

# The Effect of Water on the Adsorption of NO<sub>2</sub> in Na– and Ba–Y, FAU Zeolites: A Combined FTIR and TPD Investigation

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The adsorption of NO<sub>2</sub> was investigated and compared on Na– and Ba–Y, FAU zeolites both in the absence and presence of adsorbed water using FTIR and TPD techniques. The same ionic NO<sub>x</sub> species (NO<sup>+</sup>, NO<sup>+</sup>–NO<sub>2</sub>, NO<sub>3</sub><sup>–</sup>), formed by the disproportionation of NO<sub>2</sub>, were observed to form on both materials under dry conditions at room temperature. The thermal stabilities of these species, however, were vastly different on the two materials. Room-temperature evacuation was sufficient to decompose the NO<sup>+</sup>NO<sub>2</sub> adduct in Na–Y, while this species was stable up to 350 K over Ba–Y. The adsorbed NO<sup>+</sup> was also much more stable over Ba–Y than on Na–Y. Water significantly affected the adsorbed NO<sub>x</sub> species on both materials. In the presence of water, the IR signatures of adsorbed NO<sup>+</sup> were eliminated from both catalysts; however, it did not affect the IR feature of the NO<sup>+</sup>NO<sub>2</sub> species on Ba–Y. In the TPD spectra, the NO<sub>2</sub> desorption peak shifted from 350 K to 520 K on Na–Y preexposed to water. In Ba–Y, the high-temperature NO<sub>2</sub> desorption feature of ~470 K shifted to ~620 K as a result of adsorption on the water-containing sample, while the low-temperature peak remained unchanged.

## Introduction

The removal of NO<sub>x</sub> from automotive exhaust gases is a tremendous challenge to the catalytic community, in particular when the engine is operated under lean conditions, that is, in excess oxygen (e.g., diesel engines). Under these conditions, the traditional three-way catalysts do not work because of their very high activity for hydrocarbon oxidation that results in the depletion of the reducing agent before NO<sub>x</sub> reduction can take place. Therefore, several emerging technologies are being considered for diesel exhaust aftertreatment. Among the most promising ones are the NO<sub>x</sub> adsorber<sup>1</sup> and the nonthermal plasma assisted catalytic NO<sub>x</sub> reduction technologies.<sup>2–13</sup> Base metal oxide adsorbers (in particular BaO) are highly effective for the removal of NO<sub>x</sub> from an oxygen-rich exhaust gas mixture. Recently, we reported very promising activities for both Na– and Ba–Y, FAU zeolites in the catalytic lean NO<sub>x</sub> reduction, when the catalyst was used in conjunction with a nonthermal plasma.<sup>14</sup> In the plasma, reactive species are formed that are converted to benign compounds over these base catalysts. The two most important reactions that take place in the plasma are the almost complete conversion of NO to NO<sub>2</sub> and the formation of partially oxidized hydrocarbon species (e.g., acetaldehyde) in significant quantities. Combining the strong oxidizing power of NO<sub>2</sub> and the ease of oxidizability of CH<sub>3</sub>–CHO results in high level of NO<sub>x</sub> reduction over these base zeolite catalysts at relatively low temperatures (~473 K).

In our previous work,<sup>15</sup> we reported that exchanging the charge-compensating Na<sup>+</sup> ions for Ba<sup>2+</sup> ions in Y, FAU (Y) zeolites increases the NO<sub>x</sub> conversion by more than 10% and also widens the temperature window in which high activity can be sustained. We have suggested that one possible explanation of this activity enhancement was the stronger adsorption of NO<sub>2</sub> observed over Ba–Y in comparison to Na–Y. Here, we report

on our recent finding on the adsorption of NO<sub>2</sub> on both Na– and Ba–Y. We used FTIR spectroscopy to identify the nature of adsorbed species and correlated those finding with the results obtained from the temperature-programmed desorption (TPD) of NO<sub>2</sub>. The adsorption and desorption of NO<sub>2</sub> were investigated on both water-free (dry) and water-containing (wet) catalysts. The results show significant differences between the Na– and Ba–Y zeolites in NO<sub>2</sub> adsorption. The possible consequences of these findings on their catalytic activities will also be discussed.

## Experimental Section

The catalyst materials used in this study were prepared from a Na–Y zeolite obtained from Zeolyst International (CBV 100) and had a Si/Al ratio of 2.5. For the studies on Na–Y, the commercial powder material was used without any modification. The preparation of the Ba–Y catalysts used in this study was identical to the Ba–Y (2–2) material used in our previous study.<sup>14</sup> Briefly, the starting Na–Y zeolite was ion exchanged twice with aqueous Ba–acetate solutions at 353 K, then washed with deionized water. After each ion-exchange step, the catalyst was dried at room temperature and then calcined in air at 773 K for 4 h to reach a high ion exchange level. XRD showed that both the starting Na–Y and the prepared Ba–Y were highly crystalline. <sup>27</sup>Al and <sup>29</sup>Si NMR were used to verify the absence of extraframework aluminum.

The FTIR measurements were carried out with a Mattson Research Series FTIR spectrometer, equipped with an MCT detector, and operated at 4 cm<sup>–1</sup> resolution. Each spectrum was an average of 256 scans. The IR cell was a stainless steel six-way cube attached to both a pumping and a gas handling station and equipped with CaF<sub>2</sub> windows. The base pressure of the cell was less than 1 × 10<sup>–6</sup> Torr, and the maximum pressure attainable was 1000 Torr. The powder zeolite sample was

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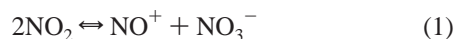
pressed onto a fine-tungsten mesh, which in turn was attached to copper heating legs sitting on ceramic feed-throughs. This setup allows the resistive heating of the sample to  $\sim 1000$  K and cooling to  $\sim 100$  K. The sample temperature was monitored through a chromel/alumel thermocouple spot welded to the top center of the tungsten grid.

After the sample was mounted in the IR cell, it was gradually heated to 773 K in a vacuum and kept at that temperature for at least 2 h to ensure the removal of water from the zeolite pores. (We also commonly baked the IR cell and the gas manifold during dehydration to minimize the readsorption of water from the walls of the IR cell into the zeolite upon completion of the annealing.) Adsorption experiments on the thus prepared samples were conducted in the following fashion: In the NO<sub>2</sub> adsorption experiments, NO<sub>2</sub> aliquots in increasing amounts were added to the sample. After 5 min equilibration time, an IR spectrum was acquired after each gas introduction. Upon completion of the adsorption experiment, the stability of the adsorbed NO<sub>x</sub> species were examined by first evacuating the sample at room temperature and then gradually heating it up to higher temperature ( $T_{\text{max.}} = 773$  K). In the experiment when the effect of H<sub>2</sub>O on the NO<sub>2</sub> adsorption was studied, first a given amount of water was added to the catalyst followed by the step-by-step addition of NO<sub>2</sub>. These experiments were also carried out in a reverse order of adsorption, that is, the sample was first saturated with NO<sub>2</sub> and then H<sub>2</sub>O was added in increasing amounts.

