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Densities of Carbon Dioxide + Nitrogen from 225 K to 450 K at Pressures up to 70 MPa

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This paper reports PVT measurements for five gravimetrically prepared mixtures of $CO_2 + N_2$ from 225 K to 450 K at pressures up to 70 MPa. These results have been determined using a continuously-weighed pycnometer. A detailed error analysis indicates that the accuracy of the densities is better than $\pm 0.1\%$. Additional PVT data for $CO_2 + N_2$ mixtures have been measured by Netherlandse Gasunie, Ruhrgas, and Gaz de France as reported by Jaeschke and Humphreys (1990).

Introduction

This paper reports experimental results for the densities of $\mathrm{CO_2} + \mathrm{N_2}$ mixtures from 225 K to 450 K at pressures up to 70 MPa using a continuously-weighed pycnometer. Burnett data and derived virial coefficients at 300 K and 320 K for this system have been reported previously by Brugge *et al.* (1989). Esper *et al.* (1989) report Burnett-isochoric measurements from 205 K to 320 K and pressures from 0.1 MPa to 48 MPa. Isochoric *pVT*, vapor pressures and saturation densities have been reported by Esper *et al.* (1989) and Duarte-Garza *et al.* (1995a).

Standard thermodynamic procedures permit evaluation of other properties from the densities. GPA/GRI Research Report RR-140 authored by Duarte-Garza *et al.* (1995b) contains: energies (internal, Helmholtz, and Gibbs), enthalpies, and entropies obtained from the data reduction method described by Duarte-Garza *et al.* (1997); second and third virial coefficients for both the pure compounds and the mixture.

Experimental Section

Materials. The carbon dioxide was Ultra Pure grade from Scientific Gas Products, Inc., with a purity better than 99.995 mol % with 40 ppm nitrogen and 40 ppm oxygen maximum contaminant concentration. The sample was degassed by evacuating a frozen sample for a least 30 min. The nitrogen was Research Grade from Air Products, with a specified purity of better than 99.9995%. No further purification was performed.

Measurements. The pycnometer consists of a sample cell of known volume suspended from an electronic balance that has been described in detail by Lau (1986) and Lau *et al.* (1997). Pressures are measured using pressure transducers that have been calibrated *in-situ* against an automatic dead-weight gauge pressure standard. The accuracy

of the pressure measurements is estimated to be ± 0.006 MPa. Temperatures are measured with a four-lead platinum resistance thermometer, which is adjacent to the sample cell on the inside surface of the compartment. The temperature is controlled to $\pm 0.002\ K$ and measured to an accuracy of ± 0.005 K on ITS-90. The mixtures are prepared gravimetrically with mole fractions accurate to ± 0.000 05, excluding the effects of sample impurity. The uncertainties in the pycnometric density measurements arise from the uncertainties in the mass determinations and the cell volume calibration. The error in the cell volume calibration, which includes random errors introduced by uncertainties in the temperature and pressure measurements, uncertainties from using a calibrating fluid whose equation of state is known, and errors from mass determinations, is about $\pm 0.04\%$. The estimated accuracy (at 95 % confidence limit) provided by Hwang et al. (1997) in the pycnometric density measurements is

$$\Delta \rho = \{(0.15)^2 + (0.0004\rho)^2\}^{1/2}$$

or

$$\frac{\Delta
ho}{
ho} = \left\{ \left(\frac{0.15}{
ho} \right)^2 + 1.6 \times 10^{-7} \right\}^{1/2}$$

where the units of density are kg⋅m⁻³.

Results and Conclusions

Table 1 contains densities measured with the pycnometer and derived compressibility factors for the five mixtures of $CO_2 + N_2$. These data cover temperatures from 225 K to 450 K and pressures up to 70 MPa.

The experimental data in this project are state-of-theart measurements and generally accurate within $\pm 0.1\%$. These results are suitable for both stringent testing and development of models and correlations. These results formed a significant contribution to the development of the American Gas Association Standard AGA-8.

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Table 1. Experimental pVT Results for CO₂ (A) + N₂ (B) at Various Mole Fractions Determined by Pycnometer. $M_{\rm r,A}=$ 28.0134, $M_{\rm r,B}=$ 44.0098

