Transient Response Analysis via a Broadened Pulse Combined with a Step Change or an Isotopic Pulse. Application to CO₂ Reforming of Methane over NiO/SiO₂

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In this paper, a transient response analysis is developed by combining a broadened pulse with a step change or an isotopic pulse. The combined method provides information about the activation of the catalyst and the catalytic reaction mechanism. The method is applied to the CO_2 reforming of methane over NiO/SiO_2 at 800 °C. The response to the broadened CH_4/CO_2 (1:1) pulse over fresh NiO/SiO_2 exhibited an induction time during which no reaction between CH_4 and CO_2 occurred, indicating that NiO/SiO_2 had no activity. As the NiO was gradually reduced by CH_4 , the reforming reaction took place, indicating that Ni^0 is the active site for this reaction. During the transient response to a step change to He in the broadened pulse of CH_4/CO_2 over a reduced NiO/SiO_2 catalyst at 800 °C, a long CO tail was observed; however, no such tail was noted in the response after a step change to He in the broadened pure CO pulse at 800 °C. This indicates that the CO desorption is rapid and that the surface reaction between C and CO species constitutes the rate-determining step of the reforming reaction. The transient response to a sharp CO pulse introduced into the broadened CO pulse indicated that, over a reduced CO over a reduced CO replaced some CO in the reaction with CO generate CO and that some CO was oxidized to CO over CO replaced some CO in the reaction with CO generate CO and that some CO was oxidized to CO over CO replaced some CO in the reaction with CO generate CO and that some CO was oxidized to CO over CO replaced some CO in the reaction species reduce this CO over CO in the reaction species reduce this CO over CO over CO replaced to CO in the reaction species reduce this CO over CO replaced to CO indicates that CO over CO over CO in the reaction over CO over

1. Introduction

One of the most important uses of methane is in the preparation of synthesis gas. As for now, steam reforming is the dominant commercial method for producing synthesis gas.^{1,2} However, this process has a poor selectivity for CO and a too high H₂/CO product ratio, unsuitable for the methanol and the Fischer-Tropsch syntheses. Although the partial oxidation of methane can provide high activity and selectivity, and a suitable CO/H₂ ratio, 3-10 this process cannot be easily controlled due to the difficulty of removing the reaction heat from the reactor, particularly from large-scale equipment.^{11,12} Therefore, in recent years, renewed interest in methane conversion to synthesis gas via the CO₂ reforming reaction has arisen. 13-22 This pathway provides a high CO selectivity and a more suitable H₂/CO ratio. Recently, Ni-based catalysts with high selectivity and activity and excellent stability have been reported. 18-22 However, there are few investigations regarding the activation process of NiObased catalysts in the reactant atmosphere and the reaction mechanism.

Transient methods were often used in catalytic research to gain insight into the adsorption—desorption kinetics and the reaction mechanism. $^{23-28}$ They involve two kinds of techniques: the pulse technique, which provides unsteady-state information, and the step change, which provides information about the transient process from one steady state to another one. A steady-state tracing technique involving a step change in which one of the compounds is labeled with an isotope was also employed. However, in the common pulse techniques, the pulse width is $1-10^2$ s; it is about 1 ms in the temporal analysis of products (TAP) technique. It is, therefore, difficult to make a step change in the reactant or to introduce an isotopic sharp pulse during a regular pulse to investigate the catalytic process.

In this paper, a transient response analysis is developed which combines a broadened pulse with a step change in reactants or a sharp isotopic pulse which is injected any time in the broadened pulse. Using such a method, the CO_2 reforming of methane over NiO/SiO_2 catalyst is investigated.

2. Transient Response Analysis of the Broadened Pulse Combined with a Step Change or an Isotopic Pulse

Figure 1 shows how the broadening of the pulse was achieved. A gas pulse of 2.5 mL was injected almost instantaneously, using the six-way valve (5) and the sample tube (6), into a carrier gas (He) and allowed to flow via the four-way valve (7) into the broadening tube (8). In the latter tube, which has a diameter of 40 mm and a length of 164 mm, the pulse was broadened to about 20 min. From the broadening tube, the pulse flowed more slowly through the four-way valve (7) and then through the six-way valve (9) to the reactor and finally to the MS equipment. During the broadened pulse, a step change in the reactants, using the four-way valve (7), or a sharp isotopic pulse of 3 μ L, using the six-way valve (9) and the sample tube (10), was introduced at selected times of the broadened pulse. The reactant and products have been continuously detected with MS equipment (HP quadrupole, 5971 Series mass selective detector).

