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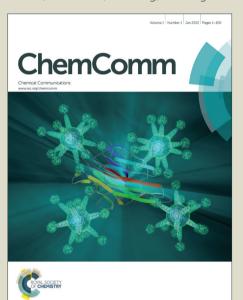
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## **ARTICLE TYPE**

# A microporous six-fold interpenetrated hydrogen-bonded organic framework for highly selective separation of C<sub>2</sub>H<sub>4</sub>/C<sub>2</sub>H<sub>6</sub>

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5 Received (in XXX, XXX) Xth XXXXXXXXX 20XX, Accepted Xth XXXXXXXXX 20XX DOI: 10.1039/b000000x

A unique six-fold interpenetrated hydrogen-bonded organic framework (HOF), for the first time, has been developed for highly selective separation of C<sub>2</sub>H<sub>4</sub>/C<sub>2</sub>H<sub>6</sub> at room temperature 10 and normal pressure.

As one of the most important petrochemicals, ethylene is used widely in chemical industry and its worldwide production exceeds that of any other organic compound (140 million tons per year by 2010). Thermal cracking of ethane as feedstock in the 15 presence of steam remains one of the most important and widely employed processes for ethylene production. Due to the similar sizes and volatilities of ethylene and ethane, traditional cryogenic distillations technology to separate ethylene from ethane requires distillation columns with over 100 trays under the conditions of 20 high pressure (23 bar) and low temperature (-25°C), which has been criticized as the most energy extensive process in the petrochemical industry.2 Therefore, tremendous effort has been devoted to develop alternative technologies,<sup>3</sup> such as membrane separation, liquid adsorbent separation and solid adsorbent 25 adsorption separation<sup>6</sup> for ethylene/ethane separation at ambient temperature and pressure with lower energy cost.

In the development of adsorption separation technology, various porous materials, such as SiO<sub>2</sub>, zeolites, molecular sieves, metal-organic frameworks (MOFs), nanoparticle/MOF 30 composite, 11 porous organic polymers (POPs), 12 activated carbons, 13 and carbon nanotubes 14 have been explored as solid adsorbent to realize olefin/paraffin separation. Two useful but distinct strategies have been proposed to achieve preferential adsorption of olefin over paraffin. One is based on reversible 35 formation of  $\pi$ -complexes of olefins with transition metal cations, the other is control of appropriate pore size and volume for size

exclusive separation. The former strategy has been successfully applied in MOFs<sup>10a</sup> and POPs<sup>12a</sup> to realize high selective adsorption for ethylene over ethane. Though such selectivity is usually very high at low pressure, it decreased significantly with 55 increasing pressure possibly due to saturation of the preferential binding sites. The latter strategy has often been used in propene/propane separation, 10b,12b however, can hardly be achieved especially for smaller ethylene and ethane molecules with tiny dimensional difference. Moreover, this strategy may 60 result in an inevitable low adsorption capacity. 10d Hence, finding new materials for the adsorptive separation of ethylene/ethane mixtures is very challenging and important.

Recently, we and several other groups have discovered that hydrogen-bonded organic framework (HOF) materials can be 65 used as a new class of porous materials for a variety of applications. 15 Because HOFs have some obvious advantages such as solvent processability and straightforward regeneration by recrystallization, while they might have different pore surfaces from those well-established porous materials, exploration of HOF 70 materials might lead to some unique new adsorbents for gas separations. Actually, the first HOF-1 exhibits superior performance to MOFs in very challenging C2H2/C2H4 separation.15h Herein, we report the synthesis of a robust hydrogen-bonded organic framework (HOF-4), which shows a 75 high adsorbed solution theory (IAST) selectivity of 14 for ethylene/ethane separation at room temperature and normal pressure.

Scheme 1. Tetrahedral building blocks.

