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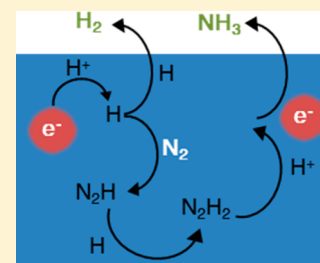
Mechanism of N<sub>2</sub> Reduction to NH<sub>3</sub> by Aqueous Solvated Electrons

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## S Supporting Information

**ABSTRACT:** Recently a novel approach to the photocatalytic reduction of molecular nitrogen under ambient conditions was reported in which hydrated electrons generated from ultraviolet illumination of diamond served as the reducing agent [Zhu, D.; Zhang, L.; Ruther, R. E.; Hamers, R. J. Photo-Illuminated Diamond as a Solid-State Source of Solvated Electrons in Water for Nitrogen Reduction. *Nat. Mater.* 2013, 12, 836–841]. This surprising reduction of N<sub>2</sub> by aqueous solvated electrons is absent from the vast existing radiolysis literature and thus has little mechanistic precedent. In this work, a combination of experimental and computational approaches is used to elucidate the detailed molecular-level mechanistic pathway from nitrogen to ammonia. A variety of approaches, including electronic structure calculations, molecular dynamics simulations, kinetic modeling, and pH-dependent experimental measures of NH<sub>3</sub> and competing H<sub>2</sub> production, implicate a hydrogen atom addition mechanism at early reduction steps and sequential protonation/direct reduction by a solvated electron at later steps, thus involving both *direct* and *indirect* reactions with solvated electrons. This work provides a framework for understanding the possible application of solvated electrons as energetic reducing agents for chemically inert species under mild conditions.



## ■ INTRODUCTION

Reduction of molecular nitrogen is extremely challenging due to its stability and chemical inertness.<sup>1,2</sup> Nonetheless, reduction of N<sub>2</sub> (and similarly stable and challenging CO<sub>2</sub>) has attracted considerable attention due to the significant associated technological payoff. Although reduction of both N<sub>2</sub> and CO<sub>2</sub> are known to occur via a variety of different processes,<sup>2,3</sup> these processes often require complex biological enzymes,<sup>4–9</sup> harsh conditions (e.g., the Haber–Bosch process<sup>10</sup>), or inefficient electrochemical<sup>3,11–13</sup> and/or homo-<sup>2,3,14</sup> or heterogeneous<sup>10,15</sup> catalytic approaches.

Photocatalysis provides an alternative and particularly intriguing method for the reduction of inert species under ambient conditions. For reduction of N<sub>2</sub> in particular, this approach was first reported and subsequently improved using various modified forms of TiO<sub>2</sub>.<sup>16–23</sup> In general, photo-reduction of N<sub>2</sub> at surfaces is inefficient due to a combination of factors including weak adsorption of the inert reactant onto the surface under ambient conditions, the multielectron nature of the pathways to energetically accessible intermediates, and reoxidation of the intermediates and product by the holes in the deep-lying valence band of TiO<sub>2</sub> and other commonly used semiconductors.<sup>24</sup> Recently, Zhu, Hamers, and co-workers demonstrated the ability to reduce N<sub>2</sub> to NH<sub>3</sub> using hydrogen-terminated diamond as a source of photoemitted, and subsequently solvated, electrons.<sup>25</sup> Because hydrogen-terminated diamond has a negative electron affinity (NEA), the conduction band lies above the vacuum level,<sup>26</sup> and the main problems encountered with TiO<sub>2</sub> can be avoided; that is, while reduction via simple *photoexcitation* of the TiO<sub>2</sub> requires N<sub>2</sub> adsorption (along with associated ammonia reoxidation), *photoemission* occurs when hydrogen-terminated diamond is illuminated under deep ultraviolet (UV) light, eliminating the

need for N<sub>2</sub> adsorption onto a solid surface and thereby minimizing product oxidation when appropriately coupled to an oxidation half-cell. Furthermore, the conduction band of diamond in water lies at a reduction potential of about −5 V versus that of the normal hydrogen electrode (NHE). Thus, in aqueous solution, the illuminated diamond serves as a source of high energy hydrated electrons capable of reducing N<sub>2</sub>. While the yield is currently small (~1–10 μg), reduction of N<sub>2</sub> (as opposed to nitrogen-containing impurities) by photoemission was confirmed by isotope-labeled studies.<sup>25</sup>

The initial proof-of-concept studies of Zhu et al. demonstrated both formation of solvated electrons and reduction of N<sub>2</sub> to NH<sub>3</sub> but did not determine the mechanistic pathway leading to ammonia. Furthermore, while the existing radiolysis literature contains a vast number of known reactions of the solvated electron, reactions involving N<sub>2</sub> are completely absent!<sup>27</sup> Thus, the lack of a mechanistic hypothesis hinders both the prospects for optimization of the system as well as possible extensions to other challenging solution-phase reductions. In the present manuscript, a combination of experimental and computational techniques is used to elucidate the detailed mechanistic pathway leading from solvated electron to ammonia in N<sub>2</sub>-saturated aqueous solution. This system serves as a convenient case study for reduction of inert species, since reduction leads to a single primary product (ammonia), in contrast to the reduction of other inert species such as CO<sub>2</sub> where multiple reduced products may be isolated.<sup>3</sup> In particular, two key fundamental questions are addressed: (1) Does the solvated electron directly reduce N<sub>2</sub> (aq) to N<sub>2</sub><sup>−</sup> (aq),

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or does it first reduce some other aqueous species? (2) With what other processes does the desired reduction compete?