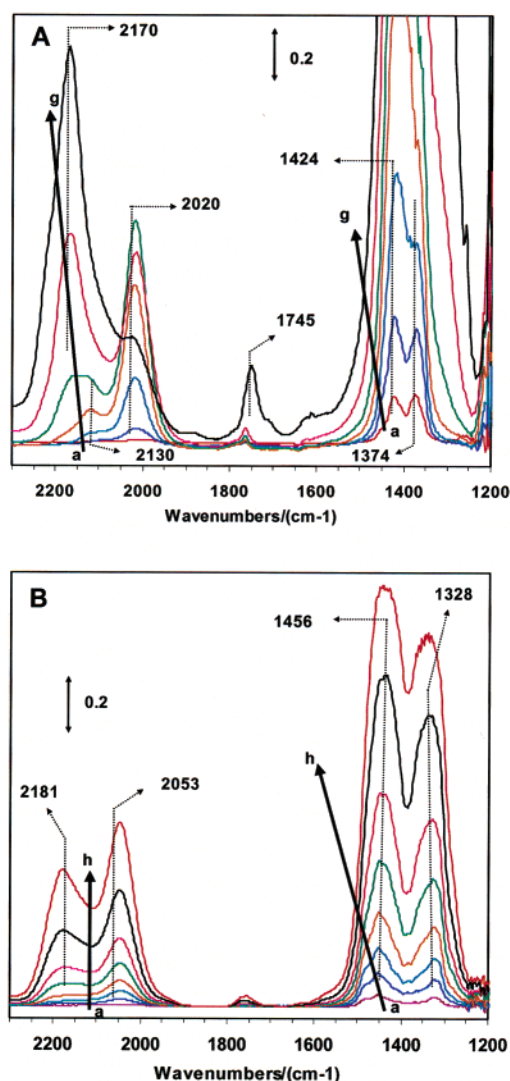
The NO<sub>2</sub> adsorption and TPD experiments were conducted on an RXM 100 catalyst characterization system (ASDI). The catalyst ( $\sim 0.025$  gr) was placed into a quartz reactor, evacuated at room temperature, and then annealed at 773 K for 2 h (the base pressure in the reactor after catalyst activation was  $< 2 \times 10^{-7}$  Torr). NO<sub>2</sub> then was adsorbed on the dehydrated catalyst. The reactor was evacuated until the base pressure dropped below  $1 \times 10^{-6}$  Torr and then a TPD program was run from 293 to 773 K at a heating rate of 5 K/min. The masses were monitored by a UTI 100 mass spectrometer, and the intensities of a series of masses were recorded. The masses monitored were 18 (H<sub>2</sub>O), 28 (N<sub>2</sub> or CO), 30 (NO), 32 (O<sub>2</sub>), 44 (N<sub>2</sub>O or CO<sub>2</sub>) and 46 (NO<sub>2</sub>). In the TPD spectra discussed in the following section, we show only the spectra for mass 30, since this was the most intense fragmentation species of NO<sub>2</sub>. Mass 46 (NO<sub>2</sub>) and mass 30 (NO) always followed the same desorption pattern in these TPD experiments.

## Results and Discussion

The adsorption of NO<sub>2</sub> on Na–Y has been discussed in detail in our previous publication.<sup>16</sup> We have shown that upon NO<sub>2</sub> adsorption, NO<sup>+</sup> and NO<sub>3</sub><sup>−</sup> species are formed as a result of the well-known disproportionation of NO<sub>2</sub> that takes place on solid catalyst surfaces<sup>16</sup>



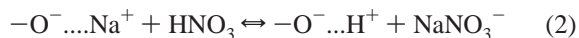
The formed NO<sup>+</sup> binds to an O<sup>−</sup> site of the zeolite framework, replacing a charge-compensating Na<sup>+</sup> ion, while the NO<sub>3</sub><sup>−</sup> binds to a Na<sup>+</sup> ion. In the presence of excess NO<sub>2</sub>, adsorption complexes such as NO<sup>+</sup>NO<sub>2</sub> or NO<sup>+</sup>N<sub>2</sub>O<sub>4</sub> can form as well. A series of IR spectra of the NO<sub>2</sub> adsorption on Na–Y is displayed in panel A of Figure 1 as a function of the amount of NO<sub>2</sub> dosed. At low NO<sub>2</sub> doses, a doublet feature is seen in the 1350–1450 cm<sup>−1</sup> range and a band at 2170 cm<sup>−1</sup>. The 1350–1450 cm<sup>−1</sup> doublet represents the split  $\nu_3$  vibrations of adsorbed NO<sub>3</sub><sup>−</sup>.<sup>17</sup> The 2170 cm<sup>−1</sup> band belongs to the N–O stretching



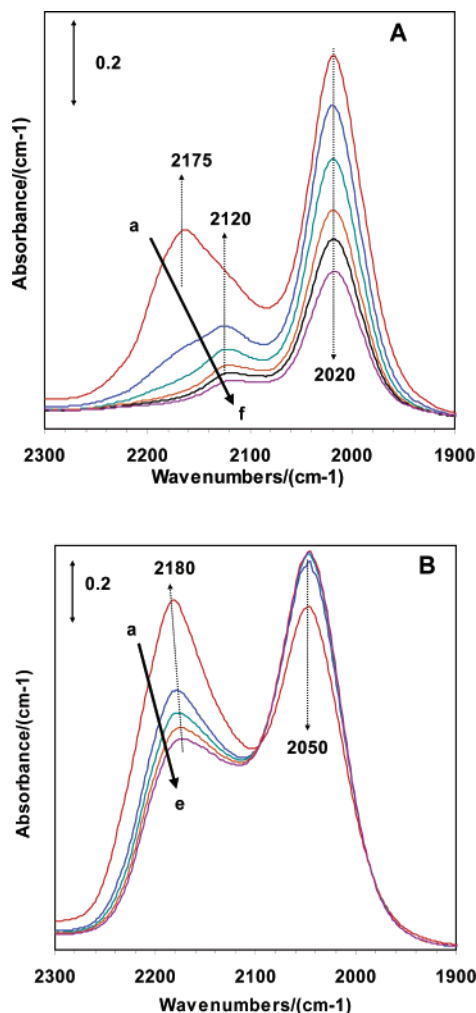
**Figure 1.** FTIR spectra following NO<sub>2</sub> adsorption on Na–Y (A) and Ba–Y (B) at 295 K. NO<sub>2</sub> doses ( $\mu\text{mol}$ ): A: 2.13 (a), 5.74 (b), 13.6 (c), 28.5 (d), 56.7 (e), 123 (f), 258 (g); B: 0.465 (a), 1.46 (b), 2.91 (c), 5.08 (d), 7.83 (e), 11.7 (f), 19.9 (g), and 32.1 (h).

vibration of the adsorbed NO<sup>+</sup> species.<sup>17</sup> A shoulder on the high-frequency side of this feature may indicate NO<sup>+</sup> adsorption on different sites available inside the zeolite structure. With increasing NO<sub>2</sub> doses, the intensities of the IR features representing both NO<sub>3</sub><sup>−</sup> and NO<sup>+</sup> increase, and a new IR feature starts developing at 2170 cm<sup>−1</sup> at higher NO<sub>2</sub> doses. We have assigned this high-frequency absorption band to a NO<sup>+</sup>NO<sub>2</sub> type of adsorption complex. As this feature develops, the intensity of the band representing NO<sup>+</sup> decreases.

