

# Long-Term Real-Time Monitoring Catalytic Synthesis of Ammonia in a Microreactor by VUV-Lamp-Based Charge-Transfer Ionization Time-of-Flight Mass Spectrometry

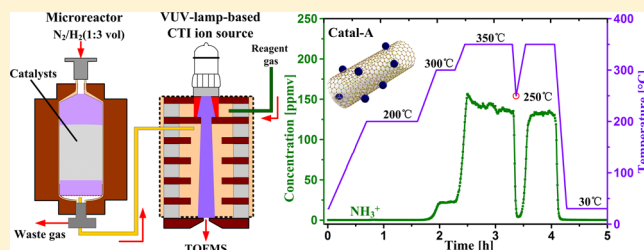
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## Supporting Information

**ABSTRACT:** With respect to massive consumption of ammonia and rigorous industrial synthesis conditions, many studies have been devoted to investigating more environmentally benign catalysts for ammonia synthesis under moderate conditions. However, traditional methods for analysis of synthesized ammonia (e.g., off-line ion chromatography (IC) and chemical titration) suffer from poor sensitivity, low time resolution, and sample manipulations. In this work, charge-transfer ionization (CTI) with  $O_2^+$  as the reagent ion based on a vacuum ultraviolet (VUV) lamp in a time-of-flight mass spectrometer (CTI-TOFMS) has been applied for real-time monitoring of the ammonia synthesis in a microreactor. For the necessity of long-term stable monitoring, a self-adjustment algorithm for stabilizing  $O_2^+$  ion intensity was developed to automatically compensate the attenuation of the  $O_2^+$  ion yield in the ion source as a result of the oxidation of the photoelectric electrode and contamination on the  $MgF_2$  window of the VUV lamp. A wide linear calibration curve in the concentration range of 0.2–1000 ppmv with a correlation coefficient ( $R^2$ ) of 0.9986 was achieved, and the limit of quantification (LOQ) for  $NH_3$  was in ppbv. Microcatalytic synthesis of ammonia with three catalysts prepared by transition-metal/carbon nanotubes was tested, and the rapid changes of  $NH_3$  conversion rates with the reaction temperatures were quantitatively measured with a time resolution of 30 s. The high-time-resolution CTI-TOFMS could not only achieve the equilibrium conversion rates of  $NH_3$  rapidly but also monitor the activity variations with respect to investigated catalysts during ammonia synthesis reactions.



The massive consumption of ammonia for agricultural and industrial use has impelled humankind to continuously increase the ammonia production. Industrially, the Haber–Bosch process is the main route to produce ammonia.<sup>1,2</sup> However, this process requires rigorous reaction conditions and consumes 1–2% of the world's annual energy supply with a significant amount of carbon dioxide released.<sup>3,4</sup> Therefore, many studies have been focused on investigating more environmentally benign catalysts for microcatalytic synthesis of ammonia under milder conditions.<sup>5–11</sup> For example, transition-metal- $N_2$  complexes have been investigated to catalyze  $N_2$  into  $NH_3$  under ambient conditions.<sup>5,6</sup> Bacterial nitrogenase enzymes have been verified to produce  $NH_3$  through biological  $N_2$  fixation under ambient temperature and pressure.<sup>7–9</sup> Some methods have been reported for measurement of the effluent ammonia during these synthesis microreactions (e.g., ion chromatography (IC)<sup>10</sup> and chemical titration).<sup>5,6,12,13</sup> Because of its poor sensitivity and off-line sample preparation, time resolution of the IC ranged from 2 to 25 h with a total of 35 mmol ammonia produced in a catalytic reaction of 75 h.<sup>10</sup> As anticipated for IC, the low-time-

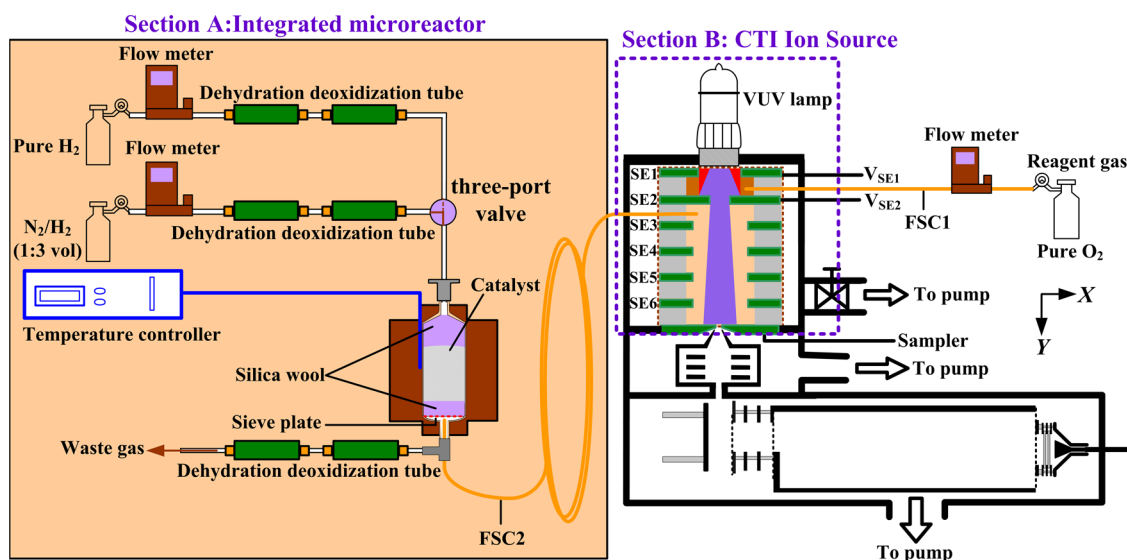
resolution data bears the risk of missing rapid and important information about the catalytic activity of studied catalysts. The chemical titration method suffers from the same disadvantage of low time resolution. Besides, because chemical titration is established on the basis of visual perception of the changes of solution color, there is a high experimenter-to-experimenter variance of results especially for ammonia with low concentration. Therefore, development of high-time-resolution and more sensitive techniques for evolved ammonia analysis becomes necessary to evaluate the catalytic efficiency of the catalysts and monitor the activity changes induced by reaction parameters.

