

# TRANSPORT PHENOMENA

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## 1. DIMENSIONAL ANALYSIS

Dimensional analysis is an invaluable tool when dealing with complex phenomena, since it helps to simplify them and to stress the important physical relationships of their parts instead of diffusion physics into complex mathematical relationships.

In transport processes, a useful guide to perform dimensional analysis is the following:

- (1) identify relevant transport properties, like fluid velocity, thermal energy flux, mass flux and so on;
- (2) identify relevant material properties, such as viscosity, thermal conduction, specific heat, density and so forth;

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- (3) choose an independently dimensional set according to the phenomenon class; *i.e.*, mechanics,  $\{M, L, T\}$  or alternatively  $\{F, L, T\}$ , thermal transport  $\{E, L, T, \Theta\}$ ;
- (4) find the number of dimensionless quantities using the  $\Pi$ -theorem:

$$n = p - r ,$$

where  $n$  is the number of dimensionless quantities,  $p$  the number of physical quantities given by the model and  $r$  the number of elements of the dimensional set;

- (5) choose the first  $\Pi$  quantity using the physical quantity being seek;
- (6) choose the rest of the  $\Pi$  quantities using the dimensions of the set;
- (7) form the model equation of the form:

$$f [\Pi_i] = 0 ,$$

where the index  $i$  runs from 1 to  $n$ .

- (8) form the final model equation by isolating the first  $\Pi$  quantity, which contains the quantity being seek; *i.e.*,

$$\Pi_1 = f [\Pi_{i-1}] ;$$

- (9) finally, seek the final form of the function  $f$  by using guessing, approximations, extreme cases, and so forth.

*Example.* Consider the case of a sphere of diameter  $d$  and mass  $m$  falling vertically in a tank of side  $l$  containing a fluid of density  $\rho_f$ . The equation of motion for the sphere velocity  $u$  reads <sup>1</sup>

$$m\dot{u} = mg - f_d ,$$

where  $g$  represents the acceleration due to gravity and  $f_d$  the drag force.

When the sphere attains its terminal velocity,  $u_t$ , then the drag is exactly balanced by the gravitational force. The task is then to obtain an expression for the drag as a function of the sphere and fluid properties.

*Solution.* The motion of the sphere disturbs the fluid around it and causes fluid flow. This fluid flow results in friction causing a frictional drag that exerts a force on the sphere. Since the frictional resistance to flow is due to viscous stresses, it is expected that the fluid dynamic viscosity  $\mu$  will be important in determining the frictional force. In addition, the force is expected to depend on the velocity of the sphere  $u$ , since a higher speed would result in a larger force. The length scales that could affect the flow are the width of the tank  $l$  and the radius of the sphere  $r$ . The density of the fluid  $\rho_f$  could also be important, since a higher force is required for accelerating a fluid with a higher density.

It is important to note that the mass of the sphere or its density should not be relevant determining the flow, once the sphere velocity is specified. This is because the fluid velocity around the sphere, which results in the frictional force, is determined by the velocity with which the sphere is moving, and the mass or density of the sphere does not affect the fluid velocity. Similarly, the acceleration due to gravity determines the gravitational force on the sphere, but does not directly affect the fluid velocity around the sphere, once the sphere velocity is specified. Therefore, it is necessary to apply some judgment at the start of dimensional analysis to distinguish the material and dynamical properties that influence in the desired quantity. It is essential to ensure that no irrelevant quantity is included in the analysis.

Now that all the relevant dimensional quantities for the drag force have been determined, it is necessary to examine which are the *important* ones. This is a skill, and can be developed only by practice. In this particular case, let us look at the length scales that are likely to be important. If the width and height of the container are large compared to the radius of the sphere, it is likely that only the radius of the sphere is a relevant length scale. On the other hand, if the sphere is very close to one of the walls of the container, say within a few radii, then the distance from the wall as well as the radius of the sphere could be important. For definiteness, let us proceed with the assumption that only the radius of the sphere is important in this case. This results in a set of important variables:

- (1) radius of sphere,  $r$ ;
- (2) velocity of sphere,  $u$ ;
- (3) dynamic viscosity of fluid,  $\mu$ ; and

<sup>1</sup> The complete model takes into account buoyancy; *i.e.*,  $m\dot{u} = mg - f_d - f_b$ , where  $f_b$  represents the buoyancy force. In this example, however, in order to stress the exposition of the dimensional analysis principles, buoyancy is ignored.

- (4) density of fluid,  $\rho_{\text{fl}}$ .

So an equation for the force has to have the form

$$f_d = f[r, u, \mu, \rho_{\text{fl}}] .$$

Since this is a dynamical problem and a force is being sought, then the set of dimensional quantities chosen is  $\{F, L, T\}$ . In such a system, the chosen variables have the dimensions:

- radius of sphere,  $\dim r = L$ ;
- velocity of sphere,  $\dim u = L/T$ ;
- dynamic viscosity of fluid,  $\mu = F/TL^2$ ; and
- density of fluid,  $\rho_{\text{fl}} = FT^2/L^4$ .

Since there are five dimensional quantities and three dimensions involved in the above relationship, there are two dimensionless groups. One of these groups has to involve the drag, while the other is a combination of the sphere diameter, velocity, and fluid properties (density and viscosity).

Let us construct the first dimensionless quantity, which we call a scaled force  $\Pi_f$ , as a combination of the drag, viscosity, velocity and the sphere radius:

$$\Pi_f = f_d \mu^a u^b r^c ,$$

where  $a$ ,  $b$  and  $c$  are the desired indices which render  $\Pi_f$  dimensionless. The dimensions of the left and right sides of the equation are to be equal, thus they form a linear system that have to be solved simultaneously. The solution results in the coefficients  $a = b = c = -1$ . Therefore, the first dimensionless quantity is equal to

$$\Pi_f = \frac{f_d}{\mu u r} .$$

The second dimensionless quantity, which we call  $\Pi_{\text{re}}$ , is a combination of the density, diameter, sphere velocity and viscosity. We write this as,

$$\Pi_{\text{re}} = \rho u^a r^b \mu^c .$$

In defining the dimensionless group, the exponent of any one of the quantities can be set equal to 1 without loss of generality. In the last equation, we have chosen to set the exponent of the density equal to 1, to bring it in accordance with the conventional definition of the Reynolds number defined a little later. The dimensions of the quantities on the right side of such an equation are, after having solved a similar system of equations,  $a = b = 1$  and  $c = -1$ . Therefore, the dimensionless number

$$\Pi_{\text{re}} = \frac{\rho u r}{\mu} .$$

The relationship between the two dimensionless quantities can finally be written as

$$g[\Pi_f, \Pi_{\text{re}}] = 0 \implies \Pi_f = \frac{f_d}{\mu u r} = h[\Pi_{\text{re}}] ,$$

where  $h$  is a function of the Reynolds number; *i.e.*,  $\Pi_{\text{re}}$ .

In the last equation, the force has been non-dimensionalized by the ‘viscous force scale’,  $(\mu r u)$ . Instead of using the viscosity, radius and velocity to non-dimensionalize the force, we could have chosen to use the density, radius and velocity instead. This would have led to the dimensionless group  $\Pi_{fI} = f/\rho u^2 r^2$ , where  $(\rho u^2 r^2)$ , the ‘inertial force scale’, is a suitable combination of density, velocity and radius with dimensions of force. It is easily verified that the dimensionless forces scaled in these two different ways are related by,

$$\Pi_f = \Pi_{\text{re}} \Pi_{fI} .$$

The Reynolds number is then a ratio of the inertial and viscous force scales,

$$\Pi_{\text{re}} = \frac{\rho u^2 r^2}{\mu r u} .$$

That is why the Reynolds number is often referred to as the balance between the viscous and inertial forces.

Further simplifications can be made in some limiting cases. When the group  $\rho u r / \mu$  is very small, then the fluid flow is dominated by viscous effects, thus, the drag should not determine on the inertial force scale. Therefore, the drag has the form  $\Pi_f = \Pi = \text{constant}$  or

$$f_d = \Pi \mu u r .$$

The limitation of dimensional analysis is that the value of the constant cannot be determined, and more detailed calculations reveal that the exact value of the constant is  $6\pi$ . This leads to ‘Stokes drag law’ for the force on a sphere in the limit of small Reynolds number,  $f_d = 6\pi \mu u r$ .

The Reynolds number can be physically interpreted as the ratio of inertial and viscous forces or as the ratio of convection and diffusion. The latter interpretation is more useful, since it has analogies in mass and thermal transfer processes. It can be proven that the diffusion coefficient

for momentum, is the ‘kinematic viscosity’,  $\nu = \mu/\rho$ , where  $\rho$  is the mass density. It is easy to verify that the kinematic viscosity has the same dimensions as the mass diffusion coefficient,  $L^2/T$ . The Reynolds number can be written as  $\Pi_{re} = ur/\nu$ , which is the ratio of convective transport of momentum (due to the fluid velocity) and diffusive transport due to momentum diffusivity.

This type of analysis could be extended to more complicated problems. For instance, if the particle falling is not a sphere but a more complicated object, such as a spheroid, then there are two length scales, the major and minor axes of the spheroid,  $r_1$  and  $r_2$ . In this case, the number of variables increases to 6 and there are three dimensional groups. One of these could be assumed to be the ratio of the lengths (aspect ratio) ( $r_1/r_2$ ).

## 2. DIMENSIONLESS QUANTITIES

Dimensionless groups can be classified into three broad categories, the dimensionless fluxes, the ratios of convection and diffusion and the ratios of different types of diffusion. Before proceeding to define dimensionless groups, we first define the diffusion coefficients for mass, momentum and energy, in order to provide a definite basis for the discussion. Here, we restrict ourselves to the macroscopic definition.

**2.1. Mass, momentum and energy diffusivities.** The fundamental constitutive relations in transport processes are the Fick’s law for mass diffusion, Fourier’s law for heat conduction and Newton’s law for viscosity. The respective diffusion coefficients can be defined as follows.

- When there is a concentration difference maintained across a slab of fluid, then there is transfer of mass from the surface at higher concentration to the surface at lower concentration. The mass flux (mass per unit area per unit time) is inversely proportional to the length and directly proportional to the difference in concentration or temperature across the material. If a concentration difference  $\Delta c$ ,  $\dim c = M/L^3$ , is maintained between two ends of a slab of length  $l$ , the mass flux  $m''$ ,  $\dim m'' = M/L^2T$ , is given by Fick’s law:

$$m'' = -\phi \frac{\Delta c}{l}.$$

Here, the negative sign indicates that mass is transferred from the region of higher concentration to the region of lower concentration.

- For the transport of thermal energy, the energy flux is related to the temperature difference by Fourier’s law. For a slab of material of length  $l$  with a temperature difference  $\Delta\theta$  across the material, the energy flux  $e''$  is given by

$$e'' = -k \frac{\Delta\theta}{l},$$

where  $k$  is the thermal conductivity, and the negative sign indicates that thermal energy is transferred from the region of higher to the region of lower temperature.

- The Newton’s law of viscosity relates the shear stress  $\tau$  (force per unit area at the wall) to the strain rate (change in velocity per unit length across the flow) for the simple shear flow of a fluid as shown in figure 1.1.2.

$$\tau_{xy} = \nu \frac{\Delta u_x}{l}.$$

It should be noted that there is no negative sign in Newton’s law, in contrast to Fick’s law and Fourier’s law. This is due to the difference in convention with regard to the definition of stress in fluid mechanics and the definition of fluxes in transport phenomena. The shear stress  $\tau_{xy}$  in Newton’s law is defined as the force per unit area at a surface in the  $x$  direction whose outward unit normal is in the  $y$  direction. In contrast, the fluxes are defined as positive if they are directed into the volume. Therefore, the shear stress is actually the negative of the momentum flux. If the stress is defined to the the force per unit area acting at a surface whose inward unit normal is in the  $x$  direction, then this would introduce a negative sign in Newton’s equation. However, it is conventional in fluid mechanics to define the stress with reference to the outward unit normal to the surface. As we will see later, this difference in convention will not affect the balance equations that are finally obtained for the rate of change of momentum.

Dimensionless quantity	Definition	Ratio
Reynolds number	$\Pi_{re} = \rho ul / \mu$	momentum convection to momentum diffusion
Prandtl number	$\Pi_{pr} = \nu / \phi_h$	momentum diffusion to thermal diffusion
Schmidt number	$\Pi_{sc} = \nu / \phi$	momentum diffusion to mass diffusion
Peclet number	$\Pi_{pe} = ul / \phi_h$	thermal convection to thermal diffusion

TABLE 1. Dimensionless quantities that are ratios of diffusivities. The Prandtl number  $\Pi_{pr} = \nu / \phi_h = c_p \mu / k$  is the ratio of momentum and thermal diffusivity and the Schmidt number  $\Pi_{sc} = \mu / \rho \phi = \nu / \phi$  the ratio of momentum and mass diffusivity.

In this course, we will adopt the convention of defining the stress  $\tau_{xy}$  as the force per unit area in the  $x$  direction acting along a surface whose outward unit normal is in the  $y$  direction and use the last equation for Newton's law of viscosity.

