

Facile synthesis of core-shell Au@CeO₂ nanocomposites with remarkably enhanced catalytic activity for CO oxidation†Jian Qi,^a Jie Chen,^{ab} Guodong Li,^{*a} Shunxing Li,^b Yan Gao^a and Zhiyong Tang^{*a}

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Uniform Au@CeO₂ core-shell submicrospheres, in which a Au nanoparticle core is coated with a shell composed of CeO₂ nanoparticles, are easily synthesized by using hydrothermal and calcinating processes. When the Au@CeO₂ core-shell submicrospheres are used for catalytic oxidation of CO to CO₂, the full conversion temperature is decreased from over 300 °C to 155 °C with respect to the conventional supported Au–CeO₂ catalysts. Furthermore, the Au@CeO₂ core-shell submicrospheres show superior catalytic stability, and no deactivation occurs after 72 h reaction. The mechanisms of the growth and the high catalytic performance of Au@CeO₂ core-shell submicrospheres are discussed in detail.

Catalytic oxidation of CO to less toxic CO₂ is always one of the hottest topics in the field of catalysis due to its important industrial applications, such as car-exhaust emission control, chemical processing, CO₂ lasers, sensors, fuel cell technology, as well as being an ideal model reaction to study the mechanism of heterogeneous catalysis.¹ Recently, much research attention has been focused on development of novel and high-efficient catalysts for CO oxidation. Among different types of catalysts, the interest in studying the inorganic oxide supported Au catalysts has increased substantially since Haruta *et al.* discovered that small Au nanoparticles (NPs) are exceptionally active for low-temperature CO oxidation.² Unfortunately, the supported Au catalysts with small sizes are usually

unstable and tend to sinter and grow into larger particles under the conditions of catalytic reactions,³ leading to loss of the unique properties registered in the original NPs. Therefore, the catalytic activity of the supported Au catalysts decays rapidly, which seriously impedes their practical applications.

In order to solve the bottleneck problem of NP migration and aggregation, many strategies have been tried and generally can be classified into four categories: (1) replacement of monocomponent Au NPs with Au-based alloy NPs,⁴ (2) confinement of Au NPs into mesoporous supports,⁵ (3) modification of the supports,^{6,7} and (4) encapsulation of Au NPs into the supports with the core-shell structure.⁸ The former three methods may improve the catalytic performance to some extent, but cannot completely avoid migration and aggregation of Au NPs. As a comparison, the last one is a more effective way, because the core-shell micro-/nano-structures have high thermal stability⁹ and recyclability.¹⁰ Generally speaking, there are two typical types of shells, organic capping agents and inorganic materials. However, the organic capping molecules have low chemical and physical resistance in the catalytic reactions,^{11–14} so the inorganic oxide shells with high stability have been broadly selected as the catalysts for CO oxidation. Among the various inorganic oxides including SiO₂,^{15,16} TiO₂,^{17–20} ZrO₂,^{21,22} CeO₂,²³ SnO₂,^{24–26} and Fe₂O₃,²⁷ CeO₂ is of special interest due to its abundant oxygen vacancy defects, high oxygen storage capacity and the relatively easy shuttles between the III and IV oxidation states, giving rise to the enhanced rates of the oxidation reaction.

It should be noted that until now only a few works have been reported on successful construction of noble metal NPs@CeO₂ core-shell composites.^{23,28–30} One of the big challenges is that classical sol-gel methods^{31,32} to prepare the micro-/nano-structured transition metal oxides are not suitable for CeO₂ owing to the low hydrolysis ability of Ce cations in water or alcohol solution.³³ Herein, we

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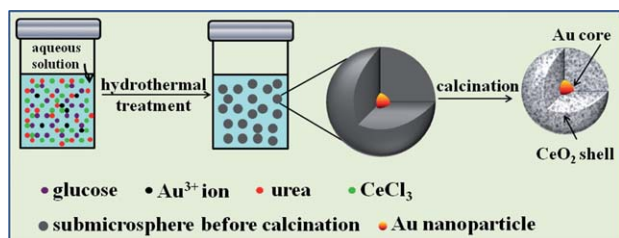
Broader context

