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Experimentation with Different Thermodynamic Cycles Used for pK_a Calculations on Carboxylic Acids Using Complete Basis Set and Gaussian-n Models Combined with CPCM Continuum Solvation Methods

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Received 28 February 2001; revised 21 May 2001; accepted 3 July 2001

ABSTRACT: Complete basis set and Gaussian-*n* methods were combined with Barone and Cossi's implementation of the polarizable conductor model (CPCM) continuum solvation methods to calculate pK_q values for six carboxylic acids. Four different thermodynamic cycles were considered in this work. An experimental value of -264.61 kcal/mol for the free energy of solvation of H⁺, $\Delta G_s(H^+)$, was combined with a value for $G_{gas}(H^+)$ of -6.28 kcal/mol, to calculate p K_q values with cycle 1. The complete basis set gas-phase methods used to calculate gas-phase free energies are very accurate, with mean unsigned errors of 0.3 kcal/mol and standard deviations of 0.4 kcal/mol. The CPCM solvation calculations used to calculate condensed-phase free energies are slightly less accurate than the gas-phase models, and the best method has a mean unsigned error and standard deviation of 0.4 and 0.5 kcal/mol, respectively. Thermodynamic cycles that include an explicit water in the cycle are not accurate when the free energy of solvation of a water molecule is used, but appear to become accurate when the experimental free energy of vaporization of water is used. This apparent improvement is an artifact of the standard state used in the calculation. Geometry relaxation in solution does not improve the results when using these later cycles. The use of cycle 1 and the complete basis set models combined with the CPCM solvation methods yielded p K_a values accurate to less than half a pKa unit. © 2001 John Wiley & Sons, Inc. Int J Quantum Chem 85: 727–741, 2001

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Contract grant sponsors: Petroleum Research Fund; NIH; Hamilton College; Merck/AAAS Undergraduate Summer Research Program.

International Journal of Quantum Chemistry, Vol. 85, 727–741 (2001) © 2001 John Wiley & Sons, Inc.

Key words: pK_a ; carboxylic acids; CBS-QB3; CBS-APNO; G2; G3; free energy; aqueous solution; thermodynamic cycles

Introduction

he field of computational chemistry is reaching the point where calculations at the level of chemical accuracy, within 1 kcal/mol, are now possible. Numerous attempts to accurately calculate pK_a values have been made, but none has achieved chemical accuracy [1-28]. The definition of pK_a is

$$pK_a = -\log K_a, \tag{1}$$

and since

$$\Delta G^0 = -2.303 \text{RT} \log K_a, \tag{2}$$

$$pK_a = \Delta G^0 / 2.303RT.$$
 (3)

Calculating accurate pK_a values is demanding, as an error of 1.36 kcal/mol in ΔG^0 gives an error of 1 pK_a unit. There are at least three sources of error in pK_a calculations. The first is the model used to calculate pK_a , which generally involves a thermodynamic cycle such as:

Cycle 1

$$AH_{gas} \xrightarrow{\Delta G_{gas}} A^{-}_{gas} + H^{+}_{gas}$$

$$\uparrow -\Delta G_{s}(AH) \quad \downarrow \Delta G_{s}(A^{-}) \quad \downarrow \Delta G_{s}(H^{+})$$

$$AH_{aq} \xrightarrow{\Delta G_{aq}} A^{-}_{aq} + H^{+}_{aq}$$

or

$$Cycle \ 2$$

$$H_2O + AH_{gas} \xrightarrow{\Delta G_{gas}} A^-_{gas} + H_3O^+_{gas}$$

$$\uparrow -\Delta G_s(H_2O) \uparrow -\Delta G_s(AH) \downarrow \Delta G_s(A^-) \downarrow \Delta G_s(H_3O^+)$$

$$H_2O + AH_{aq} \xrightarrow{\Delta G_{aq}} A^-_{aq} + H_3O^+_{aq}$$

In these cycles $\Delta G_{\rm gas}$ is calculated with high-level ab initio or density functional methods, and the ΔG_s values are calculated using a solvation method, typically a continuum dielectric approach. The p K_a values can be determined from Eq. (3), where $\Delta G^0 = \Delta G_{\rm aq}$. The second and third major errors stem from the accuracy of the calculations for $\Delta G_{\rm gas}$ and ΔG_s . Relative p K_a calculations allow one to calculate the unknown p K_a of a molecule BH from the known

 pK_a of molecule AH. In these relative calculations only the values for G_{AH} , G_{A^-} , G_{BH} , G_{B^-} , $\Delta G_s(AH)$, $\Delta G_s(A^-)$, $\Delta G_s(BH)$, and $\Delta G_s(B^-)$ are required for either thermodynamic cycle, as the values for the species involving H⁺ in cycle 1, or H₃O⁺ and H₂O in cycle 2, cancel. For this reason, accuracy in the calculation of relative pK_a values depends on the second and third main errors. We have recently reported that relative and absolute pK_a values accurate to within half a pK_a unit can be calculated for carboxylic acids [29, 30]. The absolute pK_a values were determined with thermodynamic cycle 1 [30]. In this work we analyze the errors that stem from the use of different thermodynamic cycles in pK_a calculations. This work is of fundamental importance because different workers have used different treatments of H⁺/H₃O⁺ in their own calculations.

Methods

To find the best thermodynamic cycle for calculating absolute pK_a values, we used six simple carboxylic acids that ranged in size from 24 to 68 electrons: formic acid, acetic acid, cyanoacetic acid, chloroacetic acid, oxalic acid, and pivalic acid. All calculations were performed on Origin 200 SGI servers equipped with 1-2 GB of memory and 36 GB of scratch disk space, using Gaussian 98 [31], Spartan 5.1 [32], and GAMESOL [33] software. The acids and corresponding ions were initially optimized in the gas phase at the Hartree–Fock (HF) level. We then used the CBS-QB3 [34], CBS-APNO [35, 36], G3 [37], and G2 [38] model chemistry methods to calculate G_{gas} values for various conformers of all six acids and their corresponding anions. CBS-APNO calculations were not run on chloroacetic acid and the chloroacetate anion as this method is not yet available for chlorine.

The complete basis set methods [34–36] were developed by Petersson and co-workers as a model chemistry that makes use of a complete basis set (CBS) extrapolation of the correlation energy based on the asymptotic convergence of pair natural orbital expansions [39–43]. The philosophy of the method is based on the idea that the major source of error in most ab initio calculations of molecular energies is the truncation of the one-electron

basis set. The CBS-QB3 method uses density functional theory geometries and SPCs are performed at the CCSD(T), MP4SDQ, and MP2 levels with small basis sets. The CBS-APNO method uses HF/6-311G(d,p) geometries for the frequency calculation and SPCs are carried out on QCISD/6-311G(d,p) geometries. The SPCs are expensive and use QCISD(T) and MP2 theory for correlation corrections.