p/MPa	$ ho/\mathrm{mol}\cdot\mathrm{m}^{-3}$	Z	p/MPa	$ ho/\mathrm{mol}\cdot\mathrm{m}^{-3}$	Z	p/MPa	$ ho/\mathrm{mol}\cdot\mathrm{m}^{-3}$	Z	p/MPa	$ ho/\mathrm{mol}\cdot\mathrm{m}^{-3}$	Z
				X	$\chi = 0.105 60$		7026				
88.759	21 922	1.676 61	51.819	19 990	I = 22 $1.385 67$	25.00 K 34.553	16 978	1.087 88	17.334	10 929	0.847 81
32.510	21 286	1.569 78	45.955	19 136	1.283 70	28.832	15 503	$0.994\ 13$	11.565	7 405	0.834 84
57.402	20 706	1.481 88	40.271	18 158	1.185 51	23.073	13 561	0.909 48	5.789	3 470	0.891 78
88.953	20 751	1.631 22	34.424	15 394	I = 24 1.09776	15.00 K 18.586	10 022	0.910 40	8.579	4 647	0.906 28
57.208	19 395	1.447 99	29.447	14 066	1.027 71	15.875	8 698	$0.895\ 97$	6.223	3 302	0.925 17
19.629	18 325	1.329 51	25.196	12 702	0.973 77	13.324	7 341	0.891 00	3.806	1 967	0.949 87
10.517	16 735	1.188 53	21.643	11 356	$0.935\ 60$	10.939 35.00 K	6 004	0.894 41	1.265	631	0.984 15
88.980	19 656	1.592 75	34.460	14 069	1.11166	17.697	8 484	0.946 71	8.288	3 996	0.941 33
69.626	18 547	1.459 09	30.257	12 956	1.059 92	15.189	7 356	0.937 14	6.015	2 867	$0.952\ 20$
1.662 5.014	17 418 16 304	1.346 15 1.253 06	26.580 23.281	11 838 10 708	1.019 05 0.986 76	12.832 10.538	6 240 5 118	0.933 32 0.934 49	3.740 1.408	1 754 647	0.967 75 0.987 68
39.419	15 204	1.176 70	20.372	9 599	0.963 22	10.556	3 110	0.334 43	1.400	047	0.307 00
	40.000			10.010		35.00 K			40.000		
69.124 61.286	18 656	1.563 62 1.460 78	38.736 34.711	13 916 12 989	1.174 68 1.127 75	21.802 19.227	9 171 8 227	1.003 23 0.986 26	10.090 7.932	4 433 3 472	0.960 54 0.964 10
4.492	17 705 16 756	1.372 41	30.952	12 027	1.127 73	16.819	7 286	0.986 26	5.792	2 524	0.968 41
18.534	15 806	1.295 82	27.610	11 071	1.052 45	14.481	6 326	0.96603	3.650	1 576	0.977 36
13.343	14 858	1.231 06	24.590	10 124	1.025 01	12.256	5 378	0.961 72	1.477	630	0.989 37
39.055	17 936	1.543 52	39.817	13 396	T = 30 1.191 62	00.00 K 22.642	8 840	1.026 85	10.413	4 272	0.977 21
1.675	17 032	1.451 73	35.681	12 476	1.146 58	19.933	7 919	1.009 13	8.196	3 363	0.977 05
5.165	16 118	1.372 13	31.967	11 568	1.107 87	17.400	7 007	0.995 54	5.999	2 456	0.979 25
9.506 4.370	15 219 14 306	1.304 11 1.243 41	28.534 25.493	10 638 9 743	1.075 34 1.048 99	14.971 12.682	6 088 5 188	0.985 87 0.980 01	3.767 1.537	1 534 620	0.984 50 0.993 86
1.570	14 300	1.245 41	20.400	3 743		20.00 K	3 100	0.300 01	1.557	020	0.555 00
4.747	11 381	1.147 50	23.668	8 451	1.052 61	14.819	5 542	1.005 00	6.805	2 580	0.991 34
0.700	10 405	1.108 95	20.550	7 484	1.032 03	12.114	4 567	0.996 95	4.181	1 583	0.992 69
7.037	9 428	1.077 84	17.649	6 522	1.017 08	9.397 50.00 K	3 558	0.992 65	1.740	658	0.993 89
9.189	15 932	1.492 33	42.587	11 927	I = 33 1.226 99	24.756	7 884	1.079 02	11.366	3 857	1.012 64
2.799	15 130	1.426 30	38.449	11 112	1.189 02	21.856	7 081	1.060 65	8.925	3 047	1.006 54
7.018 1.735	14 327 13 520	1.367 58 1.314 94	34.625 31.132	10 298 9 499	1.155 40 1.126 23	19.062 16.417	6 271 5 471	1.044 55 1.031 15	$6.550 \\ 4.182$	2 246 1 439	1.002 14 0.998 67