The well-defined Au@CeO₂ core-shell submicrospheres, in which a Au nanoparticle core is coated with a shell composed of CeO₂ nanoparticles, are easily synthesized by combination of hydrothermal and calcination processes. When the Au@CeO₂ core-shell submicrospheres are used for catalytic oxidation of CO to CO₂, the full conversion temperature is decreased from over 300 °C to 155 °C with respect to the conventional supported Au–CeO₂ catalysts. Furthermore, the Au@CeO₂ core-shell submicrospheres show superior catalytic stability, and no deactivation occurs after 72 h reaction. The new strategy is expected to be broadly employed to synthesize other nanomaterials with well-defined structures, which have potential applications in energy and environmental fields.

introduce a novel and simple “self-templating” technique to fabricate the Au@CeO₂ core-shell submicrospheres. HAuCl₄ and CeCl₃ as the precursors, respectively, were mixed in the aqueous solution containing glucose and urea, subsequently the solution was placed under hydrothermal conditions to generate a dark-brown suspension, and finally the suspension was subjected to calcination to obtain the desirable products. As shown in Scheme 1, formation of the Au@CeO₂ core-shell submicrospheres involves several steps: firstly, reduction of Au³⁺ ions by glucose in the solution produces Au NPs. Then, condensation of glucose in solution under hydrothermal conditions leads to formation of amorphous carbon submicrospheres, in which the Au NP is located at the center and Ce³⁺ ions are adsorbed in the matrix shell. Finally, the spontaneously formed carbon submicrospheres are used as the sacrificial templates to generate Au@CeO₂ submicrospheres through calcination in air. Impressively, when these Au@CeO₂ submicrospheres are used as the catalysts for CO oxidation, they exhibit the considerably enhanced catalytic activity and stability with respect to the conventional supported Au–CeO₂ catalysts.^{34,35}

The morphology and structure of Au@CeO₂ submicrospheres are first investigated by different characterization techniques including scanning electron microscopy (SEM), transmission electron microscopy (TEM), high-resolution transmission electron microscopy (HRTEM), high angle annular dark field scanning transmission electron microscopy (HAADF-STEM), and powder X-ray diffraction (XRD). Several important features can be recognized: (1) the prepared submicrospheres have rather uniform diameters of 178 ± 15 nm (Fig. 1a and b). (2) The magnified TEM image demonstrates that the submicrospheres have a typical core-shell structure (inset in Fig. 1b), in which a Au NP core with the diameter of about 17 nm is surrounded with a CeO₂ shell, as shown in the elemental mapping from the HAADF-STEM image (Fig. 1c). (3) The CeO₂ shell is composed of NPs with about 8–10 nm diameter (Fig. 1d), and the HRTEM image further indicates that each NP in the shell is highly crystalline with the interplanar spacings of 0.31 nm and 0.19 nm corresponding to the (111) and (220) planes of CeO₂, respectively (Fig. 1e). It is noted that the lattice spacing of Au NP cannot be observed clearly due to the thicker CeO₂ shell. (4) Finally, the crystal structure of the Au@CeO₂ submicrospheres is discerned by the powder XRD pattern (Fig. 1f). Two series of peaks, which are attributed to face-centered-cubic Au²² (blue rhombus) and fluorite-type CeO₂²³ (black triangles), respectively, are found for the core-shell submicrospheres.

How does the mixture of reactants evolve into the submicrospheres under the hydrothermal treatment? In order to answer this question, the intermediate products during the hydrothermal process are taken



Scheme 1 Schematic illustration for controlled construction of Au@CeO₂ submicrospheres with the core-shell structure *via* the hydrothermal method.

