PhD in Energy and Mineral Engineering at PSU

Nicolás's Research - Reports

Nicolás Bueno[1]   Advisor: Dr. Ayala[1]

[1]Department of Energy and Mineral Engineering
Penn State University

PennState
College of Earth
and Mineral Sciences

Table of Contents

Table of Contents

Considerations

Goal: Test the pseudopotential approach for partially misc. mixtures, under the action of a second force.

Idea: test different flow regimes based on Reynolds and Bond (Eotvos) numbers, and capture particular bubble shapes, as found by Flit R, Grace JR, Weber M. *Bubbles, drops, and particles.* New York: Academic Press; 1978.

$$R_e = \frac{\rho_l u_b d_b}{\mu_l} = \frac{u_b d_b}{\nu_l}$$

$$B_o = \frac{g \Delta \rho d_b^2}{\sigma}$$

A thermodynamic state fixes $\rho, \Delta\rho, \sigma$. Redifining R_e:

$$Re = \frac{d_b \sqrt{g d_b}}{\nu_l} = \frac{\sqrt{g d_b^3}}{\nu_l}$$

We can sweep the spectrum by fixing g (fixes B_o), and moving ν_l (fixes R_e), as:

$$\nu_l = c_s^2 (\tau_l - \frac{\Delta t}{2})$$

$$g = \frac{B_o \sigma}{\Delta \rho d_b^2}$$

$$\nu_l = \frac{\sqrt{g d_b^3}}{R_e}$$

$$\tau_l = \frac{\nu_l}{c_s^2} + \frac{\Delta t}{2}$$

Domain: (!) 300x300 mesh (2D)
Fluid: Water at 485.33 K ($T_r = 0.75$), and $P_r = 0.092$.
$\rho_l^0 = 7.679$ (), $\rho_v^0 = 0.109$. $\rho_r = 70.45$.
Initial condition: Spherical droplet with $d_o = 30$, and $w_o = 8$.

Boundary conditions: The top and bottom boundaries are PERIODIC. On the left and right boundaries a no-slip condition is imposed. At the corners, where there is a PDF that may belong to two boundaries, the enumeration and assignation of conditions is as follows:

- Corner 1 (SW): No-slip (Left)
- Corner 2 (NW): No-slip (Left)
- Corner 3 (SE): No-slip (Right)
- Corner 4 (NE): No-slip (Right)

Parameters: Shan-Chen G=-1.0.
Beta = 0.2076
Time = 100000

Single static simulation:
$\Delta\rho = 7.59285$, $d_s = 29.45$,
$\Delta P = 0.00378$ ($P_l < 0$).
$\sigma = 0.1112$.

Initial setup 2 (Amaya)

Domain: (!) 160x400 mesh (2D)
Fluid: Water at 485.33 K ($T_r = 0.75$), and $P_r = 0.092$.
$\rho_l^0 = 7.679$ (), $\rho_v^0 = 0.109$. $\rho_L/\rho_g = 70$.
$\tau_l = 210.5$. $\tau_g = 0.8$. $\mu_l/\mu_g = 10$.
Initial condition: Spherical droplet with $d_o = 40$, and $w_o = 8$.

Boundary conditions: Periodic on all boundaries (for static), walls on all boundaries (for dynamic). At the corners, where there is a PDF that may belong to two boundaries, the enumeration and assignation of conditions is as follows:

- Corner 1 (SW): No-slip (Left)
- Corner 2 (NW): No-slip (Left)
- Corner 3 (SE): No-slip (Right)
- Corner 4 (NE): No-slip (Right)

Parameters: Shan-Chen G=-1.0.
Beta = 0.2076
Time = 100000

Single static simulation:
$\Delta\rho = 7.2$ (7.7-0.5), $d_s = 40.0$,
$\Delta P = 8.5e-3 - 5.87e-3 = 2.623e-3$
$\sigma = \Delta P \cdot r = 0.05254$. $B_o = 10$. Then,
$g = \frac{\sigma B_o}{\Delta\rho d^2} = 4.5e-5$. $\mu_l = 0.85$, $\nu_l = 0.1105$. $\tau_l = 0.83$.

