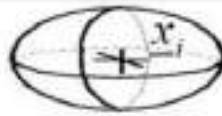
Von Karman-Pao

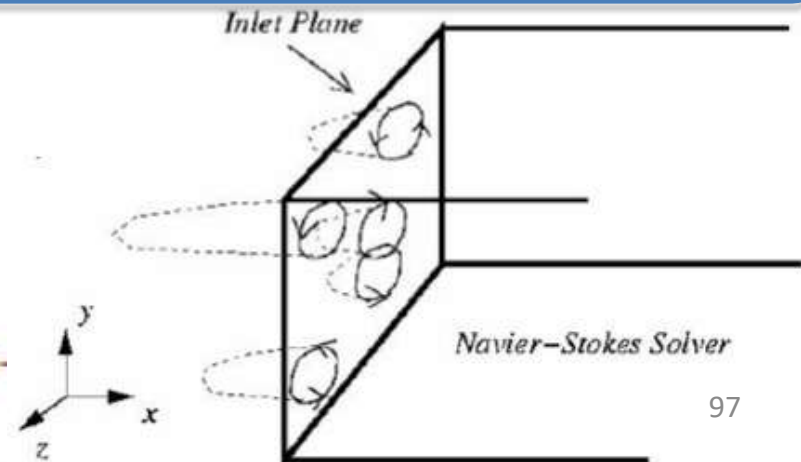
$$E(k) = \alpha \frac{u'^2}{k_e} \frac{(k/k_e)^4}{[1 + (k/k_e)^2]^{17/6}} \exp \left[-2 \left(\frac{k}{k_{Kol}} \right)^2 \right]$$



Synthetic Eddy Method

(Jarrin et al. 2006, 2009)

- Turbulent flow is a **superposition of coherent eddies** 
- Each eddy is described by a **shape function** $f_\sigma(x)$, on compact support $[-\sigma, \sigma]$
 $[-r_x; r_x] \times [-r_y; r_y] \times [-r_z; r_z]$
- Each eddy has a **random position** (y_i, z_i) on the inlet plane.
- Each eddy is convected through the inlet plane until it is not active anymore ($r_x < x_i$)
- Then, a new one is regenerated at $x_i = -r_x$



Synthetic Eddy Method

Contribution of the turbulent spot i to the velocity field is

$$u^{(i)}(x) = \varepsilon_i f_\sigma(x - x_i)$$

Gaussian

Random step (+1 or -1)

Contribution of N eddies:

$$u(x) = \frac{1}{\sqrt{N}} \sum_{i=1}^N \varepsilon_i f_\sigma(x - x_i)$$

Unsteady velocity field:

$$u'_j(\underline{x}, t) = \frac{1}{\sqrt{N}} \sum_{i=1}^N \varepsilon_{ij} f_j(\underline{x} - \underline{x}_i(t))$$

Final velocity field:

$$u_i = \bar{u}_i + a_{ij} u'_j$$

\bar{u}_i Mean velocity field

a_{ij} Deduced from prescribed Reynolds Stress Tensor R_{ij}

Mean velocity and R_{ij} must be known in advance (RANS or experiment)

$$\begin{pmatrix} \sqrt{R_{11}} & 0 & 0 \\ R_{21}/a_{11} & \sqrt{R_{22} - a_{21}^2} & 0 \\ R_{31}/a_{11} & (R_{32} - a_{21}a_{31})/a_{22} & \sqrt{R_{33} - a_{31}^2 - a_{32}^2} \end{pmatrix}$$

(Cholesky decomposition of Reynolds Stress Tensor)



POD method

Expe / Numerics

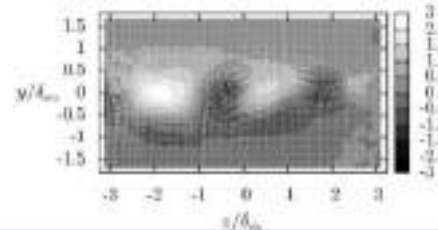
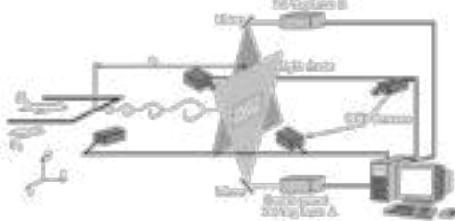
Proper Orthogonal Decomposition:

Decomposes an ensemble of unsteady snapshots into **spatial** and **temporal** eigenvectors:

$$\tilde{u}(X, t) = \sum_n a_n(t) \Phi^{(n)}(X)$$

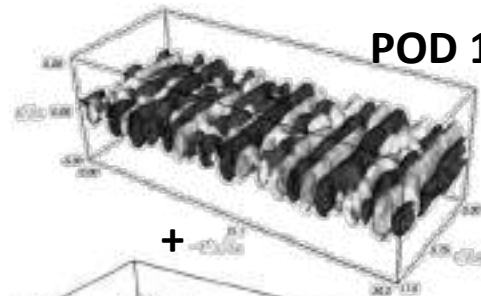
=> Allows to **reconstruct the most energetic structures** from reference