In considering the plausible mechanisms of  $\text{N}_2$  reduction by solvated electrons, it is profitable to first consider previously determined or postulated mechanisms of  $\text{N}_2$  reduction under other conditions. In the realm of heterogeneous catalysis, the Haber–Bosch process relies on both harsh conditions and a solid catalyst to dissociatively adsorb both  $\text{N}_2$  and  $\text{H}_2$ ; ammonia is then built from its atomic building blocks.<sup>28,29</sup> Since similar direct dissociation of  $\text{N}_2$  via a solvated electron is nearly inconceivable, the rate-limiting step must instead be *activation* of the N–N triple bond; this is demonstrated by the strongly unfavorable redox potential of converting  $\text{N}_2$  to  $\text{N}_2\text{H}$  (–3 V), which, in conjunction with subsequent steps, leads to an overall favorable 6 electron reduction potential (+ 0.55 V).<sup>2,15</sup>

Rather than cleaving the N–N bond, inorganic homogeneous catalysts begin the reduction process by weakening the bond for attack by a hydrogen source.<sup>2,15</sup> Similarly, one may hypothesize that the solvated electron may directly add to an antibonding  $\pi^*$  orbital of the  $\text{N}_2$  molecule to yield  $\text{N}_2^-$ , thus activating the bond for further reduction. Although  $\text{N}_2$  has a strongly unfavorable electron affinity in the gas phase, a crude estimate shows that this may be overcome via strong solvation of the nascent anion.<sup>30</sup> In enzymatic reactions, a strong coupling between electron transfer (ET) and proton transfer has been observed,<sup>5,31</sup> potentially even involving concerted proton-coupled ET (PCET). A similar mechanism could be conjectured in the present case, with the solvated electron and a water molecule serving as the electron and proton donors, respectively. While theoretical studies show that electrochemical  $\text{N}_2$  reduction may occur via a dissociative mechanism at the electrode surface, depending on the metal used for the electrode,<sup>32,33</sup> a hydrogen atom addition (HAA) may be likely in many cases as well,<sup>11</sup> where protons are first reduced at the cathode to H atom before adding to the  $\text{N}_2$ . Note that it is well known that hydrated electrons react rapidly with protons and very slowly with water in aqueous solution to form hydrogen atoms.<sup>27,34</sup> On the basis of the prior relevant mechanistic data under these diverse conditions, ET, PCET, and HAA are considered here to be the most likely candidates for reduction of  $\text{N}_2$  by solvated electrons.

We report here a comprehensive investigation into these possible mechanisms that implicates HAA at early reduction steps and sequential protonation/ET at later steps as the predominant pathway leading to ammonia. A new set of experiments are performed using an aqueous KI solution as a simpler and “cleaner” source of photoemitted hydrated electrons<sup>35</sup> (as compared to hydrogen-terminated diamond). This experimental setup confirms the contribution of *bulk* hydrated electrons to the reduction by removing any surface-dependent reactions and also allows for a study of the pH dependence of the reaction (which, in the case of diamond, could be complicated by pH-dependent changes in surface potentials or changes in the surface termination<sup>36,37</sup>). For the first time, the associated (and competing)  $\text{H}_2$  yield is also observed. A conclusive mechanistic pathway is elucidated from this new set of experiments in conjunction with a diverse set of computational approaches involving electronic structure calculations, molecular dynamics (MD) simulations, and kinetic modeling.

## METHODS

**Experimental Section.** A sample solution (10 mL) was prepared from 18.2 M $\Omega$  water and 0.1 mmol KI buffered by a  $\text{Na}_2\text{HPO}_4$ – $\text{NaH}_2\text{PO}_4$  system at the indicated pH with a total concentration of 8 mM. For pH 3 and 4 samples,  $\text{H}_3\text{PO}_4$  was also added to adjust the pH. Then the sample solution, contained in a quartz vessel, was degassed using a vacuum line, followed by 50 sccm  $\text{N}_2$  (99.999999% purity) purging for 3 h to ensure a saturated solution for the photochemical reaction. All chemicals involved are in 99.99% trace metal basis purity. Photochemical experiments were performed using a high-pressure mercury lamp (Driel Instrument, model 66921), located approximately 10 in. from the samples, for typically 11 h. A water-absorptive filter was used to eliminate infrared (IR) radiation and UV radiation below 200 nm. The production of ammonia was measured using a high-performance ammonia ion selective electrode (Orion 9512HPBNWP). Gas-phase products, especially hydrogen gas, were determined by gas chromatography–thermal conductivity detection (GC-TCD) (Shimadzu GC-8A), with  $\text{N}_2$  as the carrier gas. A colorimetric method<sup>38</sup> was used to measure the iodine (in the form of triiodide) concentration; the ultraviolet–visible (UV–vis) spectrum of the sample solution was taken right after reaction using a Shimadzu 2401PC UV–vis spectrophotometer. The absorbance at 351 nm was calibrated with known concentration samples as standards. Blank tests, including a dark control and an argon purging control (replacing  $\text{N}_2$  with Ar), were conducted to rule out potential false results from contamination.