The diffusion coefficients are the proportionality constants in the relationship between the flux of a quantity (mass, thermal energy, momentum) and the driving force. The flux of a quantity (mass, thermal energy, momentum) is the amount of that quantity transferred per unit area per unit time. The driving force for a quantity (mass, thermal energy, momentum) is the gradient (change per unit distance) in the density (quantity per unit volume) of that quantity. So the transport equations can be written in the general form

$$\left( \begin{array}{c} \text{transport of quantity} \\ \text{per unit area} \\ \text{per unit time} \end{array} \right) = \left( \begin{array}{c} \text{diffusion} \\ \text{coefficient} \end{array} \right) \frac{\left( \begin{array}{c} \text{change in density (per unit volume)} \\ \text{of the quantity} \\ \text{across the material} \end{array} \right)}{\text{thickness of the material}}$$

From dimensional analysis of the above equation, it is easy to see that the diffusion coefficients of all quantities have dimensions of  $L^2/T$ . These diffusion coefficients are defined from Fick's law, Fourier's law and Newton's law as follows.

- (1) From Fick's law, the diffusion coefficient  $\phi$  is the ratio of mass flux (mass transported per unit area per unit time) and the gradient in the concentration (mass per unit volume). Therefore, the diffusivity of mass is just the diffusion coefficient  $\phi$ .
- (2) It is possible to define a diffusion coefficient for heat transfer as follows. The difference in temperature  $\Delta\theta$  can be expressed in terms of the difference in the specific energy between the two sides as  $\Delta\theta = \Delta e / \rho c_v$ , where  $\Delta e$  is the specific thermal energy (per unit volume) and  $c_v$  the volumetric thermal capacity. With this, the equation for the thermal flux can be written as

$$e'' = \frac{k}{\rho c_v} \frac{\Delta e}{l}.$$

It is obvious that the above equation has the same form as the mass flux equation, with a thermal diffusivity  $\phi_h = k / \rho c_v$ , which has  $\dim \phi_h = L^2/T$ .

- (3) The *momentum diffusivity* is the relation between the flux of momentum (rate of transport of momentum per unit area per unit time) and the difference in the momentum density (momentum per unit volume). Consider the layer of fluid shown in figure 1.1.2. Since the momentum of a parcel of fluid is the mass of that parcel multiplied by its velocity, the momentum density is the product of the mass density  $\rho$  and velocity  $u_x$ . Therefore, the equation for the flux, expressed in terms of the momentum density, is

$$\tau_{xy} = \nu \frac{\Delta(\rho u_x)}{l},$$

where  $\nu$  is the momentum diffusivity. For an incompressible fluid with constant density, the momentum diffusivity is  $\nu = \mu / \rho$ . The momentum diffusivity, which has dimensions  $\dim \nu = L^2/T$ , is also referred to as the *kinematic viscosity*.

The dimensionless quantities ratios of diffusivities are summarized in Table 1.

**2.2. Ratio of convection and diffusion.** Convective transport takes place due to the mean flow of a fluid, even in the absence of a concentration difference. For example, if a fluid with concentration  $c$  travels with velocity  $u$  in a pipe, the total amount of mass transported per unit time is  $(cua_p)$ , where  $a_p$  is the cross-sectional area of the tube. Therefore, the flux (mass transported by the fluid, per unit area perpendicular to the flow per unit time) is  $(cu)$ . Consequently, the ratio between the rate of transport due to convective and diffusive effects is  $(ul/\phi)$ , where  $l$  is the length scale across which there is a change in the density of this quantity.

The dimensionless numbers which are ratios of convective and diffusive transport rates (Table 1)

- the Reynolds number,  $\Pi_{re} = \rho ul/\mu = ul/\nu$ , the ratio of momentum convection and diffusion,
- the Peclet number for mass transfer,  $\Pi_{pe} = ul/\phi$ , the ratio of mass convection and diffusion, and
- the Peclet number for thermal transfer,  $\Pi_{pe} = ul/\phi_h = \rho c_p ul/k$ , where  $c_p$  is the specific thermal capacity at constant pressure.

**2.3. Dimensionless numbers in natural convection.** In natural convection, the driving force for convection is the body force caused by a variation in the density of the fluid, which is in turn caused by variation in temperature. In contrast to natural convection, the characteristic flow velocity is not known *a priori*, but has to be determined from the driving force due to the density difference. If we assume there is a balance between the driving force and the viscous stresses in the fluid, dimensional analysis can be used to infer that the characteristic velocity should scale as  $u_c \approx fd/\mu$ , where  $f$  is the driving force for convection per unit volume of fluid,  $d$  is the diameter of the body or the characteristic length and  $\mu$  is the dynamic viscosity.

The driving force for convection, per unit volume of the fluid, is proportional to the product of the density variation  $\Delta\rho$  and the acceleration due to gravity  $g$ . The density variation is proportional to  $\rho\beta\Delta\theta$ , where  $\Delta\theta$  is the variation in temperature and  $\beta$  is the coefficient of thermal expansion. Therefore, the force per unit area is proportional to  $\rho g\beta\Delta\theta$ . With this, the characteristic velocity for the flow is  $u_c \approx \rho d^2 g\beta\Delta\theta/\mu$ . The *Grashof number* is the Reynolds number based upon this convection velocity,

$$\Pi_{gr} = \frac{\rho u_c d}{\mu} = \frac{\rho^2 d^3 g\beta\Delta\theta}{\mu^2}.$$

In defining the Grashof number, we used the momentum diffusivity and the body force to obtain the characteristic velocity scale. An alternative definition is the *Rayleigh number*, where the thermal diffusivity,  $k/\rho c_p$ , is used to determine the characteristic velocity. The characteristic velocity is then given by  $u_c \approx fd^2 c_p/k$ , where  $f = \rho\beta\Delta\theta$  is the driving force for convection per unit volume of fluid. The Reynolds number based on this convection velocity and momentum diffusivity is the *Rayleigh number*,

$$\Pi_{ra} = \frac{\rho^2 c_p d^3 g\beta\Delta\theta}{\mu k}.$$

The *Rayleigh-Benard* instability of a fluid layer heated from below occurs when the Rayleigh number increases beyond a critical value.

**2.4. Other dimensionless groups.** There are two important dimensionless groups involving surface tension, which are the *Weber number* and the *capillary number*. The Weber number is the ratio of inertial and surface tension forces,

$$\Pi_{we} = \frac{\rho u^2 l}{\gamma},$$

while the capillary number is the ratio of viscous and surface tension forces,

$$\Pi_{ca} = \frac{\mu u}{\gamma},$$

where  $\gamma$  is the surface tension,  $\dim \gamma = \text{F/L}$ .

In problems involving free interfaces, if the Reynolds number is low, inertial forces are negligible compared to viscous forces, and the capillary number has to be determined in

order to assess the ratio of viscous and surface tension forces. At high Reynolds number, it is appropriate to determine the Weber number in order to examine the ratio of inertial and surface tension forces. In addition to the Weber and capillary numbers, the *Bond number* is a dimensionless group appropriate for situations where a free interface is under the influence of a gravitational field. This dimensionless group is defined as the ratio of gravitational and surface tension forces,

$$\Pi_{bo} = \frac{\rho g l^2}{\gamma}.$$

**2.5. Dimensionless groups involving gravity.** The ratio of inertial and gravitational forces is given by the *Froude number*,

$$\Pi_{fr} = \frac{u^2}{gl},$$

In applications involving rotation of fluids, the Froude number is also the ratio of centrifugal and gravitational forces.

**2.6. Summary.** From the magnitudes of dimensionless quantities, one can immediately infer which effects are dominant and which are negligible. For instance, if the Reynolds number is small, then inertial effects are small compared to viscous effects. Thus, the effect of inertia can be neglected and fluid density is no longer an important parameter. However, it should be noted that though convective effects can be neglected with the Reynolds number or Peclet number is small, diffusive effects can not always be neglected even when these numbers are large, for reasons to do with the formation of momentum or thermal boundary layers near surfaces where these effects become important.

**2.7. Examples.** Some examples on the use of dimensional analysis and dimensionless quantities.

*Example.* A fluid flows through a pipe heated from the outside. The temperature of the wall of the pipe is higher than the average temperature of the fluid by a constant value  $\Delta\theta$ . The change in temperature of the fluid is due to the thermal transfer from the walls and not due to frictional heating generated by the flow. One would like to predict the rate of thermal transfer, per unit area of the wall of the pipe, so that the length of pipe required for the heat exchanger can be designed.

*Solution.* The first step is to collect the set of variables on which the thermal flux  $e''$  may depend. This can depend on the thermal properties of the fluid, the conductivity  $k$ , the specific thermal capacity  $c_p$ , the difference in temperature between the fluid and the wall  $\Delta\theta$ , the flow properties of the fluid, the density  $\rho$ , dynamic viscosity  $\mu$ , the average fluid velocity  $u$ , the diameter of the pipe  $d$  and the length of pipe  $l$ . The fundamental dimensions that we can classify these quantities into are  $\{M, L, T, \Theta\}$ .

There are nine dimensionless groups and four dimensions in Table 2, apparently necessitating five dimensionless groups. However, a further reduction is possible when *there is no interconversion between thermal energy (being transferred) and mechanical energy (driving the flow)*. In this case, it is possible to consider heat energy as a dimension H, because it is different from mechanical energy. There are now five dimensions,  $\{H, M, L, T, \Theta\}$ , and a total of nine dimensional quantities in Table 2. Therefore, there are only four dimensionless groups.

Of the dimensionless groups, the easiest one to is the ratio  $l/d$  of the length and diameter of the pipe. The dimensionless group containing  $e''$  is the *dependent* dimensionless quantity, which contains the dependent quantity, which has to be determined as a function of all the other *independent* quantities in the problem. For the independent variable  $e''$ , the relation is of the form

$$e'' d^a k^b \Delta\theta^c \mu^d \rho^e = \Pi_1.$$

The above relations can easily be solved to obtain  $a = 1$ ,  $b = c = -1$  and  $d = e = 0$ . Using these, the dimensionless group is

$$\Pi_1 = \Pi_{nu} = \frac{e'' d}{k \Delta\theta}.$$

The previous dimensionless quantity is known as the *Nusselt number*. In thermal transfer at a boundary (surface) within a fluid, the Nusselt number is the ratio of convective to conductive thermal transfer across (normal to) the boundary. In this context, convection includes both advection and conduction.

Quantity	Symbol	Dimension
Thermal flux	$e''$	$H/TL^2$
Pipe diameter	$d$	$L$
Pipe length	$l$	$L$
Average fluid velocity	$u$	$L/T$
Fluid density	$\rho$	$M/L^3$
Fluid viscosity	$\mu$	$M/LT$
Fluid specific thermal capacity	$c_p$	$H/M\Theta$
Thermal conductivity	$k$	$H/LT\Theta$
Temperature difference	$\Delta\theta$	$\Theta$

TABLE 2. Relevant quantities and their dimensions for the thermal energy transfer to a fluid flowing in a pipe.

Of the two other dimensionless groups, one can easily be identified as the Reynolds number,  $\Pi_{re} = \rho u d / \mu$ , the ratio of inertia and viscosity for this case. The second dimensionless group contains the specific thermal energy capacity,  $c_p$ . Since  $c_p$  contains both the thermal energy and mass dimensions, the dimensionless quantity has to contain the thermal conductivity,  $k$ , as well as the (viscosity  $\mu$  or density  $\rho$ ). The dimensionless quantity constructed with the specific thermal energy, viscosity and conductivity is the Prandtl number,

$$\Pi_{pr} = \frac{c_p \mu}{k}.$$

Therefore, the general expression for the average thermal flux can be written as

$$\frac{e'' d}{k \Delta\theta} = g \left[ \frac{l}{d}, \frac{\rho u d}{\mu}, \frac{c_p \mu}{k} \right]$$

or, more compactly, as

$$\Pi_{nu} = g \left[ \frac{l}{d}, \Pi_{re}, \Pi_{pr} \right].$$

Dimensional analysis has certainly simplified the problem, since it is much easier to deal with relationships between four dimensionless quantities, rather than with nine dimensional quantities. However, it is not possible to obtain further simplification using dimensional analysis. There are two possible ways to further simplify the problem. One is to do further analytic calculations that incorporate the details of the thermal and mass transfer processes. The other is to perform experiments and then to obtain empirical correlations between the parameters. In the latter case, it is sufficient to consider the variation in the thermal flux for variations in the dimensionless quantities alone and it is not necessary to examine variations in individual quantities.

*Example.* Consider a stirred tank reactor for heterogeneous catalysis, where the reactants and products are in solution and the catalyst is in the form of solid particles. The dissolved reactant R diffuses to the surface of the suspended catalyst particle, reacts at the surface and the product diffuses back into the fluid. It is necessary to determine the average flux of the reactant to the surface, given the difference in concentration  $\Delta c = c_\infty - c_s$ , where  $c_\infty$  is the concentration in the bulk and  $c_s$  is the surface concentration. There is also relative motion of characteristic velocity  $u$  between the catalyst particle and the fluid, due to stirring.

*Solution.* The different dimensional quantities of relevance are presented in Table 3.