Perret et al. 2008: POD from experiment + synthetic Fourier method



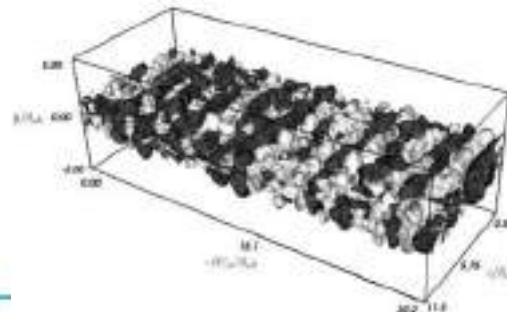
POD mode from PIV

POD 12 modes

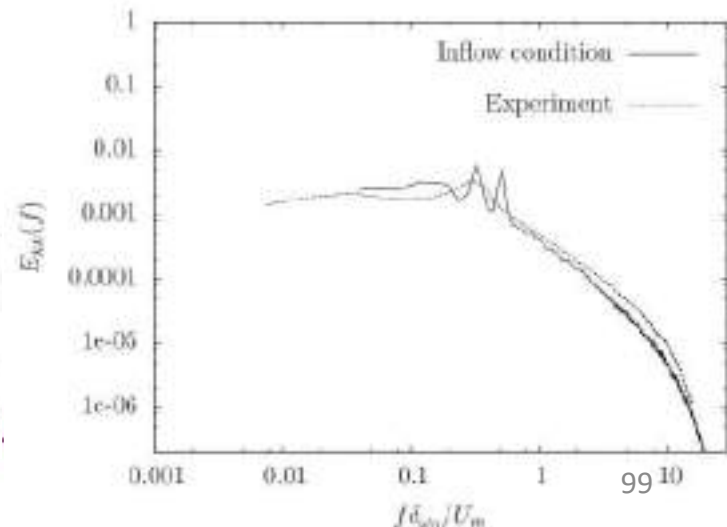


+

=



Fourier

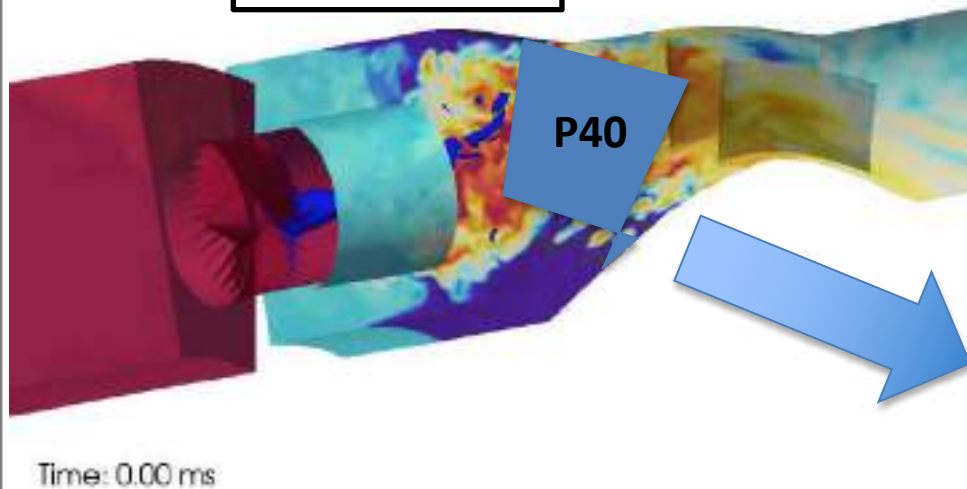




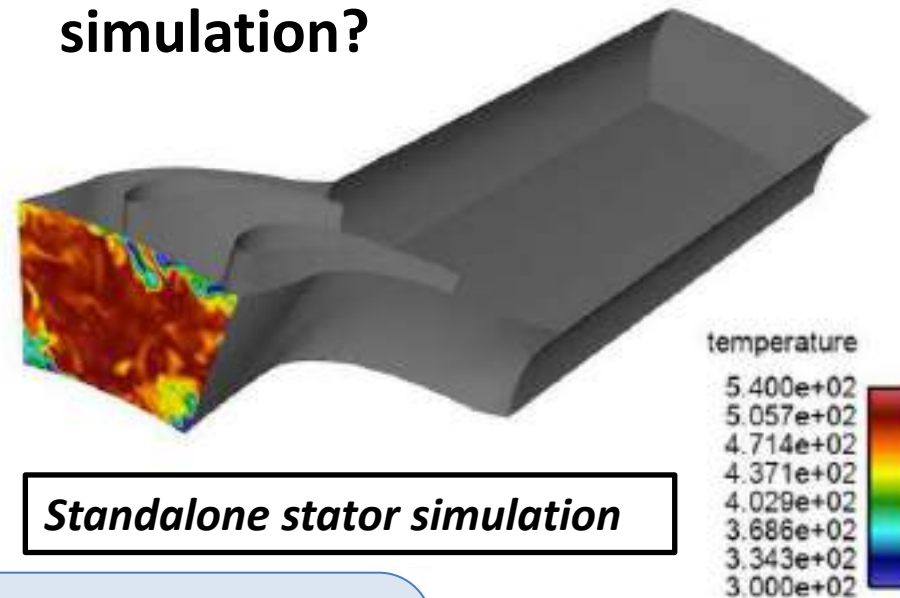
POD method

Numeric / Numeric

Integrated LES



What to impose on isolated simulation?



