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# 1 Heterogeneous Catalytic Activity of Platinum Nanoparticles Hosted 2 in Mesoporous Silica Thin Films Modified with Polyelectrolyte 3 Brushes

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  - Supporting Information

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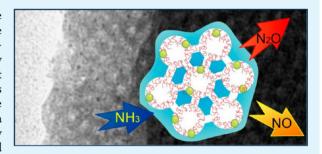
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ABSTRACT: Platinum nanoparticles of 3 nm diameter were included in mesoporous silica thin films by controlling the mesopore surface charge with a short polymer brush. This metalpolymer-mesopore nanocomposite presents high catalytic activity toward ammonia oxidation at low temperatures with 4.5% by weight platinum loading. An anomalous partial selectivity toward nitrous oxide is observed for the first time, which can be traced back to the synergy of the particles and modified surface. This effect opens a path toward the design of nanocomposite catalysts with highly controlled environments, in which the size- and function-controlled cavities can be tuned in order to lower the reaction barriers.



KEYWORDS: mesoporous films, metal-polymer nanocomposites, brush polymers, gold catalysis, ammonia oxidation, nanocatalysis

#### INTRODUCTION

27 Current research in nanocatalysis and materials science is 28 vigorously pushing the boundaries of the systems under study 29 into the domains of complex nanomaterials. 1-3 The core area 30 of research in catalysis has started to shift from studies on 31 single-crystal surfaces toward the exploration of metal nano-32 particles (MNPs).<sup>4,5</sup> The combination of MNPs and 33 mesoporous materials has been gaining increasing importance 34 in heterogeneous catalysis, exploiting the exquisite control over 35 the surface, structural and functional properties of the 36 mesoporous supports, and high and tailorable interface area 37 between both components. Mesopores are indeed highly 38 tuned nanoscopic environments that can influence the catalytic 39 behavior. Beyond the expected effects of shape and size 40 selectivity, nanoconfinement effects due to restricted volume 41 and surface curvature result in a lowering of kinetic barriers.<sup>7–9</sup> 42 Recently, a platinum-mesoporous silica catalyst prepared by 43 impregnation allowed the attainment of fast and complete 44 oxidation of low-pressure ethylene at ambient temperature. 10 A 45 correlation was also recently found between the surface 46 chemistry of the internal concave walls of mesoporous CeO<sub>2</sub> 47 and the low activation energy of a water-gas shift reaction 48 catalyzed by MNPs. 11 In addition, MNPs embedded in

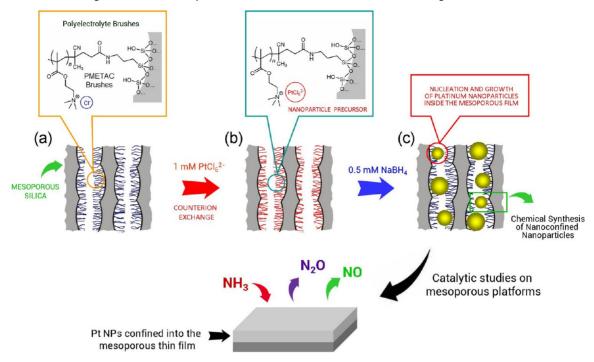
mesopores also exhibit excellent thermal stability under relevant 49 turnover conditions. 12 There seems thus to be an important 50 role of the chemical properties of the pore surface, which could 51 be advantageously tuned in order to change the catalyst activity 52 or selectivity.

Improving the catalytic performance through these nano- 54 composite systems relies on our ability to master the 55 incorporation of MNPs into the mesoporous support. Several 56 research efforts were recently made for devising new strategies 57 to incorporate platinum nanoparticles (Pt NPs) into meso- 58 porous silica for catalytic purposes. A critical aspect is the 59 particle monodispersity and homogeneity of its incorpora- 60 tion. 13-17 For example, Somorjai and co-workers developed a 61 set of protocols ranging from the hydrothermal growth of 62 mesoporous silica in the presence of polymer-stabilized Pt 63 NPs<sup>18</sup> to the sonication-aided impregnation of poly- 64 (amidoamine)-dendrimer-stabilized or poly(vinylpyrrolidone)- 65 stabilized Pt NPs that proved very successful. 19,20 Controlled 66 reduction methods within the mesopore system afford a 67

Received: June 26, 2013 Accepted: September 10, 2013



Scheme 1. Schematic Depiction of Pt NP Synthesis at the Inner Environment of a Mesoporous Silica Film<sup>a</sup>



<sup>a</sup>The chloride counterions in the as-synthesized PMETAC-modified silica films (a) are exchanged by the corresponding anionic precursors,  $PtCl_6^{2-}$  (b). Then, the platinum chloro complexes are chemically reduced to form MNPs within the nanoscale brush-coated pores (c). The scheme also describes the chemical species involved in the catalytic transformation of ammonia.

