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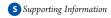
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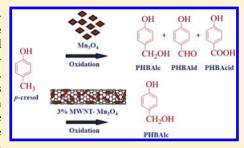
# Selectivity Tailoring in Liquid Phase Oxidation Over MWNT-Mn<sub>3</sub>O<sub>4</sub> Nanocomposite Catalysts

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**ABSTRACT:** Highly selective multiwalled nanotubes (MWNT)-Mn<sub>3</sub>O<sub>4</sub> nanocomposite catalyst was designed for liquid phase oxidation of p-cresol, which gave highest selectivity of 90% to the first step oxidation product, p-hydroxy benzyl alcohol. Mn<sub>3</sub>O<sub>4</sub> nanoparticles and MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposites were synthesized by coprecipitation route using mixed precursors under controlled conditions. The phase purity of Mn<sub>3</sub>O<sub>4</sub> and the formation of MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposites were confirmed by X-ray diffraction, Raman spectroscopy, and X-ray photoelectron spectroscopy. High-resolution transmission electron microscopy revealed the selective exposure of (101) and (001) planes of Mn<sub>3</sub>O<sub>4</sub> nanoparticles in the MWNT-Mn<sub>3</sub>O<sub>4</sub> composite, while lowering in oxidizing capacity of MWNT-Mn<sub>3</sub>O<sub>4</sub>



nanocomposite confirmed by cyclic voltametry was due to incorporation of electron rich MWNT. Thus, selectivity tuning of the new material (MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite) was found to be due to alteration in both geometric as well as electronic properties. A plausible reaction pathway also has been proposed involving the predominant role of nucleophilic lattice oxygen ( $O^{2-}$ ) species due to exposure of particular crystal planes giving highest selectivity to *p*-hydroxy benzyl alcohol.

#### 1. INTRODUCTION

Catalytic liquid phase oxidation of alkyl groups in substituted phenols is a core technology in fine chemicals and pharmaceutical industries.<sup>1-4</sup> Therefore developing new materials by modifying their intrinsic properties has been a continuing effort for the last two decades. 5-8 The major challenges in developing new catalysts are (i) stability of the metal function without leaching under oxidation conditions, (ii) maintaining activity in the presence of antioxidizing substrates like cresols, (iii) tailoring selectivity to the desired oxidation products, particularly to the first step oxidation product, and (iv) minimizing reaction time as well as the catalyst concentration. p-Cresol oxidation is an example of industrial oxidation process which involves stepwise oxidation to give a mixture of p-hydroxy benzyl alcohol, p-hydroxy benzaldehyde, and p-hydroxy benzoic acid depending upon the catalyst used and reaction conditions. 5-7,9,10 Among these, both alcohol and aldehyde derivatives are important intermediates for the manufacture of vanillin (a widely used flavoring agent), trimethoxy benzaldehyde, various agrochemicals, and pharmaceuticals such as semisynthetic penicillin, amoxicillin, and the antiemetic drug trimethobenzamide. 4,11,12 Efficient catalysts for oxidation reactions mainly involve oxides of transition metals having capability to form redox couples. In particular, Co-based catalysts systems and metals such as Cu, Mn supported on molecular sieves, carbon, or resins have been extensively studied for this oxidation reaction. 13-16 Apart from this,  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub> has also been used as efficient catalyst, but it has

been used for the oxidation of first step oxidation product of p-cresol, that is, p-hydroxy benzyl alcohol. <sup>17</sup> Among different types of catalysts, nanostructured catalysts showed higher activity than their bulk counterparts as shown in our work on nanostructured Co<sub>3</sub>O<sub>4</sub> catalysts, <sup>18</sup> which could not only be due to the size reduction (high surface/volume ratio) alone but also the modified adsorption characteristics caused by geometric and electronic effects. Hence this work was undertaken to further explore and understand the fundamental aspects of the nanostructured materials that govern their performance, especially their role in directing the selectivity pattern in a consecutive oxidation reaction. For this purpose, we have synthesized nanostructured Mn<sub>3</sub>O<sub>4</sub> and its composites with multiwalled carbon nanotube (MWNT) in different degrees of loading and investigated the correlation between its constitution, structural aspects, and the activity for oxidation of p-cresol. Mn<sub>3</sub>O<sub>4</sub> alone has been reported for catalytic oxidation of methane, carbon monoxide,  $^{19}$  decomposition of NO and  $N_2O$ ,  $^{20-22}$  deoxygenation of nitrobenzene, <sup>23</sup> while MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite has been studied for only supercapacitor and magnetism applications. 24,25 To the best our knowledge, ours is a first report of highly selective MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite developed for selective liquid phase oxidation of p-cresol to intermediate p-hydroxy benzyl

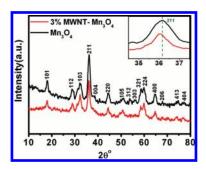
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alcohol under mild conditions. The selective formation of intermediate p-hydroxy benzyl alcohol in a sequential oxidation of p-cresol could be attributed to the alterations in geometric as well as electronic characteristics of  $Mn_3O_4$  by introducing electron rich rigid material like MWNT. The role of both these aspects has been studied in detail by high-resolution transmission electron microscopy (HR-TEM), X-ray diffraction (XRD), X-ray photoelectron spectroscopy (XPS), Raman spectroscopy and cyclic voltametry (CV).