Standalone stator simulation

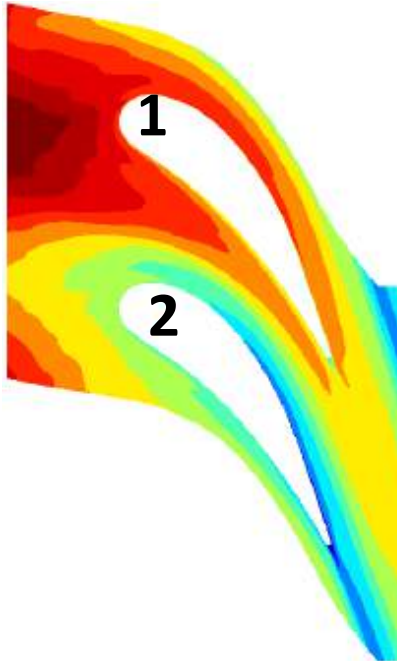
- Extract P40 fully unsteady flow fields
- Recast the data into POD modes.
- Reconstruct several inflow conditions:
 - Mean 2D profile
 - Mean 2D profile + POD modes corresponding to the PVC
 - Fully unsteady flow fields



POD method

Numeric / Numeric

**Integrated
(reference)**



Constant 2D map



2D + PVC modes



**Fully unsteady
(all modes)**



Ttotal: 430 445 460 475 490

- Reference and Full modes simulation are very similar
- PVC has a strong impact on flow field



Synthetic methods

Pros:

- Can be used as a standalone boundary condition in the main computational domain
- Relatively easy to implement
- Affordable computational cost

Cons:

- Injected turbulence **doesn't respect NS Equations.**
- An **adaptation distance** is mandatory to reach the target turbulence characteristics.



Large eddy simulations: Practical issues

LES: A brief reminder

NS equation and turbulence

LES, filtering and models

Numerics, errors and LES

Implicit LES

Wall treatment

Wall-bounded turbulence

The logarithmic law-of-the-wall

Wall-modeled LES: analytical, TBLE

Detached-Eddy Simulations

Log-layer mismatch and applications

Turbulence injection

Synthetic methods (Fourier / POD)

Precursor method

Wall-bounded turbulent injection

Precursor simulation

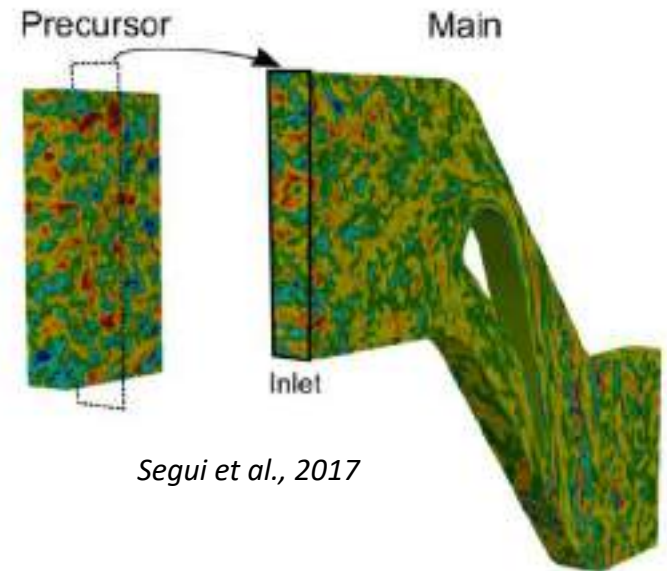
Turbulence is computed in a **separated domain**, then imposed to the main domain inlet

A **precursor** periodic **HIT** simulation is performed.

Taylor hypothesis (1938): “Frozen turbulence”

- Turbulence of the advected field and turbulence in the fixed HIT are comparable

- ⇒ The extraction plane is advected at the main domain inlet bulk velocity.
- ⇒ Extracted turbulence imposed through the NSCBC condition.