2

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<sup>†</sup> Electronic Supplementary Information (ESI) available: Synthesis and characterization of HOF-4, PXRD, TGA, FTIR, sorption isotherms, 50 breakthrough simulation, CCDC 1010353. See DOI: 10.1039/b000000x/

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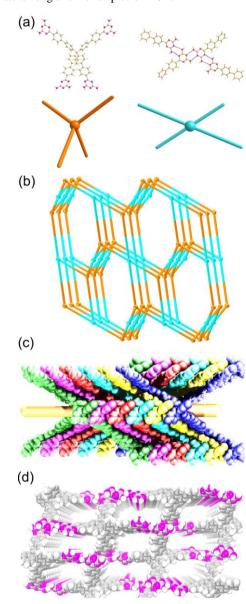
The new tetrahedral molecular tecton **2** (Scheme 1) has been synthesized as building block based on the following considerations: i) The extended tecton **2** keeps both tetrahedral symmetry and diaminopydridine in tecton **1**, which is the basic 5 building unit of HOF-1 and is capable of forming multiple hydrogen bonding and thus extending into 3D framework; ii) generally speaking, longer ligand will lead to larger voids.

The tetrahedral organic building block 2 was readily synthesized in 92% yield by the reaction of the corresponding 10 nitrile with dicyandiamide (See Scheme S1 in the Supporting Information). The colorless needle-like crystals of HOF-4 were easily isolated in 79 % yield by evaporating DMF solution of 2 for a week under room temperature. The purity of HOF-4 was confirmed by <sup>1</sup>H NMR and <sup>13</sup>C NMR spectroscopy, 15 thermogravimetric analysis (TGA), and powder X-ray diffraction (PXRD) (Fig. S1-S3). Single crystal X-ray diffraction reveals that **HOF-4** crystallizes in monoclinic space group P2/n and shows a 3D architecture consisting of six equivalent interwoven nets of **PtS** topology. For a single net, the asymmetric unit consists of 20 only half of the building block (Fig. 1a left), and each building block is connected with six neighbouring ones by 12 strong hydrogen bonds involving the 2,4-diaminotriazine (DAT) groups (Fig. 1a right, the parameters of hydrogen bonding are listed in Table S1). There exist rhombic channels in the single net along <sub>25</sub> [101] direction with an approximate dimension of 40 Å  $\times$  30 Å along the diagonals (Fig. S4). If one considers the tetrahedral building block to be a four-connected node in tetrahedral geometry, and the multiple hydrogen bonding motif of DAT groups to be a four-connected node in square planar geometry, 30 the single net of HOF-4 can then be rationalized as a 3D PtS {4<sup>2</sup>8<sup>4</sup>} network topology (Fig. 1b). Due to large void space, six equivalent nets interpenetrate each other via intermolecular  $\pi \cdots \pi$ interactions between the benzene rings (Fig. 1c). Such high fold net interpenetration is expected to enhance the framework 35 stability. 16-18 The rhombic channels along [101] direction are completed blocked due to the interpenetration, leaving a 1D rectangular channel (3.8 Å  $\times$  8.1 Å) along b axis (Fig. 1d). The pore spaces within the frameworks encapsulate a few amounts of disordered DMF solvent molecules. The potential solvent 40 accessible void space accounts approximately 42.5% of the whole crystal volume as estimated by PLATON.

With the slit rectangular channel along b axis (3.8 Å × 8.1 Å), it is reasoned that 'slim' shape molecule  $C_2H_4$  (3.28 Å × 4.18 Å × 4.84 Å) can access to the channel in **HOF-4a** readily, while relatively 'fat' shape molecule  $C_2H_6$  (3.81 Å × 4.08 Å × 4.82 Å) can hardly get through. Furthermore, the amino groups reside on the surface wall of framework might provide stronger hydrogen bonding interaction with more acidic molecule  $C_2H_4$  (pKa=44) than  $C_2H_6$  (pKa=50). We speculated that the size exclusion effect and hydrogen bonding interaction can work collaboratively to make **HOF-4** an ideal material to separate  $C_2H_4/C_2H_6$ . To test our hypothesis, gas adsorption experiment were conducted.