**Kinetic Model.** To perform a kinetic analysis of the known and possible reactions in solution, the Gepasi software package<sup>39</sup> was used to model the dynamics of a set of the most important (and well-characterized) reactions that are known to occur in the hydrated electron solution, taken from Table 2 in the review on solvated electron kinetics by Buxton et al.<sup>27</sup> Every reaction with a reported reliable measurement was considered. However, the extremely slow reaction of H atoms with water to produce  $\text{H}_2$  has been significantly revised since Buxton’s review, and the more recent rate constant for this reaction ( $4.4 \times 10^{-5} \text{ M}^{-1} \text{ s}^{-1}$ ) was used.<sup>34</sup> Also, the reaction of the buffer  $\text{H}_2\text{PO}_4^-/\text{HPO}_4^{2-}$  with solvated electron to produce H atom was included.<sup>27</sup> In addition, no reactions involving  $\text{O}_2^{2-}$  were reported in this review, but by a Gaussian-4 (G4) and polarizable continuum model (PCM) thermodynamic analysis described below,  $\text{O}_2^{2-}$  reacts very exothermically with water to form  $\text{HO}_2^-$  and  $\text{OH}^-$  ( $\Delta H_r = -20$  kcal/mol,  $\Delta H_{r,\text{gas}} = -137$  kcal/mol). Thus, it is assumed that  $\text{O}_2^{2-}$  reacts with water with a diffusion-limited rate constant ( $k_{\text{diff}} = 3 \times 10^{10} \text{ M}^{-1} \text{ s}^{-1}$ ).

To estimate the concentration of solvated electron in solution, the rate of production of solvated electron is estimated from the experimental setup ( $\text{I}^- + h\nu \rightarrow \text{I} + \text{e}^-$ , with a first-order rate constant of  $k_{\text{prod}} = 4 \times 10^{-6} \text{ s}^{-1}$ ). This rate constant was obtained by first integrating the irradiance of the light source<sup>40</sup> over the wavelengths above which the glass is transparent and below which electrons will be detached from iodide (200–254 nm) and then multiplying by the cross-section of the reaction vessel (12.8 cm<sup>2</sup>) and the quantum efficiency (QE) of creating solvated electrons from iodide. The measured QE of 0.3 (at 248 nm) was assumed for all wavelengths since the QE increases only modestly to 0.5 by 193 nm.<sup>41</sup> The transmittance is expected to be less than  $10^{-4}$ , on

the basis of the high molar absorptivity ( $885 \text{ M}^{-1} \text{ cm}^{-1}$ ),<sup>41</sup> path length (2.5 cm), and iodide concentration (0.010 M); thus, it is assumed that all of the photons between 200 and 254 nm are absorbed by the sample. The value used for the quantum yield of solvated electrons includes primary geminate recombination,<sup>41</sup> but a rate for secondary recombination due to diffusion of iodine atoms and solvated electrons in solution must be considered. Since it is a radical reaction, it is reasonable to assume that this rate is diffusion-limited ( $\text{I} + \text{e}^- \rightarrow \text{I}^-$ ;  $k_{\text{rec}} = k_{\text{diff}}$ ). A comprehensive list of all reactions used in the kinetic model and their corresponding rate constants is provided in the Supporting Information.

The initial concentrations of all species were set to zero except water (55.5 M, fixed),  $\text{H}^+$  and  $\text{OH}^-$  (fixed according to the appropriate pH),  $\text{H}_2\text{PO}_4^-$  and  $\text{HPO}_4^{2-}$  (set to the buffer concentration at the appropriate pH),  $\text{O}_2$  (100 nM, a reasonable upper bound for the amount present in the degassed water),  $\text{I}^-$  (0.01 M), and  $\text{N}_2$  (0.6 mM). Once the appropriate set of reactions with  $\text{N}_2$  were added, the Gepasi program was used to integrate the set of coupled differential equations over 11 h.

**Gas-Phase Thermochemistry.** Gas-phase transition states were located using density functional theory (DFT) with the  $\omega\text{B97X-D}^{42}$  functional with a 6-311++G(d,p) basis set as implemented in the Gaussian 09 software package.<sup>43</sup> The transition states were verified as saddle points via a frequency analysis. The one imaginary frequency was followed using the intrinsic reaction coordinate (IRC) method to verify that the two minima connected by the saddle point were the reactant and product states. The activation and reaction energies were then determined from single point calculations of the stationary points using CCSD(T) in conjunction with the triple- $\zeta$  correlation-consistent Dunning-style basis set augmented with diffuse functions (aug-cc-pVTZ). Free energies were obtained from frequency calculations of the stationary points, also at the CCSD(T)/aug-cc-pVTZ level of theory; however, the change in the gas-phase translational entropy was subtracted out and replaced by the cratic entropy ( $\sim 4\text{R}$ ) to estimate the solution-phase entropy change.<sup>44,45</sup> Where noted, the Gaussian-4 (G4) composite method<sup>46</sup> as implemented in Gaussian 09 was used to estimate thermochemical data, and enthalpies of solvation were estimated using the PCM.<sup>47</sup> For the latter calculations, DFT was used with the B3LYP functional and the 6-311++G(d,p) basis set.

**Marcus Theory.** Marcus theory<sup>48,49</sup> was used to estimate the barrier for ET from solvated electron to  $\text{N}_2$  to form  $\text{N}_2^{\cdot-}$  (aq). The details have been laid out numerous times before;<sup>48–50</sup> discussed here are the important aspects for the current application of Marcus theory. Of particular importance is the fact that in this case, the electron donor is a solvated electron and is therefore not present in the product diabatic state. Hence the two diabatic states are  $\text{N}_2 \cdots \text{e}^-$  and  $\text{N}_2^{\cdot-}$ .

The difference in the internal energy between the two diabatic states is simply the electron affinity  $A$  of  $\text{N}_2$ . It is estimated that  $A = -61 \text{ kcal/mol}$  (Bauer crudely estimates that  $A \geq -63 \text{ kcal/mol}$ <sup>30</sup> from experimental data). The solvent interacts with each state in a way that depends on the solvent configuration, whose coordinates can be represented by a collective variable  $\xi$ . The reaction coordinate  $\Delta\epsilon(\xi)$  is a collective solvent “energy gap” coordinate which is chosen to reflect the fact that the ET is driven by solvent fluctuations that provide stable solvation of the product state. It is often reasonable to assume linear solvent response to perturbations

about the equilibrium, which gives rise to a simple expression for the activation free energy in terms of the free energy of reaction and the reorganization energy.<sup>49–52</sup> However, assuming linear solvent response may not be a good approximation in the case under current investigation where the electron donor is an electron with no associated nucleus; that is, the product state contains only one cavity in the solvent, whereas the reactant state contains two. For this reason, the free energy curves of the diabatic states were estimated along the entire reaction coordinate using biased sampling.