There is a second mechanism for the adsorption of NO<sub>2</sub> on zeolites that involves water that is almost always present in the zeolite structure even after the most careful dehydration procedure. In this process, HNO<sub>3</sub> is formed that can readily initiate the



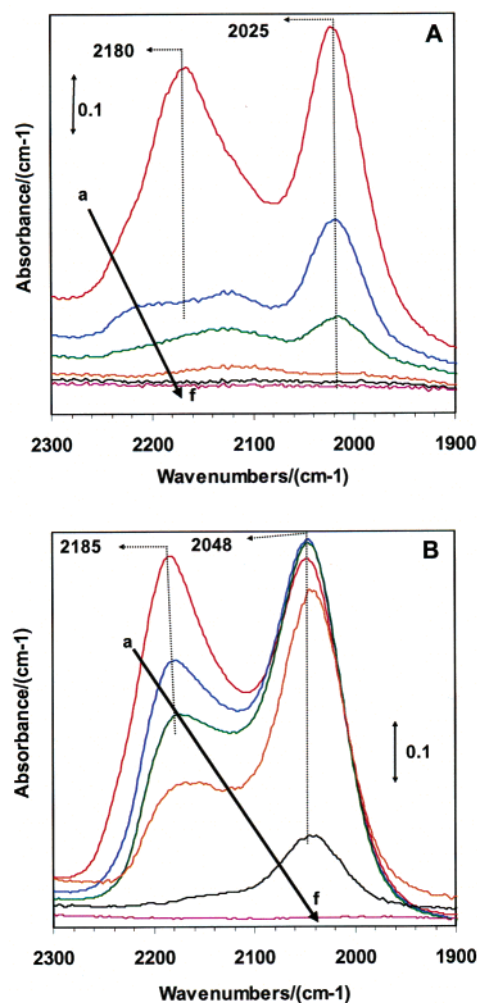
ion exchange. The thus formed Brønsted acidic site represents new adsorption centers for NO<sub>2</sub>. The NO<sup>+</sup> species formed upon the interaction of NO<sub>2</sub> with these protonic sites are represented by the IR feature at 2160 cm<sup>−1</sup> (the same IR band is seen when H–Y is contacted with NO<sub>2</sub>).



**Figure 2.** FTIR spectra after evacuation at 295 K following NO<sub>2</sub> adsorption on Na–Y (A) and Ba–Y. Evacuation time (min): A: 1 (a), 5 (b), 10 (c), 20 (d), 40 (e), 60 (f); B: 0 (a), 5 (b), 10 (c), 30 (d), and 65 (e).

The IR features that arise upon the adsorption of NO<sub>2</sub> on Ba–Y are shown in panel B of Figure 1 as a function of the amount of NO<sub>2</sub> dosed. Comparison of the absorption bands in panel A and B of Figure 1 reveals that the adsorbed species are very similar on both Na– and Ba–Y zeolites. At low NO<sub>2</sub> doses, we observe the nitrate (1300–1500 cm<sup>−1</sup>) and NO<sup>+</sup> (2053 cm<sup>−1</sup>) species adsorbed onto Ba–Y. With increasing amount of NO<sub>2</sub> introduced onto the sample, the intensities of these bands increase gradually; furthermore, new IR features develop at the high frequency side of the 2053 cm<sup>−1</sup> band. After the saturation of the 2053 cm<sup>−1</sup> feature, an intense band develops at 2180 cm<sup>−1</sup> (similarly to the 2170 cm<sup>−1</sup> band over Na–Y). We assign this feature to a NO<sup>+</sup>NO<sub>2</sub> type of adduct.

The adsorption of NO<sub>x</sub> on zeolites has been studied extensively by FTIR spectroscopy and the results of these investigations were summarized in a recent review article by Hadjiivanov.<sup>17</sup> In most of the zeolite materials studied, several adsorbed ionic species were observed upon the adsorption of NO<sub>2</sub> and in the reaction of NO + O<sub>2</sub> as well. Today it is commonly accepted that because of the disproportionation reaction of NO<sub>2</sub>, NO<sup>+</sup> and NO<sub>3</sub><sup>−</sup> species are formed inside the zeolites and are strongly held through ionic interactions. Above a threshold NO<sub>2</sub> pressure, NO<sup>+</sup> can form NO<sup>+</sup>NO<sub>2</sub> or NO<sup>+</sup>N<sub>2</sub>O<sub>4</sub> adducts. In most cases, these adducts, however, are very unstable, and can easily lose NO<sub>2</sub> to reconvert to NO<sup>+</sup>.

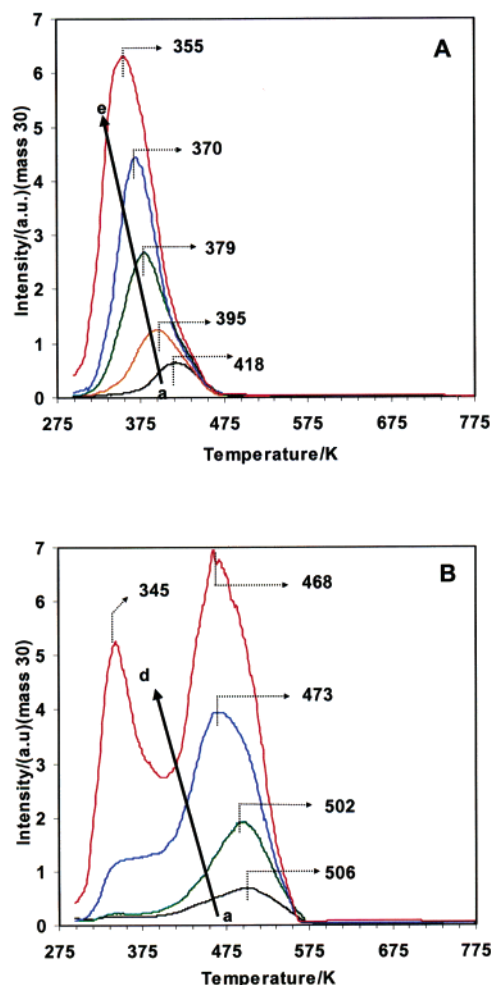


**Figure 3.** The effect of annealing on the FTIR spectra after NO<sub>2</sub> adsorption on Na–Y (A) and Ba–Y (B). A: in the presence of 0.2 Torr NO<sub>2</sub> (a), after 16-min evacuation at 295 K (b), annealing for 1 min at 373 K (c), 473 K (d), 573 K (e), and 673 K (f); B: in the presence of 0.2 Torr NO<sub>2</sub> (a), after 30-min evacuation at 295 K (b), annealing at 373 K (c), 473 K (d), 573 K (e), and 673 K (f).