#### 2. EXPERIMENTAL SECTION

- **2.1. Materials.** Manganese acetate tetrahydrate, ethanol, and xylene were obtained from Merck. Oleylamine was taken from Fluka. *p*-Cresol was supplied by Loba Chemie, while sodium hydroxide was obtained from Merck. MWNT was purchased from Aldrich Chemicals. Analytical grade and HPLC grade methanol and *n*-propanol were obtained from Rankem.
- 2.2. Catalyst Preparation. Nanostructured Mn<sub>3</sub>O<sub>4</sub> was prepared using manganese acetate, oleylamine, xylene, and ethanol by coprecipitation method.<sup>26</sup> In order to prepare 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite, commercially available MWNT was first functionalized with HNO3 and H2SO4 in 1:3 ratio. In a typical procedure, 0.24 g of manganese acetate and 0.0075 g of functionalized MWNT were properly dispersed in xylene at room temperature for 30 min. To this, 4 mL of oleylamine was added and this mixture was then transferred to a round-bottom flask that was heated from room temperature to 363 K under stirring. After the temperature reached 363 K, 1 mL H<sub>2</sub>O was added and the stirring was continued at this temperature for 3 h. Then the mixture was cooled to room temperature, and highly dispersed 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite was made to settle down by the addition of sufficient amount of ethanol. Then the solid material was isolated by centrifugation. The nanocomposite powder thus obtained was dried at 333 K for 3 h. The same procedure was followed for the synthesis of other MWNT-Mn<sub>3</sub>O<sub>4</sub> composites with different degrees of loadings by varying the ratio of Mn<sub>3</sub>O<sub>4</sub> to MWNT.
- 2.3. Characterization of Catalysts. The synthesized catalyst samples were characterized by X-ray powder diffraction using Philips X'Pert PRO diffractometer with nickel-filtered Cu  $K_{\alpha}$ radiation, Raman spectroscopy using LabRAM HR800 from JY Horiba, high-resolution transmission electron microscopy using IFEI, Tecnai F30, with 300 KV FEG and field-emission scanning electron microscopy (FESEM; Hitachi S-4200). The surfaces of the catalysts were examined by X-ray photoelectron spectroscopy on a VG scientific ESCA-3000 spectrometer using nonmonochromatized Mg  $K_{\alpha}$  radiation (1253.6 eV) at a pressure of about  $1 \times 10^{-9}$  Torr. The surface area values of all the samples were determined by Brunauer-Emmett-Teller (BET) adsorption method (Quadrasorb automatic volumetric instrument). The percentage metal oxide loading was calculated from ICP (inductive coupled plasma) analysis with Spectro 165 highresolution ICP-OES Spectrometer (model no. ARCOSFHS12). All the cyclic voltametry measurements were done with Autolab PGSTAT30 (Eco-Chemie)
- **2.4. Catalytic Activity.** All the catalytic oxidation reactions were carried out in a 300 cm<sup>3</sup> capacity high-pressure Hastelloy reactor supplied by Parr Instruments Co. U.S.A. The reactor was connected to an air reservoir held at a pressure higher than that of the reactor. A Hewlett-Packard model 1050 liquid chromatograph equipped with an ultraviolet detector was used for the



**Figure 1.** XRD spectra of  $Mn_3O_4$  and 3% MWNT- $Mn_3O_4$ ; inset shows shift of (211) peak toward lower  $2\theta$  due to addition of MWNT.

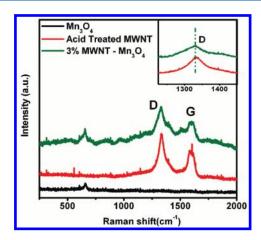
analysis. HPLC analysis was performed on a 25 cm RP-18 column supplied by Hewlett-Packard. The products and reactants were detected using a UV detector at  $\lambda_{\rm max}=223$  nm. Aqueous methanol (35%) was used as mobile phase at a column temperature of 308 K and a flow rate of 1 mL/min. Samples of 10  $\mu$ L were injected into the column using an auto sampler HP 1100.

