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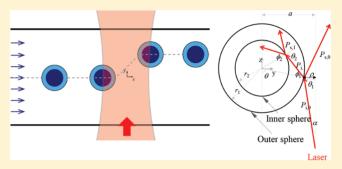
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# Behavior of Double Emulsions in a Cross-Type Optical Separation System

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ABSTRACT: The behavior of double emulsions in a cross-type optical particle separation system was studied for different combinations of refractive indices and different inner and outer layer radii. The radii and refractive indices of the double emulsions were easily adjusted by taking advantage of the coflowing geometry of a cross-type optical particle separation device. An analytical expression of the optical forces on a pair of concentric spheres was derived using the photon stream method in the ray optics regime. The predicted trajectories of the double emulsions by the optical force agreed well with the experimental data. This work has potential uses in cell



separation by morphometry, drug delivery vehicle, and emulsion-based biomedical applications.

#### 17 INTRODUCTION

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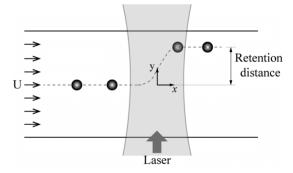
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18 Optical forces are used in a variety of fields. Their noninvasive 19 nature has been exploited in the manipulation and separation of 20 microscale biological samples, such as cells, proteins, and 21 biomolecules.<sup>3</sup> Optical beams can apply extremely small forces 22 (on the order of piconewtons)<sup>4</sup> and implement displacement 23 on the order of nanometers,<sup>5</sup> providing a useful tool for the 24 study of macromolecular interactions in soft condensed matter 25 physics. 6 As the need for optical forces has grown, a variety of 26 theoretical schemes have been developed to analyze and design 27 optical manipulators and separators. Among these, the ray 28 optics model is the most successful theoretical approach to 29 optical particle separation and is employed in optical 30 chromatography<sup>7,8</sup> and cross-type optical particle separation 31 devices. 9,10 The ray optics model describes the optical forces 32 that act on objects larger than the wavelength of the 33 illumination beam, which is common in optical particle 34 separation systems.<sup>1</sup>

Because optical chromatography and cross-type optical 36 particle separation use a loosely focused laser beam, the 37 techniques can separate many particles and prevent radiation-38 induced damage to a sample. Optical scattering forces act to 39 oppose the direction of fluid flow in optical chromatography, in 40 contrast with the optical scattering forces applied in cross-type 41 optical particle separation, which act perpendicular to the 42 direction of fluid flow. Figure 1 shows a schematic diagram of 43 the cross-type optical particle separation. Since size difference 44 and relative refractive index between particle and medium 45 adjust optical force on the particle, the optical force repels the 46 particle away from its origin position along the optical axis with 47 its own properties. The retention distance implies the lateral 48 distance caused by the optical scattering force when the laser is 49 illuminated perpendicular to the flow direction. 10,12 Since the 50 laser is illuminated perpendicular to the particle carrying fluid



**Figure 1.** Schematic diagram of the cross-type optical particle separation (COPS).

flow, particles can be continuously separated in a cross-type 51 optical particle separation system. 12 52

In the present study, the behavior of double emulsions in a 53 cross-type optical particle separation system was analyzed 54 theoretically and experimentally. A double emulsion shown in 55 Figure 2a was widely used as a microreactor for biochemical 56 f2 reactions, multicomponent microparticles for containing 57 polymerization processes, and encapsulation chambers for 58 drug delivery. Double emulsions can be also used as a 59 model of cells to approximate the nucleus and cytoplasm layers. 60 The trajectory of a pair of double emulsions moving in and out 61 of a laser beam was measured experimentally and predicted by 62 solving for the optical forces using a ray optics model and the 63 particle dynamic equations. The generation and measurement 64 of a double emulsion in a cross-type optical particle separation 65 system were conducted simultaneously. The refractive indices 66

