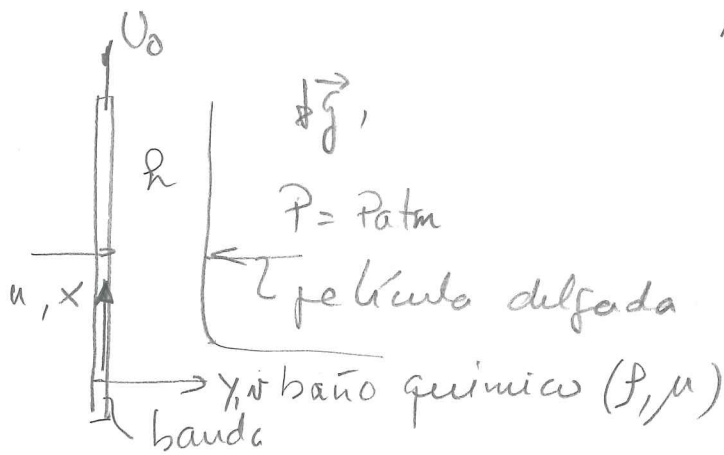


1



Un proceso estacionario,
 Asumiendo: flujo completamente
 desarrollado, laminar,
 Gradiente de presión
 nulo, y tensión de
 corte nula en la superficie
 externa de la película

Determine una expresión para
 la velocidad del flujo

Solución:

i) asumiendo flujo incompresible de un fluido Newtoniano,
 problema hidrodinámico y bidimensional, las ecuaciones de N-S son

$$a) \quad \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$b) \text{ dir-x: } u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \frac{1}{\rho} \frac{\partial p}{\partial x} + \frac{\mu}{\rho} \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) + \beta g_x$$

$$\text{dir-y: } u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = \frac{1}{\rho} \frac{\partial p}{\partial y} + \frac{\mu}{\rho} \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right) + \beta g_y$$

2i) De continuidad, en flujo desarrollado $v = v(y)$ ó $v = 0$
 C.B. en $y=0$, $\underline{v=0} \Rightarrow \underline{dv=0}$
 flujo desarrollado, $\frac{\partial u}{\partial x} = 0 \Rightarrow \underline{u=u(y)}$

$$3i) \text{ de dir-x: } 0 = \mu \frac{d^2 u}{dy^2} - \beta g$$

$$\text{de dir-y: } 0 = 0$$

$$4i) \text{ De (3i), } \frac{du}{dy} = \frac{\beta g}{\mu} y + A$$

$$u(y) = \frac{\beta g}{2\mu} y^2 + Ay + B$$

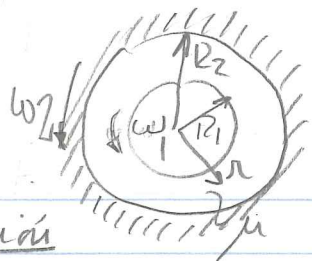
$$5i) \text{ C.B. } U(y=0) = U_0 = B$$

$$6) \quad \left. \frac{du}{dy} \right|_{y=h} = 0 = \frac{\beta g h}{\mu} + A \Rightarrow A = -\frac{\beta g h}{\mu}$$

$$6i) \text{ Por lo tanto, } \left[u(y) = U_0 + \frac{\beta g}{2\mu} (y^2 - 2hy) \right]$$

#2

5/5

Se pide $\vec{V} = (V_r, V_\theta, V_z)$; fluido - aceite a 20°C

... solución

Ecuaciones gobernantes en coordenadas cilíndricas

1) Continuidad

$$\frac{1}{r} \frac{d}{dr} (r V_r) + \frac{1}{r} \frac{d V_\theta}{d\theta} + \frac{d V_z}{dz} = 0$$