68 straightforward and reproducible strategy to tuning the 69 nanoparticle size and distribution by controlling the mesopore 70 surface. The isoelectric point (IEP) of the mesoporous matrix 71 plays a key role in the successful incorporation and dispersion 72 of negatively charged metal precursors such as  $MCl_n^{z-}$  (M = 73 Au, Pd, Pt, etc.) into the nanostructured support prior to 74 reduction. Impregnation processes of PtCl<sub>6</sub><sup>2-</sup> precursors in 75 slightly acidic conditions proceed straightforwardly in high-IEP 76 mesoporous oxides, but the same strategy leads to very low 77 nanoparticle loading in materials like silica (IEP  $\sim$  2). In order to increase the MNP loading, higher concentrations of the 79 metal precursor or reducing agents, or harsher reduction 80 conditions (i.e., higher temperatures, longer reaction times, 81 etc.), are used. These conditions lead to uncontrolled growth of 82 the metallic particles that present larger sizes and broader size 83 dispersion, which are detrimental to the catalyst activity and 84 selectivity. Pore modification strategies with molecular dangling 85 amino, ammonium, or thiol groups have been applied to change 86 the surface charge, improving impregnation of the metal 87 precursors and thus the nanoparticle control. 21,22 In a previous 88 work, we demonstrated that a highly controlled loading can be  $_{89}$  achieved by tethering polyelectrolyte brushes on mesoporous  $_{90}$  silica walls.  $^{23-26}$  This strategy offers the possibility of 91 supporting MNPs confined in a 3D nanometer-sized frame-92 work via simple in situ synthetic steps, <sup>27,28</sup> allowing the soft 93 formation of platinum colloids locally addressed into the 94 mesopores (Scheme 1).

In principle, confinement of Pt NPs in nanospaces can significantly change their activity and selectivity. In this work, we used the well-known heterogeneously catalyzed gas-phase soxidation of ammonia as a test of the catalytic properties of the Pt NPs hosted in the mesoporous films modified with cationic polymer brushes. Gas-phase oxidation of ammonia is an important process from both industrial and environmental 101 viewpoints; good illustrations are nitric acid production via 102 Ostwald process and removal of NH<sub>3</sub> produced in catalytic 103 reformers of internal combustion engines.<sup>29</sup> Experimental and 104 theoretical studies performed on platinum single-crystal 105 surfaces revealed that ammonia decomposition (i.e., the initial 106 hydrogen-atom ripping, which constitutes the highest activation 107 energy step) is greatly accelerated by the presence of adsorbed 108 oxygen or OH adspecies.<sup>30–32</sup> The same effect was also recently 109 observed in ammonia oxidation with oxygen performed on 110 rhodium single crystals.<sup>33–36</sup> Reaction products depend on 111 several factors such as the temperature and reactant partial 112 pressures. Over platinum catalysts, the following global 113 reactions take place:

$$4NH_3 + 5O_2 \rightarrow 4NO + 6H_2O$$
 (1) <sub>115</sub>

$$4NH_3 + 3O_2 \rightarrow 2N_2 + 6H_2O$$
 (2) <sub>116</sub>

$$4NH_3 + 4O_2 \rightarrow 2N_2O + 6H_2O$$
 (3)

The oxygen partial pressure was found to be the control 118 parameter changing the preferred pathway between  $N_2$  and 119 nitrous oxide (NO). High temperatures and oxygen pressures 120 favor NO formation, while the opposite results in  $N_2$  being the 121 preferred product. So far, ultrahigh-vacuum (UHV) single- 122 crystal studies have shown that  $N_2$ O is produced in significant 123 amounts only when relatively high total pressures are used 124 (>10<sup>-2</sup> mbar).  $^{37,38}$ 

To the best of our knowledge, this is the first study of the  $^{126}$  catalytic ammonia oxidation reaction with Pt NPs supported on  $^{127}$  mesoporous thin films near UHV regimes. NO is a greenhouse  $^{128}$  gas known to contribute to global warming approximately  $^{300}$   $^{129}$  times more than carbon dioxide ( $^{120}$ ); because of these  $^{130}$  deleterious effects, further insight leading to new ways of  $^{131}$ 

132 controlling its emissions is of great interest.<sup>39</sup> The approach 133 presented here applies a well-developed toolkit, usually 134 employed on precisely chosen monocrystalline materials to 135 complex MNP—oxide nanocomposites. Even if the character-136 istics of the system explored and techniques used lead to some 137 level of indetermination, valuable insight is gained considering 138 that traditional methods are not suitable to precisely assess the 139 catalytic activity and selectivity of very low quantities of 140 nanostructured matter.

#### 41 EXPERIMENTAL SECTION

142 Mesoporous nanocomposite thin film catalysts were produced 143 in two steps. First, highly homogeneous hybrid polymeric— 144 inorganic porous thin films (60–180 nm thickness) were 145 produced. Subsequently, platinum salts were adsorbed within 146 the mesopores, and Pt NPs were then obtained by mild 147 reduction. Mesoporous aminosilica films (RNH<sub>2</sub>:Si = 0.2:1) 148 were deposited onto glass substrates by dip-coating, at a 149 withdrawal speed of 2 mm/s, under 40-50% humidity. The 150 precursor solution contains tetraethoxysilane (TEOS; Merck), 151 (3-aminopropyl)triethoxysilane (APTES; Fluka, 98%), F127 152 block copolymer (Aldrich,  $M_r = 13600$ ), ethanol, water, and 153 HCl in the following molar ratio: 0.8:0.2:0.005:24:5.2:0.28 154 TEOS/APTES/F127/EtOH/H2O/HCl. Pluronic F127 block 155 copolymer was employed as the structure-directing agent. 156 Amino-containing films were consolidated by three successive 157 24 h thermal treatments at 60 and 130 °C and 2 h at 200 °C (in 158 an air atmosphere). The template was subsequently extracted 159 by submitting to acidic ethanol (0.1 mol dm<sup>-3</sup>) for 3 days, 160 according to a previously reported protocol. 40 The surface 161 amino functions were used as grafting sites for the surface-162 initiated free-radical polymerization of poly[2-163 (methacryloyloxy)ethyltrimethylammonium chloride] (PME-164 TAC) brushes. In a first step, the amino groups were 165 conjugated to 4,4'-azobis(4-cyanopentanoic acid) as a surface-166 confined initiator. 41 Subsequently, polymer brush polymer-167 ization was accomplished by surface-initiated free-radical 168 polymerization of METAC monomers in a 50 wt % solution 169 in water. Under these conditions, the aminosilica walls are 170 negatively charged, causing a preconcentration of METAC+ monomers inside the pores. The polymer content and thus the 172 charge density can be regulated by the polymerization time. For 173 the catalytic experiments presented below, samples submitted 174 to 210 min of polymerization were used.

