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PAPER

# Internal structure, hygroscopic and reactive properties of mixed sodium methanesulfonate-sodium chloride particles

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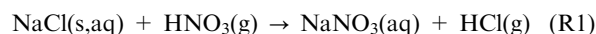
Internal structures, hygroscopic properties and heterogeneous reactivity of mixed CH<sub>3</sub>SO<sub>3</sub>Na/NaCl particles were investigated using a combination of computer modeling and experimental approaches. Surfactant properties of CH<sub>3</sub>SO<sub>3</sub><sup>−</sup> ions and their surface accumulation in wet, deliquesced particles were assessed using molecular dynamics (MD) simulations and surface tension measurements. Internal structures of dry CH<sub>3</sub>SO<sub>3</sub>Na/NaCl particles were investigated using scanning electron microscopy (SEM) assisted with X-ray microanalysis mapping, and time-of-flight secondary ion mass spectrometry (TOF-SIMS). The combination of these techniques shows that dry CH<sub>3</sub>SO<sub>3</sub>Na/NaCl particles are composed of a NaCl core surrounded by a CH<sub>3</sub>SO<sub>3</sub>Na shell. Hygroscopic growth, deliquescence and efflorescence phase transitions of mixed CH<sub>3</sub>SO<sub>3</sub>Na/NaCl particles were determined and compared to those of pure NaCl particles. These results indicate that particles undergo a two step deliquescence transition: first at ~69% relative humidity (RH) the CH<sub>3</sub>SO<sub>3</sub>Na shell takes up water, and then at ~75% RH the NaCl core deliquesces. Reactive uptake coefficients for the particle–HNO<sub>3</sub> heterogeneous reaction were determined at different CH<sub>3</sub>SO<sub>3</sub>Na/NaCl mixing ratios and RH. The net reaction probability decreased notably with increasing CH<sub>3</sub>SO<sub>3</sub>Na and at lower RH.

## Introduction

Over the last few decades, the fundamental kinetics and mechanisms of heterogeneous reactions on atmospheric particles have been of interest due to their impact on the

atmospheric environment and climate change. Sea salt aerosol, generated by wave action and bubble bursting at the ocean surface, have the second largest global burden by mass.<sup>1</sup> Airborne sea salt particles undergo heterogeneous reactions with trace atmospheric species, including OH, HNO<sub>3</sub>, O<sub>3</sub>, NO<sub>2</sub>, N<sub>2</sub>O<sub>5</sub> and ClONO<sub>2</sub>. In some of these reactions, photochemically inert halides present in sea salt can be converted to reactive halogen species X• and XO• (X = Cl and Br). These halogen species can impact the ozone budget and oxidative capacity of the atmosphere.<sup>2</sup>

A noticeable halide deficit in sea salt aerosols is reported in a number of field studies at various geographic locations.<sup>3–9</sup> In regions where sea salt particles are impacted by anthropogenic pollutants, the reaction of gas-phase nitric acid with sodium chloride



is regarded as a major contributor to halide depletion and nitrate enrichment.<sup>10–24</sup> Reaction 1 is also a net sink of atmospheric nitric acid, and hence regulates the gas-particle partitioning of HNO<sub>3</sub> and consequently impacts the atmospheric and aquatic environments.<sup>2,25</sup>

Similarly, sea salt particles also react with biogenic sulfur-containing acids through corresponding aqueous chemistry in deliquesced particles. Dimethyl sulfide (CH<sub>3</sub>SCH<sub>3</sub>, DMS) produced by marine phytoplankton is the largest source of

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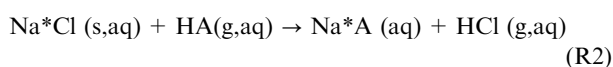
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sulfur containing species over the ocean.<sup>26</sup> DMS undergoes oxidation through a complex series of reactions with gas and liquid phase oxidants through two main pathways: hydrogen abstraction and oxygen addition.<sup>27,28</sup> The H-abstraction channel yields sulfur dioxide (SO<sub>2</sub>) which ultimately forms sulfuric acid (H<sub>2</sub>SO<sub>4</sub>), whereas the oxygen addition produces methanesulfonic acid (CH<sub>3</sub>SO<sub>3</sub>N, MSA) and a number of intermediate products, such as dimethylsulfoxide (CH<sub>3</sub>SOCH<sub>3</sub>, DMSO), dimethylsulfone (CH<sub>3</sub>SO<sub>2</sub>CH<sub>3</sub>, DMSO<sub>2</sub>), and methanesulfonic acid (CH<sub>3</sub>S(O)OH, MSIA).<sup>27,28</sup> Computer models of the multi-phase marine boundary layer (MBL) chemistry show that H<sub>2</sub>SO<sub>4</sub> is the only product that can nucleate new particles.<sup>28</sup> All other products condense onto preexisting sea salt particles where they can also contribute to chloride depletion. Consequently, the HCl acid displacement reaction of sea salt particles can be expressed more generally as:



where HA denotes acids, such as HNO<sub>3</sub>, H<sub>2</sub>SO<sub>4</sub>, SO<sub>2</sub>/H<sub>2</sub>O, MSA, MSIA, and Na\* depicts Na<sup>+</sup> as well as a variety of other cations present in sea salt, *e.g.*, Mg<sup>2+</sup>, K<sup>+</sup>, Ca<sup>2+</sup>. Table 1 shows the standard Gibbs free energies of selected aqueous reactions involving H<sub>2</sub>SO<sub>4</sub>, CH<sub>3</sub>SO<sub>3</sub>N, and HNO<sub>3</sub>. Thermodynamics favor R2 for a wide range of acids. These acid displacement reactions are driven by the release of volatile HCl and reportedly account for the formation of nitrate, non-sea-salt-sulfate (nss-SO<sub>4</sub><sup>2-</sup>) and methanesulfonate in aged sea salt particles.<sup>5,7-9,16,29,30</sup> However, subsequent reactions of CH<sub>3</sub>SO<sub>3</sub>Na and Na<sub>2</sub>SO<sub>4</sub> salts with HNO<sub>3</sub> are not thermodynamically favored. This implies that formation of sulfates and methanesulfonates in sea salt particles reduces their capacity to act as a sink for HNO<sub>3</sub>. Additionally, formation of methanesulfonate in sea salt particles is thermodynamically favored over sulfate formation.

Sea salt particles are naturally multicomponent because of the original complex composition of sea water. Their chemical composition is further complicated by interactions with biogenic and anthropogenic oxidants. These processes lead to composition and concentration changes in sea salt aerosol, and ultimately affect its chemical reactivity and physical properties. For many years, the DMS → SO<sub>2</sub> → H<sub>2</sub>SO<sub>4</sub> reaction sequence was assumed to be the dominant reaction pathway for DMS oxidation in the MBL, and significant attention was given to the physico-chemical properties of the mixed sea salt/sulfate particles.<sup>31-34</sup> However, recent modeling<sup>28</sup> and field studies<sup>30</sup> indicate that under certain conditions the DMS → CH<sub>3</sub>SO<sub>3</sub>H

oxidation pathway contributes substantially and yields elevated concentrations of CH<sub>3</sub>SO<sub>3</sub><sup>-</sup> in sea salt particles. For instance, our recent field study reported characteristic CH<sub>3</sub>SO<sub>3</sub><sup>-</sup>/nss-SO<sub>4</sub><sup>2-</sup> ratios of 0.6 and the total-S/Na ratio of 0.15 in sea salt particles collected in the area of cold ocean current along the northern California coast.<sup>30</sup> Yet, the chemistry and properties of mixed sea salt/methanesulfonate particles have not been well characterized.

Because of rapid aqueous-phase diffusion, most ionic species in liquid (deliquesced) sea salt particles are distributed homogeneously. Nevertheless, surface enhancement or depletion in mixed droplets could occur due to the difference in ion polarizability and lyophobic nature of some species. Unlike nitrate and sulfate ions, methanesulfonate ions are surfactants,<sup>35,36</sup> and accumulate on the surface of deliquesced particles. Since methanesulfonate salts are more soluble than NaCl, the surface accumulation of CH<sub>3</sub>SO<sub>3</sub><sup>-</sup> can be enhanced upon dehydration at decreasing RH.

In this work, we investigate the structure and physical properties of mixed CH<sub>3</sub>SO<sub>3</sub>Na/NaCl particles and the resulting effects of CH<sub>3</sub>SO<sub>3</sub>Na on the hygroscopic properties and chemical reactivity of NaCl particles, which we use as a laboratory proxy for mixed methanesulfonate/sea salt particles. First, we present results of molecular dynamics (MD) simulations and surface tension measurements to infer the internal distribution of ionic species within liquid (deliquesced) particles. Second, we present experimental observations of the morphological/chemical structure of dried particles using methods of microscopic chemical imaging and depth profiling that confirmed shell-core structure of mixed CH<sub>3</sub>SO<sub>3</sub>Na/NaCl particles. Finally, we discuss the observed shell-core structure of particles in the context of the hygroscopic properties and humidity-specific kinetics of their heterogeneous reaction with HNO<sub>3</sub>.

