COMBUSTION CHAMBER DEPOSITS

As Related to Carbon-Forming Properties of Motor Oils

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HE past few years have seen a renewed interest in the subject of combustion chamber deposits (4, 6, 8, 9, 11, 20), undoubtedly because of the higher octane requirements of the newer engine designs and the increasing cost of octane numbers. Most of the recent studies have dealt with the property of octane requirement increase (ORI) as related to the lead content of fuels or detergent content of oils. Between 1925 and 1939 a number of papers appeared in the literature dealing with the effect of motor oil composition on combustion chamber deposits, but since 1939 this subject has been relatively neglected.

PRIOR STUDIES

As early as 1925 Orleup (19) pointed out that most of the carbonaceous combustion chamber deposit was formed from lubricating oil. In 1931 Bahlke (1) reported a relationship between oil volatility and carbon-forming properties. This was called the "carbonization index," and it related the 90% point of an oil distillation at 1-mm. pressure to the tendency of oils to form combustion chamber carbon. In 1935 Merrill, Moore, and Bray (18) re-emphasized that motor oil is a major contributor to carbonaceous combustion chamber deposits, and pointed out that the use of distillate oils and solvent extraction, particularly in the presence of propane, decreased the carbon-forming properties of oils. This study also demonstrated the increased volatility and low carbon-forming properties of aromatic or coastal oils as compared with Pennsylvania oils.

In early work on motor oils the Conradson or similar carbon tests had been used as a criterion of carbon-forming properties (δ). However, in a review article in 1937, Gruse and Livingstone (13, 14) concluded that the carbon residue method of predicting coke deposits from oil had ceased to be more than roughly indicative because of the new solvent-refining methods used in oil manufacture. They also raised an objection to the only other method of predicting the amount of coke formed by an oil, the "carbonization index" method—the difficulty in duplicating distillations at 1-mm. pressure. Their over-all conclusion was that both the carbon residue method and the vacuum distillation method were capable of giving precise indication of carbon-forming tendencies only when applied to a given class of oils.

Everett and Keller (10), in 1939, made several attempts at developing a bench-scale laboratory test for evaluating the depositforming tendencies of oils. They reached the conclusion that the only way to get carbon deposits which would simulate those obtained in practice was by means of the cylinder of an internal combustion engine. They also concluded that the Conradson carbon residue had no reasonable correlation with the deposits found in service.

Thus, a review of the prior work shows the best laboratory evaluation procedure is the vacuum distillation technique. This method is not applicable to materials having low decomposition temperatures, nor is it suitable for studying the effect of additives on the "carbon" property of oils.

The effect of additives on the carbon-forming properties of motor oil has received little attention. Widmaier and Nenninger (22), using the Conradson carbon test, showed that formic

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acid, ethylene glycol, and dichlorohydrin reduced the coking tendencies of lubricating oils. This work is of limited interest because the test procedure used has little relationship to the combustion chamber deposit property of oils.

A recent engine study of Carr (4) evaluated the effect of motor oil additives at different detergency levels on octane requirement increase, power loss, and spark plug performance. Because the major interest in this study was evaluation of the metallic constituents of the oil additives, the test procedure employed high combustion chamber temperatures (21). These severe test conditions probably did not form carbonaceous deposits and therefore minimized any base oil effects. This study did show that unleaded paraffinic fuels or propane fuel gave much lower octane requirement increase and deposit weights than leaded cracked fuels. The authors concluded that fuel characteristics had a greater effect than motor oil on octane requirement increase.

On the other hand, Gibson (11) reported a distinct difference between a "naphthenic" and a "paraffinic" oil in one car under unspecified operating conditions, and Merrill et al. reported the same for a twelve-car test fleet in "routine operation."

PRESENT WORK

These results suggest that an engine study of the effect of motor oil on octane requirement increase and deposits should be conducted under low combustion chamber temperature conditions (moderate speed and light load) and in the absence of lead and cracked fuels. It is believed that the highest octane requirements are reached under such mild duty operation. Therefore, a laboratory engine test procedure was selected to fit this situation and was used to determine octane requirement increase for a considerable number of oils and fuels with and without additives.

Parallel with this work was the development of a laboratory carbonizing test designated "air evaporation test." This technique allowed the study of additives and synthetic oils under conditions more approaching the engine than the "carbonization index."

Using these tools, the authors attempted to relate engine octane requirement increase and deposits to the following oil compositional variables:

Oil volatility or distillation range

High viscosity blending components-bright stocks vs. viscosity index improvers

Synthetic oils

Exploratory oil additives designed to minimize deposits

ENGINE TEST PROCEDURE

It was desired to select an engine test procedure that would accentuate the contribution of motor oil to combustion chamber deposits and yet have as much significance in terms of road operation as possible. The four requirements which it was designed to meet were:

1. To operate under cycling conditions in order to avoid abnormal deposit accumulation.

To use mild conditions typical of city stop-and-go driving, so that carbonaceous deposits would be accentuated.

To run the test long enough to attain equilibrium, so that

the results would be as reproducible as possible.

4. To start each test with approximately the same initial octane requirement, as this factor is known to affect octane requirement increase and engine temperatures and pressures (17).