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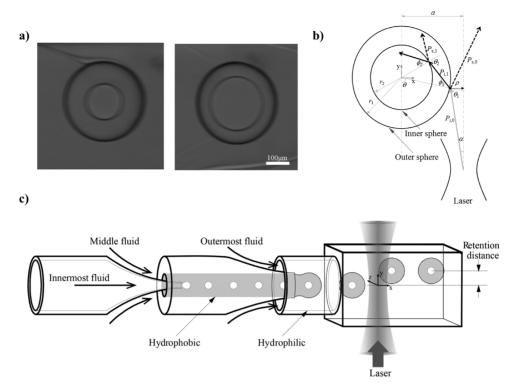


Figure 2. (a) Experimentally generated double emulsions. (b) Schematic diagram of the optical ray stream path. (c) Schematic diagram of the coflowing double emulsion generation device. The scale bar indicates  $100 \ \mu m$ .

67 and relative sizes of the inner and outer emulsions were found 68 to affect the optical force, and these effects were examined 69 closely as a function of the retention distance. The analytical 70 predictions qualitatively agreed well with the experimental 71 measurements. The present results can be applied to the sorting 72 and detection of cells by their morphological difference and 73 encapsulated drug delivery vehicles by their optical property 74 distribution of inner and outer layers.

#### 75 THEORY

The theoretical calculations using a ray optics model relied on a 77 reference frame in which concentric spheres flowed in a square 78 duct with a channel mean flow velocity  $\mathbf{U}$ , and a laser of 79 wavelength  $\lambda$  was illuminated vertically onto the sphere with 80 power P and a beam waist radius of  $\omega_0$ . The ratio of the outer 81 to inner radii was  $r_2/r_1$ , and each layer had a different refractive 82 index relative to that of the outermost fluid  $n_0$ . In the present 83 study, the photon stream method  $^{19,20}$  was used to formulate an 84 analytical expression for the optical force acting on a pair of 85 concentric spheres. To evaluate the optical force on the sphere, 86 we must determine the change in the momentum of the 87 photons. As shown in Figure 2b, the scattered momentum of 88 the photons  $\mathbf{p}_s$  can be expressed with the incident momentum 90 of the photons  $\mathbf{p}_s$  and a factor of conversion  $Q^9$ 

$$\mathbf{p}_{s} = Q \, \mathbf{p}_{i} \tag{1}$$

The optical force exerted on a sphere can be expressed from 91 eq 1 and Newton's second and third laws

$$d\mathbf{F} = -\frac{\Delta \mathbf{p}}{\Delta t} dA = -\frac{(\mathbf{p}_{s} - \mathbf{p}_{i})}{\Delta t} dA = \frac{\mathbf{p}_{i}(1 - Q)}{\Delta t} dA$$
 (2)

92 where dA is an infinitesimal area normal to the beam direction 93 and  $\Delta t$  is time. Since it is a loosely focused case, the incident

ray can be assumed parallel to the beam axis. Therefore, the  $_{94}$  conversion factor  $Q^{21}$  is

$$\begin{split} Q &= Q' \exp(\mathrm{i}\alpha) = \frac{Q_{\mathrm{N}}}{Q_{\mathrm{D}}} \\ Q_{\mathrm{N}} &= (1 - 2R_{1})(1 - 2R_{2}) \\ &= \exp[-i(\theta_{1} + \theta + 2\theta_{2} - 2\varphi_{1} - 2\varphi_{2})] - R_{1}R_{2} \\ &= \exp[-i(\theta_{1} + \theta - 2\varphi_{2})] - R_{2}(1 - 2R_{1}) \\ &= \exp[-i(\theta_{1} + \theta + 2\theta_{2} - 2\varphi_{1})] - R_{1} \\ &= \exp[-i(\theta_{1} + \theta)] \end{split}$$
 
$$Q_{\mathrm{D}} &= 1 - R_{1}R_{2} \exp[-\mathrm{i}2(\theta_{2} - \varphi_{1})] + R_{2} \exp[\mathrm{i}2\varphi_{2}] \\ &+ R_{1}(1 - 2R_{2}) \exp[-\mathrm{i}2(\theta_{2} - \varphi_{1} - \varphi_{2})] \end{split}$$
 (3)