6.821	12 700	1.266 88	27.855	8 693	1.120 23	13.867	4 670	1.020 38	1.840	635	0.995 73
	44054	4.440.04	74 000	44.000		00.00 K	0.007	4 404 04	47 005	4.050	4 0 7 0 0 0
8.655 3.076	14 254 13 559	1.448 24 1.398 75	51.633 45.922	11 939 11 018	1.300 36 1.253 21	34.122 28.750	8 837 7 698	1.161 01 1.122 96	17.385 11.889	4 950 3 463	1.056 03 1.032 28
7.528	12 807	1.350 63	40.264	10 025	1.207 64	22.860	6 331	1.085 70	5.747	1 708	1.011 72
0.500	10.000	1 417 07	45 77 45	0.010		60.00 K	0.704	1 107 00	11.000	0.001	1 007 07
38.588 57.394	12 929 11 523	1.417 87 1.331 23	45.745 40.044	9 819 8 884	1.245 17 1.204 71	28.416 22.867	6 734 5 582	1.127 83 1.094 89	11.263 5.828	2 901 1 532	1.037 67 1.016 75
1.431	10 685	1.286 48	34.451	7 895	1.166 28	17.279	4 336	1.065 08	0.020	1 002	1,010 / 0
				X	$\lambda = 0.251 \ 47$		0360				
88.723	23 105	1.589 93	54.635	21 756	T = 22 1.342 38	25.00 K 40.832	19 946	1.094 28	26.560	16 925	0.838 85
33.995	22 691	1.507 56	50.028	21 224	1.259 99	36.052	19 127	1.007 55	22.097	15 426	0.765 71
9.486	22 264	1.428 22	45.559	20 642	1.179 79	31.521	18 196	0.925 99	17.324	13 188	0.702 19
8.896	21 883	1.545 56	30.934	16 208	T = 24 0.93693	15.00 K 16.575	10 536	0.772 28	8.167	4 858	0.825 28
5.480	20 476	1.330 12	26.204	14 812	0.868 47	14.379	9 182	0.768 76	6.059	3 439	0.864 90
5.088	19 053	1.161 71	22.498	13 442	0.821 63	12.171	7 694	0.77656	3.737	2 005	0.914 97
7.041	17 617	1.032 17	19.130	11 922	0.787 71	10.182	6 283	0.795 55	1.182	594	0.976 85
8.657	20 675	1.507 16	31.649	14 752	T = 20 0.973 71	35.00 K 16.383	8 881	0.837 24	8.034	4 141	0.880 53
8.009	19 489	1.350 91	27.743	13 606	0.925 43	14.202	7 695	0.83764	5.906	2 954	0.907 41
9.373 2.394	18 309 17 145	1.223 89 1.122 24	24.334 21.323	12 429	0.888 58 0.861 84	12.108 10.055	6 499 5 307	0.845 56 0.859 91	3.669 1.242	1 772 576	0.939 73 0.978 63
6.542	17 143	1.039 61	18.758	11 229 10 070	0.845 43	10.033	3 307	0.639 91	1.242	370	0.976 03
						85.00 K			_		
39.088	19 624	1.485 71	36.619	14 619	1.057 08	20.577	9 619	0.902 76	9.840	4 598	0.903 12
30.329 52.977	18 620 17 622	1.367 31 1.268 68	32.596 29.030	13 623 12 611	1.009 74 0.971 44	18.220 15.997	8 615 7 605	0.892 51 0.887 69	7.824 5.730	3 602 2 589	0.916 65 0.933 99
6.679	16 625	1.184 90	25.912	11 614	0.941 54	13.903	6 607	$0.888\ 02$	3.582	1 581	0.956 12
1.260	15 618	1.114 87	23.106	10 611	0.918 94	11.843	5 594	0.893 43	1.354	584	0.978 42
9.107	18 739	1.478 49	38.228	13 978	T = 30 1.096 43	00.00 K 21.667	0.190	0.945 31	10.244	4 408	0.931 69
0.931	18 739 17 774	1.478 49 1.374 35	38.228	13 978	1.096 43	19.169	9 189 8 232	0.945 31 0.933 55	8.099	4 408 3 448	0.931 69
4.037	16 828	1.287 37	30.514	12 054	1.014 87	16.816	7 276	0.92656	5.937	2 496	0.953 60
18.072	15 886	1.213 17	27.295	11 104	0.985 48	14.565	6 319	0.924 07	3.713	1 533	0.971 02
12.827	14 930	1.150 01	24.350	10 142	0.962 54	12.396	5 368	0.925 79	1.436	581	0.990 88