The choice of dimensional quantities requires further discussion. It is clear that the average mass flux depends on the bulk concentration, the diffusion coefficient and the particle diameter. However, it is also necessary to include the fluid density, viscosity and the particle velocity relative to the fluid for the following reason. When the particle moves relative to the fluid, the generated flow pattern alters the distribution of the solute around the particles and thereby modifies the diffusion flux at the particle surface. The flow pattern, in turn, depends on the fluid viscosity, density and the flow velocity, and, therefore, the average mass flux could also depend on these.

In Table 3, there are seven dimensional quantities and three dimensions. On this basis, we would expect that there are four dimensionless quantities. However, a further simplification can be made by distinguishing between the mass dimension in the mass transport (the solute mass) and that in the flow dynamics (the mass of the total fluid). The flux and the diffusion coefficient contain the mass of the solute, whereas the mass of the fluid (solute plus solvent) appears in the density and fluid viscosity. If the solute concentration does not affect the fluid density and



Quantity	Symbol	Dimension	Modified dimension
Mass flux	$m''$	$M/L^2T$	$M_s/L^2T$
Diffusion coefficient	$\phi$	$L^2/T$	
Concentration difference	$\Delta c$	$M/L^3$	$M_s/L^3$
Particle diameter	$d$	$L$	
Particle velocity	$u$	$L/T$	
Fluid density	$\rho$	$M/L^3$	
Fluid viscosity	$\mu$	$M/LT$	

TABLE 3. Relevant quantities and their dimensions for the mass transfer to a particle.

viscosity, we can make a distinction between the mass dimension for the solute,  $M_s$ , from the mass dimension for the fluid,  $M$ . In the modified dimensions shown in Table 3, the mass flux and the diffusion coefficient depend on the solute mass  $M_s$ , while the density and viscosity depend on the fluid mass  $M$ . There are now four dimensions,  $\{M, M_s, L, T\}$ , and therefore there are only three dimensionless quantities.

The first dimensionless group can be constructed by non-dimensionalizing the flux by the diffusion coefficient, the concentration difference and the particle diameter:

$$\Pi_1 = m''(\Delta c)^a \phi^b d^c,$$

The indices  $a$ ,  $b$  and  $c$  are determined from dimensional consistency to provide the dimensionless flux, called the Sherwood number,

$$\Pi_{sh} = \frac{m'' d}{\phi \Delta c}.$$

Two other dimensionless groups can be defined. One of the dimensionless numbers is the Reynolds number,  $\Pi_{re} = \rho u d / \mu$ , the ratio of fluid inertia and viscosity. The second dimensionless group can be defined in two ways. One possible definition is the Schmidt number,  $\Pi_{sc} = \mu / \rho \phi$ , the dimensionless combination of the diffusivity, viscosity and density. The alternate dimensionless group is the Peclet number,  $\Pi_{pe} = u d / \phi$ , constructed from the flow velocity, diameter and the mass diffusivity. If we use the Reynolds and Schmidt numbers, then the dimensionless flux can be expressed as

$$\Pi_1 = \frac{m'' d}{\phi \Delta c} = g \left[ \frac{\rho u d}{\mu}, \frac{\mu}{\rho \phi} \right]$$

or, equivalently,

$$\Pi_{sh} = g [\Pi_{re}, \Pi_{pe}].$$

□

*Example.* In designing new processes, it is not sufficient to study the the process on the laboratory scale, but to also study the exact industrial set up on a small scale before building a larger scale industrial apparatus. Dimensional analysis plays a very important role in industrial scale up. Scaling up cannot be done by multiplying all parameters by a given factor, but the dimensionless groups have to be kept a constant while scaling up. This will be illustrated using the example of a stirred tank reactor. In this, the fluid is stirred using an impeller of a certain shape, and the impeller is to be designed so that optimum mixing is achieved for minimum power.

*Solution.* For a given impeller shape, it is necessary to estimate the power consumption for stirring at a given frequency  $f$ . The power consumption will, in general, depend on the shape and dimension of the impeller, as well as the vessel, as well as other details such as baffles, etc. If we keep the relative ratios of the lengths of the impeller, vessel, baffles, etc., a constant, then there is only one length scale in the problem, which we will consider the impeller diameter  $d$ . In addition, the power can also depend on the density of the fluid,  $\rho$ , the fluid viscosity  $\mu$  and the frequency of rotation  $f$ . An additional dependence arises on the acceleration due to gravity  $g$ . This is because sometimes during stirring, the interface of the fluid raises at the edges and lowers in the middle. This upward motion due to centrifugal forces is balanced by a downward force due to gravity and so gravity could also be an important factor. This is because it is important to ensure that the dimensions of the interface (curvature, extent of depression at the center) are also in the same proportion as the impeller diameter. When considering the interface, the surface tension (normally denoted by the symbol  $\gamma$ ) is also a relevant parameter. The surface tension has dimensions of force/length of

Quantity	Symbol	Dimension
Power	$p$	$ML^2/T^3$
Frequency	$f$	$1/T$
Diameter	$d$	$L$
Density	$\rho$	$M/L^3$
Viscosity	$\mu$	$M/LT$
Gravity	$g$	$L/T^2$
Surface tension	$\gamma$	$M/T^2$

TABLE 4. Relevant quantities and their dimensions for the calculation of the power required for the impeller in a reactor.

energy/area; *i.e.*,  $M/T^2$ . The relevant parameters with their dimensional dependencies are shown in Table 4.

The dimensionless variables derived above have the following physical interpretations. The power number,  $\Pi_{po} = p/f^3 d^5 \rho$ , is the dimensionless quantity that involves the dependent variable, the power, which has to be determined as a function of all the other independent variables. This gives the ratio of the power required to the work done by centrifugal forces. On the other hand, the Reynolds number,  $\Pi_{re} = \rho d^2 f / \mu$ , is the ratio of centrifugal forces and viscous forces, or the ratio of convection and diffusion. The dimensionless group  $f^2 d / g$  is the Froude number, which gives the ratio of centrifugal and gravitational forces. The dimensionless group  $\rho f d^3 / \gamma$  is the Weber number, which is the ratio of centrifugal and surface tension forces.

Since there are seven variables and three dimensions, it is possible to create four dimensionless groups. Let us assume these four contain  $p$ ,  $\mu$ ,  $g$  and  $\gamma$  expressed in terms of the other variables. Then, the four groups are  $(p/f^3 d^5 \rho)$ ,  $(f d^2 \rho / \mu)$ ,  $(f^2 d / g)$  and  $(\rho f^2 d^3 / \gamma)$ . Therefore, the expression for the power has to have the form:

$$\frac{p}{f^3 d^5 \rho} = g \left[ \frac{f d^2 \rho}{\mu}, \frac{f^2 d}{g}, \frac{\rho f^2 d^3}{\gamma} \right].$$

It is instructive to determine the order of magnitudes of the different dimensionless quantities in the problem. The density of the liquid is usually of the order of  $10^3 kg/m^3$ , the viscosity of a very viscous fluid such as a polymer melt could be as high as  $1 kg/m.s$  and the surface tension of a liquid-gas interface is, at maximum,  $0.1 kg/s^2$ . If the frequency is of the order of  $1 rev/sto 10 rev/s$ , the Froude number  $f^2 d / g \sim 0.1 to 10$ , indicating that both centrifugal and gravitational forces are important in the present problem. The Weber number  $\rho f^2 d^3 / \gamma \sim 104 to 106$ , which is large, indicating that the surface tension effects are small when compared to inertial effects. Therefore, the effect of surface tension can be neglected in the present application. The Reynolds number  $\rho d^2 f / \mu \sim 103 to 104$ , which is large. Therefore, it might naively be expected that viscous effects can be neglected in comparison to inertial effects. However, as it can be seen using analysis of boundary layers, diffusion *cannot* be neglected, because it is diffusive transport which is responsible for the transport of mass, momentum and energy at the bounding surfaces of the fluid. With the neglect of surface tension effects, the last relation reduces to

$$\frac{p}{f^3 d^5 \rho} = g \left[ \frac{f d^2 \rho}{\mu}, \frac{f^2 d}{g} \right].$$

In a scale up,

the dimensionless numbers have to be kept a constant.

For example, we are interested in designing a reactor with an impeller diameter of  $1m$  with a revolution of  $10 rev/s$  and the fluid in the reactor is water with density  $1000 kg/m^3$  and viscosity  $10^{-3} kg/m.s$ . In order to determine the performance, we design a smaller reactor with an impeller of size  $10cm$ . What is the fluid that should be used and what is the speed at which the reactor should operate? The speed of rotation can be determined from the consideration that the Froude number has to be a constant. If quantities for the big reactor are denoted with the subscript  $b$  and those for the small reactor are denoted by the subscript  $s$ , then for the Froude number to be a constant, we require

$$f_b^2 d_b = f_s^2 d_s.$$

Substituting the dimensions and the frequency of the big reactor, we get the impeller speed of the small reactor as  $316 rev/s$ . The choice of fluid to be used in the small reactor is determined by the condition that the Reynolds number has to be a constant:

$$\frac{\rho_b f_b d_b^2}{\mu_b} = \frac{\rho_s f_s d_s^2}{\mu_s}.$$

Relating the frequency and diameters of the two reactors, we get

$$\frac{\rho_s}{\mu_s} = 31.6 \frac{\rho_b}{\mu_b}.$$

Finally since the Reynolds number and the Froude number are kept a constant between the two configurations, the Power number is also a constant

$$\frac{p_b}{f_b^3 d_b^5 \rho_b} = \frac{p_s}{f_s^3 d_s^5 \rho_s}.$$

Therefore, the ratio of the power required in the two configurations is

$$\frac{p_b}{p_s} = 3160 \frac{\rho_b}{\rho_s}.$$

From the power requirement of the small reactor, the power estimate for the big reactor can be obtained using the above relation.

### 3. MASS AND THERMAL TRANSFER CORRELATIONS

**3.1. Dimensionless fluxes.** In mass and thermal transfer, non-dimensional fluxes are obtained by scaling the average flux by a factor

$$\frac{\text{diffusion coefficient} \times (\text{concentration or temperature difference})}{\text{characteristic length}}.$$

The dimensionless group for mass transfer is the *Sherwood number*

$$\Pi_{\text{sh}} = \frac{m''}{\phi \Delta c / l}.$$

The ratio of the flux and the concentration difference,  $m''/\Delta c$ , is called the *mass transfer coefficient*,  $k_m$ . Therefore, the Sherwood number is also written as

$$\Pi_{\text{sh}} = \frac{k_m l}{\phi}.$$

Analogous to the Sherwood number, the *Nusselt number* is a dimensionless thermal flux

$$\Pi_{\text{nu}} = \frac{e''}{\phi_h \Delta e / l},$$

where  $\phi_h$  is the thermal diffusivity and  $\Delta e$  is the difference in the energy density for a characteristic length  $l$ . Since  $\phi_h = k/\rho c_p$  and  $e = \rho c_p \theta$ , the Nusselt number becomes

$$\Pi_{\text{nu}} = \frac{e''}{k \Delta \theta / l}.$$

The ratio  $e''/\Delta \theta$  is also referred to as the *heat transfer coefficient*,  $h$ , and the Nusselt number is then written as

$$\Pi_{\text{nu}} = \frac{h l}{k}.$$

It is important to note that thermal and mass transfer coefficients,  $h$  and  $k_m$ , are *not* material properties. They do depend on the system geometry and flow conditions and can be calculated only after solving the specific transport problem. Therefore, they are derived quantities, on par with the Nusselt and Sherwood numbers. The calculation or experimentation required to obtain these is identical to that for the Nusselt and Sherwood numbers. Therefore, in this course, we shall work in terms of the Nusselt and Sherwood numbers alone and will avoid the confusion generated by introducing the thermal and mass transfer coefficients. In case a the thermal and mass transfer coefficients are necessary, they can be calculated from the Nusselt and Sherwood numbers from their definitions.

The length and velocity in dimensionless numbers for commonly encountered configurations are defined as follows.

- (1) For the flow past suspended particles, the velocity  $u$  is the difference between the particle velocity and the free-stream fluid velocity and the length is usually the particle diameter  $d$  (for spherical particles) or characteristic dimension.
- (2) For the flow past a flat plate, the length is the total length of the plate, while the velocity is the constant free-stream velocity far from the plate. The average fluxes are defined per unit surface area of the plate.

- (3) For the flow in tubes and channels, the length is the tube diameter or channel width, while the velocity is the average flow velocity through the tube or channel. The average fluxes are defined per unit surface area of the tube or channel.

### 3.2. Correlations.

## 4. ENERGY TRANSPORT

People goes to high place, water flows to low place

— JUNPING SHI, Partial Differential Equations and Mathematical Biology

All streams flow to the sea because it is lower than they are. Humility gives it its power.

— LAO TZU, Tao Te Ching

The flame that burns twice as bright burns half as long.

— LAO TZU, Tao Te Ching

Be careful with notation:

*Caution.* We use the prime notation (Lagrange's notation for derivatives) to express time rate changes; *e.g.*, when expressing a body internal energy time rate change:  $i'$ , or, equivalently,  $i' = \partial_t i$ . Note that  $\dim i' = E/T$ .

Under the same dimensional basis, we also use the prime notation to express energy flows; *e.g.*, when expressing thermal flow, *aka* thermal power,  $e'$ ; since  $\dim e' = E/T$ . The same applies for other flows, like work change rate, *aka* mechanical power,  $w'$ .

