



# Thermal fixation of sulfur dioxide

## as elemental sulfur or sulfate with sodium oxalate

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### Summary

In a new thermal reaction, gaseous  $\text{SO}_2$  is reduced to elemental  $\text{S}_8$  over powdered  $\text{Na}_2\text{C}_2\text{O}_4$  at  $370^\circ\text{C}$ . Mixtures of  $\text{SO}_2$  and dry air gave oxidation to sodium sulfate.

### Introduction

Sulfur dioxide is a troublesome pollutant arising from volcanic activity but also formed in many combustion processes. Human activities account for the release of as much as  $2 \times 10^8$  tonnes  $\text{y}^{-1}$ . This release contributes to acid precipitation and the consequent degradation of forest.  $\text{SO}_2$  decomposes thermally at very high temperatures, photochemically by irradiation with UV light, radiochemically by  $\gamma$ -rays, in electrical discharges and electrolytically.<sup>1</sup> In these reactions,  $\text{SO}_2$  is believed to react *via* reduction to  $\text{SO}_2^{\cdot-}$  and then  $\text{SO}$ . Since  $\text{SO}$  (detected spectroscopically) rapidly disproportionates to  $\text{S}_8$  and  $\text{SO}_2$ , the observed products are  $\text{S}_8$ ,  $\text{O}_2$  and  $\text{SO}_3$ .<sup>1</sup>

Large quantities of sulfur dioxide, emitted into the atmosphere by the combustion of fossil fuels and the smelting of sulfide ores,<sup>2</sup> become oxidized to sulfuric acid and contribute to acid rain. The average lifetime of sulfur dioxide in the atmosphere has been estimated to be in the range of 3–10 h.<sup>3a,b</sup> Measurements of the acidity of snow and rain have shown that in parts of the eastern US and western Europe precipitation has changed from a nearly neutral pH 200 years ago to pH 4–5 today;<sup>3a</sup> in extreme cases, (Scotland, 1974) the rain had a pH of 2.4, equivalent to the acidity of vinegar.<sup>3a</sup> Taller stacks have been constructed to relieve local pollution problems.<sup>3a</sup> However, this has turned local problems into regional ones.

Removal of  $\text{SO}_2$  from gas streams is possible by absorption of this acid gas by bases such as  $\text{NaOH}$ ,<sup>4c</sup> but the resulting sulfites are not innocuous because disposal is needed and inadvertent acid treatment releases the  $\text{SO}_2$  once again. Air oxidation of aqueous solutions of sulfites is possible and it has been extensively studied, but this adds a second step and the need for an external oxidant, a solvent and a catalyst.<sup>4d</sup> Methods for the recovery and removal of  $\text{SO}_2$  from effluent gases involve reduction to elemental sulfur.<sup>5</sup>

Allied Signal<sup>5</sup> commercialized a method for converting  $\text{SO}_2$  into  $\text{S}_8$  in 1970 as an emission control system for a Canadian sulfide ore roasting facility. It can be applied for gas streams containing 4–100%  $\text{SO}_2$ , and for concentrations below 4%, a preliminary concentrating process is combined. Although the whole process is complex and involves eleven different elements and compounds, the main reductant is methane. Other reduction processes for the reduction of  $\text{SO}_2$  to  $\text{S}_8$  involves the use of  $\text{H}_2\text{S}$  (Claus process) or  $\text{CO}$  (Bureau of Mines) as reducing agents.<sup>5</sup>

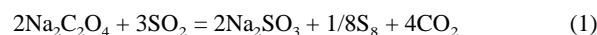
The oxidation of  $\text{SO}_2$  to  $\text{SO}_3$  is, by far, the most important reaction in the chemistry of the oxides of sulfur.<sup>2</sup> In the presence of Pt, the reaction begins at  $200^\circ\text{C}$ .<sup>6a</sup> In practical operations, the reaction is carried out at  $450^\circ\text{C}$  using Pt or  $\text{V}_2\text{O}_5$  as catalyst.  $\text{V}_2\text{O}_5$  is preferred as catalyst because it is cheaper than Pt and less susceptible to poisoning by selenium and arsenic.<sup>7</sup> A scheme has also been proposed<sup>8</sup> for the oxidation of  $\text{SO}_2$  to  $\text{SO}_3$ , with  $\text{V}_2\text{O}_5$  on silica as catalyst.

In this paper we describe a new and convenient thermal method for the reduction of  $\text{SO}_2$  to elemental  $\text{S}_8$ . When the reaction is used for the removal of  $\text{SO}_2$  from air mixtures, oxidation of  $\text{SO}_2$  to  $\text{Na}_2\text{SO}_4$  takes place instead.