p/MPa	ρ/mol⋅m ⁻³	Z	p/MPa	$ ho/\mathrm{mol}\cdot\mathrm{m}^{-3}$	Z	p/MPa	$ ho/\mathrm{mol}\cdot\mathrm{m}^{-3}$	Z	p/MPa	$ ho/\mathrm{mol}\cdot\mathrm{m}^{-3}$	Z
				XA	= 0.251 47		0360				
39.011	17 889	1.449 93	39.687	13 356	T = 32 1.116 83	20.00 K 22.962	8 850	0.975 17	10.804	4 275	0.949 87
31.506	16 985	1.361 03	35.619	12 437	1.076 42	20.261	7 913	0.962 35	8.566	3 372	0.954 78
54.928	16 066	1.284 99	32.020	11 549	1.042 06	17.748	6 998	0.95321	6.308	2 462	0.962 98
50.951	15 454	1.239 16	28.675	10 630	1.013 88	15.405	6 103	0.948 71	3.923	1 514	0.973 88
15.125	14 443	1.174 29	25.733	9 747	0.992 28	13.081	5 191	0.947 12	1.554	589	0.991 63
39.195	16 641	1.428 87	41.551	12 414	T = 35 1.150 18	50.00 K 24.223	8 189	1.016 47	8.875	3 119	0.977 80
32.429	15 801	1.357 68	37.578	11 589	1.114 25	21.446	7 354	1.002 12	6.486	2 275	0.979 70
56.348	14 958	1.294 50	33.822	10 735	1.082 67	18.790	6 513	0.991 39	4.097	1 430	0.984 53
50.943	14 118	1.239 96	30.428	9 895	1.056 71	16.208	5 661	0.983 86	1.687	586	0.98927
46.046	13 270	1.192 39	27.254	9 049	1.034 97	13.711	4 814	0.978 72			
68.727	14 796	1.396 65	51.693	12 454	I = 40 1.24804	00.00 K 34.456	9 299	1.114 12	16.675	4 918	1.019 49
63.061	14 085	1.346 20	45.922	11 501	1.200 58	28.669	8 006	1.076 72	11.547	3 455	1.004 91
57.436	13 316	1.296 93	40.281	10 470	1.156 80	23.064	6 634	1.045 36	5.867	1 767	0.998 35
						60.00 K					
38.690	13 347	1.375 51	51.698	11 088	1.246 16	34.454	8 160	1.128 50	17.196	4 420	1.039 82
63.105	12 664	1.331 82 1.288 20	45.871	10 178 9 201	1.204 56 1.165 18	28.331 23.239	6 930 5 824	1.092 65 1.066 47	11.652	3 050	1.021 06
57.351	11 899	1.200 20	40.112					1.000 47	5.613	1 490	1.006 84
				<i>X</i> _A	= 0.503 65		0700				
38.757	25 215	1.457 61	55.490	24 328	T = 22 1.219 24	25.00 K 42.734	23 236	0.983 09	29.435	21 627	0.727 53
34.284	24 936	1.378 03	51.251	23 996	1.141 68	38.334	22 777	0.899 64	25.084	20 883	0.642 08
9.971	24 649	1.300 54	47.029	23 638	1.063 50	33.940	22 255	0.815 20			
						15.00 K					
9.031	23 957	1.414 52	54.654	22 839	1.174 75	40.137	21 298	0.925 13	25.376	18 726	0.665 24
64.442 69.470	23 631 23 251	1.338 71 1.255 61	49.798 44.823	22 384 21 858	1.092 13 1.006 68	35.095 30.213	20 592 19 764	0.836 65 0.750 44	20.573	17 307	0.583 55
3.470	23 231	1.233 01	44.023	21 030		55.00 K	13 704	0.730 44			
8.418	23 282	1.386 04	55.723	22 226	I = 23 1.18249	41.210	20 604	0.943 36	27.634	18 181	0.716 89
3.922	22 936	1.314 49	50.245	21 680	1.093 10	36.441	19 902	0.863 61	22.818	16 815	0.640 04
9.345	22 555	1.240 98	45.746	21 183	1.018 57	32.023	19 128	0.78962	18.165	14 903	0.574 89
						35.00 K					
39.001	22 729	1.377 83	24.410	16 191	0.684 25	12.784	9 667	0.600 20	7.181	4 428	0.736 03
55.649 13.359	21 552 20 111	1.171 90 0.978 51	20.995 18.245	14 913 13 585	$0.63895 \\ 0.60954$	11.373 10.049	8 341 7 048	0.618 84 0.647 11	5.511 3.500	3 132 1 816	0.798 60 0.874 72