On the other hand, however, in order to preserve undecorated variables and similarly looking equations, we use an analogous notation for fluxes: the double prime notation; *e.g.*, when expressing thermal energy flux:  $e''$ . Note that now  $\dim e'' = E/L^2T$ , which is *not* the second derivative of thermal energy with respect to time; *i.e.*,  $e'' \neq \ddot{e} = d_t d_t e$ .

Therefore, in the case of any doubt, use the physicist's best allies: mathematical interpretation, physical reasoning and dimensional analysis.

### 4.1. Relation of thermal energy transfer and thermodynamics.

4.1.1. *Theory.* Consider a body of mass  $m$  and volume  $v$  being heated by an inflow of *thermal energy*, *thermal flow* or *thermal power*,  $e'$ . Due to heating, the body expands and performs *work* onto the surroundings at a rate  $w'$ . While both processes take place, on the other hand, the body *internal energy*  $i$  changes, or accumulates, at a rate  $i'$  given by the *energy conservation principle*:

$$i' = e' - w',$$

where the IUPAC sign convention for thermodynamics was used to find the signs for the different terms.

The body internal energy is related to the body *thermodynamic temperature*  $\theta$  via the phenomenological expression

$$i = cm\theta,$$

where  $c$  is a property of the body material called *specific heat capacity*<sup>2</sup>, or the capacity that a body has to store or release thermal energy,  $\dim c = E/M\Theta$ , and  $\theta$  is the body thermodynamic temperature.

If  $p dv$  is the only work that occurs, then,

$$e' = pv' + i'.$$

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<sup>2</sup> This property should really be called *specific energy capacity*, for “heat” is no more than energy in transit!

This last equation has two well-known special cases: when the body is allowed to expand freely, *constant pressure process*, and when expansion is constrained, *constant volume process*:

$$e' = \begin{cases} mc_v\theta', & \text{for constant volume processes; i.e., } dv = 0, \\ mc_p\theta', & \text{for constant pressure processes; i.e., } dp = 0, \end{cases}$$

where  $c_v$  is the *specific heat capacity at constant volume* and  $c_p$  the *specific heat capacity at constant pressure*.

When the body is made of an incompressible substance, then, for any pressure variation,  $dv = 0$  and thus the two specific capacities are equal:

$$c_v = c_p = c.$$

This approximation works well for solids and liquids. With this estimate, the energy conservation equation becomes

$$e' = i' = mc\theta'.$$

The work now is to solve the last equation to predict  $e$ . Finding the solution, however, is not possible at this stage, for  $i$  is not known *a priori*, so some principles must be added to complete the problem formulation. These principles are called *transport laws* or *constitutive equations* and are *not* a part of thermostatics. They include Fourier's law of thermal conduction, Newton's law of cooling and Stephan-Boltzmann's law of thermal radiation. Moreover, constitutive equations express physical quantities, in this case the internal energy  $i$  and thermal energy  $e$ , in terms of *state variables*, in this case temperature  $\theta$ .

4.1.2. *Technical notes.* Some technical notes on energy transfer theory.

*Technical note.* The mathematical treatment of physical phenomena of systems composed of many particles depends on the size of the system; i.e., on the number of particles composing it. To better describe such a dependence, we rely on the concepts of microscopic and macroscopic systems. Microscopic systems can be mathematically treated by statistical mechanics, while macroscopic systems by energy transfer theory.

Consider a system to be composed of  $n$  particles. A system is called *macroscopic* if

$$\frac{1}{\sqrt{n}} \ll 1,$$

which means that statistical arguments can be applied to reasonable accuracy. For instance, if we wish to keep the statistical error below one percent then a macroscopic system would have to contain more than about ten thousand particles. Any system containing less than this number of particles would be regarded as *microscopic*, and, hence, statistical arguments could not be applied to such a system without unacceptable error. Statistical quantum mechanics is required to analyze such systems.

Thermal energy transfer is based on the macroscopic description of physical phenomena; it is thus an approximation to the microscopic description of phenomena ultimately given by statistical quantum mechanics. However, thermal energy transfer can be approximated by classical statistical mechanics. This approximation is valid when the number of particles in the system.

*Technical note.* Thermal flow is also called *thermal energy transfer rate*.

*Technical note.* IUPAC sign convention: All net energy transfers *to* the system are positive. All net transfers *from* the system are negative. A useful mnemonic is the wording '+accumulation = +inflow - outflow + release - storage'.

*Note.* Statistical mechanics provides a microscopic explanation of *temperature*, based on macroscopic systems' being composed of many particles, such as molecules and ions of various species, the particles of a species being all alike. It explains macroscopic phenomena in terms of the mechanics of the molecules and ions, and statistical assessments of their joint adventures. In the statistical thermodynamic approach, by the *equipartition theorem* each classical degree of freedom that the particle has will have an average energy of  $k_b\theta/2$ , where  $k_b$  is Boltzmann's constant. The *translational motion* of the particle has three degrees of freedom, one in every direction of space, so that, except at very low temperatures where quantum effects predominate, the average translational energy of a particle in an system with temperature  $\theta$  will be  $3k_b\theta/2$ .

On the molecular level, temperature is the result of the motion of the particles that constitute the material. Moving particles carry kinetic energy. Temperature increases as this motion and the

kinetic energy increase. The motion may be the translational motion of particles or the energy of the particle due to molecular vibration or the excitation of an electron energy level.

In other words, since every degree of freedom that a particle has carries energy  $e$  that equals  $k_b\theta/2$  and since  $k_b$  is a *universal constant*, then energy is proportional to temperature:  $e \propto \theta$ . Therefore, one is entitled to think on temperature as energy, energy in “disguise”.

*Dim. Analysis.* When analyzing thermal energy transfer, the most suitable *dimensional system* is the  $ELT\Theta$  system – a *dimensionally independent system*. Within this framework, the dimensions of energy transfer, *aka* heat, of work and of internal energy are  $\dim e = \dim w = \dim i = E$  and of energy flow, *aka* thermal power or thermal flow, of work rate, *aka* mechanical power, and of internal energy change rate, *aka* accumulation, are  $\dim e' = \dim w' = \dim i' = E/T$ .

*Technical note.* In giving the dimensions of the specific heat capacity  $c$  as  $E/M\Theta$ , we are abusing of the  $ELT\Theta$  system by adding mass,  $M$ , to it. This addition extends the dimensionally *independent*  $ELT\Theta$  system to the dimensionally *dependent*, redundant,  $EMLT\Theta$  system. We do so consciously, so to stress physics instead of mathematical purity; for, in the “pure”  $ELT\Theta$  system, the dimensions of mass are  $ET^2/L^2$  and then the dimensions of the  $c$  are  $L^2/T^2\Theta$ ; disguising therefore its physical meaning. In other words, we prefer to interpret specific heat capacity as the capacity that a body has to store energy at a given temperature per unit mass or  $\dim c = E/M\Theta$ , rather than the less informative  $L^2/T^2\Theta$ .

**4.2. Modes of energy transfer.** Thermal energy is transferred inside a body or among bodies by three means:

- (1) thermal (heat) conduction;
- (2) thermal (heat) convection and
- (3) thermal radiation.

**4.2.1. Thermal conduction.** Consider a body, say a rod, being heated up to temperature  $\theta_1$  at one end while simultaneously being cooled down to  $\theta_2$  at the other end. Consider also the body to be thermally isolated everywhere but not at the ends. Then, it can be observed that, driven by the temperature difference,  $\Delta\theta = \theta_1 - \theta_2$ , the thermal flow happens from the hot end to the cold one. Since such a flow happens through the body surface, it is useful to define physical quantity, *thermal flux*, to better express the energy flow and surface relation.

*Thermal flux*,  $e''$ , is thus defined as thermal flow per unit area,  $\dim e'' = E/L^2T$ . Then, *thermal conduction*, often called heat conduction, through a body is based on experimental observation: *Fourier’s law*.

Fourier’s law states that

the local thermal flux resulting from thermal conduction is proportional to the magnitude of the temperature gradient and opposite to it in sign. Mathematically,

$$e'' = -k \text{ grad } \theta.$$

The minus sign accounts for the second law of thermostatics: thermal flow happens in the direction of *falling* temperature.

The proportionality “constant” in Fourier’s law,  $k$ , is a definite positive number describing a substance thermal property, *thermal conductivity*,  $\dim k = E/TL\Theta$ . Thermal conductivity, rather than a constant, is a coefficient, because its value depends on temperature, pressure and, in mixtures, on the composition. It is a scalar as long as the material is *isotropic*, which means that the ability of the material to conduct thermal energy depends on position within the material, but for a given position not on the direction.

Thermal conductivity values: Because of how molecules are arranged, solids will have generally higher thermal conductivity values than gases. Thus, the process of thermal energy transfer is more efficient in solids than in gases.

In a gas,  $k$  is proportional to the molecular speed and molar specific heat and inversely proportional to the cross-sectional area of molecules.

The values for  $k$  are experimentally found and presented in references as tables or figures.

*Example.* The front of a slab of lead ( $k = 35 \text{ W/m K}$ ) is kept at  $110^\circ\text{C}$  and the back is kept at  $50^\circ\text{C}$ . If the area of the slab is  $0.4 \text{ m}^2$  and it is  $0.03 \text{ m}$  thick, then compute the thermal energy flux and the thermal energy transfer rate.

*Solution.* Use Fourier's law to find the energy flux:

$$e'' = -k \text{ grad } \theta \sim -k \Delta\theta / \Delta x = -(35)((110 - 50) + 273.15)/(0.03) = 70 \text{ kW/m}^2.$$

The thermal energy transfer rate is thus

$$e' = e''s = (70)(0.4) = 28 \text{ kW}.$$

□

**4.2.2. Thermal convection.** Consider a typical convective cooling situation: cool gas flows past a warm body. The fluid immediately adjacent to the body forms a thin slowed-down region called *boundary layer*. Thermal energy is conducted into this layer, which sweeps it away and, farther downstream, mixes it into the stream. We call such a process of carrying thermal energy away from a body surface by a moving fluid *convection*. Isaac Newton considered the convective process and suggested that the cooling would be such that

$$\dot{\theta}_{\text{body}} \propto \theta_{\text{body}} - \theta_{\text{fluid}},$$

wherein  $\theta_{\text{fluid}}$  is the temperature of the incoming fluid. This statement suggests that energy is flowing from the body. But if energy is constantly replenished, then the body temperature need not change. Therefore, with  $e' = mc\dot{\theta}$ , we get

$$e' \propto \theta_{\text{body}} - \theta_{\text{fluid}} \implies e'' = \bar{f}(\theta_{\text{body}} - \theta_{\text{fluid}}),$$

where  $e'' = e'/s$ ,  $s$  is the surface area of the body and  $\bar{f}$  is the *film coefficient* or *heat transfer coefficient*. The bar over  $\bar{f}$  indicates that's an *average* over the surface of the body. Without the bar,  $f$  denotes the *local* value of the film coefficient at a point on the surface. The dimensions of both coefficients are  $\dim f = \dim \bar{f} = E/TL^2\Theta$ .

It turns out that Newton oversimplified the process description, when he made his conjecture. Thermal convection is complicated and  $\bar{f}$  can depend on the temperature difference  $\theta_{\text{body}} - \theta_{\text{fluid}} = \Delta\theta$ :

- $f$  is really independent of  $\Delta\theta$  when the fluid is forced past a body and  $\Delta\theta$  is not too large. This is called *forced convection*.
- when fluid buoys up from a hot body or down from a cold one,  $f$  varies as some weak power of  $\Delta\theta$  – typically as  $\Delta\theta^{1/4}$  or  $\Delta\theta^{1/3}$ . This is called *free* or *natural convection*. If the body is hot enough to boil a liquid surrounding it, then  $\bar{f}$  will typically vary as  $\Delta\theta^2$ .

Typical values of the film coefficient are presented in equations, tables or figures. However, they should be judiciously applied in actual designs.

**Lumped-capacity solution – heat equation.** The problem now is to predict the transient cooling of a convectively cooled object. Apply the familiar first law statement to have

$$e' = \dot{i}' \implies -\bar{f}s(\theta - \theta_{\text{fluid}}) = \text{d}_t(\rho cv(\theta - \theta_{\text{ref}})),$$

where  $s$  and  $v$  are the surface area and volume of the body,  $\theta$  the temperature of the body,  $\theta = \theta[t]$ , and  $\theta_{\text{ref}}$  is an arbitrary temperature at which the internal energy  $i$  is defined to equal zero.

The last equation can be solved by separating the variables  $\theta$  and  $t$ . After solving the equation, after applying the initial condition  $\theta[t = 0] = \theta_i$ , wherein  $\theta_i$  the body initial temperature, and after rearranging terms, one has

$$\frac{\theta - \theta_{\text{fluid}}}{\theta_i - \theta_{\text{fluid}}} = \exp[-t/\tau].$$

Note that all the physical parameters in the problem have now been “lumped” into the *time constant*  $\tau$ . This time constant represents the time required for a body to cool to  $1/e$  or 35% of its initial temperature difference above (or below)  $\theta_{\text{fluid}}$ . The ratio  $t/\tau$  can also be interpreted as

$$\frac{t}{\tau} = \frac{\bar{f}st}{\rho cv} = \frac{\text{capacity for convection from surface}}{\text{thermal capacity of the body}}.$$

Note that the thermal conductivity of the body is missing from the last equations. The reason is that we have assumed that the body temperature is nearly uniform and thus means that internal conduction is unimportant. If  $L/k\bar{f} \ll 1$ , then the body temperature  $\theta$  is almost constant within the body at any time. Therefore,

$$\frac{\bar{f}L}{k} \ll 1 \implies \theta[\xi, t] \sim \theta[t] \sim \theta_{\text{surface}}$$

and the thermal conductivity  $k$  becomes irrelevant to the cooling process. This condition must be satisfied if the lumped solution is to be accurate.