To generate the free energy as a function of the reaction coordinate, the solvent was considered explicitly, and Marcus theory was used to interpret a series of MD simulations. The simple point charge (SPC) water model<sup>53</sup> was used to describe the solvent; the Lennard-Jones (LJ) parameters for  $\text{N}_2$  placed on the nitrogen atoms were taken from the all-atom transferable potentials for phase equilibria (TraPPE) force field<sup>54</sup> and used to describe the nitrogen–water interaction using the geometric mean of the individual parameters for the mixed parameters. For  $\text{N}_2^{\cdot-}$ , the same LJ parameters were used as for  $\text{N}_2$ , and a partial charge of  $-0.5$  was placed on each N atom. The pseudopotential developed by Schnitker and Rossky<sup>55</sup> was used in its corrected form<sup>56,57</sup> to describe the electron–water interaction. The solvated electron was treated using a path integral approach<sup>58</sup> where the electron is represented by a closed ring composed of a number  $P$  of classical beads. Convergence with respect to the number of beads of the electron–oxygen and electron–hydrogen radial distribution functions and the electron radius of gyration was achieved by 200 beads, and the results were identical within statistical uncertainty to the quantum results presented previously,<sup>56</sup> so  $P = 200$  was used. Once the solvated electron–water system had been equilibrated, a representative configuration of the electron beads was taken and used for the Marcus theory simulations, with the positions of the beads fixed. This was done for several configurations with negligible changes in the activation barrier, demonstrating that sampling over additional configurations of the electron beads is unnecessary. The electron–nitrogen interaction was neglected because for a given calculation of the ET barrier, the electron–nitrogen distance was fixed during the course of the simulation.

To determine a reasonable range of distances over which the  $\text{N}_2$  and solvated electron could interact, a crude  $\text{N}_2$ –electron repulsive potential was used to compute a potential of mean force (PMF) for separating the two species. Details are provided in the Supporting Information.

As validation that these particular models for the electron–water and the  $\text{N}_2^{\cdot-}$ –water interactions will give a reasonable estimate of the solvation effects in the ET reaction, the difference in hydration enthalpy between the  $\text{N}_2^{\cdot-}$  and solvated electron is considered. The experimental value for the hydration enthalpy of the solvated electron is about  $-30$  to  $-34 \text{ kcal/mol}$ .<sup>59,60</sup> While no such corresponding value for  $\text{N}_2^{\cdot-}$  exists, it is reasonable to assume that it should be in the same range as that of a medium-sized halide (about  $-70$  to  $-90 \text{ kcal/mol}$ ),<sup>61</sup> significantly less negative than that of  $\text{OH}^-$  (about  $-120 \text{ kcal/mol}$ ).<sup>61</sup> Given that both experimental and theoretical methods for determining ion enthalpies of hydration are questionable, the relative value for  $\text{N}_2^{\cdot-}$  compared to solvated electron is much more reliable. Experimental values for  $\Delta H_{\text{hyd}}(\text{e}^-) - \Delta H_{\text{hyd}}(\text{OH}^-)$  and  $\Delta H_{\text{hyd}}(\text{e}^-) - \Delta H_{\text{hyd}}(\text{I}^-)$  are 86 and 33 kcal/mol, respectively.<sup>62</sup> The present theoretical model’s prediction for  $\Delta H_{\text{hyd}}(\text{e}^-) - \Delta H_{\text{hyd}}(\text{N}_2^{\cdot-})$  is 59 kcal/



mol, which reasonably lies between the two values. While less reliable absolute calculated values for  $\Delta H_{\text{hyd}}(\text{e}^-)$  and  $\Delta H_{\text{hyd}}(\text{N}_2^-)$  may indicate oversolvation in each case (−58 kcal/mol and −117 kcal/mol, respectively), the reasonable relative hydration value indicates that the ET barrier will be reasonably predicted to the desired accuracy, given the extremely high barrier predicted (see Results and Discussion sections).

Biased sampling was used so that solvent configurations all along the reaction coordinate were sampled. This was done by scaling the potential due to the nitrogen–electron system between the reactant and product diabatic states, similar to the procedure that Kuharski et al. used for modeling aqueous ferrous–ferric ET.<sup>52</sup> Details and a typical set of free energy curves are provided in the Supporting Information.

All of the MD simulations were run using a version of TINKER 5.0<sup>63</sup> that was locally modified to incorporate the ability to treat the electron using the path integral approach. Each simulation was run for 150 ps (following 50 ps of equilibration) with a 1.0 fs time step in the number–volume–temperature (NVT) ensemble at 298 K at the appropriate density for pure water ( $N = 216$  water molecules in a cubic box with sides of length 18.6258 Å, corresponding to 1.00 g/cm<sup>3</sup>). Periodic boundary conditions were applied with nonelectrostatic interactions cut off at 9.0 Å. Electrostatic interactions were treated with the particle mesh Ewald (PME) summation with tin foil boundary conditions and a uniform background charge.<sup>64</sup> The Ewald cutoff for real space interactions was 9 Å, and the PME summation used a  $30 \times 30 \times 30$  charge grid and 8th-order B-spline interpolation. Snapshots along the trajectory were saved every 100 fs, and the appropriate property was averaged over all snapshots.