Cilindro muy largo $\Rightarrow \frac{d}{dz} (\) \equiv 0$; y $V_z = 0$ Simetría rotacional $\Rightarrow \frac{d}{d\theta} (\) \equiv 0$ Largo $\omega(1)$ $r V_r = cte \Rightarrow V_r = 0$

$$V_\theta = f(r)$$

2) Navier-Stokes: fuerzas máximas iguales a las

$$z\text{-direc.}: -\frac{dp}{dz} = 0 \quad (i)$$

$$\theta\text{-direc.}: 0 = \mu \left(\frac{1}{r} \frac{d}{dr} \left(\frac{1}{r} \frac{d}{dr} (r V_\theta) \right) \right) \quad (ii)$$

$$r\text{-direc.}: -\frac{\rho V_\theta^2}{r} = -\frac{dp}{dr} \quad (iii)$$

$$de (ii): V_\theta = V_\theta(r) = C_1 r + \frac{C_2}{r}$$

$$\text{Condiciones de borde: } \begin{cases} (a) V_\theta(r=R_1) = \omega_1 R_1 \\ (b) V_\theta(r=R_2) = \omega_2 R_2 \end{cases}$$

$$\Rightarrow C_1 = 2 \frac{(\omega_2 R_2^2 - \omega_1 R_1^2)}{R_2^2 - R_1^2}; C_2 = R_1 R_2 \frac{(\omega_2 R_2 R_1 - \omega_1 R_1 R_2)}{R_1^2 - R_2^2}$$

$$\text{Así, } \vec{V} = (0, V_\theta, 0)$$

$$a) V_\theta = \frac{(\omega_2 R_2^2 - \omega_1 R_1^2) r}{R_2^2 - R_1^2} - \frac{1}{r} \frac{(R_1 R_2)^2 (\omega_2 - \omega_1)}{(R_2^2 - R_1^2)}$$

$$b) \omega_2 = -\omega_1$$

$$V_\theta = -\frac{(\omega_1 R_1^2 + \omega_2 R_2^2) r}{R_2^2 - R_1^2} + \frac{1}{r} \frac{(R_1 R_2)^2 (\omega_1 + \omega_2)}{(R_2^2 - R_1^2)} \quad \#$$

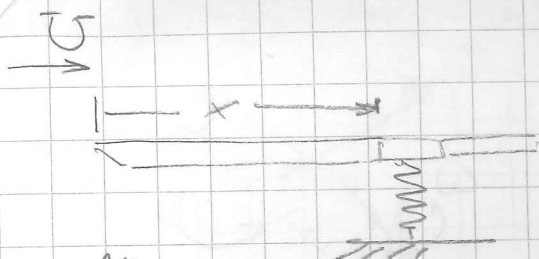
problema 3(a)

Aire a 20°C y $p = 1 \text{ Atm.}$

$x = 2 \text{ m}$

$Z_w = 2.1 \text{ Pa}$

- a) Determinar U : veloc. corriente libre
- flujo turbulento
 - fluido Newtoniano y flujo incomp.



soln:

(a) $Z_w = C_{f,x} \cdot \frac{1}{2} \rho U^2$; donde $C_{f,x} = \frac{0.0577}{Re_x^{1/5}}$; $Re_x = \frac{\rho U x}{\mu}$

$Z_w = \frac{0.0577}{\left(\frac{U x}{\nu}\right)^{1/5}} \cdot \frac{1}{2} \rho U^2 = \frac{0.02885 \rho U^{9/5} x^{1/5}}{(x/\nu)^{1/5}}$

$\Rightarrow U^{9/5} = \frac{Z_w \cdot (x/\nu)^{1/5}}{0.02885 \rho}$ dato $\left\{ \begin{array}{l} \rho = 1.2 \text{ kg/m}^3 \\ \nu = 1.49 \times 10^{-5} \text{ m}^2/\text{s} \\ Z_w = 2.1 \text{ N/m}^2 \\ x = 2 \text{ m} \end{array} \right.$

$U^{9/5} = \frac{2.1 \times (2 / 1.49 \times 10^{-5})^{1/5}}{0.02885 \times 1.2} = 643.37$