In a typical experiment, 3 g of p-cresol, 4.5 g of NaOH, and 70 cm<sup>3</sup> of *n*-propanol were heated in a flask with a reflux condenser until the NaOH dissolved completely. This reaction mixture was charged to a 300 cm<sup>3</sup> par autoclave. Then 0.02 g catalyst was added, and the reaction mixture was heated to 373 K. After the desired temperature was attained, the reactor was pressurized with 6.5 bar nitrogen and 2.4 bar oxygen. Then the reaction was started by agitating at 900 rpm. When the pressure decreased, the reactor was again filled by oxygen. This was continued up to 2 h. The progress of the reaction was monitored by observing the pressure drop in the reservoir vessel as a function of time. After 2 h the reactor was cooled to room temperature and the unabsorbed nitrogen gas was vented out. Then the content of the reactor was discharged and the final volume was noted down. The final samples were analyzed by HPLC.

#### 3. RESULTS AND DISCUSSION

3.1. Catalyst Characterization. As shown in Figure 1, the XRD patterns of both Mn<sub>3</sub>O<sub>4</sub> and 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposites were identical with an intense peak at  $2\theta = 36^{\circ}$ corresponding to (211) plane. The other peaks of lower intensity were also identical for both the samples and matched with those of tetragonal hausmannite phase (JCPDS card no. 24-0734). In both samples, no other peaks corresponding to any impurity phase(s) were seen, confirming that the product was tetragonal  $Mn_3O_4$ . In order to distinguish  $Mn_3O_4$  from  $\gamma$ - $Mn_2O_3$ , which has similar structure and unit cell parameter as that of Mn<sub>3</sub>O<sub>4</sub>, <sup>27</sup> our samples were also characterized by other techniques, which are discussed below. No signature of MWNT was observed in the XRD spectra of MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite due to low concentration (only a few percent) of MWNT in the composite. Also there is a considerable shift in the peaks of MWNT-Mn<sub>3</sub>O<sub>4</sub> composites toward lower  $2\theta$  value as shown in the inset of Figure 1. This shift in the peak is due to the strain involved during the formation of nanocomposites.

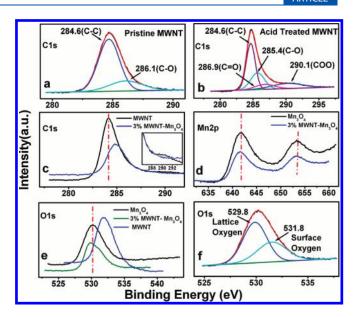
The Raman spectra for  $Mn_3O_4$ , MWNT, and MWNT- $Mn_3O_4$  nanocomposite are shown in Figure 2. A single intense peak at 659 cm<sup>-1</sup> confirmed the highly pure phase of the synthesized  $Mn_3O_4$ . In the case of the MWNT sample, the two peaks



**Figure 2.** Raman spectra of Mn<sub>3</sub>O<sub>4</sub>, acid treated MWNT, 3% MWNT-Mn<sub>3</sub>O<sub>4</sub>; inset shows broadening of D band.

observed at 1328 and 1579 cm<sup>-1</sup> correspond to D and G bands, respectively, which match well with those reported in the literature.<sup>29</sup> In the case of 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite sample, distinct peaks corresponding to MWNTs as well as Mn<sub>3</sub>O<sub>4</sub> are observed. The interesting feature of the Raman spectra of MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite is the broadening of the Mn<sub>3</sub>O<sub>4</sub> and MWNT peaks as compared to the bare Mn<sub>3</sub>O<sub>4</sub> nanoparticles and MWNT case. The broadening of D band of MWNT is shown in the inset of Figure 2. Such a broadening can occur because of two possibilities viz. (i) strain gradient originating from interface integration during the formation of MWNT-Mn<sub>3</sub>O<sub>4</sub> composite, which involves anchoring of Mn<sub>3</sub>O<sub>4</sub> on the molecular moiety like -COOH due to functionalization of MWNT and/or (ii) slightly broader particle size distribution, which in the present case was in the range of 12-15 nm. This increase in particle size can also be correlated with the inset figure in XRD spectra which was shown in Figure 1, where the peak is slightly broader in the case of Mn<sub>3</sub>O<sub>4</sub> than 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite. In addition, the nanosized nature of the material leads to a higher concentration of surface atoms and attendant phonon softening that can contribute to peak broadening. Such broadening is also reported in the case of TiO<sub>2</sub>-MWNT nanocomposite.

X-ray photoelectron spectroscopy was used to determine the surface oxidation states of all the species present in the bare Mn<sub>3</sub>O<sub>4</sub> nanoparticles and various percentages of nanocomposites (Figure 3a-f). Figure 3a,b show the C1s XPS spectra of pristine MWNT and acid-functionalized MWNT, respectively. Please note the different energy (x-axis) scales on the two figures. In the case of pristine MWNT, the C1s peak can be resolved into two peaks that represent presence of two distinct chemical states of carbon on the surface of MWNT. The peak at the binding energy 284.6 eV corresponds to C-C carbon, 31 and the peak at 286.1 is due to C-O carbon. Upon acid functionalization of MWNT, the C1s peak structure is seen to be modified significantly. After deconvolution, it exhibits four contributions for the best fit. The most resolved peak located at 284.6 eV is once again assigned to the C-C bonds, while the other three peaks having binding energies of 285.4, 286.9, and 290.1 eV correspond to carbon in the C-O, carbonyl (C=O), and carboxyl (-COOH) bonds, respectively. 24,32,33 Emergence of the new contributions clearly signifies introduction of polar oxygen groups into the surface of MWNT.