The stabilities of the adsorbed NO<sub>x</sub> species of Na– and Ba–Y at room temperature under vacuum can be deduced from the IR spectra shown in Figure 2, panels A and B, respectively. Under these conditions, the IR band representing the NO<sup>+</sup>NO<sub>2</sub> adduct (2170 cm<sup>−1</sup>) on the NO<sub>2</sub>-saturated Na–Y is almost completely removed by a 1-min evacuation suggesting that this species is very unstable in the absence of gas-phase NO<sub>2</sub> on this sample. Even the intensity of the 2020 cm<sup>−1</sup> band (adsorbed NO<sup>+</sup>) is markedly decreased upon room-temperature evacuation. On Ba–Y, however, both the NO<sup>+</sup> and NO<sup>+</sup>NO<sub>2</sub> species are much more stable against room-temperature evacuation than on Na–Y. Although some intensity of the 2180 cm<sup>−1</sup> band is lost, the 2050 cm<sup>−1</sup> band remains essentially unchanged. Annealing the NO<sub>2</sub>-saturated samples results in the complete removal of the NO<sup>+</sup> adsorbed species at 373 K from Na–Y, while on the Ba–Y sample the intensities of the NO<sup>+</sup>NO<sub>2</sub> and NO<sup>+</sup> IR bands gradually decrease (Figure 3). First, the 2180 cm<sup>−1</sup> feature loses its intensity followed by the decrease in the intensity of the 2050 cm<sup>−1</sup> band. The NO<sup>+</sup> related IR band (2050 cm<sup>−1</sup>) possesses some intensity even after annealing at 573 K.

The differences in the thermal stabilities of the adsorbed NO<sub>x</sub> species in these two catalysts are well demonstrated by the results of the NO<sub>2</sub> TPD experiments shown in Figure 4 A (Na–Y) and B (Ba–Y). In Na–Y, one desorption feature was





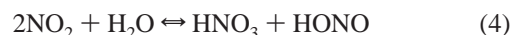
**Figure 4.** TPD spectra following NO<sub>2</sub> adsorption at 295 K on Na–Y (A) and Ba–Y (B). NO<sub>2</sub> doses (mmol): A: 2.27 (a), 4.53 (b), 9.07 (c), 13.6 (d), 22.7 (e); B: 4.53 (a), 9.07 (b), 22.7 (c), and 45.3 (d). (Weight of catalyst: 0.025 g; heating rate: 5 K/min.)

observed, and its peak position shifted to lower temperatures as the amount of adsorbed NO<sub>2</sub> was increased. At the lowest NO<sub>2</sub> dose studied, the desorption peak maximum can be seen at 418 K shifting to 355 K at the highest NO<sub>2</sub> dose. In the Ba–Y zeolite, on the other hand, two NO<sub>2</sub> desorption features can be seen (panel B of Figure 4). At the lowest NO<sub>2</sub> dose studied, only one desorption feature is present and its peak position is at 505 K. Increasing the amount of NO<sub>2</sub> adsorbed results in the development of a low-temperature desorption feature, whose peak desorption temperature does not seem to change with increasing amount of NO<sub>2</sub> dosed; it is constant at 345 K. The peak of the high-temperature desorption feature gradually downshifts as the amount of NO<sub>2</sub> adsorbed increases (similarly to the desorption feature of Na–Y). At the highest NO<sub>2</sub> dose studied, the maximum of the high-temperature feature is observed at 468 K. The coverage dependences of both the single NO<sub>2</sub> desorption feature of Na–Y and the high-temperature desorption feature of Ba–Y seem to indicate second-order desorption kinetics. From the desorption peak positions, we can estimate approximate heat of desorption values of 21–25 kcal/mol for Na–Y and 27–30 kcal/mol for Ba–Y. These estimated values may not be representative of the true desorption energies; however, their difference of ~5–6 kcal/mol is a good indicator of the stronger NO<sub>2</sub> adsorption on Ba–Y than on Na–Y.

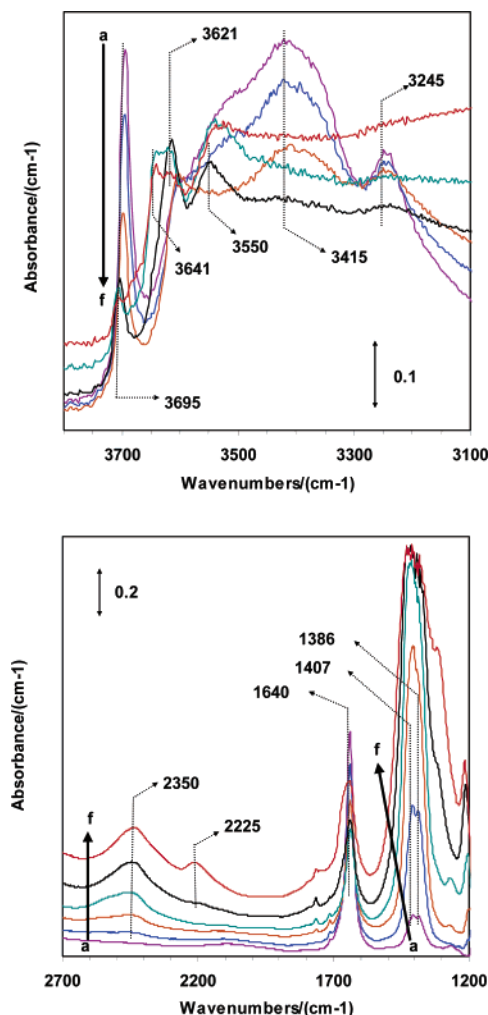
The assignments of the TPD features can be made by comparing the results of the TPD with those of the FTIR. After

NO<sub>2</sub> adsorption and full evacuation at room temperature, only NO<sup>+</sup> and NO<sub>3</sub><sup>−</sup> species are present on the Na–Y sample as shown by the single IR feature present at 2020 cm<sup>−1</sup> (NO<sup>+</sup>) and peaks in the range of 1354–1450 cm<sup>−1</sup> (NO<sub>3</sub><sup>−</sup>). In the TPD experiment, a NO<sub>2</sub> desorption feature (352–418 K) is observed as NO<sup>+</sup> and NO<sub>3</sub><sup>−</sup> recombines to give 2NO<sub>2</sub> molecules and the original clean Na–Y is restored. The situation over Ba–Y is different. After saturation with NO<sub>2</sub> and room-temperature evacuation, we observe two distinct IR absorption features (2048 and 2180 cm<sup>−1</sup>) because of the high stability of both the NO<sup>+</sup> and the NO<sup>+</sup>NO<sub>2</sub> adduct. Therefore, in the TPD experiment we observe two desorption features as well. The low-temperature peak represents the desorption of NO<sub>2</sub> from the NO<sup>+</sup>NO<sub>2</sub> adduct, while the high-temperature one arises from the recombination of the NO<sup>+</sup> and NO<sub>3</sub><sup>−</sup> species similarly to what we have shown for the NO<sub>2</sub> desorption on Na–Y. The low-temperature NO<sub>2</sub> TPD feature of Na–Y is absent because of the low thermal stability of the NO<sup>+</sup>NO<sub>2</sub> adduct on this catalyst.