We call the group  $\bar{f}L/k = \Pi_{\text{bi}}$  *Biot number*. If  $\Pi_{\text{bi}}$  were large, then the situation would be reversed in this case,  $\Pi_{\text{bi}} \ll 1$ , and then the convection process offers little resistance to the thermal transfer (conduction). We could solve the *thermal diffusion equation*, aka heat diffusion equation:

$$\alpha \partial_{xx} \theta = \partial_t \theta,$$

object to the simple boundary condition  $\theta[\xi, t] = \theta_{\text{fluid}}$ , when  $x = L$  to determine the temperature in the body and its rate of cooling, in this case.

Biot number will be therefore the basis for determining what sort of problem we have to solve.

**4.2.3. Thermal radiation.** When thermal energy is applied to a body, it generates motion of the charged particles in the body matter. Then, the body radiates electromagnetic energy – *thermal radiation*. Equivalently, this means that all matter with temperature greater than the absolute zero emits thermal radiation, or, in other words, thermal radiation can be seen as the conversion of thermal energy into electromagnetic energy. Examples of thermal radiation are the visible light and infrared light emitted by an incandescent light bulb, the infrared radiation emitted by animals and detectable with an infrared camera.

The thermal radiation of real bodies is modeled after a hypothetical radiative body called a *black-body*. If a radiation-emitting object meets the physical characteristics of a black body in thermodynamic equilibrium, then the radiation is called *black-body radiation*. There are three laws that describe the physical properties of black-bodies: Planck’s law describes the *spectrum* of black-body radiation, which depends only on the object’s temperature; Wien’s displacement law determines the most likely *frequency of the emitted radiation* and, finally, Stefan-Boltzmann law gives the black-body *radiant emissivity*.

Thermal transfer by thermal radiation: All bodies constantly emit energy by a process of electromagnetic radiation. The intensity of such energy flux depends upon the body temperature. Most of the thermal energy that reaches you when you sit in front of a fire is radiant energy. Radiant energy warms you when you walk under the sun.

Objects cooler than the fire or the sun emit much less energy, because the energy emission varies as the fourth power of absolute temperature. Very often, the emission of energy, or radiant energy transfer, from cooler bodies can be neglected in comparison with convection and conduction. (Approximate solutions and order of magnitude physics can be helpful here!) But energy transfer processes that occur at high temperatures, or with conduction or convection suppressed by evacuated insulators, usually involve a significant fraction of radiation.

The electromagnetic spectrum: Thermal radiation occurs in a range of the electromagnetic spectrum of energy emission. Accordingly, it inhabits the same wavelike properties as light or radio waves. Each quantum of radiant energy has a wavelength  $\lambda$  and a frequency  $\mu$  associated with it.

The full electromagnetic spectrum includes an enormous range of energy-bearing waves, of which thermal energy is only a small part.

Tables show the various forms over a range of wavelengths that spans 17 orders of magnitude. Thermal radiation, whose main component is usually the spectrum of infrared radiation, passes through a three-order-of-magnitude window in  $\lambda$  or  $\mu$ . This window ranges 0.1  $\mu\text{m}$  to 1000  $\mu\text{m}$ , with a geometric mean of 10  $\mu\text{m}$ .

Black-bodies: The model for the perfect thermal radiator is the so-called *black-body*. This is a body that absorbs all energy that reaches it and reflects nothing. The term is a bit confusing, since they *emit* energy. Thus, under infrared vision, a black-body would glow



with “color” appropriate to its temperature. Perfect radiators are “black” in the sense that they absorb all visible light (and all other radiation) that reaches them.

To model a black-body, a *Hohlraum* is used. What are the important features of a thermally black-body? First consider a distinction between thermal (heat) radiation and infrared radiation. *Infrared radiation* refers to a particular range of wavelengths, while thermal radiation refers to the whole range of radiant energy flowing from one body to another. Suppose that a radiant thermal flux  $e''$  falls upon a translucent plate that’s not black. A fraction  $\alpha$  of the total incident energy, called the *absorptance*, is absorbed by the body; a fraction  $\rho$ , called the *reflectance*, is reflected by the body and a fraction  $\tau$ , called the *transmittance*, passes through. Thus,

$$1 = \alpha + \rho + \tau.$$

This relation can also be written for the energy carried by each wavelength in the distribution of wavelengths that makes up thermal radiant energy from a source at any temperature.

$$1 = \alpha_\lambda + \rho_\lambda + \tau_\lambda.$$

All radiant energy incident on a black-body is absorbed, so that  $\alpha_b = \alpha_{\lambda_b} = 1$  and  $\rho_b = \tau_b = 0$ . Furthermore, the energy emitted by a black-body reaches a theoretical maximum given by Stefan-Boltzmann law.

Stefan-Boltzmann law: The energy flux radiating from a body is designated by  $e'' [t]$ ,  $\dim e'' = E/L^2T$ . The symbol  $\check{e}_{\lambda_{\text{body}}} [\lambda, \theta]$  designates the distribution function of radiative flux in  $\lambda$ , or the *monochromatic emission power*:

$$\check{e}_{\lambda_{\text{body}}} [\lambda, \theta] = d_t e'' [\lambda, \theta] \quad \text{or} \quad e'' [\lambda, \theta] = \int_0^\lambda \check{e}_{\lambda_{\text{body}}} [\lambda, \theta] d\lambda.$$

Thus,

$$e'' [\theta] = e'' [\infty, \theta] = \int_0^\infty \check{e}_{\lambda_{\text{body}}} [\lambda, \theta] d\lambda.$$

The dependence of  $e'' [\theta]$  on temperature  $\theta$  for a black-body,  $e''_{bb}$ , was found experimentally by Stefan and proved theoretically by Boltzmann. Stefan-Boltzmann law states that

$$e''_{bb} [\theta] = \sigma_{sb} \theta^4,$$

where Stefan-Boltzmann constant  $\sigma_{sb} = 5.670373(21) \times 10^{-8} \text{ W/m}^2 \text{ K}^4$ . In terms of other fundamental constants:

$$\sigma_{sb} = \frac{2\pi^5}{15} \frac{k_b^4}{h_p^3 c_0^2} = \frac{2\pi^5}{15} \frac{r_g^4}{h_p^3 c_0^2 n_a^2},$$

where  $k_b$  is Boltzmann constant,  $h_p$  Planck constant,  $c_0$  speed of light in vacuum,  $r_g$  ideal gas constant and  $n_a$  Avogadro’s number.

[a lot missing!]

**4.3. A look ahead.** To solve actual problems, three tasks must be completed:

- (1) thermal energy (heat) diffusion equation must be solved object to appropriate boundary and initial conditions;
- (2) the film (convective thermal transfer) coefficient must be determined if convection is relevant and
- (3) the factor  $F_{1-2}$  must be determined to calculate radiative thermal energy transfer.

## APPENDIX A. ENERGY CONTINUITY EQUATION

**A.1. Derivation.** Consider a body being heated from one side while being cooled from the other, opposite, side. Consider also that no work is performed. Experience shows that the body internal energy varies with time  $t$  and position  $\xi$  due to the external energy difference; *i.e.*, external energy flowing through the body external surface gets temporally and spatially distributed within the body. To model such a distribution, we will make use of the energy conservation principle.

Let  $i = i[t, \xi]$  be the internal energy density field of a non-moving control volume  $dv$  inside the body of volume  $v$ . Then, the internal energy in the whole body is  $\int_v i dv$ . Therefore, the body internal energy changes, accumulates, at a rate

$$d_t \int_v i dv = \int_v \partial_t i dv = \int_v i' dv.$$

On the other hand, let  $\partial v$  be the body outer surface, boundary, and, accordingly, let  $n ds$  be the directed control surface. Then, the thermal energy flowing *out* of the control surface is  $-e'' \cdot n ds$ . And, thus, the total thermal energy flowing out of the body through  $\partial v$  equals

$$-\int_{\partial v} e'' \cdot n ds = -\int_v \nabla \cdot e'' dv = -\int_v \text{div } e'' dv.$$

By the energy conservation principle, the internal energy change rate and the thermal flow must balance one another:

$$\int_v i' dv = -\int_v \text{div } e'' dv.$$

The last equation must be equal regardless of any control volume choice:

$$i' + \text{div } e'' = 0.$$

The next step is to relate the internal energy density with the thermal flux. This relation comes from two phenomenological laws, *aka constitutive equations*:

- (1) As mentioned in the above sections, a body internal energy is related to the body temperature  $\theta$  by

$$i = \rho c \theta,$$

where  $\rho$  and  $c$  are two body (material) properties, *mass density*, mass per unit volume, and *specific heat capacity*, the capacity that the body material has to store energy per unit mass and per unit temperature. Thus,

$$i' = (\rho c \theta)' = \partial_t (\rho c \theta) = \partial_t \rho c \theta.$$

- (2) Fourier's law of thermal energy conduction states that the thermal energy flux is proportional to the temperature gradient:

$$e'' = -k \text{ grad } \theta.$$

The minus sign in this equation accounts for the second law of thermodynamics: thermal energy flows in the direction of falling temperature. The constant of proportionality  $k$  is a body (material) property, *thermal conductivity*,  $\dim k = E/LT\Theta$ . It is dependent on both the temperature and pressure – in mixtures also on the composition.

Using the empirical laws, find that

$$\partial_t \rho c \theta = \text{div } k \text{ grad } \theta.$$

Consider, finally, the body to be composed of an homogeneous, isotropic material. Then, the mass density, the specific heat capacity and the thermal conductivity are constant. Therefore, write the last equation as

$$\partial_t \theta = \alpha \text{ lap } \theta \quad \text{or as} \quad \theta' = \alpha \text{ lap } \theta,$$

where  $\alpha$  is the *thermal diffusivity*,  $\dim \alpha = L^2/T$ , and  $\text{lap}$  Laplace operator. Refer to the last equation as the *thermal transfer equation*, the *thermal diffusion equation*, or, more commonly, as *heat equation*.

Note the definition of thermal diffusivity:  $\alpha = k/\rho c$ ; *i.e.*, thermal diffusivity is the ratio of thermal energy conduction,  $\dim k = E/LT\Theta$ , to the volumetric thermal capacity,  $\dim \rho c = E/L^3\Theta$ . Thus, in a sense, thermal diffusivity is the measure of thermal inertia. In a substance with high thermal diffusivity, thermal energy moves rapidly through it because the substance conducts energy quickly relative to its volumetric thermal capacity or “thermal bulk”.

**A.2. Technical notes.** Some explanations on the maths involved during the derivation.

*Technical note.* It is assumed that, during the thermal energy transfer, the body material is not affected by it; *i.e.*, the body material does not undergo thermal decomposition.

*Math note.* For modeling the phenomenon, energy density was assumed to be a smooth scalar field and the body to be bounded by a smooth outer surface.

*Notation.* The symbol  $d_t$  defined by  $d_t \doteq d/dt$  denotes the *ordinary* derivative with respect to time and  $\partial_t \doteq \partial/\partial t$  denotes the *partial* derivative with respect to time.

*Math note.* In going from the surface integral to the volume integral,

$$-\int_{\partial v} e'' \cdot n \, ds = -\int_v \nabla \cdot e'' \, dv = -\int_v \operatorname{div} e'' \, dv,$$

the divergence theorem was used.

*Dim. Analysis.* The accumulation in the body must balance energy outflow:

$$\int_v i' \, dv = \int_v \partial_t i \, dv = -\int_v \operatorname{div} e'' \, dv.$$

This equation satisfies a fundamental physics law: the energy conservation principle. It also satisfies another fundamental physics principle: dimensional homogeneity principle for physics law.

The dimensions of the terms in the left-hand-side, LHS, of the last equation are  $\dim \partial_t = 1/T$ ,  $\dim i = E/L^3$ , *i.e.*, internal energy *density*,  $\dim dv = L^3$ . Then, the whole LHS integral has dimensions of energy change rate, or energy flow,  $E/T$ .

The dimensions of the terms in the right-hand-side, RHS, are  $\dim \operatorname{div} = \dim \nabla \cdot = 1/L$ ,  $\dim e'' = E/L^2 T$ ,  $\dim dv = L^3$ . Then, the whole RHS integral has dimensions of energy flow,  $E/T$ .

Since the LHS and the RHS of the equation have the same dimensions, thus, the principle of dimensional homogeneity is satisfied.

*Math note.* During the derivation, we went from

$$\int_v (i' + \operatorname{div} e'') \, dv = 0 \quad \text{to} \quad i' + \operatorname{div} e'' = 0;$$

or, in other words, we made the integrand to vanish. To explain this “math move”, making the integrand equal to zero, we need to analyze how the derivation was done, mathematically – the math framework behind the deduction.