Online mass spectrometry (MS) is gaining widespread use to monitor catalytic dynamic processes without unnecessary interruptions and sample preparations.<sup>14–18</sup> For traditional electron impact ionization (EI),  $NH_3^+$  ions are formed by ionizing  $NH_3$ . However, the neutral molecule  $H_2O$  could be

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**Figure 1.** Schematic diagram of the integrated microreactor and the VUV-lamp-based  $\text{O}_2^+$  charge-transfer ionization source coupled with an orthogonal acceleration time-of-flight mass spectrometer.

ionized by EI to generate  $\text{HO}^+$  ions with a relative intensity of 20%, which interferes with the identification of  $\text{NH}_3^+$ .<sup>19</sup> Moreover, the pressure in the EI source has to be kept as low as possible to prolong the lifetime of the heated filament, which restricted further improvement of the sensitivity. Under high vacuum condition of  $10^{-4}$  Pa in an EI source, 25 ppmv  $\text{NH}_3$  failed to achieve obvious response at  $m/z = 17$  (see Figure S-1 in Supporting Information).

Various soft ionization techniques (e.g., proton transfer reaction (PTR), single-photon ionization (SPI) and chemical ionization (CI)), may meet the requirement for ammonia analysis. The higher proton affinity (PA) of  $\text{NH}_3$  (853.6 kJ mol<sup>-1</sup>) than  $\text{H}_2\text{O}$  (691 kJ mol<sup>-1</sup>) makes it possible to measure  $\text{NH}_3$  by PTR-MS, which is based on proton transfer reaction with  $\text{H}_3\text{O}^+$  to form  $\text{NH}_4^+$  ions. PTR-MS<sup>20,21</sup> was reported to determine ammonia in the atmosphere. However, the PTR-MS instrument suffers from a high instrumental background (typically several  $10^4$  cps of  $\text{NH}_4^+$  ions) as a result of intrinsic formation of  $\text{NH}_3$  from  $\text{H}_2\text{O}$  and  $\text{N}_2$  in the hollow cathode ion source.<sup>21</sup> Moreover,  $\text{H}_2\text{O}^+$  will interfere with the identification and quantification of  $\text{NH}_4^+$  because of overlapping peaks in spectra.<sup>22</sup>

SPI has been applied for analysis of complex samples (e.g., diesel fuel,<sup>23,24</sup> cigarette smoke,<sup>25,26</sup> and volatile organic compounds (VOCs)<sup>27–29</sup>). However, limited by the photon flux of the VUV lamp ( $1.0 \times 10^{11}$  photons s<sup>-1</sup>) and small photoionization cross-section of  $\text{NH}_3$  ( $1.3 \times 10^{-18}$  cm<sup>2</sup> at 118 nm),<sup>30</sup> the achievable sensitivity of  $\text{NH}_3$  by VUV-lamp-based SPI-MS is not satisfactory. Additionally, the photon flux of the VUV lamp may decay in vacuum as a result of contamination on the  $\text{MgF}_2$  window of the VUV lamp, which needs sequential external calibration for long-time continuous operation.<sup>31</sup>

Recently, Li et al.<sup>27,32</sup> developed VUV-lamp-based charge-transfer ionization ion source time-of-flight mass spectrometry (CTI-TOFMS). The VUV-lamp-based CTI ion source not only expanded the obtainable information considerably but also improved the analytical sensitivity of compounds with ionization energies below the VUV photon energy (10.6 eV). In CTI mode,  $\text{O}_2^+$  reagent ions were generated by photoelectron ionization (PEI) of pure  $\text{O}_2$  gas. The recombination

energy of  $\text{O}_2^+$  is 12.07 eV, the ionization energy of  $\text{NH}_3$  is 10.07 eV, so the charge transfer from  $\text{O}_2^+$  to  $\text{NH}_3$  is valid and efficient with product ion of  $\text{NH}_3^+$ .<sup>21</sup> CTI-MS based on a PTR-MS instrument operated with pure  $\text{O}_2$  as reagent gas has been successfully applied for measurement of atmospheric  $\text{NH}_3$ , even at low ppbv level.<sup>21,33,34</sup>

The present work describes the combination of a CTI-TOFMS to an integrated microreactor for real-time monitoring of the microcatalytic ammonia synthesis reaction with a time resolution of 30 s. A self-adjustment algorithm was designed to compensate the attenuation of the VUV lamp and the oxidation of the photoelectric electrode for long-term monitoring and wide quantification range. As a result, stable continuous monitoring of ammonia microsynthesis reactions could last at least 50 h.