Spherical regime

First case (150 x 300)

- $g = |\mathbf{g}|$ = -1e-6. $B_o = 0.0592$. $\tau_l = 2.0$, $\nu = 0.5$. $u_b = 0.0121$.
- $R_e^{\text{org}} = 0.713$. $R_e^{\text{mod}} = 0.320$.
- This is spherical regime, and far away from the other regimes according to the Grace's plot.

Ellipsoidal case

Ellipsoid case (150 x 300)

- $g = |\mathbf{g}| = $ -1e-5. $B_o = 0.592$. $\tau_l = 0.51$, $\nu = 0.0033$. $u_b \approx = 0.35$.
- $R_e^{\mathrm{org}} = 3092$. $R_e^{\mathrm{mod}} = 151.61$
- This simulation is approaching to the Mach velocity limit and a perturbation is moving the bubble from the axis. I decided to open the channel more to avoid the interaction with the wall. I have reasons to believe that the movement beyond the axis is due to whom the corner was assigned to (number of boundary).

Ellipsoid case (300 x 300)

- $g = |\mathbf{g}| = $ -1e-5. $B_o = 0.592$. $\tau_l = 0.51$, $\nu = 0.0033$. $u_b \approx = 0.35$.
- $R_e^{\mathrm{org}} = 3092$. $R_e^{\mathrm{mod}} = 151.61$
- The ellipse shape of the bubble was better seen in this case, although eventually it moves away from the center. For the most part of the simulation, the ellipsoid maintains, although it is important to understand if the viscosity of the gas phase plays any role in the deformation ("plasticity" of the bubble).
- Apr 15/22. The ellipse is not moving anymore from the center.

Dimples

Dimples case (300 x 300)

- $g = |\mathbf{g}| = $ -2e-3. $B_o = 118$ $\tau_l = 0.72$, $\nu = 0.07348$. $u_b \approx = $.
- $R_e^{\mathrm{org}} = $. $R_e^{\mathrm{mod}} = 100$
- The gravity value is too high and the method is diverging too soon. Not even with $G = $ -0.1 or $g = $ 1e-4.

Dimples case (3000 x 3000)

- $d_o = 300$. $g = |\mathbf{g}| = $ -1e-5. $B_o = 61$. $\tau_l = 0.993$, $\nu = 0.164$ $u_b \approx = $.
- $R_e^{\mathrm{org}} = $. $R_e^{\mathrm{mod}} = 100$
- Did not run

Dimples case (3000 x 3000)

- $d_o = 300$. $g = |\mathbf{g}| = $ -1e-5. $B_o = 61$. $\tau_l = 5.43$, $\nu = 1.64$ $u_b \approx = $.
- $R_e^{\mathrm{org}} = $. $R_e^{\mathrm{mod}} = 10$
- Did not run

Table of Contents

Forcing scheme

Taking advantage of the mutual interactions between components, the pseudopotential is accounting only for attraction between components, while an extra term accounts for the usual repulsion term:

$$F_i^\sigma = -\frac{1}{c_s^2 \delta t} \sum_\alpha w_\alpha e_{\alpha,i} \left[\frac{R_s T}{1 - b_m \rho} - c_s^2 \right] \rho_\sigma(\mathbf{x} + \mathbf{e}_\alpha \delta t)$$

$$-\psi^\sigma \sum_{\sigma_2} G_{\sigma,\sigma_2} \sum_\alpha w_\alpha e_{\alpha,i} \psi^{\sigma_2}(\mathbf{x} + \mathbf{e}_\alpha \delta t)$$

Where ψ and G_{σ,σ_2} are defined as:

$$\psi^\sigma = \rho^\sigma \sqrt{\frac{a^\sigma}{f(b\rho)}}$$

$$G_{\sigma,\sigma_2} = \frac{2(\Lambda_{\sigma,\sigma_2} - 1)}{c_s^2 \delta t} \tag{1}$$

where $f(b\rho)$ is the density-dependent polynomial in the denominator of the attraction term in the cubic equation of state. Here, the terms a, b are given in mass-basis, so proper conversions must be taken care of.

