

# Vanadium-Node-Functionalized UiO-66: A Thermally Stable MOF-Supported Catalyst for the Gas-Phase Oxidative Dehydrogenation of Cyclohexene

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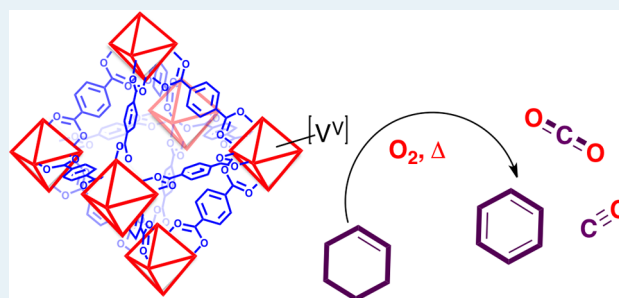
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## S Supporting Information

**ABSTRACT:** The OH groups on the Zr-based nodes of ultrastable UiO-66 can be metallated with V<sup>V</sup> ions in a facile fashion to give the derivative VUiO-66. This metallated MOF exhibits high stability over a broad temperature range and displays high selectivity for benzene under low-conversion conditions in the vapor-phase oxidative dehydrogenation of cyclohexene (activation energy ~110 kJ/mol). The integrity of the MOF is maintained after catalysis as determined by PXRD, ICP-AES, and SEM.

**KEYWORDS:** metal–organic framework, gas-phase catalysis, cyclohexene oxidation, UiO-66, vanadium



Although metal–organic frameworks (MOFs),<sup>1–3</sup> a crystalline and porous class of materials, have been extensively used as catalysts or catalyst supports<sup>4–11</sup> in solution phase, their usage in gas- and vapor-phase catalysis has been rare<sup>12–24</sup> and limited thus far, with the majority of reported examples focused on the oxidation of CO to CO<sub>2</sub>. Nonetheless, MOFs possess many desirable properties that make them highly attractive as gas-phase catalysts: (1) Their intrinsic crystallinity allows for the design and deployment of single-site, and uniformly dispersed catalytic species, yielding catalysts with excellent selectivity. (2) Their high surface areas—in comparison with zeolites, metal oxide supports, and other porous materials—can engender a very high density of catalytic sites, enabling higher chances of contact with substrates. (3) Their tailorable porosity can provide a special cavity environment for substrates to interact with catalytically active sites, similar conceptually to the secondary interaction spheres of enzyme active sites, which can further enhance activity and selectivity.

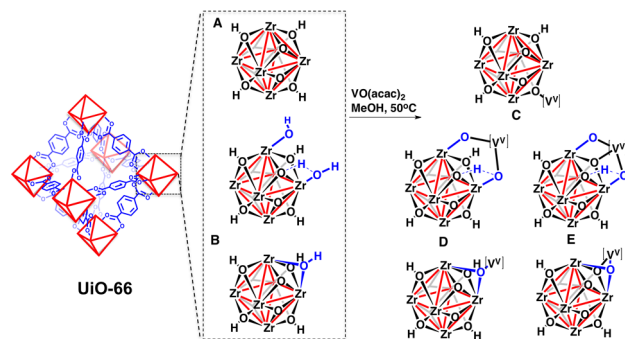
For a MOF to be broadly used as a catalyst for gas-phase reactions, it must have high thermal stability, good structural stability to activation, and excellent mechanical robustness. Given the high temperatures (>200 °C) that are typically required for gas-phase catalysis, the relatively low thermal stability of many early MOFs was often thought as a major obstacle to their realization as viable heterogeneous catalysts in industrially valuable processes. Although there were relatively few MOFs capable of withstanding such high temperatures for prolonged periods without physical or chemical degradation,<sup>25</sup>

recent synthetic progresses have yielded many frameworks that are remarkably stable to high temperatures. Such enhanced thermal stability of the frameworks, and therefore of the catalytically active species that they support, are critical for the exploration of MOFs as heterogeneous catalysts and catalyst supports. Herein, we report the functionalization of the hydroxyl-presenting nodes of UiO-66 with V<sup>V</sup> ions, which constitutes a highly stable MOF-supported catalyst for the gas-phase oxidation of cyclohexene. This metallated MOF exhibits high stability over a broad temperature range and shows high catalytic selectivity for benzene formation under low-conversion conditions. Our work illustrates that MOF platforms with high thermal stability can, indeed, be used as catalysts and catalyst supports for high-temperature gas-phase chemical transformations.