**Figure 3.** XPS spectra of (a) C1s spectra of pristine MWNT, (b) C1s spectra of acid treated MWNT, (c) comparison of C1s spectra of MWNT, 3% MWNT-Mn<sub>3</sub>O<sub>4</sub>. Inset shows the enlarged view of the 285 to 295eV binding energy region. (d) comparison of Mn2p spectra for Mn<sub>3</sub>O<sub>4</sub>, 3% MWNT-Mn<sub>3</sub>O<sub>4</sub>, (e) comparison of O1s XPS spectra Mn<sub>3</sub>O<sub>4</sub>, 3% MWNT-Mn<sub>3</sub>O<sub>4</sub>, MWNT, and (f) O1s spectra of 3% MWNT-Mn<sub>3</sub>O<sub>4</sub>.

The C1s spectra of MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite (3% case shown, others at low concentrations being nominally similar) and MWNT nanoparticles are compared in Figure 3c, which reveals a significant shift toward the higher binding energy in the case of the nanocomposites. This shift can be attributed to the considerable strain imparted to the C–C bond configuration of MWNT and the related modification of the electronic environment due to the anchoring of Mn<sub>3</sub>O<sub>4</sub> nanoparticles on the surface of MWNT. The inset to Figure 3c is the enlarged view of the same spectra in the region of the binding energy from 285 to 295 eV. A distinct hump is clearly seen around 290 eV in the spectrum of MWNT that is due to the carboxylic group on the surface of MWNT. But this hump is absent in the case of the nanocomposite. This signifies the attachment of Mn<sub>3</sub>O<sub>4</sub> to the carboxylic oxygen present on the surface of MWNT.

Figure 3d shows the comparison of the Mn2p XPS spectra for 3% MWNT-Mn $_3$ O $_4$  nanocomposite and bare Mn $_3$ O $_4$  nanoparticles. These two spectra are nearly similar having almost equal binding energy. The peak at a binding energy of 641.7 eV is due to Mn2p3/2 and the peak at 653.3 eV is assigned to Mn2p1/2. These binding energy values match with the reported values for Mn $_3$ O $_4$ .  $^{24,34-36}$ 

The comparison of O1s spectra for MWNT, bare Mn<sub>3</sub>O<sub>4</sub>, and 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> are shown in Figure 3e. Comparing all the O1s spectra, it can be seen that there is a shift in the case of the nanocomposites toward lower binding energy, which is again due to the strain involved during the formation of composites. The O1s peaks for the nanocomposites are more similar to the O1s peak of bare Mn<sub>3</sub>O<sub>4</sub>, which is due to the uniform dispersion of Mn<sub>3</sub>O<sub>4</sub> nanoparticles on the surface of MWNT with good surface coverage. The binding energy for O1s is shown in Figure 3f for the case of 3% MWNT-Mn<sub>3</sub>O<sub>4</sub>. After deconvolution, the peak shows two contributions. The peak at a binding energy of 529.8 eV is due to the lattice oxygen and the peak present at 531.8 eV can be attributed to either surface OH groups or other oxygen containing groups.<sup>34</sup>

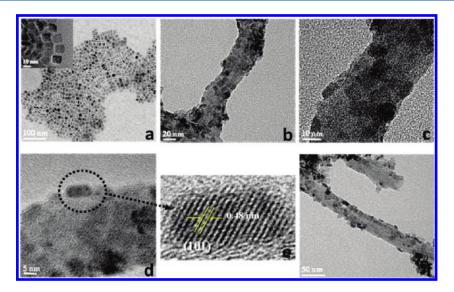


Figure 4. (a) HR-TEM image of  $Mn_3O_4$ ; inset is a high-magnification image showing 8-10 nm particles. (b-f) HR-TEM image of 3% MWNT- $Mn_3O_4$ .

Table 1. BET Surface Area Measurements of  $Mn_3O_4$ , MWNT, 3% MWNT- $Mn_3O_4$ 

Sl. no	catalyst	BET surface area $(m^2/g)$
1	$Mn_3O_4$	65.89
2	3% MWNT-Mn <sub>3</sub> O <sub>4</sub>	20.14
3	MWNT	15.5

Figure 4a shows HR-TEM image of Mn<sub>3</sub>O<sub>4</sub>, revealing highly faceted morphology with a nanoparticle size in the range of 8–10 nm (Figure 4a inset). As shown in Figure 4b–f, MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite is again faceted type but with some degree of elongation along the MWNT length. This could be attributed to the anisotropic surface diffusion of adsorbed species and the differential role of axis vs curvature. These nanoparticles are seen to be uniformly dispersed on the MWNT surface with a size distribution of  $\sim$ 12-15 nm (Figure 4c,d). Figure 4e is a section of a Mn<sub>3</sub>O<sub>4</sub> nanoparticle showing the axial growth in the direction of (101) with a lattice spacing of 0.48 nm and the other exposed side along the (001) plane. This was inferred from the interplane angle measured directly from the HR-TEM image. All these HR-TEM images of MWNT-Mn<sub>3</sub>O<sub>4</sub> composites indicate that most of the exposed sides of Mn<sub>3</sub>O<sub>4</sub> nanoparticles were along two specific planes (101) and (001).

