

Hydroamination of ethylene by aniline: catalysis in water

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The platinum-catalyzed and halide-promoted hydroamination of ethylene with aniline is reported for the first time in the presence of simple sodium halides in water. Compounds K_2PtX_4 ($X = Cl$ or Br), PtX_2 or PtX_4 (0.3% mol) in the presence of an aqueous solution of excess NaX and aniline under ethylene pressure (25 bar) affords *N*-ethylaniline with 60–85 turnovers after 10 h at 150 °C. The best result (TON = 85) was obtained in the presence of excess $NaBr$, whereas a slightly lower activity was observed with $NaCl$ (60 cycles) and practically no activity with NaF or NaI (2–4 cycles). The reaction also produces *N,N*-diethylaniline (up to 1 cycle) and 2-methylquinoline (up to 8 cycles) as by-products. The influence of added H^+ and different oxidizing agents was also examined.

Introduction

Catalytic hydroamination, the direct formation of a new C–N bond by addition of the N–H bond to an unsaturated C=C function in the presence of a catalyst, is a subject of current interest both for fundamental research and for the chemical industry.^{1–3} It is an atom-economical reaction constituting an interesting alternative entry to higher amines, which currently is mostly achieved by the catalyzed condensation of ammonia or amines with alcohols.⁴ Since most primary alcohols are industrially produced from alkenes (hydroformylation–hydrogenation sequence),^{5,6} the hydroamination process would suppress at least one step and avoid the coproduction of water. The intermolecular version of this reaction with non-activated olefins is still a great challenge to chemists.^{2,3} The direct reaction of ethene with compounds containing N–H bonds (amines, amides, etc.) is of particular interest for the large-scale synthesis of ethyl-substituted nitrogen compounds.

An interesting catalytic system (in terms of both activity and operating conditions) for the platinum-catalyzed addition of aniline to ethylene was introduced in 2004 by Brunet and co-workers.⁷ Other reports of Pt-based intermolecular hydroamination reactions (mostly of ethylene or norbornene) have subsequently appeared.^{8–14} All these catalytic systems appear to be effective for weakly basic amines such as aryl-substituted sulfonamides, carboxamides, and electron-deficient anilines, while they did not lead to a satisfactory conversion for more basic amines. For example, no reaction was observed for the ethylene hydroamination with secondary amines in the presence of $[PtCl_2(C_2H_4)]_2/PPH_3$ ⁸ or for the norbornene hydroamination with aniline in the presence of $(COD)Pt(OTf)_2$.⁹

The Brunet system, consisting of simple platinum halides (PtX_2 ¹⁵ or PtX_4 ¹²) in the presence of a molten halide salt, nBu_4PX , as a promoter, appears the simplest and most effective among the family of platinum catalysts. The initial report focused on the properties of nBu_4PX as an ionic solvent,^{7,15} but a more detailed study of catalytic activity as a function of halide nature and X/Pt ratio revealed that the salt rather functions as an activator through the presence of the coordinating halide anion,¹² with bromide leading to the highest activity increase for the addition of aniline to ethylene. Catalytic schemes based on the dominant role of $[PtBr_4]^{2-}$ or $[PtBr_3(C_2H_4)]^-$ have then been proposed.^{13,16}

The Brunet catalyst is already quite simple and robust, because it is made up of commercially available ligandless platinum halides plus an organic halide additive with no need to use organic solvents, and was shown to be nearly as efficient when taking no special precaution to remove air from the system. However, we strove to further simplify it by changing the salt additive to a more readily available and less expensive alkali metal halide, dissolved in water. These are the “greenest” possible conditions that one can imagine for this atom-economical transformation. We were pleased with the results of this investigation, which will be shown in this contribution.

Experimental

Methods and materials

$PtCl_2$ (STREM), $PtBr_2$ (Alfa Aesar), $PtCl_4$ (STREM), $PtBr_4$ (STREM), K_2PtCl_4 (Alfa Aesar), K_2PtBr_4 (Aldrich), $PdBr_2$ (Aldrich), Pt black (STREM), NaF (Alfa Aesar), NaX ($X = Cl, Br, I$ Acros Organics), $CuCl_2$ (STREM), and nBu_4PBr (Aldrich) were used as received. Benzoquinone (Acros) was resublimed before use. Aniline and 2-methylquinoline (Alfa Aesar), *N*-ethylaniline and *N,N*-diethylaniline (Acros), and *N,N*-dibutylaniline (Acros) were distilled under vacuum and kept under argon in the dark. Distilled water was degassed by an argon flow before each experiment. DMSO, DMF (VWR Prolabo) and EtOH (Carlo Erba) were used as received and degassed by an argon flow before experiments. Ethylene (N25)

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was purchased from Air Liquide. Unless otherwise stated, all the manipulations were performed under argon.