Pople and co-workers [37, 38, 44–47] have developed the Gaussian methods (G1, G2, G3, and MP2 variants), which are extrapolation schemes similar to the CBS model chemistries. The G2, G3, CBS-QB3, and CBS-APNO model chemistries are state-of-the-art models for accurate thermochemistry [34, 37, 48, 49].

The absence of imaginary frequencies verified that all structures were true minima at their respective levels of calculation. Higher energy conformers were also computed using each method for five of the acids. The absolute value of each energy, in hartrees, have been previously reported [29, 30].

We computed ΔG_s using Barone and Cossi's implementation of the polarizable conductor model (CPCM) [50], which is based on the polarized continuum model (PCM) of Tomasi and co-workers [51-57]. In this method the solute cavities are modeled on the optimized molecular shape and include both electrostatic and nonelectrostatic contributions to the energies. The CPCM calculations were performed as SPCs using the 6-31G(d) and 6-31+G(d) basis sets on the HF/6-31G(d) and HF/6-31+G(d) geometries for each of the six systems. Geometry optimizations were also performed using CPCM/HF/6-31G(d). In all of the CPCM calculations the surface of each sphere was subdivided into 240 triangular tesserae, and the area of the tesserae was set at 0.3 Å². All CPCM calculations were performed using Gaussian 98 [31].

Using different combinations of $G_{\rm gas}$ and $\Delta G_{\rm s}$ values, and different thermodynamic cycles, we calculated the absolute p K_a for each acid in its lowest energy gas-phase conformation. In addition, we calculated the conformational average of the aqueous free energies of the acids [59] and computed the absolute p K_a values for each of the six acids.

We compared four different thermodynamic cycles in this work. Besides the two cycles outlined in the introduction, we used the following cycles, which are based on the work of Nascimento and coworkers [21, 28].

$$Cycle 3$$

$$H_2O_{gas} + AH_{gas} \xrightarrow{\Delta G_{gas}} A^-_{gas} + H_3O^+_{gas}$$

$$\uparrow -\Delta G_{vap} \qquad \uparrow -\Delta G_s \qquad \downarrow \Delta G_s \qquad \downarrow \Delta G_s$$

$$H_2O(l) + AH_{aq} \xrightarrow{\Delta G_{aq}} A^-_{aq} + H_3O^+_{aq}$$

$$Cycle 4$$

$$H_2O_{gas} + AH_{gas} \xrightarrow{\Delta G_{gas}} A^-_{gas} + H_3O^+_{gas}$$

$$\uparrow \Delta G_{vap} \qquad \uparrow -\Delta G_s \qquad \downarrow \Delta G_s \qquad \downarrow \Delta G_s$$

$$AH_{aq} \qquad A^-_{aq} + H_3O^+_{aq}$$

$$\uparrow -\Delta G_{relax} \qquad \downarrow \Delta G_{relax} \qquad \downarrow \Delta G_{relax}$$

$$H_2O(l) \; + AH_{aq,relax} \overset{\Delta G_{aq,relax}}{\rightarrow} A^-_{aq,relax} + H_3O^+_{aq,relax}$$

The difference between cycle 2 and cycle 3 is that the experimental free energy of vaporization of water is used instead of the free energy of solvation. Cycle 4 includes the relaxation of each molecule in solution, from the gas-phase geometry to the solution geometry, obtained by optimizing each molecule in the presence of the dielectric continuum [21, 28].

In Eqs. (2) and (3), our ΔG^0 is ΔG_{aq} from the thermodynamic cycles. Therefore all of our p K_a calculations use the formula

$$pK_a = \Delta G_{aq}/2.303 \text{ RT.} \tag{4}$$

In our thermodynamic cycles,

$$\Delta G_{\rm aq} = \Delta G_{\rm gas} + \Delta \Delta G_{\rm sol},\tag{5}$$

and for cycle 1,

$$\Delta \Delta G_{\text{sol}} = \Delta G_s(H^+) + \Delta G_s(A^-) - \Delta G_s(AH). \quad (6)$$

The values for $G(H^+_{gas})$ and $\Delta G_s(H^+)$ are derived from experiment. We have used the values $G(H^+_{gas}) = -6.28$ kcal/mol and $\Delta G_s(H^+) = -264.61$ kcal/mol. The calculation of ΔG_{gas} uses a reference state of 1 atm, and the calculations of ΔG_s use a reference state of 1 M. Converting the ΔG_{gas} reference state (24.46 L at 298.15 K) from 1 atm to 1 M is accomplished using:

$$\Delta G_{\rm gas}(1 \text{ M}) = \Delta G_{\rm gas}(1 \text{ atm}) + RT \ln(24.46).$$
 (7)

Using these values, the pK_a values using the first thermodynamic cycle are given by Eq. (8):

$$pK_a = [G(A^-_{gas}) - G(AH_{gas}) + \Delta G_s(A^-) - \Delta G_s(AH) - 269.0]/1.3644.$$
 (8)

The pK_a 's calculated with cycle 2 used Eq. (9):

$$pK_{a} = \left[G(H_{3}O^{+}_{gas}) - G(A^{-}_{gas}) - G(AH_{gas}) - G(H_{2}O_{gas}) + \Delta G_{s}(H_{3}O^{+}) + \Delta G_{s}(A^{-}) - \Delta G_{s}(AH) - \Delta G_{s}(H_{2}O)\right]/1.3644 - 1.74303,$$
(9)

where we have subtracted the log of the water concentration at 298 K to convert pK for cycle 2 to p K_a . The p K_a 's calculated with cycle 3 used Eq. (10):

$$pK_a = \left[G(H_3O^+_{gas}) - G(A^-_{gas}) - G(AH_{gas}) - G(H_2O_{gas}) + \Delta G_s(H_3O^+) + \Delta G_s(A^-) - \Delta G_s(AH) + 2.05 \right] / 1.3644 - 1.74303,$$
(10)

where ΔG_{vap} is 2.05 kcal/mol.

