

Estimator-Enhanced Feedback-based Optimization with Applications to Power Systems

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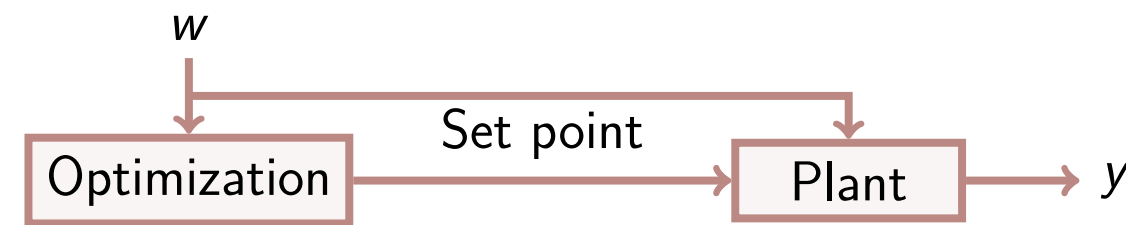
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Background

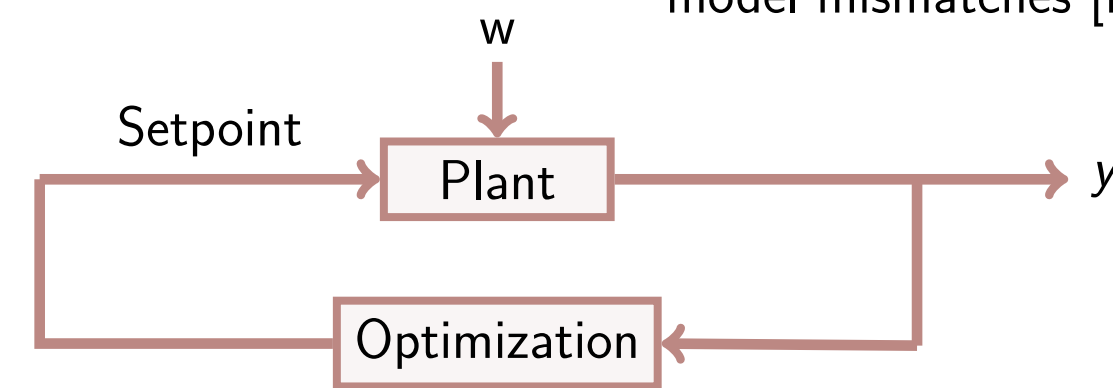
Offline Optimization

- Model-based
- Requires an estimate or measurement of the Disturbance



Feedback-based Optimization (Online Optimization)

- Operates autonomously without external set points
- More robust against uncertainties and model mismatches [Hauswirth '24]



Problem Formulation

Plant Model

- Consider the stable LTI system, w is constant.

$$\begin{aligned}\dot{x} &= Ax + Bu + Ew \\ \dot{w} &= 0 \\ y &= Cx\end{aligned}$$

- Steady-state input-to-output map for fixed u and w is:
- Where $\Pi_u := -CA^{-1}B$ and $\Pi_w := -CA^{-1}E$.

$$\bar{y} = \Pi_u \bar{u} + \Pi_w w$$

Optimization Problem

- Want to drive the output and input of the plant to the solution of the optimization:

$$\text{minimize}_{\bar{y}, \bar{u}} f(\bar{u}) + g(\bar{y})$$

$$\text{subject to } \bar{y} = \Pi_u \bar{u} + \Pi_w w$$

- The optimization can be written:

$$\min_{\bar{u}} f(\bar{u}) + g(\Pi_u \bar{u} + \Pi_w w)$$

- Solve optimization using:

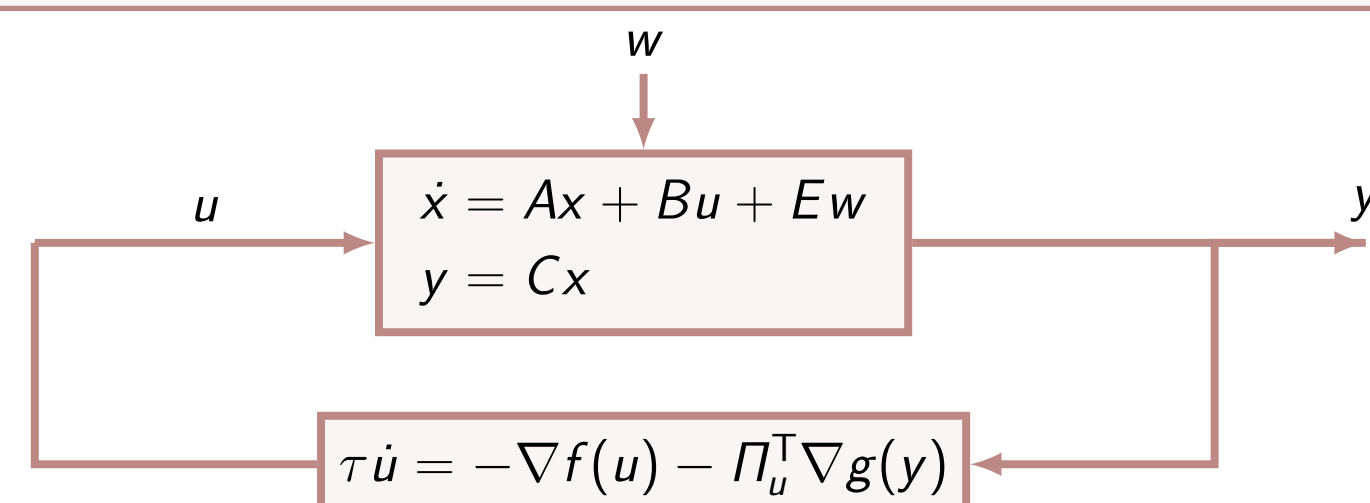
$$\tau \dot{u} = -\nabla f(u) - \Pi_u^T \nabla g(\Pi_u u + \Pi_w w)$$

Closed-loop System

- Replace \bar{y} with the *measured* output value of y

$$\tau \dot{u} = -\nabla f(u) - \Pi_u^T \nabla g(y)$$

Closed-loop is stable for sufficiently slow controller [Menta '18]



