

Viscous forces then give motion as shown

(i.e. Still unstable at  $Ra=0$ )  
i.e. in absence of gravity

This is a form of "Marangoni" convection (in particular this is called "thermo-capillary motion" aka "thermo-Marangoni")

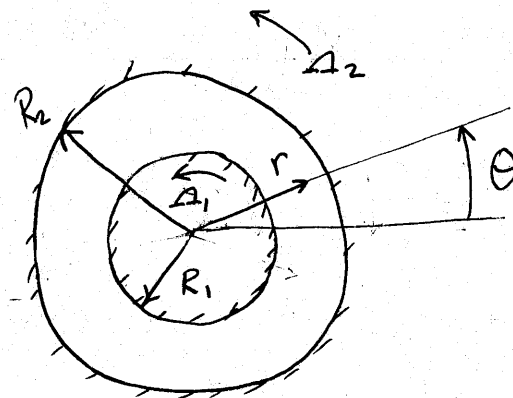
Buoyancy forces are also present if  $Ra > 0$

→ Other patterns have been documented, some due to imperfection (T.P.)

Ⓒ) Taylor-Couette Instability: Flow between rotating cylinders

"Centrifugal Instability" (cf ~~gravitational~~, capillary & thermal)

Consider viscous flow between concentric circular cylinders



N-S eqn. for incomp. flow (dimensional)

$$\text{div } \vec{u} = 0$$

Continuity

$$\vec{u}_t + (\vec{u} \cdot \nabla) \vec{u} = -\frac{1}{\rho} \nabla P + \gamma \nabla^2 \vec{u}$$

Momentum

Write N-S eqns in cylindrical coordinates  $(r, \theta, z)$ . For basic state (unperturbed)

$$\frac{\partial}{\partial t} = 0 \quad \frac{\partial}{\partial z} = 0 \quad \frac{\partial}{\partial \theta} = 0 \quad ; \quad u_1 = u_r = 0, \quad u_2 = u_\theta = V, \quad u_3 = u_z = 0$$

(See Schlichting, P.66)

Velocity in r-direction (not to be mistaken as a partial derivative)

Continuity:

$$\frac{1}{r} \frac{\partial}{\partial r} (r u_r) + \frac{1}{r} \frac{\partial u_\theta}{\partial \theta} + \frac{\partial u_z}{\partial z} = 0$$

∴ every term in continuity is zero

(this would've told us that  $u_r = 0$  if we didn't know already)

r-momentum transport eqn.

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$$\frac{\partial u_r}{\partial t} + u_r \frac{\partial u_r}{\partial r} + \frac{u_\theta}{r} \frac{\partial u_r}{\partial \theta} - \frac{u_\theta^2}{r} + u_z \frac{\partial u_r}{\partial z} = -\frac{1}{\rho} \frac{\partial p}{\partial r} + \nu \left( \nabla^2 u_r - \frac{u_r}{r^2} - \frac{2}{r^2} \frac{\partial u_\theta}{\partial \theta} \right)$$

in our notation:

$$-\frac{V^2}{r} = -\frac{1}{\rho} \frac{\partial p}{\partial r}$$

⇓

$$\boxed{\frac{dp}{dr} = \rho \frac{V^2}{r}}$$

Where  $\nabla^2 \equiv \frac{\partial^2}{\partial r^2} + \frac{1}{r} \frac{\partial}{\partial r} + \frac{1}{r^2} \frac{\partial^2}{\partial \theta^2} + \frac{\partial^2}{\partial z^2}$   
(Laplace operator in cylin. coord.; for ref., see Kaplan)

Pressure gradient = Centrifugal force

(since we don't know  $\frac{dp}{dr}$  a priori, we can't use this to solve for  $V$ , so use  $\theta$ -momentum eqn.)