The engine used in the tests was a standard model, 1948 Chevrolet. It was new, or rebuilt according to the manufacturer's specifications. The auxiliary equipment, such as exhaust system, pan and jacket cooling, carburetion, etc., was the same as that used in the CRC-L-4-545 test (7). A modified L-4 break-in schedule was used. The combustion chamber and head assembly was rebuilt after each test. A complete engine overhaul was done after every four tests, or more often if necessary. The test engines were considered to have normal oil consumption, the rule being that consumption should be less than 1 quart per 1000 miles. The test was discontinued and the engine rebuilt if oil was consumed at a higher rate, if the beam load fell below 100 pounds at full throttle, or if the final compression pressures were less than 110 pounds per square inch.

The test conditions which were adopted are shown in Table I. Initial octane requirement used was 72 ± 2. Octane requirement measurements were made at 15-hour intervals and the tests were run to 100 hours, or approximately 4000 miles. This period was extended if necessary to obtain octane requirement equilibrium. The test was reproducible both as to deposit weights and octane requirement increase, as shown by check experiments. At the conclusion of the test, a final octane requirement measurement was made and piston top and valve deposits were removed and weighed.

TABLE I. CHEVROLET COMBUSTION CHAMBER DEPOSIT TEST CONDITIONS (TI)---- 100 h-----

(Tin	ne, 100 nours)	
	I dle	Cruise
Time, minutes Speed, r.p.m. Load, brake horse power Air-fuel ratio Water outlet, ° F. Water inlet, ° F. Oil sump, ° F. Spark, degrees	500 0 11.2 ii	25 2000 0 13.5-14.5 165 155 195
OCTANE DE	MAND MEASTISEMENT	

Speed, r.p.m. 1000
Load Full throttle
Jacket, ° F.
Spark advance, degrees 11 before top center

LABORATORY AIR EVAPORATION TEST

The factors involved in the formation of carbonaceous residues from motor oil in engine combustion chambers are (1, 14, 18, 19):

- Volatilization
- Oxidation
- 3. Thermal decomposition
- Iron catalysis (new factor)

In devising a test it was attempted to include all these factors.

The apparatus was a horizontally mounted APPARATUS. electric furnace, 32 inches long, with a steel core 4.5 inches in inside diameter. The ends of the furnace were closed with Transite disks, one of which was removable to allow the introduction of a sample tray. The removable disk contained holes for an air inlet tube and a thermocouple. The thermocouple was centrally located in the furnace and was connected to a Micro-

max controller recorder.

A double-deck Transite tray, which held the oil sample dishes, 2 inches in diameter, fitted into the furnace. Six dishes could be

positioned in the center part of the furnace.

Additional furnace end windings and a small fan mounted in the closed end of the furnace were used to reduce temperature gradients. The temperature gradient in the sample area of the furnace, when operating at 625° F., was \pm 5° F.

Test Procedure. Approximately 2 grams of oil were weighed into the containers. The samples were placed in the

furnace at the operating temperature and maintained under selected time and temperature conditions. Three cubic feet per hour of laboratory compressed air were passed through the furnace to furnish oxidizing conditions. At the end of the test period the sample dishes were removed from the furnace, cooled, and weighed. The weight of the residue was determined and the physical characteristics, such as appearance and adherence, were noted.

The low-carbon steel dishes were prepared for use by burning off carbon accoust deposits from the preceding test by placing in a muffle furnace at 1000° F., and scale was then removed from the dishes by policible and the dishes by policible and scale was then removed from the dishes by polishing with steel wool.

TABLE II. EFFECT OF IRON CATALYST AND TEMPERATURE ON OIL RESIDUE WEIGHT

(Time, 3 hours. Oils, 95 V.I. solvent-refined Mid-Continent, heart-cut)

	Wt	. % Residue	9
	Steel dish,	Glass	dish
Oil 100° F. Vis. (SUS)	625° F.	625° F.	650° F.
157	8.5	1.5	1.2
516	19.2	8.4	2.8
452^{a}	21.6	11.1	5.8
1590	57.2	31.6	20.4

^a Blend of 40% (157 at 100° F, vis.) +60% (880 at 100° F, vis.).

Test Development Studies: The first variable investigated was temperature. Several oils were tested in glass dishes at 550°, 650°, and 750° F. The coking temperature was about 650° F.; at 750° F. very low results were obtained, while at 550° F. the residues were semiliquid and did not resemble carbonaceous deposits. A narrower temperature range, 625° to 650° F., was studied with a series of solvent-refined oils of varying distillation range (Table II). These data illustrate several significant points:

The heavier oils gave increasing amounts of residue, in agree-

ment with the engine experience described above.

Much less residue remained at 650° F. than at 625° F.

This illustrates that small temperature variations can affect the competing phenomena of oil oxidation and evaporation.

Steel dishes gave much higher residues than did the glass containers. As iron is encountered by oil in almost all engine combustion chambers, this catalytic factor was considered to be very important, and steel dishes were adopted.

Aluminum, in other tests, was found to be noncatalytic, giving results similar to those obtained in glass dishes. The test, therefore, gives results on aluminum vs. steel pistons similar to those reported by Merrill, Moore, and Bray (18) in engines.

Another important question in residue formation is the relative contribution of oxidation and thermal decomposition. This point is illustrated in Table III, which reports tests on several oils in steel dishes at 625° F. for 3 hours in an air atmosphere and a nitrogen atmosphere. The inert atmosphere resulted in a decreased residue weight for all mineral oils, and it was particularly noticeable with the coastal oil. As engine combustion chambers are subject to oxidizing conditions, it was thought that air should be present in any test intended to measure the combustion chamber deposit-forming properties of a motor oil.