As the ideal MOF support platform, we selected the Zr-based UiO-66 framework,<sup>26</sup> a MOF known to have exceptional thermal and mechanical stability. UiO-66 is composed of 12-coordinate Zr(O)<sub>4</sub>(OH)<sub>4</sub> nodes, each linked to 12 carboxylates of terephthalate ligands to form super tetrahedral and super octahedral cages (Scheme 1) with apertures of approximately 6 Å. It has been reported to be stable to up to ~540 °C, based on thermogravimetric analysis, and up to ~375 °C, based on

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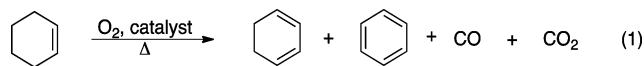
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Scheme 1. Metallation of UiO-66 with  $\text{O}=\text{V}(\text{acac})_2$ <sup>a</sup>

<sup>a</sup>Left: Structure of UiO-66 and its proposed idealized (A) and defective (B) hydroxyl-presenting nodes. Right: Proposed possible products C–E. <sup>b</sup>For presentation clarity, the central clusters in structures A–E are drawn without charge-compensating ligands.

temperature-programmed PXRD.<sup>27</sup> It is also stable to water and many organic solvents.<sup>26</sup> Additionally, it can withstand high pressure without mechanical degradation,<sup>28</sup> making it highly attractive as a support in fixed-bed flow reactors for gas-phase reactions.<sup>29</sup>

As a model reaction for testing UiO-66-based catalysts, we selected the gas-phase oxidative dehydrogenation of cyclohexene into benzene (eq 1). This transformation is of potential



interest in benzene purification because cyclohexene is a persistent impurity in large-scale benzene production (~20 M tons/yr globally).<sup>30</sup> The possibility for this reaction to yield several different products in the presence of oxygen additionally serves as a convenient probe for catalyst activity/selectivity evaluation. We note that although cyclohexene is typically a liquid at ambient temperature and pressure, the vapor-phase oxidative dehydrogenation of cyclohexene has been reported.<sup>30–32</sup> Given that the  $\text{Zr}^{\text{IV}}$  ions in the node of UiO-66 have minimal activity in oxidation catalysis,<sup>33</sup> we chose to incorporate redox-active  $\text{V}^{\text{V}}$  ions via reaction with the available  $-\text{OH}$  groups of the nodes. We note that Laribi et al. have demonstrated that the  $-\text{OH}$  groups on the Zr node of UiO-67, an analogue of UiO-66, can react with and immobilize  $\text{Mg}^{\text{II}}$  ions as well as  $\text{Au}^{\text{I}}$  phosphine species.<sup>34</sup> More recently, the  $-\text{OH}$  groups on the node of the Zr-based clusters in the NU-1000 MOF platform have also been metallated with  $\text{Zn}^{\text{II}}$  and  $\text{Al}^{\text{III}}$  using atomic layer deposition.<sup>35</sup>

By metallating the  $-\text{OH}$  groups on the nodes of UiO-66 with  $\text{V}^{\text{V}}$  ions, we were encouraged by previous reports of supported vanadium oxides being capable of catalyzing the oxidative dehydrogenation of propane,<sup>36–38</sup> *n*-butane,<sup>39–41</sup> and cyclohexane.<sup>42</sup> We envisioned the node of UiO-66 to behave as a discrete solid-support-like “ligand” for the  $\text{V}^{\text{V}}$  center, but with a more well-defined display of OH groups that affords only one type of catalytic species (Scheme 1, structures A and C), as opposed to the many species that may be present in conventional vanadium oxide-supported heterogeneous catalysts.<sup>43</sup> However, we note that UiO-66 has been reported to have missing linkers, possibly exposing additional  $-\text{OH}$  groups<sup>44</sup> that could participate in metal-binding (Scheme 1, structure B). Although there have been examples of MOF-

based gas-phase catalysis with active sites present at the node,<sup>15,20–22</sup> on ligands,<sup>12,13</sup> or being encapsulated in the MOF pores<sup>16,17</sup> (including a recent report on the use of Au nanoparticle@UiO-66 for CO oxidation<sup>24</sup>), our work represents one of a very few examples of a node-supported active metal species.