3. Experimental Section

- **3.1. Catalyst Preparation.** NiO/SiO₂ (containing 13.6 wt % Ni) catalysts were prepared by impregnating SiO₂ (Aldrich) with an aqueous solution of nickel nitrate (Alfa). The obtained paste was dried at room temperature in air and then decomposed and calcined at 800 °C in air for 1.5 h. The surface area and the pore size distribution of the catalyst were determined by nitrogen adsorption, using a Micromeritics ASAP 2000 instrument. The BET surface area and the average diameter of the pores were 362 m²/g and 52 Å, respectively.
- **3.2. Transient Response Analysis.** The transient experiments were performed at 800 °C under atmospheric pressure with the equipment presented in Figure 1. The catalyst powder (weight, 0.02 g) was held on quartz wool in a vertical quartz

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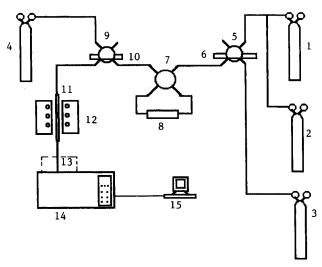


Figure 1. Transient response system: (1) CH₄/CO₂ (1:1) cylinder, (2) Ar cylinder, (3) He cylinder, (4) ¹⁸O₂ cylinder, (5) six-way valve, (6) sample tube, (7) four-way valve, (8) broadening tube, (9) six-way valve, (10) sample tube, (11) reactor, (12) electrical furnace, (13) inlet capillary system, (14) MS, (15) computer.

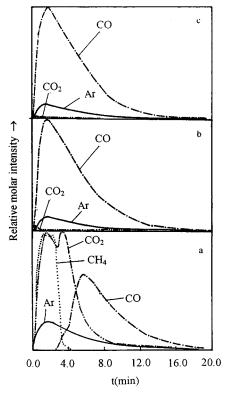


Figure 2. Responses of CH₄, CO₂, CO, and Ar as a function of time for broadened pulse of CH₄/CO₂/Ar (2.5 mL) over a fresh NiO/SiO₂ catalyst at 800 °C: (a) first pulse, (b) second pulse, and (c) third pulse.

tube reactor (2 mm i.d.) in an electronically controlled furnace of large heat capacity to keep the temperature constant. Helium (60 mL/min) was used as the carrier gas. The feed gas contained CO₂, CH₄ (CO₂/CH₄ 1:1), and 13.4% Ar as inner standard. The pulses were of 2.5 mL and 3 µL for the broadened reactant pulse and the short isotopic pulse, respectively.

4. Results and Discussion

4.1. Transient Response Analysis of the Broadened Pulse.

Figure 2 presents the response curves when only the broadened pulse is present; it contains the responses of three succesive pulses, each introduced after the previous one was exhausted. In the response curves of the first pulse, there are two peaks

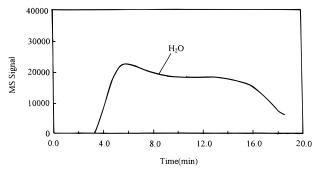


Figure 3. Response curve of H₂O as a function of time for the first broadened pulse of CH₄/CO₂/Ar (2.5 mL) in Figure 2.

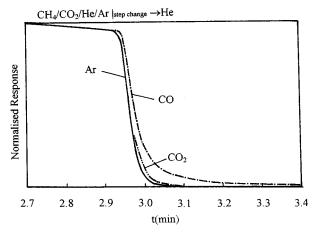


Figure 4. MS signal response curves of CO₂, CO, and Ar as a function of time for a broadened pulse of CH₄/CO/Ar combined with a step change to pure carrier (He) over NiO/SiO₂ subjected previously to 10 broadened succesive exhausted pulses.

for CO₂ at 1.8 and 3.5 min, a peak for CO at about 5.8min, and a peak for CH₄ at about 1.8 min. For the second pulse, there are very small peaks for CO₂ and CH₄ and a high one for CO. For the third pulse, the response is similar to the second one. This figure shows that the CO peak increases and the CO₂ peak decreases with increasing pulse number.