$\theta$ -momentum:

$$\frac{d^2 V}{dr^2} + \frac{1}{r} \frac{dV}{dr} - \frac{V}{r^2} = 0$$

there are terms inside  $\mu(\dots)$   
(d.e. for  $V$  states that there is no net viscous force on fluid element)

Solution of this O.d.e.:

$$V = Ar + \frac{B}{r}$$

for the tangential velocity ( $u_r = u_z = 0$ )

(important observation)

Note that this solution tells us that all axisymmetric, rotating flows are made up of 2 components:

\* Solid-body rotation,  $Ar$  (constant times radius)

\* Potential (or "Free") vortex,  $\frac{B}{r}$

Recall:  $u_\theta = \frac{\Gamma}{2\pi r}$ , and  $u_r = 0$  Define a Vortex in Potential flow. In our notation this is  $V = \frac{\text{Const}}{r}$

(true, no matter what the BCs are)

BC. (Viscous flow)

$$V = \Omega_1 R_1$$

$$\text{at } r = R_1$$

$$V = \Omega_2 R_2$$

$$\text{at } r = R_2$$

Hence, A & B are found:

$$V = \frac{\Omega_2 R_2^2 - \Omega_1 R_1^2}{R_2^2 - R_1^2} r + \frac{(\Omega_1 - \Omega_2) R_1^2 R_2^2}{R_2^2 - R_1^2} \frac{1}{r}$$

Special cases:

$$1) \Omega_2 = \Omega_1 = \Omega$$

gives

$$V = \Omega r$$

Solid-body rotation throughout the gap.

No deformation, i.e. no strain

$$2) R_2 \rightarrow \infty, \Omega_2 = 0$$

gives

$$V = \frac{1}{r} \Omega_1 R_1^2$$

outer cylinder removed

Using definition of Circulation  $\Gamma = \oint \vec{u} \cdot d\vec{l}$  and apply it on surface of inner cylinder,

$$\Gamma = (\Omega_1 R_1) 2\pi R_1 = 2\pi \Omega_1 R_1^2$$

$\Rightarrow V = \frac{\Gamma}{2\pi r}$  (i.e. removal of outer cylinder) results in a Potential Vortex flow

We introduce small disturbances in the following form -

Velocity components  $u, v, w$ ; consider only axisymmetric disturbances which are periodic in  $z$ :

(why this form? it is observed as first bifurcation vs. other forms such as rotating waves)

$$u = u_1(r) e^{\sigma t} \cos \alpha z$$

$$v = v_0(r) + v_1(r) e^{\sigma t} \cos \alpha z$$

$$w = w_1(r) e^{\sigma t} \sin \alpha z$$

$$p = p_0(r) + p_1(r) e^{\sigma t} \cos \alpha z$$

where  $\alpha$  is wave number (in water waves,  $k$  was denoting wave number)

$\sigma$  is frequency (if real, then

disturbances grow, if imaginary, then motion is oscillatory)

(Note that  $p_0(r)$  is obtained from  $r$ -momentum eqn. for base flow)  
 $\uparrow$  base flow pressure distribution

B.C.  $u_1 = v_1 = w_1 = 0$  at  $r = R_1$  and  $r = R_2$

(1)

$$V_0 = Ar + \frac{B}{r}$$

(A and B are known, as shown above)

$$\frac{dP_0}{dr} = \rho \frac{V_0^2}{r}$$

(4 unknown functions,  $u_1, v_1, w_1, P_1$ ; 4 eqns., 3 momentum, 1 continuity)

Substitute in (full) Navier-Stokes eqns., neglect products of small quantities, eliminate  $w_1$  and  $P_1$ :

(Come up w/ 2 ode's)

$$\nabla(L - \alpha^2 - \frac{\sigma}{\nu})(L - \alpha^2) u_1(r) = 2\alpha^2 \frac{V_0(r)}{r} v_1(r)$$

and  $\nabla(L - \alpha^2 - \frac{\sigma}{\nu}) v_1(r) = 2A u_1(r)$

where an operator  $L$  has been defined.

$$L(\cdot) \equiv \frac{d^2(\cdot)}{dr^2} + \frac{1}{r} \frac{d(\cdot)}{dr} - \frac{(\cdot)}{r^2}$$

(looks similar to Laplacian in cylindrical coordinates except that it's missing the  $z$ -term)

B.C.'s  $u_1 = v_1 = \frac{du_1}{dr} = 0$  at  $r = R_1$  and  $r = R_2$

This is a complicated eigenvalue problem for  $\sigma$  in terms of other parameters

(i.e. it has a solution for  $u_1$  &  $v_1$  for each value of  $\sigma$ )

Can rewrite in non-dimensional form.