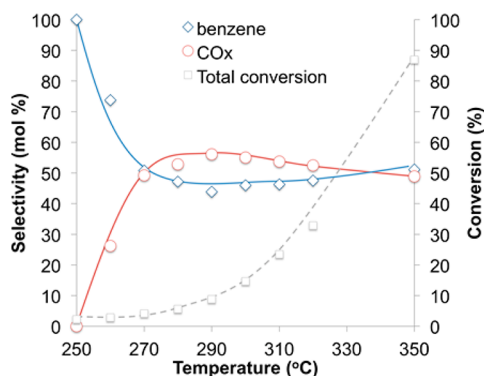
Microcrystalline samples of UiO-66, a white powder comprising octahedral particles of  $\sim 0.5\text{--}1\ \mu\text{m}$ , was synthesized using a slight modification of a reported procedure that employs acetic acid as a modulator.<sup>45</sup> Its PXRD pattern agreed well with the simulated pattern, and its BET surface area ( $\sim 1240 \pm 120\ \text{m}^2/\text{g}$ ) matched the reported values (Figures S1–S3 in the Supporting Information (SI)). TGA (Figure S4 in the SI) and micropore volume ( $0.47\ \text{cm}^3/\text{g}$ ) analyses of the MOF suggested  $\sim 0.6/12$  of the 1,4-benzenedicarboxylate (BDC) linkers are missing.<sup>46</sup> (This is the equivalence of 5% of the sites that can be occupied by the ditopic linkers or  $\sim 9.5\%$  of the sites that can be occupied by a monotopic modulator/ligand). The NMR spectrum in  $\text{DMSO}-d_6$  (Figure S14 in the SI) of  $\text{D}_2\text{SO}_4$ -dissolved UiO-66 after activation showed a small amount of acetic acid ( $\sim 11.5\ \text{mol}\%$  of the total ligands), which presumably existed as acetate ions that cap the missing-linker sites after synthesis (see Figure S10 in the SI for supporting data).

The metallation of UiO-66 with vanadyl acetylacetonate ( $\sim 8\ \text{\AA}$  in size) was carried out in MeOH to afford VUiO-66 as an off-yellow powder with unchanged PXRD pattern and nearly unchanged BET surface area ( $1220 \pm 100\ \text{m}^2/\text{g}$ ,  $0.46\ \text{cm}^3/\text{g}$  micropore volume) (Figures S1–S3 in the SI). Inductively coupled plasma atomic-emission analysis (ICP–AES) indicated a V loading of  $\sim 0.10 \pm 0.01\ \text{V}/\text{Zr}$ . NMR analysis of the  $\text{D}_2\text{SO}_4$ -dissolved metallated MOF indicated that very little of the initially present acetic acid (acetate) remained and that the acac ligand was not present (Figures S14–S15 in the SI). Thus, we speculate that the V reagent has reacted with the  $-\text{OH}$  groups (shown in blue, Scheme 1, structure B) that were present at the missing-linker sites of the nodes. Presumably, these reactive and more-accessible groups could arise if the acetate caps in the as-synthesized materials were displaced by water during the metallation process (see Scheme 1, structures B and D for some possible binding modes and Figure S10 in the SI for supporting data). Indeed, when we attempted to remove the acetate capping by treating the as-synthesized UiO-66 with a DMF solution of diluted HCl, we observed the growth of additional peaks in its in situ DRIFTS spectrum that can be attributed to new  $-\text{OH}$  species (Figure S10 in the SI). In combination with the NMR analysis, these data strongly supported the hypothesis that the  $-\text{OH}$  groups at missing-linker sites could form and react with the  $\text{O}=\text{V}(\text{acac})_2$  reagent.

Although we cannot rule out the possibility that the bridging hydroxyl groups on the nodes of UiO-66 also reacted with  $\text{O}=\text{V}(\text{acac})_2$ , we suspect that the low reactivity of these groups<sup>34</sup> made them less likely to react before the  $-\text{OH}$  groups at missing-linker sites. In addition, the low density of metallation (a maximum 15% of bridging hydroxyl groups being metallated if there were no missing-linker sites) made it difficult to quantify, using DRIFTS,<sup>34</sup> the amount of bridging  $-\text{OH}$  groups that could compete for the available  $\text{O}=\text{V}(\text{acac})_2$ . Indeed, the DRIFTS spectra (Figure S9 in the SI) of activated samples of UiO-66, VUiO-66, and UiO-66 that have been capped with either acetate or benzoate (see Sections S2–S3 in the SI) all showed similarly sharp hydroxyl peaks  $\sim 3674\ \text{cm}^{-1}$ , attributable to the bridging  $-\text{OH}$  group on the node.<sup>34,47</sup>