The force can be split into the real and imaginary parts, and  $_{96}$  they are equivalent to the z and y axis force components. An  $_{97}$  infinitesimal optical force exerted by a single photon stream is  $_{98}$  given by

$$dF_{x-y} = \frac{N}{\Delta t} \frac{h}{\lambda} \left[ (\cos \alpha - \text{Re}\{Q\}) \mathbf{y} - (\sin \alpha - \text{Im}\{Q\}) \right]$$
$$\cos \phi \mathbf{x} r_1^2 \sin \theta \cos \theta_1 d\theta d\phi \tag{4}$$

where N is the number of photons transported through the ray,  $_{100}$  h is Planck's constant,  $\lambda$  is the wavelength of the light, and  $\mathbf{z}$  and  $_{101}$   $\mathbf{r}$  are the axial and radial unit vectors, respectively. By  $_{102}$  integrating the relations over the integration bounds that  $_{103}$  determine the trajectory of the photon stream impinging on the  $_{104}$  interface between the inner  $(\theta_{\rm h})$  and outer  $(\theta_{\rm m})$  spheres

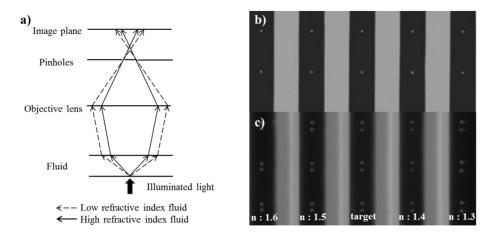
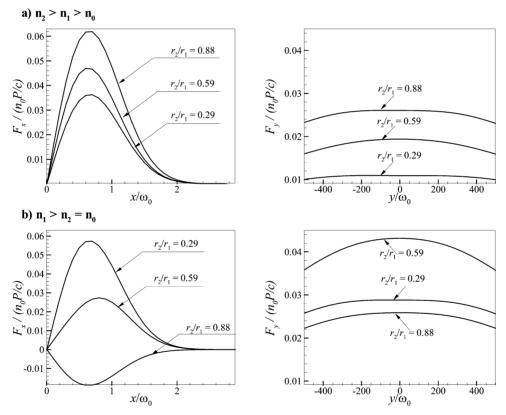


Figure 3. (a) Schematics of the microimage defocusing refractometer. (b) Image spots are on the focal plane. (c) Image spots are out of the focal plane.



**Figure 4.** (a) Radial and axial force distributions for  $n_2 > n_1 > n_0$  (Case 1:  $r_1/\omega_0 = 0.85$ ,  $\lambda/\omega_0 = 5.32 \times 10^{-3}$ ,  $n_1/n_0 = 1.056$ , and  $n_2/n_0 = 1.106$ ). (b) Radial and axial force distributions for  $n_1 > n_2 = n_0$  (Case 2:  $r_1/\omega_0 = 0.85$ ,  $\lambda/\omega_0 = 5.32 \times 10^{-3}$ ,  $n_1/n_0 = 1.106$ , and  $n_2/n_0 = 1$ ).

$$\theta_{\rm h} = \sin^{-1} \left( \frac{n_1}{n_0} \frac{r_2}{r_1} \right) - \alpha \qquad \theta_{\rm m} = \frac{\pi}{2} - \alpha$$
 (5)

Then, the axial and radial forces  $F_v$  and  $F_x$  can be derived as

$$F_{y} = \frac{n_{0}}{c} r_{1}^{2} \int_{0}^{2\pi} \left[ \int_{\theta_{h}}^{\theta_{m}} I(\rho, y) [\cos \alpha - \text{Re}\{Q_{h}\}] \right]$$

$$\sin \theta \cos \theta_{1} d\theta + \int_{0}^{\theta_{h}} I(\rho, y) [\cos \alpha - \text{Re}\{Q\}] \sin \theta$$

$$d\theta \cos \theta_{1} d\phi$$
(6)

$$F_{x} = -\frac{n_{0}}{c} r_{1}^{2} \int_{0}^{2\pi} \left[ \int_{\theta_{h}}^{\theta_{m}} I(\rho, y) [\sin \alpha - \text{Im}\{Q_{h}\}]] I(\rho, y) \right]$$

$$[\sin \alpha - \text{Im}\{Q_{h}\}] \sin \theta \cos \theta_{1} d\theta$$

$$+ \int_{0}^{\theta_{h}} I(\rho, y) [\sin \alpha - \text{Im}\{Q\}] \sin \theta d\theta \cos \theta_{1}] \cos \phi$$

$$d\phi \qquad (7)$$

## **EXPERIMENTAL SECTION**

As shown in Figure 2c, the system we studied included three layers of 108 glass microcapillaries that formed a coflowing geometry, 18,19 which 109 generated a water—oil—water double emulsion. A square glass tube (1 110