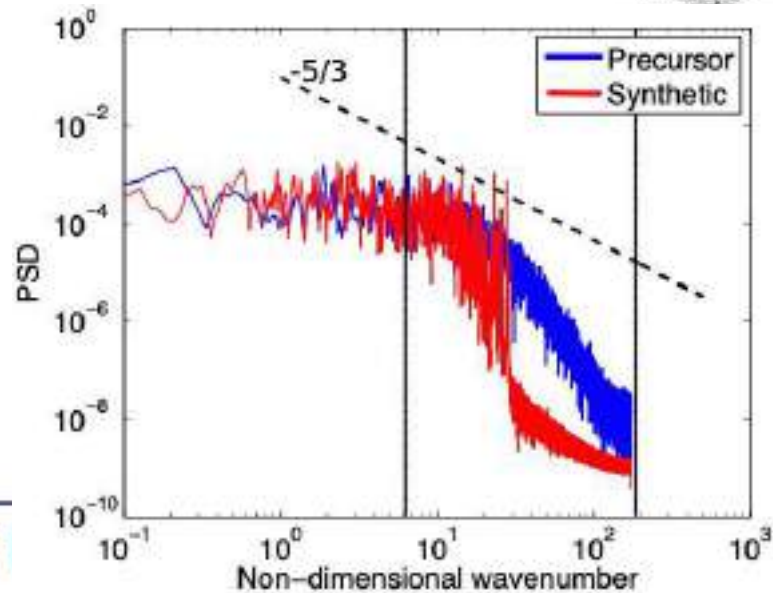
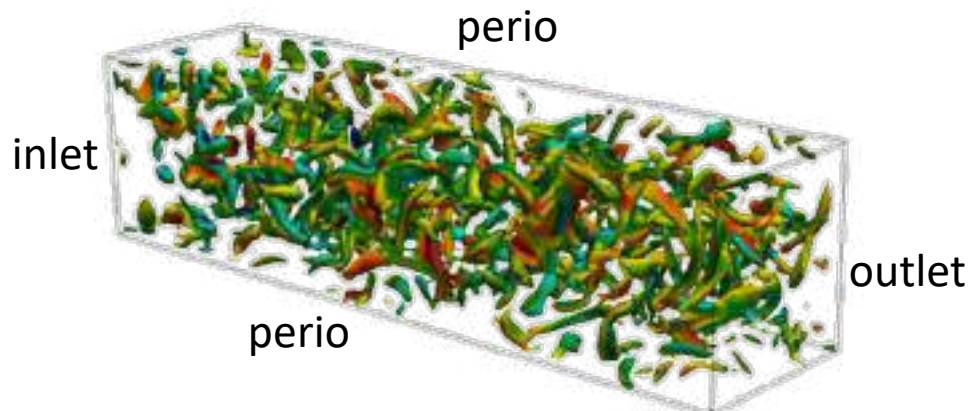
Segui et al., 2017



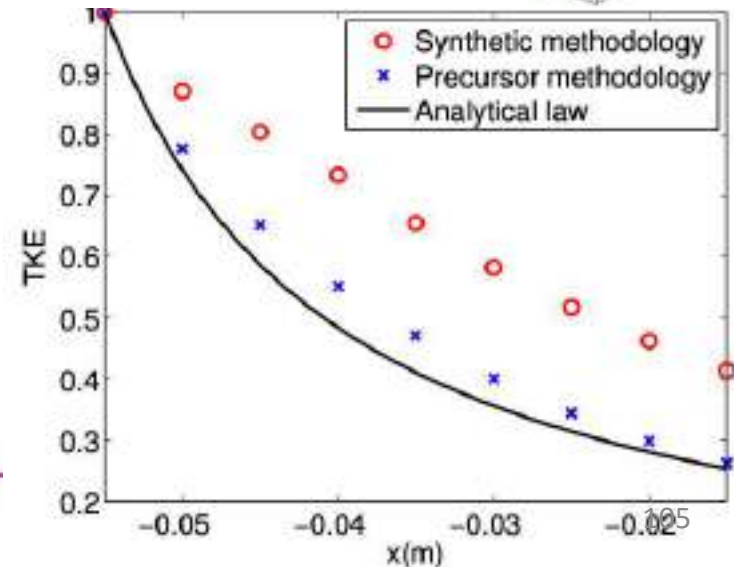
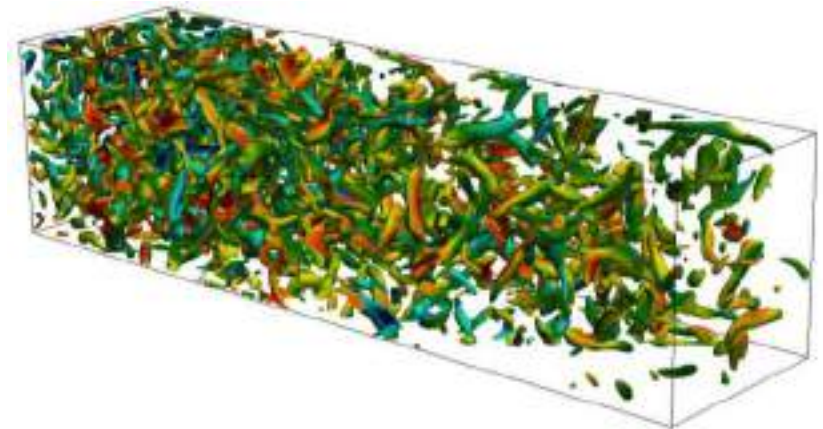
Precursor simulation

Assessment: Turbulent channel

Synthetic Fourier Method (Kraichnan)



Precursor simulation





Precursor simulation

Pros:

- Almost completely eliminates the errors encountered with synthetic methods
- Provides excellent results.