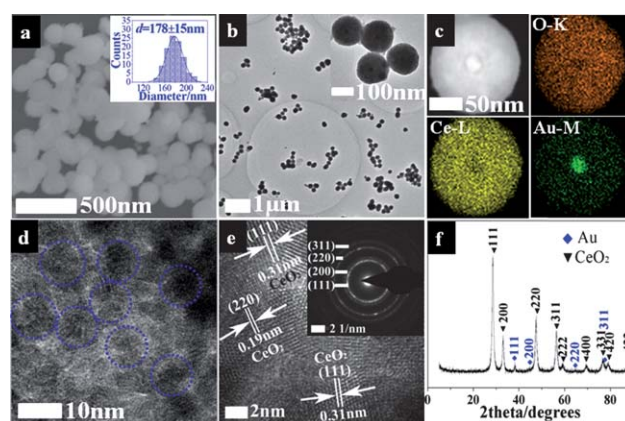


Fig. 1 (a) SEM image of Au@CeO₂ submicrospheres. The inset is the corresponding size histogram. (b) TEM image of Au@CeO₂ submicrospheres. The inset is the magnified TEM image. (c) HAADF-STEM mapping image of one submicrosphere. (d) TEM image of the CeO₂ shell of the submicrospheres. (e) HRTEM image of the submicrospheres. The inset is the selected area electron diffraction (SAED) image, indicating the polycrystalline nature of the CeO₂ shell. (f) XRD pattern of the submicrospheres.

out for characterization. Since such intermediate products are not subjected to calcination treatment, we denote them as pre-Au@CeO₂ submicrospheres. After the hydrothermal reaction only for 10 min, the pre-Au@CeO₂ core-shell submicrosphere is already formed (Fig. 2aI). With the reaction proceeding, the overall diameters of the pre-Au@CeO₂ submicrospheres gradually increase from ~60 nm to ~230 nm, while the sizes of Au NP cores remain ~17 nm (Fig. 2aI–2aIV). We also notice that the low-contrast thin shells appear and grow with a size increase of the pre-Au@CeO₂ submicrospheres

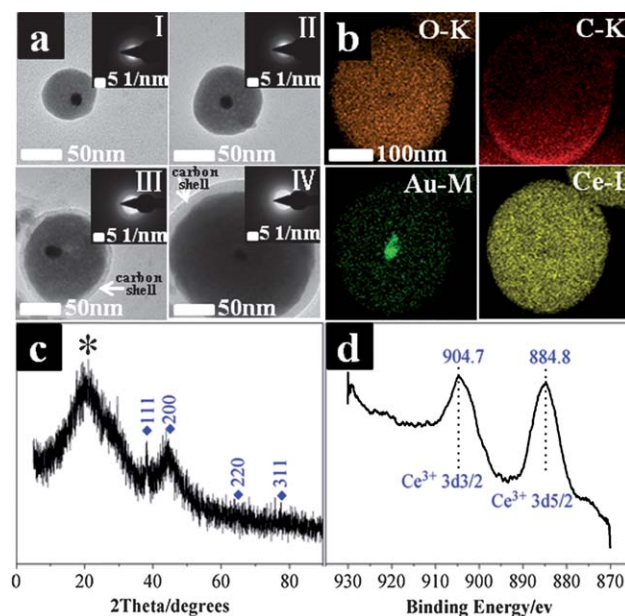


Fig. 2 (a) TEM images and corresponding SAED patterns (inset) of pre-Au@CeO₂ submicrospheres at 160 °C for different reaction times: (I) 10 min, (II) 1 h, (III) 6 h, and (IV) 20 h. (b) HAADF-STEM mapping image of the submicrosphere obtained after 20 h reaction. (c) and (d) represent the corresponding XRD and XPS patterns of (b).