The rate constant  $k$  for ET was calculated from the activation free energy ( $\Delta G^\ddagger$ ) using<sup>65</sup>

$$k = \frac{2\pi}{\hbar} V^2 (4\pi\lambda k_B T)^{-1/2} \exp[-\beta\Delta G^\ddagger]$$

where  $V$  is the electronic coupling between the reactant and product states and is generously taken to be 10 meV to provide an upper bound for the estimated rate. In this expression for parabolic free energy curves,  $\lambda = G_2(x_1) - G_1(x_1) = G_1(x_2) - G_2(x_2)$  is the reorganization energy, where  $G_i(x_j)$  is the free energy of diabatic state  $i$  at the location along the reaction coordinate where the free energy of diabatic state  $j$  is a minimum. In the case where the curves are not parabolic, these two expressions are not necessarily equivalent. The expression that returned the smallest value of  $\lambda$  was used, so as to provide an upper bound for the rate constant. For the system presented here, the values differed by up to a factor of 4, corresponding to a difference of only a factor of 2 in the predicted rate, which is a trivial difference compared to the order-of-magnitude estimate obtained.

Preliminary results for the PCET barrier were calculated using the two-dimensional (2D) generalization of Marcus theory of Kobra and Hammes-Schiffer for an atomistic treatment of the solvent.<sup>66</sup> However, it was assumed that proton transfer in the presence of the  $\text{N}_2\cdots\text{e}^-$  complex was unimportant (since  $\text{N}_2\text{H}^+$  is unlikely to form in  $\text{N}_2$ -saturated water), resulting in a simpler sampling of the potential energy surfaces. In the 2D generalization of Marcus theory, 2 collective solvent coordinates are used to describe the reaction coordinate, one for ET and one for proton transfer. The proton transfer coordinate was approximated to be parabolic,

while the ET coordinate was sampled using the same biasing potential used for ET.

## RESULTS

Under UV illumination of the  $\text{N}_2$ -saturated aqueous KI solution, reduction of  $\text{N}_2$  gas to  $\text{NH}_3$  was observed in addition to production of hydrogen gas and the oxidized iodide in the form of molecular iodine. The observed yields of  $\text{NH}_3$ ,  $\text{H}_2$ , and  $\text{I}_2$  are presented in Table 1 for several pH values ranging from 2

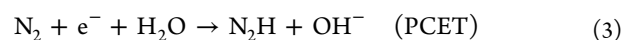
**Table 1. Observed pH Dependence of  $\text{NH}_3$  and  $\text{H}_2$  Yields (nmol) Compared to  $\text{I}_2$  Yield (nmol)**

pH	$\text{NH}_3$ yield	$\text{H}_2$ yield	expected $\text{I}_2$ yield <sup>a</sup>	$\text{I}_2$ yield
2.0	<LD <sup>b</sup>	575	575	562
3.0	3.2	349	354	339
4.0	3.6	226	231	244
4.6	6.9	208	218	231
5.0	8.2	183	195	213
6.0	6.6	202	212	187
7.0	3.2	231	236	228
8.0	2.5	173	177	217

<sup>a</sup>The expected  $\text{I}_2$  yield is the  $\text{H}_2$  yield added to three-halves of the  $\text{NH}_3$  yield. <sup>b</sup>Limit of detection (LD) is 2 nmol.

to 8. Throughout this manuscript, we refer to the product “yield” as the absolute amount produced under the experimental conditions and reaction times reported in the Methods section, consistent with the prior work of Zhu et al.<sup>25</sup> Higher pH conditions were not considered due to the dominance of the disproportionation reaction of  $\text{I}_2$  with  $\text{OH}^-$  under basic conditions.<sup>67</sup> The majority of the reduced product is  $\text{H}_2$ , accounting for most of the electrons lost by the oxidized  $\text{I}^-$ . Ammonia, by contrast, is a minor product with smaller yields than previously reported for the reduction by photo-emitted electrons from diamond; this may be due to a higher local solvated electron concentration induced in the vicinity of the diamond surface, potentially opening second-order (2 electron) reduction pathways. The good agreement between the measured  $\text{I}_2$  yield and the expected  $\text{I}_2$  yield (based on the measured  $\text{H}_2$  and  $\text{NH}_3$  yields) demonstrates that the majority of reduced products have been identified and quantified. On the basis of the experimental setup described above and the observed  $\text{I}_2$  yield, we estimate that the quantum yield (fraction of photons that result in a solvated electron that produces  $\text{NH}_3$  or  $\text{H}_2$ ) at pH 7 is  $4 \times 10^{-3}$ . Since the quantum yield of solvated electrons is 0.3, this indicates that the vast majority of solvated electrons ultimately recombine (directly or indirectly) with  $\text{I}$  atoms.

Because of the necessary activation of the inert N–N triple bond, the initial elementary reaction of  $\text{N}_2$  is likely to be rate limiting and thus demands considerable attention. As discussed above, we anticipate that the most likely initial elementary step is one of the following:



However, since the ammonia yields are currently very low, almost any thermodynamically favorable reaction that activates the N–N bond could be involved and should be considered;

even activation via oxidation by an  $O_2$  derivative may be plausible, given trace oxygen remaining in the degassed solution (e.g., rate-limiting oxidation to nitrate followed by subsequent reduction to ammonia). We therefore also consider the reaction of  $N_2$  with other low-concentration species that are generated by solvated electrons in water with nontrivial amounts of  $O_2$  (e.g., hydroxyl radical and hydrogen peroxide). To systematically enumerate *all* possible mechanisms, a list of all potential species in solution was constructed. The associated reaction enthalpy of each species with  $N_2$  was estimated from enthalpies of formation and solvation (see Tables S2–S4 in the Supporting Information), calculated using standard electronic structure methods (see Supporting Information for details on thermodynamic screening). Eight additional plausible reactions with favorable, or mildly unfavorable, enthalpies of reactions were found, involving reaction of  $N_2$  with 5 different reactants (Table S1 in the Supporting Information). However, all of these additional reactions were eliminated based on a combination of factors (i.e., highly improbable transition states, reactant's high reactivity with water, or an estimated upper bound on the reactant's equilibrium concentration); see Supporting Information for details. We thus consider reactions 1–3 as the only plausible initial mechanistic steps.