As we have mentioned in the previous paragraphs, there is more than one mechanistic possibility for NO<sub>2</sub> to adsorb on the Na– and Ba–Y zeolites studied here. One is the disproportionation of NO<sub>2</sub> to form NO<sup>+</sup> and NO<sub>3</sub><sup>−</sup> according to reaction 1 that we observe to be operative on the fully dehydrated zeolite samples. The other one is the interaction of NO<sub>2</sub> with adsorbed water in the channels of zeolites. Reactions that may take place between NO<sub>2</sub> and H<sub>2</sub>O in the zeolite channels are



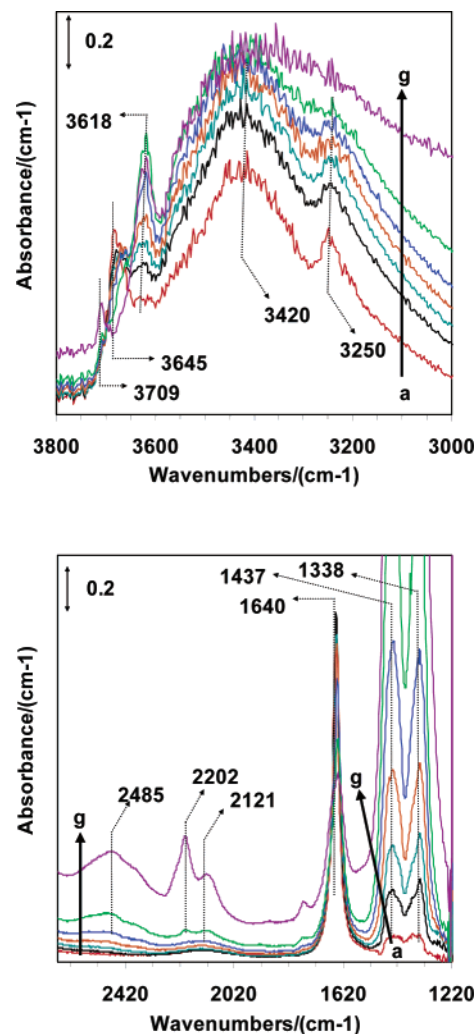
The HNO<sub>3</sub> formed in these processes can instantly interact with the charge-compensating ions (Na<sup>+</sup> or Ba<sup>2+</sup>) creating Brønsted acidic sites and Na(Ba)-nitrates (reaction 2). If this reaction sequence is correct, we expect to see the formation of Brønsted acidic OH groups, Na(Ba)-nitrates, HONO, and no adsorbed NO<sup>+</sup> following NO<sub>2</sub> exposure to hydrated samples. As it turns out, this is exactly the case. Addition of H<sub>2</sub>O to a dry Na–Y zeolite results in the appearance of absorption features in the IR spectrum that are characteristic of the adsorbed water in zeolites. The absorption bands represent δ<sub>HOH</sub> vibrations (1640 cm<sup>−1</sup>), ν<sub>OH</sub> vibrations of free O–H groups (3695 cm<sup>−1</sup>), and ν<sub>OH</sub> vibrations of associated OH groups (3100–3600 cm<sup>−1</sup>) of adsorbed water. The broad bands in the 3100–3600 cm<sup>−1</sup> region arises from water adsorbed onto cations located in different crystallographic positions.<sup>18</sup> A series of IR spectra obtained upon the adsorption of NO<sub>2</sub> on the wet Na–Y zeolite is presented in Figure 5. In this experiment, first water was added to the dry Na–Y, and then NO<sub>2</sub> was introduced onto the wet sample in increasing amounts at room temperature, and changes in the IR spectra were monitored. In Figure 5, spectrum a represents a typical IR spectrum of water adsorbed on Na–Y. Addition of a small amount of NO<sub>2</sub> onto the wet Na–Y sample resulted in the appearance of a doublet absorption band that is characteristic of NO<sub>3</sub><sup>−</sup> groups associated with Na<sup>+</sup> ions. At the same time, the intensities of both the 3695 cm<sup>−1</sup> and 1640 cm<sup>−1</sup> bands of adsorbed water started to decrease. Concomitantly, in the O–H stretching vibrational region new bands appear with peak positions characteristic of Brønsted acidic OH groups of Y zeolites (3640 and 3550 cm<sup>−1</sup>). The intensities of adsorbed water-related bands gradually decrease, while those of the NO<sub>3</sub><sup>−</sup> and zeolitic OH features increase with increasing amounts of NO<sub>2</sub> dosed. With the increase of adsorbed NO<sub>2</sub> amount, a new band develops at the low-frequency side of the NO<sub>3</sub><sup>−</sup> bands at 1270



**Figure 5.** FTIR spectra of  $\text{NO}_2$  adsorption on  $[\text{H}_2\text{O}]_{\text{ads}}\text{-Na-Y}$  at 295 K. Doses ( $\mu\text{mol}$ ):  $\text{H}_2\text{O}$ : 11.1 (a),  $\text{N}_2\text{O}$ : 2.55 (b), 6.98 (c), 17.5 (d), 40.2 (e), and 86.5 (f).

$\text{cm}^{-1}$ . This band represents adsorbed  $\text{NO}_2^-$  species probably originating from the adsorption of HONO. (This adsorbed surface species is absent when  $\text{NO}_2$  is adsorbed onto dry Na-Y.) In the  $\nu_{\text{OH}}$  region, the intensity of the band representing the stronger Brønsted acid sites of Y zeolite at  $3640\text{ cm}^{-1}$  decreases after significant amount of  $\text{NO}_2$  is added to the system, and a new feature develops at around  $3620\text{ cm}^{-1}$ . This  $\nu_{\text{OH}}$  vibration may represent the O-H stretching vibrations of  $\text{HNO}_x$  molecules formed after all the charge-compensating  $\text{Na}^+$  ions were replaced by  $\text{H}^+$ .

