# MEC E 430 Formula Sheet

#### Non-Dim of NS

$$t^* = ft, \ \vec{x}^* = \frac{\vec{x}}{L}, \ v^* = \frac{\vec{v}}{V}$$
 
$$P^* \frac{P - P_{\infty}}{P_0 - P_{\infty}}, \ g^* = \frac{\vec{g}}{g}, \ \vec{\nabla}^* = L\vec{\nabla}$$
 Non-dimensionalized NS:

$$[\operatorname{St}] \frac{\partial v^*}{\partial t^*} + (\vec{v} \cdot \vec{\nabla}) \vec{v}^* = -[\operatorname{Eu}] \vec{\nabla} P^*$$

$$+ [Fr^{-2}]\vec{g}^* + [Re^{-1}]\vec{\nabla}^2 \vec{v}^*$$

where

$$St = \frac{fL}{V}, Eu = \frac{P_0 - P_{\infty}}{\rho V^2}$$
$$Fr = \frac{V^2}{gL}, Re = \frac{\rho VL}{\mu}$$

### Creeping Flow (Stokes Flow)

 $Re \ll 1$ , viscous forces dominate, inertia negligible. NS becomes:

$$\vec{\nabla}P = \mu \vec{\nabla}^2 \vec{v}$$

Drag on creeping flow,

$$F_D = cVL\mu, \ F_{D, \rm sphere} = 3\pi\mu VD$$
 Typical balance for falling sphere:

$$\begin{split} W &= F_D + F_{\rm buoyancy} \\ F_{\rm buoyancy} &= \frac{\pi D^3}{6} \rho_{\rm fluid} g, \; W = \rho_{\rm particle} \frac{\pi D^3}{6} g \end{split}$$

# Inviscid Flow (Euler Flow)

Viscous stresses are negligible,  $\tau \approx 0$ . Typically high Re, away from wall. Can't specify no-slip at wall.

$$\rho \left[ \frac{\partial \vec{v}}{\partial t} + (\vec{v} \cdot \vec{\nabla}) \vec{v} \right] = -\vec{\nabla} P + \rho \vec{g}$$

$$\frac{P}{\rho} + \frac{V^2}{2} + gz = \text{constant along streamline}$$

Check shear to make sure 0:

$$\tau = \mu \frac{\partial U}{\partial y}$$

$$\tau_{r\theta} = \mu \left( r \frac{\partial}{\partial r} \left( \frac{u_{\theta}}{r} \right) + \frac{1}{r} \frac{\partial u_r}{\partial \theta} \right)$$

#### Irrotational Flow

$$u = \frac{\partial \phi}{\partial x}, \ v = \frac{\partial \phi}{\partial y}, \ w = \frac{\partial \phi}{\partial z}$$
$$u_r = \frac{\partial \phi}{\partial r}, \ u_\theta = \frac{1}{r} \frac{\partial \phi}{\partial \theta}, \ u_z = \frac{\partial \phi}{\partial z}$$

 $\vec{\nabla} \times \vec{v} = 0$ . Velocity potential,  $\phi$ ,

Solve cont.  $(\nabla^2 \phi = 0)$ , calculate  $\vec{v}$ , and calculate P from Bernoulli, Bernoulli is constant everywhere for irrotational flow.

$$\nabla^2 \phi = \frac{\partial^2 \phi}{\partial x^2} + \frac{\partial^2 \phi}{\partial y^2} + \frac{\partial^2 \phi}{\partial z^2} = 0$$
$$\nabla^2 \phi = \frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial \phi}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 \phi}{\partial \theta^2} + \frac{\partial^2 \phi}{\partial z^2} = 0$$

### **Boundary Layer**

Laminar BL assumptions are: steady, incomp, 2D, Re is large such that  $\delta/x \ll 1$ , BL stays laminar:

$$u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} = v\frac{\partial^2 u}{\partial y^2}$$
$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

Blasius similarity variable

$$\eta = y\sqrt{\frac{U_{\infty}}{\nu x}}, \ f' = \frac{f}{U_{\infty}}$$

Blasius solution for flat plate:

	Laminar	Turbulent
BL Thick.	$\frac{\delta}{x} = \frac{4.91}{\sqrt{\text{Re}_x}}$	$\frac{\delta}{x} = \frac{0.16}{(\mathrm{Re}_x)^{1/7}}$
Displ. Thick.	$\frac{\delta^*}{x} = \frac{1.72}{\sqrt{\text{Re}_x}}$	$\frac{\delta^*}{x} = \frac{0.20}{(\text{Re}_x)^{1/7}}$
Momen. Thick.	$\frac{\theta}{x} = \frac{0.664}{\sqrt{\mathrm{Re}_x}}$	$\frac{\theta}{x} = \frac{0.016}{(\mathrm{Re}_x)^{1/7}}$
Local Skin Fric. Coeff.	$C_{f,x} = \frac{0.664}{\sqrt{\mathrm{Re}_x}}$	$C_{f,x} = \frac{0.027}{\text{Re}_x^{1/7}}$

Displacement thickness

$$\delta^* = \int_0^\delta (1 - \frac{u}{U_\infty}) \, dy$$

Momentum thickne

$$\theta = \int_0^\delta \frac{u}{U_\infty} (1 - \frac{u}{U_\infty}) \, dy$$

Drag Coefficient

$$C_D = \frac{2F_D}{\rho V^2 A}$$

#### 1D Isentropic Nozzle

Assumptions: 1D (negligible boundary layer effects); steady; adiabatic; ideal gas; isentropic; inlet conditions do not change appreciably. Stagnation properties:

$$h_0 = h + \frac{V^2}{2}$$
$$T_0 = T + \frac{V^2}{2c_n}$$

If isentropic:

$$\frac{P_0}{P} = \left(\frac{T_0}{T}\right)^{\frac{k}{k-1}}$$
$$\frac{\rho_0}{\rho} = \left(\frac{T_0}{T}\right)^{\frac{1}{k-1}}$$