Reaction 2 initially seems implausible due to the highly unfavorable gas-phase electron affinity of  $N_2$ , estimated by thermodynamics,<sup>30</sup> electron scattering,<sup>68</sup> and theoretical calculations<sup>69</sup> to be between 50 and 60 kcal/mol. However, it has been shown that strong intermolecular interactions can be used to trap  $N_2^-$  even in the gas phase,<sup>70</sup> and thus strong solvation of  $N_2^-$  in water may make this reaction thermodynamically feasible. Assuming that the free energy of solvation of  $N_2^-$  lies between that of  $O_2^-$  (about  $-80$  kcal/mol)<sup>30</sup> and  $OH^-$  (about  $-100$  kcal/mol),<sup>71</sup> and given that the solvation free energy of the electron is about  $-40$  kcal/mol,<sup>59,60</sup> the solvent could stabilize the product of reaction 2 over its reactants by 40–60 kcal/mol, approximately sufficient to account for the unfavorable electron affinity. Thus, while  $N_2^-$  would certainly be a short-lived intermediate, subsequent reaction with water and/or protons would lead to more stable reduced species. PCET (reaction 3) then represents the extreme limit of *concerted* (rather than sequential) electron/proton transfer. We therefore consider all three potential reactions using a kinetic analysis.

The rates of the known reactions of solvated electron in aqueous solution<sup>27,34</sup> were used as input for a kinetic model whose resulting set of coupled differential equations was then integrated over the experimental UV illumination time. However, solution-phase rate constants for reactions 1–3 were still needed as input for the model. For reaction 1, the rate constant was estimated to be  $930\text{ M}^{-1}\text{ s}^{-1}$  from a gas-phase CCSD(T)/aug-cc-pVTZ calculation based on transition state theory (TST),<sup>1</sup>

$$k = \frac{k_B T}{h} e^{-\Delta G^\ddagger/k_B T}$$

where  $k_B$  is Boltzmann's constant,  $T$  is room temperature,  $h$  is Planck's constant, and  $\Delta G^\ddagger$  is the free energy of activation which was adjusted to estimate the solution-phase (rather than gas-phase) loss of translational entropy. The solution-phase barrier and corresponding rate constant for reaction 2 were estimated within the context of Marcus theory,<sup>48–50</sup> where the solvent was described explicitly in MD simulations. The rate constant for ET (reaction 2) was estimated from the Marcus

theory pseudo-first-order rate constant to be  $4 \times 10^{-6}\text{ s}^{-1}$ . Note that this rate constant is an electronic rate for a given (fixed) geometry and ignores the fact that the probability of obtaining that two-body geometry is much less than unity. Thus, it is an upper bound for the actual rate constant, ignoring mass transport. The barrier and corresponding rate constant for reaction 3 was considered in a similar manner but as a proton-coupled ET within the 2D extension of Marcus theory developed by Hammes-Schiffer and co-workers.<sup>66</sup> Only  $H_2O$  and not  $H^+$  (or  $H_3O^+$ ) was considered as the PCET proton donor, since the latter reacts extremely rapidly (diffusion limited) with a solvated electron to produce  $H$  atom. Preliminary results using  $H_2O$  as the proton donor indicated that the PCET barrier and the corresponding rate constant are both qualitatively similar to those for ET, as might be expected since one high-energy penalty (adding an electron to  $N_2$ ) is replaced by another (heterolytically cleaving a water O–H bond).

The activation free energies for these reactions are given in Table 2, along with the estimated yield of  $NH_3$  resulting from

**Table 2. Free Energies of Activation (kcal/mol) and Estimated Ammonia Yields (nmol) at pH 7.0 from the Kinetic Model, for HAA and ET**

rxn.	reactant	$\Delta G^{\ddagger}$	$NH_3$ yield <sup>a</sup>	equil. $NH_3$ yield <sup>b</sup>
1	H	13.4	360	4.6
2	$e^-$	24	$2.3 \times 10^{-7}$	
expt. $NH_3$ yield			3.2	

<sup>a</sup>Includes the activation barrier but excludes the reverse reaction.

<sup>b</sup>Includes both the activation barrier and the reverse reaction, assuming a thermoneutral reaction.

the kinetic model, assuming that every reaction with  $N_2$  ends in the desired product (and neglecting any reverse reaction). Comparing to the experimental yield at pH 7.0 of 3.2 nmol, reaction 1 (HAA) is the only feasible pathway, producing a yield near the same order of magnitude as (but considerably larger than) the experimental data, while ET exhibits negligible yields; this allows the elimination of direct ET and, because of the similar barriers, PCET processes as the initial reduction step.