(arrowed parts in Fig. 2aIII). Elemental mapping by HAADF-STEM reveals that Ce and O are homogeneously distributed inside the pre-Au@CeO₂ submicrospheres, whereas the thin shell is enriched with the element C (Fig. 2b and S1†). This result indicates that adsorption of Ce ions is simultaneous with the growth of the carbon matrix, but the adsorption speed of Ce ions is relatively slower, so a pure carbon thin shell is produced. Moreover, the diffusive rings in SAED images demonstrate that the carbon matrices of all the intermediate products are amorphous (insets in Fig. 2a). The amorphous nature of carbon matrices is proved by XRD measurement of pre-Au@CeO₂ core-shell submicrospheres, in which a broad peak corresponding to amorphous carbon is distinguished (starred peak in Fig. 2c). The XRD result also tells us that the Au NP cores in the pre-Au@CeO₂ submicrospheres are already crystalline (blue rhombus peaks in Fig. 2c), but Ce is of amorphous nature and no characteristic peaks are discerned. X-ray photoelectron spectrum (XPS) analysis further shows two peaks located around 884.8 eV and 904.7 eV for pre-Au@CeO₂ submicrospheres, which coincide with the Ce³⁺ valence state³⁶ (Fig. 2d). This result is also consistent with the above analysis that Ce³⁺ ions are adsorbed into the carbon matrix of pre-Au@CeO₂ submicrospheres during the hydrothermal process.

Next, we investigate the role of the precursors including glucose, CeCl₃ and urea on formation of pre-Au@CeO₂ core-shell submicrospheres. Firstly, in the absence of glucose, the products of the dendritic morphology are obtained in the mixed solution of CeCl₃ and urea (Fig. S2†). Furthermore, there is no Au element to be detected. This result indicates that glucose acts as not only the source for formation of carbon submicrospheres but also the reduction agent for Au³⁺ ions. Secondly, similar submicrospheres can be produced in the mixture of glucose and CeCl₃, even without urea (Fig. S3†). However, the products after calcination are multi-shelled CeO₂ submicrospheres rather than Au@CeO₂ core-shell submicrospheres (Fig. S4†). One plausible explanation is that decomposition of urea under the hydrothermal condition would release OH[−] ions, which provide an alkaline environment. In the solution containing urea, the functional groups of carbon submicrospheres such as carboxylic acid are deprotonated and can adsorb more Ce³⁺ ions based on the electrostatic attractions. So the content of Ce³⁺ ions in the submicrospheres decreases in the absence of urea. The calcination of carbon submicrospheres containing less of Ce³⁺ easily gives rise to generation of multi-shelled hollow structures, which is recently explored by us.³⁷ Also, due to the low mechanical strength of multi-shelled hollow structures, the submicrospheres are easily broken and difficult to encapsulate Au NPs (Fig. S4†). Evidently, these products are not suitable for studying the catalytic properties of nanocomposites.

Lastly, the hydrothermal products of the mixture of HAuCl₄ and glucose without CeCl₃ are examined. The core-shell submicrospheres with the sizes of around 600 nm, in which a crystalline Au NP core of about 60 nm diameter is coated with an amorphous carbon shell, are found (Fig. 3a–c). Compared with the product in the presence of Ce³⁺ ions (Fig. 2a), the relatively large size of the submicrospheres is understood, considering that adsorption with Ce³⁺ ions may slow down the growth speed of the carbon matrix. The Fourier transform infrared (FTIR) spectrum is used to identify the functional groups present in the submicrospheres (Fig. S5†). One of the most important features is appearance of the absorption bands at 1700 and 1620 cm^{−1}. These bands are attributed to C=O and C=C vibrations, which reveal that formation of carbon submicrospheres mainly