TABLE III. EFFECT OF OXIDIZING ATMOSPHERE ON OIL RESIDUE WEIGHT

(Time, 3 hours. Temp., 625° F. Steel dish)

		Wt. % Residue						
Oil Type	v.I.	100° F. vis. (SUS)	Nitrogen	Air				
Coastal A	34	525	0.8	9.5				
Solvent refined Mid- Continent	98	452	9.9	21.6				
Conventionally refined Mid-Continent	65	225	1.7	7.9				
Paraffin wax (127° F. m.p.)			1.3	3.4				
Synthetic polyether	141	312	1.4	0.7				

On the basis of these and other studies, the test conditions adopted for the air evaporation test were: 3 hours, 625° F., steel container, 2-gram oil sample, 3 liters of air per hour. A photograph of the apparatus is shown in Figure 1. Figure 2 shows the appearance of typical deposits formed from a synthetic, a coastal, and a solvent-refined Mid-Continent oil.

To illustrate the reproducibility of the air evaporation test under the standard conditions, oil 5 (Table IV) was submitted to a series of eighteen tests. The average residue value obtained was $22.2 \pm 1.3\%$, indicating an average deviation of 5.8%.

EFFECT OF OIL COMPOSITION

EFFECT ON EQUILIBRIUM OCTANE REQUIREMENT INCREASE AND DEPOSIT WEIGHT. In the first engine study, unleaded straight-run fuel was used in order to eliminate any lead or fuel effect on octane requirement increase and deposits, so that the lubricant contribution would be clearly evident. Table IV shows the results obtained on a variety of oils under these conditions.

A synthetic polyether oil (No. 1) gave a zero octane requirement increase and a very low deposit weight. The coastal, conventionally refined, and blend of solvent-refined oils gave equivalent engine results. The results illustrate that under the conditions involved, minor variations in mineral oil lubricant composition were not reflected in changes in octane requirement increase or deposit weight. Major compositional variations, such as the addition of residual bright stock or a detergent additive, gave significantly different deposit and octane requirement increase results. However, they were well below reported field results in which leaded fuels had commonly been used. The possibility always exists that longer operation of the engines would give higher values, although the increase in requirement had leveled off for a minimum of 12 hours before the end of the experiment.

An unusual result was noted in test 7, in which chromium and manganese naphthenates were blended (2) with oil 5. The test showed a normal deposit weight, but only 1 octane requirement increase, which might be attributable to the catalytic influence of the oil additives. A similar catalytic effect has been reported for boron and silicon compounds when used as fuel additives (16).

EFFECT ON OCTANE REQUIREMENT INCREASE AND DEPOSIT WEIGHT. In order to reduce possible fuel effect, but to introduce the lead effect, several engine tests were done in which oil composition was varied using straight-run fuel containing 0.5 ml. of tetraethyllead (see Table V). As with no tetraethyllead, two of

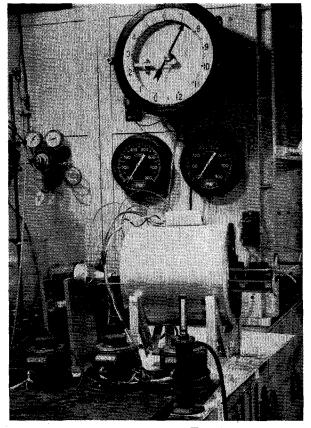


Figure 1. Air Evaporation Test Apparatus

the oils in this study, the coastal oil (test 9) and a blend of solvent-refined neutral and overhead bright stock (test 10) gave similar octane requirement increase values (14 and 12) and deposit weights, although these were substantially higher than in the absence of tetraethyllead. The solvent-refined neutral (test 11), used in the afore-mentioned blend, gave a lower octane requirement increase value of 9 and a much lower deposit weight.

The solvent-refined neutral was also blended with sufficient amounts of Paratone, Acryloid, and a polybutene oil to obtain about the same viscosity as the oil used in test 10, which contained an overhead bright stock. These three oils (tests 12, 13, and

14) all showed octane requirement increase values of 8, and two of them, the Paratone and Acryloid blends, gave only half as much deposit weight as was obtained with the base oil (test 11).

A comparison of the oils containing polymers with the bright stock blend (test 10) is of interest. Compared with the neutral oil, the bright stock caused an increase in octane requirement increase and deposit weight, whereas the polymers did not affect octane requirement increase and caused a reduction in deposit weight. The polymers, probably because of their relative ease of thermal decomposition, not only did not contribute to deposit formation, but appeared to cause deposit removal. The polymer concentrations used here were much higher than are normally used for viscosity index improvement.

A comparison which may be made between the data shown in Tables IV and V is the effect of the addition of 0.5 ml.

Table IV. Oil Composition vs. Engine Deposit Weight and Octane Requirement Increase

(Unleaded straight-run fuel)

No.	Oil Type	v.i.	100° F. Vis.	Engler 90% Pt.,	Equilib- rium ORI	Piston Top Deposit Wt., G.	Weight % Residue, Air Evaporation Test
1	Synthetic polyether	141	312	8214	0	0.5	2.1
2	Coastal A	34	525	900	6	3.3	9.5
3	Conventionally refined Mid-C.	65	313	888	7	3.6	13.4
4	Heart-cut S.R. Mid-C.	95	157	870	3	3.8	8.5
5	Blend of S.R. Mid-C. 40% 4 + 60% (85 at 210° F. vis.)	98	452	1003	5	3,3	21.6
6	Blend of S.R. Mid-C. 68% 4 + 32% (250 at 210° F. vis.)	98	459	1063ª	7	4.7	24.8
7	5 + 0.25% chromium naphthenate $+ 0.25%$ manganese naphth.	98	452	1003	1	3.6	39.0
8	$5 + 2\%$ metal + P_2S_6 additive	98	452	1003	. 8	5.1	• • •
a	Decomposition temperature.						