### Results

We previously reported that powdered sodium oxalate at  $450$ – $460^\circ\text{C}$  is an efficient selective reducing agent for highly unreactive species such as fluorocarbons, converting perfluorodecalin to perfluoronaphthalene, for example.<sup>9</sup> The ready availability of the reagent ( $\$8/\text{kg}$  in bulk) permits the method to be considered for commercial application. We therefore examined it for the reduction of  $\text{SO}_2$ .

Passing  $\text{SO}_2$  over a packed bed of powdered  $\text{Na}_2\text{C}_2\text{O}_4$  at  $370^\circ\text{C}$  led to the production of elemental sulfur by reduction of  $\text{SO}_2$ . Not all the  $\text{SO}_2$  was destroyed in this one-pass apparatus, but in a multipass apparatus with trap-to-trap distillation using dry ice cooling of the sink trap, three passes were found to be sufficient to reduce the whole charge of  $\text{SO}_2$  (5.23 g, 81.7 mmol, 95%) according to the following equation.



The expected amount of sulfur was removed from the oxalate bed by extraction with  $\text{CS}_2$  to constant weight. The unreacted  $\text{Na}_2\text{C}_2\text{O}_4$  was determined by titration with  $\text{KMnO}_4$  solution and the  $\text{Na}_2\text{SO}_3$  product by titration with  $\text{NaI}_3$  solution. In the titration of  $\text{Na}_2\text{SO}_3$  with  $\text{I}_2$ ,  $\text{Na}_2\text{SO}_3$  is oxidized to  $\text{Na}_2\text{SO}_4$  and we also

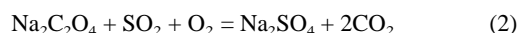
### Green Context

The conversion of sulfur dioxide from a pollutant into a useful raw material such as elemental sulfur or sulfate is a valuable achievement. This paper describes such conversions using reactants such as sodium oxalate. This is a new reaction—under non-aerobic conditions the product is sulfur, under oxidative conditions, sulfate is formed. DJM

determined the amount of  $\text{Na}_2\text{SO}_4$  formed by precipitation with  $\text{BaCl}_2$  and gravimetric determination of the resulting  $\text{BaSO}_4$ . We found that the moles of  $\text{Na}_2\text{SO}_3$  determined by titration and the  $\text{Na}_2\text{SO}_4$  determined gravimetrically were identical, indicating that no  $\text{Na}_2\text{SO}_4$  was formed when  $\text{SO}_2$  was passed through the oxalate bed. After the  $\text{SO}_2$  was consumed, the  $\text{CO}_2$  formed gave an acid soluble precipitate ( $\text{CaCO}_3$ ) from  $\text{Ca}(\text{OH})_2(\text{aq})$  but was not determined quantitatively.

To examine potential applications for removing  $\text{SO}_2$  from air, we moved to mixtures of  $\text{SO}_2$  and dry air and found that neither sulfite nor sulfur were now formed. Since these two species were found to be stable to air at the temperatures of the reaction, they are not being formed and then subsequently oxidized by air. Therefore, a different pathway must be involved.

A 1:1 (v/v)  $\text{SO}_2$ /dry air mixture was passed over powdered sodium oxalate in a single-pass reactor. The stoichiometry of eqn. (2) was determined for this new reaction as follows. The sulfate was determined gravimetrically with  $\text{BaCl}_2$ . Sodium sulfite was absent because the bed residue showed no reaction with aq.  $\text{NaI}_3$ . Finally, one mole of oxalate, determined by titration with  $\text{KMnO}_4$  of the oxalate remaining, was found to be consumed per mole of sulfate formed.



We have applied this reaction to the removal of  $\text{SO}_2$  from air mixtures using single pass and multiple pass apparatus. In the single pass apparatus, where excess air is present, we found that as the length of  $\text{Na}_2\text{C}_2\text{O}_4$  bed increases, so does the % $\text{SO}_2$  removed (Fig. 1). The percentage of  $\text{SO}_2$  removed was

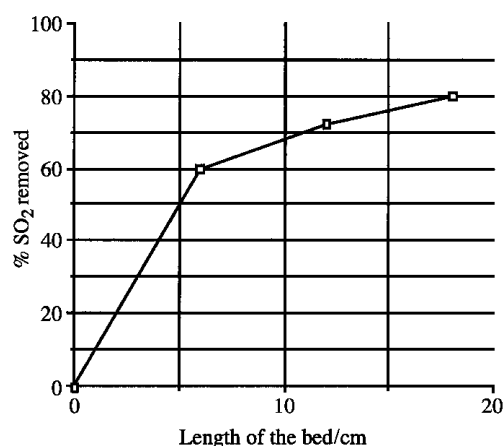


Fig. 1 Efficiency of  $\text{SO}_2$  removal versus bed length.

determined by measuring the different amounts of  $\text{SO}_2$  absorbed in a solution of  $\text{NaI}_3$  when identical gas flow was passed through a cold and a hot oxalate bed.