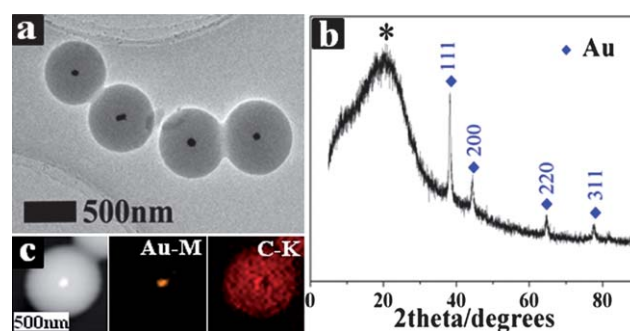


Fig. 3 (a) TEM image of core-shell submicrospheres prepared in the absence of Ce³⁺ ions. (b) and (c) represent corresponding XRD pattern and HAADF-STEM mapping images of (a). In (b), the broad peak at ~20° (star) points to the amorphous carbon,⁴⁰ while the sharp peaks (blue rhombus) stand for the crystalline Au.

originates from aromatization of glucose during the hydrothermal process.³⁸ It is also noted that in addition to the bands in the range of 1000–1300 cm^{−1} corresponding to the C–OH stretching and OH bending vibrations of residual glucose, there is a characteristic COO[−] absorption band at 1370 cm^{−1},³⁹ suggesting partial oxidation of the OH or CHO functional group of glucose by Au³⁺ ions.

Altogether with the above experimental facts, we can conclude the formation mechanism of Au@CeO₂ core-shell submicrospheres (Fig. S6† and 1). The Au³⁺ ions in the solution are firstly reduced to Au⁰ by glucose under the hydrothermal condition. At the same time, the dehydration–condensation reaction happens among the glucose molecules, resulting in formation and growth of the aromatic compounds and oligosaccharides around Au NPs (Fig. S6†). Urea in the solution is continuously decomposed to release OH[−] ions, which promote adsorption of Ce³⁺ ions with the functional groups of submicrospheres from carbonization of glucose. Therefore, pre-Au@CeO₂ submicrospheres are synthesized. In the subsequent calcination process, carbon in the submicrospheres is burned out, and thus the size of submicrospheres shrinks from ~230 nm to ~178 nm. Simultaneously, Ce³⁺ ions in the submicrospheres are oxidized to CeO₂ (it can be confirmed by characteristic XPS peaks at 882.7 eV and 901.1 eV, corresponding to Ce⁴⁺ valence state,³⁶ Fig. S7†), leading to formation of Au@CeO₂ submicrospheres (Fig. 1). It should be pointed out that the sizes of Au NP cores are maintained around 17 nm during the calcination process, though the overall sizes of the submicrospheres are considerably decreased. This result demonstrates the excellent physical confinement of CeO₂ shells, which effectively prevent possible sintering, migration and growth of Au NP cores.

To evaluate the performance of Au@CeO₂ core-shell submicrospheres for catalytic oxidation of CO, a contrast sample is prepared by simply mixing Au NPs with the similar diameters of 14 nm and the CeO₂ submicrospheres (referred to as Au–CeO₂, see the detailed synthesis in the ESI†). Synthesis of CeO₂ submicrospheres follows the recipe of Au@CeO₂ core-shell submicrospheres except that no Au³⁺ precursors are added. In order to make such performance evaluation more comparable, all the physicochemical properties of Au–CeO₂ including the content of Au NPs, the particle size of CeO₂, specific surface area, pore volume and average pore diameter are tuned to be close to those of Au@CeO₂ (Fig. S8 and Table S1†). For example, the content of Au NPs in Au–CeO₂ and Au@CeO₂ are 1.00 wt% and 0.93 wt%, respectively (Table S1†). Both Au–CeO₂ and Au@CeO₂