The XPS spectrum of VUiO-66 showed a V 2p peak with binding energy of 517 eV, consistent with the value expected for  $V^V$  (Figure S11 in the SI). The visible-Raman spectrum of an as-prepared VUiO-66 sample does not show the signature band at  $993\text{ cm}^{-1}$  for the  $V=O$  moiety in  $V_2O_5$  (Figure S12 in the SI); neither does it show any band that can be attributed to a  $V=O$  species, presumably due to a combination of low V loading and the presence of adsorbed water.<sup>48</sup> Heating this sample to  $400\text{ }^\circ\text{C}$  also did not result in any  $V=O$  bands in the  $900\text{--}1050\text{ cm}^{-1}$  region. Although the UV-Raman spectrum of a VUiO-66 sample that has been heated to  $400\text{ }^\circ\text{C}$  showed the presence of  $V\text{--}O\text{--}Zr$  bond<sup>48,49</sup> as a broad hump at  $700\text{--}1018\text{ cm}^{-1}$  (Figure S12 in the SI), we were unable to get better-resolved spectra under the limited laser power and dehydrating conditions of our experiments, for which measurements can be carried out without completely destroying the MOF platform. However, analysis of the diffuse-reflectance UV-vis spectrum of VUiO-66 (Figure S13 in the SI) clearly revealed an edge energy of  $3.38\text{ eV}$  that is consistent with the presence of mostly monomeric  $VO_x$  species with a minor oligomeric component.<sup>50</sup> Together, these results agreed well with the presence of isolated  $V^V$  species expected from the immobilization of monomeric  $O=V(\text{acac})_2$  reagent onto  $\text{--OH}$  sites on the node of UiO-66.

Using  $O_2$  as the oxidant, the oxidative dehydrogenation of cyclohexene was carried out in a packed-bed flow reactor in the  $250\text{--}350\text{ }^\circ\text{C}$  range. At  $250\text{ }^\circ\text{C}$  and low-conversion conditions ( $<2\%$  conversion), VUiO-66 catalyzed the formation of benzene with 100% molar selectivity (Figure 1). However,

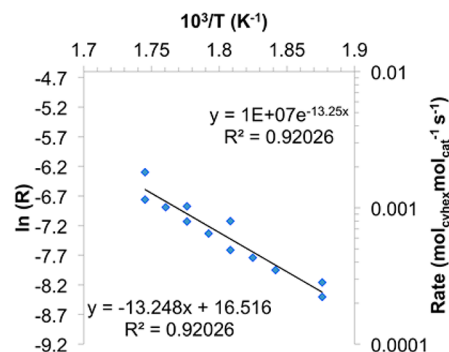


**Figure 1.** Selectivities (in mol %) for benzene (blue diamonds) and  $CO_x$  ( $CO + CO_2$ , red circles), and total conversion (%) as a function of temperature. The lines are provided only as visual guides. For individual plots of  $CO$  and  $CO_2$  selectivities, please see Figure S18 in the SI.

this molar selectivity quickly degraded (to  $\sim 83\text{ C\%}$  when corrected for the C stoichiometry; see Figure S19 in the SI) at slightly higher temperatures. Interestingly, this drop in selectivity leveled out above  $270\text{ }^\circ\text{C}$  with the majority of the byproducts ( $\sim 40\text{--}50\text{ mol \% CO}$  and  $CO_2$ , Figure 1;  $17\text{ C\%}$ ) attributable to combustion; only a very small amount ( $<1\text{ mol \%}$ , not shown) of cyclohexadiene, the incomplete dehydrogenation product, was observed. A control study of the oxidative dehydrogenation of cyclohexene using the unmetallated parent UiO-66 material showed only minor background reaction ( $<10\%$  conversion at  $350\text{ }^\circ\text{C}$ , Figure S20 in the SI), implying that the majority of the catalytic activity was from the supported vanadium species.

The oxidative dehydrogenation of cyclohexene on VUiO-66 exhibits Arrhenius-like behavior in the  $260\text{--}300\text{ }^\circ\text{C}$  temper-

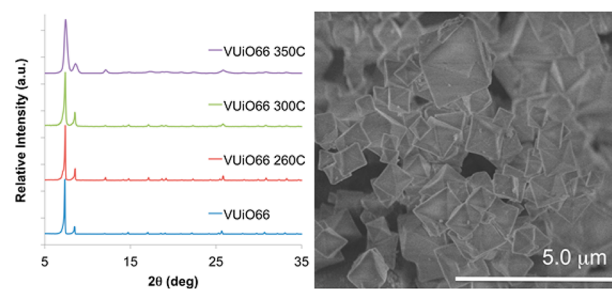
ature range, giving higher conversions at higher temperatures (Figure 2). In the presence of VUiO-66, the oxidative