Speed of sound:

$$c = \sqrt{\left(\frac{\partial P}{\partial \rho}\right)_s} = \sqrt{kRT}$$

Mach number:

$$Ma = \frac{V}{c}$$

For an expansion with  $\uparrow A$ :

	Subsonic	Supersonic
	$\downarrow V, \text{Ma}$	$\uparrow V, Ma$
	$\downarrow P, \rho$	$\uparrow P, \rho$
and if $c_p$	is constant:	
-	$\frac{T_0}{T} = 1 + \frac{k - 1}{2}$	$\frac{-1}{2}$ Ma <sup>2</sup>
=	$\frac{P_0}{P} = \left(1 + \frac{k}{2}\right)$	$\left(\frac{c-1}{2}\mathrm{Ma}^2\right)^{\frac{k}{k-1}}$
	$=\frac{\rho_0}{\rho}$	
	, ,	

When Ma= 1 (at throat), critical properties

$$\begin{split} \frac{T^*}{T_0} &= \frac{2}{k+1} \\ \frac{P^*}{P_0} &= \left(\frac{2}{k+1}\right)^{\frac{k}{k-1}} \\ &= \frac{\rho^*}{\rho_0} \end{split}$$

so exit pressure:

$$\begin{split} P_e &= \begin{cases} P_b, & P_b > P^*(\text{subsonic}, \text{Ma} < 1) \\ P^*, & P_b \leq P^*(\text{sonic/chocked}, \text{Ma} = 1) \end{cases} \end{split}$$
 mass flow:

 $\dot{m} = \rho A V$ 

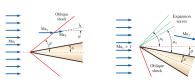
$$= P_0 A \text{Ma} \sqrt{\frac{k}{RT_0}} \left( 1 + \frac{k-1}{2} \text{Ma}^2 \right)^{\frac{-k-1}{2(k-1)}}$$

$$\dot{m}_{\text{max}} = P_0 A^* \sqrt{\frac{k}{RT_0}} \left(\frac{2}{k+1}\right)^{\frac{k+1}{2(k-1)}}$$

$$= \rho^* A^* V^*$$

note, max mass flow is when Ma= 1 and  $A = A^*$ . For converging-diverging nozzles,

$$\frac{A}{A^*} = \frac{1}{\text{Ma}} \left( \frac{2}{k+1} \cdot \left( 1 + \frac{k-1}{2} \right) \right)^{\frac{k+1}{2(k-1)}}$$



Oblique Shock

Expansion Fan

#### **Normal Shock**

Region 1 is upstream, Region 2 is downstream. The shock is not isentropic.

$$T_{01} = T_{02}$$

$$Ma_2 = \sqrt{\frac{(k-1)Ma_1^2 + 2}{2kMa_1^2 - (k-1)}}$$

$$\frac{P_2}{P_1} = \frac{2k\text{Ma}_1^2 - (k-1)}{k+1}$$

$$\frac{\rho_2}{\rho_1} = \frac{P_2/P_1}{T_2/T_1} = \frac{(k+1)\mathrm{Ma}_1^2}{2 + (k-1)\mathrm{Ma}_1^2} = \frac{V_1}{V_2}$$

$$\frac{T_2}{T_1} = \frac{2 + \operatorname{Ma}_1^2(k-1)}{2 + \operatorname{Ma}_2^2(k-1)}$$

$$\frac{P_{02}}{P_{01}} = \frac{\text{Ma}_1}{\text{Ma}_2} \left( \frac{1 + \text{Ma}_1^2(k-1)/2}{1 + \text{Ma}_2^2(k-1)/2} \right)^{\frac{k+1}{2(k-1)}}$$

$$s_2 - s_1 = c_p \ln \left(\frac{T_2}{T_1}\right) - R \ln \left(\frac{P_2}{P_1}\right)$$

### Oblique Shock

 $\theta$  is the turning angle,  $\beta$  is the shock angle. If thin boundary layer,  $\delta = \theta$ . The normal components of the shock is the same as a **normal shock**. Use  $Ma_n$  and  $V_n$  for normal components. Pressure, temperature, and density are still  $P_0, T_0, \rho_0$ . The normal components:

$$\begin{aligned} \operatorname{Ma}_{1,n} &= \operatorname{Ma}_1 \sin \beta \\ \operatorname{Ma}_{2,n} &= \operatorname{Ma}_2 \sin(\beta - \theta) \\ \tan \theta &= \frac{2 \cot \beta (\operatorname{Ma}_1^2 \sin^2 \beta - 1)}{\operatorname{Ma}_1^2 (k + \cos 2\beta) + 2} \end{aligned}$$

Mach angle,

$$\mu = \sin^{-1} (1/Ma_1)$$

# **Expansion Waves**

$$\theta = \nu(\mathrm{Ma}_2) - \nu(\mathrm{Ma}_1)$$

$$\nu(\text{Ma}) = \sqrt{\frac{k+1}{k-1}} \tan^{-1} \sqrt{\frac{k-1}{k+1}} (\text{Ma}^2 - 1)$$
$$-\tan^{-1} \sqrt{\text{Ma}^2 - 1}$$

Use isentropic relations to find properties across the wave.