## EXPERIMENTAL SECTION

The apparatus for online monitoring of ammonia microsynthesis consists of an integrated microreactor device and a VUV-lamp-based charge-transfer ionization ion source coupled with a home-built orthogonal acceleration time-of-flight mass spectrometer (CTI-TOFMS), as shown in Figure 1.

**VUV-Lamp-Based CTI Ion Source.** Full details of the VUV-lamp-based CTI ion source have been reported before.<sup>27</sup> Thus, only a brief description is given here. The CTI ion source as shown in section B of Figure 1 includes a commercial VUV krypton discharge lamp (10.6 eV, Cathodeon Ltd., Cambridge, U.K.) and an ionization cavity. The ionization cavity was made by six 1 mm thick stainless steel electrodes (SE1–SE6) and six 5 mm thick PTFE insulation washers. SE2 separated the ionization cavity into two regions: reagent ion-producing region between VUV lamp and SE2 electrode, ion–molecule reaction region between SE2 electrode and sampler electrode. The reagent gas  $\text{O}_2$  and the effluent gas from microreactor were directly introduced into the reagent ion-producing region and the ion–molecule reaction region by a 250  $\mu\text{m}$  i.d. 0.5 m long deactivated fused-silica capillary (FSC1) and a 200  $\mu\text{m}$  i.d. 0.5 m long deactivated fused-silica capillary (FSC2), respectively. The pressure in the ion source was maintained at 40 Pa by a 3.5 L/s dry scroll pump (Agilent Technologies Inc., California,

U.S.A.), and the variation of the pressure was less than 0.4 Pa during microcatalytic reactions.

The ion source could work at two different operation modes, SPI and CTI modes, by simply adjusting the voltage of SE1 ( $V_{SE1}$ ) while keeping the voltages on other electrodes unchanged. In SPI mode,  $V_{SE1}$  was set at 30 V to hinder the PEI of the reagent molecules, and  $NH_3$  was mainly ionized by the VUV photons. In CTI mode,  $V_{SE1}$  was set higher than 40 V so that the photoelectrons emitted from the SE2 electrode surface (as shown in eq 1) could ionize  $O_2$  efficiently through eq 2.<sup>35,36</sup> The  $O_2^+$  reagent ions were then transferred to the ion–molecule reaction region where  $NH_3$  molecules were ionized through the charge-transfer reaction, as described in eq 3. The voltages of SE2 electrode ( $V_{SE2}$ ) and the sampler electrode were maintained at 18 and 7 V, respectively.



**Kinetic Model of Charge-Transfer Reaction.** In charge-transfer reaction, the changes with time of the number densities of  $O_2^+$  reagent ions  $[O_2^+]_t$  and  $NH_3^+$  product ions  $[NH_3^+]_t$  in the ion source are described by the following kinetic equations<sup>37</sup>

$$\frac{d[O_2^+]_t}{dt} = -[O_2^+]_t \frac{D_{P(O_2^+)}}{\Lambda^2} - [O_2^+]_t k[NH_3] \quad (4)$$

$$\frac{d[NH_3^+]_t}{dt} = -[NH_3^+]_t \frac{D_{P(NH_3^+)}}{\Lambda^2} + [O_2^+]_t k[NH_3] \quad (5)$$

Here  $k$  is the rate coefficient of eq 3 with an experimental datum of  $1.0 \times 10^{-9} \text{ cm}^3 \text{ s}^{-1}$ .<sup>38</sup>  $[NH_3]$  is the number density of the  $NH_3$  molecules in the ion source with calculated results of  $5.66 \times 10^8 \text{ cm}^{-3}$  to  $2.83 \times 10^{12} \text{ cm}^{-3}$ , corresponding to 0.2–1000 ppmv  $NH_3$  in sample gas (see the Supporting Information S-2 for detailed calculation equation).<sup>37</sup>  $D_{P(O_2^+)}$  and  $D_{P(NH_3^+)}$  are the diffusion coefficients of the  $O_2^+$  reagent ions and the  $NH_3^+$  ions with calculated results of  $602 \text{ cm}^2 \text{ s}^{-1}$  and  $729 \text{ cm}^2 \text{ s}^{-1}$  at 298 K and 40 Pa, respectively.<sup>39</sup>  $\Lambda$  is the characteristic diffusion length of the ion source determined from only its dimensions, and  $\Lambda^2$  is  $6.22 \times 10^{-2} \text{ cm}^2$  for CTI ion source.<sup>40</sup>

An exact solution of eq 4 and eq 5 gives the relationship between the product and the reagent ion number densities as<sup>37,41</sup>

$$[NH_3^+]_t = k[O_2^+]_t [NH_3] t \frac{\exp\left(k[NH_3]t + \frac{D_{P(O_2^+)} - D_{P(NH_3^+)}}{\Lambda^2} t\right) - 1}{k[NH_3]t + \frac{D_{P(O_2^+)} - D_{P(NH_3^+)}}{\Lambda^2} t} \quad (6)$$