## Computational and experimental methods

### Molecular dynamics calculations

Classical molecular dynamics (MD) simulations of CH<sub>3</sub>SO<sub>3</sub>Na in water and in concentrated aqueous solutions of NaCl and Na<sub>2</sub>SO<sub>4</sub> were performed in the standard aqueous slab geometry<sup>37</sup> with the interfaces perpendicular to the *z*-axis of the simulation box. A tetragonal prismatic unit cell was used with dimensions of 30 Å × 30 Å × 100 Å which contained 864 water molecules. All systems included 10 CH<sub>3</sub>SO<sub>3</sub><sup>-</sup> and Na<sup>+</sup> ions (corresponding to ~0.8 M). In the simulated concentrated solutions, additional 96 Na<sup>+</sup> and Cl<sup>-</sup>, or 192 Na<sup>+</sup> and

**Table 1** Standard Gibbs free energy of reactions<sup>a</sup>

	Reaction	$\Delta G_r^\circ$ (kJ/mol)
i	$\text{NaCl}_{(\text{aq})} + \text{H}_2\text{SO}_{4(\text{aq})} \rightarrow \text{NaHSO}_{4(\text{aq})} + \text{HCl}_{(\text{aq})}$	-11.4
ii	$2\text{NaCl}_{(\text{aq})} + \text{H}_2\text{SO}_{4(\text{aq})} \rightarrow \text{Na}_2\text{SO}_{4(\text{aq})} + 2\text{HCl}_{(\text{aq})}$	-0.1
iii	$\text{NaCl}_{(\text{aq})} + \text{CH}_3\text{SO}_3\text{H}_{(\text{aq})} \rightarrow \text{CH}_3\text{SO}_3\text{Na}_{(\text{aq})} + \text{HCl}_{(\text{aq})}$	> -15.8
iv	$\text{NaCl}_{(\text{aq})} + \text{HNO}_{3(\text{aq})} \rightarrow \text{NaNO}_{3(\text{aq})} + \text{HCl}_{(\text{aq})}$	0
v	$\text{Na}_2\text{SO}_{4(\text{aq})} + 2\text{HNO}_{3(\text{aq})} \rightarrow 2\text{NaNO}_{3(\text{aq})} + \text{H}_2\text{SO}_{4(\text{aq})}$	0.1
vi	$\text{CH}_3\text{SO}_3\text{Na}_{(\text{aq})} + \text{HNO}_{3(\text{aq})} \rightarrow \text{NaNO}_{3(\text{aq})} + \text{CH}_3\text{SO}_3\text{H}_{(\text{aq})}$	6.8
vii	$\text{Na}_2\text{SO}_{4(\text{aq})} + 2\text{CH}_3\text{SO}_3\text{H}_{(\text{aq})} \rightarrow 2\text{CH}_3\text{SO}_3\text{Na}_{(\text{aq})} + \text{H}_2\text{SO}_{4(\text{aq})}$	> -22.5

<sup>a</sup> See Appendix A for values of the Gibbs free energy of formation.

96  $\text{SO}_4^{2-}$  ( $\sim 6$  M) ions were added. By applying periodic boundary conditions at a constant volume, an infinite slab with two water/vapor interfaces perpendicular to the  $z$ -axis was produced.<sup>38</sup>

In all MD simulations the non-bonded interactions were terminated at 12 Å and long-range electrostatic interactions were accounted for using the particle mesh Ewald procedure.<sup>39</sup> The energy of each of the systems was first minimized (10 000 steps of steepest descent minimization) to avoid bad contacts. Then the systems were equilibrated for several hundred picoseconds before a 2 ns simulation run. Simulations were performed at 300 K with 1 fs time steps. Hydrogen bonds were constrained using the SHAKE algorithm.<sup>40</sup> Geometries and energy data were recorded every 500 steps. A polarizable force field was employed in all simulations. For water, the POL3 model<sup>41</sup> was used. Potential parameters for  $\text{CH}_3\text{SO}_3^-$  were constructed using the general amber force field (GAFF) set,<sup>42</sup> while those of other ions were taken from a previous study.<sup>43</sup> Fractional charges for the anions were evaluated using the standard RESP procedure employing the Gaussian 03 package.<sup>44</sup> The partial charges, Lennard-Jones parameters, and polarizabilities of all ions are presented in Table 2. All polarizable molecular dynamics (MD) simulations were performed using the Amber 8 program package.<sup>45</sup>

### Surface tension measurements

The Wilhelmy plate method<sup>46–48</sup> was used to measure equilibrium surface tension of aqueous solutions. Prior to the experiments, a platinum Wilhelmy plate was dipped into a 50:50 (v/v) mixture of nitric and sulfuric acids, washed in deionized water, and heated overnight at 200 °C. The plate was attached to a microbalance *via* a thin metal wire and placed over the bottom of a beaker. An aqueous solution of known concentration was added to the beaker dropwise until the lower edge of the platinum plate was immersed into the water layer. The force on the plate due to wetting was measured by the microbalance and used to calculate surface tension according to the Wilhelmy equation.<sup>46</sup> Measurements were carried out for aqueous solutions of NaCl,  $\text{Na}_2\text{SO}_4$ ,  $\text{NaNO}_3$ ,  $\text{CH}_3\text{SO}_3\text{Na}$  and  $\text{CH}_3\text{SOCH}_3$  over the concentration range of 0.5 to 4 M for each solute.

### Preparation of particle samples for chemical imaging, hygroscopic, and kinetics studies

Nearly monodisperse, mixed  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles were prepared by atomizing an aqueous 0.5 M solution of NaCl and  $\text{CH}_3\text{SO}_3\text{Na}$  (both from Aldrich, Inc., 99.99% purity) with the  $\text{CH}_3\text{SO}_3\text{Na}$ -to-NaCl molar mixing ratio ranging from 0.01 to 0.1.

**Table 2** Parameters of the Lennard-Jones potential ( $\sigma$  and  $\epsilon$ ), polarizabilities ( $\alpha$ ) and partial electric charges used in MD calculations

Ions	Atoms	$\sigma$ (Å)	$\epsilon$ (eV)	$\alpha$	Partial electric charge
$\text{CH}_3\text{SO}_3^-$	C	1.9080	0.1094	0.878	−0.260
	H	1.4870	0.0157	0.135	0.012
	S	2.0000	0.2500	2.900	1.32
	O	1.6612	0.2100	0.434	−0.70
$\text{SO}_4^{2-}$	S	1.9924	0.2500	0.0	2
	O	1.7680	0.2	1.4	−1
$\text{Cl}^-$	Cl	2.4350	0.100	3.69	−1
$\text{Na}^+$	Na	1.319	0.130	0.24	1

Prior to sizing and deposition, the particles were dried in a diffusion drier (TSI, Inc., Model 3062). Dry particles were deposited onto TEM grid substrates (Carbon Type-B, 400 mesh nickel grids, Ted Pella, Inc.) and silicon wafer chips mounted on the impaction plate of the 5th stage of a micro-orifice uniform deposit impactor (MOUDI) (MSP, Inc., Model 110). The aerodynamic cutoff size of the fifth stage is 1.0  $\mu\text{m}$ . As in previous studies,<sup>49–52</sup> the size uniformity of deposited particles was confirmed by computer-controlled scanning electron microscopy (CCSEM) analysis over 2000 particles on several different grids. The number size distributions of deposited  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles were log-normal with median diameters approximately of 0.85  $\mu\text{m}$  ( $\bar{D}_p$ ), measured as equivalent circle diameters of projected areas of particles in microscopy images.

### Particle analyses

Computer-controlled scanning electron microscopy with energy dispersed analysis of X-rays (CCSEM/EDX) was used to determine the elemental composition and loading density of substrate-deposited particles. The microscope is equipped with an EDAX spectrometer (EDAX, Inc., Model PV7761/54 ME) that has an Si(Li) detector 30 mm<sup>2</sup> in active area and an ATW2 window. The system is equipped with *Genesis*<sup>TM</sup> hardware and software (EDAX, Inc.) for computer-controlled analyses. The X-ray spectra were acquired for a period of 10 s under a beam current of  $\sim 500$  pA and an accelerating voltage of 20 kV. For quantification of the EDX results, the *Genesis*<sup>TM</sup> software utilizes a microanalysis method that relates X-ray intensities to elemental concentrations through theoretically calculated equivalent intensities of corresponding peaks.<sup>53</sup> Details of the CCSEM/EDX particle analysis can be found elsewhere.<sup>54</sup>

A TRIFT II time-of-flight secondary ion mass spectrometer (TOF-SIMS) (Physical Electronics, Inc.) was used for imaging and depth profiling of dry  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles. The particles collected on silicon wafer chips were placed in a sample holder and subject to a  $^{69}\text{Ga}^+$  source of primary ions in high-spatial resolution mode. An accelerating voltage of 25 kV and a  $^{69}\text{Ga}^+$  dose rate of  $5.6 \times 10^{17}$  ions cm<sup>−2</sup> were used. A combination of static and dynamic modes of operation allowed depth-profiled speciation of different ions characteristic of individual particles.<sup>52,55</sup>

### Hygroscopic growth experiments

Hygroscopic properties of  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles were studied using a micro-FT-IR spectrometer. Detailed descriptions of the micro-FTIR experimental apparatus, the sample cell, and relevant experimental procedures are reported elsewhere.<sup>51,52</sup> Briefly, the apparatus comprises a Bruker A590 IR microscope equipped with a liquid nitrogen cooled Mercury-Cadmium-Telluride (MCT) detector and interfaced with a FTIR spectrometer (Bruker, Model IFS 66/S). TEM grids containing particle samples are placed in a temperature-controlled sealed environmental stage (Linkam<sup>TM</sup>, Model THMS 600). The RH over the substrate is controlled by a nitrogen flow at  $\sim 1$  L min<sup>−1</sup> with a controlled humidity from a dew point generator (LI-COR<sup>TM</sup>, Model LI-610). A dew point hygrometer (Vaisala<sup>TM</sup>, Model HMP234) measured the RH. Hygroscopic

growth measurements were carried out at room temperature of  $T = 23\text{ }^{\circ}\text{C}$ . Spectra were acquired by co-adding 512 scans at a resolution of  $4\text{ cm}^{-1}$ . The total scan time was 3.2 min. Condensed-phase water was confirmed by the OH stretching and bending modes at  $\sim 3400$  and  $\sim 1640\text{ cm}^{-1}$ , respectively. The integrated absorbance between  $3660$  to  $2750\text{ cm}^{-1}$  (OH stretch) was used to determine deliquescence relative humidity (DRH) and efflorescence relative humidity (ERH).