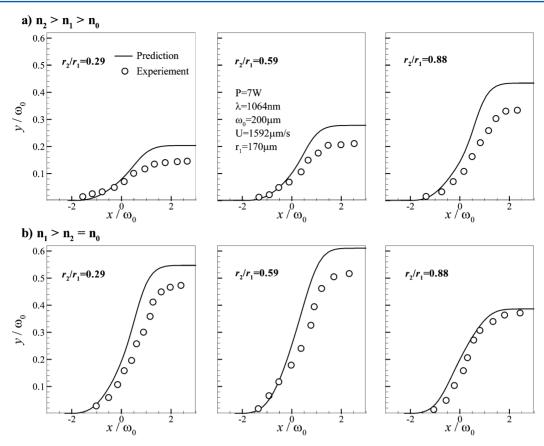


Figure 5. Trajectories for the double emulsions for (a)  $n_2 > n_1 > n_0$  and (b)  $n_1 > n_2 = n_0$ . The laser wavelength was  $\lambda = 1064$  nm; the beam waist radius was  $\omega_0 = 200 \ \mu \text{m}$ .

111 mm  $\times$  1 mm) provided a dynamic observation area in the cross-type 112 optical particle separation system. Because these two components were 113 fabricated on a single device, we generated a double emulsion and 114 simultaneously observed the double emulsion behavior in the presence 115 of optical forces. The glass microcapillaries were fabricated using the 116 conventional heating and pulling method (inner radius 10–180  $\mu$ m).

Octadecyl trichlorosilane (Sigma Aldrich) treatment was performed 117 on the inner surface of the middle capillary to prevent the water 118 119 medium from coating the glass surface. <sup>19</sup> Since middle capillary was 120 treated as a hydrophobic surface, the innermost aqueous medium was 121 emulsified in the middle oleic phase fluid under coaxial flow. The oleic phase emulsion was subsequently emulsified in the outer aqueous 122 123 fluid. The innermost aqueous medium was encapsulated by an oleic 124 phase droplet at the tip of the middle capillary as the oleic phase 125 emulsions were generated. Each capillary was connected to a pulsation 126 free multichannel syringe pump (Nemesys, Cetoni GmbH) for 127 adjusting the volumetric flow rate of each fluid flow. The net fluid 128 flow rate was about 5700  $\mu$ L/h and the emulsion velocity in the 129 microchannel was about 1592  $\mu m/s$ . The outer radius of an emulsion 130 was about 150  $\mu$ m and the inner radius of an emulsion varied over the range 40-130  $\mu$ m as a function of the inner and middle fluid flow rates. The aqueous solution of 2 wt % polyvinyl alcohol (Sigma 133 Aldirch) was used for the outermost fluid. Ethoxylated trimethylolpropane triacrylate (Sigma Aldrich, n = 1.470) and polydimethylsilox-135 ane oil (Sigma Aldrich, n = 1.405) were used as the middle oil phase of 136 the water/oil/water double emulsion. CaCl<sub>2</sub> was added to aqueous solution to adjust the refractive index at the inner aqueous phase.