For the continuously formed  $NH_3^+$  ions, their residence time in the ion source varies from zero up to the total reaction time  $t_r$ .  $t_r$  is calculated to be  $3.3 \times 10^{-5} \text{ s}$  from the reduced near-zero-field mobility  $K$  ( $2.45 \times 10^4 \text{ cm}^2 \text{ V}^{-1} \text{ s}^{-1}$ ),<sup>39</sup> the electric field strength in the ion–molecule reaction region ( $3.67 \text{ V cm}^{-1}$ ), and the length of the ion–molecule reaction region (30 mm).<sup>42</sup> Thus, for  $t = t_r$ , eq 6 can be expressed as

$$[NH_3^+]_{t_r} = k[O_2^+]_{t_r} [NH_3] t_r D_e \quad (7)$$

where  $D_e$ , defined as the differential diffusion enhancement coefficient, is used to describe the effect of the differential diffusion and expressed as

$$D_e = \frac{\exp\left(k[NH_3]t_r + \frac{D_{P(O_2^+)} - D_{P(NH_3^+)}}{\Lambda^2} t_r\right) - 1}{k[NH_3]t_r + \frac{D_{P(O_2^+)} - D_{P(NH_3^+)}}{\Lambda^2} t_r} \quad (8)$$

For  $NH_3$  with a concentration of 0.2 ppmv to 1000 ppmv,  $D_e$  varies from 0.9671 to 1.0131 with a small variation of 4.76%, and the diffusions of the ions impose little influence on the number density of the  $NH_3^+$  ions. Thus, according to eq 7, stabilizing the number density of the  $O_2^+$  ions is essential to obtain a steady response of the  $NH_3^+$  ions and wide linear concentration range by charge-transfer ionization.

**Combination of the Integrated Microreactor and CTI-TOFMS.** The integrated microreactor, as shown in section A of Figure 1, includes a vertical quartz tube microreactor with an inner diameter of about 8 mm and a temperature controller. Both ends of the microreactor were filled with silica wool, and 100 mg of catalyst was placed between the silica wools. The CTI-TOFMS was coupled to the microreactor through FSC2, which was inserted just underneath the silica wool to reach a dead volume of about 0.2 mL. The sampling rate of TOFMS through FSC2 was  $15 \text{ mL min}^{-1}$ , so the dead time was about 0.5 s, and real-time monitoring was realized. The feed gas  $N_2/H_2$  1:3 (vol), dehydrated by 5A type high strength molecular sieve (Dalian Sheng Mai Company, Dalian, China) and deoxygenated by 401 type Deoxidizer (Dalian Sheng Mai Company, Dalian, China), passed through the catalyst bed with a flow rate of  $20 \text{ mL min}^{-1}$ , and the excess gas was exhausted after dehydration and deoxidization treatment.

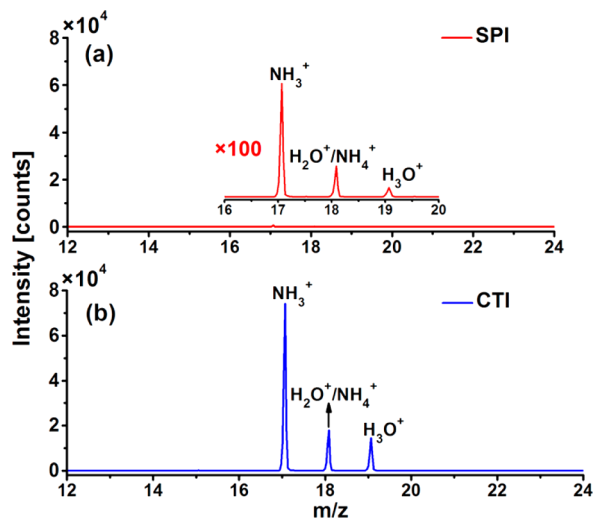
The TOF mass analyzer was operated in linear mode with a mass resolution of 900 (fwhm) at  $m/z = 78$ . The data were recorded with 30 s for a single analysis by a 100 ps time-to-digital converter (TDC) (model 9353, Ametek, Inc., Oak Ridge, TN, U.S.A.) at a repetition rate of 33 kHz. All the microcatalytic reactions were operated at atmospheric pressure, and the temperature-programmed procedures for the catalysts are listed in table S-1 of the Supporting Information.

**Sample Preparation.** Two ammonia standard gas mixtures with concentrations of 25 ppmv and 5000 ppmv in  $N_2/H_2$  1:3 (vol) (Dalian Special Gas Company, Dalian, China) were further diluted with  $N_2/H_2$  1:3 (vol) to a series of lower concentrations by using mass flow controllers. The purity of all gases was 99.999%. Three catalysts based on transition metals, provided by State Key Laboratory of Catalysis in Dalian Institute of Chemical Physics, were named as Catal-A,<sup>12</sup> Catal-B, and Catal-C, respectively. Catal-A with transition metal nanoparticles Ru deposited on the outside wall of carbon nanotubes was prerduced in a flow of  $H_2$  at 450 °C for 12 h. After being packed into the microreactor, it was further online activated in  $H_2$  flow with  $50 \text{ mL min}^{-1}$  from 30 to 200 °C for 60 min, from 200 to 300 °C at  $5 \text{ °C min}^{-1}$ , and finally at 300 °C for 60 min. Catal-B and Catal-C were prepared with same transition metal precursor and carbon nanotubes in two different methods, yielding two different types of structures.<sup>43,44</sup> Before the microcatalytic reaction, Catal-B and Catal-C were both online reduced by  $H_2$  from room temperature to 550 °C with a heating rate of  $4 \text{ °C min}^{-1}$  and then held at 550 °C for 2 h.