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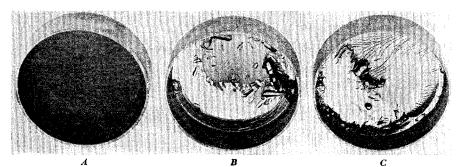


Figure 2. Typical Results of Air Evaporation Test A. Synthetic B. Coastal C. Mid-Continent

per gallon of tetraethyllead in the tests on the coastal oil, the solvent-refined neutral, and the solvent-refined blend (tests 1, 4, and 5 with 9, 11, and 10). The effect of the tetraethyllead in straight-run fuel was to increase the octane requirement increase by 6 to 8 numbers.

EFFECT ON OCTANE REQUIREMENT INCREASE AND DEPOSIT Weight. To include both the lead effect and commercial fuel effect, a series of tests was done using L-4 (CRC-L-4-545 test) fuel, which was a blend of 20% straight-run and 80% cracked containing 3 ml. of tetraethyllead per gallon (see Table VI). In this series of tests four oils gave much higher deposit weights than at 0.5 ml. of tetraethyllead, but about the same octane requirement increase (high). These oils were: white oil, a coastal oil, a blend of solvent-refined neutral and overhead bright stock, and

the latter containing chromium and manganese naphthenates. The oil containing the naphthenates is the same composition, which showed an octane requirement increase value of 1 with unleaded straight-run fuel. With the leaded fuel the octane requirement increase increased to 16-perhaps because of the inactivation of a catalytic effect by lead compounds.

The other three oils which were tested might be considered as synthetic oils. These gave low octane requirement increase values. The oils were a synthetic polyether oil (test 19) giving an octane requirement increase of 3 and a low deposit weight, a synthetic polybutene oil (No. 20) with an octane requirement increase of 4 and a very low deposit weight, and a 132° F. melting point paraffin wax (No. 21) with an octane requirement increase of 3 and an intermediate deposit weight. These three oils all have a high volatility or low decomposition temperature, which may explain the low deposit weight and octane requirement increase. These results were obtained even though a high lead content and a gasoline containing a high proportion of cracked materials were used.

These studies show that lead residues are collected in the combustion chamber by oil residues under these mild engine conditions. The amount of lead residue collected apparently is dependent on the deposit-forming properties of the oil.

The low octane requirement increase obtained with paraffin wax has some

special interest. In the recent literature (6, 11) it has been customary to ascribe poor engine deposit properties to "paraffinic" oils and improved performance to "naphthenic" oils. The good result shown for paraffin wax suggests that paraffinic materials are not inherently objectionable. A more accurate nomenclature would classify oils as naphthenic (poor deposit properties) and aromatic (good deposit properties). On this basis there are volatility differences which can explain the observed results.

AIR EVAPORATION TESTS ON ENGINE-TESTED OILS

In Table VII are shown the physical properties of the oils used in the engine studies described above. No relation was found between the Conradson carbon values and the engine results. The air evaporation test showed some qualitative relationships with the engine data.

For example, the two synthetic oils and the paraffin wax (Table VI), which gave low engine octane requirement increase and deposits, showed very low air evaporation residues. The white oil and coastal oil had intermediate residue values, and the solventrefined blend gave a high result. These residue values rated the oils in the same order as the Engler 90% point, or the highest (decomposition) temperature recorded in an attempt at distillation. Thus, the air evaporation test predicted the engine proper-

TABLE V. OIL COMPOSITION VS. ENGINE DEPOSIT WEIGHT AND OCTANE REQUIREMENT Increase

(Straight-run fuel, 0.5 ml. TEL)

No.	Oil Type	v.i.	100° F. Vis.	Engler 90% Pt.,	Equilib- rium ORI	Piston Top Deposit Wt., G.	Residue, Air Evaporation Test
9	Coastal A	34	525	900	14	12.4	9.5
10	Blend of solvref. Mid-C. 40% 4 + 60% (85 at 210° F. vis.)	98	4 52	1003	12	14.8	21.6
11	Heart-cut solvref. Mid-C. (test 4)	95	157	870	9	8.7	8.5
12	11 + 16% Paratone	127	557		8	4.5	9.7
13	11 + 11% Aeryloida	141	478		8	4.6	7.4
14	11 + 31% Polybuteneb	105	500		8	8.5	12.8
	Blend of 50 parts 150 + 125 Indopol H-35.	parts 7	10.				