35.192	18 811	0.849 08	16.080	12 265	0.595 03	8.649	5 731	0.684 94	1.140	538	0.961 70
29.030	17 505	0.752 67	14.235	10 905	$0.592\ 45$						
						75.00 K					
39.014 55.386	22 139 20 861	1.363 36 1.161 17	26.449 22.837	15 778 14 506	0.733 14 0.688 53	13.921 12.286	9 416 8 098	0.646 60 0.663 54	7.643 5.790	4 332 3 063	0.771 63 0.826 73
15.081	19 595	1.101 17	19.987	13 241	0.660 17	10.850	6 889	0.688 82	3.684	1 807	0.820 73
37.149	18 322	0.886 76	17.566	11 921	0.644 45	9.299	5 612	0.724 69	1.152	522	0.965 19
31.129	17 054	0.798 31	15.661	10 692	0.640 61						
						35.00 K					
39.189	21 561	1.354 22	30.659	16 028	0.807 23	16.990	10 479	0.684 22	9.050	4 948	0.771 86
57.633 18.491	20 450 19 343	1.189 32 1.057 93	26.842 23.732	14 917 13 814	0.759 37 0.724 99	15.270 13.678	9 375 8 273	$0.687\ 37$ $0.697\ 72$	7.376 5.543	3 837 2 732	0.811 24 0.856 22
41.194	18 238	0.953 18	21.142	12 705	0.702 25	12.150	7 173	0.714 82	3.502	1 627	0.908 34
35.359	17 137	0.870 73	18.932	11 599	0.688 80	10.616	6 055	0.739 89	1.192	522	0.963 66
						00.00 K					
39.028	20 667	1.339 03	33.118	15 368	0.863 95	18.707	10 069	0.744 84	9.643	4 758	0.812 51
58.681 50.230	19 607 18 541	1.199 86 1.086 11	29.248 26.056	14 302 13 259	0.819 87 0.787 84	16.744 14.914	9 007 7 942	0.745 29 0.752 85	7.789 5.819	3 695 2 645	0.845 11 0.882 00
13.426	17 488	0.995 53	23.267	12 195	0.764 90	13.165	6 888	0.766 25	3.652	1 579	0.882 00
37.763	16 425	0.921 73	20.829	11 123	0.750 74	11.413	5 818	0.786 45	1.262	516	0.980 51
						20.00 K					
39.044	19 595	1.324 33	35.685	14 568	0.920 66	20.472	9 547	0.805 95	10.290	4 535	0.852 81
59.508 51.900	18 570 17 566	1.204 42 1.110 48	31.758 28.435	13 560 12 565	0.880 25 0.850 56	18.276 16.233	8 532 7 546	0.805 09 0.808 53	$8.230 \\ 6.074$	3 525 2 518	0.877 52 0.906 64
45.580	16 571	1.033 81	25.458	11 549	0.828 50	14.233	6 542	0.817 71	3.800	1 518	0.940 86
40.180	15 562	0.970 42	22.859	10 551	0.814 29	12.261	5 537	0.832 27	1.353	518	0.981 71
						50.00 K					
69.156	18 130	1.310 78	38.917	13 499	0.990 68	22.752	8 871	0.881 34	11.077	4 229	0.900 08
61.236 54.438	17 210 16 287	1.222 71 1.148 57	34.980 31.453	12 579 11 650	0.955 59 0.927 75	20.228 17.857	7 930 7 005	0.876 55 0.875 99	8.801 6.454	3 301 2 370	0.916 19 0.935 79
18.458 18.458	15 342	1.148 57 1.085 38	28.285	10 720	0.927 75 0.906 69	17.857	6 083	0.875 99 0.879 62	4.034	2 370 1 446	0.935 78
43.405	14 430	1.033 64	25.426	9 801	0.891 47	13.325	5 157	0.887 91	1.476	5 12	0.990 63
						00.00 K					
88.619	15 943	1.294 13	51.725	13 625	1.141 48	34.424	10 252	1.009 62	17.447	5 539	0.947 10
33.139	15 271	1.243 18	45.830	12 615	1.092 36	28.635	8 807	0.977 63	11.530	3 641	0.952 17
57.289	14 473	1.190 19	40.049	11 490	1.048 04	22.930	7 212	0.955 99	6.060	1 884	0.967 16

