

WYDZIAŁ MECHANICZNY ENERGETYKI I LOTNICTWA
POLITECHNIKA WARSZAWSKA

MKWS

PROJECT 1

Combustion parameters for propane-air mixture

Oliwia Waclawek

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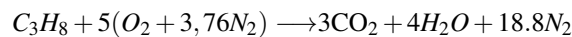
1 Introduction

The aim of this project was to observe the process of burning a propane-air mixture and influence of initial parameters on this process. Four burning parameters for different initial parameters were calculated in Cantera program. The results were presented on graphs (four graphs for each experiment) showing dependencies between time and:

- temperature
- hydrogen mole fraction
- oxygen mole fraction
- propane mole fraction

The experiment was divided into three sections. In each section two initial parameters were defined in the beginning and remained constant, and the other parameter was changed for each experiment in a section. It allows to observe the influence of every parameter individually.

An assumed simplification was that the air in burning reaction consists of oxygen and nitrogen only and their ratio is 1:3,76. With this assumption stoichiometric chemical reaction takes the following form:



Assuming that combustion is complete and that nitrogen does not take part in combustion and does not convert into NO_x

2 Variable pressure

In this section four experiments were run. The temperature and the equivalence ratio were constant and equal to:

$$T=1000K$$

$$\phi = 0.5$$

The pressure was different for each experiment

2.1 $p=50000\text{Pa}$

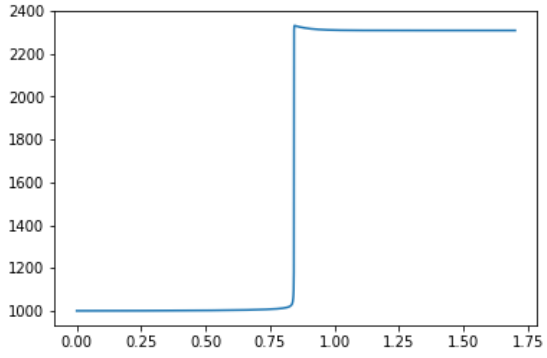


Figure 1: T [K]

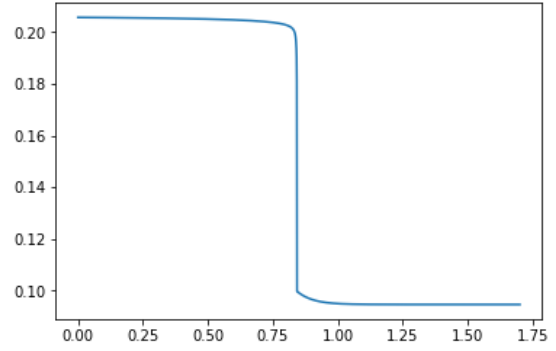


Figure 3: O_2 mole fraction

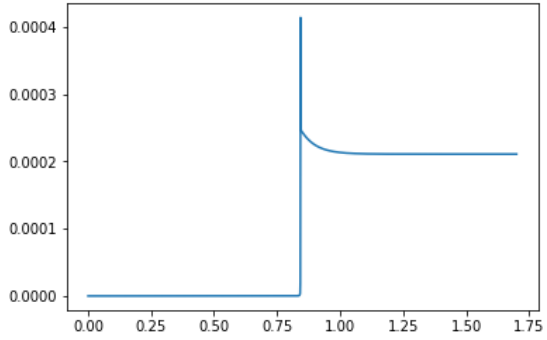


Figure 2: H mole fraction

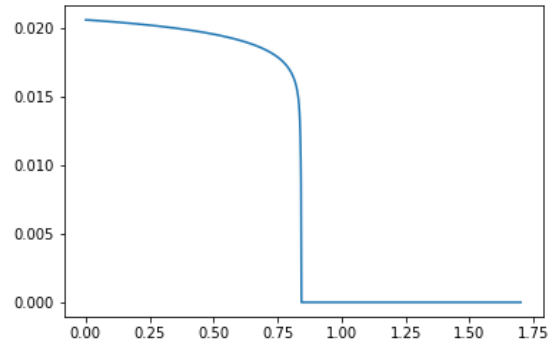


Figure 4: C_3H_8 mole fraction

2.2 $p=150000\text{Pa}$

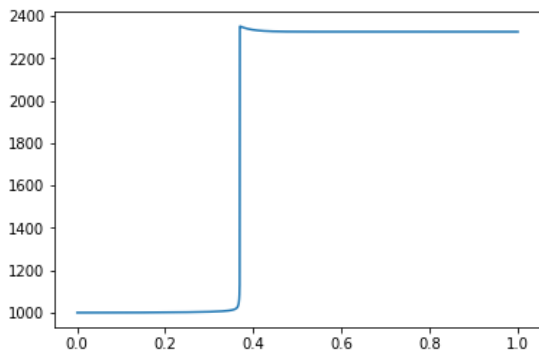


Figure 5: T [K]