We have also used the trap to trap multipass apparatus in the presence of dry air by passing a 1:1 (v/v)  $\text{SO}_2$ /air mixture through the bed and condensing the unreacted  $\text{SO}_2$ . The condensed  $\text{SO}_2$  was passed back and forth from trap to trap in a stream of excess dry air until the reaction finished. By connecting the exit of the apparatus to a 0.05 M  $\text{NaI}_3$  solution, we were able to determine the amount of  $\text{SO}_2$  that escapes the apparatus because of imperfect cooling of the trap. We found that 89% of  $\text{SO}_2$  was retained in the bed as  $\text{Na}_2\text{SO}_4$  and ca. 10% escapes. There is no significant  $\text{SO}_2$  absorption in the cold bed.

Other substrates were not reduced under these conditions. For example,  $(\text{C}_6\text{H}_5)_3\text{PO}$ ,  $(\text{C}_6\text{H}_5)_3\text{P}(\text{O})$ ,  $(\text{CH}_3)_2\text{SO}_2$  and  $(\text{CH}_3)_2\text{SO}$

were unchanged when passed through the sodium oxalate bed at temperatures of 370 °C to 450 °C.

## Mechanism

The main point of this paper is to report the results, but some preliminary mechanistic discussion is presented here.

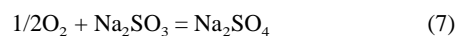
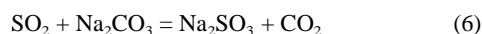
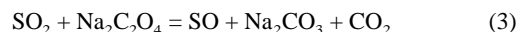
### Sulfur formation

A number of possible mechanisms might operate for the reduction of  $\text{SO}_2$  to  $\text{S}_8$ . The most plausible intermediates seem to be  $\text{SO}_2^{\cdot-}$  and then  $\text{SO}$ , as previously proposed.<sup>1</sup> The known disproportionation of  $\text{SO}$  to give  $\text{S}_8$  and  $\text{SO}_2$ , followed by absorption of the acidic  $\text{SO}_2$  by the basic  $\text{Na}_2\text{CO}_3$  formed on oxidation of oxalate, is expected to yield the other observed product  $\text{Na}_2\text{SO}_3$ .

### Sulfate formation

The  $\text{SO}_2$  oxidation with air raised the question whether  $\text{SO}_2$  or  $\text{O}_2$  or even  $\text{CO}_2$  (300 ppm in air) was reacting with oxalate. Passing pure dry air over the oxalate bed at the reaction temperature produced no change in the bed instead of the oxidation of the oxalate to  $\text{Na}_2\text{CO}_3$  that we had originally expected, so neither  $\text{CO}_2$  nor  $\text{O}_2$  react directly. Other work<sup>9b</sup> shows that even pure  $\text{CO}_2$  does not react with hot sodium oxalate. It might seem remarkable that a reagent that reduces such inert substrates as perfluorocarbons and even CFCs<sup>10</sup> fails to react with  $\text{O}_2$ , but an important caveat is that the temperature used here (370 °C) is far lower than in the fluorocarbon work (465 °C) and mechanistic work on the fluorocarbon reaction shows that incipient decomposition of the oxalate to carbon is required for reaction with the fluorocarbons. Given that  $\text{O}_2$  does not react with the oxalate, the most likely possibility is that  $\text{O}_2$  intercepts a reduction product from the  $\text{SO}_2$ . The three most plausible candidates are the 1-, 2- and 4-electron reduction products of  $\text{SO}_2$ :  $\text{SO}_2^{\cdot-}$ ,  $\text{SO}$  and  $\text{S}$  atoms.