The procedure for the production of pore-embedded Pt NPs was adapted from ref 28. Briefly, in a preconcentration step, the hybrid films were immersed in an aqueous solution of 1 mM  $^{178}$   $^{18}$ 

Water adsorption—desorption isotherms (at 298 K) were measured by ellipsometric porosimetry (EP; SOPRA GESSA). 187 From the measured isotherms, pore-size distributions were 188 obtained using models based on the Kelvin equation, 189 considering the respective contact angles. The contact angle 190 of water to the films was determined using a Ramé-Hart 190 191 CA. Field-emission scanning electron microscopy (FE-SEM) 192 images were obtained with a ZEISS LEO 982 Gemini 193 microscope in the secondary-electron mode; transmission

electron microscopy (TEM) images were obtained with a 194 Philips CM200 microscope with EDAX, to perform energy- 195 dispersive spectroscopy (EDS). Grazing incidence, small-angle 196 X-ray scattering (GI-SAXS) measurements were performed at 197 the XRD2 beamline of Laboratório Nacional de Luz Síncrotron 198 (LNLS), Brazil, using a six-circle Huber diffractometer and a 199 2D PILATUS detector (energy = 8 keV; sample-to-detector 200 distance = 50.7 cm). The incident angle was fixed at  $\theta = 0.2^{\circ}$  201 with an integration time of 60 s. X-ray reflectometry (XRR) 202 measurements were performed on the same LNLS beamline; in 203 order to obtain accurate density values, measurements were 204 performed under low-humidity conditions (under a stream of 205 dry  $N_2$ ).

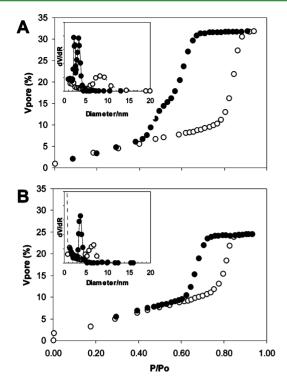
Diffuse-reflectance infrared Fourier transform spectroscopy 207 (DRIFTS) measurements were performed using a Nicolet 208 Magna 560 instrument, equipped with a liquid-nitrogen-cooled 209 MCT-A detector. DRIFTS measurements were performed by 210 depositing scratched film samples on a KBr-filled DRIFTS 211 sample holder.

The experimental setup used for monitoring the catalytic 213 activity of Pt NPs hosted in the modified mesoporous films is 214 similar to the one previously described for surface catalysis 215 experiments on single-crystal surfaces. 42 The UHV chamber is 216 pumped by a turbomolecular pump combined with an ion 217 pump and a titanium sublimation pump. After bakeout, the 218 system can maintain a base pressure of less than  $3 \times 10^{-10}$  219 mbar. A chromium-aluminum thermocouple spot-welded to 220 the back of the sample was used for temperature measurements, 221 and because the active material was supported on glass (which 222 limits the maximum operating temperature to \$350 °C), 223 indirect heating was conducted by a tungsten filament on the 224 back of the sample. An annealing procedure, as applied usually 225 in UHV experiments on metallic samples, was not possible, and 226 therefore the minimum base pressure reached was as low as 1 × 227  $10^{-7}$  mbar. After several Ar<sup>+</sup>-ion bombardments ( $p_{Ar} = 3 \times 10^{-5}$  228 mbar) and heat ( $T_{\text{max}} = 300$  °C) cleaning cycles were 229 conducted, activation of the supported nanoparticle was carried 230 out via oxidation (O2) and reduction (H2) cycles of 231 approximately 40 min at 250 °C, using pressures of  $1 \times 10^{-5}$  232 mbar. To ensure the effectiveness of the cleaning procedure 233 applied, reaction/cleaning cycles were repeated until subse- 234 quent measurements of the catalytic activity displayed no 235 difference. An analogous procedure was also employed by 236 Somorjai and co-workers to remove the polymeric capping 237 layer. 12 The reaction rates were obtained using a differentially 238 pumped quadrupole mass spectrometer, which was connected 239 to a cone brought approximately 1 mm in front of the 240 catalytically active surface, avoiding in this way any spurious 241 signals coming from the hot filament or other parts of the 242 experimental setup. Signals corresponding to m/e 18, 28, 30, 243 and 44 were followed (as was usually done for experiments on 244 the same reaction system) in order to determine the amounts 245 of H<sub>2</sub>O, N<sub>2</sub>, NO, and N<sub>2</sub>O, respectively, produced for a given 246 reaction regime.