### Kinetic measurements of $\text{HNO}_3$ heterogeneous uptake on particles

Kinetic uptake coefficient of  $\text{HNO}_3(\text{g})$  on mixed  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles was determined using the Particle-on-Substrate Stagnation Flow Reactor (PSSFR) technique described elsewhere.<sup>49</sup> In each experiment a single TEM grid loaded with  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles of a known number density per sample area ( $N_s$ ) was exposed to a constant flow of nitrogen doped with  $\text{HNO}_3$  and  $\text{H}_2\text{O}$  with known mixing ratios. Flow rate of a  $\text{HNO}_3/\text{H}_2\text{O}/\text{N}_2$  mixture was controlled by mass flow controllers. The reactor was passivated prior to each experiment for a minimum of 2 h with a flow of the  $\text{HNO}_3/\text{H}_2\text{O}/\text{N}_2$  mixture to ensure no significant loss of  $\text{HNO}_3$  on the walls of the apparatus and its gas lines. Particles were first wetted by a flow of moist air ( $\text{RH} = 80\%$ ) generated by a dew point generator (Li-Cor, Inc., Model LI-610) for 2 min prior to switching on a gas stream of the  $\text{HNO}_3/\text{H}_2\text{O}/\text{N}_2$  mixture with selected RH and  $\text{HNO}_3$  concentration. During each experiment, both RH and  $\text{HNO}_3$  concentration were monitored continuously by an inline RH sensor (Honeywell, inc., model HIH4000) and a chemiluminescence  $\text{NO}_y$  analyzer (Thermo Environmental, Inc., model 42C-Y), respectively. The fluctuations were less than 1% and 5% in RH and  $\text{HNO}_3$  concentration, respectively.

The experimental protocol is similar to that used in previous studies.<sup>49,56</sup> CCSEM/EDX analysis was used to measure the overall  $\text{Cl}^-$  loss from the reacted  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles, which can be expressed as follows:

$$-\frac{d[\text{Cl}^-]_d}{dt} = k_I[\text{Cl}^-]_d \quad (1)$$

where brackets denote molar concentration, the subscript  $d$  denotes the NaCl droplet and  $t$  is the reaction time. The apparent, pseudo first-order rate constant  $k_I$  is nearly time invariant over the range of reaction time studied, as shown in the previous NaCl and  $\text{CaCO}_3$  studies,<sup>50,57</sup> and its value may be determined from

$$k_I = -\frac{1}{t} \ln \left( \frac{[\text{Cl}^-]_{d,t}}{[\text{Cl}^-]_{d,t=0}} \right) = -\frac{1}{t} \ln \left( \frac{[\text{Cl}/\text{Na}]_t^{\text{EDX}}}{[\text{Cl}/\text{Na}]_{t=0}^{\text{EDX}}} \right) \quad (2)$$

whereas Cl/Na ratios are measured in individual particles by the CCSEM/EDX analysis. For the approach employed here, a formal stoichiometry of reaction R1 is assumed and changes in  $[\text{Cl}^-]$  are used for rate constant calculations. Previous results<sup>57</sup> demonstrated that the reaction stoichiometry is conserved under these experimental conditions. As will be shown in this work,  $\text{CH}_3\text{SO}_3\text{Na}$  is nearly inert to  $\text{HNO}_3$ . Hence, the presence of a small amount of  $\text{CH}_3\text{SO}_3\text{Na}$  is not expected to affect the stoichiometry of R1. In principle,

enrichments of O and N could be also used for determining  $k_I$ , but quantitative detection of these low-Z elements is not as accurate as Cl detection because of inherent constraints of the CCEM/EDX analysis.<sup>54</sup>

The uptake coefficient was determined from measurements of the pseudo first-order rate constant  $k_I$ , as will be discussed below. The effect of  $\text{CH}_3\text{SO}_3\text{Na}$  on the reactive uptake  $\text{HNO}_3(\text{g})$  on NaCl particles was examined in detail. The uptake coefficients were determined for deliquesced  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles at 80% RH for two  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  mixing ratios (0.05 and 0.1), and a range of particle loadings ( $N_s = 5 \times 10^4$  to  $7 \times 10^6\text{ cm}^{-2}$ ). The limit of low particle loading ( $N_s < 10^5\text{ cm}^{-2}$ ) where the uptake coefficient represents that of a single particle was determined in these experiments, following the procedure established in a previous study.<sup>56</sup> In the second series of experiments, RH = 40% was selected, and  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  mixing ratios were varied from 0.01 to 0.1. To ensure that the uptake coefficient represents that of a single particle, the experiments were performed with a subset of samples with the particle density below  $10^5\text{ cm}^{-2}$ . Experiments were also carried out at 20 and 60% RH to further investigate the humidity effect on the  $\text{HNO}_3$  uptake.

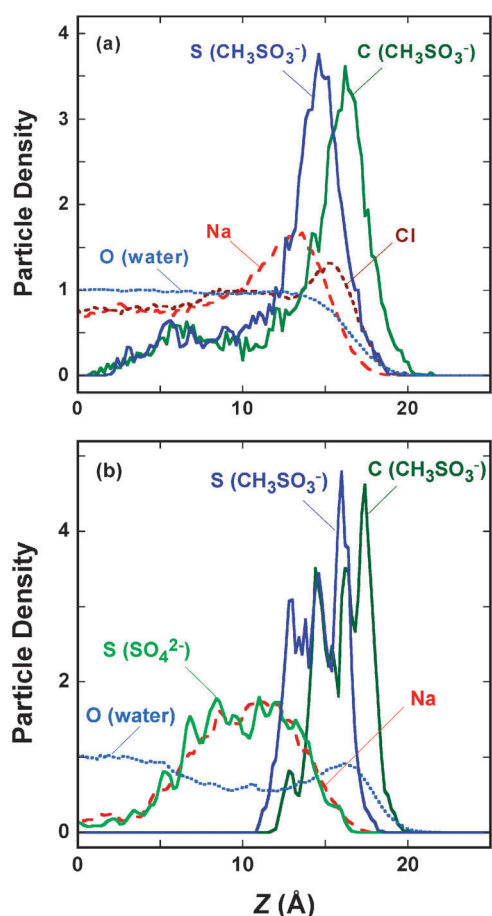
For the vast majority of measurements, free stream  $\text{HNO}_3$  concentrations ranged from 4 to 13.5 ppb, similar to the 10–20 ppb level in polluted environments.<sup>58</sup> High  $\text{HNO}_3$  concentrations ( $\sim 80$  ppb) were used only to probe the reactivity of pure  $\text{CH}_3\text{SO}_3\text{Na}$  with  $\text{HNO}_3$ . Most samples had less than 30% chloride depletion upon exposure to  $\text{HNO}_3$ .