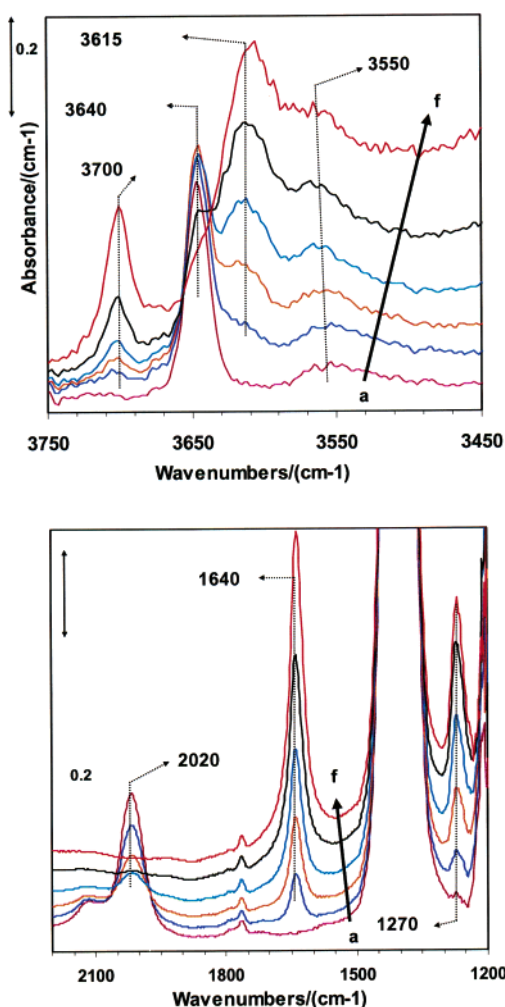
The adsorption of  $\text{NO}_2$  on water-exposed Ba-Y follows similar trends to that observed for Na-Y. The series of IR spectra recorded upon the adsorption of  $\text{NO}_2$  on wet Ba-Y is displayed in Figure 6. Upon  $\text{H}_2\text{O}$  adsorption on the dry Ba-Y, the  $\delta_{\text{HOH}}$  and  $\nu_{\text{OH}}$  vibrations of adsorbed water are seen at  $1640\text{ cm}^{-1}$  and in the  $3000\text{--}3750\text{ cm}^{-1}$  region, respectively. The addition of a small amount  $\text{NO}_2$  results in the appearance of the split nitrate band in the  $1300\text{--}1500\text{ cm}^{-1}$  range and the development of a new  $\nu_{\text{OH}}$  band at  $3620\text{ cm}^{-1}$ . In contrast to the  $\text{NO}_2$  adsorption on dry Ba-Y, no IR features of adsorbed  $\text{NO}^+$  are seen at low  $\text{NO}_2$  pressures. With increasing  $\text{NO}_2$  doses, the intensities of the nitrate features increase while that of the adsorbed water decrease. At high  $\text{NO}_2$  pressures (in the presence of gas-phase  $\text{NO}_2$  in the IR cell), bands representing  $\text{NO}^+$  and  $\text{NO}^+\text{NO}_2$  are visible. It is possible that these latter species are formed on the adsorption sites that were not occupied by water



**Figure 6.** FTIR spectra of  $\text{NO}_2$  adsorption on  $[\text{H}_2\text{O}]_{\text{ads}}\text{-Ba-Y}$  at 295 K. Doses ( $\mu\text{mol}$ ):  $\text{H}_2\text{O}$ : 16.6 (a),  $\text{NO}_2$ : 2.91 (b), 5.48 (c), 9.55 (d), 17.8 (e), 32.8 (f), and 112 (g).

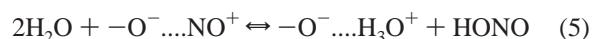
because of the initial low water dose used in the experiment or on the protonic sites of the zeolite. However, it is evident that on both Na- and Ba-Y the presence of water definitely inhibits the formation of  $\text{NO}^+$  species, while  $\text{NO}_3^-$  and  $\text{NO}_2^-$  species are readily formed. Since there is a competition between  $\text{NO}_2$  and  $\text{H}_2\text{O}$  for the same adsorption sites<sup>19</sup> (charge-compensating cations), at small  $\text{NO}_2$  doses  $\text{NO}_2$  cannot directly interact with the  $\text{Na}^+$  or  $\text{Ba}^{2+}$  ions but rather with the  $\text{H}_2\text{O}$  molecules strongly adsorbed onto these cations. At higher  $\text{NO}_2$  pressures, because of the adsorption/desorption equilibrium between  $\text{H}_2\text{O}$  and  $\text{NO}_2$ , some  $\text{H}_2\text{O}$ -free adsorption sites can open up where  $\text{NO}_2$  can adsorb as  $\text{NO}^+$ . However, at these elevated  $\text{NO}_2$  pressures,  $\text{NO}^+$  immediately interacts with  $\text{NO}_2$  and forms the  $\text{NO}^+\text{NO}_2$  adducts.

In the reverse experiment, the zeolite samples were first saturated with  $\text{NO}_2$  and the weakly adsorbed species were removed by evacuation at room temperature (see Figure 2). Then  $\text{H}_2\text{O}$  was adsorbed onto the thus prepared samples and IR spectra were recorded as the amount of  $\text{H}_2\text{O}$  dosed was increased. The results of these experiments are shown in Figures 7 and 8 for Na- and Ba-Y, respectively. As we have mentioned previously, only  $\text{NO}^+$  and nitrate species are present on dry Na-Y zeolite after  $\text{NO}_2$  adsorption. On the other hand, on the Ba-Y both  $\text{NO}^+$  and a  $\text{NO}^+\text{NO}_2$  adduct are present at room temperature. Addition of water brings about significant changes in the IR spectra of these  $\text{NO}_2$ -saturated catalysts. After the first small

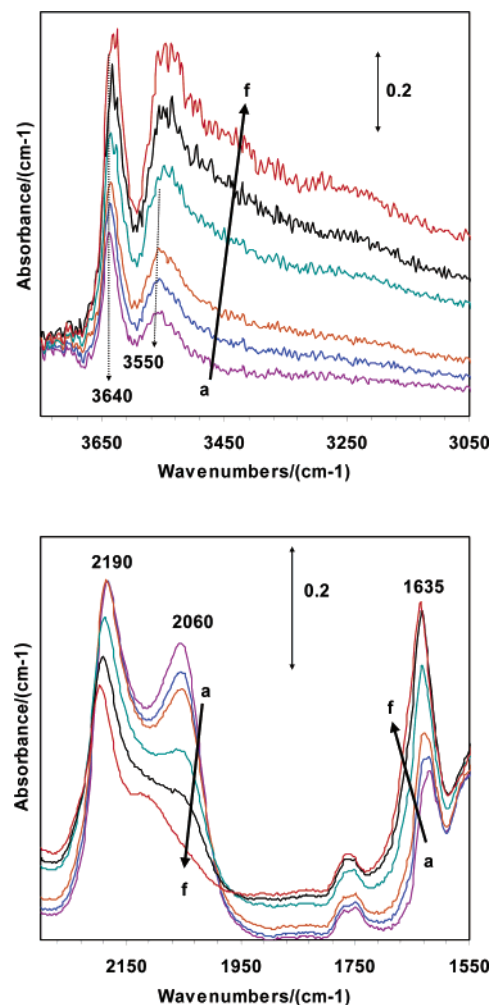


**Figure 7.** FTIR spectra of water adsorption on [NO<sub>2</sub>]<sub>ads</sub>-Na-Y at 295 K. The catalyst was evacuated for 60 min after NO<sub>2</sub> adsorption (a), and then water was dosed ( $\mu$ mol): 1.10 (b), 2.74 (c), 4.63 (d), 7.23 (e), and 10.6 (f).

