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# Packed Bed Reactor Technology for Chemical-Looping Combustion

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PRESENTATION - 18

# Packed Bed Reactor Technology for Chemical-Looping Combustion

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# Packed Bed Reactor Technology for Chemical-Looping Combustion

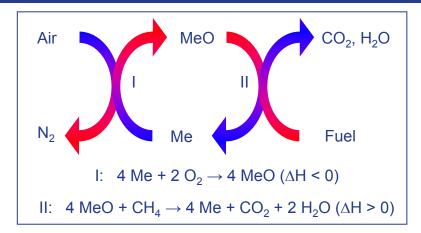
S. Noorman, M. van Sint Annaland, J.A.M. Kuipers (UT)
N.A.M. ten Asbroek, P.H.M. Feron (TNO)



2<sup>nd</sup> IEAGHG Oxyfuel Combustion Workshop 25<sup>th</sup> and 26<sup>th</sup> of January 2007, Windsor, USA



# **Chemical-looping Combustion**

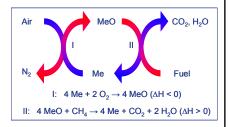


- Power production with inherent CO<sub>2</sub> separation
- · Direct contact between air and fuel is avoided

2

#### Introduction

- Chemical-looping Combustion:
  - Potential for very high CO<sub>2</sub> capture efficiency
  - ➤ No energy penalty for separation
  - ➤ No NO<sub>x</sub> formation
  - Direct implementation in power plants is challenging



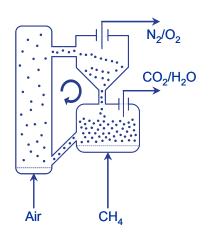
- Important research themes:
  - > Oxygen carrier (MeO = NiO, Fe<sub>2</sub>O<sub>3</sub>, Mn<sub>3</sub>O<sub>4</sub>, CuO)
  - > Implementation in power plant
  - Reactor concepts

Oxidizing and reducing conditions must be imposed alternately

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# **Reactor Concepts**

Recirculation or stationary solids?

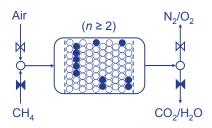


- Disadvantage of fluidization:
  - > Recirculation of particles
  - Difficult gas-solid separation (formation of fines)
- Packed bed (membraneassisted) CLC:
  - > Stationary solids
  - Periodic switching of gas streams
  - Dynamically operated parallel reactors (gas switching system)
  - ➤ Natural gas → combined cycle!

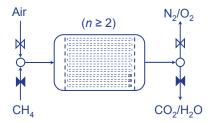
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#### **Packed Bed CLC**

· Packed bed CLC (UT):



 Packed bed membraneassisted CLC (TNO):



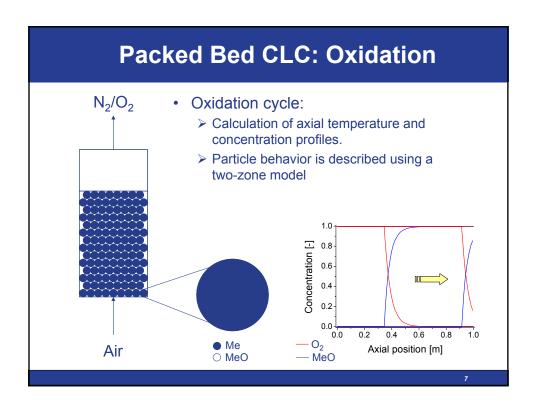
- Process demands:
  - ➤ Constant high-temperature air stream
  - ➤ High overall and CO₂ capture efficiency
  - > Continuous operation
  - > Extreme conditions (T<sub>out</sub> = 1300-1500 K, p = 20-30 bar)

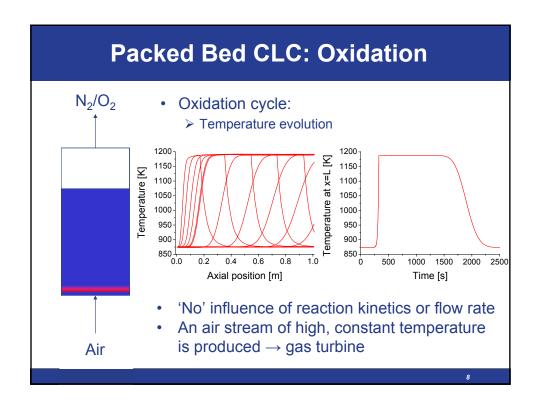
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# **Project Goal**

- Evaluation of the feasibility of packed bed CLC as an alternative power production technology:
  - Can CLC be carried out using packed bed (membraneassisted) technology?
  - ➤ How can packed bed CLC with an optimal overall energy efficiency be realized?
  - ➤ How does packed bed CLC perform, compared to fluidized bed CLC and other CO₂ capture processes?
- This presentation:
  - Modeling and experimental work on packed bed CLC.