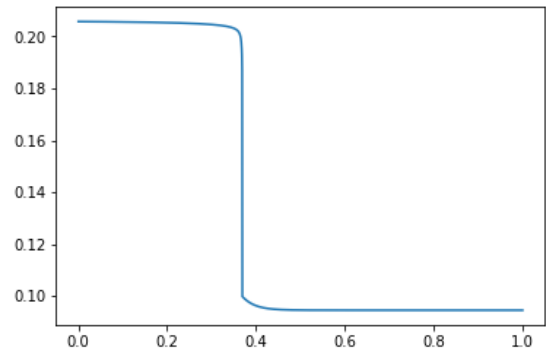


Figure 6: O_2 mole fraction

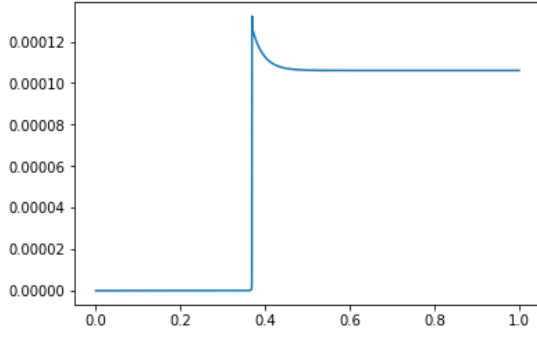


Figure 7: H mole fraction

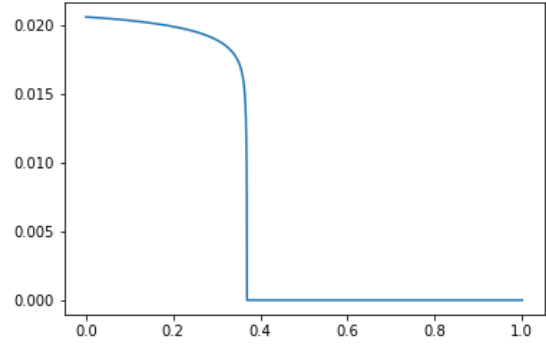


Figure 8: C₃H₈ mole fraction

2.3 $p=300000\text{Pa}$

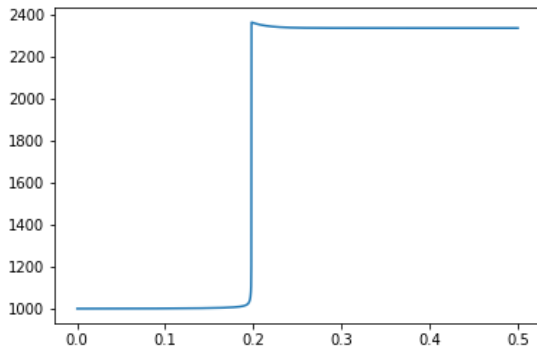


Figure 9: T [K]