# ■ RESULTS AND DISCUSSION

Mesoporous thin films produced in the conditions reported  $^{249}$  above display highly organized pore arrays with cubic-derived  $^{250}$  mesostructure (Im3m) with a cubic cell parameter a of  $^{19.6}$  nm,  $^{251}$  as assessed by SAXS; uniaxial contraction results in ellipsoidal-  $^{252}$  shaped pores (Figure 1A). The pore size and pore volume were  $^{253}$  fi extracted from the water adsorption—desorption isotherms  $^{254}$  obtained from EP shown in Figure 2. EP measurements of the  $^{255}$  figure  $^{259}$ 

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**Figure 1.** Water adsorption—desorption isotherms, obtained by EP, of silica thin films containing a propylamino function (A) and PMETAC brushes after 210 min of polymerization time (B). The insets in each panel correspond to the pore-size distribution of both samples. Open symbols correspond to adsorption (inset: pore size), and closed symbols correspond to desorption (inset: neck size).

amino-functionalized silica films yield 32% pore volume, and an 256 average major pore diameter of 8.3 nm, calculated from the 257 isotherm adsorption branch taking into account a contact angle 258 of 30° (Figure 1A). This is in good agreement with the SEM 259 micrographs (see the Supporting Information, SI). A two-step 260 desorption branch is observed in the initial hybrids; this could 261 be due, in principle, to either inhomogeneities of the mesopore 262 structure or the existence of some pore plugging, which can 263 lead to two different neck sizes. Structural analysis by TEM and 264 SAXS ruled out inhomogeneities; therefore, we concluded that 265 a fraction of the necks could correspond to pore plugging, 266 probably by some remaining surfactant. Analysis of the 267 isotherm desorption branch was performed according to the 268 model proposed by Boissière et al., 43 leading to neck sizes of 269 3.4 and 2.3 nm diameter.

After polymerization, the silica films presented a contact 271 angle of 61°, corresponding to a more hydrophobic surface. EP 272 measurements performed on PMETAC-containing samples 273 yielded significant differences. The film pore volume decreased 274 to 24% and the pore diameter to 6.8 nm; a unique neck size of 275 3.8 nm was obtained from the desorption curve (see Figure 276 1B). The slight neck enlargement and disappearance of the 277 smaller neck fraction are probably a consequence of complete 278 template extraction after the polymerization step, which is 279 performed in a polar medium; some extra condensation leading 280 to pore rearrangement cannot be ruled out. From these 281 measurements, it can be concluded that a significant fraction of 282 the mesopore volume is filled with the polymer, albeit leaving 283 necks large enough for the swift diffusion of molecular species. 284 The pore volume obtained by EP is in good agreement with 285

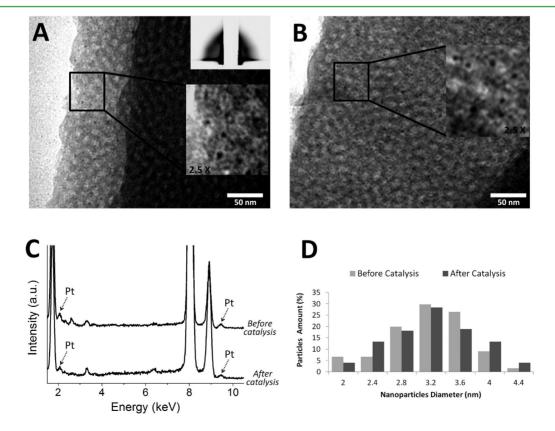


Figure 2. TEM micrographs of platinum-loaded mesoporous silica before (A) and after (B) one catalytic cycle. The inset in part A shows a GI-SAXS pattern; details (2.5×) of the nanoparticles are shown in both panels. EDS spectra of films (C) and particle-size distributions of Pt NPs (D) before and after catalysis (counting 300 nanoparticles).

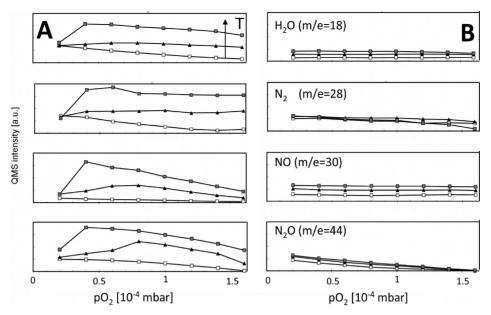


Figure 3. (A) Plot of the TOF (arbitrary units) for different reaction products versus oxygen partial pressure ( $\times 10^{-4}$  mbar), for increasingly higher temperatures. All of the experiments were carried out using a fixed ammonia pressure of  $4 \times 10^{-5}$  mbar. Ambient temperature (30 °C) was taken as the reference for no catalytic activity and therefore is not shown. A TOF peak can be observed when the reactant ratio is approximately 1:1. (B) Same experiments as those described in part A but using a bare mesoporous support material sample. Catalytic measurements correspond to 90 ( $\square$ ), 140 ( $\triangle$ ), and 220 (gray  $\square$ ) °C.

286 XRR measurements that estimate that the polymer occupies 287 10% of the pore volume. These results allow one to estimate an 288 average polymerization degree of  $n \approx 4.5$ , according to a 289 previous determination of the amino content in PMETAC-290 modified films, in which an 83% of pore filling afforded an n of 291 ca. 30-32.

The PMETAC polymer incorporated is just enough to switch the surface charge, endowing a positive charge to the pores at moderately acidic pH values. This permits the incorporation of  $PtCl_6^{2-}$  and its subsequent mild reduction to Pt NPs. The presence of PMETAC was confirmed by DRIFTS (see the SI, Figure 1). A slight tint change is observed after PtCl<sub>6</sub><sup>2-</sup> reduction, suggesting that a reduction reaction takes place. TEM images of the films submitted to this reduction cycle show that MNPs with an average diameter of  $3.0 \pm 0.6$  mm (obtained by counting 300 particles; Figure 2D) are located within the mesopores (Figure 2A).