The p K_a 's calculated with cycle 4 used Eq. (11):

$$pK_a = [G(H_3O^{+}_{gas}) - G(A^{-}_{gas}) - G(AH_{gas}) - G(H_2O_{gas}) + \Delta G_s(H_3O^{+}) + \Delta G_{relax}(H_3O^{+})$$

+
$$\Delta G_{\rm s}({\rm A}^{-})$$
 + $\Delta G_{\rm relax}({\rm A}^{-})$ - $\Delta G_{\rm s}({\rm AH})$
- $\Delta G_{\rm relax}({\rm AH})$ + 2.05]/1.3644 - 1.74303. (11)

Results

The conformers of the carboxylic acids are displayed in Figure 1, along with the experimental pK_a 's of each acid. The conformationally averaged ΔG_s values for the six carboxylic acids and their anions, obtained using the CBS-QB3 gasphase and CPCM solvation methods, are given in Table I [30]. CPCM/6-31G(d)//HF/6-31G(d), CPCM/6-31+G(d)//HF/6-31+G(d) are denoted **S1**, **S2**, and **S3**, respectively. Table II contains the previously reported calculated pK_a 's and mean unsigned errors from thermodynamic cycle 1 and Eq. (8) [30]. Table III contains the calculated pK_a 's and errors

FIGURE 1. Experimental pK_a values and structures of the conformers of acetic, chloroacetic, cyanoacetic, formic, oxalic, and pivalic acids.

	Acetic	Formic	Cyanoacet	tic Chloro	acetic	Oxalic	Pivalic	Water
S1 S2 S3	-6.93 -7.65 -7.72	-7.39 -8.38 -8.43	-13.24 -14.32 -14.52	_9. _10. _10.	.56	-11.56 -12.58 -12.73	-5.97 -6.70 -6.78	-6.37 -7.26 -7.23
	Acetate	Formate	Cyanoacetate	Chloroacetate	Oxalate	Pivalate	H ^{+ c}	H_3O^{+d}
S1 S2 S3	-76.58 -77.18 -77.58	-76.15 -76.58 -77.10	-68.72 -69.51 -69.99	-69.48 -70.11 -70.57	-74.92 -75.35 -75.72	-71.04 -71.97 -72.42	-264.61 -264.61 -264.61	-104.00 -104.00 -104.00

a From Ref. [30].

when using thermodynamic cycle 2 and Eq. (9), with all values calculated using one of the five gas-phase methods and one of the three solvation procedures. Table IV contains the calculated pK_a 's and errors from thermodynamic cycle 3 and Eq. (10). Table V contains the calculated pK_a 's and errors from thermodynamic cycle 4 and Eq. (11). This cycle differs from cycle 3 only in that the gas-phase geometries are allowed to relax in solution, a procedure first used by Nascimento and co-workers [21, 28]. Table VI contains a pK_a error analysis of each of five gas-phase computational methods combined with three condensed-phase methods, for each of the four thermodynamic cycles.

Discussion

REVIEW OF PREVIOUS WORK USING THERMODYNAMIC CYCLE 1

Table I contains the previously reported conformationally averaged values for ΔG_s . The previously reported [30] absolute p K_a values are presented in Table II for thermodynamic cycle 1 using the values in Table I and the previously reported [29] values for $G_{\rm gas}$ for the acids and the anions. The value of -6.28 comes from the Sackur–Tetrode equation [66] to evaluate the entropy combined with inclusion of translational energy at 298 K [67]. The value for $\Delta G_s({\rm H^+})$ was obtained using the average of three published experimental values for the gas-phase dissociation of acetic acid in thermodynamic cycle 1 [61–63] the experimental ΔG_s values

for acetic acid (-6.69 kcal/mol) and acetate ion (-77 kcal/mol) [68], and the experimental value for $\Delta G_{\rm aq}$ (2.303RT p $K_a = 6.48$ kcal/mol) [69].

The CBS-QB3 gas-phase method and the S1 solvation procedure predict absolute pK_a values of 5.34, 3.47, 2.33, 3.44, 0.92, and 5.60 for acetic, formic, cyanoacetic, chloroacetic, oxalic, and pivalic acids, respectively (Table II) [30]. The largest deviation is $0.59 \text{ p}K_a$ units, and the mean unsigned error (MUE) for the six acids is $0.41 \text{ p} K_a$ units using this combination of gas-phase and condensed phase methods. Using the CBS-QB3 gas-phase method, the S2 solvation procedure gives a MUE for the six acids of 0.37 p K_a units, while S3 solvation gives a MUE of $0.24 \,\mathrm{p} K_a$ units. Results for the other gas-phase methods are similar. The CBS-APNO method is quite accurate, although it failed for one conformer of pivalic acid [70]. The G2 gas-phase methods and the S1, S2, and S3 solvation methods were reliable for all but pivalic acid. The G3 method combined with the S1, S2, and S3 solvation methods were least accurate for chloroacetic, oxalic, and pivalic acids.

A key problem for previous workers trying to make absolute pK_a predictions is the value to use for $\Delta G_s(H^+)$ [30, 71, 72]. The difference between the recalculated value of -264 kcal/mol of Tissandier et al. [72] and the commonly used values of -259.5 to -262.5 kcal/mol is in itself enough to make the error in calculated absolute pK_a calculations as large as one to three pK_a units. We derived a value of -264.6 kcal/mol from the experimental thermodynamic cycle of acetic acid, where all quantities are known except for $\Delta G_s(H^+)$. As Table II shows, the

 $^{^{}b}$ S1 = CPCM/HF/6-31G(d)//HF/6-31G(d); S2 = CPCM/HF/6-31+G(d)//HF/6-31G(d); S3 = CPCM/HF/6-31+G(d)//HF/6-31+G(d).

^c From experimental values for acetic acid, see text for details.

d Experimental value, Ref. [74].

TABLE II $_$ p K_a values using CBS and Gaussian-n models, CPCM solvation calculations, and cycle 1. a,b