Instrumentation

The GC analyses were performed on a Hewlett-Packard HP 4890 chromatograph equipped with an FID, an HP 3395 integrator and a 30 m HP1 capillary column. Under the selected operating conditions [helium as carrier gas at $p = 50$ kPa, $T_{\text{start}} = 65$ °C (2 min), $\Delta T = 6$ °C min⁻¹, $T_{\text{end}} = 200$ °C (20 min)] the retention times were: PhNH₂, 7 min; PhNH₂Et, 11 min; PhNEt₂, 12 min; quinaldine, 15 min; PhN(*n*Bu)₂ (external standard), 21 min. Small amounts of by-products (maximum intensity of 50% relative to the peak of PhNEt₂) were eluted after 13, 15, 17 and 18 min. Calibration curves for each compound were obtained using pure samples at several different concentrations. NMR (¹H and ¹³C{¹H}) investigations were carried out on a Bruker DPX300 spectrometer operating at 300.1 MHz (¹H) and 75.47 MHz (¹³C{¹H}). D₂O (traces) and CD₂Cl₂ (traces) were added for locking purposes for the analysis of the water-rich and organic-rich phases, respectively.

Hydroamination of ethylene by aniline

Catalytic experiments were conducted in a 100 ml stainless steel autoclave without glass liner under magnetic stirring. It was experimentally observed (see Results and discussion) that the use of glass liners results in inhomogeneous conditions with loss of reproducibility. In a typical procedure, the autoclave was charged with the Pt compound (PtX₂, or PtX₄, or K₂PtX₄; 0.13 mmol) and the desired excess amount of NaX (see Results and discussion section), closed, and submitted to vacuum/argon cycles. Degassed water (15 or 5 ml) and then aniline (4.15 ml, 45 mmol) were added to the autoclave by syringe through a valve equipped with septum and the ethylene pressure adjusted to 25 bar (*ca.* 100 mmol). The temperature was then raised to 150 °C. After 10 h, the autoclave was allowed to cool to room temperature and slowly vented. The entire reaction mixture was treated with the external standard (*N,N*-dibutylaniline) and extracted with dichloromethane (*ca.* 60 ml). The organic layer was analyzed by GC and GC-MS. Each run presented in this work was performed at least twice (up to five times for the most relevant results). A statistical analysis of reproducibility gives the following errors for the measured turnover number (TON) values: PhNH₂Et, ±10; PhNEt₂ and quinaldine, ±1.

Results and discussion

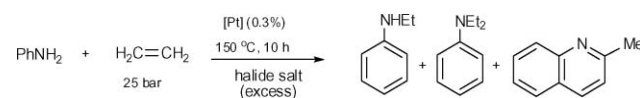
Our study started with a verification of the previously published experimental work.⁷ We found the same results at the qualitative level, with the reaction producing *N*-ethylaniline (major), *N,N*-diethylaniline (traces) and 2-methylquinoline or quinaldine (minor), see Scheme 1. However, the occasional lack of reproducibility encouraged us to test the reaction in the absence of glass liner, yielding reproducibly higher TON, see Table 1. This phenomenon is attributed to the accumulation of condensed substrate vapours in the small cavity between the glass liner and the autoclave walls, as indeed experimentally observed. As shown in Table 1, the previously reported decrease of the activity upon increasing the salt amount was confirmed.

Table 1 Pt-catalyzed aniline addition to ethylene in the presence of *n*Bu₄Br^a

Run	Salt/Pt	Glass liner	PhNH ₂ TON	PhNEt ₂ TON	Quinaldine TON	Conv. (%)	Ref.
	10	Yes	130	1	10	40	13
	150	Yes	80	1	10	26	7
1	10	No	140	3	15	45	^b
2	150	No	100	1	15	33	^b

^a Conditions: PtBr₂ (0.13 mmol), aniline (4.15 mL), ethylene (25 bar at RT), *n*Bu₄Br, $T = 150$ °C, $t = 10$ h. ^b This work.