## RESULTS AND DISCUSSION

**Ionization of  $NH_3$  in SPI and CTI Modes.** As  $NH_3$  (IE = 10.07 eV) can be ionized both in SPI and CTI modes, 25 ppmv  $NH_3$  in  $N_2/H_2$  1:3 (vol) was tested, and the mass spectra are

illustrated in Figure 2a and b, respectively. In SPI mode, the peak intensity of the  $\text{NH}_3^+$  ions was only 713 counts when  $V_{\text{SEI}}$



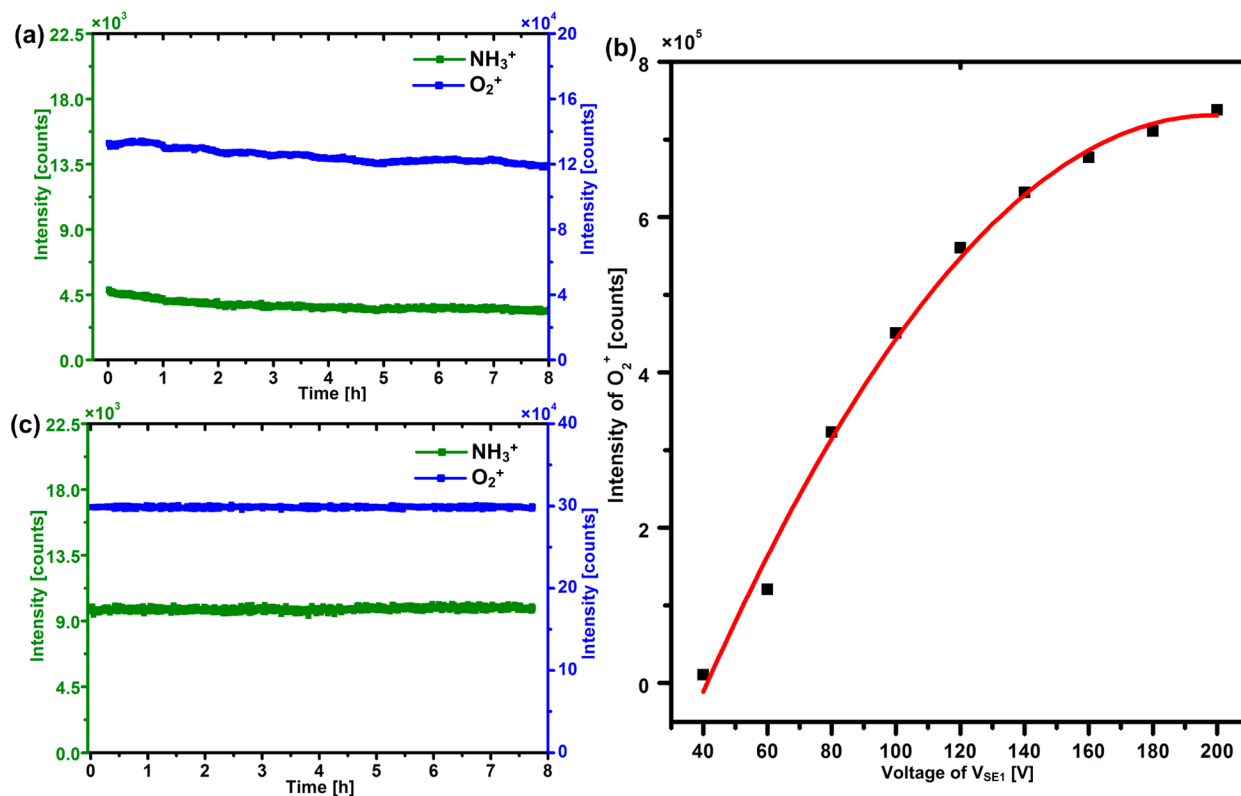
**Figure 2.** (a) Mass spectrum of 25 ppmv  $\text{NH}_3$  in  $\text{N}_2/\text{H}_2$  1:3 (vol) in SPI mode when  $V_{\text{SEI}}$  was set at 30 V. (b) Mass spectrum of 25 ppmv  $\text{NH}_3$  in  $\text{N}_2/\text{H}_2$  1:3 (vol) in CTI mode when  $V_{\text{SEI}}$  was set at 180 V.

was 30 V; however, in CTI mode, the peak intensity of the  $\text{NH}_3^+$  ions dramatically increased to 74169 counts when  $V_{\text{SEI}}$  was 180 V, and the sensitivity is improved by about 100-fold. Therefore, CTI mode was employed in the next experiments for better sensitivity. On the basis of eq 7, sensitivity can be

improved by increasing the number density of the  $\text{O}_2^+$  ions in CTI mode.