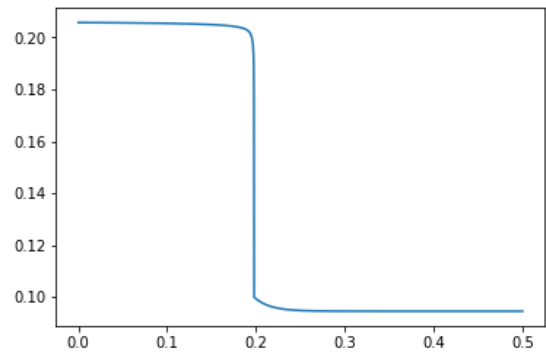


Figure 11: O₂ mole fraction

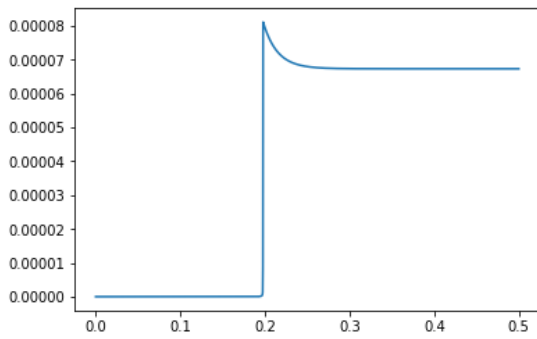


Figure 10: H mole fraction

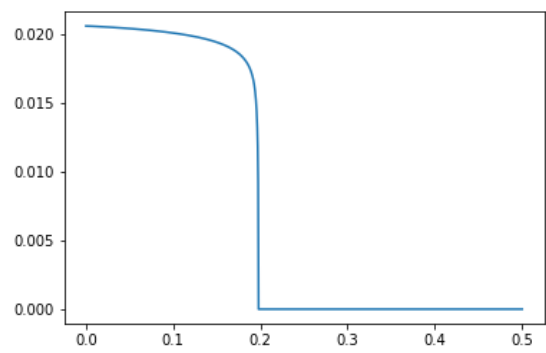


Figure 12: C₃H₈ mole fraction

2.4 $p=600000\text{Pa}$

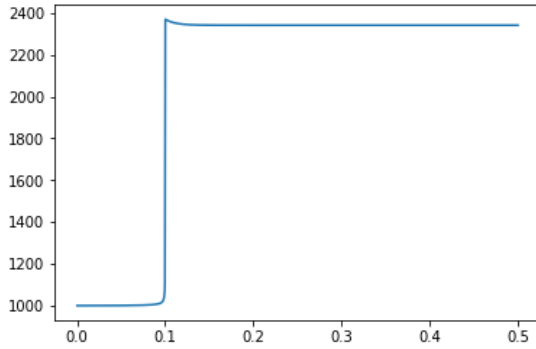


Figure 13: T [K]

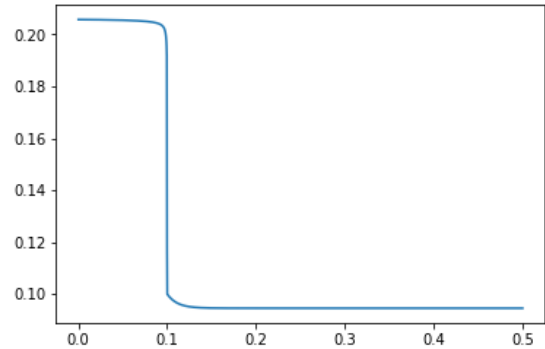


Figure 15: O_2 mole fraction

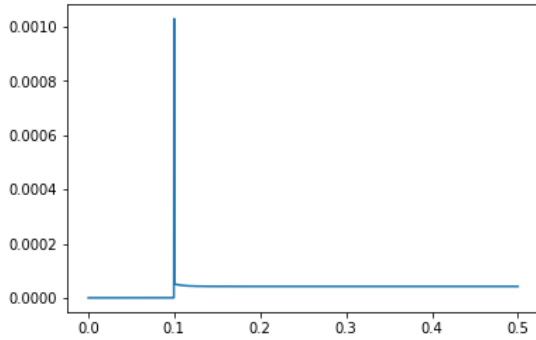


Figure 14: H mole fraction

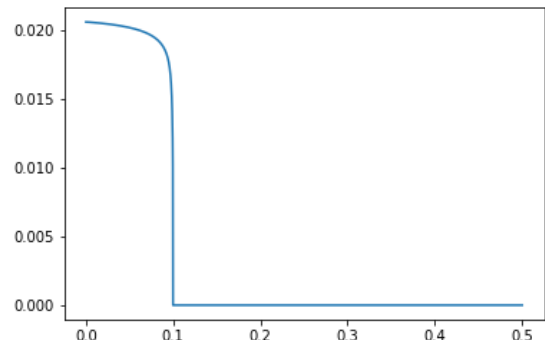


Figure 16: C_3H_8 mole fraction

We can see that the higher the initial pressure, the faster the combustion occurs. In fourth experiment the initial pressure is 12 times higher than in the first one and the combustion in the fourth one takes place circa 8 times faster than in the first one.

The maximum temperatures in all experiments are similar (circa 2350K), which means that initial pressure has no influence on maximum combustion temperature.

Characteristics all similar except for hydrogen mole fraction characteristic. The maximum value (the peak) and the output value (when returns to const.) decreases as the pressure increases. The exception is the last experiment for which the max value is the highest of all.

3 Variable temperature

In this section four experiments were performed. The pressure and the equivalence ratio were constant and equal to:

$$p = 101325\text{Pa} = 1\text{atm}$$

$$\phi = 1$$

The temperature was different for each experiment.