138 We measured the refractive index of a 6 M CaCl<sub>2</sub> solution (n = 139 1.469) using the defocused microrefractometer method. A schematic 140 diagram of the refractometer is shown in Figure 3a. Since the refractive 141 indexes of each reference fluid are different, the refractive angle at the 142 interface of fluid and glass varies with the refractive index of the fluid. 143 When a spot is located on the focal plane, whether two pinhole 144 apertures are in front of the image plane or not, a single spot image

appears at the image plane in Figure 3b. In the case of a spot moving 145 away from the focal plane, the spot image is separated as two blurred 146 spot images at the image plane in Figure 3c. The distances between 147 each spot image are determined by the refractive index of the fluid. 148 The device simply consists of five silicon-etched microfluidic channels 149 and 3  $\mu$ m patterned spots on their bottom glass surfaces, and each 150 channel is filled with reference fluids and target fluid. Since the spot 151 images for all fluids are captured in the same image frame, the 152 refractive index of target fluid can be obtained by simple curve fitting 153 from a single step measurement. In this device, four authorized 154 refractive index fluids n = 1300, 1400, 1500, and 1600 (Cargille 155 Laboratories) were used as reference fluids.

To prevent absorption of 1064 nm light by the water media, heavy 157 water ( $D_2O$ ) was used as the aqueous phase. The refractive index 158 and diameter of each emulsion layer were adjusted to generate a model 159 for cell-nucleus morphometry systems (Case 1:  $n_1 > n_2 > n_0$ ) using a 160 water/oil/water double emulsion or a hollow sphere (Case 2:  $n_1 > n_2 = 161$   $n_0$ ). The laser beam waist radius was adjusted using a spherical lens 162 and was illuminated vertically in the direction of the fluid flow. Since 163 the vertical alignment between the incident angle of light and the 164 sidewall of the square capillary was crucial, the device was aligned 165 using a custom-made 5-axis stage for alignment. Since the double 166 emulsions passed the light within a very short time and the optical 167 scattering force was perpendicular to the gravitational force, the 168 influence of the gravitational force on the vertical displacement was 169 negligible.

#### ■ RESULTS AND DISCUSSION

Figure 4 shows the normalized optical force distributions for 172 fd both cases during the cross-type particle separation. As is true 173 for most biological cells, the inner of the concentric spheres had 174 a larger refractive index than the outer sphere. The refractive 175 index of the cell nucleus is usually higher than that of the cell 176

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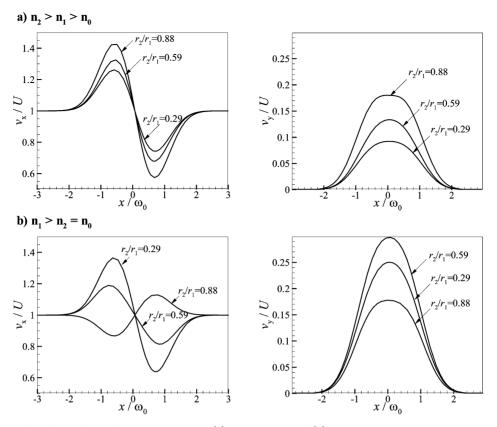


Figure 6. Variations in the velocity of the double emulsions for (a)  $n_2 > n_1 > n_0$  and (b)  $n_1 > n_2 = n_0$ 

177 cytoplasm.  $^{21,24}$  For Case 1, the calculations were performed for three ratios of inner to outer sphere radii,  $r_2/r_1 = 0.29$ , 0.59, and 179 0.88 in Figure 4a. The axial and radial forces both increased as 180 the inner sphere radius increased. A sphere in which the 181 refractive index of the inner sphere was higher than that of the 182 outer sphere yielded more refracted trajectories for photons 183 that passed through the inner sphere. This meant that more 184 momentum was transferred to the emulsion.

For Case 2, the refractive index ratio was adjusted to  $n_1/n_0$  = 185 186 1.106,  $n_2/n_0 = 1$ , which included an outer sphere with a high refractive index and an inner sphere and outer fluid with lower identical refractive indices. As shown in Figure 4b, the optical 189 force distributions differed from those of Case 1. Total internal 190 reflection could explain this unexpected force distribution. Since the refractive index of the inner sphere was smaller than 192 that of the outer sphere, total internal reflection occurred at the 193 interface of the inner sphere. From Figure 2b, the critical angle 194 at the interface between the inner and outer spheres was 195 defined by  $\sin \theta_{2,\text{crit}} = n_2/n_1$ , which is equivalent to  $\sin \theta_{1,\text{crit}} =$ 196  $r_2/r_1$ . When the total internal reflection occurred, the photons 197 were totally reflected backward at the interface of the inner 198 sphere so that the axial force increased. As the relative size of 199 the inner sphere decreased, total internal reflection occurred at 200 smaller values of  $\theta_1$ , and more photons underwent total internal 201 reflection. However, the relative size of the inner sphere 202 increased, and total internal reflection occurred at larger values 203 of  $\theta_1$  such that fewer photons underwent total internal 204 reflection. For  $r_2/r_1 = 0.88$ , the lower refractive index of the 205 inner sphere compared to the outer sphere and the effects of 206 total internal reflection were relatively small because of the 207 large size ratio. The radial force distribution of the laser beam 208 repelled the sphere away from the center axis of the laser beam 209 to a region near the laser beam waist. In the radial force