The Pt NPs occupy less than 2% pore volume, as estimated from analysis of the XRR critical-angle shift (see the SI, Figure 305 2a). The metal content was determined following the procedure described in ref44. Briefly, a change in the electronic density ( $\rho$ ) of the films due to the presence of MNP implies a 308 shift in the critical angle  $\theta_c$ . From the critical-angle measurements, the electronic density of the film after and before platinum infiltration can be directly calculated using eq 1

$$\rho = \pi \theta_{\rm c}^2 / \lambda^2 r_{\rm e} \tag{1}$$

312 where  $\lambda$  is the X-ray wavelength and  $r_{\rm e}$  is the classical radius of 313 the electron. Finally, we can determine the volume fraction of 314 the Pt NPs  $(F_{\rm Pt})$  using eq 2:

$$F_{\text{Pt}} = (\rho_{\text{film+Pt}} - \rho_{\text{film}})/\rho_{\text{Pt}}$$
 (2)

316 where  $\rho_{\rm film}$  is the electronic density of the film before 317 infiltration,  $\rho_{\rm film+Pt}$  is the electronic density of the film after 318 platinum infiltration, and  $\rho_{\rm Pt}$  is the platinum electronic density 319 (4.1414  $\times$  10<sup>24</sup>).

The platinum loading value obtained using XRR is consistent 320 with the 2:98 Pt/Si atomic ratio obtained by EDS (Figure 2C), 321 which corresponds to a mass content of approximately 4.5% of 322 platinum in the nanocomposite samples. SEM analysis of the 323 whole sample did not detect MNP sitting on the film surface 324 (see the SI, Figure 3). This result stresses the importance of the 325 preconcentration of negatively charged platinum(II) precursors 326 within the pore system, probably because of the much larger 327 pore surface area. In a previous work, we demonstrated that 328 pore topology and surface functionalization can indeed be used 329 as synthetic tools to precisely locate MNPs within the 330 mesopores rather than at the film surface.<sup>28</sup> In this way, robust 331 mesopore-metal nanocomposite catalysts with accessible 332 porosity on the order of 20% were produced in situ, as 333 demonstrated by the water uptake observed by XRR of samples 334 submitted to low and high relative humidity conditions (see the 335 SI, Figure 2b). It is worth noting that the very mild conditions 336 presented here lead to the highly localized and controlled 337 growth of small platinum particles only in polymer-modified 338 mesopores. Indeed, the bare silica surface and PtCl<sub>6</sub><sup>4-</sup> present 339 negative charge for pH > 2, leading to an insignificant metal 340 adsorption within the pores for a wide range of adsorption- 341 reduction conditions. In order to obtain Pt NPs on pure 342 mesoporous silica, higher concentrations of the metal salt or the 343 reducing agent, or higher temperatures or longer reduction 344 times, are typically used. Normally, these harsher conditions 345 lead to uncontrolled growth of the metallic particles, and larger 346 particle sizes with larger size distributions are obtained. This is 347 an issue regarding the preparation of completely comparable 348 samples containing small, controlled Pt NPs within the 349 nonmodified silica mesopores.

Regarding measurements of the catalytic activity, it is 351 important to stress that the active surface area of the material 352 depends on the metal loading in the mesoporous matrix. This 353 amount is small compared to the reactor volume (approx- 354 imately 80 L). Because of this fact, high sensitivity to 355

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356 contamination can be expected. This could result in a 357 misleading interpretation of the experimental results in the 358 sense that a good catalyst may appear to be inactive either 359 because of contamination or because it was in an inactive state 360 at the time of measurement. For this reason, every experiment 361 was compared with a baseline obtained using a similar polymer-362 modified mesoporous silica film without Pt NPs (inactive). For 363 the reasons discussed above, we chose ammonia oxidation as 364 our probe reaction, and we explored different partial pressures 365 and temperatures to assess changes in the reactivity and 366 selectivity observed compared with the results obtained using 367 single crystals. Given the great amount of possible regimes in terms of reactant partial pressures and temperatures, we have chosen a particular domain of these variables in which platinum 370 is catalytically active according to previous experiments performed on platinum single-crystal surfaces. Namely, a 372 constant ammonia partial pressure was set to  $4 \times 10^{-5}$  mbar, 373 temperatures used were 90, 140, and 220 °C, and oxygen partial pressures used were in the range between  $2 \times 10^{-5}$  and  $1.5 \times 10^{-5}$  $^{375}$   $^{10^{-6}}$  mbar.  $^{45,46}$  An additional problem arises when m/e 44 is 376 considered, which corresponds to both CO2 and N2O 377 molecules. Given the polymer content of the sample, one cannot, in principle, rule out some  $CO_2$  contribution to the m/e44 signal, which would obscure the assessment of the catalytic 380 activity. To avoid this uncertainty, we have performed blank experiments using the mesoporous silica film without Pt NPs in 382 order to estimate the contribution of CO<sub>2</sub>. In this way, we were able to obtain N<sub>2</sub>O production for the Pt NP-containing sample 384 by subtracting both signals. It is worth noting that the polymer 385 integrity is maintained after catalytic measurements because 386 FTIR signals corresponding to the polymer are observed in 387 samples analyzed after catalysis (see the SI, Figure 1). Parts A 388 and B of Figure 3 show the kinetic measurements performed on 389 the mesoporous silica thin films with and without Pt NPs, 390 respectively. The evident difference in the profiles for the m/e391 44 signal between parts A and B of Figure 3 can only be due to 392 ammonia oxidation reaction, producing N<sub>2</sub>O.