Cons:

- Implementation is not straightforward
- One-way coupling: no information from main simulation to precursor (e.g. acoustic wave)
- Computational cost



Large eddy simulations: Practical issues

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Synthetic methods (Fourier / POD)

Precursor method

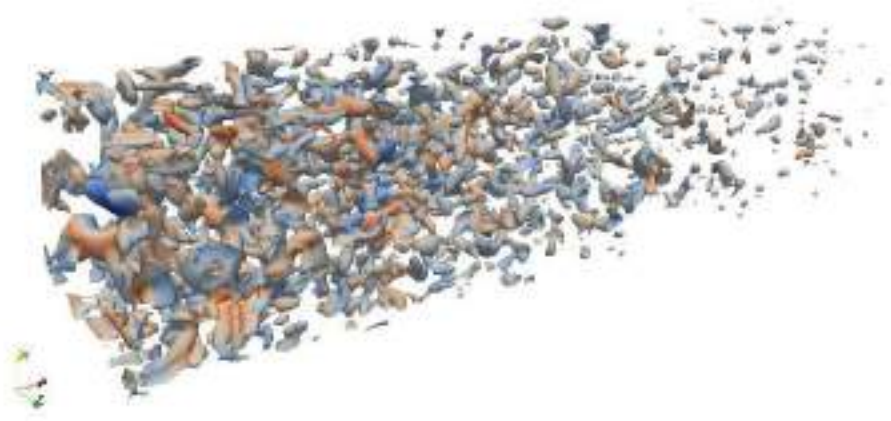
Wall-bounded turbulent injection



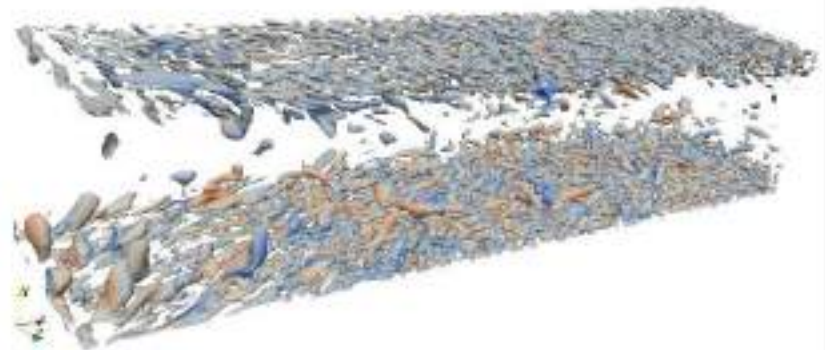
Wall-bounded turbulence injection

Turbulence injection:

Homogeneous, isotropic



Non-homogeneous,
anisotropic

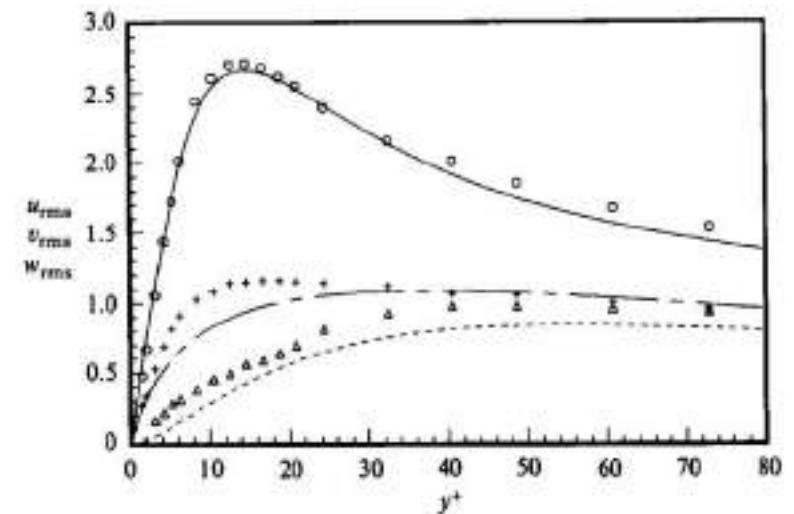
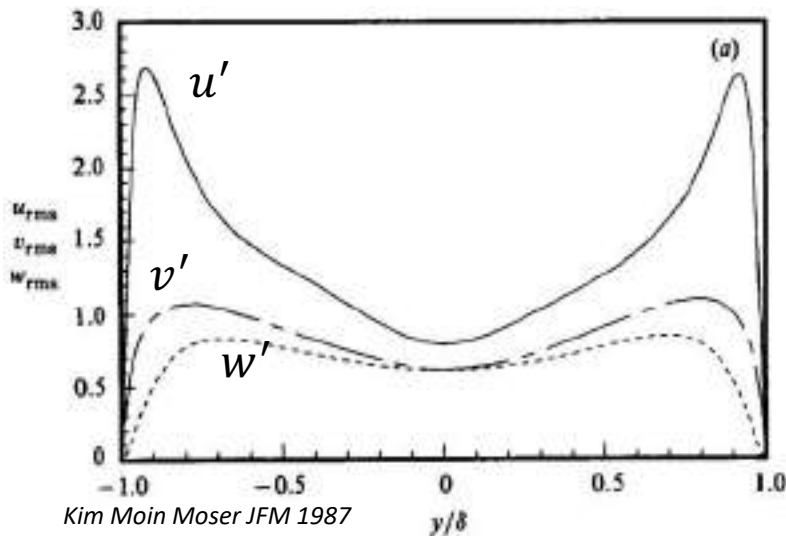
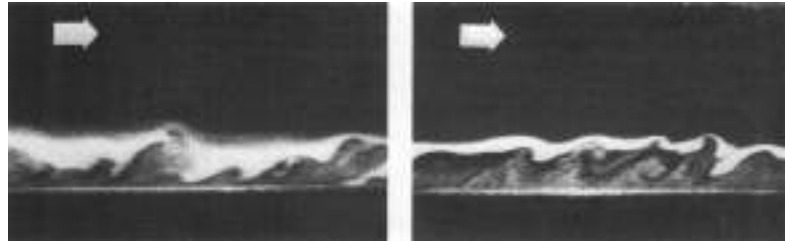