All subsequent experiments were therefore run in the absence of glass liner.



Scheme 1

The process was then investigated with aqueous NaBr in place of *n*Bu₄PBr. This salt was initially selected because the bromide anion was previously shown to yield the best activities for the tetra-*n*-butylammonium salt series (see Introduction). All runs were carried out over 10 h, the same lapse of time used in the previous work with *n*Bu₄PBr.⁷ The same three products shown in Scheme 1 were again obtained in roughly the same proportions, with only a marginally lower catalytic activity, see Table 2, run 3. Some other organic compounds were also detected in trace amounts (<0.5%), among which 1,2,3,4-tetrahydro-2-methylquinoline could be identified on the basis of a GC-MS analysis. Note that exactly the same product composition was previously observed when using *n*Bu₄PBr, underlying the same mechanism.⁷ Note also that no catalysis was observed in the absence of PtBr₂ (run 4), and a very low activity was recorded in the presence of PtBr₂ but in the absence of NaBr (run 5). Thus, the activating role of the bromide salt is confirmed for the new catalytic conditions reported here.

One question that needs to be addressed is the effect of the reaction time and of possible catalyst deactivation. The Brunet catalyst was already shown to deposit inactive metallic Pt with activities reaching a plateau after *ca.* 10 h: the TON for the *N*-ethylaniline product was 37 after 1 h, 64 after 2.5 h, 72 after 5 h and 80 after 10 h.⁷ We have therefore tested our system at longer reaction time (runs 6 and 7). Activities were essentially the same as after 10 h, confirming that the catalyst is totally

Table 2 Pt-catalyzed aniline addition to ethylene in the presence of aqueous NaBr^a

Run	Salt/Pt	Time/h	PhNH ₂ TON	PhNEt ₂ TON	Quinaldine TON	Conv. (%)
3	150	10	85	1	8	27
4	^b	10	~0.6	0	1	0.5
5	0	10	5	~0.1	1	1.7
6	150	24	90	1	8	28
7	150	48	90	1	8	28

^a Conditions: PtBr₂ (0.13 mmol), aniline (4.15 ml), ethylene (25 bar at RT), NaBr (150 equiv.) in water (15 mL), $T = 150$ °C. ^b Same amount of NaBr as in run 3, in the absence of PtBr₂.

Table 3 Pt-catalyzed aniline addition to ethylene. Influence of the NaBr and water amounts^a

Run	Salt/Pt	Water/ mL	PhNHet TON	PhNEt ₂ TON	Quinaldine TON	Conv. (%)
8	10	15	24	~0.3	3	8
9	100	15	64	1	6	20
10	200	15	45	1	5	15
11	500	15	27	6	3	10
12	10	5	62	2	7	20
13	50	5	74	3	8	24
14	100	5	61	3	8	21
15	150	5	31	2	7	11

^a Conditions as in Table 2, except for the amount of NaBr and/or water.

deactivated. Visual inspection of the reaction mixture confirms the total conversion of the catalyst into the metallic state. The discharged reaction mixture consists of a two phase system with a colorless aqueous phase and a black stable suspension in the organic layer.

We next proceeded to investigate the influence of the NaBr amount. Runs 3 and 4 involved ~2 g of NaBr, whereas >10 g can be dissolved in the same amount of water at room temperature. It should be noted that aniline is also partially soluble in water (3.6 g per 100 mL at 20 °C)¹⁷ and this certainly has an influence on the NaBr solubility. At the reaction temperature of 150 °C, the water/aniline miscibility is expected to significantly increase and the NaBr solubility may also increase, but a miscibility study of the water/aniline/NaBr ternary system does not appear to be available. We were only able to find a phase diagram of the water-aniline mixture at 1 atm, showing equilibrium between two phases containing respectively 16% and 78% aniline at 150 °C. The presence of NaBr in large quantities is expected to render the two liquids less miscible, thus a biphasic system is certainly present under catalytic conditions. In addition, the system is further complicated by the presence of ethylene. A phase diagram investigation for this complex mixture is beyond the scope of the present study. The catalytic results obtained in the presence of variable NaBr amounts are presented in Table 3.