$0.2 \ U = 36.32 \text{ m/s}$

(b) Espesor de capa límite δ @ $x=2$: $\frac{\delta}{x} = \frac{0.37}{Re_x^{1/5}}$ 0.5

$\delta(x) = \frac{0.37 x}{\left(\frac{U \cdot x}{\nu}\right)^{1/5}} = \frac{0.37 \times 2}{\left(\frac{36.32 \times 2}{1.49 \times 10^{-5}}\right)^{1/5}} = 0.034 \text{ m} = 3.4 \text{ cm.}$

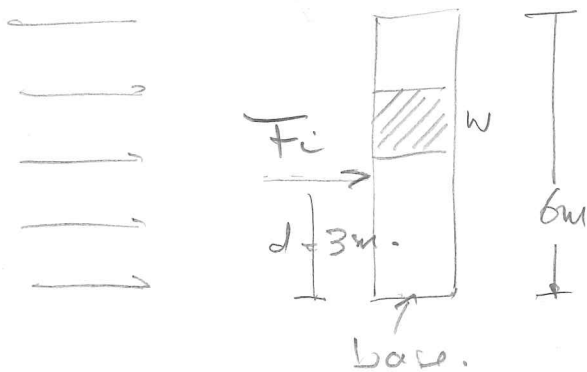
(c) Velocidad u @ $y = 5.5 \text{ cm}$

Debido a que $y = 5.5 \text{ cm} > \delta(x) \Big|_{x=2}$, $u(y) = U =$ 0.5

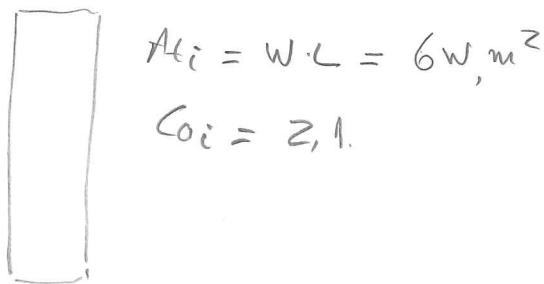
#35 Se pide determinar qual pulso está mais soltado.

(i°)

$$U_0 = 1,5 \text{ m/s}$$



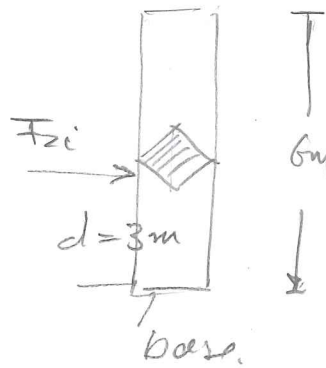
$$F_i = C_{oi} \frac{1}{2} \rho U_0^2 A_{ti}$$



$$F_i = 2,1 \times \frac{1}{2} \rho U_0^2 \times 6w$$

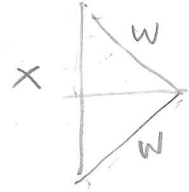
$$F_i = 6,3 \rho U_0^2 w$$

(zi)



$$F_{zi} = C_{zi} \frac{1}{2} \rho U_0^2 A_{zi}$$

$$X = \sqrt{w^2 + w^2} = \sqrt{2} w$$



$$A_{zi} = \sqrt{2} w L = 6\sqrt{2} w, m^2$$

$$C_{zi} = 1,6$$

$$F_{zi} = 1,6 \times \frac{1}{2} \rho U_0^2 \sqrt{2} 6w$$

$$F_{zi} = 6,788 \rho U_0^2 w$$

$$\frac{F_{zi}}{F_i} = \frac{6,788}{6,3} = 1,077$$

\Rightarrow A pulso (zi) está mais soltado ja
que $F_{zi} = 1,077 F_i$ ($F_{zi} > F_i$)

$$M_{Fi} = F_i \times d$$

$$M_{F_{zi}} = F_{zi} \times d. > M_{Fi}$$