To find the energy distribution inside our given body, we have followed Riemann’s ideas on integration. He would have said:

To find the energy distribution within the body, follow the process:

- first, divide the body volume  $v$  into  $n$  smaller control volumes  $dv_i$ , where  $i$  runs from 1 to  $n$ . Note that the number and sizes of the control volumes are up to you. There is neither a fixed number nor a fixed size. In fact, they not even need be all of the same size! Nevertheless, do make sure that  $n$  is large enough to cover the whole body volume.
- Then, find the energy distribution in each control volume and
- finally, find the total energy distribution inside of the whole of the body by adding the energy distribution of the  $n$  control volumes together by means of integration.

Note that the result has to be *independent* on the number of control volumes and on their sizes.

To explain this better. Say, for instance, that you take  $n$  control volumes of equal size  $dv_1$  and, say, I take  $m$  smaller control volumes of size  $dv_2$ ; or,  $n < m$  since  $dv_1 > dv_2$ . Say both choices cover the whole body. Then, you calculate the energy distribution of your control volumes and so do I. To find the total energy distribution, you next add the energy distribution of every of your control volumes and so do I. Finally, we compare results. Good maths requires both results, your total energy distribution and mine, be the same!

This explanation implies, mathematically, the vanishing integrand.

*Notation.* Another common form of writing the heat equation is by using the geometric derivative:  $\partial_t \theta = \alpha \nabla^2 \theta$ .

*Technical note.* As it stands, the heat equation,  $\theta' = \alpha \operatorname{lap} \theta$ , is written in vector notation; thus, it is valid in *any* coordinate system. However, once a particular coordinate system is selected, then,

the appropriate form of Laplace operator must be found. For instance, in a Cartesian coordinate system,  $[x, y, z]$ , the heat equation becomes

$$\theta' = \partial_t \theta = \alpha \partial_k \partial_l g^{kl} \theta \quad \text{or} \quad \theta_{,t} = \alpha \theta_{,\xi\xi} = \alpha (\theta_{,xx} + \theta_{,yy} + \theta_{,zz}) ,$$

The second equation follows from two facts of Cartesian coordinate systems: the metric  $g$  does not depend on position, thus  $\partial_k \partial_l g^{kl} \theta = g^{kl} \partial_k \partial_l \theta$  and  $g = \text{diag}[1, 1, 1]$ .

For non-Cartesian coordinate systems, however,  $g$  does depend on position, so  $\partial_k \partial_l g^{kl} \theta \neq g^{kl} \partial_k \partial_l \theta$  and therefore the derivatives of the metric with respect to the coordinates and the metric coefficients  $g^{kl}$  must be found.

*Notation.* Consider a smooth scalar field  $\phi = \phi[x, y, z]$ . Then, the comma derivative notation is defined as

$$\phi_{,x} = \frac{\partial \phi}{\partial x}, \quad \phi_{,y} = \frac{\partial \phi}{\partial y}, \quad \phi_{,z} = \frac{\partial \phi}{\partial z}, \quad \phi_{,xy} = \frac{\partial}{\partial x} \frac{\partial \phi}{\partial y} \quad \text{and so on.}$$

*Geometry.* Remember that, in vector calculus, divergence is an operator that measures the magnitude of a vector field's source or sink at a given point, in terms of a signed scalar. Or, more technically, the divergence represents the volume density of the outward flux of a vector field from an infinitesimal volume around a given point.

Then, recall the equation:

$$i' = -\text{div } e'' .$$

This equation models the phenomenon of a body being heated up from one side while being cooled down from another side or the phenomenon of a body releasing energy from its center while it cools down. Take the second phenomenon. The LHS of the model equation represents the rate at which a body internal energy changes with respect to time: the rate at which energy is released from the center to the outer portions of the body and finally to the environment surrounding the body.

The RHS, on the other hand, because of the divergence, represents how the central energy diffuses from the center throughout the body to the environment. It has a minus sign because energy is being dissipated instead of being accumulated.

The equality holds, physically, because energy is conserved: if it is being released and not accumulated within the body, energy has no other place to go but to its surrounding environment.

*Geometry.* Recall that Laplace operator  $\text{lap } f[\xi]$  of a function  $f$  at a point  $\xi$ , up to a constant depending on the dimension, is the rate at which the average value of  $f$ , over spheres centered at  $\xi$ , deviates from  $f[\xi]$  as the radius of the sphere grows; *i.e.*, Laplace operator of a function represents the difference between the value of the function at a point and the average of the values at surrounding points. Another way of looking at Laplace operator is by writing it in a Cartesian coordinate system  $[x, y, z]$ :

$$\text{lap} = \nabla^2 = \partial_{xx} + \partial_{yy} + \partial_{zz} .$$

See that, then, this operator finds the *change in the change* of the function (if you make a graph, the change in the slope) in all directions from the point of interest. That may not seem very interesting, until you consider that acceleration is the change in the change of position with time or that the maxima and minima of functions (peaks and valleys) are regions in which the slope changes significantly.

Now, recall the thermal diffusion equation:

$$\theta' = -\alpha \text{lap } \theta .$$

This equation models the phenomenon of a body being heated up from one side while being cooled down from another side or the phenomenon of a body releasing energy from its center while it cools down. Take the second phenomenon. The LHS of the model equation represents the rate at which a body temperature changes with respect to time: the rate at which temperature diffuses from the center to the outer portions of the body and finally to the environment surrounding the body. In an analogous way as internal energy in the  $i' = -\text{div } e''$  equation. Something unsurprising, since energy and temperature are related via the equipartition theorem.

The RHS, on the other hand, because of Laplace operator, represents how the central temperature diverges from the center to the surrounding points. It has a minus sign because temperature is being dissipated instead of being gathered. The coefficient  $\alpha$ , thermal diffusion, is a body material property that acts as both a dimensional conversion factor between temporal temperature changes and spatial temperature changes ( $\dim \theta' = \Theta/T$  and  $\dim \text{lap } \theta = \Theta/L^2$ ) or as representing how a material diffuses or infuses temperature (internal energy). Thermal conductors diffuse (infuse) temperature (internal energy) at a greater rate than thermal insulators.

**A.3. Another derivation.** [John H. Lienhard IV, John H. Lienhard V, a heat transfer book] In this reference, the energy continuity equation is called heat diffusion equation, *aka* heat conduction equation in other sources.

**A.3.1. Objective.** We must now develop some ideas that will be needed for the design of thermal (heat) exchangers. The most important of these is the notion of an overall *thermal energy transfer coefficient*, *aka* heat transfer coefficient. This is a measure of the general resistance of a thermal (heat) exchanger to the flow of energy (heat), and usually it must be built up from analyses of component resistances. Although we shall count radiation among these resistances, this overall energy transfer coefficient is most often dominated by *convection and conduction*.

We need to know values of the film coefficient  $\bar{f}$  to handle convection. Calculating  $\bar{f}$  becomes sufficiently complex that we defer it to later chapters. For the moment, we shall take the appropriate value of  $\bar{f}$  as known information and concentrate upon its use in the overall heat transfer coefficient.

The thermal (heat) conduction component also becomes more complex than the planar analyses we did in earlier chapters. But its calculation is within our present scope. Therefore we devote this section to deriving the full thermal conduction equation, *aka* heat conduction or heat diffusion equation, solving it in some fairly straightforward cases, and using our results in the overall coefficient. We undertake that task next.

Consider the general temperature distribution in a three-dimensional body as depicted in Fig. 2.1 (a body being heated by a candle). For some reason, say heating from one side, the temperature of the body varies with time and space. This field  $\theta = \theta[\xi, t] = \theta[x, y, z, t]$ , defines instantaneous *isothermal surfaces*,  $\theta_1$ ,  $\theta_2$  and so on.

We next consider a very important vector associated with the scalar,  $\theta$ . The vector that has both the magnitude and direction of the maximum increase of temperature at each point is called the *temperature gradient*,  $\text{grad } \theta$ :

$$\text{grad } \theta = \nabla \theta = \gamma^i \partial_i \theta = \hat{x} \partial_x \theta + \hat{y} \partial_y \theta + \hat{z} \partial_z \theta.$$

**A.3.2. Fourier's law.** "Experience" – that is, physical observation – suggests two things about the thermal flow that results from temperature nonuniformities in a body. These are:

- (1)  $e''$  and  $\text{grad } \theta$  are exactly opposite one another in direction <sup>3</sup>:

$$\frac{e''}{|e''|} \propto -\frac{\nabla \theta}{|\nabla \theta|}$$

and

- (2) the magnitude of the thermal flux is directly proportional to the temperature gradient:

$$|e''| \propto |\nabla \theta|.$$

Notice that the thermal flux is now written as a quantity that has a specified direction as well as a specified magnitude. Fourier's law summarizes this physical experience succinctly as

$$e'' = -k \nabla \theta = -k \text{grad } \theta.$$

The coefficient  $k$  – the thermal conductivity – also depends on position and temperature in the most general case:

$$k = k[\xi, \theta[\xi, t]].$$

Fortunately, most materials (though not all of them) are very nearly *homogeneous*. Thus we can usually write  $k = k[\theta]$ . The assumption that we really want to make is that  $k$  is constant. Whether or not that is legitimate must be determined in each case. As is apparent from Fig. 2.2 and Fig. 2.3,  $k$  almost always varies with temperature. It always rises with  $\theta$  in gases at low pressures, but it may rise or fall in metals or liquids. The problem is that of assessing whether or not  $k$  is approximately constant in the range of interest. We could safely take  $k$  to be a constant for iron between 0 °C to 40 °C (see Fig.

<sup>3</sup> This is a consequence of the second law of thermostatics: thermal energy flows in the direction of falling temperature.

2.2), but we would incur error between  $-100^\circ\text{C}$  to  $800^\circ\text{C}$ . Thus, if  $\Delta\theta$  is not large, one can still make a reasonably accurate approximation using a constant average value of  $k$ .

We must now write the thermal energy conduction equation in three dimensions. We begin with the energy conservation principle – thermal energy flow equals energy accumulation within the body:

$$e' = i'.$$

This time we apply the last equation to a three-dimensional control volume, as shown in Fig. 2.4.1. The control volume is a finite region of a conducting body, which we set aside for analysis. The surface is denoted as  $s$  and the volume and the region as  $v$ ; both are at rest. An element of the surface,  $ds$ , is identified and two vectors are shown on  $ds$ : one is the unit normal vector,  $\hat{n}$  (with  $|\hat{n}| = 1$ ), and the other is the thermal energy flux vector,  $e'' = -k \text{grad } \theta = -k \nabla \theta$ , at that point on the surface.

We also allow the possibility that a volumetric thermal energy release flow equal to  $r'$ ,  $\text{dim } r' = E/TL^3$ , is distributed through the region. This might be the result of chemical or nuclear reaction, of electrical resistance heating (Joule heating), of external radiation into the region or of still other causes.

With reference to Fig. 2.4, we can write the thermal energy flow conducted *out* of  $ds$ , in dimensions of  $E/T$ , as

$$(-k \nabla \theta) \cdot (\hat{n} ds).$$

The thermal energy released (or accumulated) within the region  $v$  must be added to the total energy flow into  $s$  to get the overall rate of thermal energy addition to  $v$ :

$$e' = - \int_s (-k \nabla \theta) \cdot (\hat{n} ds) + \int_v r' dv.$$

The rate of energy increase (accumulation) of the region  $v$  is

$$i' = \int_v (\partial_t \rho c \theta) dv,$$

where the derivative of  $\theta$  is in partial form because  $\theta$  is a function of both position,  $\xi$ , and time,  $t$ .

Finally, we combine  $e'$  and  $i'$  using the energy conservation principle. After rearranging the terms, we obtain

$$\int_s (-k \nabla \theta) \cdot (\hat{n} ds) = \int_v (\partial_t \rho c \theta + r') dv.$$

To get the left-hand side into a convenient form, we introduce Gauss's theorem, which converts a surface integral into a volume integral. This reduces the last equation into

$$\int_v (\nabla \cdot k \nabla \theta - \partial_t \rho c \theta + r') dv.$$

Next, since the region  $v$  is arbitrary, the integrand must vanish identically. We therefore get the *thermal energy diffusion equation* in three dimensions:

$$\nabla \cdot k \nabla \theta + r' = \partial_t \rho c \theta.$$

The limitations on this equation are:

- Incompressible medium. (This was implied when no expansion work term was included.)
- No convection. (The medium cannot undergo any relative motion. However, it can be a liquid or gas as long as it sits still.)

If the variation of  $k$  with  $\theta$  is small and if the medium is homogeneous, then  $k$  and  $\rho c$  can be factored out of the last equation to get:

$$\nabla^2 \theta + \frac{1}{k} r' = \frac{1}{\alpha} \partial_t \theta,$$

where  $\alpha = k/\rho c$  is the body thermal diffusivity. In a sense, thermal diffusivity is the measure of thermal inertia. In a substance with high thermal diffusivity, thermal energy moves rapidly through it because the substance conducts energy quickly relative to its volumetric thermal capacity or “thermal bulk”.