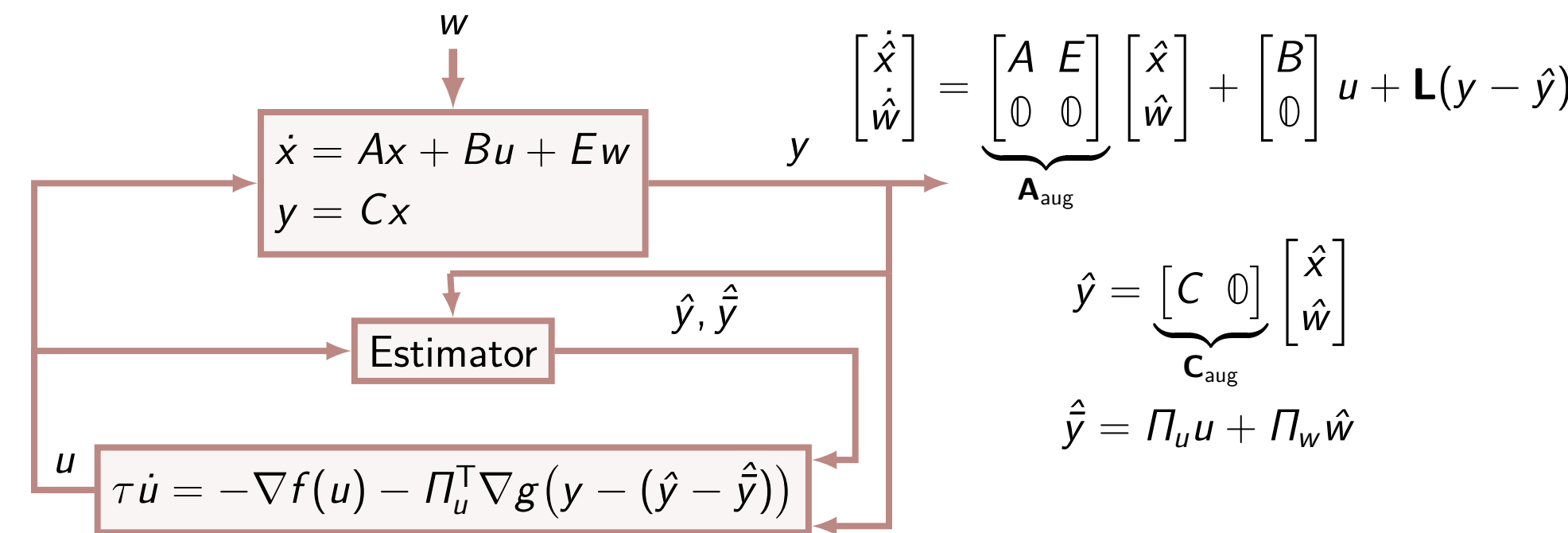
Motivation and Proposed Design

Motivation

- The **ideal** implementation assumes access to the **steady-state output** \bar{y}
- But \bar{y} is **not directly measurable** and we only measure the $y(t)$

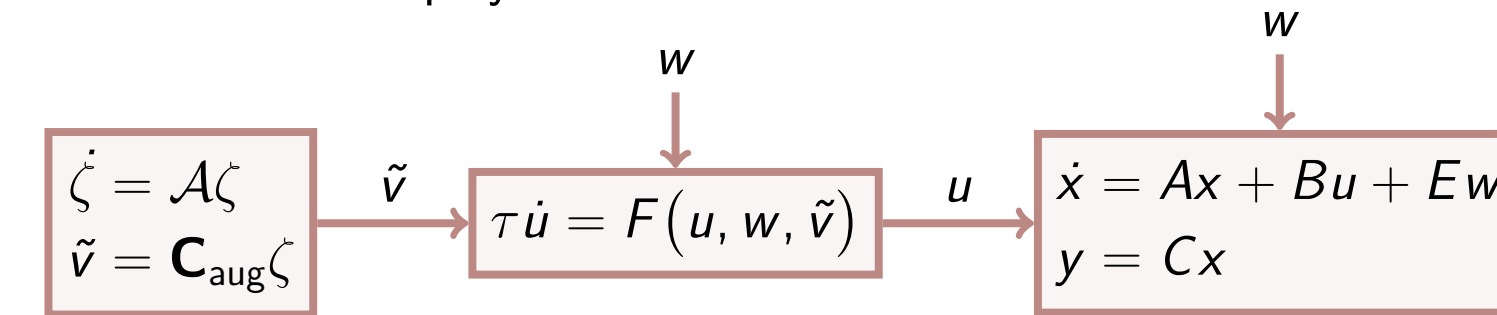
Goal

- Use further **model information** to produce *estimate* \hat{y} , then fed into the controller
- The estimator-enhanced feedback-based optimization (**EE-FBO**) design



Stable under fast controller and estimator tuning; convergence is then limited by the plant dynamics.

Proof Idea: The closed-loop system will have form of a **cascade**



- Select \mathbf{L} such that $\mathcal{A} = \mathbf{A}_{\text{aug}} + \mathbf{L}\mathbf{C}_{\text{aug}}$ is Hurwitz