Table 1 shows the surface area values for bare  $Mn_3O_4$  and the MWNT- $Mn_3O_4$  nanocomposites. The surface area of the bare  $Mn_3O_4$  nanoparticles was found to be 65.8  $m^2/g$ , which is seen to decrease substantially (to about 20  $m^2/g$ ) in the case of the 3% MWNT- $Mn_3O_4$  nanocomposite. This decrease in the surface area of nanocomposites could be due to the dispersion of  $Mn_3O_4$  on a confined area of the MWNT matrix. This is also in accordance with the increase in particle size from 8–10 nm to 12–15 nm of bare  $Mn_3O_4$  and  $MWNT-Mn_3O_4$  nanocomposites, respectively. The surface area of only MWNT was found to be 15  $m^2/g$ . In the nanocomposite, the  $Mn_3O_4$  nanoparticles are anchored uniformly on the surface of MWNT, shielding some portion of the MWNT surface and dominating the  $m^2/g$  area estimate, albeit with somewhat enhanced size (12–15 nm).

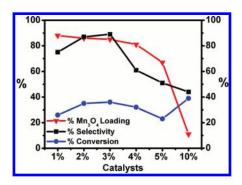


Figure 5. Percentage loading of  ${\rm Mn_3O_4}$  from ICP analysis in comparison with selectivity and conversion.

The percent loading of metal oxide in the composites was studied by ICP analysis. The highest metal loading of 88% was observed for the case of 1% MWNT-Mn<sub>3</sub>O<sub>4</sub> catalyst (Figure 5). The percent loading slightly decreased from 88 to 86 and 85% for 2 and 3% MWNT cases, respectively. Beyond 3% MWNT case, the metal oxide loading decreased continuously and significantly to 11% in the case of 10% MWNT, the maximum MWNT concentration examined in this work. The percent conversion and the selectivity patterns roughly follow similar trend as a function of nanocomposite composition, except for the 10% case. Also they bear an interesting nonmonotonic correlation, vis a vis, the metal oxide loading. The % selectivity is seen to increase up to 90% in the case of 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> and then decreases. This could be explained by the relative degree of heterogeneous and homogeneous nucleation of Mn<sub>3</sub>O<sub>4</sub> nanoparticles. At low MWNT concentration (e.g., the 1% MWNT-Mn<sub>3</sub>O<sub>4</sub> case), due to less concentration of MWNT it is possible that a fraction of Mn<sub>3</sub>O<sub>4</sub> nanoparticles is formed by homogeneous nucleation and the same is not anchored on MWNT leading to higher performance. With increasing percent of MWNT to 2 and 3%, more Mn<sub>3</sub>O<sub>4</sub> nanoparticles would form on the surface of MWNT and homogeneous nucleation contribution should decrease (Figure 6) leading to increasing conversion and selectivity. For further increase in MWNT percent (e.g., 4-10%), although all

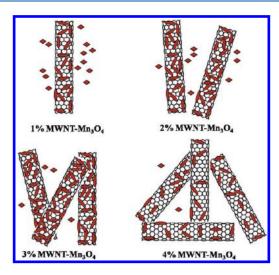


Figure 6. Possible homogeneous and heterogeneous nucleation of  $Mn_3O_4$  nanoparticles in 1-4% MWNT- $Mn_3O_4$  nanocomposites.

## Scheme 1. Reaction of p-Cresol

the nanoparticles would form on the MWNT surface, the exposed MWNT surface containing acid groups would get exposed more and more, leading to the formation of nonoxidation products. This would then decrease the selectivity considerably, as observed.

**3.2. Activity Measurement.** The activity results of bare Mn<sub>3</sub>O<sub>4</sub> and MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposites for the oxidation of *p*-cresol are discussed on the basis of conversion of *p*-cresol and selectivity to various products. The % conversion and selectivity were calculated by using eqs 1 and 2 respectively as follows

$$\%\textit{Conversion} = \frac{\textit{C}_{i} - \textit{C}_{f}}{\textit{C}_{i}} \times 100 \tag{1}$$

$$\% \textit{Selectivity} = \frac{C_p}{C_x} \times 100 \tag{2}$$

where

 $C_i$  = initial concentration of p-cresol

 $C_{\rm f}$  = final concentration of *p*-cresol

 $C_p$  = concentration of product formed

 $C_x$  = concentration of p-cresol consumed

In order to study the product distribution, a few preliminary experiments of p-cresol oxidation were carried out using  $\rm Mn_3O_4$  and  $\rm MWNT\text{-}Mn_3O_4$  nanocomposites in n-propanol solvent under high-pressure conditions. The progress of the reaction was monitored by liquid phase analysis as a function of time. It was observed that the initial oxidation product was p-hydroxy benzyl alcohol that undergoes further oxidation to give p-hydroxy benzaldehyde and p- hydroxyl benzoic acid. On the basis of

this the reaction pathway of p- cresol oxidation is shown in Scheme 1.

