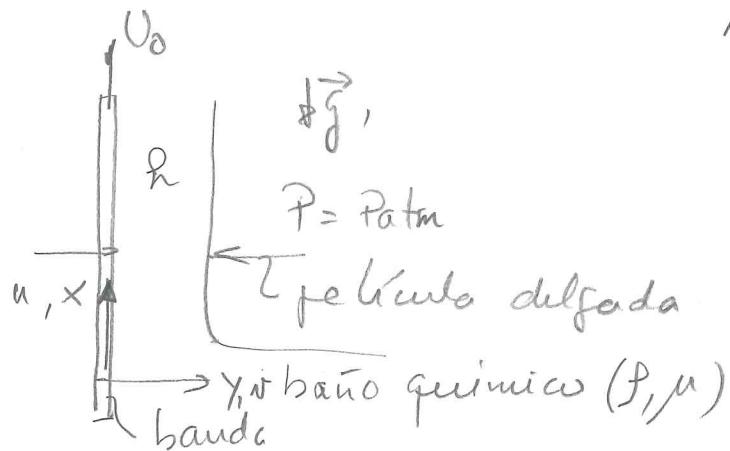


1



Un proceso estacionario,
Aunviendo flujo completamente
desarrollado, laminar,
gradiente de presión
nulo, y fuerzas de
corte nulo en la superficie
externa de la placa.

Determine una expresión para
la velocidad del flujo

Solución:

i) Aunviendo flujo incompresible de un fluido Newtoniano,
problema hidrodinámico y bidimensional. Las ecuaciones de N-S son

$$a) \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$b) \text{dir-x: } u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = f \frac{\partial p}{\partial x} + \mu \left(\frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right) + \frac{\rho g}{\mu} x$$

$$\text{dir-y: } v \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = f \frac{\partial p}{\partial y} + \mu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial z^2} \right) + \frac{\rho g}{\mu} y$$

ii) De continuidad, en flujo desarrollado $v = v(x)$ ó $v = ct$
c. B. $w|_{y=0} = 0, v|_{y=0} = c \Rightarrow c = 0$
flujo desarrollado, $\frac{\partial u}{\partial x} = 0 \Rightarrow u = u(y)$

$$3i) \text{ dir-x: } 0 = \mu \frac{d^2 u}{dy^2} - fg$$

$$\text{dir-y: } 0 = 0$$

$$4i) \text{ De (3i), } \frac{du}{dy} = \frac{fg}{\mu} y + A$$

$$u(y) = \frac{fg}{\mu} y^2 + A y + B$$

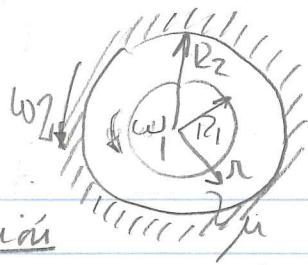
$$5i) \text{ C.B. } u(y=0) = U_0 - B$$

$$\left. \frac{du}{dy} \right|_{y=h} = \mu \left. \frac{du}{dy} \right|_{y=h} = 0 = \frac{fg h}{\mu} + A \Rightarrow A = -\frac{fg h}{\mu}$$

$$6i) \text{ Por lo tanto, } \boxed{u(y) = U_0 + \frac{fg}{2\mu} (y^2 - 2hy)}$$

#2

5/5



Se pide $\vec{V} = (V_r, V_\theta, V_z)$; fluido - aceite a 20°C

solución

Ecuaciones gobiernantes en coordenadas cilíndricas

1) Continuidad

$$\frac{1}{r} \frac{\partial}{\partial r} (r V_r) + \frac{1}{r} \frac{\partial V_\theta}{\partial \theta} + \frac{\partial V_z}{\partial z} = 0$$

Cilindro muy largo $\Rightarrow \frac{\partial}{\partial z} = 0$, y $V_z = 0$

Simetría rotacional $\Rightarrow \frac{\partial}{\partial \theta} = 0$

Algo m (1) $r V_r = cte \Rightarrow V_r = 0$

$$V_\theta = f(r)$$

2) Newton-Stokes: fuerzas nulas iguales a cero

$$z\text{-direc.: } - \frac{\partial p}{\partial z} = 0 \quad (i)$$

$$\theta\text{-direc.: } 0 = \mu \left(\frac{1}{r} \frac{\partial}{\partial r} (r V_\theta) \right) \quad (ii)$$

$$r\text{-direc.: } - \frac{f V_\theta^2}{r} = - \frac{\partial p}{\partial r} \quad (iii)$$

$$\text{de (ii): } V_\theta = V_\theta(r) = C_1 r + \frac{C_2}{r}$$

$$\begin{aligned} \text{Condiciones de bndr: } & (a) V(r=R_1) = \omega_1 R_1 \\ & (b) V(r=R_2) = \omega_2 R_2 \end{aligned}$$

$$\Rightarrow C_1 = 2 \left(\frac{\omega_2 R_2^2 - \omega_1 R_1^2}{R_2^2 - R_1^2} \right); C_2 = R_1 R_2 \left(\frac{\omega_2 R_2 R_1 - \omega_1 R_1 R_2}{R_2^2 - R_1^2} \right)$$

$$\text{Asi, } \vec{V} = (0, V_\theta, 0)$$

$$a) V_\theta = \frac{(\omega_2 R_2^2 - \omega_1 R_1^2)r}{R_2^2 - R_1^2} - \frac{1}{r} \frac{(R_1 R_2)^2 (\omega_2 - \omega_1)}{(R_2^2 - R_1^2)}$$

$$b) \omega_2 = -\omega_1$$

$$V_\theta = - \frac{(\omega_1 R_1^2 + \omega_2 R_2^2)r}{R_2^2 - R_1^2} + \frac{1}{r} \frac{(R_1 R_2)^2 (\omega_1 + \omega_2)}{(R_2^2 - R_1^2)}$$

Wolkerma 3(a)

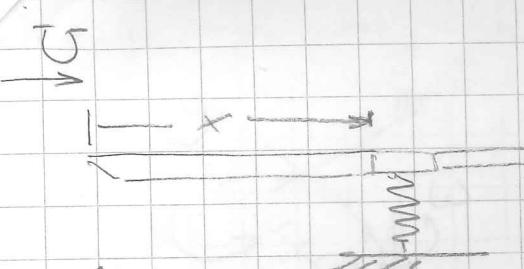
Aire a 20°C y $P = 1 \text{ atm}$.