Table 1 (Continued)

i adie i	(Continuea	.)									
p/MPa	ρ/mol⋅m ⁻³	Z	p/MPa	ρ/mol⋅m ⁻³	Z	p/MPa	ρ/mol⋅m ⁻³	Z	p/MPa	ρ/mol⋅m ⁻³	Z
				Х	$a_A = 0.503 65$	$M_{\rm r} = 36.$	0700				
					T = 4	50.00 K					
68.770	14 241	1.290 66	51.741	11 920	1.160 14	34.390	8 760	1.049 25	17.215	4 659	0.987 57
63.009 57.446	13 527 12 774	1.244 95 1.201 95	45.854 40.196	10 950 9 923	1.119 22 1.082 66	28.731 23.022	7 513 6 148	1.022 09 1.000 83	11.855 5.842	3 221 1 581	0.983 70 0.987 60
37.440	12 774	1.201 33	40.130					1.000 65	3.042	1 361	0.307 00
				X	$T_{\rm A} = 0.711~05$.3670				
68.765	26 795	1.371 82	52.872	26 038	1 = 2. 1.085 43	25.00 K 37.012	25 081	0.788 82	26.429	24 251	0.5825 5
63.528	26 562	1.278 46	47.575	25 745	0.987 80	31.663	24 690	0.685 51	20.934	23 708	0.472 00
58.351	26 316	1.185 25	42.444	25 438	0.891 90						
00.040	05 577	1 005 14	54041	0.4.000		45.00 K	00.001	0.010.70	04.157	00.000	0.500.70
69.042 64.182	25 577 25 327	1.325 14 1.244 02	54.941 49.385	24 802 24 441	1.087 45 0.991 92	39.256 34.043	23 681 23 217	0.813 78 0.719 81	24.157 18.997	22 096 21 291	0.536 70 0.438 01
58.841	25 034	1.153 85	44.239	24 074	0.902 10	29.624	22 763	0.638 87			
					T=20	65.00 K					
68.931	24 364	1.284 06	34.035	21 489	0.718 83	18.559	18 633	0.452 05	13.579	16 527	0.372 90
57.785 48.415	23 656 22 939	1.108 65 0.957 91	28.869 24.672	20 782 20 072	0.630 47 0.557 87	16.504 14.781	17 937 17 194	0.417 60 0.390 16	13.579	16 527	0.372 90
40.590	22 223	0.828 96	21.376	19 375	0.500 73						
						75.00 K					
68.988	23 767 22 918	1.269 50 1.082 49	32.303 27.197	20 349 19 483	0.694 28 0.610 52	17.915 16.008	16 944 16 059	0.462 42	13.428 12.490	14 346 13 475	0.409 37 0.405 38
56.724 46.572	22 047	0.923 86	23.293	18 633	0.546 73	14.525	15 175	$0.43596 \\ 0.41862$	12.490	13 475	0.405 38
38.614	21 195	0.796 79	20.170	17 758	0.49676						
						85.00 K					
69.080 55.607	23 187 22 172	1.257 27 1.058 39	21.011 17.501	16 709 15 193	0.530 66 0.486 12	11.337 10.346	9 846 8 477	0.485 91 0.515 05	7.189 5.658	4 491 3 158	0.675 53 0.756 09
44.919	21 141	0.896 65	15.302	13 835	0.466 76	9.405	7 147	0.555 34	3.656	1 813	0.750 03
35.358	19 920	0.749 06	13.685	12 503	0.461 90	8.387	5 810	0.609 19	1.088	480	0.956 55
26.656	18 313	0.614 26	12.389	11 145	0.469 11						
69.024	22 289	1.241 52	26.095	16 536	T = 30 0.63266	00.00 K 14.704	10 785	0.546 59	8.735	5 069	0.690 85
55.166	21 140	1.046 19	22.632	15 389	0.589 60	13.465	9 665	0.558 53	7.292	3 920	0.745 77
44.719	19 993	0.896 72	19.974	14 258	0.561 63	12.271	8 495	0.579 11	5.602	2 776	0.809 03 0.882 74
36.720 30.675	18 843 17 686	0.781 26 0.695 34	17.845 16.111	13 091 11 921	0.546 50 0.541 82	11.181 9.989	7 382 6 207	0.607 23 0.645 18	$3.567 \\ 1.147$	1 620 475	0.882 74 0.968 08
						20.00 K					
68.951	21 146	$1.225\ 54$	29.742	15 577	0.717 63	16.988	10 025	0.63690	9.068	4 460	0.764 17
56.959 47.500	20 044 18 927	1.068 05 0.943 25	26.138 23.221	14 465 13 356	0.679 15 0.653 46	15.338 13.797	8 906 7 791	0.647 29 0.665 59	7.231 5.144	3 343 2 228	0.812 97 0.867 76
40.063	17 804	0.845 75	20.797	12 248	0.638 19	12.287	6 684	0.690 91	2.761	1 113	0.932 37
34.288	16 696	0.771 87	18.747	11 132	0.632 96	10.719	5 567	$0.723\ 68$	1.224	472	0.974 66
						50.00 K					
69.088 59.363	19 557 18 546	1.213 94 1.099 92	35.089 31.309	14 540 13 540	0.829 28 0.794 60	20.562 18.453	9 524 8 497	0.741 90 0.746 27	10.712 8.374	4 501 3 369	0.817 82 0.854 14
51.469	17 546	1.008 01	28.076	12 538	0.769 49	16.502	7 500	0.756 09	6.421	2 490	0.886 14
45.039	16 558	0.934 71	25.267	11 530	0.753 05	14.597	6 506	0.770 99	3.980	1 474	0.927 86
39.580	15 541	0.875 17	22.802	10 530	0.744 12	12.664	5 498	0.791 52	1.333	469	0.976 68
68.723	17 122	1.206 85	51.834	14 909	$I = 40$ $1.045\ 37$	00.00 K 34.480	11 432	0.906 88	17.097	5 912	0.869 54
63.024	16 465	1.150 93	45.987	13 915	0.993 70	28.678	9 833	0.87694	11.537	3 866	0.897 30
57.544	15 751	1.098 49	40.123	12 749	0.946 29	22.998	8 013	0.862 98	5.890	1 881	0.941 52
68.603	15 125	1.212 27	51.741	12 816	$T = 48$ $1.079 \ 03$	50.00 K 34.452	9 485	0.970 80	17.260	4 939	0.934 02
62.976	14 436	1.165 95	45.928	11 827	1.079 03	28.755	8 106	0.948 11	11.587	3 275	0.934 02
57.406	13 678	1.121 73	40.166	10 720	1.001 42	23.164	6 621	0.935 07	5.867	1 622	0.966 76
				X	$t_A = 0.909 \ 21$, $M_{\rm r} = 42$.	5575				
						25.00 K					
68.831 63.930	28 071 27 922	1.310 72 1.223 88	49.927 44.731	27 446 27 252	0.972 39 0.877 39	34.971 30.735	26 858 26 672	0.696 01 0.615 97	23.482 15.997	26 326 25 923	0.476 80 0.329 86
59.307	27 772	1.141 51	40.095	27 071	0.791 71	25.841	26 445	0.522 33	11.238	25 636	0.234 33
54.341	27 605	1.052 26									
00.000	00.000	1.050.07	F0.010	00.000		45.00 K	05 440	0.074.00	17 407	04.044	0.050.01
68.926 63.374	26 926 26 722	1.256 64 1.164 24	52.013 46.110	26 268 26 007	0.972 04 0.870 37	34.971 29.357	25 446 25 125	0.674 66 0.573 59	17.497 11.846	24 311 23 827	0.353 31 0.244 06
57.687	26 505	1.068 44	40.397	25 728	0.770 80	23.315	24 738	0.462 67	11.010	20 021	0.21100
					T=20	65.00 K					
68.251	25 744	1.203 24	41.002	24 360	0.76392	22.907	22 978	0.452 45	13.391	21 862	0.278 00
61.833 56.018	25 466 25 189	1.101 99 1.009 34	36.809 32.721	24 091 23 801	0.693 45 0.623 95	20.145 17.673	22 696 22 420	0.402 84 0.357 76	11.756 9.953	21 611 21 301	0.246 89 0.212 07
50.756	24 919	$0.924\ 43$	29.107	23 523	0.561 60	15.450	22 147	0.316 62	8.547	21 030	0.184 46
45.612	24 633	0.840 39	25.874	23 250	0.505 08						