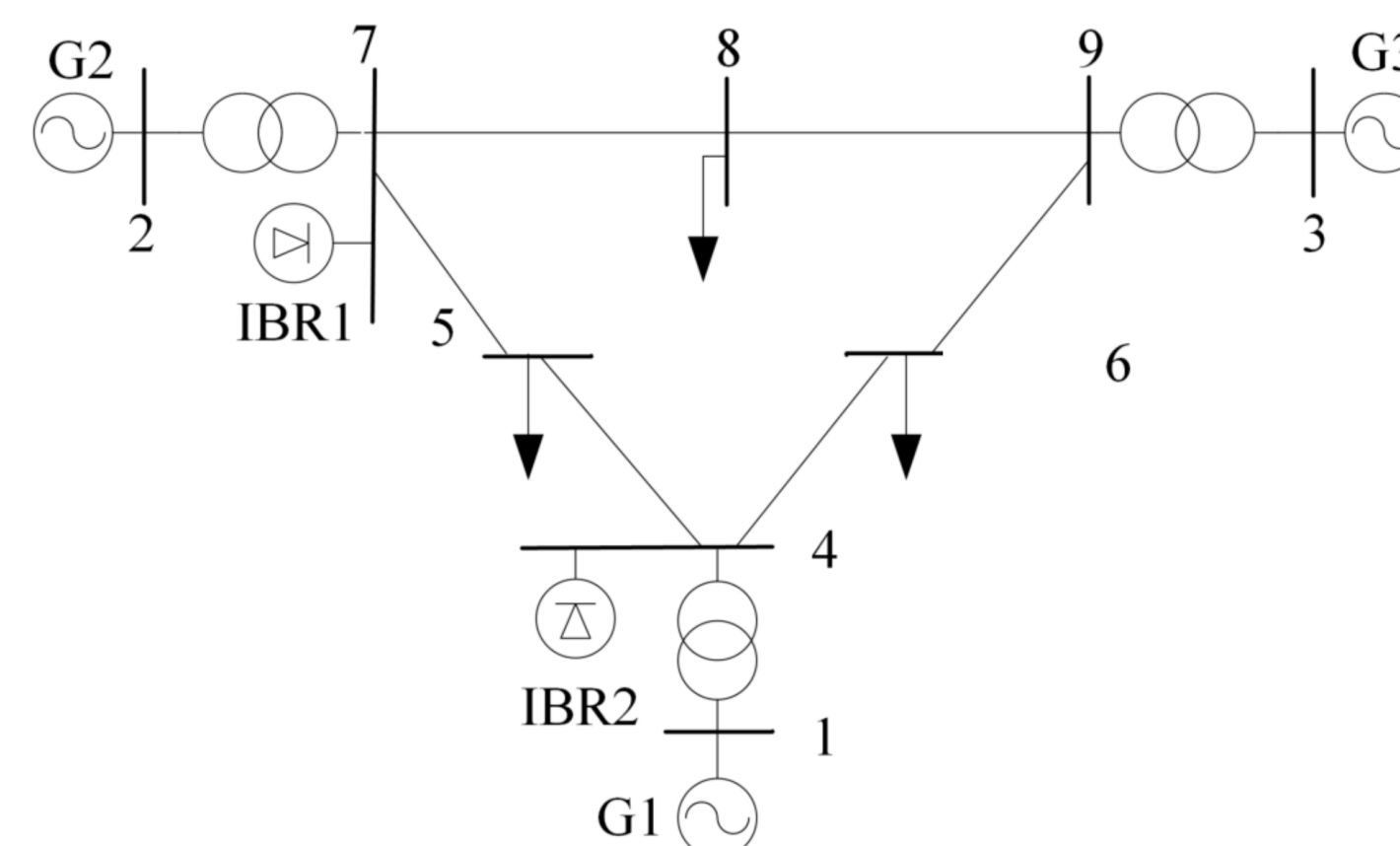
- Define error variables $\tilde{x} := x - \hat{x}$, $\tilde{w} := w - \hat{w}$, $\tilde{y} := y - \hat{y}$, and consider $\tilde{\zeta} = [\tilde{x} \ \tilde{w}]^T$

$$\dot{\tilde{\zeta}} = \mathcal{A} \tilde{\zeta}, \quad \tilde{y} = \mathbf{C}_{\text{aug}} \tilde{\zeta}, \quad \hat{y} = \Pi_u u + \Pi_w (w - \tilde{w})$$

$$\tau \dot{u} = -\nabla f(u) - \Pi_u^T \nabla g(\tilde{y} + \hat{y}) = -\nabla f(u) - \Pi_u^T \nabla g(\Pi_u u + \Pi_w w + \underbrace{C\tilde{x} - \Pi_w \tilde{w}}_{:=\tilde{v}}) := F(u, \tilde{v})$$