TABLE VI. OIL COMPOSITION VS. ENGINE DEPOSIT WEIGHT AND OCTANE REQUIREMENT INCREASE

 $(L-4 fuel^a)$

No.	Oil Type	V.I.	100° F. Vis.	Engler 90% Pt.,	Equilib- rium ORI	Piston Top Deposit Wt., G.	Weight % Residue, Air Evaporation Test
15	Heavy white oil	83	368	918	13	23.0	9.9
16	Coastal B	28	616	939	13		11
17	Blend of solvref. Mid-C. 68% 4 + 60% (85 at 210° F. vis.)	98	452	1003	11 6	29.75	2 1.6
18	5 + 0.25% chromium naphthenate + 0.25% manganese naphthenate	98	452	1003	16	21.5	3 9
19	Synthetic polyether	141	312	821 °	3	7.5	2.1
20	Polybutene ^d	105	516	792°	4	4.4	3.5
21	132° F. m.p. pffn. wax			806	3	12.5	3.4
а	20% straight-run + 80% cr	acked.	TEL cont	tent 3 ml. p	er gallon.		

b Premium commercial fuel. TEL content 1.1 ml. per gallon.

Decomposition temperature
 Indopol L-50, mol. wt. 660.

					TABLE	VII. Properties of Oils Used in Initial Engine Studies	ERTIES O	r Oils 1	Used II	n Initi	al Eng	INE ST	UDIES							
Table Tabl			Vis.	(SUS)		%	A D.						Engler	Distillat						%
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$		V.I.	H	7. F.		Carbon	Grav.	1	2%	10%	20%	30%	1		1		. ^			Recovered
312 6.2.7 13.4 24.9 659 736 766 804 851 854 873 884 888 919 945 813 836 831 850 864 873 884 889 919 312 62.7 2.1 0.012 32.2 688 751 770 780 783 894 832 839 860 870 870 890 974 989 1003 910 452 60.8 21.6 0.02 32.2 688 771 777 806 824 892 893 860 870 870 870 974 980 910 974 910 <t< td=""><td></td><td>34</td><td>525</td><td>55.5</td><td></td><td>0.039</td><td>22.5</td><td></td><td>727</td><td>734</td><td>799</td><td>814</td><td>825</td><td></td><td></td><td></td><td></td><td>000</td><td>933</td><td>97.5</td></t<>		34	525	55.5		0.039	22.5		727	734	799	814	825					000	933	97.5
312 62.7 2.1 0.012 11.0 570 813 833 839 838 821 Decomposition 157 43.7 43.7 43.7 730 773 770 780 783 804 832 839 860 870 893 910 452 60.8 21.6 0.03 30.2 693 714 777 806 824 892 950 960 974 989 1005 1056 1056 1056 1056 1056 1056 1056<		65	313	50.0	13.4		24.9	629	736	992	808	845	851					88	919	98.3
157 43.7 8.6 0.002 32.2 688 751 773 770 780 783 804 832 839 860 870 870 896 974 890 970 870 970 971 970 771 806 824 892 960 974 980 970 970 970 970 971 772 806 874 870 974 980 970		141	312	62.7	2.1	0.012	11.0	570		813	833	839	838	821			Decon	nposition		
452 60.8 21.6 0.03 30.5 693 714 777 806 824 892 939 960 974 989 1003 1016 1035 458 64.3 99.9 0.005 29.3 687 783 794 825 830 810 836 849 870 909 939 954 516 65.5 3.5 0.018		95	157	43.7	8.5	0.002	32.2	889	751	753	770	780	783							97.6
459 61.5 24.8 0.185 29.3 709 751 763 784 804 830 863 993 1058 1063 b 868 54.3 9.9 0.005 29.3 687 783 794 825 830 856 868 879 891 905 918 944 810 58.0 11.0 0.054 23.0 601 622 733 785 802 810 836 849 870 900 939 954 811 516 66.5 3.5 0.018		86	452	8.09	21.6	0.03	30.5	693	714	777	908	824	892							98.4
368 54.3 9,9 0,005 29,3 687 783 784 825 830 856 868 879 891 905 918 944 616 58.0 11.0 0.054 23.0 601 622 733 785 80 810 836 849 870 900 939 954 516 66.5 3.5 0.018 438 537 564 614 665 694 797 797 792 Decomposition 37.1 3.4 671 712 714 750 760 766 775 785 794 806 843 516 30.8 643 870 880 903 916 93 916 93 916 93 916 93 916 93 916 950 950 950 950 950 950 950 950 950 <		86	459	61.5	24.8	0.185	29.3	209	751	292	784	804	830)63 b			
616 58.0 11.0 0.054 23.0 601 622 733 785 802 810 836 849 870 900 939 954 516 66.5 3.5 0.018 438 537 564 614 665 694 797 797 792 Decomposition 37.1 3.4 712 714 750 752 760 766 775 785 794 806 843 516 19.2 840 873 880 90 903 916 93 942 950 958 1000 1590 57.2 27.2 1060 1060 1060 93 916 93 916 93 950 958 1000		88	368	54.3	6.6	0,005	29.3	289	783	794	825	830	856					918	944	98.0
516 66.5 3.5 0.018 438 537 564 614 665 694 797 792 Decomposition 37.1 3.4 671 712 714 750 752 760 766 775 785 794 806 843 516 19.2 840 873 880 90 903 916 930 942 950 958 1000 1590 57.2 1020 1050 1060 1060 1060 Decomposition		28	616	58.0	11.0	0.054	23.0	109	622	733	785	803	810					939	954	96.0
37.1 3.4 643 712 714 750 752 760 766 775 785 794 806 843 516 19.2 840 873 880 890 903 916 930 942 950 958 1000 1590 57.2 1020 1050 1060 1060 Decomposition		105	516	66.5	3.5	0.018		438		537	564	614	665				792	Dec	omposition	
516 19.2 840 873 880 890 903 916 930 942 950 958 1590 57.2 1020 1050 1060 2060 Becomposition	Paraffin wax microcrystal- line wax	:	:	37.1	3.4 30.8	:		671 643	712	714	750	752	094	766 Deco	775 mpositio			908	843	0.66
		95 95	$\begin{array}{c} 516 \\ 1590 \end{array}$;;	19.2	::		840 1020		873 1050	880 1060	890	903			942 gecombos		958	1000	

ties of the low deposit-forming oils, but the engine did not differentiate between an intermediate and high air evaporation residue.