*Geometry.* As seen in the thermal energy diffusion equation, *aka* heat equation, when there are no volumetric thermal energy releases, *i.e.*,  $r' = 0$ , then we have

$$\theta_{,t} = \alpha \theta_{,\xi\xi}.$$

Here thermal diffusivity can be geometrically interpreted as the ratio of the time derivative of temperature to its *curvature*, quantifying thus the rate at which temperature concavity is “smoothed out”.

*Technical note.* Notice the reactive term  $r'/k$ . It has the dimensions of

$$\dim \frac{r'}{k} = \frac{E/TL^3}{E/TL\Theta} = \frac{\text{flow of chemical energy release}}{\text{thermal energy conduction}}.$$

Thus, if thermal conduction is high, then thermal energy coming from the reaction flows quickly through the body, being then released to the environment. Otherwise, then thermal energy coming from the reaction is stored within the body, this, in turns, enhances the reaction rate, since  $r = f[\theta]$ .

**A.4. Yet another derivation.** [Evans M. Harrell II and James V. Herod, Linear Methods of Applied Mathematics. <http://www.mathphysics.com/pde/HEderiv.html>]

Newton articulated some principles of thermal flow through solids, but it was Fourier who created the correct systematic theory. Inside a solid there is no convective transfer of thermal energy and little radiative transfer, so temperature changes only by conduction, as the energy we now recognize as molecular kinetic energy flows from hotter regions to cooler regions.

- (1) The first basic principle of thermal energy is that the thermal energy contained in a material (internal energy) is proportional to the temperature, the density of the material and a physical characteristic of the material called the *specific thermal capacity*. In mathematical terms,

$$i = \int_v \rho c \theta [t, \xi] \, dv.$$

- (2) For the other principles of thermal transfer, let us do some experiments with the following materials: a hot stove, some iron rods of different, relatively short lengths and various widths and various ceramic rods of different lengths and widths. Since these will be thought experiments only, it will be safe to use a finger as the probe. Putting your finger right on the stove will convince you that the energy transfer is proportional to the difference in temperature between your finger and the stove. Using, if necessary, a different, undamaged finger, you will also find that the rate of thermal transfer is inversely proportional to the length of an iron rod intervening between your finger to the stove (fixing the cross-sectional area). In other words, the rate of thermal flow from one region to another is proportional to the temperature gradient between the two regions. You will probably also agree that the rate of thermal flow will be proportional to the area of the contact; for example, a short pin with one end on a hot stove and the other touching your hand is preferable to putting the palm of your hand on a frying pan. Finally, a ceramic material on the stove being usually more pleasant to the touch than hot iron, we see that the rate of thermal transfer depends on the material, as measured with a physical constant known as the *thermal conductivity*. The second basic principle is thus that

the thermal transfer (thermal flow, thermal power) through the boundary of a region is proportional to the thermal conductivity, to the gradient of the temperature across the region and to the area of contact, so if the boundary of the region  $v$  is written as  $\partial v$ , with outward normal vector  $n$ , then

$$e' = \int_{\partial v} k n \cdot \text{grad } \theta [t, \xi] \, ds.$$

If we differentiate the internal energy equation with respect to time, applying the differentiation under the integral sign, and apply divergence theorem to the thermal transfer integral, then we find that

$$\int_v \partial_t \rho c \theta [t, \xi] \, dv = \int_v \operatorname{div} k \operatorname{grad} \theta [t, \xi] \, dv .$$

Since the region  $v$  can be an arbitrary piece of the material under study, the integrands must be equal at almost every point. If the material under study is made out of an homogeneous, isotropic substance and if temperature gradients are not so big, then  $\rho$ ,  $c$  and  $k$  are independent of the position  $\xi$ . Thus, we obtain the thermal diffusion equation

$$\partial_t \theta [t, \xi] = \alpha \operatorname{lap} \theta [t, \xi] ,$$

where  $\alpha = k/\rho c$  is called *thermal diffusivity*. Ordinary substances have values of  $\alpha$  ranging from about  $5 \text{ cm}^2/\text{g}$  to  $9000 \text{ cm}^2/\text{g}$ .

The one-dimensional thermal diffusion equation in Cartesian coordinates

$$\theta_{,t} = \alpha \theta_{,xx}$$

would apply, for instance, to the case of a long, thin metal rod wrapped with insulation, since the temperature of any cross-section will be constant, due to the rapid equilibration to be expected over short distances.

**A.5. Solutions to the thermal diffusion equation.** We are now in position to calculate the temperature distribution or thermal flux in bodies with the help of the heat diffusion equation. In every case, we first calculate  $\theta [\xi, t]$ . Then, if we want the thermal flux as well, we differentiate  $\theta$  to get  $e''$  from Fourier's law.

The thermal diffusion equation is a partial differential equation (p.d.e.) and the task of solving it may seem difficult, but we can actually do a lot with fairly elementary mathematical tools. For one thing, in one-dimensional steady-state situations the heat diffusion equation becomes an ordinary differential equation (o.d.e.); for another, the equation is linear and therefore not too formidable, in any case. Our procedure can be laid out, step by step:

- (1) Play with geometrical analysis – make sketches, pics and drawings, physical analysis, dimensional analysis and approximate methods. Guess the solution beforehand. Even if you are proven wrong by the formal analysis, guessimations enhance physical intuition!

*Note.* In the analysis of thermal transfer, the dimensionally independent system  $\{E, L, T, \Theta\}$  is generally the most adequate. However, the SI system, based on  $\{M, L, T, \Theta\}$ , should not be overlooked.

- (2) Pick the coordinate scheme (coordinate system) that best fits the problem and identify the independent variables that determine  $\theta$ .
- (3) Write the appropriate d.e., starting with one of the forms of the thermal diffusion equation.

*Note.* Non-dimensionalization of the d.e. prior to obtain its solution provides a deeper physical understanding of the phenomenon regardless if it results in an “easier” equation to solve. Use and interpret physically the resulting non-dim. equation as well as any characteristic physical quantities and dimensionless numbers.

*Remark.* If non-dimensionalization is considered, then do not forget to include all of the physical quantities: quantities that appear in the diffusion equation, in the initial conditions and in the boundary conditions.

- (4) Obtain the general solution of the d.e. (This is usually the easiest step.)
- (5) Write the “side conditions” on the d.e. – the initial and boundary conditions. This is the trickiest part and the one that most seriously tests our physical or “practical” understanding any heat conduction problem. Normally, we have to make two specifications of temperature on each position coordinate and one on the time coordinate to get rid of the constants of integration in the general solution.

*Warning. Very Important:* Never, never introduce inaccessible information in a boundary or initial condition. Always stop and ask yourself, “Would I have access to a numerical



value of the temperature (or other data) that I specify at a given position or time?" If the answer is no, then your result will be useless.

- (6) Substitute the general solution in the boundary and initial conditions and solve for the constants. This process gets very complicated in the transient and multidimensional cases. Numerical methods are often needed to solve the problem.
- (7) Put the calculated constants back in the general solution to get the particular solution to the problem.

*Note.* Non-dimensionalization of the solution can also be helpful at this stage. Not only, non-dim. reduces the number of physical quantities to analyze, so does become useful when plotting equations.

- (8) Play with the solution – look it over– see what it has to tell you. Make any checks you can think of to be sure it is correct. Again dimensional analysis is the first tool to apply! Approximate methods and the use of characteristic quantities are also valuable.
- (9) If the temperature field is now correctly established, we can, if we wish, calculate the thermal flux at any point in the body by substituting  $\theta [\xi, t]$  back into Fourier's law.

**A.6. Examples.** Some examples on using the proposed method for solving the thermal diffusion equation.

*Example.* A large, thin concrete slab of thickness  $l$  is “setting”. Setting is an exothermic process that releases  $r'$ ,  $\dim r' = E/TL^3$ , unit  $r' = \text{W/m}^3$ . The outside surfaces are kept at the ambient temperature, so  $\theta_w = \theta_\infty$ . What is the maximum internal temperature?

*Guess.* Thermal energy is being released from the slab center to its walls. If its assumed that the center temperature is greater than the wall (ambient) temperature, then temperature attains its maximum at the center and decreases to ambient temperature. Additionally, since the outer surfaces are kept at constant temperature, then the process is to be steady, but ranging spatially throughout the slab thickness. If one measures the spatially variation as  $x$ , then the slab temperature must satisfy  $\theta = \theta [x]$ .

Another important point is given by the symmetry of the problem. The center temperature is maximum at the center,  $l/2$ , and minimum at the walls,  $x = 0$  and  $x = l$ , with a smooth decay. This gives a room to think about the temperature distribution inside the slab as a parabola with its vertex at  $\theta_{\max}$  and with its directrix greater than the horizontal line formed by the wall temperatures,  $\theta_w$ , at  $x = 0$  and  $x = l$ .

*Dim. Analysis.* Place a Cartesian coordinate axis that runs from one wall to the other covering the slab thickness; let  $x$  measure distances within the thickness:  $0 \leq x \leq l$ . Since temperature distribution is independent on time (steady process), then  $\theta = \theta [x]$  and thus  $x$  is the independent quantity and  $\theta$  the dependent quantity. Finally, the slab geometry provides two parameters,  $x$  and  $l$ , and the slab material, concrete, provides the thermal property,  $k$ , thermal conductivity.

Choose the set  $\{E, L, T, \Theta\}$  as the dimensionally independent set of dimensions. Within this system, the quantities dimensions are:

$$\dim x = \dim l = L, \quad \dim \theta = \dim \theta_w = \Theta, \quad \dim r' = E/TL^3 \quad \text{and} \quad \dim k = E/LT\Theta.$$

According to Buckingham's theorem, the model can be described by  $6 - 4 = 2$  dimensionless quantities. The first dimensionless quantity,  $\Pi_1$ , must include, as an advice, the sought quantity,  $\theta$ . Form this group by <sup>4</sup>

$$\Pi_1 = \frac{k(\theta - \theta_w)}{r'l^2} = \frac{\text{conduction energy flow gradient}}{\text{released energy flow gradient}} = \frac{\text{conduction gradient}}{\text{“production” gradient}}.$$

The second dimensionless quantity,  $\Pi_2$ , can be formed by the geometrical parameters:

$$\Pi_2 = x/l.$$

Then, according to the dimensionally homogeneity principle for physics laws, the model can be written as

$$f[\Pi_1, \Pi_2] = 0 \implies \Pi_1 = f[\Pi_1, \Pi_2] \implies k(\theta - \theta_w)/r'l^2 = f[x/l].$$

The last equation is the final result of dimensional analysis. The actual form of the function  $f$  has to be determined by experiment or by analytic considerations.

<sup>4</sup> A dimensionless quantity that includes  $\theta$  is readily available:  $\theta/\theta_w$ . However, in thermal transfer, temperature differences are more important than temperatures alone, since differences are the driving force behind the transfer.

*Approx. Solution.* After dimensional analysis was carried away, we arrived to

$$k(\theta - \theta_w)/r'l^2 = f[x/l] .$$

When guessing the solution, on the other hand, we established that a parabola can express the temperature dependence on the thickness distance. Accordingly, the function  $f$  can be then hypothesize to satisfy

$$k(\theta - \theta_w)/r'l^2 = a(x/l)^2 + b(x/l) + c ,$$

where the coefficients  $\{a, b, c\}$  must be determined.

These coefficients can be calculated using the theorem that states that three points uniquely determine a parabola. These points are

$$\begin{cases} [x/l = 0, k(\theta - \theta_w)/r'l^2 = 0] , \\ [x/l = 1/2, k(\theta - \theta_w)/r'l^2 = \Pi] , \\ [x/l = 1, k(\theta - \theta_w)/r'l^2 = 0] , \end{cases}$$

where  $\Pi$  is an unknown dimensionless quantity that, geometrically, shows the parabola height, its distance from the horizontal line formed by the  $x$ -axis to the parabola vertex and, physically, the maximum value of temperature,  $\theta_{\max} = \theta[1/2]$ , attained at  $x/l = 1/2$ , or,

$$\Pi = k(\theta_{\max} - \theta_w)/r'l^2 .$$

Using the points in the hypothetical equation for  $f$ , one finds that

$$a = -4\Pi, \quad b = 4\Pi \quad \text{and} \quad c = 0 ,$$

and, thus, one arrives at

$$\frac{k(\theta - \theta_w)}{r'l^2} = 4\Pi \frac{x}{l} \left(1 - \left(\frac{x}{l}\right)\right) .$$

Doing honest physics (*i.e.*, solving the differential equation), one finds that  $4\Pi = 1/2$  or  $\Pi = 1/8$ , thus the model becomes

$$\frac{k(\theta - \theta_w)}{r'l^2} = \frac{1}{2} \frac{x}{l} \left(1 - \left(\frac{x}{l}\right)\right)$$

and, finally, the maximum temperature,  $\theta_{\max}$ , is attained at

$$\Pi = \frac{k(\theta_{\max} - \theta_w)}{r'l^2} = \frac{1}{8} . \quad \square$$

*Solution.* This solution is based in the general procedure to solve the thermal diffusion equation.