**Figure 2.** Arrhenius plot for VUiO-66-catalyzed oxidation dehydrogenation of cyclohexene in the differential conversion regime ( $\sim 10\%$ ) and reaction-rate-limited temperature regime of  $260\text{--}300\text{ }^\circ\text{C}$  where mass-transfer limitations are absent. For consistency, turnover frequency (rate =  $R$ ) is calculated on the basis of the data obtained at  $t = 18\text{ h}$ .<sup>53</sup>

dehydrogenation of cyclohexene is calculated to have an activation energy of  $110 \pm 10\text{ kJ/mol}$  ( $26.3\text{ kcal/mol}$ ), which is comparable to reported values ( $16\text{--}24\text{ kcal/mol}$ ) determined by Rioux et al. for various sizes of Pt nanoparticles supported on SBA-15.<sup>32,51</sup> For comparison, VUiO-66 offers much better selectivity for benzene than the best ( $\sim 8\%$ ) of a series of Co clusters supported on metal oxides<sup>31</sup> and similar selectivity to  $VO_x$  on monolithic alumina.<sup>42</sup> However, it is less selective for benzene at high conversions compared with a recently reported  $Au\text{--}Pd/TiO_2$  catalyst ( $99\%$  selectivity at  $100\%$  conversion).<sup>30</sup>

The PXRD patterns of the VUiO-66 catalyst after 18 h catalytic runs at several temperatures (Figure 3, left panel) are



**Figure 3.** Left: PXRD patterns of UiO-66 and VUiO-66 after catalysis at  $260$ ,  $300$ , and  $350\text{ }^\circ\text{C}$ . Right: SEM image of VUiO-66 particles after catalyzing cyclohexene oxidative dehydrogenation at  $350\text{ }^\circ\text{C}$  for  $18\text{ h}$ .

identical to that of the as-synthesized material, indicating that the crystallinity of the V-functionalized MOF is retained even after prolonged heating at  $350\text{ }^\circ\text{C}$ . Notably, conversions remain at a stable, high level ( $\sim 85\%$ ), even after  $48\text{ h}$  on stream at  $350\text{ }^\circ\text{C}$  (Figure S24 in the SI).<sup>52</sup> ICP-AES analysis revealed that the V content ( $\sim 0.1\text{ V/Zr}$ ) remains the same after catalysis, indicating that there is no leaching of the active site. Consistent with all of these observations, the SEM image of VUiO-66 after catalysis at  $350\text{ }^\circ\text{C}$  also showed well-defined octahedral particles (Figure 3, right panel), further demonstrating the excellent robustness of the UiO-66 platform.

In summary, we have decorated the hydroxyl-presenting nodes of UiO-66 to form a robust VUiO-66 catalyst and demonstrated it to be active in the gas-phase oxidative



dehydrogenation of cyclohexene, selectively forming benzene at low conversion (100 mol % selectivity at 2% conversion). This selectivity remains at a good level (~80 mol % of cyclohexene is converted to benzene at moderate to high conversions), suggesting that the environment of the active catalyst remains unchanged across a broad range of temperatures and reaction conditions. Most notable is the observation that the MOF support maintains excellent structural integrity at temperatures as high as 350 °C, as determined by PXRD, ICP-AES analysis, and SEM imaging.

From a broader perspective, we envision the metallation of the nodes of highly stable MOFs to be a general strategy for the deployment of a broad range of other metal-ion-containing catalysts capable of effecting many important gas-phase reactions. We anticipate that UiO-66, and other emerging ultrastable MOFs<sup>35,54–57</sup> in which metal species can be easily incorporated, will open up new research directions and fulfill the potential of MOFs as a versatile and robust class of supports for heterogeneous gas-phase chemical reactions.

## ■ ASSOCIATED CONTENT

### ■ Supporting Information

Materials and methods; synthesis of UiO-66, capped-UiO-66, HCl-treated UiO-66, and VUiO-66; PXRD patterns, N<sub>2</sub> isotherms; TGA, XPS, Raman, DRIFTS, and catalysis data. This material is available free of charge via the Internet at <http://pubs.acs.org>.

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### Notes

The authors declare no competing financial interest.

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## ■ ABBREVIATIONS

MOF = metal–organic frameworks; BET = Brunauer–Emmett–Teller; TGA = thermogravimetric analysis; PXRD = powder X-ray diffraction; SEM = scanning electron microscopy; TOF-SIMS = time-of-flight secondary ion mass spectrometry

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- (53) As the reaction progresses, the MOF suffers from gradual deactivation that is most likely due to coking based on BET SA and TGA analyses (Figures S21–S23 in the SI), given that its structural integrity and metal loading is maintained (see discussion in the main text).
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