It is clearly seen that upon increasing the NaBr amount beyond 150 equivalents the total activity decreases (runs 10 and 11), which is in agreement with the results obtained in the presence of *n*Bu₄PBr (Table 1), while the selectivity tends to shift in favour of the *N,N*-diethylamine product. Reducing the amount of salt also resulted in loss of activity (runs 8 and 9). This behaviour is different from that of the *n*Bu₄PBr promoter, for which a higher activity was observed with a Br/Pt ratio of 10 (Table 1). The best activity remains that observed in run 3 (Table 2) with 150 equivalents of NaBr per Pt. Note also that the entire NaBr amount was found dissolved (not observed as a solid) in all the recovered mixtures. Next, we have tested the influence of the amount of water in the medium. Reducing the amount of water from 15 to 5 mL for either a tenfold (run 12) or a fifty-fold (run 13) excess of NaBr gave a higher activity, close to that of run 3 in Table 2. However, upon further increasing the NaBr amount the overall activity decreases (runs 14, 15). In this case the best activity was found with a fifty-fold excess.

The influence of H⁺ on the reaction was also examined. This study was justified by the previous report of a positive effect of

Table 4 Pt-catalyzed aniline addition to ethylene. Influence of added acids.^a

Run	Acid (eq.)	PhNHet TON	PhNEt ₂ TON	Quinaldine TON	Conv. (%)
16	HBr (1)	88	2	8	28
17	HBr (3)	78	3	7	25
18	HBr (5)	41	4	5	14
19	HBr (20)	26	9	3	11
20	CF ₃ COOH (1)	79	2	8	25
21	Et ₂ O·HBF ₄ (3)	51	4	6	17

^a Conditions as in Table 2, run 3, except for the acid addition.**Table 5** Pt-catalyzed aniline addition to ethylene. Influence of oxidants^a

Run	Additive (eq.)	PhNHet TON	PhNEt ₂ TON	Quinaldine TON	Conv. (%)
22	— ^b	43	2	5	14
23	CuCl ₂ (5), HCl (5) ^b	24	2	2	8
24	HCl (5) ^b	39	2	6	13
25	CuCl ₂ (5)	15	1	1	5
26	CuCl ₂ (5) ^b	20	2	3	7
27	benzoquinone (10)	69	1	7	22
28	DMSO ^b (10)	13	0.4	6	6
29	DMSO (10)	23	1	7	9

^a Conditions as in Table 2, run 3, except for the additive. ^b Experiment run without removing air from the aniline and from the autoclave head space.

catalytic amounts of strong acids (3 equiv. per Pt), which would be levelled in strength to anilinium in the reaction medium.⁷ The same phenomenon might be expected under the present catalytic conditions, since aniline is a stronger base than water. The catalytic results, see Table 4, show that acids do not have a promoting effect under the present conditions. Rather, a small but significant decrease of activity was revealed in the presence of excess acid. One equivalent of acid (either HBr or CF₃COOH) has essentially no effect on the activity (*cf.* runs 16 and 20 with run 3), but further acid addition (runs 17–19, 21) has a negative effect on the activity. Note also that the reaction selectivity changes, the TON decreasing for ethylaniline and quinaldine and increasing for diethylaniline as the amount of HBr increases (runs 16–19).

We have also investigated the effect of specific oxidants as additives, in an attempt to avoid the deposition of Pt⁰ or oxidize it back to an active form of the catalyst. Pt⁰ is not active for the ethylene hydroamination: a test run in the presence of the same catalytic amount of platinum black gave only a 0.6% conversion with *ca.* 1 TON for ethylaniline and 1 TON for quinaldine (essentially the same results as in the control without Pt compound, run 4). Agents such as benzoquinone,^{18–20} O₂/CuCl₂,^{21–23} or O₂/DMSO²⁴ were shown to oxidize Pd⁰ for related catalytic systems. The results are shown in Table 5. We first carried out the reaction in the presence of air (run 22), yielding approximately half the activity recorded under argon (run 3). Further addition of CuCl₂ and HCl to the system (conditions of the Wacker process) further decreases the activity. The negative effect of strong acids has been pointed out above (runs 16–19), but note that the presence of CuCl₂ also seems

Table 6 Pt-catalyzed aniline addition to ethylene. Influence of added solvents^a

Run	Additive/mL	PhNHEt TON	PhNEt ₂ TON	Quinaldine TON	Conv. (%)
30	DMSO (7)	0	0	0	0
31	DMF (7)	3	0	1	1
32	EtOH (2)	72	2	8	23