Wall-Bounded flows



Reminder: Statistics in a BL

Head Bandyopadhyay JFM 1981



Non-uniformity of statistics (U_{rms} , V_{rms} , W_{rms}) in a turbulent boundary layer.

=> Turbulent BL requires dedicated turbulence injection !

Smirnov /Celik transformation

For an anisotropic velocity correlation tensor r_{ij} :

=> Let find a **transformation tensor** a_{ij} which **diagonalizes** r_{ij} : $r_{ij} \equiv \overline{u'_i u'_j}$

$$a_{mi} a_{nj} r_{ij} = \delta_{mn} c_n^2$$

$$a_{ik} a_{kj} = \delta_{ij}$$

$$a_{ij} = \begin{pmatrix} \sqrt{R_{11}} & 0 & 0 \\ R_{21}/a_{11} & \sqrt{R_{22} - a_{21}^2} & 0 \\ R_{31}/a_{11} & (R_{32} - a_{21}a_{31})/a_{22} & \sqrt{R_{33} - a_{31}^2 - a_{32}^2} \end{pmatrix}$$

c_n corresponds to the fluctuations (u', v', w') to inject, to satisfy with r_{ij}

$$c_n = \{c_1, c_2, c_3\} \longrightarrow (u', v', w')$$

Smirnov Methodology:

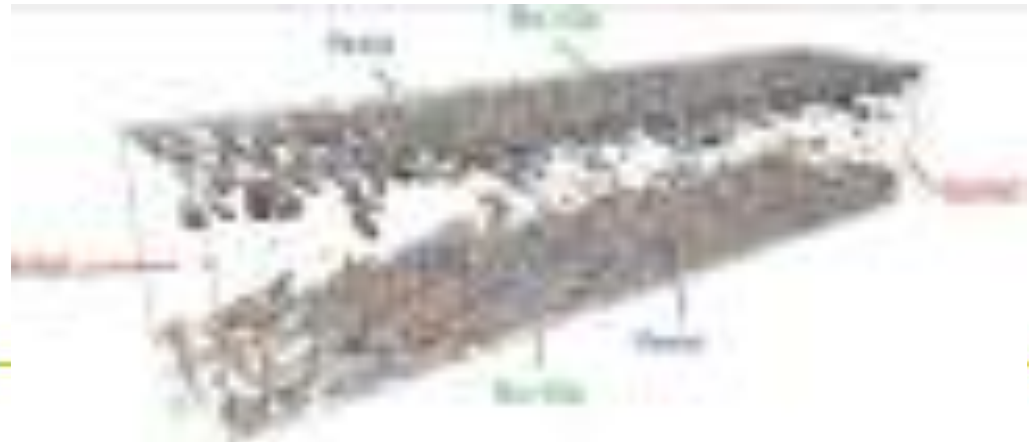
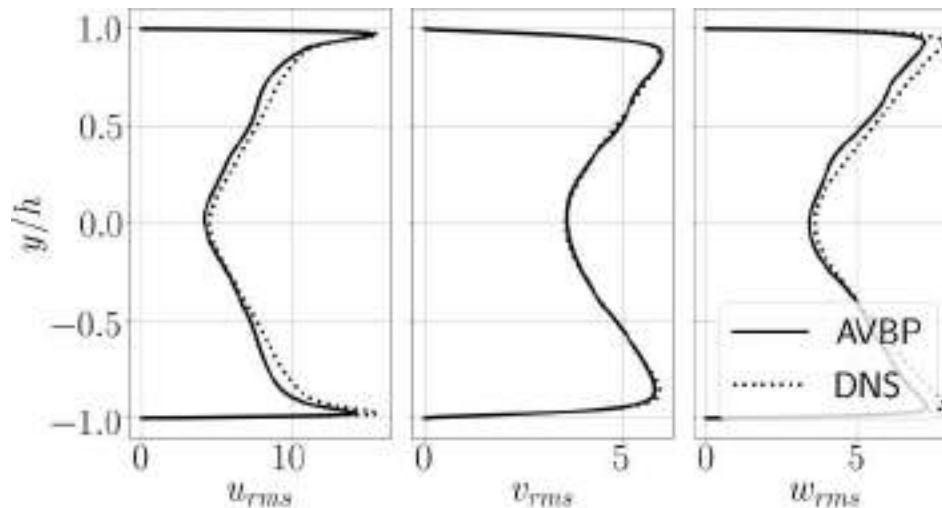
- Generate an **isotropic** fluctuation through **Kraichnan** method => $v'_i(\vec{x}, t)$
- Apply **scaling** and **orthogonal transformation** to this isotropic flow fields

$$w_i = c_{(i)} v_{(i)}$$

$$u_i = a_{ik} w_k$$

Synthetic method for wall-bounded flows

Application: Imposition of r_{ij} extracted from a DNS (Hoyas / Jimenez 2008.)