## Results and discussion

### Internal composition of deliquesced and Dry $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$ particles

MD simulations and measurements of surface tension over bulk solutions were used to infer the internal distribution of ionic species in deliquesced  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles. Pure NaCl particles at 75% RH have an approximate water-to-solute ratio (WSR) of 9,<sup>52,59,60</sup> which corresponds to approximately 6 M concentration. To match this ratio, MD modeling included 864 water molecules, 96 NaCl molecules and 10  $\text{CH}_3\text{SO}_3\text{Na}$  molecules simulated in slab geometry. Additional simulations were performed for 864  $\text{H}_2\text{O}$ , 96  $\text{Na}_2\text{SO}_4$  and 10  $\text{CH}_3\text{SO}_3\text{Na}$  molecules to explore the effects of sulfates on the surface partitioning of methanesulfonate. The distribution of species at the air–water interface was quantified using density profiles, *i.e.*, averaged abundances of ions and water molecules across the simulated slab. Fig. 1 shows density profiles of the species present in an  $\sim 0.8\text{ M}$   $\text{CH}_3\text{SO}_3\text{Na}$  aqueous solution with  $\sim 6\text{ M}$  of NaCl (panel a) and  $\sim 6\text{ M}$  of  $\text{Na}_2\text{SO}_4$  (panel b) normalized such that the integrals under all the curves are identical. A strong surface propensity of  $\text{CH}_3\text{SO}_3^-$  is observed in both cases, exemplified by large surface peaks of its C and S atoms. These two density profiles also reveal that this anion prefers an orientation at the surface with the  $\text{SO}_3^-$  group oriented toward the aqueous bulk, and the methyl group pointed into the vapor. This particular orientation is graphically illustrated by a snapshot of the  $\text{CH}_3\text{SO}_3\text{Na}/\text{Na}_2\text{SO}_4/\text{water}$  slab, as shown in Fig. 2 where the



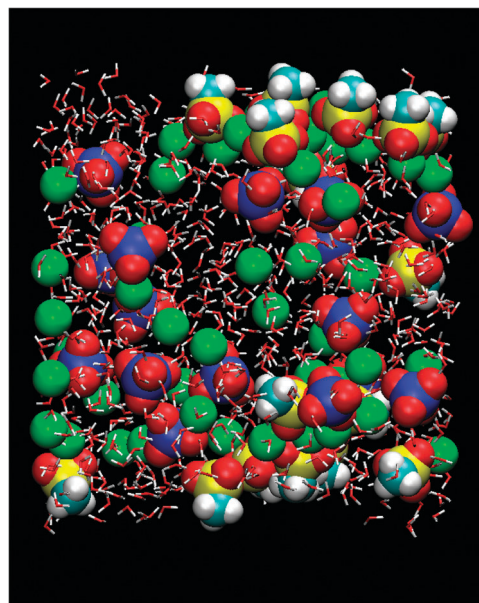


**Fig. 1** Density profiles (arbitrary units) from two molecular dynamics (MD) slab simulations consisting of 864 H<sub>2</sub>O, 96 NaX, and 10 CH<sub>3</sub>SO<sub>3</sub>Na molecules. Panel (a): X = Cl; panel (b): X = SO<sub>4</sub>. Small Z values correspond to slab interior.

solution/vapor interfaces are at the top and bottom of the image. A similar orientation of the hydrophobic methyl group was previously observed for the acetate ion.<sup>61,62</sup> The density profile indicates that chloride ion also exhibits a surface propensity,<sup>63</sup> although this propensity is much weaker than for CH<sub>3</sub>SO<sub>3</sub><sup>−</sup>. In contrast, both sodium and sulfate are repelled from the surface. These two ions have a strong tendency to pair and to aggregate in the subsurface area, which affects the water structure in the surface and subsurface.

Surface tension was extracted from the simulated anisotropy of the pressure tensor.<sup>64</sup> The results suggest a significant decrease of surface tension with an increased CH<sub>3</sub>SO<sub>3</sub>Na concentration (Table 3). Over the concentration range of 0.1 to 2 M, the variation of the surface tension computed is greater than experimental values, which will be reported below. The cause for the discrepancy is likely an overestimated ion pairing (particularly at the interface) due to inaccuracies in the force field.

Fig. 3 shows the experimental surface tension isotherms of aqueous solutions of NaCl, Na<sub>2</sub>SO<sub>4</sub>, NaNO<sub>3</sub>, CH<sub>3</sub>SO<sub>3</sub>Na and CH<sub>3</sub>OCH<sub>3</sub>Na measured at room temperature. Based on the decay of the surface tension with increasing solute concentrations, a characteristic lyophobic behavior for both CH<sub>3</sub>SO<sub>3</sub>Na and CH<sub>3</sub>OCH<sub>3</sub>Na salts is observed. Therefore, CH<sub>3</sub>SO<sub>3</sub>Na tends



**Fig. 2** A snapshot from molecular dynamics (MD) simulation of a slab consisting of 864 H<sub>2</sub>O, 96 Na<sub>2</sub>SO<sub>4</sub>, and 10 CH<sub>3</sub>SO<sub>3</sub>Na molecules. Color coding: Na—green, C—cyan, O—red, H—white, S in SO<sub>4</sub><sup>2−</sup> ions—blue, H—white, S in CH<sub>3</sub>SO<sub>3</sub><sup>−</sup> ions—yellow.

**Table 3** Simulated changes in surface tension  $\Delta\sigma$  of aqueous CH<sub>3</sub>SO<sub>3</sub>Na compared to pure water as a function of concentration. The mean statistical error of these values is  $\sim 1$  dyne/cm

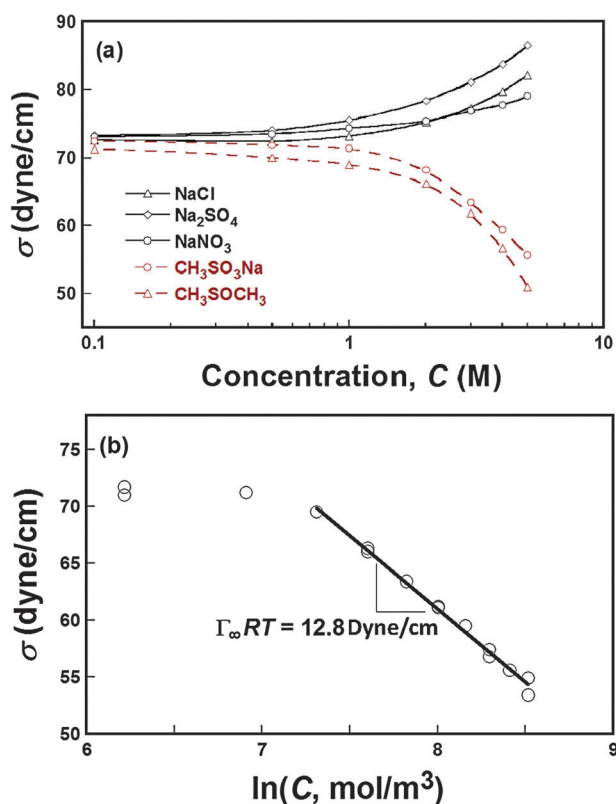
Molarity	$\Delta\sigma = \sigma - \sigma_{\text{H}_2\text{O}}$ (dyne/cm)
0.1	−0.6
0.5	−3.0
1.0	−8.6
1.5	−16.8
2.0	−21.9

to concentrate on the droplet surface, in agreement with the MD results. From the surface tension measurements, the surface concentration of CH<sub>3</sub>SO<sub>3</sub>Na ( $\Gamma$ ) may be estimated from the Gibbs isotherm for an ideal solution,

$$\left(\frac{\partial\sigma}{\partial\ln C}\right)_{p,T} \cong -\Gamma_{\infty}RT, \quad (3)$$

where  $C$  is the molar concentration and  $R$  is the gas constant. For the CH<sub>3</sub>SO<sub>3</sub>Na solutions, the slope from a plot of  $\sigma$  versus  $\ln C$  yields a  $\Gamma_{\infty}RT$  value equal to 12.8 dyne/cm, as shown in Fig. 3b, where  $\Gamma_{\infty}$  denotes the surface concentration of CH<sub>3</sub>SO<sub>3</sub><sup>−</sup> at the saturated limit of an aqueous CH<sub>3</sub>SO<sub>3</sub>Na solution. Based on the value of the slope, we calculated  $\Gamma_{\infty} = 3 \times 10^{14} \text{ cm}^{-2}$  at 298.2 K. This surface concentration corresponds to a surface area of 0.33 nm<sup>2</sup> per molecule. We should note here that in reality the surface concentration can be somewhat different due to non-ideal behavior.

Using the thermodynamic properties and hygroscopic growth data of NaCl particles,<sup>65</sup> at 75% RH, the growth factor of particle size is calculated to be 1.8, *i.e.*, a 0.85  $\mu\text{m}$  dry particle grows to 1.5  $\mu\text{m}$  droplet when deliquesced. At this droplet size, if all CH<sub>3</sub>SO<sub>3</sub>Na molecules are in the surface layer, the minimum molar concentration of CH<sub>3</sub>SO<sub>3</sub>Na



**Fig. 3** (a) Surface tension,  $\sigma$ , as a function of concentration (b) a surface tension isotherm of aqueous  $\text{CH}_3\text{SO}_3\text{Na}$ . Symbols are experimental data; lines in panel (a) are drawn to guide the eye; the line in panel (b) is a linear fit to data.

corresponding to saturated surface coverage is  $\sim 0.0175 \text{ M}$ . Assuming a corresponding  $\text{NaCl}$  concentration of  $6 \text{ M}$ , a  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  ratio greater than  $\sim 0.0035$  would be sufficient to cover the entire particle surface with  $\text{CH}_3\text{SO}_3^-$  ions. This estimated ratio is well below the mixing ratios of  $\sim 0.01$ – $0.1$  characteristic, for instance, for the ambient sea salt particles present along the ocean shore in northern California.<sup>30</sup> Given the surfactant properties of  $\text{CH}_3\text{SO}_3\text{Na}$  and that it does not react with  $\text{HNO}_3(\text{g})$  (see Table 1), we expect that even small amounts of this salt may inhibit the heterogeneous reactivity of the entire  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particle with  $\text{HNO}_3$  (and possibly with other gas-phase species). At a given concentration, the degree to which the droplet surface can be covered by  $\text{CH}_3\text{SO}_3\text{Na}$  is droplet size dependent. However, even for particles as small as  $0.1 \mu\text{m}$  the  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  ratio necessary to cover the particle surface with  $\text{CH}_3\text{SO}_3^-$  is  $\sim 0.05$ , well within the range reported for ambient particles.