^a Conditions as in Table 2, run 3, except for the additive.

to have a negative effect in this case, because the activity in the presence of CuCl₂ alone is lower than that in the presence of HCl alone (run 24), and this does not greatly depend upon whether the catalysis is run under argon (run 25) or in the presence of air (run 26). The presence of benzoquinone or DMSO/air also does not improve the results (runs 27 and 28). The activity in the presence of DMSO under argon (run 29) is slightly better than in air (run 28), but still lower than that of run 3 in the absence of DMSO. The formation of a Pt⁰ deposit was still observed in all these catalytic runs.

As mentioned above, the catalytic reaction most certainly occurs in a biphasic system at 150 °C. Thus, we have explored the effect of the addition of compatibilizing solvents, in an attempt to homogenise the system. The addition of bipolar aprotic solvents such as DMF or DMSO (*ca.* 7 ml) completely homogenise the system aniline-water-NaBr (150 eq.) at room temperature. The catalytic results, see Table 6, show complete or nearly complete deactivation by DMSO (run 30) or DMF (run 31), respectively. It should be noted that DMSO and DMF are also strong ligands. In a previous study, we have shown that isolated Pt-aniline complexes lose the aniline and/or ethylene ligand upon dissolution in DMSO.¹⁶ On the other hand, heating the same complexes in DMF leads to decomposition. Thus, although DMSO and DMF are able to homogenise the system, they probably lead to other stable and catalytically inactive Pt complexes. Conversely, the addition of EtOH leads to a marginally lower activity (*cf.* run 32 and run 3).

Another important point to investigate was the influence of the halide nature. We have tested the entire series of sodium halides NaX, including the fluoride not previously investigated along the *n*Bu₄PX series.^{7,10,12} The results, reported in Table 7, show that practically no reaction takes place when X = F or I. The highest activities were observed in the middle of the group for X = Br and Cl, with Br being slightly better. These results perfectly parallel those previously established for the *n*Bu₄PX system.

Table 7 Pt-catalyzed aniline addition to ethylene. Influence of the halogen in NaX^a

Run	Salt	PhNHEt TON	PhNEt ₂ TON	Quinaldine TON	Conv. (%)
33	NaF	2	0	1	1
34	NaCl	60	1	5	19
35	NaI	4	~ 0.3	2	2

^a Conditions as in Table 2, run 3, except for the nature of NaX.**Table 8** Catalyzed aniline addition to ethylene. Influence of the pre-catalyst nature^a

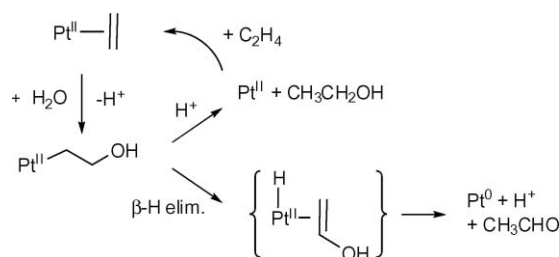
Run	[Pt]	PhNHEt TON	PhNEt ₂ TON	Quinaldine TON	Conv. (%)
36	K ₂ PtCl ₄	86	1	8	27
37	K ₂ PtBr ₄	81	1	7	25
38	PtCl ₂	70	1	8	23
39	PtI ₂	19	1	2	7
40	PtCl ₄	80	2	8	26
41	PtBr ₄	76	3	6	24
42	PdBr ₂	1	0	~0.3	0.4

^a Conditions as in Table 2, run 3, except for the nature of the pre-catalyst.

Finally, we have tested other sources of Pt different from PtBr₂, namely K₂PtX₄, PtX₄ (X = Cl or Br) or PtX₂ (X = Cl, I), and also PdBr₂. According to the proposed mechanism,^{13,16} all the Pt precatalysts should yield [PtBr₄]²⁻ dominant species in the presence of excess NaBr, or [PtBr₃(C₂H₄)]⁻ in the presence of C₂H₄.¹⁶ Furthermore, PtX₄ could be easily reduced to the same Pt^{II} complexes under the catalytic conditions, for example by ethylene to form CH₂BrCH₂Br. Indeed, compounds PtBr₂, PtBr₄ and PtCl₄ were previously shown to have essentially the same catalytic activity in the presence of the same excess amount of *n*Bu₄PBr.¹² As can be seen from the results in Table 8, the different Pt compounds also give essentially identical results under the new conditions reported in this contribution. Only marginally lower activities were obtained with PtCl₂ (run 38), perhaps because it slowly decomposes upon standing in air and a partially impure sample may have been used. Much poorer results were also obtained with PtI₂ (run 39), possibly for similar reasons.