composites present the typical type IV N_2 sorption isotherms with a H3 hysteresis loop⁴¹ (Fig. S8†), which is usually considered to be indicative of gas adsorption in the mesopores.^{42,43} The corresponding specific surface areas are 80.6 and 82.5 $m^2 g^{-1}$, pore volumes are 0.082 and 0.091 $m^3 g^{-1}$, and average pore sizes are 2.1 and 2.2 nm with a narrow distribution for Au–CeO₂ and Au@CeO₂ composites, respectively. The presence of such mesoporous structures in both Au–CeO₂ and Au@CeO₂ submicrospheres mainly originates from the voids between CeO₂ NP aggregates (Fig. 1d), which ensure efficient mass transfer of gas molecules during the catalytic process. The evaluation of catalytic activity was performed in a fixed-bed reactor coupled online with a gas chromatograph (GC) (see the catalytic activity measurement for CO oxidation in the Experimental section of the ESI†). Fig. 4 shows the typical conversion ratio of CO as a function of reaction temperature over three catalysts under the conditions that the feed gas containing 1.0 vol% CO, 1.6 vol% O₂ and balance He was allowed to pass through the reactor at a total flow rate of 50 mL min^{−1}, corresponding to a gas hourly space velocity (GHSV) of 15 000 mL h^{−1} g_{cat}^{−1}. It can be seen that the Au@CeO₂ sample is already active at room temperature and the CO conversion ratio is about 20%, whereas at this temperature, the Au–CeO₂ shows a lower conversion of 10% and pure CeO₂ submicrosphere has no activity. With increasing the reaction temperature, the complete CO conversion temperature for the Au@CeO₂ sample is about 155 °C, which is quite remarkable.⁹ As a comparison, the CO conversion ratios over Au–CeO₂ at 300 °C and pure CeO₂ at 310 °C are 87% and 76%, respectively. Evidently, the presence of Au NPs regardless of whether they are inside or outside the CeO₂ support could efficiently enhance the catalytic activity of CeO₂, demonstrating the synergetic effect of Au and CeO₂ during the catalytic process. We also would like to stress that the activity of Au–CeO₂ in this work is lower than those reported in the literature,^{44–47} and this may be attributed to the below reasons: (1) Au–CeO₂ used here is not subjected to a calcination step because calcination of Au–CeO₂ would lead to a significant increase in Au particle sizes. Thus, the presence of citrate capping agent may partially suppress the activity of Au–CeO₂. (2) The sizes of Au NPs are around 14 nm and relatively large, thus leading to a low catalytic activity. Nevertheless, the temperature of full CO conversion is much lower for Au@CeO₂ core-shell submicrospheres compared

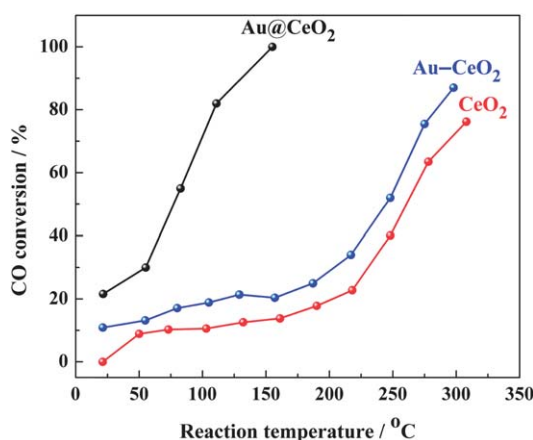


Fig. 4 Catalytic activity of Au@CeO₂, Au–CeO₂, and pure CeO₂ composites for CO oxidation. Feed gas containing 1.0 vol% CO, 1.6 vol% O₂ and balance He is at a total flow rate of 50 mL min^{−1}, corresponding to a GHSV of 15 000 mL h^{−1} g_{cat}^{−1}.

with the mixed Au–CeO₂ composites. Except for possible partial removal of citrate after calcination, the remarkably higher activity of Au@CeO₂ core-shell submicrospheres is most likely attributed to the perimeter interface effects between the metal NPs and transition metal oxide supports.^{48–50} Compared to the simple mixture of Au NPs and CeO₂ submicrospheres, the core-shell structure of Au@CeO₂ enables maximizing the contact area between Au NP and CeO₂, while minimizing the area of bare Au NPs. As a result, Au@CeO₂ core-shell submicrospheres show the high catalytic activity.