Figure 2 shows that, for the first pulse, the first CO₂ peak appears at the same position as the peaks of Ar and CH₄ and that no CO is present at that position. This indicates that the first CO₂ peak can be attributed to the CO₂ unreacted in the feed gas. The second CO2 peak appears after that of Ar (with a time difference of 1.8 min), at a time at which CH₄ is no longer present. It can, therefore, be attributed to the CH₄ reaction with NiO, which results in the formation of Ni⁰ and CO₂. It is worth noting that water was detected in the response curve after the first CO₂ peak but before the second CO₂ peak (Figure 3). This confirms that NiO is reduced by CH₄ to Ni⁰. Calculations based on the second CO₂ peak of Figure 2a indicate that about 44% of the NiO of the catalyst was reduced to Ni⁰. The CO peak appears after the second CO₂ peak, indicating that Ni⁰ constitutes the active site for the production of CO. This also explains why the response curve of CO exhibits an induction time and why CO increases and CO2 decreases with the pulse number (Figure 2).

4.2. Transient Response Analysis of the Broadened Pulse Combined with a Step Change. The response to a step change in the broadened CH₄/CO₂/Ar pulse was carried out over a catalyst previously subjected to 10 succesively exhausted CH₄/ CO₂ (1:1) pulses. Figure 4 shows that, when CH₄/CO₂/Ar/He is replaced via a step change with He, the CO2 response curve almost coincides with that of Ar, whereas the CO response curve has a long tail. The long tail of CO may be due to (a) the CO desorption from the catalyst surface or (b) the CO formation

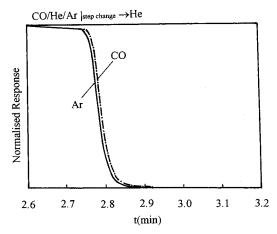


Figure 5. MS signal response curves of CO and Ar as a function of time for a broadened pulse of CO/Ar combined with a step change to pure carrier over NiO/SiO₂ subjected previously to 10 broadened succesively exhausted pulses.

by the surface reaction between the C and O species. To make a choice between the two, the response curve to a step change from CO/Ar/He to He in a broadened pulse of CO/Ar is presented in Figure 5, which shows that the CO response is near that of Ar. This eliminates the possibility (a) that the desorption of CO is responsible for the long tail; in other words, the long tail is due to the surface reaction between the C and O species, which constitutes the rate-determining step. In addition, the long CO tail also indicates that the C species cannot easily desorb. Consequently, the adsorbed species containing C cannot be CH_4 , because of its small adsorption energy (about 6 kcal/mol). It is, therefore, reasonable to suggest that a dissociative adsorption of CH_4 takes place, i.e., $CH_{4(g)} + Ni \rightarrow \cdots \rightarrow CH_{x(s)} + (4 - x)H_{(s)}$.

4.3. Transient Response Analysis of the Broadened Pulse Combined with an Isotopic Sharp Pulse. The combination between the CO₂ reforming and the partial oxidation of CH₄ may become a useful process, 13 because the CO₂ reforming is endothermic, while the partial oxidation is exothermic. For this reason, a transient response of a sharp ¹⁸O₂/Ar pulse of 3 μL into a broadened CH₄/C¹⁶O₂ pulse of 2.5 mL over a NiO/SiO₂ catalyst, previously subjected to 10 CH₄/CO₂ succesively exhausted pulses, was carried out. Figure 6 shows that the responses of CO18 and C16OO18 are much longer than that of Ar. The tail of CO¹⁸ is about 10 min long, whereas the Ar pulse has a width of only 0.1 min. This suggest that ¹⁸O forms relatively stable species on the catalyst surface by oxidizing Ni⁰ to Ni¹⁸O. Figure 6 also shows that the response of C¹⁶O decreases and that of C16O2 increases rapidly when the 18O2/Ar pulse is injected, and that, subsequently, they recover rapidly the original curves. However, no methane response was detected. The C¹⁶O decreases because ¹⁸O₂, being more reactive, replaces some of C16O2 in its reaction with CH4 and generates C18O. The C16O2 increases because it is replaced by ¹⁸O₂. No methane response is detected because it is completely consumed by its reaction with $C^{16}O_2$ and $^{18}O_2$.

5. Conclusion

This paper emphasizes that the transient response of a broadened pulse combined with a step change or a sharp isotopic pulse is a useful method in the study of heterogeneous processes. The following useful information was obtained regarding the CO_2 reforming of methane over NiO/SiO_2 : (1) Ni^0 is the active site; (2) the reaction between C and O species on Ni^0 is the rate-determining step; and (3) the introduction of a small amount of $^{18}O_2$ in the broadened $CH_4/C^{16}O_2$ pulse replaces some $C^{16}O_2$ in the reaction with CH_4 and generates $C^{18}O$.