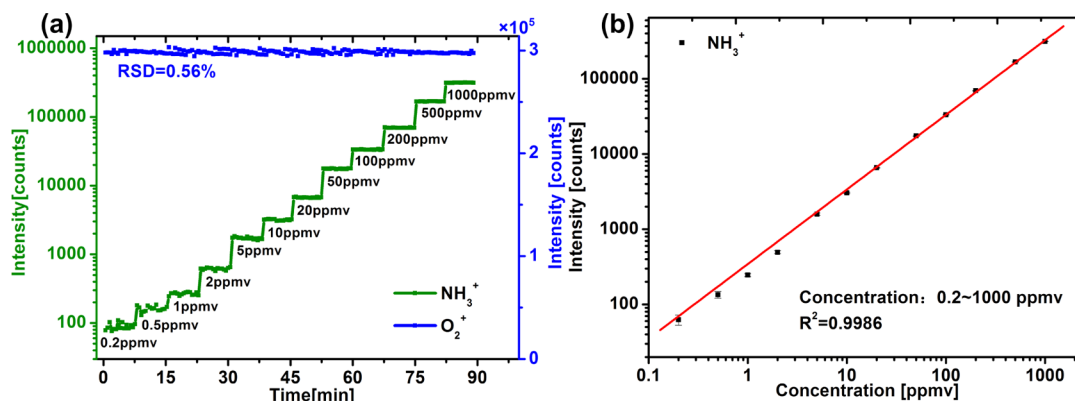
**Algorithm to Stabilize the Intensity of  $\text{O}_2^+$  Reagent Ions.** According to eq 7, the number density of the  $\text{NH}_3^+$  ions exiting from the ion source,  $[\text{NH}_3^+]_t$ , is influenced by the number density of the  $\text{O}_2^+$  ions exiting from the ion source  $[\text{O}_2^+]_t$ . Figure 3a shows the intensity variations of the  $\text{O}_2^+$  ions and  $\text{NH}_3^+$  ions when  $V_{\text{SEI}}$  is fixed at 70 V. The relative standard deviations (RSDs) of the  $\text{O}_2^+$  and  $\text{NH}_3^+$  intensities were 3.34% and 8.44%, respectively. Therefore, it is necessary to stabilize  $[\text{O}_2^+]_t$  for accurate measurement of  $\text{NH}_3$  at a certain concentration. In our CTI-MS,  $[\text{O}_2^+]_t$  is affected by the number density of the  $\text{O}_2$  reagent molecules, the VUV photon flux, the photoelectron emission efficiency of the electrode and the number density of the  $\text{NH}_3$  molecules. The number density of the  $\text{O}_2$  reagent molecules is always constant in our experiment. The VUV photon flux and the photoelectron emission efficiency of the electrode may decrease due to contamination of the VUV lamp and oxidation of the electrode during long-term measurement. For a high concentration of the  $\text{NH}_3$  molecules up to thousands of ppmv,  $[\text{O}_2^+]_t$  may decrease so significantly that accurate quantification of  $\text{NH}_3$  fails to obtain.

Figure 3b displays the correlation between the peak intensity of the  $\text{O}_2^+$  ions and the value of  $V_{\text{SEI}}$ . The peak intensity of the  $\text{O}_2^+$  ions increased from 10 886 counts to 738 157 counts with an enhancement of more than 60-fold when  $V_{\text{SEI}}$  was changed from 40 to 200 V. Obviously, it is an effective solution to compensate the decay of the peak intensity of the  $\text{O}_2^+$  ions by elevating the value of  $V_{\text{SEI}}$ . Therefore, we designed an algorithm

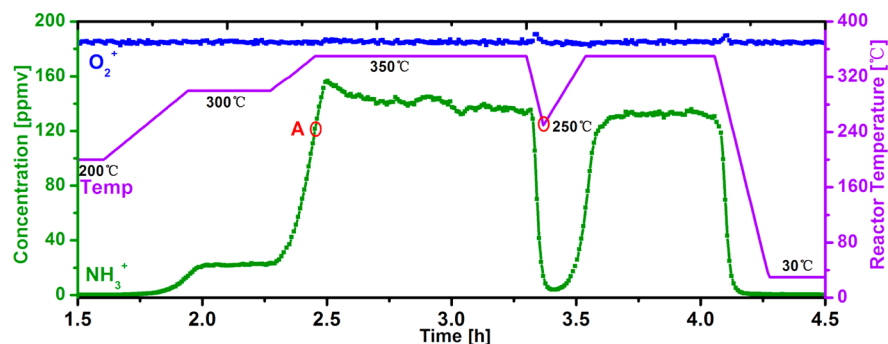


**Figure 3.** (a) Peak intensity profiles of the  $\text{O}_2^+$  and  $\text{NH}_3^+$  ions of 25 ppmv  $\text{NH}_3$  in CTI mode without the algorithm. (b) Peak intensity of the  $\text{O}_2^+$  reagent ions at different values of  $V_{\text{SEI}}$  in CTI mode. (c) Peak intensity profiles of the  $\text{O}_2^+$  and  $\text{NH}_3^+$  ions of 25 ppmv  $\text{NH}_3$  in CTI mode after presetting  $\text{O}_2^+$  intensity at 300 000 counts by the algorithm.