Table 1 (Continued)

p/MPa	$ ho/\mathrm{mol}\cdot\mathrm{m}^{-3}$	Z	p/MPa	$ ho/\mathrm{mol}\cdot\mathrm{m}^{-3}$	Z	p/MPa	$ ho/\mathrm{mol}\cdot\mathrm{m}^{-3}$	Z	p/MPa	$ ho/\mathrm{mol}\cdot\mathrm{m}^{-3}$	Z
				XA	= 0.909 21	$M_{\rm r} = 42.$	5575				
					T = 28	35.00 K					
69.019	24 622	1.182 95	32.843	22 197	0.624 41	18.648	20 368	0.386 37	11.374	18 528	0.259 06
57.355	24 004	1.008 34	27.142	21 590	0.530 53	15.654	19 763	0.33427	10.034	17 939	0.236 05
47.721	23 398	0.860 70	22.447	20 981	0.451 49	13.219	19 144	0.291 40	9.013	17 344	0.219 30
39.762	22 807	0.735 73									
					T = 30	00.00 K					
69.020	23 782	1.163 51	19.704	18 760	0.421 08	9.037	10 155	0.356 77	6.831	4 538	0.603 48
55.550	22 961	0.96992	14.523	17 058	0.341 33	8.608	8 614	0.400 63	5.587	3 189	0.702 37
43.810	22 057	0.79629	11.758	15 317	0.307 75	8.212	7 276	0.452 48	3.708	1 815	0.819 04
34.664	21 157	0.656 85	10.406	13 659	0.305 43	7.677	5 940	0.518 14	1.031	433	0.954 58
26.591	20 089	$0.530\ 66$	9.571	11 836	0.324 19						
					T=32	20.00 K					
69.065	22 654	1.145 85	19.987	16 109	0.466 33	11.919	9 576	0.467 81	7.881	4 417	0.670 61
55.533	21 695	0.962 07	17.288	14 842	0.437 79	11.058	8 274	0.502 31	6.126	3 043	0.756 64
41.924	20 402	0.772 33	15.306	13 493	0.426 35	10.159	6 975	0.547 42	3.955	1 746	0.851 37
31.439	18 961	0.623 19	13.907	12 176	0.42928	9.113	5 667	0.604 40	1.111	435	0.959 93
24.524	17 533	0.525 71	12.841	10 884	0.443 43						
					T = 35	50.00 K					
69.093	21 003	1.130 45	29.105	15 591	0.641 49	17.249	10 177	0.582 43	10.053	4 773	0.723 77
56.576	19 928	0.97559	25.639	14 510	0.607 20	15.798	9 097	0.596 76	8.306	3 688	0.773 92
46.868	18 849	0.854 45	22.896	13 418	0.586 37	14.396	8 003	0.618 14	6.290	2 598	0.831 97
39.302	17 754	0.760 70	20.684	12 336	0.576 18	13.019	6 914	0.647 06	3.957	1 517	0.896 35
33.571	16 677	0.691 74	18.865	11 265	0.575 47	11.601	5 849	0.681 57	1.220	434	0.96598
					T = 40	00.00 K					
68.626	18 399	1.121 50	51.935	16 437	0.95004	34.588	13 100	0.79389	17.344	6 764	0.770 99
63.073	17 828	1.063 77	45.955	15 496	0.891 70	28.277	11 221	0.757 72	11.728	4 263	0.827 21
57.472	17 176	1.006 10	40.612	14 494	0.842 50	23.033	9 253	$0.748\ 47$	6.627	2 218	0.898 38
					T = 45	50.00 K					
68.731	16 183	1.135 13	51.720	13 928	0.992 48	34.466	10 455	0.881 09	17.241	5 291	0.870 92
62.897	15 502	1.084 41	45.919	12 928	0.949 32	28.330	8 796	0.860 82	11.920	3 542	0.899 46
57.367	14 773	1.037 88	40.171	11 781	0.911 35	22.817	7 111	0.857 59	5.856	1 654	0.946 28