\$2	Ac	etic acid p	$K_a = 4$	1.75	Fo	rmic acid į	oKa =	3.75	Cyan	oacetic ac	id p <i>K</i> a	= 2.45
\$1	Solvation	$\Delta\Delta G_{sol}$	p <i>K</i> a	Difference	Solvation	$\Delta\Delta G_{sol}$	р <i>К</i> а	Difference	Solvation	$\Delta\Delta G_{sol}$	p <i>K</i> a	Difference
\$2				_		CBS-C	QB3					
S3	S1	-334.26	5.34	0.59	S1	-333.37	3.47		S1	-320.09	2.33	-0.12
CBS-APNO S1 -334.26 5.06 0.31 S1 -333.37 3.86 0.11 S1 -320.09 2.31 -0.14 S2 -334.47 4.91 0.16 S3 -332.28 3.93 0.18 S3 -320.09 2.31 -0.14 S1 -334.26 4.59 -0.16 S1 -333.37 3.29 -0.46 S1 -320.09 1.97 -0.41 S2 -334.14 4.67 -0.08 S2 -332.81 3.70 -0.05 S2 -319.80 2.18 -0.2 S3 -334.47 4.43 -0.32 S3 -333.28 3.35 -0.40 S3 -320.09 2.26 -0.18 S1 -334.26 4.87 0.12 S1 -333.37 3.63 -0.12 S1 -320.09 2.26 -0.18 S2 -334.14 4.96 0.21 S2 -332.73 3.63 -0.10 S3 -320.09 2.26												0.09
\$1	S3	-334.47	5.19	0.44	S3	-333.28	3.53	-0.22	S3	-320.08	2.34	-0.11
\$\frac{\text{S2}}{\text{S3}} - 334.47 \ \ \frac{\text{5.15}}{\text{ 0.40}} \ \ \text{S2} \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \						CBS-A	PNO					
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$												-0.14
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$												0.07
S1 -334.26 4.59 -0.16 S1 -333.37 3.29 -0.46 S1 -320.09 1.97 -0.44 S2 -334.14 4.67 -0.08 S2 -332.28 1.370 -0.05 S2 -319.80 2.18 -0.21 CBMP2 S1 -334.26 4.87 0.12 S1 -333.37 3.63 -0.12 S1 -320.09 2.26 -0.15 S2 -334.47 4.96 0.21 S2 -332.81 4.04 0.29 S2 -319.80 2.48 0.01 G3 G3 C32 C33.28 4.23 0.48 S3 -320.08 2.60 0.19	S3	-334.47	4.91	0.16	S3	-333.28	3.93	0.18	S3	-320.08	2.31	-0.14
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$						G2	<u>!</u>					
\$\begin{array}{c c c c c c c c c c c c c c c c c c c												-0.48
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$												-0.27
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	S3	-334.47	4.43	-0.32	S3	-333.28	3.35	-0.40	S3	-320.08	1.97	-0.48
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$						G2M	P2					
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$			_							-320.09	2.26	-0.19
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$												0.03
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	S3	-334.47	4.72	-0.03	S3	-333.28	3.70	-0.05	S3	-320.08	2.27	-0.18
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$						G3	3					
\$\begin{array}{c c c c c c c c c c c c c c c c c c c												0.15
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$												0.37
CBS-QB3 \$1	S3	-334.47	5.07	0.32	S3	-333.28	4.23	0.48	S3	-320.08	2.61	0.16
S1 -324.42 3.44 0.59 S1 -327.97 0.92 -0.31 S1 -329.68 5.60 0.55 S2 -324.16 3.63 0.78 S2 -327.38 1.36 0.13 S2 -329.88 5.46 0.44 CBS-APNO Method not available for chlorine S1 -327.97 1.24 0.01 See Ref. [70] G2 G2 G2 G2 S1 -327.97 1.15 -0.08 S1 -329.68 6.51 1.44 G2 G2 S1 -324.42 3.21 0.36 S1 -327.97 1.15 -0.08 S1 -329.68 6.51 1.44 S2 -324.16 3.40 0.55 S2 -327.38 1.58 0.35 S2 -329.88 6.37 1.33 G2MP2 S1	Chlor	oacetic ac	id p <i>K</i> a	= 2.85	O	xalic acid p	$K_a = 1$	1.23	Pi	valic acid p	$oK_a = 1$	5.03
S2 -324.16 3.63 0.78 S2 -327.38 1.36 0.13 S2 -329.88 5.46 0.43 CBS-APNO Method not available for chlorine S1 -327.97 1.24 0.01 See Ref. [70] G2 S1 -327.97 1.15 0.08 S1 -329.68 6.51 1.44 S2 -324.42 3.21 0.36 S1 -327.97 1.15 -0.08 S1 -329.68 6.51 1.44 S2 -324.16 3.40 0.55 S2 -327.38 1.58 0.35 S2 -329.88 6.37 1.34 G2MP2 S1 -324.42 3.49 0.64 S1 -327.97 1.52 0.29 S1 -329.68 6.76 1.73 S2 -324.16 3.68 0.83 S2 -327.38 1.95 0.72 S2 -329.88 6.62 1.58 S3 -324.53 3.41 0.56 S3 -327.6						CBS-C	QB3					
S3	S1	-324.42	3.44	0.59		-327.97	0.92	-0.31		-329.68	5.60	0.57
CBS-APNO Method not available for chlorine S1												0.43
Method not available for chlorine S1	S3	-324.53	3.36	0.51	S3	-327.60	1.20	-0.03	S3	-330.25	5.19	0.16
\$2						CBS-A	PNO					
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	Method	l not availa	ble for	chlorine				0.01		See Ref	f. [70]	
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$												
\$1					S3	-327.60	1.51	0.28				
S2 -324.16 3.40 0.55 S2 -327.38 1.58 0.35 S2 -329.88 6.37 1.34 S3 -324.53 3.13 0.28 S3 -327.60 1.42 0.19 S3 -330.25 6.10 1.01 G2MP2 S1 -324.42 3.49 0.64 S1 -327.97 1.52 0.29 S1 -329.68 6.76 1.73 S2 -324.16 3.68 0.83 S2 -327.38 1.95 0.72 S2 -329.88 6.62 1.56 S3 -324.53 3.41 0.56 S3 -327.60 1.79 0.56 S3 -330.25 6.34 1.33						G2	2					
\$\begin{array}{c ccccccccccccccccccccccccccccccccccc	S1	-324.42	3.21	0.36	S1				S1	-329.68	6.51	1.48
G2MP2 \$1												1.34
S1 -324.42 3.49 0.64 S1 -327.97 1.52 0.29 S1 -329.68 6.76 1.73 S2 -324.16 3.68 0.83 S2 -327.38 1.95 0.72 S2 -329.88 6.62 1.59 S3 -324.53 3.41 0.56 S3 -327.60 1.79 0.56 S3 -330.25 6.34 1.33	S3	-324.53	3.13	0.28	S3	-327.60	1.42	0.19	S3	-330.25	6.10	1.07
S2 -324.16 3.68 0.83 S2 -327.38 1.95 0.72 S2 -329.88 6.62 1.50 S3 -324.53 3.41 0.56 S3 -327.60 1.79 0.56 S3 -330.25 6.34 1.30						G2M	P2					
S3 -324.53 3.41 0.56 S3 -327.60 1.79 0.56 S3 -330.25 6.34 1.3												1.73
												1.59
(Continued)	S3	-324.53	3.41	0.56	S3	-327.60	1.79	0.56	S3	-330.25	6.34	1.31
						(Contin	ued)					

TABLE II ___ (Continued).