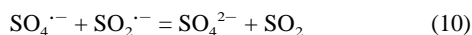
Eqn. (3)–(7) illustrate a proposed mechanism *via*  $\text{SO}$  as intermediate. Sulfur monoxide, which can be formed when  $\text{SO}_2$  is reduced with sulfur vapor in a glow discharge,<sup>6b</sup> has been considered as an intermediate in other reduction reactions of  $\text{SO}_2$  to  $\text{S}_8$ .<sup>6</sup> Since it is unstable at all temperatures it disproportionates into  $\text{S}_8$  and  $\text{SO}_2$ . However  $\text{S}$  atoms readily react with oxygen to give  $\text{SO}_2$ .<sup>11</sup> Another difficulty with this mechanism is that the oxygen atom removed from the  $\text{SO}_2$  by sodium oxalate to generate  $\text{SO}$ , would be expected to initially appear in the product in the form of  $\text{Na}_2\text{CO}_3$  as shown in eqn. (3). In the presence of  $\text{SO}_2$  this carbonate would be converted to  $\text{Na}_2\text{SO}_3$ . For the observed product to be  $\text{Na}_2\text{SO}_4$ , the initially formed  $\text{Na}_2\text{SO}_3$  would have to be oxidized by air. We find, however, that  $\text{Na}_2\text{SO}_3$  is stable to dry air under our reaction conditions. Therefore a mechanism involving  $\text{SO}$  and  $\text{S}$  atoms as intermediates seems unlikely.



This made us suspect that the radical<sup>12</sup>  $\text{SO}_2^{\cdot-}$  was the more likely intermediate that reacts with  $\text{O}_2$ . Its formation would involve a single electron transfer (SET) from the surface of the crystal. A SET mechanism is also consistent with our earlier observation<sup>9</sup> that  $\text{Cl}_3\text{C}-\text{CCl}_3$  is formed when  $\text{CCl}_4$  is passed over

$\text{Na}_2\text{C}_2\text{O}_4$  at a similar temperature (320 °C), since this product is most easily rationalized by recombination of two  $\text{CCl}_3^\cdot$  radicals formed by SET to  $\text{CCl}_4$ . Of course,  $\text{CCl}_4$  is a different class of substrate, so this may not be relevant.

The  $\text{SO}_2^{\cdot-}$  radical was previously observed in dithionite solutions by electron paramagnetic resonance.<sup>13</sup> Prior mechanistic studies<sup>14</sup> suggest that air oxidation of dithionite solutions to  $\text{SO}_4^{2-}$  goes *via* the pathway of eqn. (8)–(10).



Our data are consistent with a similar mechanism operating in the sodium oxalate reaction. If so, it is an unusual case of an  $\text{O}_2$  oxidation where the substrate and not  $\text{O}_2$  is reductively activated.

## Conclusions

In this paper, we describe a simple thermal method for the reduction of  $\text{SO}_2$  to  $\text{S}_8$  using hot sodium oxalate. When the reaction was used for the removal of  $\text{SO}_2$  from air mixtures, we found that oxidation of  $\text{SO}_2$  to  $\text{Na}_2\text{SO}_4$  took place instead of reduction to  $\text{S}_8$ . A mechanism is discussed.

## Experimental

### Reduction of sulfur dioxide

#### Trap to trap multipass (TM) or single pass (SP) experiment

The apparatus, consisting of a glass tube wrapped with a heating tape, was connected either to a pair of cold traps on each end (TM) or to the gas source *via* a flow meter (SP) and loaded with powdered sodium oxalate (40.0 g, 298.5 mmol). The substrate was passed (70 mL  $\text{min}^{-1}$  for 2.5 h) through the heated (370 °C) oxalate bed (SP) or passed through the oxalate bed (70 mL  $\text{min}^{-1}$  for 2.5 h) and condensed in the trap (TM) and subsequently passed from trap to trap by heating the source trap and cooling the sink trap (acetone/dry ice,  $-78^\circ\text{C}$ ).

The unreacted sodium oxalate was determined by titration with 0.15 M  $\text{KMnO}_4$ . Sulfur (0.85 g, 26.56 mmol) was isolated from the bed by extraction with carbon disulfide to constant weight. Sodium sulfite (6.69 g, 51.08 mmol) was also found in the bed which was determined by titration with 0.2 M  $\text{NaI}_3$  solution and the sodium sulfate thus formed was determined gravimetrically using  $\text{BaCl}_2$ . Only three passes were required to convert the full sample (5.23 g, 81.72 mmol, 95%) into sulfur and sodium sulfite.