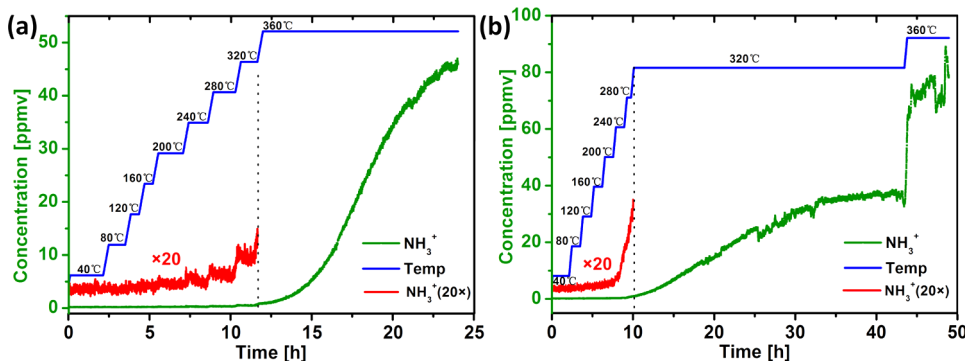




**Figure 4.** (a) Peak intensities of the NH<sub>3</sub><sup>+</sup> ions in N<sub>2</sub>/H<sub>2</sub> 1:3 (vol) at different concentrations in CTI mode. (b) Linear calibration curve for NH<sub>3</sub> in the concentration range from 0.2 ppmv to 1000 ppmv.



**Figure 5.** Time course of concentration of NH<sub>3</sub> in the outflow gas with Catal-A. Reaction conditions: catalyst, 100 mg; feed gas, N<sub>2</sub>/H<sub>2</sub> 1:3 (vol) with a flow rate of 20 mL min<sup>-1</sup>; pressure, 0.1 MPa.



**Figure 6.** Time courses of concentration of NH<sub>3</sub> in the outflow gas with (a) Catal-B and (b) Catal-C. Reaction conditions: catalyst, 100 mg; feed gas, N<sub>2</sub>/H<sub>2</sub> 1:3 (vol) with a flow rate of 20 mL min<sup>-1</sup>; pressure, 0.1 MPa.

to stabilize the intensity of the O<sub>2</sub><sup>+</sup> ions by automatically adjusting the value of  $V_{SEI}$ . With the algorithm, the present value of  $V_{SEI}$  is adjusted by comparing the O<sub>2</sub><sup>+</sup> intensity of the previous measurement cycle (30 s) with the preset O<sub>2</sub><sup>+</sup> intensity, the simplified principle is expressed as follows:

$$V_{n+1} = V_n + \eta \left( 1 - \frac{I_n}{I_0} \right) V_n \quad (n = 1, 2, 3 \dots) \quad (9)$$

where  $n$  is the number of the measurement cycle,  $V_{n+1}$  is defined as the present value of  $V_{SEI}$  required,  $V_n$  is equivalent to the previous value of  $V_{SEI}$ ,  $I_0$  (counts) is the preset intensity of the O<sub>2</sub><sup>+</sup> ions,  $I_n$  (counts) represents the O<sub>2</sub><sup>+</sup> ion intensity of the previous measurement cycle, and  $\eta$  is the calibration coefficient.

Figure 3c depicts the intensity variation of 25 ppmv NH<sub>3</sub> during 8 h of continuous measurement stabilizing the O<sub>2</sub><sup>+</sup> reagent ions at 300 000 counts with the algorithm. The greatest variation between the measured and the preset O<sub>2</sub><sup>+</sup> intensity was 1.65%. The RSDs of the O<sub>2</sub><sup>+</sup> and NH<sub>3</sub><sup>+</sup> intensities were 0.38% and 1.3%, respectively. So, the following measurements were all performed with the above algorithm, and the O<sub>2</sub><sup>+</sup> ion intensity was fixed at 300 000 counts to facilitate long-term accurate quantitative measurement of ammonia.

**Limit of Quantification (LOQ) and Linear Dynamic Range.** Figure 4a displays continuous monitoring of NH<sub>3</sub><sup>+</sup> ion intensity at different concentrations of NH<sub>3</sub>. The weak background signal at  $m/z = 17$  was 30 counts accumulated in 30 s, which may result from the ionization of feed gas N<sub>2</sub>/H<sub>2</sub> 1:3 (vol) or permeation of atmospheric ammonia (~100 ppbv)

into the instrument through polytetrafluoroethylene (PTFE) tubes.<sup>21</sup> The step-by-step intensity response of  $\text{NH}_3^+$  with the increased  $\text{NH}_3$  concentration reflected that the dead time and memory effect were small and negligible. The RSDs at different concentrations ranged from 0.5% (1000 ppmv) to 11% (0.2 ppmv), which revealed good precision. Figure 4b represents the calibration curve of the  $\text{NH}_3^+$  ions, and almost 4 orders of magnitude dynamic range was obtained from 0.2 ppmv to 1000 ppmv with a good linear correlation coefficient ( $R^2 = 0.9986$ ). Based on the  $S/N = 10$  criteria, the LOQ for  $\text{NH}_3$  is calculated to be 76 ppbv, which is adequate for online analysis of  $\text{NH}_3$  in microcatalytic reactions. On the basis of eq 7, the stable quantitative performance and wide linear dynamic range of the current method were attributed to the stabilization of  $\text{O}_2^+$  ion intensity and small variation of  $D_e$  with the upward concentration of  $\text{NH}_3$  molecules.

**Applications in Monitoring of Three Microcatalytic Synthesis Reactions.** Figure 5 and Figure 6 depict the profiles of  $\text{NH}_3$  concentration (in ppmv) in the effluent from the microreactor with three different catalysts.