However, while the HAA pathway is plausible, it does not provide a stable thermodynamic sink that can feed subsequent elementary steps. We thus consider the following two-step process,



yielding an activated, thermodynamically stable,  $N_2H_2$  intermediate that is presumably rapidly reduced to  $NH_3$ . Electronic structure calculations estimate that the free energy of 1a in the gas-phase is  $+8$  kcal/mol (which compares well to an experimental *enthalpy* of reaction of  $+6$  kcal/mol<sup>72</sup>). However, the dielectric constant of the solvent gives rise to a stabilization of the product estimated at  $\sim 3$  kcal/mol using PCM solvation. Explicit hydrogen bonding of  $N_2H$  with water will further stabilize the product; gas-phase calculations estimate that the strength of the hydrogen bond between  $N_2H$  and one water molecule is  $\sim 5$  kcal/mol. We thus assume an overall thermoneutral reaction, resulting in a rate constant for the reverse reaction of  $930\text{ M}^{-1}\text{ s}^{-1}$  as determined by detailed

balance. In contrast, reaction 1b is very exothermic ( $\Delta H_r = -63$  kcal/mol from the G4 electronic structure calculations); therefore,  $N_2H_2$  provides a stable thermodynamic sink for the further facile reduction to  $NH_3$ . This subsequent step is assumed to proceed with a diffusion-limited rate constant in the kinetic model; the result is shown in the last column of Table 2, with a predicted  $NH_3$  yield of 4.6 nmol, quite close to the observed value of 3.2 nmol.

## DISCUSSION

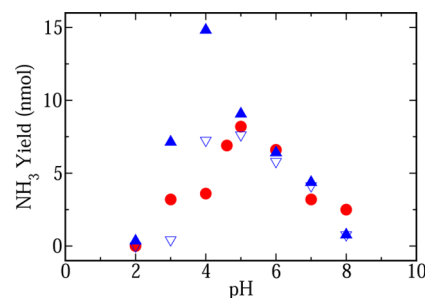
On the basis of these analyses, it appears likely that the mechanism for aqueous  $N_2$  reduction to  $NH_3$  by solvated electron proceeds by H atom addition through both  $N_2H$  and  $N_2H_2$  intermediates. Note that this conclusion has been drawn from the kinetic model by neglecting any potential photochemical effects. The continuous illumination of the sample under the UV light may affect any intermediate along the reaction path from  $N_2$  to  $NH_3$ . The most likely effect of the light seems to be photolysis of water from the deep UV light that is not absorbed by the quartz reaction vessel; most, but not all, of this has been filtered out by a water bath in front of the sample.

However, the H atom addition mechanism alone does not explain the experimental observation that the  $NH_3$  yield decreases and eventually shuts off as the pH is decreased (see Table 1). Thus, the initial H addition to  $N_2$  cannot be rate limiting at low pH. Otherwise, as the pH decreases, H concentration should increase (due to solvated electrons reacting with the increased number of protons), and production of  $N_2H_2$  (and therefore  $NH_3$ ) should also increase, in contrast to experimental observations.

A resolution comes from considering subsequent reduction steps involving expected partially reduced intermediates, such as diazene ( $N_2H_2$ ) or hydrazine ( $N_2H_4$ ), which also have been posited as intermediates in the photocatalytic reduction at semiconductor surfaces.<sup>73</sup> In particular, the latter is almost always protonated under the experimental conditions ( $pK_a = 8.0^{69}$ ), yielding  $N_2H_5^+$ . Electronic structure calculations estimate that the protonated species has a solution-phase electron affinity of approximately +3 kcal/mol, allowing for reaction with a solvated electron, and yielding a reduced neutral species, and eventually  $NH_3$ . In contrast, these same electronic structure methods suggest a substantial barrier to direct H atom addition to hydrazine (approximately 5 kcal/mol). Thus the predominant pathway for later reduction is expected to consist of *sequential* protonation and direct reduction by solvated electron. At low pH, this process will be hindered by the very low steady-state concentrations of solvated electron (since they rapidly react with protons), while at higher pH values (4–7), there are sufficient solvated electrons available such that these later steps are not rate-limiting. A similar argument could also be made for diazene (gas-phase barrier to H addition of 2 kcal/mol, solution-phase proton affinity of +6 kcal/mol,  $N_2H_3^+$  solution-phase electron affinity of -72 kcal/mol) or for any other intermediates between  $N_2H_2$  and  $NH_3$  that are expected to have a high  $pK_a$ .

This conclusion is supported by the kinetic model. To incorporate this effect,  $N_2H_2$  is assumed to react with solvated electrons with a diffusion-limited rate constant to produce  $NH_3$  (although, in practice, this must occur via a series of elementary steps). Anywhere from one to four steps involving direct electron addition (as opposed to H atom addition) could be involved. Data for including both two and four direct ET steps

are presented in Figure 1, and the general shape of the pH dependence is captured well in both cases. The discrepancies

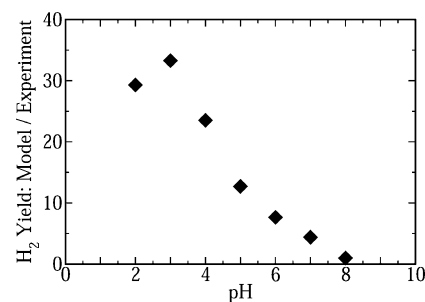


**Figure 1.** pH dependence of ammonia yield from the kinetic model with 2 (closed triangles, ▲) and 4 (open triangles, ▽) direct ET steps. Yields from experiment are shown in closed circles (●).

between the model and experiment are well within the uncertainties of the model, with the steady-state H atom concentration and the solution-phase exothermicity of reaction 1a as the two major sources of uncertainty in the results.