Results on catalyst screening for *p*-cresol oxidation are shown in Figure 7. Bare Mn<sub>3</sub>O<sub>4</sub> shows 46% conversion of p- cresol and a selectivity of 43% toward p-hydroxy benzyl alcohol, the remaining constituents being p-hydroxy benzaldehyde and p-hydroxy benzoic acid. p-cresol conversion decreased to 26 and 35% in the case of 1 and 2% MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposites. In the case of 3% MWNT-Mn<sub>3</sub>O<sub>4</sub>, the conversion remains almost same, that is, 36%. But conversion decreases in the case of 4 and 5%, which was 32 and 23%, respectively. This decrease in *p*-cresol conversion for MWNT-Mn<sub>3</sub>O<sub>4</sub> composite was not in the proportion to the decrease in surface area from 65 to 20 m<sup>2</sup>/g for the change in material from bare Mn<sub>3</sub>O<sub>4</sub> to MWNT-Mn<sub>3</sub>O<sub>4</sub> composite respectively. Nevertheless, the decrease in surface area was attributed to the dispersion of Mn<sub>3</sub>O<sub>4</sub> on a confined area of MWNT that also might restrict the access of substrate molecules to the active sites on the surface of catalyst. This explanation is supported by a separate oxidation experiment carried out using a physical mixture of 3% MWNT and Mn<sub>3</sub>O<sub>4</sub> in which 42% conversion of p-cresol was obtained which was very close to that obtained for bare Mn<sub>3</sub>O<sub>4</sub>. This experiment also showed that the selectivity of p-hydroxy benzyl alcohol is due to the composite formation only.

It is interesting to note a steep increase in the selectivity to an intermediate product, *p*-hydroxy benzyl alcohol up to 90% for both 2 and 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> composite catalysts as compared to 43% in the case of bare Mn<sub>3</sub>O<sub>4</sub>. *p*-Cresol oxidation over a variety of heterogeneous catalysts reported so far (Supporting Inforamtion, Table 1), has shown mainly the formation of *p*-hydroxy benzaldehyde. Thus, the challenging task of obtaining the highest selectivity up to 90% toward first step oxidation product (*p*-hydroxy benzyl alcohol) was achieved by 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposites. The critical role of addition of MWNT on the selectivity pattern is discussed in detail below.

In the case of the MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposites, selective exposure of two planes (101) and (001) of Mn<sub>3</sub>O<sub>4</sub> was observed due to the structured support unlike the case of bare Mn<sub>3</sub>O<sub>4</sub> where several planes can be exposed to the substrate molecules. Such correlations between the exposure of selective planes and catalytic activity have been reported. <sup>37,38</sup> Figure 8a represents the crystal structure of Mn<sub>3</sub>O<sub>4</sub>, which corresponds to a normal spinel structure with Mn<sup>2+</sup> and Mn<sup>3+</sup> in tetrahedral and octahedral sites, respectively. The selectively exposed planes (001) and (101) appear as shown in Figure 8b,c, respectively, which clearly indicate that the (001) plane contains only Mn3+ species and the (101) is composed of a mixture of Mn<sup>3+</sup> and Mn<sup>2+</sup> species. Between Mn<sup>3+</sup> and Mn<sup>2+</sup> species, Mn<sup>3+</sup> is active for oxidation of p-cresol, because of its ability to be reduced to Mn<sup>2+</sup> thus forming a redox couple  $(Mn^{3+} \leftrightarrow Mn^{2+})$ . A plausible mechanistic pathway for p-cresol oxidation over MWNT-Mn<sub>3</sub>O<sub>4</sub> composite is shown in Figure 9. This oxidation pathway is proposed considering the role of lattice oxygen as a primary oxidant in the oxidation process. <sup>23,39-41</sup>As shown in Figure 9, the first step involves the adsorption of p-cresol molecule on the  $\mathrm{Mn}^{3+}$  sites followed by C-H bond polarization. 42 Formation of C-O bond takes place by the abstraction of one of the lattice oxygen associated with Mn3+, which in turn gets reduced to Mn2+ as shown in the second step. The lattice oxygen vacancy created on the  $Mn^{3+}$  site is compensated by the neighboring  $Mn^{2+}$  atom. Concurrently, the electron produced at the Mn3+ center is transferred to the neighboring Mn<sup>2+</sup> site. The molecular oxygen

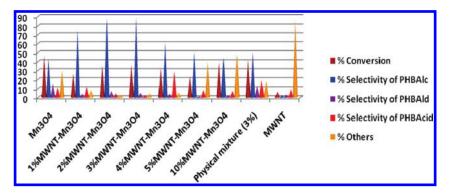


Figure 7. Activity results of the catalysts.