Before examining adsorption properties, the guest solvent solvent solvent exchange with acetone and then vacuumed at 100 °C to obtain desolvated **HOF-4a** which is thermally stable up to 400 °C. The porosity of **HOF-4a** was evaluated by CO<sub>2</sub> gas sorption at 196 K (Fig. 2a). The

type I isotherm shows a very sharp uptake at  $P/P_0 < 0.1$ , indicative of a microporous material. Because of the flexible nature of the HOF, there exists small degree of sorption hysteresis. The isotherm gives an apparent Brunauer-Emmett-Teller (BET) surface area of 312 m<sup>2</sup>g<sup>-1</sup> (Fig. S5), which is moderate among a few examples of HOFs



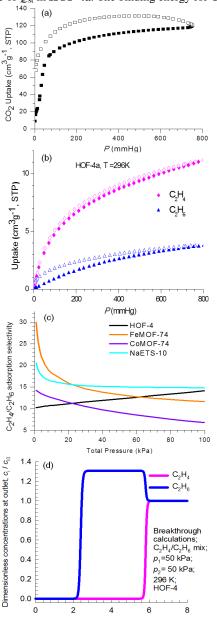
**Fig. 1** X-ray structure of **HOF-4** featuring (a) the basic organic building block in which the central carbon atoms act as tetrahedral nodes (brown balls) and centres of multiple hydrogen bonding motif act as square planar nodes (cyan balls); (b) simplified binodal four-connected PtS (4<sup>2</sup>8<sup>4</sup>) topology; (c) six-fold interpenetrated frameworks; (d) the rectangular channels (3.8 × 8.1 Å) along *b* axis (C, gray; H, white; N, pink).

with permanent porosity. 15d

Establishment of permanent microporosity of **HOF-4** allows us to examine its utility as an adsorbent for industrially important  $^{75}$  C<sub>2</sub>H<sub>4</sub>/C<sub>2</sub>H<sub>6</sub> separations. Interestingly, the C<sub>2</sub>H<sub>4</sub> uptakes of 17.3 cm³ g¹¹ at 273 K and 11.1 cm³ g¹¹ at 296 K are systematically about three times higher than C<sub>2</sub>H<sub>6</sub> uptakes of 5.1 cm³ g¹¹ at 273 K and 3.6 cm³ g¹¹ at 296 K at 1 atm (Fig. S6 and Fig. 2b). This

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discovery motivated us to examine its feasibility for the industrially important  $C_2H_4/C_2H_6$  separation in more details. The pure component isotherm data were fitted with the Langmuir isotherm model (Fig. S7). To understand the binding energy at 5 low coverage, isosteric heats of adsorption of  $C_2H_4$  and  $C_2H_6$  in **HOF-4a** are calculated. Fig. S8 presents data on the loading dependence of  $Q_{st}$  in **HOF-4a**. The binding energy for  $C_2H_4$  in



**Fig. 2** (a) CO<sub>2</sub> sorption isotherm at 196K; (b) Single-component sorption isotherms for  $C_2H_4/C_2H_6$  in **HOF-4a** at 296 K (Solid symbol: adsorption, open symbol: desorption); (c) Comparison of the IAST calculations of  $C_2H_4/C_2H_6$  adsorption selectivities for **HOF-4**, FeMOF-74, CoMOF-74, and NaETS-10 at 296 K; (d) Transient breakthrough of an equimolar  $C_2H_4/C_2H_6$  mixture in an adsorber bed packed with **HOF-4** in the adsorption phase of a PSA operation. The inlet gas is maintained at partial pressures  $p_1 = p_2 = 50$  kPa, at a temperature of 296 K.

Dimensionless time,  $\tau = t u / \varepsilon L$ 

**HOF-4a** is 44 kJ mol<sup>-1</sup>, which is comparable in magnitude to that

of MgMOF-74 and CoMOF-74. <sup>10g</sup> In contrast, the binding energy for C<sub>2</sub>H<sub>6</sub> in **HOF-4a** is only about 14 kJ mol<sup>-1</sup>, indicating that the **HOF-4a/**C<sub>2</sub>H<sub>4</sub> interaction is much stronger than **HOF-4a/**C<sub>2</sub>H<sub>6</sub> interaction at low coverage. Because **HOF-4a** is quite flexible, so its pores can be slightly enlarged to accommodate small amount of C<sub>2</sub>H<sub>6</sub> during adsorption process.