Solvation	$\Delta\Delta G_{sol}$	р <i>Ка</i>	Difference	Solvation	$\Delta\Delta G_{sol}$	р <i>Ка</i>	Difference	Solvation	$\Delta\Delta G_{sol}$	р <i>Ка</i>	Difference
					G3	3					
S1	-324.42	3.69	0.84	S1	-327.97	1.99	0.76	S1	-329.68	7.06	2.03
S2	-324.16	3.88	1.03	S2	-327.38	2.42	1.19	S2	-329.88	6.91	1.88
S3	-324.53	3.61	0.76	S3	-327.60	2.26	1.03	S3	-330.25	6.64	1.61

a From Ref. [30].

correct value for $\Delta G_s(H^+)$ must be in the range of -264 kcal/mol [30].

The Sackur–Tetrode equation [66] was used to evaluate the entropy, $G(H^+)$, which yields a value of -7.76 kcal/mol for TS(H^+) at 298 K and 1 atm pressure. Including translational energy, the total gasphase free energy of the proton is -6.28 kcal/mol at 298 K [67].

THERMODYNAMIC CYCLE 2

Table III contains the results of pK_a calculations using thermodynamic cycle 2 and Eq. (9). None of the methods are accurate. The MUE in pK_a ranges from 2.4 to 5.3 p K_a units. It is no surprise that previous workers who have used cycle 2 have reported that quantitative prediction of absolute pK_a values are not possible [13, 20, 24]. We can assess the quality of this cycle by using available experimental numbers. Using acetic acid, where $\Delta G_s(AH)$ is -6.7 kcal/mol [65], $\Delta G_s(A^-)$ is -77.0kcal/mol [65], $\Delta G_s(H_2O)$ is -6.3 kcal/mol [73], and $\Delta G_s(H_3O^+)$ is -104 kcal/mol [74], $\Delta \Delta G_{sol}$ has a value of -168.1 kcal/mol. Combining this value with the computed value for ΔG_{gas} for the top line in cycle 2 will give us an estimate for the value for ΔG_{aq} , which can be compared to the same value as that determined from the pK_a . If the data in the thermodynamic cycle were accurate, one would get the same value for ΔG_{aq} as determined from the p K_a . Acetic acid has a p K_a of 4.75, so ΔG_{aq} is 6.48 kcal/mol.

Using the CBS-QB3 calculated values for acetic acid (-228.792813 hartrees), water (-76.355104 hartrees), acetate anion (-228.241528 hartrees), and H_3O^+ (-76.615647 hartrees), the CBS-QB3 $\Delta G_{\rm gas}$ value is 182.4 kcal/mol. Combining the CBS-QB3 value for $\Delta G_{\rm gas}$ and the experimental value for $\Delta \Delta G_{\rm sol}$ yields 13.4 kcal/mol for the value of $\Delta G_{\rm aq}$ determined from cycle 2, which is higher than $\Delta G_{\rm aq}$ obtained directly from the experimental p K_a by

about 7 kcal/mol. If we use the $\Delta G_{\rm s}$ numbers calculated with the **S3** procedure (-106.27, -77.58, -7.72, and -7.23 for ${\rm H_3O^+}$, acetate ion, acetic acid, and water, respectively), then $\Delta\Delta G_{\rm sol}$ is -168.9, with no improvement in $\Delta G_{\rm aq}$.

Where is the error? Our previous work showed that relative pK_a calculations for these same carboxylic acids were quite accurate, and in these calculations the subtraction of one thermodynamic cycle from another meant that the results from using either thermodynamic cycle 1 or thermodynamic cycle 2 would be equivalent [29]. In relative pK_a calculations the only unique numbers are the gas-phase values G_{gas} for each acid and its corresponding anion, and the ΔG_s values for each acid and each anion. The values for $G(H^+_{gas})$ and $\Delta G_s(H^+)$ in thermodynamic cycle 1, and $G(H_3O_{gas})$, $G(H_3O^+_{gas})$, $\Delta G_s(H_3O^+)$, and $\Delta G_s(H_2O)$ in thermodynamic cycle 2, all cancel in relative pK_a calculations. The error in using thermodynamic cycle 2 for absolute pK_a calculations must therefore be in one or more or the following terms: $G(H_2O_{gas})$, $G(H_3O_{gas}^+)$, $\Delta G_s(H_3O_-^+)$, or $\Delta G_s(H_2O)$. Nascimento and co-workers have suggested that the error is in $\Delta G_s(H_2O)$ [21, 28]. They reason that the thermodynamic definition of solvent energy [73, 78] is inappropriate when the solute and the solvent are the same species, as a solvated water molecule is indistinguishable from any other water molecule [28]. They proposed that it would be more appropriate to identify the transformation of water in the thermodynamic cycle with the vaporization process, and that using $\Delta G_s(H_2O)$ instead of $\Delta G_{\text{vap}}(H_2O)$ in the cycle represents a source of error that leads to an overestimation of pK_a values [21]. They have used thermodynamic cycle 4 for their work on carboxylic acids [21] and aliphatic acids, thiols, and halogenated carboxylic acids [28]. We will describe how their cycle, and a modified cycle, works with our calculations in the next section.

 $^{^{}b}$ S1 = CPCM/HF/6-31G(d)//HF/6-31G(d); S2 = CPCM/HF/6-31+G(d)//HF/S-31G(d); S3 = CPCM/HF/6-31+G(d)//HF/6-31+G(d).

TABLE III $_{\rm p}K_a$ values using CBS and Gaussian-n models, CPCM solvation calculations, and cycle 2. $^{\rm a}$