Catalysis experiments were carried out for increasingly higher 394 temperatures; ambient temperature (30 °C) was considered as 395 a reference for no catalytic activity, and therefore the intensity 396 of the quadrupole mass spectrometry (QMS) signal at any 397 higher temperature was obtained by subtracting such a reference value. For a platinum single-crystal catalyst, a marked 399 selectivity shift is observed depending on whether the 400 conditions correspond to O2 (preferred products NO and 401 H<sub>2</sub>O) or NH<sub>3</sub> (preferred products N<sub>2</sub> and H<sub>2</sub>O) excess on the 402 reactant mixture feed.<sup>23</sup> Differently, results obtained using Pt 403 NPs demonstrated that, upon increasing oxygen partial pressure 404 for any given temperature, the production rate of all of the 405 monitored species showed a maximum value for an NH<sub>3</sub>/O<sub>2</sub> 406 ratio close to 1:1. Two striking features can be observed when 407 parts A and B of Figure 3 are compared: first, there is evident 408 measurable catalytic activity of the mesoporous silica film 409 containing Pt NPs, even at relatively low temperatures; second, 410 there is considerable production of N<sub>2</sub>O in the same regime 411 where the other reaction products are formed. This latter aspect 412 is surprising provided that this catalytic behavior was not 413 previously observed in any experiment performed on this 414 pressure regime over platinum single-crystal surfaces.

415 It can be hypothesized that, aside from the reaction 416 mechanism operating on platinum single-crystal surfaces,<sup>47</sup> 417 which were analyzed elsewhere and provide a plausible 418 explanation for selectivity toward N<sub>2</sub> or NO, Pt NPs confined in mesopores are able to increase the yield of  $N_2O$  through 419 different active catalytic sites not present on single-crystal 420 geometries. Furthermore, it is likely that the above-mentioned 421 differences arise as a result of deviations from the simplistic 422 Langmuir—Hinshelwood (adsorption—desorption) reaction 423 assumed in single-crystal catalysts.

Interestingly, no change in the nanoparticle size was 425 observed by TEM or XRR after successive catalytic cycles. A 426 Student's t test performed over the nanoparticle size histograms 427 before and after reaction does not show statistically significant 428 differences, with a confidence level p < 0.05. This demonstrates 429 that nanoparticles trapped inside the pore systems exhibit high 430 stability and that the catalyst is potentially recyclable. Current 431 efforts are directed toward testing the long-term catalytic 432 activity of these nanocomposites.

A marked reactivity increase as the temperature increases is 434 observed in all of the experiments. Surprisingly, a marked 435 decrease in NO production is observed as the oxygen 436 proportion in the reactant mixture increases, contrary to what 437 was observed in previous experiments performed on platinum 438 single crystals.<sup>37</sup>

Absolute values for the turnover frequency (TOF, expressed 440 as product molecules formed per square centimeter per 441 second) were estimated following the same procedure as that 442 used for ammonia oxidation over single-crystal catalysts (see 443 refs 37 and 38). Interestingly, these values were found to be in 444 the  $10^{14}$ – $10^{15}$  s<sup>-1</sup> cm<sup>-2</sup> range, which is comparable to the ones 445 found for single-crystal experiments. The applied TOF 446 calculation procedure makes use of the collision frequency, as 447 derived from kinetic gas theory, and assumes that the surface 448 density of catalytically active sites is equal to the number of 449 metallic surface atoms exposed for a certain crystallographic 450 orientation. Despite the uncertainty of these two factors 451 introduced because of the rugosity of the mesoporous support, 452 the nonuniform size and spatial distribution, and the 453 polycrystallinity of the active Pt NPs (approximately 4.5% by 454 weight), the TOF estimations mentioned above constitute a 455 promising result regarding the catalytic activity of this new 456 material. Bearing in mind the limitations discussed, one can also 457 estimate the selectivity changes when the oxygen partial 458 pressure and temperature are increased. For the complete 459 parameter range explored, N2 remains the preferred product 460 and displays an almost constant TOF value as the oxygen 461 pressure is increased for the highest temperature tested (220 462 °C), as can be observed in Figure 3. Both NO and N<sub>2</sub>O 463 production, as measured via QMS signals, represent approx- 464 imately 40-50% of the molecular nitrogen production. For the 465 low end of the temperatures and oxygen pressures used, the 466 ratio (NO/N<sub>2</sub>O) remains near (1:1), and as higher temper- 467 atures and pressures are used, the selectivity shifts toward an 468 increase in NO production up to a ≈1:0.6 ratio. 469

#### CONCLUSIONS

In this work, a straightforward and reproducible method to 471 insert Pt NPs with potentially tunable catalytic activity within a 472 controlled mesoporous environment is presented. This method 473 is based on the tailored control of the mesopore surface. In the 474 first step, METAC<sup>+</sup> monomers readily adsorb onto the silica 475 surface, permitting the development of a short-chain polymer 476 preferentially within the pore volume. In the second step, the 477 platinum(IV) precursor anions adsorb onto the positively 478 charged surface, and an ensuing soft reduction method grants 479 the controlled formation of MNPs within the mesopores. The 480

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481 system presents high catalytic activity even at low temperatures 482 with low platinum loading (ca. 4.5% by mass), demonstrating 483 the high accessibility of the heterogeneous catalyst. An 484 anomalous partial selectivity toward NO is observed for the 485 first time, which can be attributed to a synergetic effect between 486 the nanoparticles and modified surface. This effect opens a path 487 toward the nanodesign of nanocomposite catalysts with highly controlled environments, in which the synergy of thoroughly 489 size- and function-controlled cavities can be tuned in order to 490 lower the reaction barriers and lead to sustainable catalysts by 491 design.