We further performed calculation using the Ideal Adsorbed Solution Theory (IAST) of Myers and Prausnitz.<sup>20</sup> Fig. 2c provides a comparison of the adsorption selectivity of C<sub>2</sub>H<sub>4</sub>/C<sub>2</sub>H<sub>6</sub> in equimolar mixtures as a functional of total bulk gas phase pressure in HOF-4a and three well-known porous materials 30 (MOF materials: FeMOF-74<sup>10a</sup> and CoMOF-74<sup>10g</sup>; Zeolite material: NaETS-10<sup>8c</sup>) at 296 K. It is worthy noting that the adsorption selectivity in respect of C<sub>2</sub>H<sub>4</sub>/C<sub>2</sub>H<sub>6</sub> for **HOF-4a** is up to 14 at 1 atm and room temperature, which is not only surpassing the best MOF materials but also is comparable to the 35 best zeolite material NaETS-10 for such an important separation, highlighting **HOF-4a** as a promising material for the  $C_2H_4/C_2H_6$ separation for industrial usage. The large pore spaces have enabled both FeMOF-74 and CoMOF-74 to take up much more C<sub>2</sub>H<sub>6</sub> with the increasing pressure; while the narrow pore sizes 40 with **HOF-4a** has limited its adsorption capacity for C<sub>2</sub>H<sub>6</sub> even under increasing pressure, so HOF-4a is unique for C<sub>2</sub>H<sub>4</sub>/C<sub>2</sub>H<sub>6</sub> separation: the separation selectivity increases with the increasing pressure.

In order to further validate the feasibility, the breakthrough simulation experiments were carried out using the established methodology described in early publications of Krishna (see supporting information for details). The simulated breakthrough curves (Fig. 2d) clearly show that **HOF-4a** can efficiently separate  $C_2H_4$  from the  $C_2H_4/C_2H_6$  mixture at room temperature. The more poorly adsorbed saturated  $C_2H_6$  breaks through earlier and can be recovered in nearly pure form (Fig. S9). During the adsorption cycle,  $C_2H_6$  at purities > 99% can be recovered for a certain duration. Once the entire bed is in equilibrium with the partial pressures  $p_1 = p_2 = 50$  kPa, the desorption, or "blowdown" cycle is initiated, by applying a vacuum or purging with inert gas. 99.95% of ethylene can be recovered during the time interval, which can satisfy the purity requirement for production of ethylene as feedstock in polymer industry.

In summary, we have prepared and characterized a unique sixfold interpenetrated **HOF-4** material with PtS topology by using
an expanded tetrahedral tecton **2**. The high degree of
interpenetration not only enhanced the structure integrity but also
appropriately tuned the channel size to make **HOF-4** an ideal
absorbent for C<sub>2</sub>H<sub>4</sub>/C<sub>2</sub>H<sub>6</sub> separation. This is the first example of
sporous hydrogen-bonded organic framework for such an
important industrial hydrocarbon separation, during which
channel confinement effect and hydrogen bonding interactions
appear to simultaneously control the uptake of different C2
hydrocarbons. It is believed that this work could render new
strategy in designing robust HOFs with permanent porosity and
promote more investigation on separation of small hydrocarbons
using novel porous organic materials.

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‡Crystal data for **HOF-4**:  $C_{61}H_{48}N_{20}$ , M = 1061.17, monoclinic,

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space group P2<sub>1</sub>/*n*, a = 20.212(2) Å, b = 7.725 (2) Å, c = 26.666(2),  $\beta$  = 90.606 (8) ° V = 3920.81(2) Å<sup>3</sup>, Z = 2,  $D_c$  = 0.899 g cm<sup>3</sup>, T = 193 (2) K, F(000) = 1108.0, final  $R_1$  = 0.0976 for I >  $2\sigma(I)$ ,  $wR_2$  = 0.2139 for all data, GOF = 1.133, CCDC 1010353.

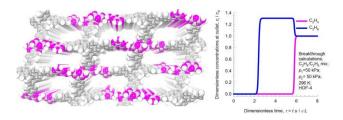
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