15

$$x = 2 \text{ m}$$

$$\tau_w = 2.1 \text{ Pa}$$

- a) Determinar U : velo. corriente lib.
- flujo turbulento
 - fluido Newtoniano y flujo incompr.



Soln:

$$(a) \tau_w = C_{f, \epsilon} \frac{1}{2} \rho U^2 ; \text{ donde } C_{f, \epsilon} = \frac{0.0577}{0.1} \frac{R_x}{Re}^{1/5} ; \frac{R_x}{0.1} = 0.1$$

$$\tau_w = \frac{0.0577}{(\frac{U x}{D})^{1/5}} \frac{1}{2} \rho U^2 = \frac{0.02885 \rho U^{9/5}}{(x/D)^{1/5}}$$

$$\Rightarrow U^{9/5} = \frac{\tau_w \cdot (x/D)^{1/5}}{0.02885 \rho} \text{ datos} \quad \begin{cases} \rho = 1.2 \text{ kg/m}^3 \\ \rho = 1.49 \times 10^{-5} \text{ m}^2/\text{s} \\ \tau_w = 2.1 \text{ N/m}^2 \\ x = 2 \text{ m} \end{cases}$$

$$U^{9/5} = 2.1 \times \frac{(2 / 1.49 \times 10^{-5})^{1/5}}{0.02885 \times 1.2} = 643.37$$

$$0.2 U = 36.32 \text{ m/s}$$

$$(b) \text{ Efecto de capa límite f(x) } \quad \frac{f}{x} = \frac{0.37}{Re_x^{1/5}} \quad 0.5$$

$$f(x) = \frac{0.37 x}{(U \cdot x/D)^{1/5}} = \frac{0.37 x}{(36.32 \times 2 \times 1.49 \times 10^{-5})^{-1/5}} = 0.034 \text{ m} \\ = 3.4 \text{ cm.}$$

$$(c) \text{ Velocidad } u \text{ a } y = 5.5 \text{ cm}$$

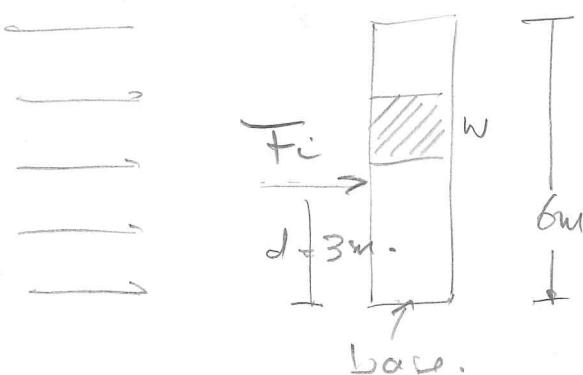
$$\text{Debido a que } y = 5.5 \text{ cm} > f(x) \quad \left. \frac{u}{U} = \frac{y}{f(x)} \right|_{x=2}, \quad u(y) = U = \text{m/s}$$

Se pide determinar cuál polar está más solicitado.

#35

(1°)

$$U_0 = 1,5 \text{ m/s}$$



$$\bar{F}_i = C_{0i} \frac{1}{2} \rho U_0^2 A_{ti}$$

$$A_{ti} = w \cdot L = 6w, \text{ m}^2$$

$$C_{0i} = 2,1$$

$$\bar{F}_i = 2,1 \times \frac{1}{2} \rho U_0^2 \cdot 6w$$

$$\bar{F}_i = 6,3 \rho U_0^2 w$$

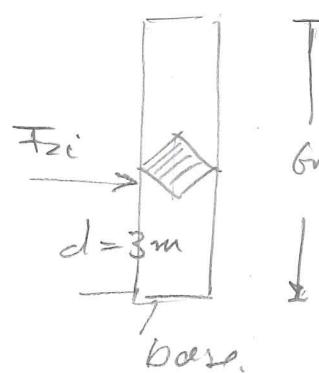
$$\frac{\bar{F}_{zi}}{\bar{F}_i} = \frac{6,788}{6,3} = 1,077$$

\Rightarrow El polo (2i) está más solicitado ya que $\bar{F}_{zi} = 1,077 \bar{F}_i$ ($\bar{F}_{zi} > \bar{F}_i$)

$$N\bar{F}_i = \bar{F}_i \times d$$

$$M\bar{F}_{zi} = \bar{F}_{zi} \times d. > M\bar{F}_i$$

(2i)



$$\bar{F}_{zi} = C_{0i} \frac{1}{2} \rho U_0^2 A_{zi}$$

$$A_{zi} = \sqrt{2} w L = 6\sqrt{2} w, \text{ m}^2$$

$$C_{0zi} = 1,6$$

$$\bar{F}_{zi} = 1,6 \times \frac{1}{2} \rho U_0^2 \sqrt{2} 6w$$

$$\bar{F}_{zi} = 6,788 \rho U_0^2 w$$

$$x = \sqrt{w^2 + w^2} \\ = \sqrt{2} w \\ \times \begin{array}{c} w \\ \diagdown \\ \sqrt{2} w \end{array}$$