Synthetic method for wall-bounded flows

Yao 2002–Sandham 2003

Fluctuations in the **inner** and **outer** part of the BL have **different characteristic scales**

=> Specific disturbances are introduced in each part.

Inner fluctuations: Streaks, with energy max at $y_{p,j}^+$

$$\hat{u}^{\text{inner}} = c_{1,0} y^+ e^{-y^+/y_{p,0}^+} \sin(\omega_0 t) \cos(\beta_0 z + \phi_0)$$

Outer fluctuations:

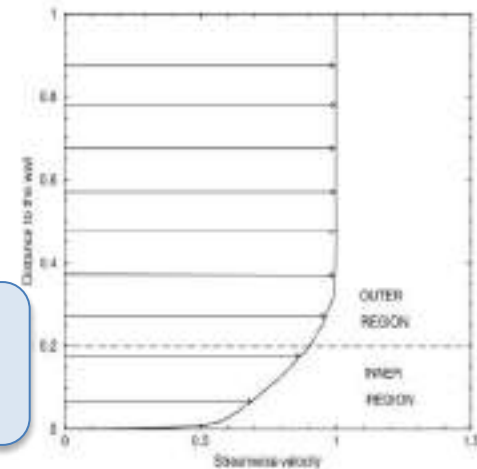
$$\hat{u}^{\text{outer}} = \sum_{j=1}^3 c_{1,j} y / y_{p,j} e^{-y/y_{p,j}} \sin(\omega_j t) \cos(\beta_j z + \phi_j)$$

ϕ_j Phase shift

ω_j Forcing frequency

β_j Spanwise wave number

To be adapted depending on the boundary layer





Wall-bounded flows

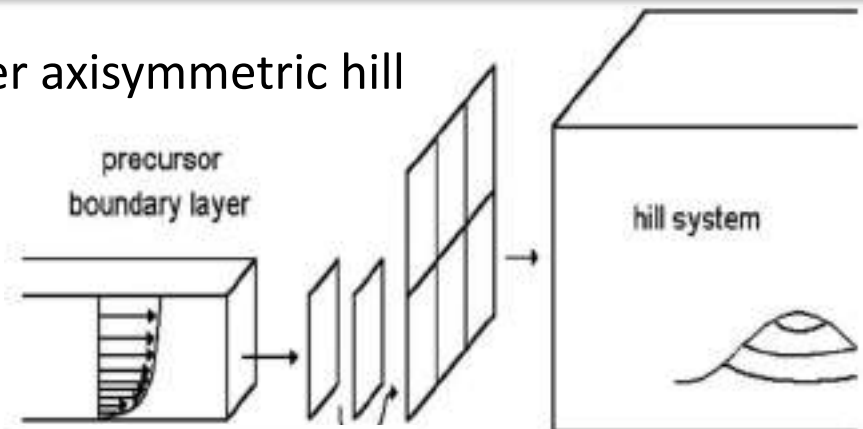
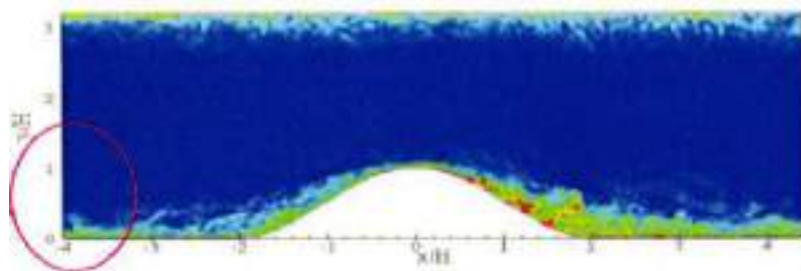
Precursor simulation

Issue: How can we create **representative turbulence** to impose a **boundary layer** of given size δ ?