water dose, the  $\delta_{\text{HOH}}$  mode of adsorbed water appears at 1640  $\text{cm}^{-1}$ , the intensities of the  $\nu_{\text{OH}}$  vibrations of Brønsted acidic OH groups (3640 and 3550  $\text{cm}^{-1}$ ) increase, the  $\nu_{\text{NO}}$  of NO<sub>2</sub><sup>-</sup> (1270  $\text{cm}^{-1}$ ) develops, while the intensities of the NO<sup>+</sup> features (2020 and 2114  $\text{cm}^{-1}$ ) decrease. With the increase in the amount of water dosed, the features of adsorbed H<sub>2</sub>O and NO<sub>2</sub><sup>-</sup> increase gradually, while those of NO<sup>+</sup> decrease and ultimately completely disappear at the highest water dose applied. Similar trends are seen for water adsorption on the NO<sub>2</sub> saturated Ba-Y sample displayed in Figure 8. The intensity of the IR band of adsorbed NO<sup>+</sup> species (2053  $\text{cm}^{-1}$ ) decreases as water is added to the system and disappears at higher water dosages. Strikingly, there is no change in the intensity of the IR band we have assigned to the NO<sup>+</sup>NO<sub>2</sub> adduct. This is somewhat surprising, since this is the species that is removed first upon annealing the NO<sub>2</sub>-saturated sample. This observation can be rationalized by assuming that the NO<sub>2</sub> in the NO<sup>+</sup>NO<sub>2</sub> adduct interacts fairly strongly with NO<sup>+</sup> thus protecting it from the reaction with water. On the other hand, NO<sup>+</sup> species (just like in the Na-Y case) are susceptible to an attack by the incoming water molecules and this reaction can form HONO and acid sites:



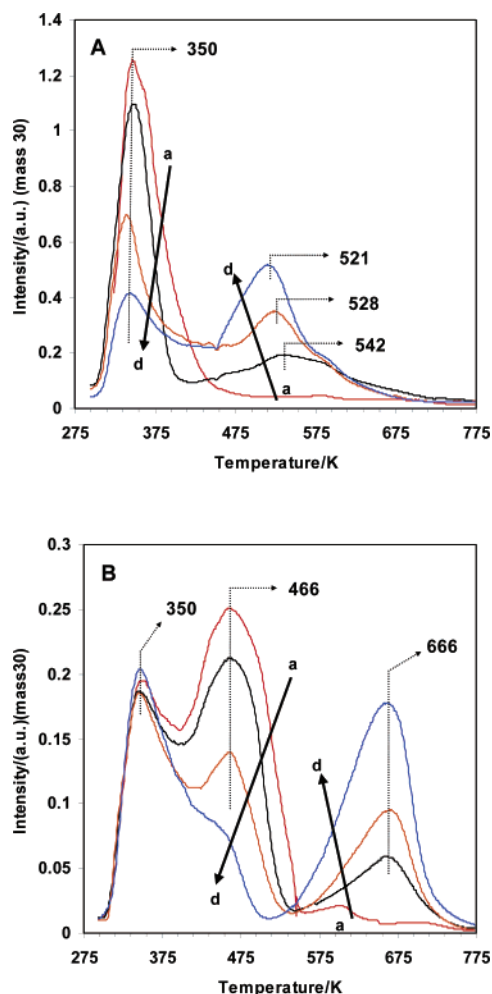
The effect of water on the NO<sub>2</sub> TPD in Na- and Ba-Y is shown in Figure 9. The activated (dry) zeolite samples were



**Figure 8.** FTIR spectra of water adsorption on [NO<sub>2</sub>]<sub>ads</sub>-Ba-Y at 295 K. The catalyst was evacuated for 120 min after NO<sub>2</sub> adsorption (a), and then water was dosed ( $\mu$ mol): 1.08 (b), 1.96 (c), 3.62 (d), 5.50 (e), and 9.65 (f).

contacted with a certain amount of water, then NO<sub>2</sub> was added to the “wet” samples, followed by evacuation and finally TPD. The amount of water added was varied, while that of NO<sub>2</sub> was kept constant at a level that is sufficient for full saturation determined from adsorption experiments. Preadsorbed water significantly altered the NO<sub>2</sub> desorption profiles on both catalysts studied. Over Na-Y (panel A), a high-temperature desorption peak appeared at 520 K in the NO<sub>2</sub> TPD spectrum when the sample was preexposed to a small amount of water prior to saturation NO<sub>2</sub> adsorption. At the same time, the low-temperature desorption feature lost some of its intensity. Increasing the amount of water added onto the activated sample, but keeping the NO<sub>2</sub> dose constant, results in the increase of the high-temperature desorption peak intensity and the decrease in the low-temperature one. There is an interconversion between these two desorption features, that is, as the intensity of the low-temperature desorption feature decreases, that of the high-temperature one increases. At the highest water dose studied, the intensity of the high-temperature desorption feature is higher than that of the low-temperature one. These changes in the NO<sub>2</sub> TPD profile of Na-Y as a consequence of water preadsorption correlate well with the results of the FTIR experiments. These results underscore the relationship between the 2020  $\text{cm}^{-1}$  IR feature and the NO<sub>2</sub> desorption feature at 352 K. On the dry Na-Y at room temperature, only the IR absorption features of adsorbed NO<sup>+</sup> and NO<sub>3</sub><sup>-</sup> are seen on the evacuated, NO<sub>2</sub>-





**Figure 9.** The effect of water on the TPD spectra of adsorbed  $\text{NO}_2$  on Na- (A) and Ba-Y (B). The catalysts were first exposed to  $\text{H}_2\text{O}$  and then saturated with  $\text{NO}_2$ .  $\text{H}_2\text{O}$  doses ( $\mu\text{mol}$ ): 0 (a), 90.6 (b), 227 (c), and 907 (d) (Weight of catalyst: 0.025 g; heating rate: 5 K/min.)

saturated sample. These species, formed through reaction 1, can recombine and desorb as  $\text{NO}_2$  upon heating the sample, resulting in the disappearance of the  $2020\text{ cm}^{-1}$  IR band and the evolution of the TPD feature at 352 K. On the other hand, when water is added either prior to or following  $\text{NO}_2$  adsorption, the  $2020\text{ cm}^{-1}$  IR feature of adsorbed  $\text{NO}^+$  is absent and only the signatures of  $\text{NO}_3^-$  and  $\text{NO}_2^-$  are present. These species are stable on the wet Na-Y sample, and upon heating they desorb as  $\text{NO}_2$  at a higher temperature of  $\sim 505\text{ K}$ . The high-temperature  $\text{NO}_2$  desorption peak is always accompanied by the desorption of water (not shown here), which strongly suggests that  $\text{NO}_2$  is formed in the reverse of reaction 4.