	Acetic	acid			Formic	acid			Cyanoace	etic aci	<u></u>
Solvation	$\Delta\Delta G_{sol}$	p <i>K</i> a	Difference	Solvation	$\Delta\Delta G_{sol}$	p <i>K</i> a	Difference	Solvation	$\Delta\Delta G_{sol}$	p <i>K</i> _a	Difference
					CBS-Q	B3					
S1	-167.28	9.37	4.62	S1	-166.39		3.75	S1	-153.11	6.36	3.91
S2	-166.27	10.11	5.36	S2	-164.94		4.81	S2	-151.93	7.22	4.77
S3	-166.63	9.85	5.10	S3	-165.44	8.19	4.44	S3	-152.24	7.00	4.55
					CBS-AF	ON					
S1	-167.28	8.21	3.46	S1	-166.39	7.01	3.26	S1	-153.11		3.00
S2	-166.27	8.95	4.20	S2	-164.94		4.32	S2	-151.93		3.86
S3	-166.63	8.68	3.93	S3	-165.44	7.70	3.95	S3	-152.24	6.09	3.64
					G2						
S1	-167.28	8.22	3.47	S1	-166.39		3.17	S1	-153.11		3.15
S2	-166.27	8.96	4.21	S2	-164.94		4.24	S2	-151.93		4.02
S3	-166.63	8.70	3.95	S3	-165.44	7.62	3.87	S3	-152.24	6.24	3.79
					G2MF	2					
S1	-167.28	8.51	3.76	S1	-166.39	7.27	3.52	S1	-153.11		3.45
S2	-166.27	9.25	4.50	S2	-164.94		4.58	S2	-151.93		4.31
S3	-166.63	8.98	4.23	S3	-165.44	7.96	4.21	S3	-152.24	6.53	4.08
					G3						
S1	-167.28	8.61	3.86	S1	-166.39		3.80	S1	-153.11	5.99	3.54
S2	-166.27	9.35	4.60	S2	-164.94		4.87	S2	-151.93		4.41
S3	-166.63	9.09	4.34	S3	-165.44	8.25	4.50	S3	-152.24	6.63	4.18
	Chloroac	etic acio	t		Oxalic	acid			Pivalic	acid	
					CBS-Q	B3					
S1	-157.44	7.47	4.62	S1	-160.99	4.95	3.72	S1	-162.70	9.63	4.60
S2	-156.29	8.31	5.46	S2		6.04	4.81	S2	-162.01	10.14	5.11
S3	-156.69	8.02	5.17	S3	-159.76	5.86	4.63	S3	-162.41	9.84	4.81
					CBS-AF	ON					
				S1	-160.99	4.38	3.15				
				S2	-159.51	5.47	4.24				
				S3	-159.76	5.29	4.06				
					G2						
S1	-157.44	6.85	4.00	S1	-160.99	4.79	3.56	S1	-162.70		5.12
S2	-156.29	7.69	4.84	S2	-159.51	5.87	4.64	S2	-162.01		5.63
S3	-156.69	7.40	4.55	S3	-159.76	5.69	4.46	S3	-162.41	10.36	5.33
					G2MF	2					
S1	-157.44	7.13	4.28	S1	-160.99		3.92	S1	-162.70		5.37
S2	-156.29	7.97	5.12	S2	-159.51	6.23	5.00	S2	-162.01		5.87
S3	-156.69	7.68	4.83	S3	-159.76	6.05	4.82	S3	-162.41	10.61	5.58
					(Continu	ued)					

TABLE III __ (Continued).

Solvation	$\Delta\Delta G_{sol}$	p <i>K</i> a	Difference	Solvation	$\Delta\Delta G_{sol}$	p <i>K</i> a	Difference	Solvation	$\Delta\Delta G_{sol}$	p <i>K</i> a	Difference
					G3						
S1	-157.44	7.08	4.23	S1	-160.99	5.38	4.15	S1	-162.70	10.45	5.42
S2	-156.29	7.93	5.08	S2	-159.51	6.46	5.23	S2	-162.01	10.96	5.93
S3	-156.69	7.63	4.78	S3	-159.76	6.28	5.05	S3	-162.41	10.66	5.63

^a S1 = CPCM/HF/6-31G(d)//HF/6-31G(d); S2 = CPCM/HF/6-31+G(d)//HF/6-31G(d); S3 = CPCM/HF/6-31+G(d)//HF/6-31+G(d).

THERMODYNAMIC CYCLES 3 AND 4

Thermodynamic cycle 3 is the same as cycle 2, except with $-\Delta G_s(H_2O)$ replaced by $\Delta G_{vap}(H_2O) =$ 2.05 kcal/mol [77]. Table IV contains the results of using cycle 3 and Eq. (10). The improvement over cycle 2 is dramatic, and we see that simply replacing the free energy of solvation of water with the free energy of vaporization gives reasonable predictions of the pK_a 's of most of the molecules with most of the methods. The Gaussian-n models do not work well for pivalic acid, where the MUEs exceed 1 p K_a unit. Overall the results are not as good as those for cycle 1 (Table II) but are clearly superior to those for cycle 2 (Table III). Clearly, replacing $\Delta G_s(H_2O)$ of -6.3 kcal/mol with $\Delta G_{vap}(H_2O)$ of 2.053 kcal/mol leads to a dramatic improvement in calculating pK_a 's when using a cycle that includes an explicit water.

Table V contains the results of using cycle 4 and Eq. (11). In this cycle we have included the relaxation energy obtained by a CPCM/HF/6-31G(d) S1 geometry optimization of each molecule in aqueous solution. Nascimento and co-workers have argued that inclusion of this term in their work was responsible for the accuracy of their pK_a calculations [21, 28]. However, we find that inclusion of geometry relaxation for these carboxylic acids has little effect but tends to make the calculated pK_a 's more negative. Geometry optimization results in lower pK_a values, so that whenever cycle 3 gives results that are too positive (such as CBS-QB3 and S1 for acetic acid) then the pK_a values are improved by geometry optimization in aqueous solution. The exception to the trend is for formic acid, where the pK_a values increase for all methods. This is a consequence of the small size of formic acid and formate anion, so that the relaxation energy is very small for these two species and the overall $\Delta \Delta G_{sol}$ is dominated by the $\Delta G_s(H_3O^+)$ term.

STANDARD STATES AND FREE ENERGIES OF VAPORIZATION AND SOLVATION

We have seen that using a value for ΔG_{vap} of 2.053 kcal/mol works in cycles 3 and 4 while using a value for ΔG_s of -6.3 kcal/mol does not work for cycle 2. The discrepancy between

$$H_2O(1,298.15 \text{ K}) \rightarrow H_2O(g,298.15 \text{ K}),$$

 $\Delta G_{\text{vap}} = 2.053 \text{ kcal/mol}$

and

$$H_2O(g, 298.15 \text{ K}) \rightarrow H_2O(l, 298.15 \text{ K}),$$

 $\Delta G_s = -6.3 \text{ kcal/mol}$

must be investigated. The standard state for a pure liquid or solid is the substance in the condensed phase under a pressure of one atmosphere [77]. The values for ΔG_f^0 listed in the tables in the *CRC* Handbook of Chemistry and Physics [77] represent the change in the appropriate thermodynamic quantity when one gram-formula weight of the substance in its standard state is formed isothermally at the indicated temperature from the elements, each in its appropriate reference state. This means that $\Delta G_f^0[H_2O(l, 298.15 \text{ K})]$ in the CRC Handbook has a standard state of 55.53 M and $\Delta G_f^0[H_2O(g,$ 298.15 K)] has a standard state of 1 atm. Using the free energies of formation of liquid and gaseous water yields the value of 2.053, when the reference state is 55.53 M, 298.15 K for liquid water and 1 atm, 298.15 K for water vapor. Winget et al. have pointed out that the relationship between intermolecular interactions and free energies of transfer between phases is most direct if one uses the same standard concentration for both phases [78]. This is most often a standard state of one mole per liter for both the gas- and liquid-phase components, which is the standard state that we have tried to use in our thermodynamic cycles. Converting $\Delta G_{\rm M}$ from a standard state of H₂O(l, 298.15 K, 55.53 M) and