Taylor Expansion

Generic form:

$$F_i = \sum_{\alpha} T(\mathbf{x} + \mathbf{e}_{\alpha}\delta t) w_{\alpha}\mathbf{e}_{\alpha}$$

Replacing the Taylor expansion of T

$$F_i = T(\mathbf{x})\sum_{\alpha} w_{\alpha}\mathbf{e}_{\alpha} + \partial_j T\delta t \sum_{\alpha} w_{\alpha}\mathbf{e}_{\alpha}\mathbf{e}_{\alpha}^j + \frac{\delta t^2}{2}\partial_j\partial_k(T)\sum_{\alpha} w_{\alpha}\mathbf{e}_{\alpha}\mathbf{e}_{\alpha}^j\mathbf{e}_{\alpha}^k +$$

$$\frac{\delta t^3}{6}\partial_j\partial_k\partial_l(T)\sum_{\alpha} w_{\alpha}\mathbf{e}_{\alpha}\mathbf{e}_{\alpha}^j\mathbf{e}_{\alpha}^k\mathbf{e}_{\alpha}^l$$

Continuum approach:

$$F_i = c_s^2\delta t\partial_i T + \frac{c_s^4\delta t^3}{2}\partial_i\partial_{kk}(T)$$

Resulting pressure;

$$p = c_s^2\sum_{\sigma}\rho_{\sigma} + \frac{c_s^2\delta t}{2}\sum_{\sigma}\sum_{\sigma_2} G_{\sigma,\sigma_2}\psi_{\sigma}\psi_{\sigma_2} + \sum_{\sigma}(\frac{R_s T}{1 - b_m\rho} - c_s^2)\rho_{\sigma}$$

$$p = \frac{R_s T}{(1 - b_m\rho)}\rho - \frac{a_m\rho^2}{f(b_m\rho)}$$

Table of Contents

Simulation setup

From van der Waals implementation into the
phase behavior model (C++):

Name, mw, pc, tc, acen, vc, shift
C3 0.044097 615.8 666.05 0.1522 0.0 0.0
C5 0.044097 488.5 845.80 0.2514 0.0 0.0

Conditions:
$P = 275.36$ psi, $T = 192.34$ F. $z = [0.5, 0.5]$

Results from flash:
Densities $= 13.5852$ lb/ft3, 2.3956 lb/ft3
(4.693187 lu, 0.8275917 lu)
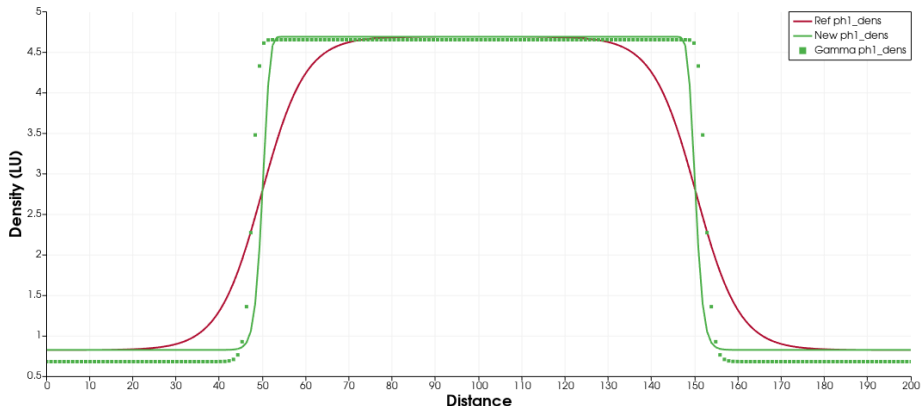Fugacities $= 906.34$ kPa, 604.423 kPa
(0.043939432 lu, 0.029302344 lu)
Liquid composition $= [0.36357, 0.63643]$
Gas composition $= [0.54527, 0.45473]$
$K_i = 1.49975, 0.714505$. $\gamma = 0.642$

Results

The density profile converges to the correct values given by the vdW EoS. The splitting coefficient, with no calibration in β, compromises the vapor density to under predicted values.