Ammonia oxidation over single-crystal and polycrystalline 492 493 platinum catalysts involves the formation of NO in an intermediate step. Whether NO desorbs as a final product or participates in further reaction steps depends on a number of 496 factors such as adsorption energies (i.e., the number and type of surface sites available in the catalyst), reactant partial pressures, 498 and coverage of other adspecies (specifically O-ads). In this preliminary study, we have observed a considerable reduction 500 of temperature for measurable catalytic activity, together with 501 an increase in the N2O proportion on the products. This 502 illustrates that the hybrid/nanocomposite materials presented 503 here have a great potential to tune the catalytic properties of 504 confined Pt NPs in order to achieve different reaction products. 505 We attribute the observed selectivity shift toward NO 506 production to be closely related to an increment of the oxygen 507 supply to the reaction system generated by the polymer support 508 of Pt NPs. We anticipate that engineering different pore sizes or 509 changing the polymer nature or amount within the mesopores 510 will result in different particle densities and particle-matrix 511 interactions. The systematic exploration of nanoparticle 512 confinement and interactions with tailored hybrid mesoporous 513 matrixes and its consequences in the catalytic activity will bring 514 out further insight that can be used in a rational fashion for 515 novel catalyst design.

#### ASSOCIATED CONTENT

#### 517 S Supporting Information

518 FTIR and XRR patterns of hybrid and platinum-laden 519 mesoporous thin films and a representative FE-SEM top-view 520 micrograph of a platinum-loaded polymer-silica film. This 521 material is available free of charge via the Internet at http:// 522 pubs.acs.org.

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- 527 Notes
- 528 The authors declare no competing financial interest.

#### **ACKNOWLEDGMENTS**

530 This work was partially carried out at Leibniz University 531 Hannover by the Prof. R. Imbihl research group. M.R. gratefully 532 acknowledges valuable discussions and financial support 533 received from Deutsche Akademischer Austauschdienst, 534 CONICET, the Max Planck Society, ABTLuS (for access to 535 LNLS beamlines SAXS2 and XRD2), and UNSAM and 536 ANPCyT (Grants PICT 2010-0026, 2008-1848, and PICT-537 PRH 163/08). M.C.F., M.R., O.A., and G.J.A.A.S.-I. are 538 CONICET staff members. Dr. P. Bozzano and G. Zbihlei

(CNEA) are thanked for the TEM images, and Dr. G. Ybarra 539 (INTI) is gratefully acknowledged for FTIR measurements.

#### REFERENCES

- (1) Surface and Nanomolecular Catalysis; Richards, R., Ed.; CRC 542 Press: Boca Raton, FL, 2006.
- (2) Nanocatalysis; Heiz, U., Landman, U., Eds.; Springer-Verlag: 544 Heidelberg, Germany, 2006. 545
- (3) Nanoparticles and Catalysis; Astruc, D., Ed.; VCH-Wiley: 546 Weinheim, Germany, 2007.
- (4) Catalysis and Electrocatalysis at Nanoparticle Surfaces; Wieckowski, 548 A., Savinova, E. R., Vayenas, C. G., Eds.; Marcel Dekker: New York, 549 550
- (5) Nanotechnology in Catalysis; Zhou, B., Hermans, S., Somorjai, G. 551 A., Eds.; Springer Science: New York, 2004; Vol. 1.
- (6) For example, see the special issue Functional Porous Materials: 553 Luque, R.; Garcia-Martinez, J. ChemCatChem 2013, 5 (4), 825-1031. 554 (7) Centi, G.; Perathoner, S. Coord. Chem. Rev. 2011, 255, 1480-555 556
- (8) Díaz, U.; Brunel, D.; Corma, A. Chem. Soc. Rev. 2013, 42, 4083-557 4097.
- (9) Huang, S.; Hara, K.; Fukuoka, A. Energy Environ. Sci. 2009, 2, 559 1060 - 1068560
- (10) Jiang, C.; Hara, K.; Fukuoka, A. Angew. Chem., Int. Ed. 2013, 52, 561 6265 - 6268
- (11) Wen, C.; Zhu, Y.; Ye, Y.; Zhang, S.; Cheng, F.; Liu, Y.; Wang, P.; 563 Tao, F. ACS Nano 2012, 6, 9305-9313. 564
- (12) Rioux, R. M.; Song, H.; Hoefelmeyer, J. D.; Yang, P.; Somorjai, 565 G. A. J. Phys. Chem. B 2005, 109, 2192-2202.
- (13) Datta, K. K. R.; Reddy, B. V. S.; Ariga, K.; Vinu, A. Angew. 567 Chem., Int. Ed. 2010, 49, 5961-5965. 568
- (14) Fukuoka, A.; Kimura, J.-I.; Oshio, T.; Sakamoto, Y.; Ichikawa, 569 M. J. Am. Chem. Soc. 2007, 129, 10120-10125.
- (15) Huang, T.; Tu, W. Appl. Surf. Sci. 2009, 255, 7672-7678.
- (16) Prashar, A. K.; Mayadevi, S.; Rajamohanan, P. R.; Nandini Devi, 572 R. Appl. Catal., A **2011**, 403, 91–97.
- (17) Zhu, J.; Xie, X.; Carabineiro, S. A. C.; Tavares, P. B.; Figueiredo, 574 J. L.; Schomäcker, R.; Thomas, A. Energy Environ. Sci. 2011, 4, 2020-575
- (18) Song, H.; Rioux, R. M.; Hoefelmeyer, J. D.; Komor, R.; Niesz, 577 K.; Grass, M.; Yang, P.; Somorjai, G. A. J. Am. Chem. Soc. 2006, 128, 578 3027 - 3037.
- (19) Witham, C. A.; Huang, W.; Tsung, C.-K.; Kuhn, J. N.; Somorjai, 580 G. A.; Toste, F. D. Nat. Chem. 2010, 2, 26-41.
- (20) Kuhn, J. N.; Huang, W.; Tsung, C.-K.; Zhang, Y.; Somorjai, G. 582 A. J. Am. Chem. Soc. 2008, 130, 14026-14027.
- (21) Gutiérrez, L.-F.; Hamoudi, S.; Belkacemi, K. Catalysts 2011, 1, 584 97 - 154.
- (22) Yang, C.-M.; Liu, P.-H.; Ho, Y.-F.; Chiu, C.-Y.; Chao, K.-J. 586 Chem. Mater. 2003, 15, 275-280.
- (23) Brunsen, A.; Díaz, C.; Pietrasanta, L. I.; Yameen, B.; Ceolín, M.; 588 Soler-Illia, G. J. A. A.; Azzaroni, O. Langmuir 2012, 38, 3583-3592. 589
- (24) Brunsen, A.; Cui, J.; Ceolín, M.; del Campo, A.; Soler-Illia, G. J. 590 A. A.; Azzaroni, O. Chem. Commun. 2012, 48, 1422-1424.
- (25) Calvo, A.; Yameen, B.; Williams, F. J.; Soler-Illia, G. J. A. A.; 592 Azzaroni, O. J. Am. Chem. Soc. 2009, 131, 10866-10868.
- (26) Calvo, A.; Yameen, B.; Williams, F. J.; Azzaroni, O.; Soler-Illia, 594 G. J. A. A. Chem. Commun. 2009, 2553-2555. 595
- (27) Azzaroni, O.; Soler-Illia, G. J. A. A. Chem. Soc. Rev. 2011, 40, 596 1107 - 1150.
- (28) Calvo, A.; Fuertes, M. C.; Yameen, B.; Williams, F. J.; Azzaroni, 598 O.; Soler-Illia, G. J. A. A. Langmuir 2010, 26, 5559-5567.
- (29) Chilton, T. H. In The manufacture of nitric acid by the oxidation 600 of ammonia; Chemical Engineering Progress Monograph Series; 601 American Institute of Chemical Engineers: New York, 1960; Vol. 602 603
- (30) Novell-Leruth, G.; Ricart, J. M.; Pérez-Ramírez, J. J. Phys. Chem. 604 C 2008, 112, 13554-13562.