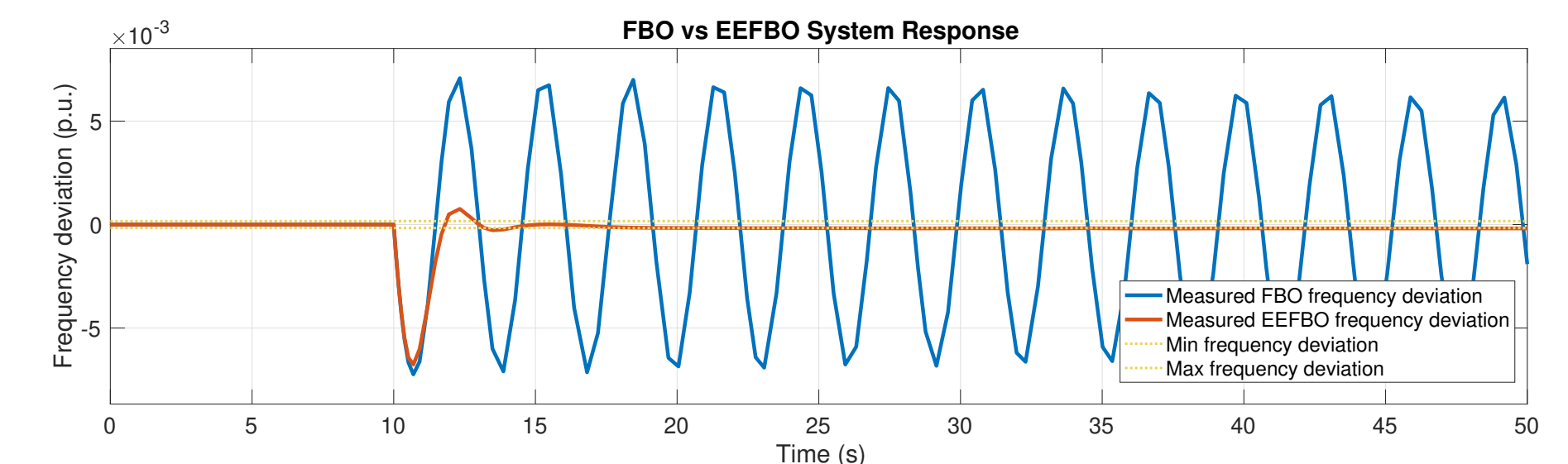
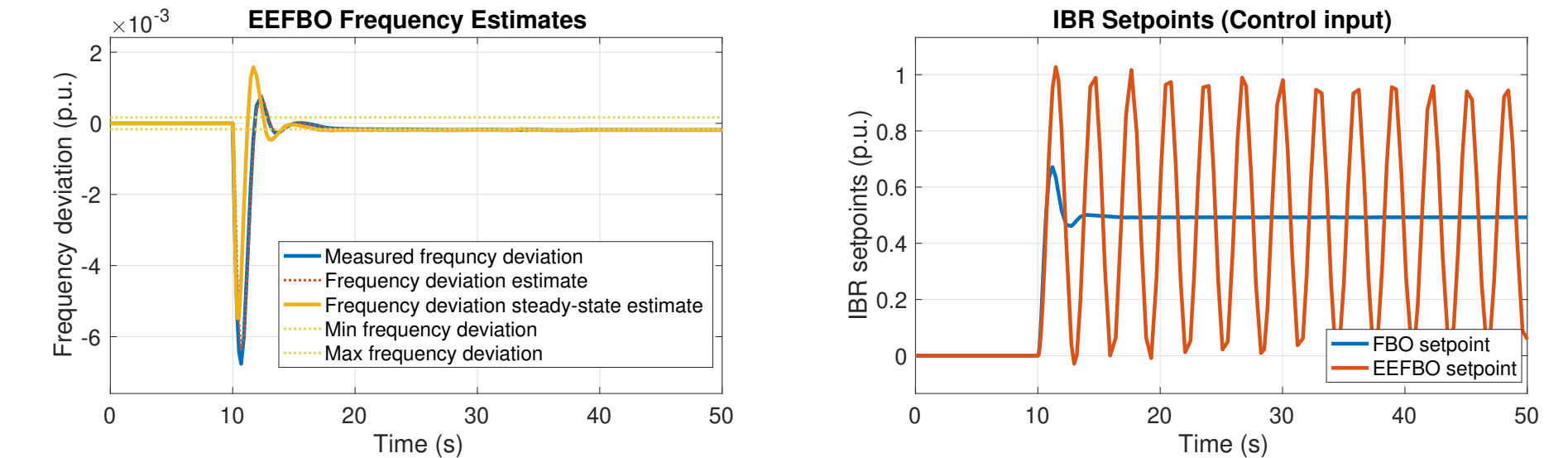
Power System Application

Using the system frequency response (SFR) model, design EE-FBO to compute IBR setpoints that rapidly restore frequency within operational limits

