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ADDITION/CORRECTION

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Correction to *P*, ρ, *T* Measurements and Isobaric Vapor−Liquid Equilibria of the 1,3,3-Trimethyl-2-oxabicycle[2,2,2]octane + Propan-1-ol Mixture: Cubic and Statistical Associating Fluid Theory-Based Equation of State Analysis [*Journal of Chemical & Engineering Data* **2010**, *55*, 5932–5940 DOI: 10.1021/je100577v]. Marcos Torcal, Sandra García-Abarrio, Juan I. Pardo,* Ana M. Mainar, and José S. Urieta

In the original document (*J. Chem. Eng. Data* **2010**, *55* (12), 5932−5940), page 5937, Table 7 and page 5938, Table 9 contained errors in the data concerning 1,8-cineole. The corrected data are reported.

Table 7. Coefficients for the Equations of Vapor Pressure. The Equation of Antoine Provides P^{sat}/kPa Using T/K . Capital Letters: Equation of Antoine; Lower Case Letters: Wagner Equation

	A/a	B/b	C/c	d	T_{min}/K	T_{max}/K
1,8-cineole	13.9128	3523.60	−70.03		326.65	449.15
1-propanol[a]	−8.53706	1.96214	−7.6918	2.945		T_c[a]

[a] Ref 14.

Table 9. Properties and Parameters of the Pure Components Used for the Application of the EOS

PR and PT		T_c/K		P_c/MPa		ω
1,8-cineole		661.12[a]		3.019[a]		0.338[b]
propan-1-ol		536.98[c]		5.175[c]		0.629[c]
SAFT	m	v^{oo}/L·mol^{-1}	u^0/k/K	κ	ε/k/K	range T/K
1,8-cineole	5.2966	0.015698	250.71	0	0	326.65−449.15
propan-1-ol	3.240[d]	0.0120[d]	225.68[d]	0.01968[d]	2619[d]	293−493[d]
PC-SAFT	m_i	σ_i/Å	ε_i/k/K	$k^{A_iB_i}$	$\varepsilon^{A_iB_i}/k$/K	range T/K
1,8-cineole	3.4254	4.0597	291.37	0	0	326.65−449.15
propan-1-ol	2.9997[e]	3.2522[e]	233.40[e]	0.015268[e]	2276.8[e]	240−537[e]

[a] Joback's method, ref 35. [b] Lee−Kesler method, ref 36. [c] Ref 13. [d] Ref 38. [e] Ref 42.

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