Results

The pressure with the new scheme converges to the correct pressure value. The splitting scheme, as the density of the vapor is lower, the convergence pressure is also lower. Due to the small compressibility of the liquid, to achieve this value of pressure, small changes in density are needed, so the liquid density is not compromised.
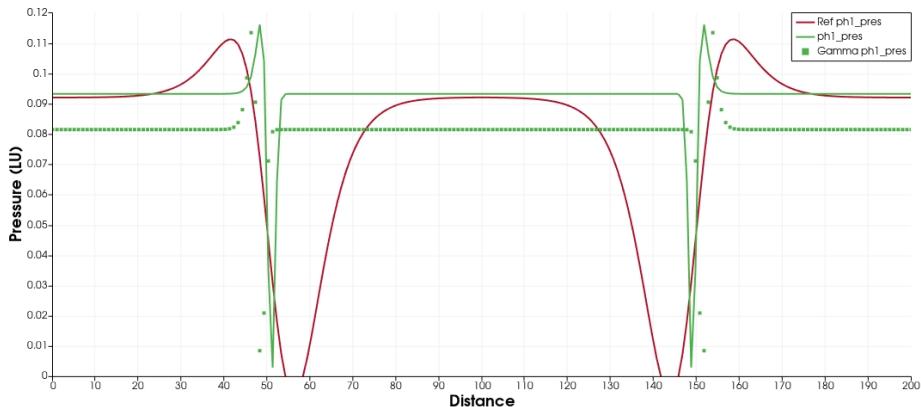
Results

The compositions in both cases do not match with equilibrium values. This is due that the model does not allow for diffusion if the pressure is already in equilibrium. These results suggest that transport is favored to keep the liquid properties are they were initialized, and balances the vapor properties accordingly.

Results
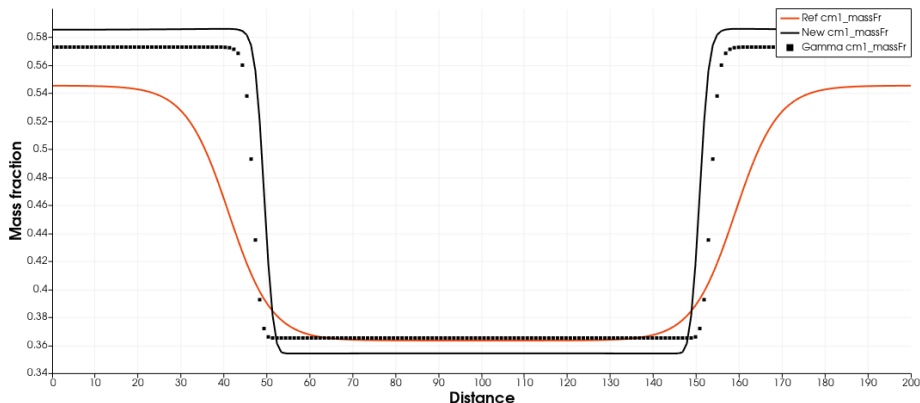
Fugacities prove the non chemical-equilibrium in the system.
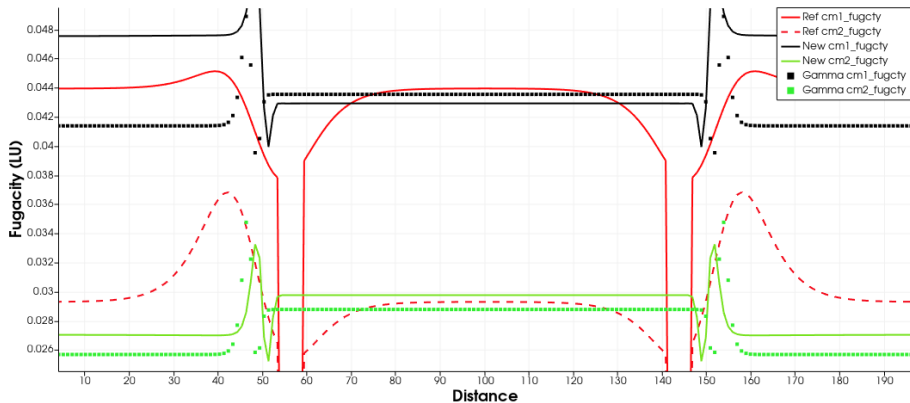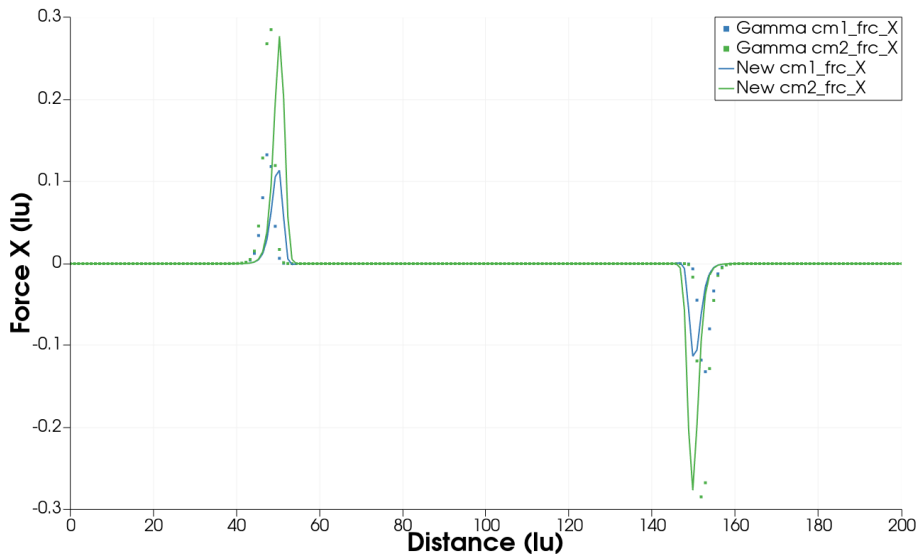
Table of Contents