Choose a Cartesian coordinate system with  $\xi$  varying only in one-dimension, so that

$$0 \leq x \leq l \quad \text{and} \quad \theta = \theta[x] .$$

Write the model equation for a one-dimensional, steady state case:

$$\theta_{,xx} = -r'/k .$$

Obtain the general solution to the model equation by integration to have

$$\theta = -\frac{r'}{k}x^2 + c_1x + c_2 ,$$

where  $c_1$  and  $c_2$  are integration constants.

Apply, next, the boundary conditions

$$\theta[x=0] = \theta_w \quad \text{and} \quad \theta[x=l] = \theta_w .$$

Substitute the boundary conditions into the general solution to have

$$c_1 = \frac{r'l}{2k} \quad \text{and} \quad c_2 = \theta_w .$$

Replace the values of the constants into the general solution to find the particular solution

$$\theta = -\frac{1}{2} \frac{r'}{k}x^2 + \frac{1}{2} \frac{r'}{k}x + \theta_w ,$$

which can be written in the dimensionless form:

$$\frac{k(\theta - \theta_w)}{r'l^2} = \frac{1}{2} \frac{x}{l} \left(1 - \left(\frac{x}{l}\right)\right) .$$

Finally, as a verifying step, note that the resulting temperature distribution is parabolic and, as expected, symmetrical. It satisfies the boundary conditions at the wall and maximizes in the center. By nondimensionalizing the result, a simple curve can represent all situations. That is highly desirable when the calculations are not simple, as they are here. (Even here  $\theta$  actually depends on five different quantities and its solution is a single curve on a two-coordinate graph.) $\square$

## APPENDIX B. COORDINATE SYSTEMS AND INDEX NOTATION

**B.1. Cartesian coordinate system.** Consider a region  $\mathcal{V}$  to be a part of an  $n$  dimensional Euclidean space,  $\mathcal{E}^n$ . Consider, next, a Cartesian coordinate system; *i.e.*, a coordinate system equipped with a frame  $\{\gamma_k\}$  whose elements satisfy

$$\gamma_k \cdot \gamma_l = g_{kl} = [k = l]_{IV} .$$

If frame elements satisfy the last equation, then they are *orthogonal* to each other and *normal* (have unit length); thus, the frame  $\{\gamma_k\}$  is said to be *orthonormal*.

Express now the position of any point  $\xi$  in  $\mathcal{V}$  as an  $n$ -tuple

$$\xi = [\xi^1, \dots, \xi^n] ,$$

or as a linear combination of the frame elements

$$\xi = \xi^k \gamma_k ,$$

where the elements of  $\{\xi^k\}$  are called the *components of  $\xi$  onto the  $\{\gamma_k\}$  frame*. (Einstein summation convention in force!)

To find the components of  $\xi$  on  $\{\gamma_k\}$ , apply

$$\xi^k = \xi \cdot \gamma_k .$$

**B.1.1. Reciprocal Cartesian coordinate system.** Consider now a reciprocal Cartesian coordinate system  $\{\gamma^k\}$  whose elements are the inverse <sup>5</sup> of the  $\{\gamma_k\}$  elements:

$$\gamma^k = \gamma_k^{-1} = \gamma_k ,$$

since the frame elements are orthonormal; *viz.*,  $\gamma_k^{-1} = \gamma_k / \gamma_k^2$ , but  $\gamma_k^2 = 1$ .

**B.1.2. Geometric derivative, gradient, divergence, Laplacian.** Define the geometric derivative (operator)  $\nabla$  by its components as <sup>6</sup>

$$\nabla = \gamma^k \partial_k .$$

This means, treat the geometric derivative as another vector.

Consider a scalar field  $\phi = \phi[\xi]$ . Then, define the gradient of  $\phi$  by

$$\text{grad } \phi = \nabla \phi = \gamma^k \partial_k \phi .$$

Consider next a vector field  $\psi = \psi[\xi]$ . Then, define the divergence of  $\psi$  by

$$\text{div } \psi = \nabla \cdot \psi = \gamma^k \partial_k \cdot \gamma^l \psi_l = \partial_k g^{kl} \psi_l ,$$

where  $g^{kl} = \gamma^k \cdot \gamma^l$ .

Finally, define Laplace operator on a scalar field  $\phi$  by

$$\text{lap } \phi = \text{div grad } \phi = \nabla \cdot \nabla \phi = \gamma^k \partial_k \cdot \gamma^l \partial_l \phi = \partial_k \partial_l g^{kl} \phi .$$

**B.2. Alternative coordinate systems.** Consider next another, alternative, coordinate system  $\{\gamma_{k'}\}$ , related to the Cartesian coordinate by

$$\xi^k = f \left[ \xi^{k'} \right] .$$

It is possible now to express the Cartesian frame  $\{\gamma_k\}$  in the alternative coordinate system by using the *tangent vectors  $\{\gamma_{k'}\}$  defined by* <sup>7</sup>

$$\gamma_{k'} = \partial_{k'} \xi .$$

These tangent vectors need *not* be orthogonal nor normal.

<sup>5</sup> The square of a vector  $a$  is defined as  $a^2 = aa$ , which, by axiom,  $a^2 \in \mathcal{E}^1$ . The inverse of a nonzero vector  $a$  is then defined as  $a^{-1} = a/a^2$ .

<sup>6</sup> In traditional notation,

$$\nabla = \gamma^k \frac{\partial}{\partial \xi^k} = \hat{x} \frac{\partial}{\partial x} + \hat{y} \frac{\partial}{\partial y} + \hat{z} \frac{\partial}{\partial z} .$$

<sup>7</sup> In traditional notation:

$$\gamma_{k'} = \partial_{k'} \xi = \frac{\partial \xi}{\partial \xi^{k'}} .$$

Onto this alternative frame  $\{\gamma_{k'}\}$ , any point position  $\xi$  can be expressed as a linear combination of the alternative frame elements:

$$\xi = \xi^{k'} \gamma_{k'},$$

where  $\xi^{k'} = \xi \cdot \gamma_{k'}$ .

The metric coefficients for the alternative frame are found by

$$g_{k'l'} = \gamma_{k'} \cdot \gamma_{l'}.$$

## APPENDIX C. NOTATION

### C.1. Maths.

#### C.1.1. Sets.

- set: set A,  $\mathcal{A}$ .
- n-dim set: nset nA,  $\mathcal{A}^n$ .
- n-dim. Euclidean space: espace n,  $\mathcal{E}^n$ .
- region: region A,  $\mathcal{A}$ .
- elements of a set. elset(a,b,c),  $\{a, b, c\}$ .
- tulpe. tuple(a,b,c),  $[a, b, c]$ .

#### C.1.2. Functions.

- function value at: vat x,  $[x]$ .

#### C.1.3. Geometric objects.

- boundary: bound,  $\partial$ .
- area: area,  $a$ .
- surface: surf,  $s$ .
- volume: vol,  $v$ .
- diameter: diam,  $d$ .
- length: length,  $l$ .
- radius: radius,  $r$ .

#### C.1.4. Geometric algebra.

- magnitude: magn u,  $|u|$ .
- inner product: iprod,  $a \cdot b$ .
- outer product: oprod,  $a \wedge b$ .
- inverse: inv a,  $a^{-1}$ .
- unit vector: uvec a,  $\hat{a}$ .

#### C.1.5. Geometric calculus.

- geometric derivative: gder,  $\nabla$ .
- Laplace operator (derivative): lder,  $\nabla^2$ .
- divergence: div,  $\text{div}$ .
- gradient: grad,  $\text{grad}$ .
- Laplace operator: lap,  $\text{lap}$ .

#### C.1.6. Calculus.

- differential operator: dx,  $d$ .
- difference operator: Dx,  $\Delta$ .

#### C.1.7. Derivatives.

- dot derivative: dt a,  $\dot{a}$ .
- dot dot derivative: ddt a,  $\ddot{a}$ .
- expanded ordinary derivative: xod at,  $\frac{da}{dt}$ .
- expanded partial derivative: xpd at,  $\frac{\partial a}{\partial t}$ .
- indexed ordinary derivative: iod t,  $d_t$ .
- indexed partial derivative: ipd t,  $\partial_t$ .
- indexed geometric derivative: igder k,  $\partial_k$ .
- comma derivative: cder Tt,  $T_{,t}$ .

C.1.8. *Index notation.*

- basis vector: bvec,  $\gamma$ .
- frame (basis) element: fbvec 1,  $\gamma_1$ .
- reciprocal frame (basis) element: rbvec 1,  $\gamma^1$ .
- frame: frm k,  $\{\gamma_k\}$ .
- reciprocal frame: rfrm k,  $\{\gamma^k\}$ .
- metric: met,  $g$ .
- metric in frame: finet 12,  $g_{12}$ .
- metric in reciprocal frame: rmet 12,  $g^{12}$ .
- up indexed partial derivative: upipd 1,  $\partial^1$ .
- down indexed partial derivative: dnipd 1,  $\partial_1$ .
- frame (contravariant) components: fvec pos 1,  $\xi^1$ .
- reciprocal frame (covariant) components: rvec pos 1,  $\xi_1$ .

C.1.9. *Matrices.*

- diagonal: diag, diag.
- signature: sig, sig.

C.1.10. *Brackets.*

- Iverson brackets: iverson k,  $[k]_{\text{Iv}}$ .

C.2. **Physics.**C.2.1. *Mechanics.*

- position: pos,  $\xi$ .
- pressure: press,  $p$ .
- velocity: vel,  $u$ .
- acceleration due to gravity: grav,  $g$ .
- force: force,  $f$ .
- drag (force): drag,  $drag$ .
- buoyancy (force): buoy,  $f_b$ .
- shear stress: shear,  $\tau$ .
- surface tension: surftens,  $\gamma$ .
- frequency: freq,  $f$ .
- power: power,  $p$ .

C.2.2. *Energy transport.*

- time change rate: rate a,  $a'$ .
- flow: flow q,  $q'$ .
- flux: flux q,  $q''$ .
- thermal energy (heat): then,  $e$ .
- mechanical work: work,  $w$ .
- internal energy: ien,  $i$ .
- accumulation (*e.g.*, internal energy): accu ien,  $i'$ .
- thermodynamic temperature: temp,  $\theta$ .
- specific heat capacity: kshcap,  $c$ .
- thermal diffusivity: kthdiff,  $\alpha$ .
- thermal conductivity: kthcond,  $k$ .
- coefficient of thermal expansion: kthexp,  $\beta$ .
- local film (heat transfer) coefficient (thermal convection): kthconv,  $f$ .
- global (average) film coefficient: kavthconv,  $\bar{f}$ .
- time constant (conduction-convection lumped solution): ktime,  $\tau$ .
- thermal radiation absorbance: absorb,  $\alpha$ .
- thermal radiation reflectance: reflect,  $\rho$ .
- thermal radiation transmittance: transm,  $\tau$ .
- body energy flux distribution function: dbflux,  $\tilde{e}_{\lambda_{\text{body}}}$ .
- black-body energy flux: bbflux,  $e''_{\text{bb}}$ .
- black-body energy flux distribution function: dbbflux,  $\tilde{e}_{\lambda_{\text{bb}}}$ .

C.2.3. *Mass transport.*

- n (number of) particles: npart,  $n$ .
- mass: mass,  $m$ .
- mass density: dens,  $\rho$ .
- chemical reaction thermal energy: chthen,  $r$ .
- mass concentration: conc,  $c$ .

C.2.4. *Momentum transport.*

- dynamic viscosity: dynvis,  $\mu$ .
- kinematic viscosity: kinvis,  $\nu$ .

C.2.5. *Waves.*

- wavelength: wlen,  $\lambda$ .
- wave frequency: wfreq,  $\mu$ .

C.2.6. *Physical constants.*

- Boltzmann constant: kboltz,  $k_b$ .
- Stefan-Boltzmann constant: kstef,  $\sigma_{sb}$ .
- Planck constant: kplanck,  $h_p$ .
- speed of light in vacuum: klight,  $c_0$ .
- ideal gas constant: kgas,  $r_g$ .
- Avogadro's number: kavog,  $n_a$ .

C.3. **Dimensional analysis.**

- units of a physical quantity: unit q, unit  $q$ .
- dimension of a physical quantity: dim q, dim  $q$ .
- physical dimension: phdim L, L.
- physical dimension of temperature: phdimtemp,  $\Theta$ .
- dimensionless quantity: kdim,  $\Pi$ .
- characteristic physical quantity: chpq,  $u_c$ .
- scaled physical quantity: scpq,  $\bar{u}$ .
- Biot number: kbiot,  $\Pi_{bi}$ .
- Reynolds number: kreynolds,  $\Pi_{re}$ .
- Prandtl number: kprandtl,  $\Pi_{pr}$ .
- Schmidt number: kschmidt,  $\Pi_{sc}$ .
- Peclet number: kpeclet,  $\Pi_{pe}$ .
- Grashof number: kgrashof,  $\Pi_{gr}$ .
- Rayleigh number: krayleigh,  $\Pi_{ra}$ .
- Weber number: kweber,  $\Pi_{we}$ .
- Capillar number: kcapillar,  $\Pi_{ca}$ .
- Bond number: kbond,  $\Pi_{bo}$ .
- Froude number: kfroud,  $\Pi_{fr}$ .
- Nusselt number: knusselt,  $\Pi_{nu}$ .
- Sherwood number: ksherwood,  $\Pi_{sh}$ .
- power number: kpower,  $\Pi_{po}$ .