TABLE IV $_$ p K_a values using CBS and Gaussian-n models, CPCM solvation calculations, and cycle 3. a

	Acetic	acid			Formic	acid			Cyanoace	etic aci	d
Solvation	$\Delta\Delta G_{sol}$	p <i>K</i> _a	Difference	Solvation	$\Delta\Delta G_{sol}$	p <i>K</i> _a	Difference	Solvation	$\Delta\Delta G_{sol}$	p <i>K</i> a	Difference
					CBS-C	QB3					
S1 S2 S3	-171.60 -171.48 -171.81	6.20 6.29 6.05	1.45 1.54 1.30	S1 S2 S3	-170.71 -170.15 -170.62	4.74	0.58 0.99 0.65	S1 S2 S3	-157.43 -157.14 -157.42	3.40	0.74 0.95 0.75
					CBS-A	PNO					
S1 S2 S3	-171.60 -171.48 -171.81	5.04 5.13 4.89	0.29 0.38 0.14	S1 S2 S3	-170.71 -170.15 -170.62	4.25	0.09 0.50 0.16	S1 S2 S3	-157.43 -157.14 -157.42	2.50	-0.17 0.05 -0.16
					G2						
S1 S2 S3	-171.60 -171.48 -171.81	5.06 5.14 4.90	0.31 0.39 0.15	S1 S2 S3	-170.71 -170.15 -170.62	4.17	0.01 0.42 0.07	\$1 \$2 \$3	-157.43 -157.14 -157.42	2.65	-0.01 0.20 -0.01
					G2M	P2					
S1 S2 S3	-171.60 -171.48 -171.81	5.34 5.43 5.19	0.59 0.68 0.44	S1 S2 S3	-170.71 -170.15 -170.62	4.51	0.35 0.76 0.42	S1 S2 S3	-157.43 -157.14 -157.42	2.94	0.28 0.49 0.29
					G3						
S1 S2 S3	-171.60 -171.48 -171.81	5.45 5.54 5.29	0.70 0.79 0.54	S1 S2 S3	-170.71 -170.15 -170.62	4.80	0.64 1.05 0.70	S1 S2 S3	-157.43 -157.14 -157.42	3.04	0.38 0.59 0.39
	Chloroace	etic aci	d		Oxalic	acid			Pivalic	acid	
				-	CBS-C	QB3					
S1 S2 S3	-161.76 -161.50 -161.87	4.30 4.49 4.22	1.45 1.64 1.37	S1 S2 S3	-165.31 -164.72 -164.94	2.22	0.56 0.99 0.83	S1 S2 S3	-167.02 -167.22 -167.59	6.32	1.44 1.29 1.02
					CBS-A	PNO					
				S1 S2 S3		1.22 1.65 1.49	-0.01 0.42 0.26				
					G2						
S1 S2 S3	-161.76 -161.50 -161.87	3.68 3.87 3.60	0.83 1.02 0.75	S1 S2 S3	-165.31 -164.72 -164.94		0.39 0.82 0.66	S1 S2 S3	-167.02 -167.22 -167.59	6.84	1.95 1.81 1.54
					G2M	P2					
S1 S2 S3	-161.76 -161.50 -161.87	3.96 4.15 3.88	1.11 1.30 1.03	S1 S2 S3	-165.31 -164.72 -164.94		0.75 1.19 1.03	S1 S2 S3	-167.02 -167.22 -167.59	7.08	2.20 2.05 1.78
					(Contin	ued)					

TABLE IV _

(Continued).

	<u> </u>										
Solvation	$\Delta\Delta G_{sol}$	р <i>Ка</i>	Difference	Solvation	$\Delta\Delta G_{sol}$	р <i>К</i> а	Difference	Solvation	$\Delta\Delta G_{sol}$	р <i>К</i> а	Difference
					G3	}					
S1	-161.76	3.92	1.07	S1	-165.31	2.21	0.98	S1	-167.02	7.29	2.26
S2	-161.50	4.11	1.26	S2	-164.72	2.64	1.41	S2	-167.22	7.14	2.11
S3	-161.87	3.84	0.99	S3	-164.94	2.48	1.25	S3	-167.59	6.87	1.84

 $^{^{}a}\,\textbf{S1} = \text{CPCM/HF/6-31G(d)//HF/6-31+G(d)//HF/6-G(d)$

TABLE V ____

pKa values using CBS and Gaussian-n models, CPCM solvation calculations, and cycle 4.a

	Acetic	acid			Formic	acid		Cyanoacetic acid			
Solvation	$\Delta\Delta G_{sol}$	р <i>К</i> а	Difference	Solvation	$\Delta\Delta G_{sol}$	р <i>К_а</i>	Difference	Solvation	$\Delta\Delta G_{sol}$	p <i>K</i> a	Difference
					CBS-C	QB3					_
S1	-172.44	5.59	0.84	S1	-170.45	4.52	0.77	S1	-158.25	2.59	0.14
					CBS-AI	PNO					
S1	-172.48	4.40	-0.35	S1	-170.26	4.17	0.42	S1	-158.25	1.68	-0.77
					G2						
S1	-172.48	4.41	-0.34	S1	-170.23	4.11	0.36	S1	-158.25	1.84	-0.61
					G2M	P2					
S1	-172.48	4.69	-0.06	S1	-170.24	4.44	0.69	S1	-158.25	2.13	-0.32
					G3						
S1	-172.47	4.81	0.06	S1	-170.29	4.70	0.95	S1	-158.25	2.23	-0.22
	Chloroace	tic aci	d		Oxalic	acid			Pivalic	acid	
					CBS-C	QB3					
S1	-162.51	3.75	0.90	S1	-166.45	0.95	-0.28	S1	-167.96	5.78	0.75
					CBS-AI	PNO					
				S1	-166.09	0.65	-0.58				
					G2						
S1	-162.65	3.03	0.18	S1	-166.45	0.79	-0.44	S1	-168.02	6.25	1.22
					G2M	P2					
S1	-162.64	3.32	0.47	S1	-166.44	1.16	-0.07	S1	-168.03	6.49	1.46
					G3						
S1	-162.69	3.24	0.39	S1	-166.42	1.40	0.17	S1	-168.01	6.56	1.53