Reactions 1a and 1b both depend on the concentration of H atom, and so the  $NH_3$  yield is essentially second order in H atom concentration. Thus, given the uncertainty of the rates used in the model, small errors in predicting H atom concentration (for example due to errors in approximating the rate of electron production or recombination or neglecting photolysis of water by very low-wavelength light) can easily explain the differences between predicted and observed  $NH_3$  yields. On the basis of the reaction rates and species concentrations, reaction 1a can be assumed to be in quasi-equilibrium. As such, the model is *extremely* insensitive to the detailed solution phase hydrogen addition reaction barrier. For example, decreasing the rate constant by 2 orders of magnitude only decreases the ammonia yield by a factor of 2. However, the results are modestly influenced by estimates of the reaction free energy of reaction 1a and the resulting equilibrium. Overall, the experimental drops in yield at both high and low pH are well-described by the model's simple description of the competition between protons producing H atoms at high pH and solvated electrons necessary for later steps at low pH.

In contrast to the good agreement for  $NH_3$  yields, the  $H_2$  production is overestimated by the model at most pH values, from a factor of 4 at pH 7 to more than a factor of 30 at low pH (Figure 2). The increase in  $H_2$  yield with pH values decreasing from 7, observed in Table 1, is easily understood by the known fast reaction of protons with solvated electrons to form H atoms which in turn react to form  $H_2$ .<sup>27</sup> At low pH, protons



**Figure 2.** Ratio of  $H_2$  yield predicted by the model to that observed experimentally as a function of pH.



(supplied by the buffer) compete more favorably with I atoms (recombination) for reaction with solvated electrons. (Although there are several processes by which  $H_2$  can be produced, the  $H + H$  pathway is second-order in H atom and will therefore dominate at low pH.) Indeed, the kinetic model for  $I^-$  in pure water (no  $O_2$ ,  $N_2$ , or buffer, but  $[H^+]$  and  $[OH^-]$  held fixed at the appropriate pH) indicates that  $H_2$  production should increase by nearly 3 orders of magnitude from pH 8 to pH 2. However, the experimentally measured  $H_2$  yield increases by less than a factor of 5 over the same range.

This discrepancy can be resolved by noting that I atoms can react with  $H_2$  to form HI, as previously observed both in the gas phase<sup>74</sup> and in relatively high yields in a high-temperature aqueous environment.<sup>75</sup> Indeed, indirect recombination of solvated electrons with I atoms by first reacting with a proton has been postulated before.<sup>68</sup> Preliminary experiments demonstrate the feasibility of such a process for the present system; reacting saturated aqueous  $H_2$  and  $I_2$  under the photochemical conditions of this study (with the photolysis of  $I_2$  to I) yields spectroscopic data consistent with  $I_2$  converted to  $I^-$ , along with a corresponding drop in pH. Control experiments show no  $I^-$  in the absence of  $H_2$ . As such, while the exact mechanism is still debated,<sup>76</sup> it appears likely that  $H_2$  product is being reoxidized under the current conditions. As a result, aqueous  $H^+$  and  $I^-$  are formed, consuming  $H_2$  and  $I_2$ , essentially serving to recombine the solvated electron with I atoms via a proton mediator. This accounts for the relatively small change in  $H_2$  yield as a function of pH while still observing conservation of charge through comparison of the reduction and oxidation product yields in Table 1. The omission of these reactions also explains the large discrepancies between the model and the experimental  $H_2$  yield at low pH values, where indirect recombination occurs in larger quantities due to the increased amounts of  $H_2$  available. We also note that this indirect recombination is not included in our estimate of the quantum yield, which is therefore a lower bound due to undetected  $I_2$ .

## CONCLUSIONS

Reduction of stable species, such as  $N_2$ , via solvated electrons presents interesting challenges and potential opportunities. The present work provides a first step toward a more fundamental understanding of the mechanism of these complex processes. Overall, it is found that reduction of  $N_2$  to  $NH_3$  occurs via a combination of initial direct H atom addition and subsequent sequential protonation/ET. The unique combination of these two reduction pathways, including both *direct* and *indirect* reactions with solvated electrons, leads to a characteristic pH dependence that has been verified by a combination of experimental and computational methods, along with detailed kinetic modeling. We conclude that the proposed mechanism, involving HAA at initial steps, and sequential protonation/direct reduction by solvated electrons at later steps, is the only plausible mechanism for  $N_2$  reduction by aqueous solvated electrons.

Overall, this mechanism is likely quite similar to what would be expected in some electrochemical reductions of  $N_2$  at electrode surfaces, depending on the metal used. However, because of the potentials involved, it is expected that the direct reduction of protons to  $H_2$  would be a dominant side reaction. In particular, the extremely high local concentration of adsorbed H atoms at the electrode surface, coupled with the small amount of adsorbed  $N_2$ , would most likely lead to nearly

exclusive production of  $H_2$  over  $NH_3$ . In contrast, reduction by solvated electrons in bulk solution reduces the local H atom concentration and allows  $N_2$  reduction to compete more favorably with  $H_2$  production, although the latter is still the majority product. Thus, maximizing selectivity for the desired reduction over  $H_2$  production seems to be one of the principle challenges for such solvated electron-mediated reductions in aqueous solution. This also suggests the potential promise of related reductions in electrochemically stable nonaqueous solvents, which may proceed via alternative pathways with increased selectivity and efficiency.

## ASSOCIATED CONTENT

### Supporting Information

Details of methods used for and results obtained from the thermodynamic screening. Further details of methods used for calculating  $N_2$ -solvated electron PMFs, along with a figure of representative PMFs. Further details of the biased sampling method used. Figure showing representative Marcus curves for the ET reaction. Figure showing reaction barrier as a function of  $N_2$ -solvated electron distance for the ET reaction. Tables of the 83 neutral and ionic species used for the thermodynamic screening and their calculated enthalpies of formation and solvation. Table containing rate constants used in the kinetic model. This material is available free of charge via the Internet at <http://pubs.acs.org>.

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### Notes

The authors declare no competing financial interest.

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