At lower RH, when mixed  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles begin to dehydrate, because of their different water solubility,  $\text{NaCl}$  crystallizes first and then  $\text{CH}_3\text{SO}_3\text{Na}$  crystallizes. The solubility of  $\text{CH}_3\text{SO}_3\text{Na}$  and  $\text{NaCl}$  salts in  $100 \text{ cm}^3$  of water at  $T = 25^\circ\text{C}$  are at least  $90 \text{ g}$  (determined in the course of this work) and  $40 \text{ g}$ ,<sup>66</sup> respectively. Hence, dry  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles have a multilayered structure with the methanesulfonate salt concentrated on the top layer. This structure may change the hydration response and reactivity of the particles compared to those of pure  $\text{NaCl}$ . For effloresced, mixed  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$

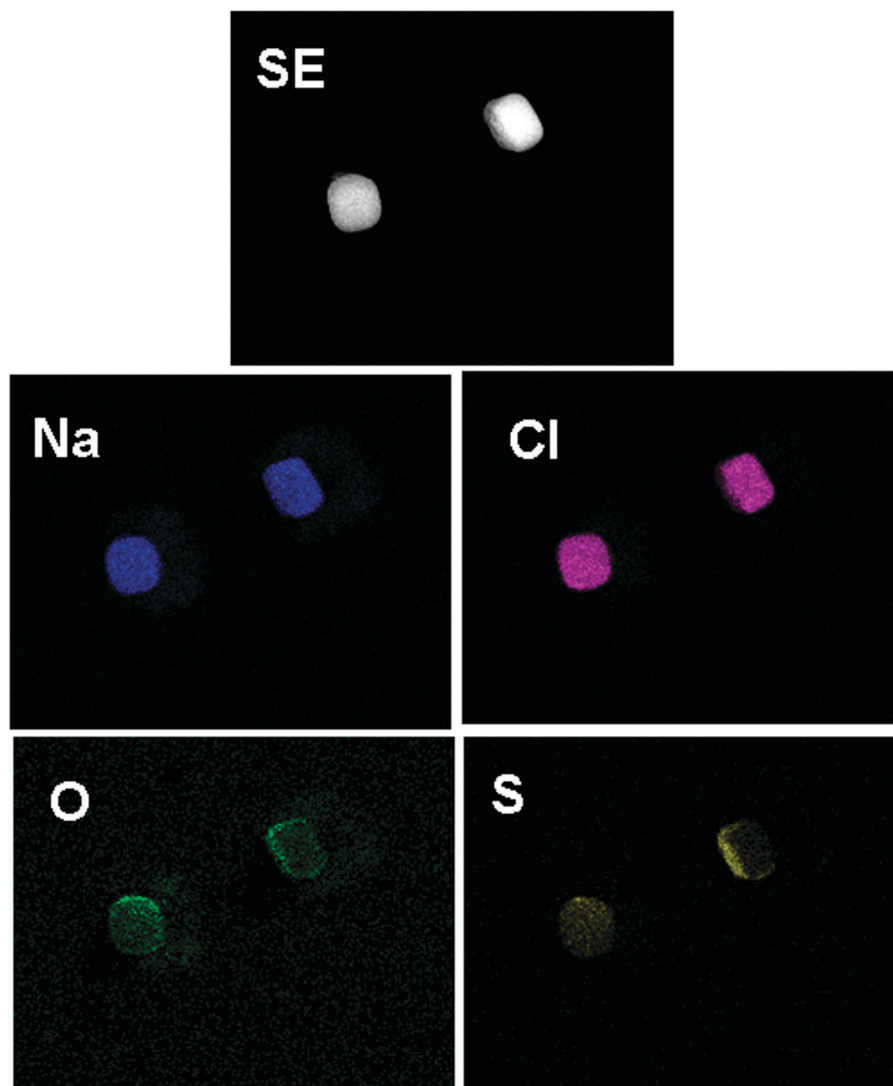
particles with  $0.01$ – $0.1$  mixing ratios and diameters of  $\sim 0.85 \mu\text{m}$ , the surface density of  $\text{CH}_3\text{SO}_3^-$  should exceed  $3 \times 10^{14} \text{ cm}^{-2}$ . Hence, the impact of  $\text{CH}_3\text{SO}_3\text{Na}$  on  $\text{HNO}_3$  reactive uptake in mixed  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles at lower RH should be more significant, as we show in a subsequent section.

SEM/EDX mapping and TOF-SIMS depth profiling were used to interrogate the internal composition of dry  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles. Fig. 4 displays an SEM image and EDX elemental maps of two dry particles with mixing ratios of  $0.05$ . As expected, no discernible spatial variations in  $\text{Na}$  and  $\text{Cl}$  were observed over the particles, but the intensities of  $\text{S}$  and  $\text{O}$  are clearly higher in the particle shell areas, which is indicative of  $\text{CH}_3\text{SO}_3^-$  enrichment on the particle surface.

To further confirm the multilayer structure of dry  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles, TOF-SIMS depth profiling was performed on particles (mixing ratio =  $0.1$ ) collected on a silicon wafer. The top panel of Fig. 5 shows spatial distributions of the  $\text{Cl}^-$  and  $\text{Na}^+$  ions recorded over two separate portions of the sample during negative and positive experimental modes, respectively. The maps indicate the location of particles probed in two experiments. Intensities of  $\text{Cl}^-$ ,  $\text{O}^-$ ,  $\text{OH}^-$ ,  $\text{SO}_3^-$ , and  $\text{Na}^+$  TOF-SIMS signals as a function of time (which corresponds to depth from the particle surface) are shown in the bottom panel of Fig. 5. As anticipated, the  $\text{SO}_3^-$ ,  $\text{O}^-$ , and  $\text{OH}^-$  ion signals decrease rapidly at the beginning of the depth profiling, whereas the  $\text{Na}^+$  and  $\text{Cl}^-$  ion signals both exhibit characteristic but somewhat different rise-and-fall behaviors. The  $\text{Na}^+$  ion signal reaches a maximum intensity within the first  $5 \text{ s}$ , probably due to surface contamination. The  $\text{Cl}^-$  ion signal peaks near  $80 \text{ s}$  due to the  $\text{CH}_3\text{SO}_3\text{Na}$  surface coating, which is consistent with temporal profiles of  $\text{SO}_3^-$ ,  $\text{O}^-$  and  $\text{OH}^-$  ions. The signal then levels off for about  $500 \text{ s}$ , and gradually drops afterwards. Based on a half-life of  $\sim 1800 \text{ s}$  observed in these experiments for the decay of the  $\text{Cl}^-$  and  $\text{Na}^+$  ion signals and the known  $\sim 1 \mu\text{m}$  size of particles, we estimate a depth profiling rate of  $0.28 \text{ nm s}^{-1}$  for these experimental conditions. Therefore, the  $\text{CH}_3\text{SO}_3\text{Na}$  surface layer is calculated to be  $\sim 25 \text{ nm}$  thick. All of the ion-count profiles are consistent with the SEM findings, indicating a core-shell, multilayer structure in  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles: a  $\text{NaCl}$  core and a  $\text{CH}_3\text{SO}_3\text{Na}$  shell.

### Hygrosopic behavior of mixed $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$ particles

During hydration and dehydration, particles change their size, phase and water-to-solute ratios—physicochemical properties critical to the understanding of the heterogeneous reactive uptake. Fig. 6a shows the FTIR spectra recorded for mixed  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles with the mixing ratio of  $0.1$  during the hydration cycle at increased RH. The absorption band due to  $\nu_8(\text{SO}_3^-)$  asymmetric stretch is clearly observed at  $1201 \text{ cm}^{-1}$  over the entire range of RH. In the high RH spectra, the appearance of the  $\nu(\text{H}_2\text{O})$  stretching and the  $\delta(\text{H}_2\text{O})$  bending bands at  $\sim 3400$  and  $\sim 1640 \text{ cm}^{-1}$ , respectively, indicate the presence of condensed-phase water. The integrated absorbance of the  $\nu(\text{H}_2\text{O})$  band (from  $3660$  to  $2750 \text{ cm}^{-1}$ ) was used to quantify the amount of water present in the particles.<sup>51,52</sup> Condensed-phase water is not detected until  $\sim 69\% \text{ RH}$ , at which point the  $\nu(\text{H}_2\text{O})$  and  $\delta(\text{H}_2\text{O})$



**Fig. 4** Secondary electron image and X-ray elemental maps (Na, Cl, O and S) of  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles with the mixing ratio of 0.05.

absorption bands begin to appear. At this RH, the  $\text{CH}_3\text{SO}_3\text{Na}$  shell becomes aqueous as indicated by a rapid increase in the absorbance of the water bands. Further increase in the RH to 75% shows a considerably greater amount of water taken up due to the dissolution of the NaCl core. At higher RH, completely aqueous droplets are formed and which continue to grow hygroscopically.