 $^{^{}a}\,\textbf{S1} = \text{CPCM/HF/6-31G(d)//CPCM/HF/6-31G(d)}.$

G_{gas}	$\Delta\Delta G_{sol}$	MSE	MUE	STDEV	G_{gas}	$\Delta\Delta G_{sol}$	MSE	MUE	STDEV
-	Thermodyn	amic cycle	e 1			Thermody	namic cycl	e 2	
CBS-QB3	S1	0.17	0.41	0.49	CBS-QB3	S1	4.20	4.20	4.63
CBS-QB3	S2	0.37	0.37	0.51	CBS-QB3	S2	5.05	5.05	5.54
CBS-QB3	S3	0.12	0.24	0.33	CBS-QB3	S3	4.78	4.78	5.25
CBS-APNO	S1	0.07	0.15	0.21	CBS-APNO	S1	3.22	3.22	3.72
CBS-APNO	S2	0.36	0.36	0.46	CBS-APNO	S2	4.15	4.15	4.80
CBS-APNO	S3	0.12	0.19	0.23	CBS-APNO	S3	3.89	3.89	4.50
G2	S1	0.11	0.51	0.75	G2	S1	3.75	3.75	4.17
G2	S2	0.31	0.44	0.68	G2	S2	4.60	4.60	5.07
G2	S3	0.06	0.46	0.59	G2	S3	4.33	4.33	4.77
G2MP2	S1	0.41	0.51	0.84	G2MP2	S1	4.05	4.05	4.49
G2MP2	S2	0.61	0.61	0.88	G2MP2	S2	4.90	4.90	5.39
G2MP2	S3	0.36	0.45	0.69	G2MP2	S3	4.63	4.63	5.10
G3	S1	0.78	0.78	1.08	G3	S1	4.17	4.17	4.61
G3	S2	0.98	0.98	1.20	G3	S2	5.02	5.02	5.52
G3	S3	0.73	0.73	0.96	G3	S3	4.75	4.75	5.23
	Thermodyn	amic cycle	e 3			Thermody	namic cycl	e 4	
CBS-QB3	S1	1.04	1.04	1.22	CBS-QB3	S1	0.52	0.61	0.74
CBS-QB3	S2	1.23	1.23	1.39					
CBS-QB3	S3	0.99	0.99	1.12					
CBS-APNO	S1	0.05	0.14	0.20	CBS-APNO	S1	-0.32	0.53	0.64
CBS-APNO	S2	0.34	0.34	0.44					
CBS-APNO	S3	0.10	0.18	0.21					
G2	S1	0.58	0.58	0.98	G2	S1	0.06	0.53	0.68
G2	S2	0.78	0.78	1.04		-			
G2	S 3	0.53	0.53	0.82					
G2MP2	S1	0.88	0.88	1.20	G2MP2	S1	0.36	0.51	0.77
G2MP2	S2	1.08	1.08	1.31				-	
G2MP2	S 3	0.83	0.83	1.07					
G3	S1	1.00	1.00	1.28	G3	S1	0.48	0.55	0.83
G3	S2	1.20	1.20	1.42			-		
G3	S3	0.95	0.95	1.17					

 $\rm H_2O(g,298.15~K,1~atm)$, to a standard state of $\rm H_2O(l,298.15~K,1~M)$ and $\rm H_2O(g,298.15~K,1~M)$ can be achieved using Eq. (7), adding RT ln(24.46) to convert the water vapor reference state, and then by adding RT ln(55.5) to convert the liquid water reference state. Adding RT ln(24.46) and RT ln(55.5) to 2.053 yields 6.3 kcal/mol for the vaporization of water. Thus $\Delta G_{\rm vap}$ and $\Delta G_{\rm s}$ are the same numbers, but of opposite sign, as one would expect. Thus we are left with the conclusion that cycles 3 and 4 are get-

ting the right result for the wrong reason and that cycle 2 does not work. Further investigation into these cycles is warranted.

ERROR ANALYSIS

Table VI contains a summary of the errors obtained by each of the four thermodynamic cycles combined with the CBS and Gaussian-*n* gas phase and **S1**, **S2**, and **S3** solvation procedures, for the

five acids where ΔG_{gas} is known experimentally. This analysis reveals that the most accurate results for the absolute calculation of pK_a values for formic, acetic, cyanoacetic, chloroacetic, oxalic, and pivalic acids are obtained using CBS methods and cycle 1. Combining CBS-QB3 and CBS-APNO with the CPCM solvation methods S1, S2, and S3 yields MUEs less than 0.42 pK_a units and STDEVs less than $0.52 \text{ p}K_a$ units. Good results are also obtained with cycle 3 and all of the gas-phase and solvation methods, with MUEs ranging from 0.30 to 0.60 p K_a units and STDEVs ranging from 0.40 to 0.82 pKa units. Because of standard state problems, we believe that this agreement is fortuitous. Use of cycle 4, which includes geometry relaxation in solution using the S1 solvation procedure does not make much of a difference in the results. This finding makes sense since the CPCM method was parameterized based on gas phase geometries [50-58].

Overall the error analysis gives confidence that these methods can predict accurate pK_a values, with the CBS-QB3 and CBS-APNO methods accurate to less than half a pK_a unit when using thermodynamic cycle 1. Cycle 1 is more accurate than the other cycles as there are fewer terms (each term with its own uncertainty) in this cycle compared to cycles 2–4.

Conclusion

The CBS-QB3 [34] and CBS-APNO [35, 36] methods can be combined with CPCM [50] continuum solvation methods to calculate pK_a values for carboxylic acids accurate to within half a pK_a unit [30]. Thermodynamic cycles that include an explicit water in the cycle are not accurate when the free energy of solvation of a water molecule is used, but appear to become accurate when the experimental free energy of vaporization of water is used [21, 28]. However, this apparent agreement seems to be an artifact of the standard states used in considering ΔG_{vap} and ΔG_{s} . Geometry relaxation in solution does not improve the results. The reason why cycle 2 is not accurate is not readily apparent, but it is clear that cycle 1 has fewer terms, and each term adds to the error in the overall calculation of a p K_a value.

ACKNOWLEDGMENTS

We thank Steve Feldgus and Ed Sherer for helpful discussions. Acknowledgment is made to the donors of the Petroleum Research Fund, administered by the ACS, and to the NIH, and to Hamilton College for support of this work. M.D.L. acknowledges support from the Merck/AAAS Undergraduate Summer Research Program.

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pK_a CALCULATIONS ON CARBOXYLIC ACIDS

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