In Figure 5, the Catal-A was first used to evaluate the quantitative performance of the CTI-TOFMS method on monitoring the concentration of  $\text{NH}_3$  in the microcatalytic synthesis. The concentration of  $\text{NH}_3$  started to increase rapidly around 255 °C, and an equilibrium concentration of 22 ppmv was achieved after the temperature was kept at 300 °C for 5 min. Then, the concentration of  $\text{NH}_3$  reached a peak value of 155.7 ppmv shortly after the microreactor was heated to 350 °C (at point A) and decreased slowly to an equilibrium concentration of 134 ppmv. Part of  $\text{NH}_3$  at the peak concentration was presumed to come from desorption of  $\text{NH}_3$  previously formed at lower temperatures. The microreactor was cooled down to 250 °C with a rate of 25 °C  $\text{min}^{-1}$  after being kept for 51 min at 350 °C, and the microreactor was then immediately heated back to 350 °C with a rate of 10 °C  $\text{min}^{-1}$ . The rapid changes of  $\text{NH}_3$  concentration according to temperature variations were clearly recorded. For example, the concentration of ammonia reached the same equilibrium value of 134 ppmv in 10 min after the temperature of the microreactor reached 350 °C again, and then the concentration of ammonia decreased to the baseline in 13 min after the reactor was cooled to ambient temperature. Catal-A exhibited stable catalytic activity, as there was no equilibrium concentration difference between the first temperature condition of 350 °C and the second one. The above results indicate good repeatability and reliability of the current CTI-TOFMS method.

Figure 6a,b show the concentration variation of  $\text{NH}_3$  in the effluent gas with time at different temperatures using two catalysts (a) Catal-B and (b) Catal-C. As shown in Figure 6a, relative low equilibrium concentrations of  $\text{NH}_3$  for Catal-B were achieved quickly between 40 and 320 °C, whereas it took about 12.3 h to reach the equilibrium concentration of 46 ppmv at 360 °C. From Figure 6b, we can see that there was no  $\text{NH}_3$  observed below 240 °C, the concentration of  $\text{NH}_3$  started to increase from 240 °C, and an equilibrium concentration of 37 ppmv at 320 °C was achieved more than 33 h later. However, the concentration of  $\text{NH}_3$  reached its equilibrium value of 75 ppmv at 360 °C in only less than 32 min. Besides, there were obvious variations of conversion rate of  $\text{NH}_3$  observed especially between the 25th hour and the 35th hour at 320 °C, and the variations became significant at 360 °C, which

suggest the activity variations of Catal-C at corresponding temperatures.

The equilibrium conversion rates of  $\text{NH}_3$ , which is used to evaluate the catalytic activity of the investigated catalysts, can be calculated directly from the amount of catalyst, the flow rate, and the measured equilibrium concentration of  $\text{NH}_3$  in the effluent gas. The conversion rates of  $\text{NH}_3$  for Catal-B were  $3.67 \times 10^{-4} \text{ mol g}^{-1} \text{ h}^{-1}$  at 320 °C and  $3.30 \times 10^{-2} \text{ mol g}^{-1} \text{ h}^{-1}$  at 360 °C; however, those for Catal-C were  $2.69 \times 10^{-2} \text{ mol g}^{-1} \text{ h}^{-1}$  at 320 °C and  $5.50 \times 10^{-2} \text{ mol g}^{-1} \text{ h}^{-1}$  at 360 °C, respectively.

In summary, the concentration of synthesized  $\text{NH}_3$  with low conversion rates under moderate conditions can be obtained in real-time with the highly sensitive CTI-TOFMS. The high-time-resolution continuous monitoring of the microreactions could acquire the activity changes of the studied catalysts in catalysis process. It should be noticed that the RSDs of the  $\text{O}_2^+$  ion intensity were all smaller than 0.5% during the microcatalytic reactions, which implies excellent stability of the CTI-TOFMS method with the self-adjustment algorithm.

## CONCLUSION

In this study, a high-sensitivity and high-time-resolution CTI-TOFMS method was presented for long-term real-time monitoring of ammonia during microcatalytic synthesis reaction with a time resolution of 30 s. A self-adjustment algorithm was used to stabilize the peak intensity of  $\text{O}_2^+$  ions in the VUV-lamp-based CTI ion source for accurate quantification and wide linear dynamic range (0.2–1000 ppmv) during long-term monitoring. The microcatalytic reaction of feed gas  $\text{N}_2/\text{H}_2$  1:3 (vol) with three different catalysts prepared by transition-metal/carbon nanotubes were tested, and the rapid changes of  $\text{NH}_3$  conversion rates with the reaction temperatures were monitored with a time resolution of 30 s. The high-time-resolution monitoring data indicates that CTI-TOFMS can obtain the equilibrium conversion rates of  $\text{NH}_3$  rapidly and provide information about the activity of investigated catalysts during catalytic reaction process.

Combined with intelligent self-adjustment and proper preset intensity of the reagent ions, the high time resolution of CTI-TOFMS provides a promising tool for long-term monitoring of various reaction processes besides ammonia microcatalytic synthesis reaction. With the technique, not only the conversion rates of the products but also the information on product distribution at different reaction stages can be acquired to evaluate the activities of the studied catalysts and to explore the reaction mechanism and pathways.

## ASSOCIATED CONTENT

### Supporting Information

Additional information as noted in the text. This material is available free of charge via the Internet at <http://pubs.acs.org/>.

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### Notes

The authors declare no competing financial interest.

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