#### Attempted reaction with oxygen

A flow of  $\text{O}_2$  (33.3 mL  $\text{h}^{-1}$ ) was passed through a  $\text{Na}_2\text{C}_2\text{O}_4$  bed (40.0 g, 298.5 mmol) at 370 °C. After 3 h flow, the  $\text{Na}_2\text{C}_2\text{O}_4$  in the bed was determined by titration with 0.15 M  $\text{KMnO}_4$  solution showing that no reaction had occurred. We repeated this experiment, but after 3 h, the  $\text{O}_2$  flow was closed and a flow of  $\text{SO}_2$  (10 mL  $\text{min}^{-1}$ ) was passed through the bed. After a few minutes, condensation of  $\text{S}_8$  was observed in the air cooled condenser placed at the exit of the bed. This indicates, that at the temperature of eqn. (3),  $\text{SO}_2$  was reduced to  $\text{S}_8$ , while  $\text{O}_2$  did not react with the bed.

#### Reaction with sulfur dioxide and dry air

##### Single pass (SP) experiment

Sodium oxalate (40.4 g, 301.9 mmol) was placed in the reactor and a 1:1 mixture of  $\text{SO}_2$  (flow: 14.0 mL  $\text{min}^{-1}$ ) and dry air was passed through the hot bed (370 °C) for 10 h. The solid mixture

in the bed was dissolved in water and the unreacted sodium oxalate (19.26 g, 143.73 mmol) was determined by titration with 0.15 M  $\text{KMnO}_4$  solution. The solution failed to react with an aqueous solution of  $\text{NaI}_3$ , indicating the absence of sodium sulfite. However,  $\text{Na}_2\text{SO}_4$  (22.4 g, 158.0 mmol) was found in the bed as determined gravimetrically with  $\text{BaCl}_2$ . We found that one mole of sodium oxalate (21.2 g, 158.0 mmol) was consumed per mole of  $\text{Na}_2\text{SO}_4$  (22.4 g, 158.0 mmol) formed.

### Removal of sulfur dioxide from air

#### Single pass experiment

A stream of dry air (flow 13.7 mL  $\text{min}^{-1}$ ) was passed through a dilute solution of  $\text{Na}_2\text{SO}_3$  (0.05 M) which was acidified with an excess of  $\text{HCl}$  (10 mL  $\text{HCl}_{(\text{c})}$ ). The gas stream was then passed through the hot  $\text{Na}_2\text{C}_2\text{O}_4$  cylindrical bed (40.0 g, 0.30 mol per bed) with the following dimensions: 6.0 cm and 1.7 cm. The removing efficiency increases with the retention time of  $\text{SO}_2$  in the bed (number of beds used). We measured the results for one, two and three beds. The percentage of  $\text{SO}_2$  removed was calculated by running identical experiments with cold  $\text{Na}_2\text{C}_2\text{O}_4$  bed(s). The  $\text{SO}_2$  unretained in the bed was trapped in 500 mL solution of  $\text{NaI}_3$  (0.05 M), reacted with a known amount of  $\text{Na}_2\text{SO}_3$  and titrated by return with  $\text{NaI}_3$ . The data obtained are reported in Table 1. The average concentration of  $\text{SO}_2$  in the stream was in the range 1.5–3.0% v/v as determined by measuring the volume of air and the absorbed  $\text{SO}_2$  in a 0.2 M  $\text{NaI}_3$  solution.

**Table 1** Removal of  $\text{SO}_2$  from air

Number of beds	Length of the bed/cm	% $\text{SO}_2$ removed
1	6	60
2	12	72
3	18	80

#### Trap to trap multipass experiment in the presence of air

The apparatus, consisting of a glass tube wrapped with a heating tape, was connected to a pair of cold traps on each end (TM) loaded with powdered sodium oxalate (40.0 g, 298.5 mmol). A mixture of 1:1  $\text{SO}_2$ /dry air was passed (30 mL  $\text{min}^{-1}$  for 3.5 h) through the heated (370 °C) oxalate bed. The unreacted  $\text{SO}_2$  was condensed in the trap (TM) and subsequently passed from trap to trap in a stream of dry air by heating the source trap and cooling the sink trap (acetone/dry ice,  $-78^\circ\text{C}$ ). The exit of the apparatus was connected to a trap containing 500 mL 0.05 M  $\text{NaI}_3$  in order to capture the  $\text{SO}_2$  that escapes from the trap due to imperfect cooling (0.30 g, 4.68 mmol). Unreacted sodium oxalate was determined by titration with 0.15 M  $\text{KMnO}_4$  and the  $\text{Na}_2\text{SO}_4$  (5.55 g, 39.1 mmol) gravimetrically determined by precipitation with  $\text{BaCl}_2$ , showing that 89% of the  $\text{SO}_2$  (2.5 g, 39.1 mmol) was retained in the bed.

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