Domain: 160x400 mesh (2D)

Fluid: C3 and C5

Acentric	Tc	Pc	Mw
0.1522	370	42.46	0.044097
0.2514	469.9	33.68	0.072150

Temperature 362.0 K (Tr = 0.83).
Equilibrium conditions: ρ_l, ρ_v (lbm/ft3)
= 31.89, 1.86. mw_l, mw_v (g/mol) =
61.95, 51.88. $\bar{\rho}_{\text{ratio}}$ = 14.32. K_1, K_2 =
1.987, 0.436. γ = 0.583.
.

Boundary conditions: Full periodic.
Initial conditions: Time 10000. Bubble
in thermodynamic equilibrium, r_0, w_0 = .

Two models were tested: new forcing
scheme, and the Sankarana model.
Parameters: Shan-Chen G=-1.0.
Beta = 0.2076
Time = 100000

Single static simulation:
$\Delta\rho$ = 7.59285, d_s = 29.45,
ΔP = 0.00378 ($P_l < 0$).
σ = 0.1112.

Results Sankarana

In this model, the pseudopotential is given by $\psi_1 = \sqrt{\frac{\rho_1}{1-b_1\rho_1} - a_1\rho_1^2 - \rho_2}$ and $\psi_2 = \rho_2$

Initialization: $\rho_l = 5.75$, $\rho_v = 2.17$. $z_{1,l} = 0.98$, $z_{1,v} = 0.48$. $r_e = 24.5$, $w = 5.0$.

Static results:
$\rho_l = 5.77$, $\rho_v = 2.18$. $z_{1,l} = 0.98$, $z_{1,v} = 0.53$. For $r_e = 27$, $\Delta p = \frac{\sigma}{r} = 0.00274$. $\sigma = 0.074$.

$$B_o = \frac{g\Delta\rho d_b^2}{\sigma} = 141.465e3 \cdot g$$

$$M_o = \frac{g\Delta\rho\mu_l^4}{\sigma^3\rho_l^2} = \frac{g\Delta\rho\nu_l^4\rho_l^2}{\sigma^3} = 294.952e3 \cdot g \cdot \nu_l^4$$

Report XXX XX - 202X

Main discussion points:

- Topic 1
- Topic 2

Sample frame title

This is a text in second frame. For the sake of showing an example.

- Text visible on slide 1

Sample frame title

This is a text in second frame. For the sake of showing an example.

- Text visible on slide 1
- Text visible on slide 2

Sample frame title

This is a text in second frame. For the sake of showing an example.

- Text visible on slide 1
- Text visible on slide 2
- Text visible on slides 3

Sample frame title

This is a text in second frame. For the sake of showing an example.

- Text visible on slide 1
- Text visible on slide 2

- Text visible on slide 4

In this slide

In this slide
the text will be partially visible

In this slide
the text will be partially visible
And finally everything will be there

Sample frame title

In this slide, some important text will be highlighted because it's important. Please, don't abuse it.

Remark

Sample text

Important theorem

Sample text in red box

Examples

Sample text in green box. The title of the block is "Examples".

Two-column slide

This is a text in first column.

$$E = mc^2$$

- First item
- Second item

This text will be in the second column and on a second tought this is a nice looking layout in some cases.