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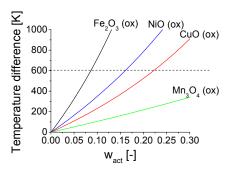


# **Oxygen Carrier Properties**

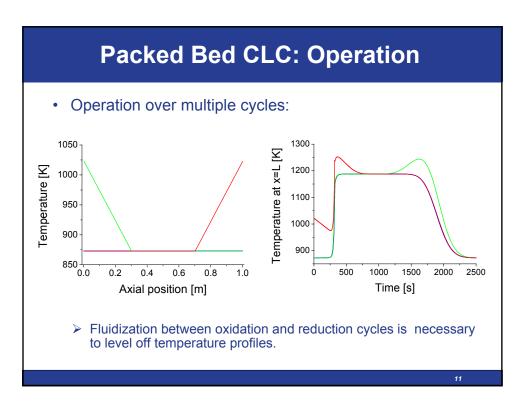
- · Analytical approximation:
  - ➤ Infinitely high reaction rate
  - ➤ No influence of conduction

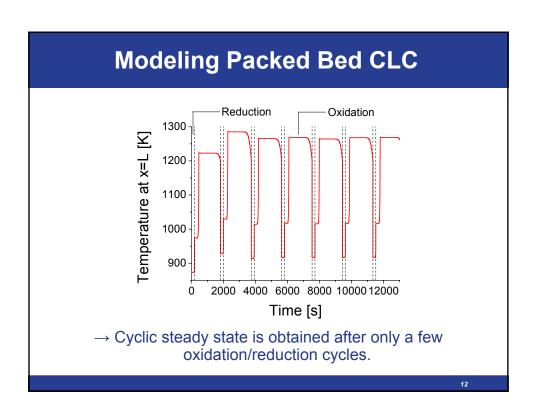
$$\Delta T = \frac{(-\Delta H_R)}{\frac{C_{p,s}M_{act}}{W_{act}}\xi} - \frac{C_{p,g}M_{O_2}}{W_{q,O_2}^{in}}$$

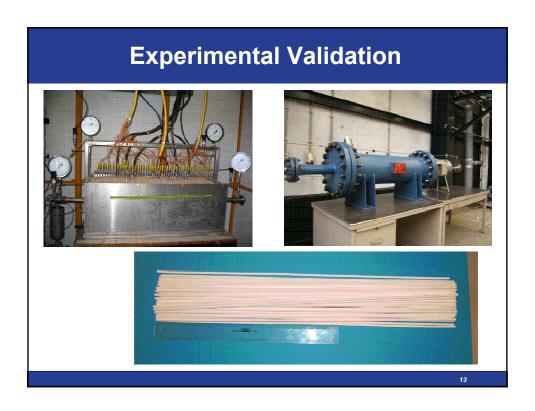
- Temperature increase can be tuned:
  - > Active content
  - Support material
  - Oxygen concentration

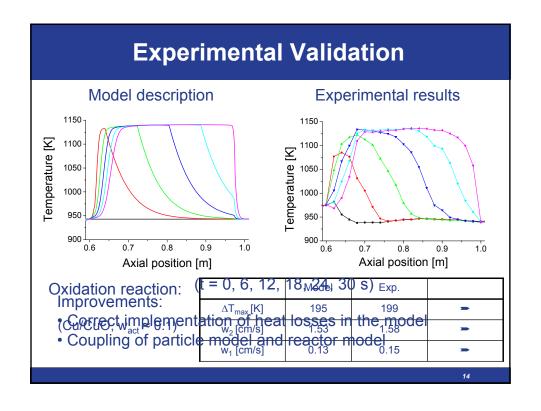


**Packed Bed CLC: Reduction** CO<sub>2</sub>/H<sub>2</sub>O Reduction cycle: > Efficient use of fuel ➤ High CO₂ capture efficiency ➤ Selectivity to CO₂ and H₂O Incomplete regeneration of part of the bed 1.0 MeO Concentration [-] 0.8 0.6 0.4 0.2 0.0 0.0 MeO 0.4 0.6 8.0 CH₄ Axial position [m]



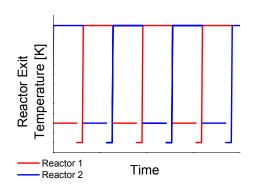






# **Implementation**

- Implementation in power plant:
  - ➤ Combined cycle to maximize overall energy efficiency
- · Process design:
  - > Pressure drop
  - > Number of reactors
  - Reactor sizing
  - > Heat integration, etc.
- Important features:
  - Compact design
  - Suitable for part-load operation



15

### **Conclusions**

- Packed bed (membrane-assisted) CLC is an interesting alternative power production technology:
- Process operation:
  - > Oxidation cycle: generation of high temperature air stream
  - ➤ Reduction cycle: combining efficient use of fuel and high CO₂ capture efficiency
- Implementation in power plant:
  - > Combined cycle
- Future work:
  - Experimental validation of packed bed CLC
  - > Process design and efficiency calculations

1