The air evaporation test showed a wide difference in residue weight for the solvent-refined neutral and its blend containing overhead bright stock (Table V) in agreement with the engine deposit data. The addition of polymers to the solvent-refined neutral did not increase the air evaporation residue weight or engine deposits. So in this comparison the air evaporation test gave the same relative differentiation as the engine on the effect of the addition of a bright stock and polymers to a solvent-refined

EVALUATION OF OIL BLENDS

In the preceding sections it was shown, in an exploratory manner, that special combinations of lubricants and fuels could be selected which would minimize octane requirement increase and deposits. An important question was the performance which would be obtained with typical petroleum-derived oil blends when used in combination with a leaded commercial fuel. To answer this question, the eight oil blends whose physical properties are shown in Table VIII were prepared and subjected to the Chevrolet CCD test and the air evaporation test. The oil blends were made up to an SAE 20 viscosity grade, with all of the oils having the same 210° viscosity of 45 Saybolt seconds. The oils included a heart-cut solvent-refined neutral and a neutral blended with the following:

- Overhead, solvent-refined bright stock
- Residual, solvent-refined bright stock Residual, Pennsylvania bright stock
- 3.
- VI improver A VI improver B

Also tested were a low viscosity index coastal neutral and a blend of a coastal neutral and coastal bright stock. One per cent of a commercial zinc dithiophosphate lubricating oil additive was added to each blend.

The three bright stock blends were tested in duplicate engine tests, while the other five oils were submitted to single tests. The results (Table IX) from the duplicate tests illustrate the repeatability of the engine procedure on octane requirement increase and deposit weights. A commercial regular fuel having a lead content of 1.5 ml. per gallon was used. In the engine tests the piston top, inlet valve, and exhaust valve deposits were weighed separately and their carbon contents were determined.

The test results are shown in Table IX. On the basis of deposit weights, the fuels fell into two groups, one of which gave two or three times as much deposit weight as the other. In spite of these large differences in deposit weights, no significant differences in octane requirement increase were observed. The similarity in octane requirement increase results might be attributed to the commercial fuel (4, 11, 12).

Even though octane requirement increase differences were not observed, it would appear desirable to minimize combustion chamber deposits as much as possible by using the optimum techniques of motor oil blending. The data show that the residual solvent-refined bright stock and the residual Pennsylvania bright stock gave the highest deposit weights and total grams of engine carbon. The overhead, solvent-refined bright stock gave nearly as much total engine deposit, but a slightly smaller amount of carbonaceous deposit. The solvent-refined neutral oil gave only about one half as much deposit as the bright stock blends. The addition of viscosity index improver A to the neutral oil blend gave results similar to the neutral oil, but the use of viscosity index improver B caused a decrease in deposit weight similar to that shown in Table VI. It is noteworthy that such a low concentration (1.15%) of viscosity index improver could affect deposit weight. The coastal neutral and the coastal bright stock blends gave low deposit weight results which were even below those obtained with the high viscosity index neutral. Thus, the

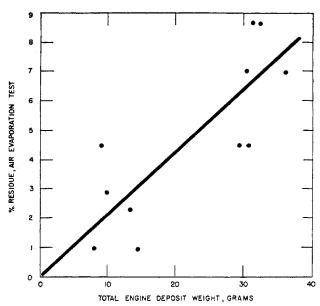


Figure 3. Total Engine Deposit Weight vs. Per Cent of Air Evaporation Test

Data from Table IX

coastal bright stock did not contribute to deposit formation as did the high viscosity index bright stock.

The carbon contents of the deposits showed little variation between the oils, again suggesting that the oil residues capture the lead residues. The inlet valve deposits showed a much higher carbon content than the piston top deposits, undoubtedly because this is a cooler region of the combustion chamber. The ratio of deposit weights between the low deposit-forming oils and the high deposit-forming oils was similar for both inlet valve and piston tops.

An interesting and unexpected result was the variation in exhaust valve deposit weights. The oils containing high viscosity index bright stocks showed two to three times as much exhaust valve deposit as the other oils. The result was unex-

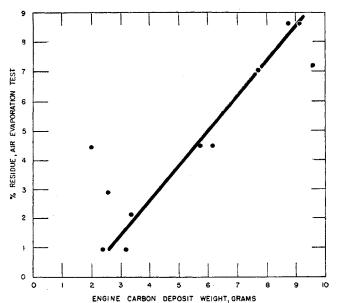


Figure 4. Engine Carbon Deposit Weight vs. Per Cent Residue of Air Evaporation Test Data from Table IX

COMPOSITION AND PROPERTIES OF OILS" AND BLENDING STOCKS USED IN FINGINE DEPOSIT STUDY TABLE VIII.