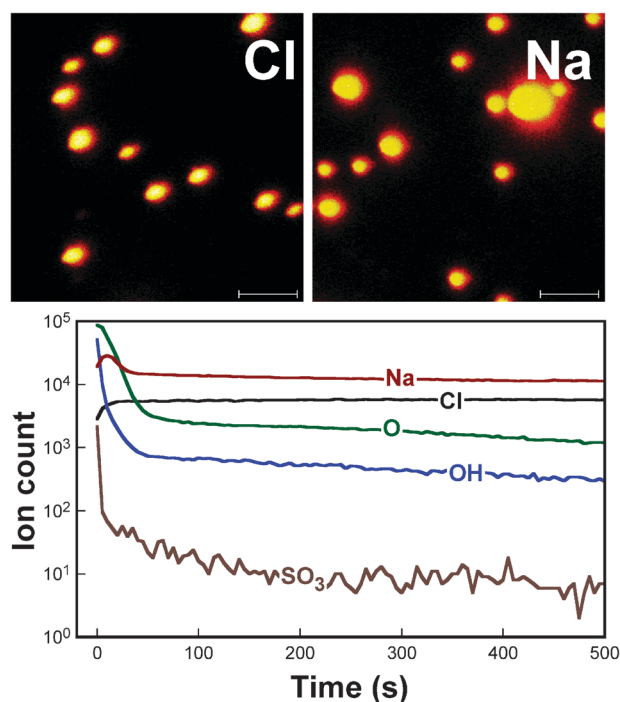
Fig. 6b combines the results of a hydration/dehydration experiment on  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles. The change of water content is expressed as the  $\nu(\text{H}_2\text{O})$  band intensity at a specific RH (integrated from 3660 to 2750  $\text{cm}^{-1}$ ), normalized to that at 80% RH. The normalized values are plotted as a function of RH. For comparison, experimental data<sup>52,65</sup> for pure NaCl particles are also included. The phase transitions observed and the extent of the water uptake and dehydration agree well with the hygroscopic properties of pure  $\text{CH}_3\text{SO}_3\text{Na}$  and NaCl particles, for which reported deliquescence RH values are 71%<sup>51</sup> and 75%,<sup>65</sup> respectively. Above 69% RH, the water content of the  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles initially increases due to the deliquescence of the  $\text{CH}_3\text{SO}_3\text{Na}$  component. The subsequent deliquescence of NaCl results in a second,

abrupt change in the water uptake at 75% RH. Upon evaporation, the particles slowly shed their water content until the RH reaches  $\sim 47\%$  efflorescence relative humidity (ERH), where crystallization occurs. In contrast to the hydration behavior, no distinct two-step efflorescence event was observed in the dehydration experiment. This could arise from the close ERH values of pure  $\text{CH}_3\text{SO}_3\text{Na}$  and NaCl particles and lower accuracy of the efflorescence detection in experiments with substrate deposited particles.<sup>52</sup>

#### Heterogeneous uptake kinetics of $\text{HNO}_3$ on mixed $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$ particles

Fig. 7 shows typical SEM images of  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles before and after exposure to gas-phase  $\text{HNO}_3$ . Morphological changes indicative of reactive transformation are clearly seen. EDX spectra reveal a depletion of chlorine after the reaction. The experimental net uptake coefficient ( $\gamma_{\text{net}}$ ) is calculated<sup>49</sup> from

$$\gamma_{\text{net}} = \frac{4k_I[\text{Cl}^-]_{d,0}}{\bar{c}_{\text{HNO}_3}[\text{HNO}_3]_{\infty}} \frac{V_d}{S_d} = \frac{2[\text{Cl}^-]_{d,0}\bar{D}_d}{3\bar{c}_{\text{HNO}_3}} \frac{k_I}{[\text{HNO}_3]_{\infty}} \quad (4)$$

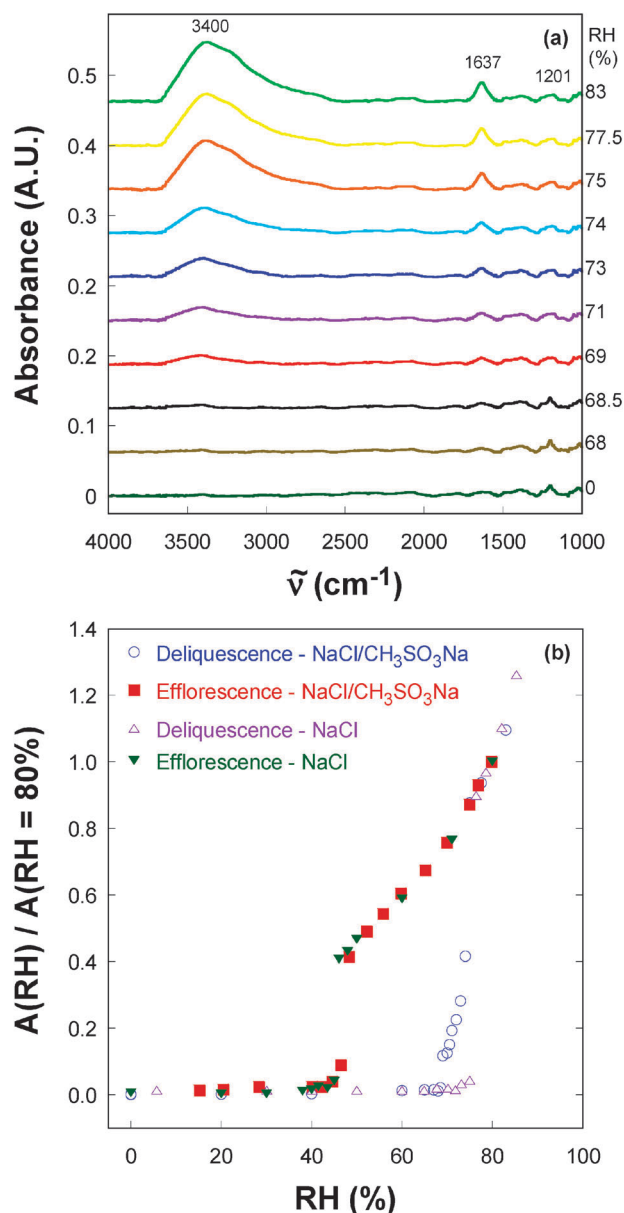


**Fig. 5** TOF-SIMS analysis of  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles with the mixing ratio of 0.1. Top panel: maps of  $\text{Cl}^-$  and  $\text{Na}^+$  ions recorded over two separate areas of the sample. Size bar is  $3\ \mu\text{m}$ . Bottom panel: intensities of  $\text{Cl}^-$ ,  $\text{O}^-$ ,  $\text{OH}^-$ ,  $\text{SO}_3^-$ , and  $\text{Na}^+$  ions as a function of time recorded in two depth profiling experiments (positive and negative modes).

where  $V_d/S_d$  is the droplet volume-to-surface area ratio,  $\bar{c}_{\text{HNO}_3} = 3.18 \times 10^4\ \text{cm s}^{-1}$  is the mean molecular speed of  $\text{HNO}_3$ ,  $\bar{D}_d$  is the deliquesced droplet or dry particle diameter, depending on the RH, and  $k_I$  is the pseudo-first-order rate constant in the limit of small particle loading ( $N_s \rightarrow 0$ ) determined from EDX measurements and using eqn (2).<sup>49,56</sup> Eqn (4) would be exact if the heterogeneous reaction occurred around the entire sphere of the droplet. However, the substrate-based experiment limits the gaseous reactant flux to a hemisphere rather than the entire droplet. To account for this, the uptake coefficient reported here is twice of that directly measured, *i.e.*,

$$\gamma_{\text{net}} = \frac{4[\text{Cl}^-]_{d,0}\bar{D}_d}{3\bar{c}_{\text{HNO}_3}} \frac{k_I}{[\text{HNO}_3]_{\infty}}, \quad (5)$$

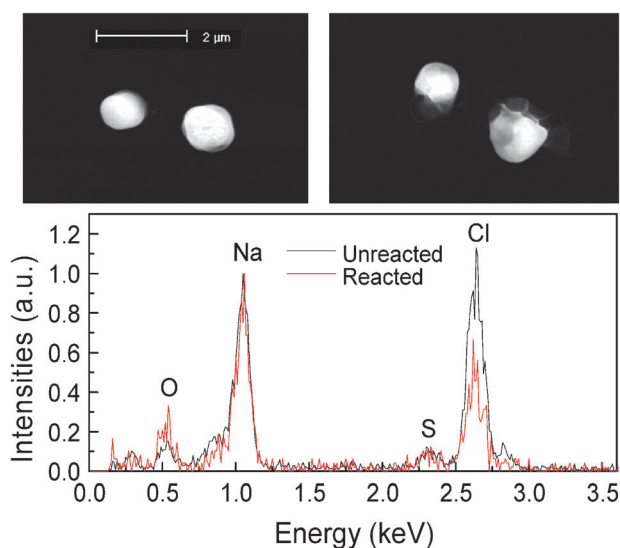
According to eqn (5), the particle size and initial concentration of chloride are required for uptake coefficient calculations. For experiments at  $\text{RH} = 40\%$  (below the efflorescence point), the dry particle diameter ( $0.85\ \mu\text{m}$ ) was used. For experiments at 60 and 80% RH, the particle (droplet) diameters were estimated as  $1.4\ \mu\text{m}$  and  $1.6\ \mu\text{m}$ , respectively, using the hygroscopic growth data of NaCl particles.<sup>65</sup> Literature<sup>24</sup> values for the RH-dependent chloride concentration in NaCl particles were used to estimate initial chloride concentrations in the mixed  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles. Namely, the following values of  $[\text{Cl}^-]_{d,0}$  were estimated: 37, 30, 11 and 6 M at 20, 40, 60 and 80% RH, respectively.