Also, we compared the catalytic activity of Au@CeO₂ core-shell submicrospheres with different Au contents. As shown in Fig. S9,† the order of catalytic activity is obtained as follows: 0.93% Au@CeO₂ > 0.55% Au@CeO₂ > 1.97% Au@CeO₂. The difference in the catalytic activity mainly originates from different sized Au NPs in the CeO₂ submicrospheres. The sizes of Au NPs inside both 0.55% Au@CeO₂ and 0.93% Au@CeO₂ samples are around ~17 nm (Fig. 1c and S10†), and the increase of the Au content is favorable for improvement of the catalytic activity. However, for the 1.97% Au@CeO₂ sample, the sizes of Au NPs are about 23 nm (Fig. S11†), and larger size Au NPs are not favorable for catalytic oxidation of CO, resulting in the lower catalytic activity.⁵¹

The stability is another important indicator to evaluate the performance of the catalysts. To make the comparison fair, we intentionally set the temperature of the catalytic reaction at the same temperature of 120 °C for both Au@CeO₂ and Au–CeO₂ samples. At 120 °C, the CO conversion ratio is around 85.1% and 20.9% on Au@CeO₂ and Au–CeO₂ catalysts, respectively. As shown in Fig. 5, no deactivation occurs for the Au@CeO₂ core-shell submicrospheres when the catalytic reaction is performed at 120 °C for 72 h. The TEM image further reveals that there are no obvious changes in the size, shape and structure of the core-shell submicrospheres (Fig. S12†). In contrast, the deactivation happens over the Au–CeO₂ catalyst, and the corresponding CO conversion ratio at 120 °C is decreased from 20.9% to 9.3% after 72 h reaction. As discussed above, many factors, *e.g.*, the size of Au NPs, the surface density of citrate capping agents and the contact area between CeO₂ and Au, would influence the activity of the catalysts. In this work, the deactivation is mainly caused by migration and sintering of Au NPs in the mixed Au–CeO₂ catalysts, which is confirmed by TEM observation that the average sizes of Au NPs are increased from original 14 nm to 18 nm after the

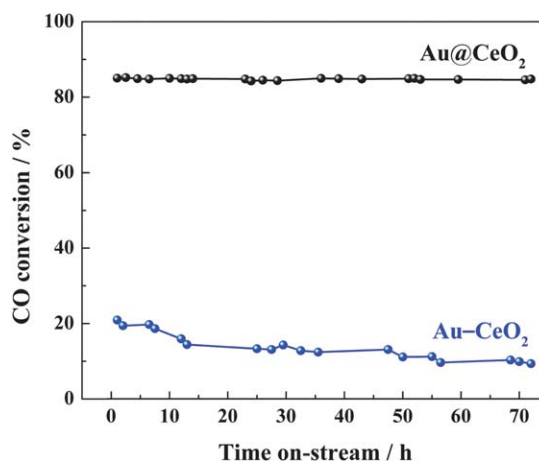


Fig. 5 Stability test of Au@CeO₂ and Au–CeO₂ at 120 °C for catalytic CO oxidation under the conditions of Fig. 4, respectively.

catalytic reaction (Fig. S13†). Notably, encapsulation of a single Au NP inside the CeO₂ matrix for Au@CeO₂ samples can effectively improve their stability during the catalytic process (Fig. S14†).

In conclusion, we have developed a novel and facile synthesis strategy to construct the Au@CeO₂ core-shell submicrospheres by combination of the hydrothermal and calcinating processes. The obtained Au@CeO₂ product is characterized by a Au NP core coated with a shell self-assembled by spherical CeO₂ NPs. The large contact areas between Au NP cores and CeO₂ matrices promote the catalytic oxidation of CO, while the mesopores inside CeO₂ NP aggregates are favorable for high efficiency mass transfer during the CO oxidation process, thus resulting in high catalytic activity. Furthermore, the core-shell structures can immobilize the Au NP cores and prevent possible migration and sintering, leading to superior catalytic stability. The new strategy is expected to be broadly employed to synthesize other nanomaterials of well-defined structures, which have potential applications in energy and environmental fields.

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