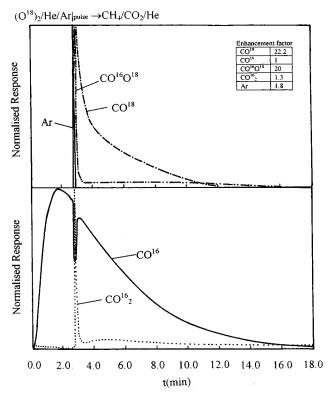


Figure 6. Normalized responses of C¹⁶O₂, C¹⁶O, C¹⁸O, C¹⁶O¹⁸O and Ar as a function of time for the broadened pulse of CH₄/C¹⁶O₂/Ar combined with a sharp pulse of ¹⁸O₂/Ar over NiO/SiO₂ subjected previously to 10 broadened succesively exhausted pulses.

References and Notes

- (1) Trimm, D. L. Catal. Rev. Sci. Eng. 1977, 16, 155.
- (2) Rostrup-Nielsen, J. R. In *Catalysis Science and Technology*; Anderson, J. R., Boudart, M., Eds; Springer: New York, 1984; Vol. 5.
 - (3) Hickman, D. A.; Schmidt, L. D. Science 1993, 259, 343.
- (4) Ashcroft, A. T.; Cheetham, A. K.; Foord, J. S.; Green, M. L. H.; Grey, C. P.; Murrell, A. J.; Vernon, P. D. F. *Nature* **1990**, *344*, 319.
- Choudhary, V. R.; Rajput, A. M.; Prabhakar, B. J. Catal. 1993, 139, 326.
 - (6) Hu, Y. H.; Ruckenstein, E. J. Catal. 1996, 158, 260.
 - (7) Hu, Y. H.; Ruckenstein, E. Catal. Lett. 1995, 34, 41.
 - (8) Ruckenstein, E.; Hu, Y. H. Catal. Lett. 1995, 35, 265.
- (9) Dissanayake, D.; Rosynek, M. P.; Kharas, K. C. C.; Lunsford, J. H. J. Catal. 1991, 132, 117.
 - (10) Hu, Y. H.; Au, C. T.; Wan, H. L. Chin. Sci. Bull. 1995, 40, 303.
- (11) Dissanayake, D.; Rosynek, M. P.; Lunsford, J. H. J. Phys. Chem. 1993, 97, 3644.
- (12) Choudhary, V. R.; Rajput, A. M.; Prabhakar, B. Angew. Chem., Int. Ed. Engl. 1994, 33, 2104.
- (13) Ashcroft, A. T.; Cheetham, A. K.; Green, M. L. H.; Vernon, P. D. F. Nature 1991, 352, 225.
- (14) Richardson, J. T.; Paripatyadar, S. A. Appl. Catal. 1990, 61, 293.
- (15) Yamazaki, O.; Nozaki, T.; Omata, K.; Fujimoto, K. Chem. Lett. 1992, 10, 1953.
 - (16) Gadalla, A. M.; Sommer, M. E. Chem. Eng. Sci. 1989, 44, 2825.
 - (17) Rostrup-Nielsen, J. R.; Hansen, J.-H. B. J. Catal. 1993, 144, 38.
- (18) Zhang, Z.; Verykios, X. E. J. Chem. Soc., Chem. Commun. 1995, 1, 71.
 - (19) Hu, Y. H.; Ruckenstein, E. J. Catal. 1996, 163, 306.
 - (20) Ruckenstein, E.; Hu, Y. H. Appl. Catal. 1995, 133, 149.
 - (21) Hu, Y. H.; Ruckenstein, E. Catal. Lett. 1996, 36, 145.
 - (22) Hu, Y. H.; Ruckenstein, E. Catal. Lett. 1997, 43, 71.
 - (23) Winslow, P.; Bell, A. T. J. Catal. 1985, 91, 142.
 - (24) Biloen, P. J. Mol. Catal. 1983, 21, 17.
 - (25) Soong, Y.; Krishna, K.; Biloen, P. J. Catal. 1986, 97, 330.
- (26) Greten, G.; Lafyatis, D. S.; Froment, G. F. J. Catal. 1995, 154,
- (27) Bennett, C. O. Catal. Rev.-Sci. Eng. 1976, 13, 121.
- (28) Efstathiou, A. M.; Lacombe, S.; Mirodatos, C.; Verikios, X. E. J. Catal. 1994, 148, 639.
- (29) Happel, J. Isotopic Assessment of Heterogeneous Catalysis; Academic Press: San Diego, 1986.
 - (30) Gleaves, J. T.; Ebner, J. R. U.S. Patent 4,626,421, 1986.