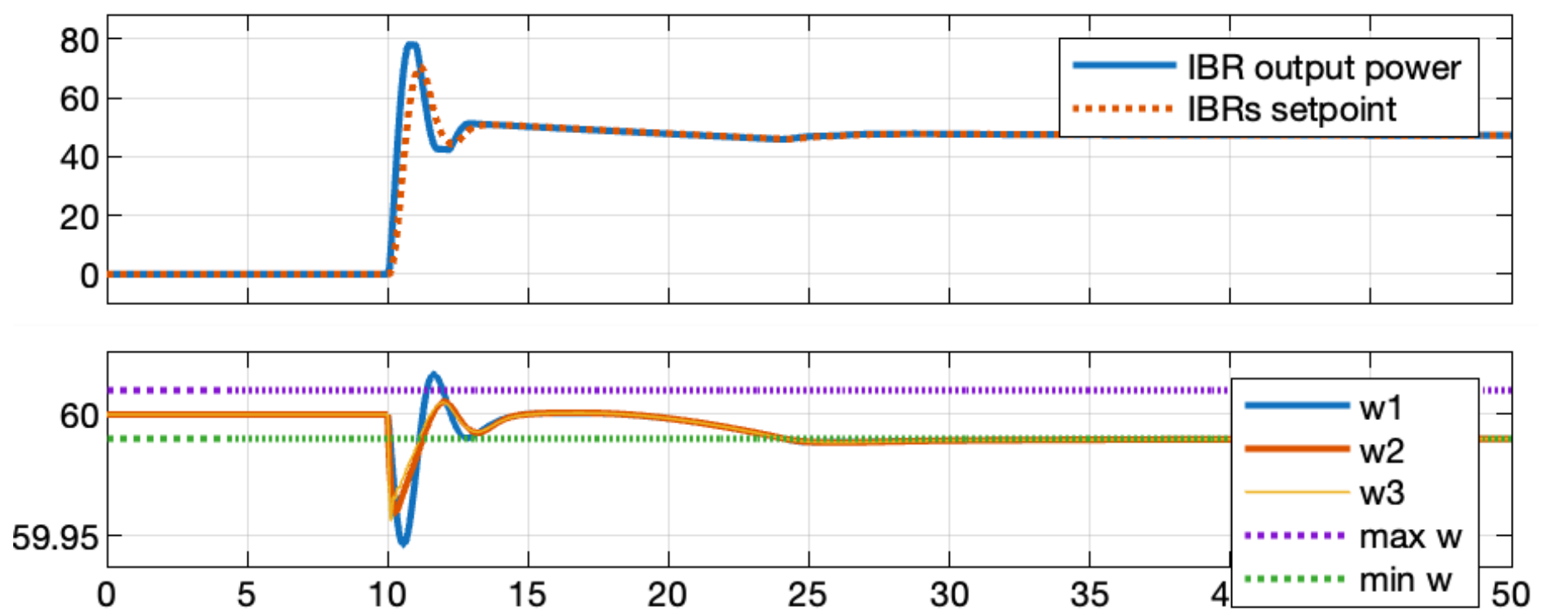


Simulation Results

- FBO becomes unstable by decreasing τ while EE-FBO remains stable



- Real model simulation with small τ with EEFBO.



Conclusion

Summary

- The stability of the closed-loop system depends on the controller's speed, which can be very slow, leading to poor performance
- By incorporating **model information** and designing an estimator, the closed-loop remains stable **without limitations**.

Future Work

- Extend the results to the **nonlinear plant** [Hauswirth '21]
- Explore alternative estimator designs that reduce reliance on model information in the design process

References

- [Hauswirth '24] Hauswirth, A., He, Z., Bolognani, S., Hug, G., Dorfler, F. (2024). Optimization algorithms as robust feedback controllers. *Annual Reviews in Control*, 57:100941. DOI: 10.1016/j.arcontrol.2024.100941.
- [Menta '18] Hauswirth, B., Bolognani, S., Hug, A., Dorfler, F., Menta, A. (2018). Stability of Dynamic Feedback Optimization with Applications to Power Systems. *Fifty-sixth Annual Allerton Conference on Communication, Control, and Computing*, held at Allerton House, Monticello, Illinois, October 2-5, 2018. ISBN: 9781538665961.
- [Hauswirth '21] Hauswirth, B., Bolognani, S., Hug, A., Dorfler, F. (2021). Timescale Separation in Autonomous Optimization. *IEEE Transactions on Automatic Control*, 66(2):611-624. DOI: 10.1109/TAC.2020.2989274.