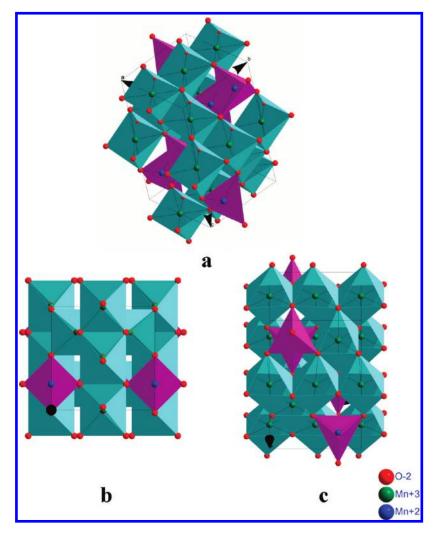
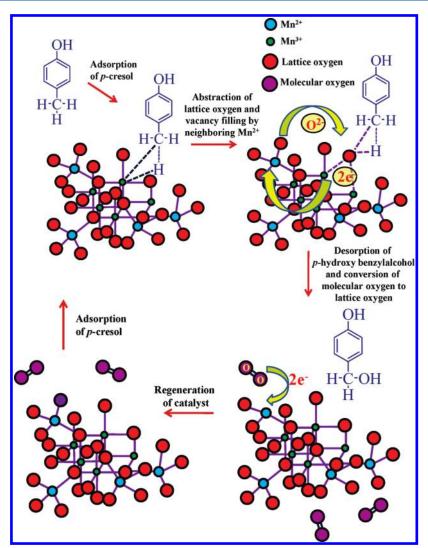


Figure 8. Crystal structure of (a) normal spinel  $Mn_3O_4$ , (b) (001) plane of  $Mn_3O_4$  spinel showing only  $Mn^{3+}$ , and (c) (101) plane of  $Mn_3O_4$  showing both  $Mn^{2+}$  and  $Mn^{3+}$ .

is adsorbed on the vacant  $\mathrm{Mn}^{2+}$  site and it gets converted to lattice oxygen to replenish the oxygen loss. The last step involves desorption of p-hydroxy benzyl alcohol leading to the regeneration of catalyst, and another p-cresol molecule gets adsorbed and the cycle is repeated. Thus,  $\mathrm{Mn}^{2+}$  and  $\mathrm{Mn}^{3+}$  maintain a catalytic redox cycle for the conversion of molecular oxygen to lattice oxygen ( $\mathrm{O}^{2-}$ ) and hence the reoxidation of active centers ( $\mathrm{Mn}^{3+}$ ) takes place. Apart from the nucleophilic

lattice oxygen species  $O_2^{-}$ , some other reactive electrophilic oxygen species such as  $O_3^{-}$  and  $O_2^{-}$  are also formed from the molecular oxygen. However, it is considered that the formation of nucleophilic lattice oxygen species on the surface are responsible for selective oxidation, while the electrophilic oxygen species are considered as strong oxidants leading to deep oxidation products. In the case of the MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite, the formation of lattice oxygen species may be



**Figure 9.** Possible mechanism pathway of oxidation of *p*-cresol to *p*-hydroxy benzyl alcohol.

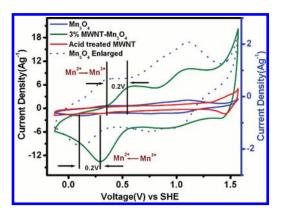


Figure 10. Cyclic voltametry measurements of acid treated MWNT, Mn<sub>3</sub>O<sub>4</sub>, and 3% MWNT-Mn<sub>3</sub>O<sub>4</sub>.

more favored than the formation of electrophilic oxygen species due to the selective exposure of planes. This would lead to the oxidation of *p*-cresol primarily to *p*-hydroxy benzyl alcohol preventing the formation of subsequent oxidation products such as *p*-hydroxy benzaldehyde and *p*-hydroxy benzoic acid.