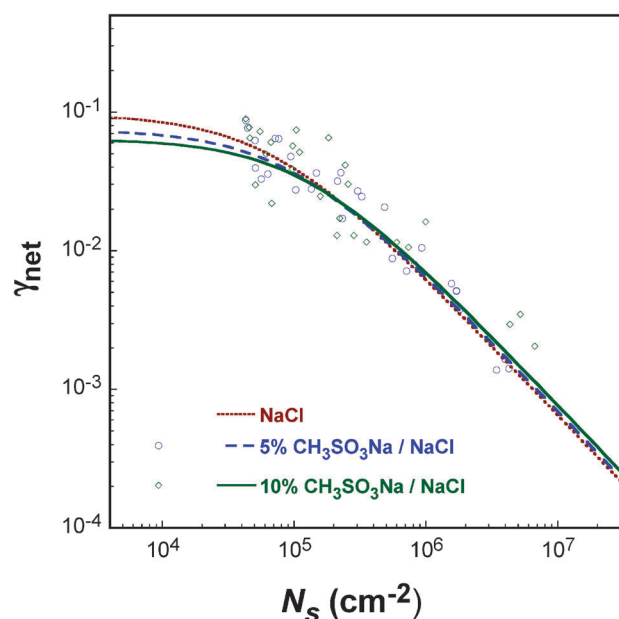
**Fig. 6** (a) FTIR spectra of  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles (mixing ratio = 0.1) exposed to increasing% RH. (b) Representation of hygroscopic growth by ratios of integrated area of OH stretching mode relative to that at  $\text{RH} = 80\%$ , measured for the same  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles in hydration and dehydration experiments. Data of NaCl is included for comparison (Liu *et al.*, 2007).

A typical plot of  $\gamma_{\text{net}}$  values *versus*  $N_s$  is shown in Fig. 8. For comparison, the reactive uptake coefficients of  $\text{HNO}_3$  on NaCl determined in a previous study<sup>49</sup> are also included in the figure. Trend lines in the plot represent nonlinear fits to data using the equation:<sup>56</sup>  $\gamma_{\text{net}}(N_s) = (1/\gamma_{\text{net}}(N_s \rightarrow 0) + cN_s)^{-1}$ . Corresponding values of  $\gamma_{\text{net}}$  in the limit of small particle loading ( $N_s \rightarrow 0$ ) are summarized in Table 4. The uncertainty factors of the measured  $\gamma_{\text{net}}$  values were determined in the same manner as in the previous work.<sup>49,50</sup> For deliquesced particles at 80% RH, the reactive uptake of  $\text{HNO}_3$  does not exhibit measurable differences with varying  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$





**Fig. 7** Top panels: SEM images of  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles before (left) and after (right) reaction with 11.6 ppb of gaseous  $\text{HNO}_3$  at 80% RH for 15 min. Bottom panel: representative EDX spectra of an individual  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particle before and after reaction.



**Fig. 8**  $\gamma_{\text{net}}$  values for  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles with mixing ratios of 0.05 and 0.1 measured at RH = 80% as a function of particle number density  $N_s$  on the substrate surface. Symbols: experimental data, lines: fit to data. The curve fitted  $\gamma_{\text{net}}$  values for pure NaCl particles from Liu *et al.*, 2007<sup>49</sup> are shown for comparison.

mixing ratios. The uptake coefficients  $\gamma_{\text{net}}$  are slightly lower than that measured for pure NaCl particles using the identical experimental procedure.<sup>49</sup> However, these differences are within the experimental uncertainty and therefore do not confirm that  $\text{CH}_3\text{SO}_3\text{Na}$  is inhibiting the reaction. Rather, the results indicate that the  $\text{CH}_3\text{SO}_3^-$  accumulation on droplet surfaces does not alter substantially the heterogeneous reactivity of NaCl with gas-phase  $\text{HNO}_3$ . For typical sizes of sea salt

particles (a few micrometres), gas-phase diffusion of  $\text{HNO}_3$  is the rate limiting step in the reactive uptake of  $\text{HNO}_3$  onto NaCl. The  $\text{CH}_3\text{SO}_3^-$  surfactant layer does not appear to affect the interfacial transport of  $\text{HNO}_3$  strongly enough to become the rate determining step, *i.e.*, transport across the gas-particle interface is still faster than the gas-phase diffusion.

Additional series of experiments were carried out at 20 and 40% RH, below the efflorescence point of mixed  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles. The mixing ratios were varied (0.02, 0.05 and 0.1) to investigate how the amount of surface covered with  $\text{CH}_3\text{SO}_3\text{Na}$  affects  $\text{HNO}_3$  uptake. The measured reactive uptake coefficients  $\gamma_{\text{net}}$  ( $N_s \rightarrow 0$ ) are listed in Table 4. Unlike the data obtained at 80% RH, significant and consistent reduction of  $\gamma_{\text{net}}$  values was observed below the efflorescence RH. Under these conditions, the reactive uptake is limited by the chemical kinetics of  $\text{HNO}_3$  reacting on the surface of NaCl crystals,<sup>2</sup> and not by the gas-phase diffusion. Heterogeneous reaction of  $\text{HNO}_3$  with solid NaCl occurs at surface reactive sites—surface defects, steps and edges, and is limited by the availability of these sites. The inhibiting effect observed for mixed  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles is associated with covering the reactive sites on the NaCl core by the non-reactive  $\text{CH}_3\text{SO}_3\text{Na}$  shell. The suppression of the reactive uptake for RH below efflorescence is consistently observed over the entire range of  $\text{CH}_3\text{SO}_3\text{Na}$  surface coverage. If we assume a spherical core-shell structure for the 0.85  $\mu\text{m}$  particle and the cross section of the  $\text{CH}_3\text{SO}_3\text{Na}$  molecule of 18  $\text{\AA}^2$ , approximately 7 layers of  $\text{CH}_3\text{SO}_3\text{Na}$  cover the NaCl surface at a mixing ratio of 0.01. Therefore, it is not surprising that even at the lowest coverage, the  $\gamma_{\text{net}}$  value decreases by a factor of two. Additionally, the uptake coefficient decreases for particles with larger  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  mixing ratios which would have higher surface coverage of  $\text{CH}_3\text{SO}_3\text{Na}$ . For the  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  mixing ratio of 0.1, the reactive uptake is five times smaller than that of pure NaCl. However, some reaction still occurs, indicating that surface coverage of NaCl by  $\text{CH}_3\text{SO}_3\text{Na}$  is imperfect. This conclusion is also supported by the SEM/EDX mapping image shown in Fig. 4.

It is known that reactive uptake on dry NaCl particles is highly dependent on the amount of surface absorbed water<sup>2</sup> even though the particles are in a solid, crystalline phase. Measured uptake coefficients for  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles with a mixing ratio of 0.1 (see Table 4) indicate persistent inhibition of reactive uptake on the mixed particles over the entire range of RH, as compared to pure NaCl particles. The inhibiting effect is around a factor of two for 60% RH, and the effect is more pronounced for 40% and 20% RH, where the uptake rate drops by a factor of 5. Again, this trend is consistent with a core-shell structure of mixed  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles and with a  $\text{CH}_3\text{SO}_3\text{Na}$  shell that is inert towards reaction with  $\text{HNO}_3$ .

Although  $\text{CH}_3\text{SO}_3\text{Na}$  is expected to be unreactive towards  $\text{HNO}_3$  (based on thermochemistry considerations) the lack of reaction was confirmed experimentally. We exposed pure  $\text{CH}_3\text{SO}_3\text{Na}$  particles to very high concentration of  $\text{HNO}_3$  ( $\sim 80$  ppb) at 80% RH for over 10 h and analyzed the changes in the S/Na ratio. The CCSEM/EDX results showed no measurable differences before and after the exposure. If the uncertainty of the S/Na values was taken as an estimation of

**Table 4** Experimental uptake coefficients ( $\gamma_{\text{net}}$ ) for the heterogeneous reaction of  $\text{HNO}_3$  with mixed  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles measured at different RH conditions. Data for NaCl particles are taken from Liu *et al.*, 2007