A last catalytic run was performed with PdBr₂ (run 42). Both platinum(II) and palladium(II) complexes activate olefins toward nucleophilic attack, but in contrast to their Pd(II) counterparts, Pt(II) alkyl complexes are less prone to β-hydride elimination, whereas they maintain reactivity toward protonolysis. Thus, Pd systems resulting from amine nucleophilic addition to coordinated ethylene usually prefer to undergo oxidative amination.^{1,20,25} However, run 42 led to essentially no reaction. Neither the expected hydroamination products nor the oxidative amination products were detected by either gas chromatography or ¹H NMR in both the organic and the aqueous phases (a few small and unassigned resonances corresponded to <0.5% of aniline consumption).

An interesting question concerns the possible nucleophilic addition of water to coordinated ethylene. Such reactivity would result in parallel catalytic processes (formation of ethanol by protonolysis with regeneration of Pt^{II}, although the reverse process has rather been shown to be favored²⁶) or stoichiometric processes (formation of acetaldehyde by β-H elimination with formation of Pt⁰ as in the Pd-catalyzed Wacker process), see Scheme 2. The latter events might in fact rationalize the slightly lower TON (faster catalytic deactivation) of this aqueous catalytic system relative to the Brunet system. Note that, although no direct nucleophilic attack of Pt^{II}-coordinated olefins by water or alcohols has been reported under neutral conditions,²⁷ both ethanol and acetaldehyde were previously observed from the reaction of Pt^{II}-ethylene derivatives upon



Scheme 2

standing in water and ethylene glycol may also be formed in the presence of oxidants.^{28–32} In an aqueous aniline environment, it is also envisageable that acetaldehyde may be present as the hydrate $\text{CH}_3\text{CH}(\text{OH})_2$ or transformed to the imine $\text{CH}_3\text{CH}=\text{NPh}$. In order to verify whether any of these products are formed, an NMR (^1H and $^{13}\text{C}\{^1\text{H}\}$) analysis of both the aqueous and organic phases was performed for runs 6 and 7. In addition to the recognizable resonances of aniline and the three observed products (Scheme 1), other small resonances were indeed visible in the methyl proton region (δ ca. 1.8, 1.4 and 1.3), and only in the organic phase. Integration of these resonances, however, indicated that they correspond to <1 TON. Thus, even assuming that one of these resonances belong to ethanol, we can conclude that the catalyzed ethylene hydration is much less efficient than the hydroamination by aniline. The possible formation of a small stoichiometric amount of CH_3CHO , $\text{CH}_3\text{CH}=\text{NPh}$, or other products of further reactions cannot be excluded and it may indeed contribute to faster catalyst deactivation.

Conclusions

The efficiency and potential of the Pt-catalysed ethylene hydroamination by aniline under green operating conditions (NaBr/water as additive) has been demonstrated. The optimized conditions (run 3 in Table 2) lead to about 85 catalytic turnovers in 10 h. Although the catalytic activity, in terms of TON, is ca. 44% lower than the system operating with nBu_4PBr and without water under identical conditions, this new system represents a valuable gain in terms of operational simplicity and environmental impact, because the nBu_4PBr salt can be replaced by the much more accessible, less toxic,^{33,34} and water-soluble NaBr. New mechanistic information is also given by the lack of a major inhibiting effect of water or ethanol, whereas the presence of large amounts of DMF and DMSO results in a dramatic decrease of catalytic activity, as was already shown earlier for phosphine ligands.⁷ The absence of significant amounts of ethanol in the reaction products demonstrates that hydration is not competitive relative to the addition of the aniline N–H bond, whereas possible stoichiometric Wacker-type processes leading to Pt reduction may rationalize the slightly lower performance of the aqueous system relative to $\text{PtBr}_2/\text{nBu}_4\text{PBr}$. Higher turnovers cannot be achieved because of complete catalyst deactivation. A future challenge will be to engineer a catalyst for which this deactivation process is retarded or eliminated.

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