- (31) Offermans, W. K.; Jansen, A. P. J.; van Santen, R. A.; Novell-
- 607 Leruth, G.; Ricart, J. M.; Pérez-Ramírez, J. J. Phys. Chem. C 2007, 111, 608 17551-17557.
- (32) Offermans, W. K.; Jansen, A. P. J.; van Santen, R. A. Surf. Sci. 609 610 **2006**, 600, 1714-1734.
- (33) Rafti, M.; Lovis, F.; Imbihl, R. Catal. Lett. 2012, 142, 16-21.
- (34) Rafti, M.; Uecker, H.; Lovis, F.; Krupennikova, V.; Imbihl, R. 612
- 613 Phys. Chem. Chem. Phys. 2012, 14, 5260-5264.
- (35) Imbihl, R.; Scheibe, A.; Zeng, Y. F.; Günther, S.; Kraehnert, R.;
- 615 Kondratenko, V. A.; Baerns, M.; Offermans, W. K.; Jansen, A. P. J.; van 616 Santen, R. A. Phys. Chem. Chem. Phys. 2007, 9, 3522-3540.
- 617 (36) Imbihl, R.; Scheibe, A.; Lins, U. Surf. Sci. 2005, 577, 1-14.
- (37) Bogicevic, A.; Hass, K. C. Surf. Sci. Lett. 2002, 506, L237-L242.
- (38) Kraehnert, R.; Baerns, M. Chem. Eng. J. 2008, 137, 361-375. 619
- (39) Ravishankara, A. R.; Daniel, J. S.; Portmann, R. W. Science 2009, 620 621 326, 123-125.
- (40) Calvo, A.; Angelome, P. C.; Sanchez, V. M.; Scherlis, D. A.;
- 623 Williams, F. J.; Soler-Illia, G. J. A. A. Chem. Mater. 2008, 20, 4661.
- (41) Huang, W.; Skanth, G.; Baker, G. L.; Bruening, M. L. Langmuir 624 625 **2001**, 17, 1731.
- (42) Rafti, M.; Lovis, F.; Zeng, Y. F.; Imbihl, R. Chem. Phys. Lett. 627 2007, 446, 323-328.
- (43) Boissière, C.; Grosso, D.; Lepoutre, S.; Nicole, L.; Brunet-628
- 629 Bruneau, A.; Sanchez, C. Langmuir 2005, 21, 12362.
- (44) Fuertes, M. C.; Marchena, M.; Marchi, M. C.; Wolosiuk, A.; 631 Soler-Illia, G. J. A. A. Small 2009, 5, 272-280.
- (45) Kim, M.; Pratt, S. J.; King, D. A. J. Am. Chem. Soc. 2000, 122, 632 633 2409-2410.
- 634 (46) Bradley, J. M.; Hopkinson, A.; King, D. A. J. Phys. Chem. 1995, 635 99, 17032-17042.
- 636 (47) Guthrie, W. L.; Sokol, J. D.; Somorjai, G. A. Surf. Sci. 1982, 109, 637 390-418.