For a reference length can use the gap size:

$$d = R_2 - R_1$$

Reference velocity for  $V (= u_\theta)$  is  $\Omega_1 R_1$   
 tangential velocity

" " "  $u (= u_r)$  is  $\Omega, R, \frac{v}{A d^2}$  (2)

radial  
Velocity

$\underbrace{A d^2}_{[1/\text{time}]}$

● If equations are nondimensionalized in this way, there will appear one dimensionless Parameter:

$$T = - \frac{4A \Omega_1 d^4}{v^2} \quad \text{"Taylor no."} \quad (\text{Show it's dimensionless})$$

(Watch the notation, we had used T for temperature, in Bénard convection)

We will usually be considering  $A < 0$  (will stay same if it's stable) where  $v = Ar + \frac{B}{r}$

Special Cases:   
 "Narrow gap" approximation   
  $\frac{d}{r} \ll 1$ ,  $\frac{\Omega_2}{\Omega_1} \approx 1$  and negligible  $v$    
  $\Rightarrow L() \approx \frac{d^2()}{dr^2} \Rightarrow v_0 \approx \Omega r$    
 (i.e. inviscid)

● Differential equations give   
 (dimensional form)  $\frac{d^2 v_1}{dr^2} - \left(1 + \frac{4A \Omega_1}{\sigma^2}\right) \alpha^2 v_1 = 0$    
 ( $\alpha$  is wavenumber in 2-dir., and  $\sigma$  is frequency)

B.C.  $v_1 = 0$  at  $r = R_1$  and  $r = R_2$

Solution is  $v_1 = (\text{constant}) \sinh \frac{n\pi(r-R_1)}{d}$

and substitution into differential equation gives:

$$- \frac{n^2 \pi^2}{d^2} - \left(1 + \frac{4A \Omega_1}{\sigma^2}\right) \alpha^2 = 0$$

or  $\sigma^2 = \frac{-4A \Omega_1}{1 + \frac{n^2 \pi^2}{\alpha^2 d^2}}$

Taking  $\Omega_1 > 0$  (no loss of generality)

(3)

●  $\sigma$  is real if  $A < 0$ , giving 1 root which grows with time ( $\Rightarrow$  unstable)

$\sigma$  "imaginary"  $A > 0$  giving oscillatory motion ( $\Rightarrow$  neutral stability), i.e. disturbances neither grow or decay

Recall 
$$A = \frac{\Omega_2 R_2^2 - \Omega_1 R_1^2}{R_2^2 - R_1^2}$$

$\therefore \begin{cases} \Omega_2 R_2^2 < \Omega_1 R_1^2 & \text{get instability} \end{cases}$

●  $\begin{cases} \Omega_2 R_2^2 > \Omega_1 R_1^2 & \text{get stability} \end{cases}$

$\therefore$  For inviscid flow, Circulation must increase radially, otherwise unstable  
(recall)  $\Gamma = V \cdot 2\pi R$  (for axisymmetric flow)  
 $= (\Omega R) 2\pi R = (\text{const.}) \Omega R^2$

If  $\frac{d}{dr}$  is not small and  $\Omega_2$  is not close to  $\Omega_1$ , same conclusion can be reached.

The general result: "Rayleigh's criterion" (for inviscid flow)

● States that flow is stable if and only if  $\frac{d}{dr} (r V_0)^2 > 0$   
i.e. Square of the circulation should not decrease as you go out radially (for  $R_1 < r < R_2$ )  
When  $V_0 = Ar + \frac{B}{r}$  is the velocity of the base flow