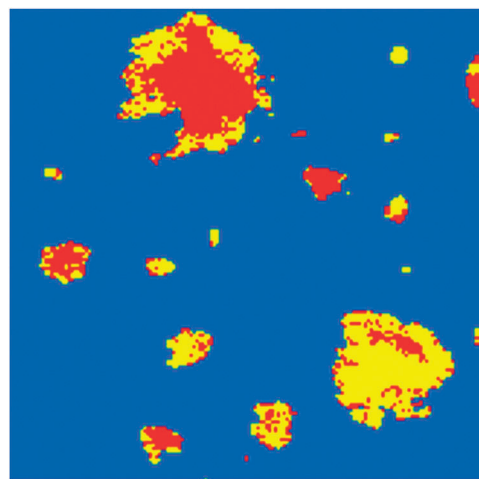
Composition	80% RH $D_d = 1.6 \mu\text{m}$	60% RH $D_d = 1.4 \mu\text{m}$	40% RH $D_d = 0.85 \mu\text{m}$	20% RH $D_d = 0.85 \mu\text{m}$
NaCl	0.11 ( $\times 2.9/\div 2.8$ )	0.20 ( $\times 2.9/\div 2.8$ )	0.10 ( $\times 2.9/\div 2.8$ )	0.02 ( $\times 2.9/\div 2.8$ )
$\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$ (2/100)	—	—	0.05 ( $\times 2.9/\div 2.8$ )	—
$\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$ (5/100)	0.09 ( $\times 2.5/\div 2.5$ )	—	0.035 ( $\times 2.9/\div 2.8$ )	—
$\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$ (10/100)	0.08 ( $\times 2.5/\div 2.5$ )	0.09 ( $\times 2.5/\div 2.5$ )	0.020 ( $\times 2.5/\div 2.5$ )	0.003 ( $\times 2.5/\div 2.5$ )
$\text{CH}_3\text{SO}_3\text{Na}$	$< 10^{-5}$	—	—	—

the possible reaction extent, an upper limit for  $\gamma_{\text{net}}$  of  $10^{-5}$  for the uptake of  $\text{HNO}_3$  onto  $\text{CH}_3\text{SO}_3\text{Na}$  particles is obtained.

## Conclusions

In this study, surface activity of  $\text{CH}_3\text{SO}_3^-$  ions in aqueous (deliquesced) particles, and shell-core structures of dry mixed  $\text{CH}_3\text{SO}_3\text{Na}/\text{NaCl}$  particles were investigated using a combination of experimental and modeling approaches for chemical imaging. The results suggest that surfaces of aqueous (deliquesced) sea salt particles contain substantial amount of  $\text{CH}_3\text{SO}_3^-$  ions, while in the dry (effloresced) particles, methanesulfonate salts may form a layer of coating that modifies particle hygroscopicity and atmospheric reactivity. Water and  $\text{HNO}_3$  reactive uptake measurements were carried out to assess the effects of particle internal composition on these properties. Consistent with the core-shell structures, the initial uptake of water by dry particles is governed by the hygroscopicity of the  $\text{CH}_3\text{SO}_3\text{Na}$  shell that deliquesces at 68–69% RH, followed by the NaCl deliquescence at 75–76% RH. However, addition of the  $\text{CH}_3\text{SO}_3^-$  ions shows no detectable impact on the efflorescence RH. We have shown that the  $\text{CH}_3\text{SO}_3\text{Na}$  shell in dry particles inhibits their reactivity with  $\text{HNO}_3$  and presumably also with nitrogen oxides. The inhibition is more substantial at lower RH, and higher  $\text{CH}_3\text{SO}_3\text{Na}$  concentrations.

Accumulation of  $\text{CH}_3\text{SO}_3\text{Na}$  salt on the surface of evaporating particles is a result of its higher solubility with respect to NaCl. However, in an atmospheric environment, dehydration behavior and internal composition of multi-component sea salt particles processed with  $\text{CH}_3\text{SO}_3\text{H}$  will be more complex because of highly soluble magnesium, potassium, and ammonium salts ( $\text{MgSO}_4 \cdot \text{H}_2\text{O}$ ,  $\text{KMgCl}_3 \cdot 6\text{H}_2\text{O}$ ,  $\text{NH}_4\text{HSO}_4$  *etc.*) that may also accumulate on the particle surface. Fig. 9 shows X-ray spectro-microscopy chemical maps of sulfur containing salts in individual marine particles collected in MASE 2005 field study.<sup>30</sup> Complex, non homogeneous distribution of  $\text{CH}_3\text{SO}_3^-$  and  $\text{SO}_4^{2-}$  salts in individual particles can be inferred from a range of  $\text{CH}_3\text{SO}_3^-/\text{SO}_4^{2-}$  ratios measured for different particles areas as indicated by red and yellow colors. Qualitatively, the presence of both  $\text{CH}_3\text{SO}_3^-$  and  $\text{SO}_4^{2-}$  salts at particle edges is suggested from these maps. Surface accumulation of sulfates will have similar inhibiting impact on the atmospheric reactivity of dry sea salt particles, while chlorides present on the surface may have somewhat replenishing effects. The influence of other highly soluble salts and quantitative speciation of surface chemical composition of real sea salt particles are interesting topics for additional investigations following the case study presented here.



**Fig. 9** STXM/NEXAFS chemical map ( $12 \mu\text{m} \times 12 \mu\text{m}$ ) of sulfur constituents in a sample of individual marine particles collected at the Point Reyes National Seashore, California, during MASE 2005 experiment. Two types of externally mixed particles have been reported in this sample: sea salt and sulfate particles. Red and yellow colors indicate portions of particles with  $\text{CH}_3\text{SO}_3^-/\text{SO}_4^{2-}$  ratios above and below 20/80, respectively. Specific details of the STXM/NEXAFS analysis of these particles can be found in Hopkins *et al.*, 2007.

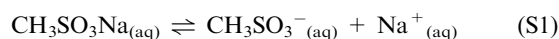
## Appendix

### Standard Gibbs free energy of selected aqueous salts (Table 5)

**Gibbs free energy of formation of methylsulfonate acid and salts.** The Gibbs free energy of formation for the  $\text{CH}_3\text{SO}_3^-$  anion is estimated from the  $\text{CH}_3\text{SO}_3\text{H}$  acid dissociation constant. The  $pK_a$  value for  $\text{CH}_3\text{SO}_3\text{H} \rightleftharpoons \text{CH}_3\text{SO}_3^- + \text{H}^+$  is  $-1.2$ .<sup>68</sup> Thus,  $\Delta G_f^\circ(\text{CH}_3\text{SO}_3^-)_{\text{ai}}$  can be determined using the following equation:

$$\Delta G_r^\circ = -RT \ln K_a = 2.303RT pK_a,$$

which yields the Gibbs free energy of reaction  $\Delta G_r^\circ = -15.78 \text{ kJ/mol}$ . The standard Gibbs free energy of formation of  $\text{CH}_3\text{SO}_3\text{H}_{(\text{aq})}$  is  $-527.3 \text{ kJ/mol}$ .<sup>69</sup> Hence,  $\Delta G_f^\circ(\text{CH}_3\text{SO}_3^-)_{\text{aq}}$  is  $-543.1 \text{ kJ/mol}$ . Unfortunately, the free energy  $\Delta G_{\text{r,S1}}^\circ$  for



is not available, but its value is expected to be negative and typically a few kcal/mol. We find

$$\begin{aligned} \Delta G_f^\circ(\text{CH}_3\text{SO}_3\text{Na})_{\text{ai}} &= \Delta G_f^\circ(\text{Na}^+)_{\text{ai}} + \Delta G_f^\circ(\text{CH}_3\text{SO}_3^-)_{\text{ai}} \\ &- \Delta G_{\text{r,S1}}^\circ > -805.0 \text{ kJ/mol}. \end{aligned} \quad (1)$$

**Table 5** Standard Gibbs free energy of formation of aqueous salts

Species	$\Delta G_f^\circ$ (kJ/mol <sup>-1</sup> )	References
NaCl(aq)	-393.1	Lide (2008) <sup>66</sup>
Na <sub>2</sub> SO <sub>4</sub> (aq)	-1268.4	Lide (2008) <sup>66</sup>
NaHSO <sub>4</sub> (aq)	-1017.8	Lide (2008) <sup>66</sup>
NaNO <sub>3</sub> (aq)	-373.2	Lide (2008) <sup>66</sup>
(NH <sub>4</sub> )SO <sub>4</sub> (aq)	-903.1	Lide (2008) <sup>66</sup>
CH <sub>3</sub> SO <sub>3</sub> Na(aq)	> -805.0	Estimated, this work
CH <sub>3</sub> SO <sub>3</sub> NH <sub>4</sub> (aq)	> -622.5	Estimated, this work
H <sub>2</sub> SO <sub>4</sub> (aq)	-744.5	Lide (2008) <sup>66</sup>
CH <sub>3</sub> SO <sub>3</sub> H(aq)	-527.3	Guthrie and Gallant (2000) <sup>67</sup>
HNO <sub>3</sub> (aq)	-111.3	Lide (2008) <sup>66</sup>
HCl(aq)	-131.2	Lide (2008) <sup>66</sup>
HCl(g)	-95.3	Lide (2008) <sup>66</sup>

where  $\Delta G_f^\circ(\text{Na}^+)_{\text{ai}}$  is -261.9 kJ mol<sup>-1</sup>,<sup>70</sup> Likewise, since  $\Delta G_f^\circ(\text{NH}_4^+)_{\text{ai}}$  is -79.4 kJ,<sup>70</sup> we find  $\Delta G_f^\circ(\text{CH}_3\text{SO}_3\text{NH}_4)_{\text{ai}}$  to be > -622.5 kJ/mol.

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