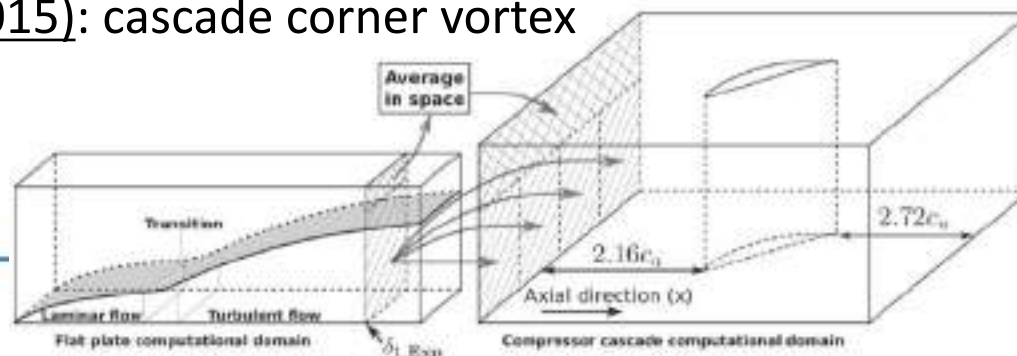
Precursor simulation:

Simulation of a turbulent boundary layer over a flat plate, until the desired BL thickness.

Castagna et al., (2014): turbulent flow over axisymmetric hill



Xie et al. (2015): cascade corner vortex

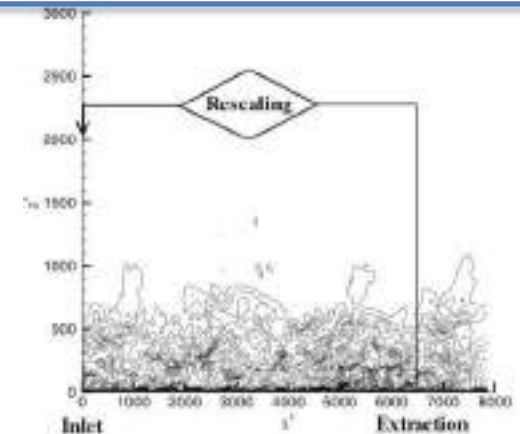




Wall-bounded flows

Recycling – Rescaling method

Recycling method: Lund, 1998



- Information imposed at the inlet based on the information extracted from a plane downstream
- No longer need a precursor simulation

Issue:

- The boundary layer thickness spatially increases...
=> The **flow extracted** downstream must be **rescaled** before being used at the inlet plane.



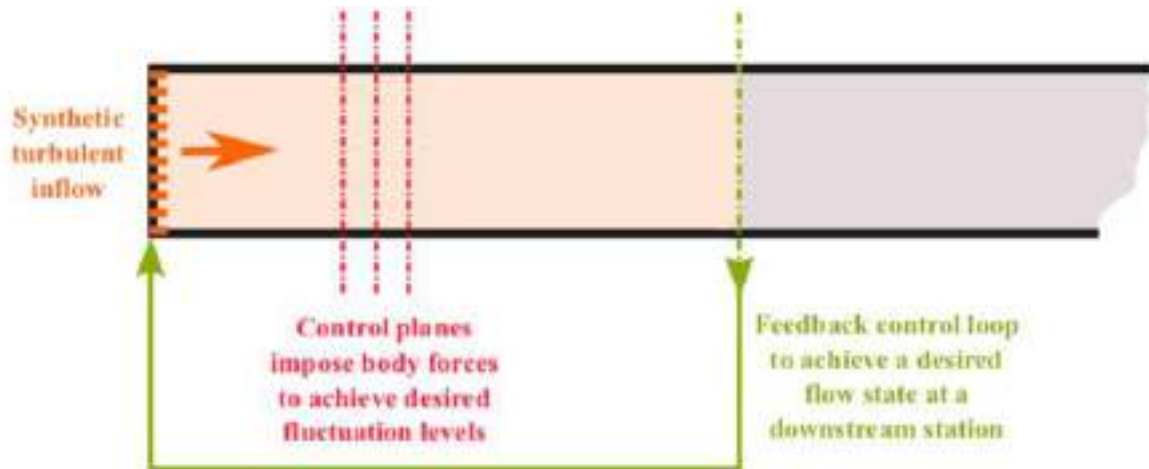
Wall-bounded flows

Recycling – Rescaling method

Efficient, but must be used with care:

- Only valid for fully turbulent self-similar boundary layers
- Implementation / parallelization not straightforward
- Extraction plane must be far enough, to avoid spurious coupling

Suggested improvement (*Spille-Kohoff and Kaltenbach, 2001*):



Active control planes, where the wall-normal velocity fluctuations are amplified or damped to **match a target Reynolds shear stress**.



A few conclusion

- Accounting for turbulence injection is mandatory for real flows.
- Random / **white noise is not accurate** since it does not account for turbulence coherence.
- **Synthetic methods** (Fourier/POD) are much more reliable. However, still lack of physics.
- **Precursor simulations** provide excellent results. However, computational cost significantly increases.
- Specific **care** must be taken for **wall-bounded flows**.



General conclusions

- LES must face “**real-life**” **issues** when dealing with real flows: several **errors** are induced.
 - Numerical scheme must be accurate enough (2nd order minimum).
 - **Numerical / modeling** errors can be highly **coupled**.
- **LES** is efficient for massively **separated industrial flows**, where RANS is not.
 - For attached boundary layers, **modeling is mandatory** to reduce the computational cost.
 - Validity of such models for real flows is still an **open question**...
- **Turbulence injection** is mandatory for numerous flows. There is still work to do for an accurate coupling with NSCBC.
- LES is **still an expert** approach... A use in the industry is currently beginning.