Literature Cited

Brugge, H. B.; Hwang, C.-A.; Rogers, W. J.; J. C. Holste; Hall, K. R. Experimental cross virial coefficients for binary mixtures of carbon dioxide with nitrogen, methane and ethane at 300 and 320 K. *Physica* **1989**, *A156*, 382–416.

Duarte-Garza, H. A.; Holste, J. C.; Hall, K. R.; Marsh, K. N.; Gammon, B. E. Isochoric pVT and Phase Equilibrium Measurements for Carbon Dioxide + Nitrogen. J. Chem. Eng. Data ${\bf 1995a}$, 40, 704–

Duarte-Garza, H. A.; Brugge, H. B.; Hwang, C.-A.; Eubank, P. T.; Holste, J. C.; Hall, K. R.; Gammon, B. E.; Marsh, K. N. Gas Processors Association/Gas Research Institute Research Report RR-140, 1995b.

Duarte-Garza, H.; Holste, J. C.; Hall, K. R.; Iglesias-Silva, G. A. A technique for preparing thermodynamic property tables using incomplete data sets. *Fluid Phase Equilib.* **1997**, in press. Esper, G. J.; Bailey, D. M.; Holste, J. C.; Hall, K. R. Volumetric

behavior of near-equimolar mixtures of carbon dioxide + methane and carbon dioxide + nitrogen. Fluid Phase Equilib. 1989, 49, 35-

Hwang, C-A.; Duarte-Garza, H. A.; Eubank, P. T.; Holste, J. C.; Hall, K. R.; Gammon, B. E.; Marsh, K. N. Gas Processors Association/ Gas Research Institute Research Report RR-138, 1995.

Jaeschke, M.; Humphreys, A. E. GERG Technical Monograph 4, The GERG Databank of High Accuracy Compressibility Factor Measurements; Verlag des Vereins Deutscher Ingenieure: Dusseldorf, Germany, 1990.

Lau, W.-W. R. A Continuously Weighed Pycnometer Providing Densities for Carbon Dioxide + Ethane Mixtures Between 240 and 350 K at Pressures Up to 35 MPa. Ph.D. Dissertation, Texas A&M University, College Station, TX, 1986.

Lau, W. R.; Hwang, C.-A.; Brugge, H. B.; Iglesias-Silva, G. A.; Duarte-Garza, H. A.; Rogers, W. J.; Hall, K. R.; Holste, J. C.; Gammon, B. E.; Marsh, K. N. A continuously weighed pycnometer for measuring fluid properties. *J. Chem. Eng. Data* **1997**, 42, 738–744.

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