		80% 80% 85%	865 921 969	851 896 1042	850 889 1008	820 840 858	790 811 860	790 813 829	769 801 823	780 822 853	
		70% 80	830 8	823 8	829 8	800 8	783 79	778 7	745 70	7 097	
	$q^{\mathbf{u}}$	%09	818	608	811	783	770	762	728	741	
	Engler Distillation ^b	20%	908	798	803	770	761	751	710	729	
	gler Di	40%	791	790	788	756	753	743	969	712	
		30%	780	777	783	743	741	738	683	701	
		•	769	768	763	733	734	730	670	069	
		10%	754	757	756	725	722	722	655	629	
		, 5%	3 742	2 742	7 743	. 712	714	718	648	899	
		2%	723	732	727	:	:	:	:	:	
		IBP	708	269	669	670	620	119	588	640	
Cop			0.01	0.02	0.12	0.27	0.20	0.20	0.22	0.29	
Wt. % Residue	Air Evap.	Test	7.0	8.6	4.6	1.0	2.2	1.0	2.9	4.5	
		V.I.	26	94	86	96	109	115	61	r.	95
(SOS)	100° 210°	Ξ.	45	45	45	45	45	45	45	45	42.7
Vis.	100	Ŧ	179	182	178	180	169	163	362	262	145
		Oil Composition	86.5% A + 13.5% overhd. solvref. brt. stk. (92 V.I., 154 vis. at 210° F.)	92.5% A + 7.5% resid. solvref. brt. stk. (94 V.I., 238 vis. at 210° F.)	91. 5% A + 8.5% resid. Penn. brt. stk. (99 V.I., 154 vis. at 210° F.)	25 Heart-cut high V.I. neutral Heart-cut solvref. Mid-C.	98.25% A + 1.75% V.I. improver A	97.7% A + 1.15% V.I. improver B	51.9% Coastal neut, (8 VL-47 vis. at 210° F.) + 48.1% Coastal neut. (-2 V.I., 43 vis. at 210° F.)	87.5% Coastal neut. (-2VI, 43 vis. at 210° F.) + 12.5% coastal brt. stk. (-38 V.I., 83 vis. at 210° F.)	Heart-cut solvref. neut.
		Name	Overhead brt. stk. blend	23 Residual brt. stk. blend	24 Penn brt. stock blend	Heart-cut high V.I. neutral	26 Improver blend	27 Improver blend	28 Coastal neutral	29 Coastal brt. stk. blend	Oil A
		No.	22								

 a All oils contained 1% zinc hexyl dithiophosphate additive. b ASTM Method D 1160–51T.

TABLE IX. ENGINE OCTANE REQUIREMENT INCREASE, DEPOSIT WEIGHT, AND DEPOSIT ANALYSIS DATA (Fuel, commercial regular, 1.5 ml. TEL per gallon)

Eng.		Corr.	Combus. Zone	Total Eng.	Pistor	Top Dep	osits	Inlet	Valve Dep	osits		
Test No.	Blend	Equil. ORIª	Deposit, G.	Carbon, G.	Weight,	Carbon,	Carbon,	Weight,	Carbon,	Carbon,	Exhaust Va Deposit, g.	% Carbon
22	Overhead brt. stk.	9	$\frac{29.8}{30.1}$	6.3 5.6	$\frac{20.7}{21.5}$	$\substack{15.3\\11.8}$	$\substack{3.2 \\ 2.5}$	$9.1 \\ 9.4$	$\begin{array}{c} 33.7 \\ 33.0 \end{array}$	$\frac{3.1}{3.1}$	$\begin{smallmatrix}2.2\\2.2\end{smallmatrix}$	
23	Residual brt. stk.	9 11	$35.5 \\ 30.4$	$\frac{9.8}{7.5}$	$\frac{23.7}{20.1}$	$\frac{24.4}{18.4}$	$\substack{5.8\\3.7}$	$\substack{11.9\\10.3}$	$\frac{33.4}{36.6}$	$\begin{smallmatrix}4.0\\3.8\end{smallmatrix}$	2.0	2.5
24	Penn brt. stk.	14 11	$\frac{32.4}{31.5}$	$\substack{8.6\\9.1}$	$\frac{22.2}{18.8}$	$\substack{22.8\\21.9}$	5.0 4.1	$\begin{smallmatrix}10.3\\12.8\end{smallmatrix}$	$\begin{array}{c} 35.1 \\ 39.1 \end{array}$	$\begin{array}{c} 3.6 \\ 5.0 \end{array}$	$^{1.2}_{1.7}$	
25	Heart-cut high V.I. neutral	10	14.5	3.1	9.2	20.8	1.9	5.3	22.9	1.2	0.8	
26	V.I. improver A blend	9	13,1	3.2	6.7	19.7	1.3	6.4	30.0	1.9	0.9	
27	V.I. improver B blend	8	8.8	2.2	5.1	20.5	1.0	3.7	33.7	1.2	0.9	
28	Coastal neutral	8	10.0	2.7	5.2	22.3	1.1	4.8	32.9	1.6	0.7	1.5
29	Coastal brt. stk.	9	9.6	2.0	6.4	18.5	1.2	3.2	24.8	0.8	0.9	

^a Corrected ORI (equilibrium) = measured ORI + 2 (29.4 - barometric pressure in inches of Hg (+ 0.25) humidity, grains/lb. of dry air - 80).

pected because this zone of the combustion chamber operates at a rather high temperature and the deposits were not carbonaceous in nature, as indicated by the low carbon analyses of 1.5 to 2.5%. These results suggest that oil composition, aside from additive content, may play a part in the amount and type of exhaust valve deposit and valve durability.