The effect of water on the  $\text{NO}_2$  TPD of Ba-Y is shown in panel B of Figure 9. The high-temperature ( $\sim 470\text{ K}$ ) desorption feature shifts upward to  $\sim 660\text{ K}$ . Strikingly, both the intensity and the position of the low-temperature desorption peak stay practically unchanged. Similarly to the Na-Y case, the inter-conversion between the two high-temperature  $\text{NO}_2$  desorption features, as a result of adsorbed water, is apparent over Ba-Y. At the highest water dose studied, the high-temperature  $\text{NO}_2$  desorption feature of dry Ba-Y is completely absent, while the  $660\text{ K}$  desorption peak reaches its maximum intensity. Correlating the IR and TPD results again helps to explain the observed changes brought about by the coexistence of  $\text{H}_2\text{O}$  and  $\text{NO}_2$  on Ba-Y. Water addition onto the  $\text{NO}_2$ -saturated Ba-Y sample selectively eliminated the  $2050\text{ cm}^{-1}$  IR band assigned

to adsorbed  $\text{NO}^+$ . Meanwhile, the  $\text{NO}^+\text{NO}_2$  adduct was unaffected by preadsorbed  $\text{H}_2\text{O}$ . This somewhat surprising result can be explained by the high reactivity of the  $\text{NO}^+$  species. As water is added to the Ba-Y sample containing both  $\text{NO}^+$  and  $\text{NO}^+\text{NO}_2$  adducts, it can react with  $\text{NO}^+$  preferentially (and as it turns out exclusively) resulting in the decrease and the ultimate disappearance of the  $2050\text{ cm}^{-1}$  IR absorption feature. The  $\text{NO}^+$  in the  $\text{NO}^+\text{NO}_2$  adduct seems to be protected from reacting with water by its strong interaction with  $\text{NO}_2$ . As we have shown previously,  $\text{NO}^+\text{NO}_2$  adduct is much more stable over Ba-Y than on Na-Y. Simple room-temperature evacuation completely eliminates the IR feature of  $\text{NO}^+\text{NO}_2$  on Na-Y, while on Ba-Y this adduct decomposes at around  $350\text{ K}$ . This high stability of the  $\text{NO}^+\text{NO}_2$  adduct in Ba-Y is the reason for the lack of change observed in both the  $2185\text{ cm}^{-1}$  IR band and the low-temperature  $\text{NO}_2$  TPD feature.

The results presented here may help in understanding the significantly different catalytic activities of Na- and Ba-Y zeolites in the nonthermal plasma assisted selective catalytic reduction of  $\text{NO}_x$ . Under dry conditions,  $\text{NO}^+$  forms in both catalysts; however, its stability in the two materials is vastly different. The much higher stability of  $\text{NO}^+$  in Ba-Y translates to a higher concentration of this species at the temperature that the catalytic reaction of interest is run ( $\sim 475\text{ K}$ ). Because we suspect that this species is an important one in the overall  $\text{NO}_x$  reduction process, its presence in appreciable concentrations is desirable. Under practical conditions, however, water is always present in the exhaust gas mixture, significantly affecting both the nature and the concentration of adsorbed species present on the surface of the working catalyst. At  $475\text{ K}$  operating temperature under these high humidity conditions, zeolites contain appreciable amount of water in their channels. Just approaching it from the  $\text{NO}_2$  adsorption standpoint, we showed how significantly water affected both the nature and the quantity of adsorbed  $\text{NO}_x$  species. In Na-Y, water readily reduces the number of  $\text{NO}^+$  species even at room temperature. The quantity of  $\text{NO}^+$  species is also decreased by the presence of water in Ba-Y, but some  $\text{NO}^+\text{NO}_2$  species can form even in the presence of water and may play a role in the observed high activity of Ba-Y.

Here, we only discussed the effect of water on the  $\text{NO}_x$  adsorption over these catalysts. However, its influence on the adsorption and reactivity of other compounds present in the exhaust gas mixture (in particular partially oxidized hydrocarbons) is unquestionable. In fact, there are indications that water is advantageous in the catalytic process because of its role in suppressing the condensation reaction of acetaldehyde that could eventually lead to catalyst deactivation.<sup>20</sup>

## Conclusions

The interaction of  $\text{NO}_2$  with both Na- and Ba-Y, FAU zeolites resulted in the formation of the same type of ionic species. In the absence of adsorbed water,  $\text{NO}^+$  ions formed by the disproportionation of  $\text{NO}_2$  are adsorbed onto framework  $\text{O}^-$  sites associated with the charge-compensating cationic positions of the zeolite, while  $\text{NO}_3^-$  ions are bound to the charge-compensating cations. At high  $\text{NO}_2$  dosages,  $\text{NO}^+\text{NO}_2$  adducts can form on both catalysts. The thermal stabilities of these adsorbed  $\text{NO}_x$  species strongly depend on the nature of the charge-compensating cation. The adsorption of these species is much weaker over Na-Y as a large fraction of the  $\text{NO}^+$  and  $\text{NO}_3^-$  desorb even upon evacuation at  $295\text{ K}$ . On the other hand, all the adsorbed  $\text{NO}_x$  species are much more stable over Ba-Y, so much so, that even most of the  $\text{NO}^+\text{NO}_2$  species are

present on this catalyst following room temperature evacuation. The presence of water dramatically influences the adsorption of NO<sub>2</sub> on both materials, as it competes for the available adsorption sites and also reacts with some of the adsorbed NO<sub>x</sub> species. The number of adsorbed NO<sup>+</sup> species decrease with increasing amount of H<sub>2</sub>O added, and HNO<sub>x</sub> species are formed that by interacting with the charge-compensating cations form zeolitic -O-H groups and M<sup>n+</sup>(NO<sub>x</sub>)<sub>n</sub>. The NO<sub>2</sub> TPD feature in Na-Y shifts from 350 to 520 K, while on Ba-Y the corresponding TPD feature shifts from 470 to 670 K. The large differences presented here for the stabilities of adsorbed NO<sub>x</sub> species over these two catalysts seem to strongly correlate with their vastly different catalytic activities observed in the non-thermal plasma assisted NO<sub>x</sub> reduction.

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