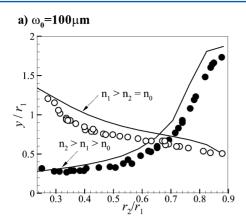
distribution, when the photons underwent total internal 210 reflection, the sphere was pushed away from the beam axis. 211 This pushing effect increased as the relative size of the inner 212 sphere increased, since the critical angle increased as the 213 relative size of the inner sphere increased. As shown in Figure 214 4b, the pushing effect was dominant at  $r_2/r_1 = 0.88$  and the 215 radial force acted in an outward direction from the laser beam 216 axis.

Trajectories of the emulsion in the cross-type particle  $^{218}$  separation system are experimentally observed and plotted in  $^{219}$  Figure 5. The predicted trajectories are also shown for  $^{220}$  fs comparison. The equations describing the dynamics of double  $^{221}$  emulsions subject to cross-type optical particle separation can  $^{222}$  be expressed as  $^{10}$   $^{223}$ 

$$m_{p} \frac{\mathrm{d}r}{\mathrm{d}t} - 6\pi\mu r_{p}(U - V_{p}) = F \qquad \mathbf{U} = U\hat{\mathbf{x}}$$

$$\mathbf{V}_{p} = \nu_{p}\hat{\mathbf{x}} + w_{p}\hat{\mathbf{y}} \quad \mathbf{F} = F_{y}\hat{\mathbf{y}} + F_{x}\hat{\mathbf{x}}$$
(8)

where  $m_{\rm p}$  is the particle mass,  ${\bf r}$  is the particle position vector,  $\mu$  224 is the dynamic viscosity of the fluid,  ${\bf F}$  is the optical force vector 225 from eqs 6 and 7, and  ${\bf U}$  and  ${\bf V}_{\rm p}$  are the fluid and particle 226 velocity vectors, respectively. As shown in Figure 5, the 227 experimental data were qualitatively in good agreement with 228 the predicted data, although the experimental values were 229 slightly lower than the predicted values. This small discrepancy 230 was attributed to the fact that both the inner and outer 231 emulsions consisted of only liquid, and their behaviors differed 232 from that of a solid concentric sphere. If two liquids had 233 relatively high mutual solubility or low mutual solubility but 234 were generated a long time before, the diffusion of two liquids 235 made a graded refractive index interface and the optical force 236 distribution at the graded refractive index interface had a 237



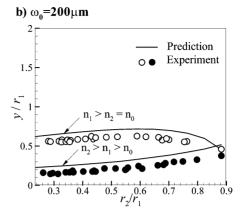


Figure 7. Effect of the retention distance on the ratio of the radii  $(r_2/r_1)$  for (a)  $\omega_0 = 100 \ \mu m$  and (b)  $\omega_0 = 200 \ \mu m$ .