CORRELATION OF TEST RESULTS

Good correlation was found between the air evaporation test residue and engine deposit weights. As shown in Figure 3, the air evaporation test roughly predicted the total engine deposit weight, although the engine did not differentiate to the same degree as the test. The total engine carbon deposit weight (Figure 4, based on piston top and inlet valve deposits) is more closely reflected in the air evaporation test. The only oil which deviated from the correlation line was the coastal bright stock blend, which formed more residue in the air evaporation test than in the engine.

Oil volatility, as originally suggested by Bahlke (1), also predicted the amount of engine deposit. As shown in Figure 5, the Engler 95% point showed correlation with the total engine deposit weights, although again the engine was not so sensitive as

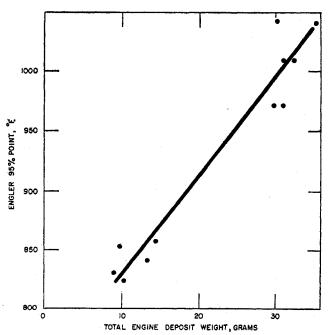


Figure 5. Engine Deposit Weight vs. Engler 95% Point

the test. A clearer picture of oil volatility differences is shown in Figure 6. These data illustrate the tail-end volatility difference between the residual and overhead bright stock blends and the fact that the coastal bright stock blend, even though it contained a high viscosity blending agent, was more volatile than the high viscosity index neutral oil.

EFFECT OF PHOSPHORUS COMPOUNDS

Another approach to the problem of minimizing the contribution of motor oils to combustion chamber deposits is the use of additives. Such additives probably should function as antioxidants at combustion chamber temperatures. By delaying oxidation, a larger percentage of the oil would have an opportunity to vaporize and leave the combustion chamber.

To evaluate this concept, a series of phosphorus compounds was tested in the air evaporation test. Two of the more promising additives were then submitted to Chevrolet CCD tests with leaded and unleaded fuels. The oil used in this study was a blend of solvent-refined neutral and overhead bright stock (see Table VIII, engine tests 5, 10, and 20).

As shown in Table X, P₄S₃ and P₄Se₃ (3, 15) effected a reduction in air evaporation residue weight by 40%. These two additives, when engine tested in the same oil, using unleaded straight-run fuel, reduced piston top deposit weights by 45 and 30%, and gave significant decreases in octane requirement increase (Table X).

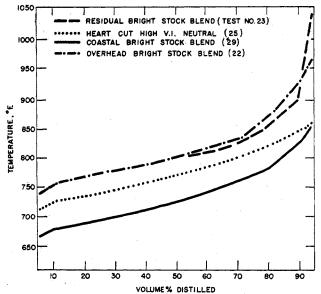


Figure 6. Engler Distillation Curves of Four Oils

% Reduction

TABLE X. EFFECT OF PHOSPHORUS ADDITIVES ON ENGINE OCTANE REQUIREMENT INCREASE AND DEPOSIT WEIGHT

(Oil blenda of 95 V.I. heart-cut solvent-refined Mid-Continent oils)

Concn.,	Additive	Fuel	TEL Con- tent	Equilib- rium ORI	Piston Top Deposit Wt. G.,	in Engine Deposit Wt. Due to Addtv.	Evap., Test, Wt. %
	None	Straight-run	0	5	3.3		22.3
	None	L-4	3	11	29.7		
0.25	Phosphorus sesquisulfide	Straight-run	0	1	1.8	45.3	13.5
0.25	Phosphorus sesquisulfide	L-4	3	10	33.8		
0.25	Phosphorus sesquiselenide	Straight-run	0	2	2.3	30.3	12.6
0.25	Phosphorus sesquiselenide	L-4	3	12	31.1		
40%	(43.7 at 210° F. vis)	+ 60% (85 at	210° F	. vis.).			

The reduction in engine deposit weight was comparable to that obtained in air evaporation test residue.

These same additives were also engine tested using a leaded fuel containing cracked components (L-4 fuel). In the presence of the lead and fuel factors the effectiveness of the additives was not evident.

Several significant deductions may be made from these results.

Lubricating oil oxidation may be retarded in the temperature region of 625° F.
Such antioxidant action decreases residue formation, probably

by increasing the time for oil volatilization before carbonization.

'he air evaporation test can be used to study such effects. This antioxidant activity can be observed in terms of reduced engine combustion chamber deposits and octane requirement increase, in the absence of fuel and lead effects.

SUMMARY

A bench-scale test, called the air evaporation test for measuring the combustion chamber deposit-forming tendencies of motor oil, and a laboratory engine procedure called the Chevrolet CCD test were developed. Utilizing these tools, it was demonstrated that lubricant composition is an important variable in the formation of carbonaceous combustion chamber deposits.

The tendencies of an oil to form deposits may be predicted by oil volatility or air evaporation test residue. Several high volatility or thermally decomposed oils gave low engine deposit values and low octane requirement increase when used with leaded commercial fuels.

Two coastal oils, a light neutral and its blends with two viscosity improvers, gave substantially lower engine deposit weights than comparable blends containing relatively nonvolatile bright stocks. Octane requirement increase differences were not observed between these petroleum-derived oils.

The air evaporation test was used to demonstrate that oil antioxidants may be effective in minimizing residue formation at 625° F. The antioxidants were shown to decrease engine deposits and octane requirement increase in the absence of the fuel and lead factors.

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