The selective formation of intermediate *p*-hydroxy benzyl alcohol can be also explained by comparing redox potential profiles of various catalysts obtained by CV measurements. For this purpose, CV measurements were performed at a scan rate of 50 mV s<sup>-1</sup> for the acid-treated MWNT, Mn<sub>3</sub>O<sub>4</sub> nanoparticles, and 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite samples over the potential range of 1.6 to -0.2 V with standard hydrogen electrode (SHE) and 2 M aqueous KCl solution. Figure 10 shows the plots of current density versus potential for all the above cases. Since MWNT did not show any oxidation activity (Figure 7) as expected, no oxidation or reduction peaks were observed. However, Mn<sub>3</sub>O<sub>4</sub> nanoparticles and 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite showed clearly the presence of oxidation and reduction peaks (blue and green respectively, Figure 10). In both cases, the first anodic peak in the low potential region could be assigned to the oxidation of Mn<sup>2+</sup> to Mn<sup>3+</sup>, while the second one to the oxidation of Mn<sup>3+</sup> to Mn<sup>4+</sup>. Similarly, the cathodic peak present at higher potential could be assigned to the reduction of Mn<sup>4+</sup> to Mn<sup>3+</sup> and the second one to the reduction of Mn<sup>3+</sup> to Mn<sup>2+</sup>. Comparison of the reduction peaks of Mn<sub>3</sub>O<sub>4</sub> nanoparticles and 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite, showed a clear and substantial shift (~200 mV) toward higher potential values for 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite. Reduction peak indicates the

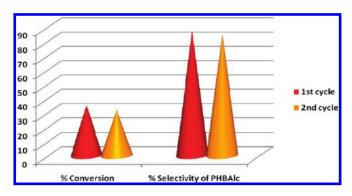


Figure 11. Catalyst recycling results of 3% MWNT-Mn<sub>3</sub>O<sub>4</sub>.

oxygen reduction ability hence, higher the potential value higher is the oxygen reduction ability, that is, lesser oxidizing ability. Thus lesser oxidizing ability of 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> composite than that of Mn<sub>3</sub>O<sub>4</sub> is quiet evident from their CV profiles. Similar study has been reported in the case of iron nitride-doped carbon nanofibers. From this discussion, it can be inferred that Mn<sub>3</sub>O<sub>4</sub> nanoparticles show higher oxidizing ability than that of MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite, which results into deep oxidation giving a mixture of all the sequential oxidation products. Therefore, an electron rich system such as MWNT was deliberately introduced in the present composite to increase the electron density on Mn<sub>3</sub>O<sub>4</sub> that restricts the oxidizing ability of the MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite to achieve highest selectivity to *p*-hydroxy benzyl alcohol.

The selective formation of *p*-hydroxy benzyl alcohol (90%) could also be well correlated with the experimental observation that the moles of oxygen consumed for the p-cresol oxidation over MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposites are lower (0.026 mols) than those consumed over bare Mn<sub>3</sub>O<sub>4</sub> (0.034 mols for 43% selectivity to alcohol and remaining aldehyde and acid) under identical conditions. With an increase in MWNT concentration from 4 to 10%, not only the selectivity to p-hydroxy benzyl alcohol is seen to decrease but also no other sequential oxidation product formation such as aldehyde and acid is noted. Instead other byproduct formation is observed. Similar product distribution was also observed for the case of only acid-treated MWNT where mainly other byproduct formation was observed without any significant conversion to well-defined sequential oxidation products. The decrease in selectivity in the case of 4, 5, and 10% MWNT nanocomposites can thus be attributed to the decrease in the percentage of Mn<sub>3</sub>O<sub>4</sub> loading.

In order to study the stability of our catalysts, the recycling experiments were carried out in the following way: after the first oxidation run with the fresh 3% MWNT-Mn<sub>3</sub>O<sub>4</sub> nanocomposite catalyst, it was filtered out and dried in an oven at 373 K for 3 h and was recharged to the reactor for the subsequent run. The procedure was followed for two subsequent oxidation experiments, and the results are shown in Figure 11. The catalyst was found to retain its activity even after second recycle. Also no leached component of the catalyst was found in the solution under the reaction conditions which is confirmed by its characterization.

# 4. CONCLUSION

The nanocomposites of  $Mn_3O_4$  nanoparticles with functionalized MWNT (% MWNT between 0–10%) synthesized by coprecipitation route show excellent activity for liquid phase

oxidation of *p*-cresol. It was clear from CV analysis that introduction of an electron rich system such as MWNT increased the electron density over  $Mn_3O_4$  that could control the deep oxidation ability resulting in highest selectivity toward the first step oxidation product, that is, *p*-hydroxy benzyl alcohol. Also HR-TEM results reveal the exposure of particular crystal planes (101, 001) of  $Mn_3O_4$  in the case of the nanocomposite that favors the formation of nucleophilic lattice oxygen  $(O^{2-})$  species responsible for the highest selectivity of 90% to *p*-hydroxy benzyl alcohol, which was dramatically higher than that observed for the bare  $Mn_3O_4$  nanoparticles (43%). The catalyst was recycled twice with retention of its activity. No leached components of the catalyst were found in solution under the reaction conditions of the present work.

#### ASSOCIATED CONTENT

**Supporting Information.** A summary of literature on various heterogeneous catalyst systems used for oxidation of *p*-cresol has been given as Table 1 in the Supporting Information. This material is available free of charge via the Internet at http://pubs.acs.org.

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