238 different distribution against the sharp interface. However, the 239 mutual solubility of the present study was very low. For Case 1, 240 the retention distance of the double emulsion increased as  $r_2/r_1$ 241 increased in Figure 5a. Because both the gradient and scattering 242 forces on the double emulsions increased in Case 1, as shown 243 in Figure 4a, the retention distance also increased. As 244 mentioned earlier, because the inner emulsion had a larger 245 refractive index, the transferred photon momentum was 246 increased as the size of the inner emulsion increased, as shown in Figure 4a. The different behavior of the emulsion is shown in Figure 5b. For Case 2, the refractive index ratio  $(n_2/n_2)$ 249  $n_1$ ) was smaller than 1; the transferred photon momentum decreased as the inner emulsion radius increased. However, total internal reflection and the angle between the ray and the 252 beam increased the retention distance of  $r_2/r_1 = 0.59$  compared to  $r_2/r_1 = 0.29$ , and the smallest retention distance was  $r_2/r_1 =$ 

Numerical simulations permit the decomposition of the 255 double emulsion behavior into each directional velocity component to estimate the dynamics for each direction.<sup>10</sup> Figure 6 shows the velocity components of each case. For Case 1, the velocity distributions in the y and z directions changed significantly as the ratio of the inner to outer emulsion 261 increased. Figure 6a plots the acceleration and deceleration of the emulsion as it passed through the center axis of the laser beam due to each component of the optical force, as shown in 264 Figure 4a. Figure 6b shows different behavior, that is, the gradient force distribution of  $r_2/r_1 = 0.59$  shown in Figure 4b 266 was smaller than that corresponding to  $r_2/r_1 = 0.29$ , and the ydirectional velocity distribution was small. For  $r_2/r_1 = 0.88$ , the radial velocity displayed the opposite behavior as a result of the gradient force distribution, as mentioned earlier.

The effects of the laser beam waist radius on the behavior were investigated by calculating and experimentally measuring the retention distance of a double emulsion for two cases. In the first case, the laser beam waist  $(\omega_0)$  was larger than the radius of the emulsion  $(r_1)$ . In the second case,  $\omega_0$  was comparable to or smaller than the radius of the emulsion. The retention distance as a function of the ratio of the inner to outer radii is plotted in Figure 7. The experimental measurements agreed well with the theoretical predictions. For Case 1  $(\omega_0$  = 100  $\mu$ m) shown in Figure 7a, the retention distance increased as the inner radius increased, and it decreased as the inner radius increased for Case 2. In contrast, a different trend was observed for  $\omega_0$  = 200  $\mu$ m, as shown in Figure 7b. The retention distance in Case 1 displayed a similar directional

change with increasing inner emulsion radius for both beam 284 waist radii, but the retention distance of  $\omega_0 = 100 \,\mu\text{m}$  was larger 285 than that corresponding to  $\omega_0$  = 200  $\mu$ m. As mentioned earlier, 286 the inner emulsion impinging condition  $(\theta_{
m h})$  increased as the 287 beam waist radius  $(\omega_0)$  decreased. This meant that more 288 photons could impinge on the inner emulsion surface as the 289 beam waist radius decreased. Additionally, a larger gradient 290 force for smaller beam waist radii lengthened the trapping time 291 for the double emulsion, consistent with the nonlinear behavior 292 of cross-type optical particle separation systems described in 293 our previous study. 25 The retention distances for Case 2, in 294 which total internal reflection occurred at the interface of the 295 inner emulsion, followed a different trend for each beam waist 296 radius. This could be explained in terms of the inner emulsion 297 impinging conditions  $\theta_{\rm h}$ . In contrast with Case 1, the lower 298 refractive index of the inner emulsion resulted in total internal 299 reflection at the interface between the inner and outer 300 emulsions.

#### CONCLUSIONS

We experimentally investigated the behavior of the double 303 emulsions in a cross-type optical separation system based on 304 the trajectories and the final retention distance. The behavior of 305 the double emulsion was predicted using the photon stream 306 method and particle dynamic equations. We confirmed that the 307 behavior of the double emulsion in the cross-type optical 308 particle separation system agreed well with the predicted 309 results. The effects of the optical force on the continuous 310 separation of the double emulsion depended on the size of the 311 inner emulsion layer and the refractive index ratio between the 312 inner and outer emulsions. We additionally found that total 313 internal reflection at the interface of the inner emulsion 314 produced complex behavior for water/oil/water double 315 emulsions or hollow spheres. The observed and predicted 316 behaviors of the double emulsions in the presence of optical 317 forces have important implications for cell manipulation, cell- 318 nucleus morphometric models, and emulsion-based drug 319 delivery vehicles. 320

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Notes 325

The authors declare no competing financial interest.

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