3.1 T=900K

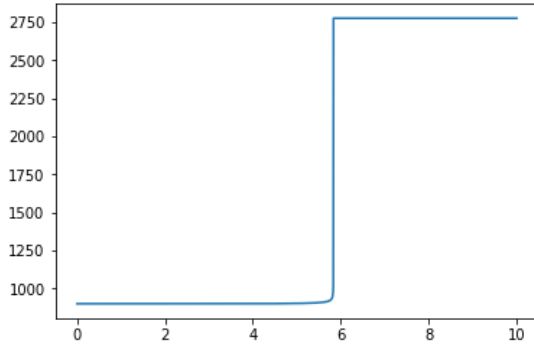


Figure 17: T [K]

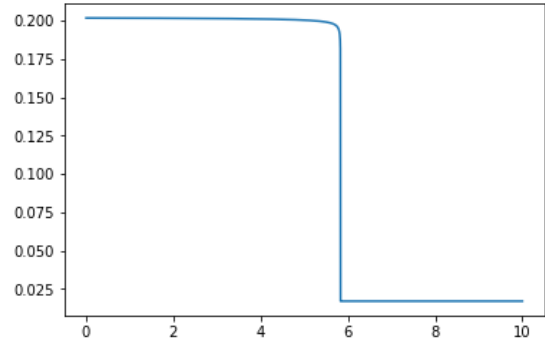


Figure 19: O_2 mole fraction

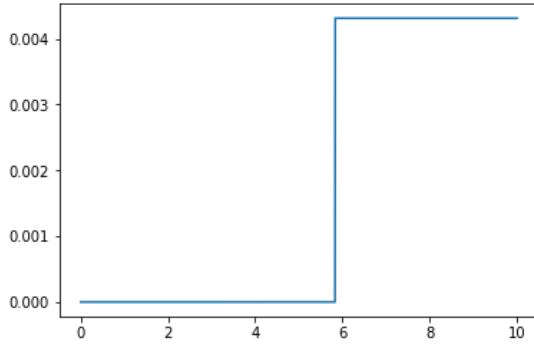


Figure 18: H mole fraction

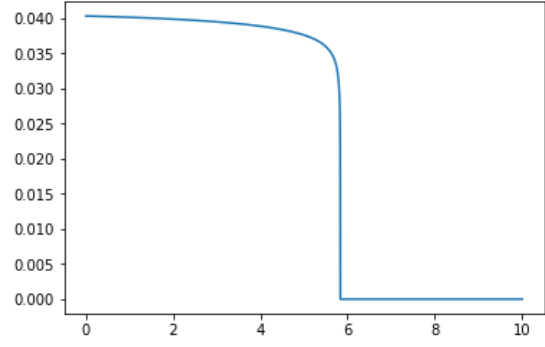


Figure 20: C_3H_8 mole fraction

3.2 T=1000K

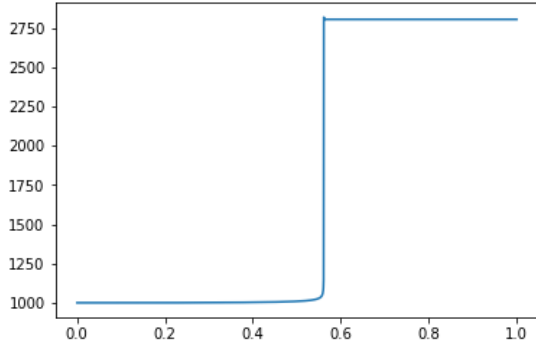


Figure 21: T [K]

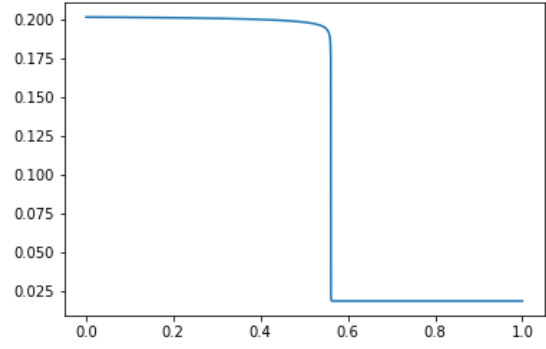


Figure 22: O_2 mole fraction

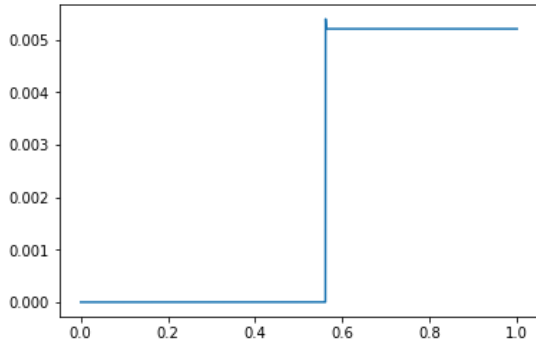


Figure 23: H mole fraction

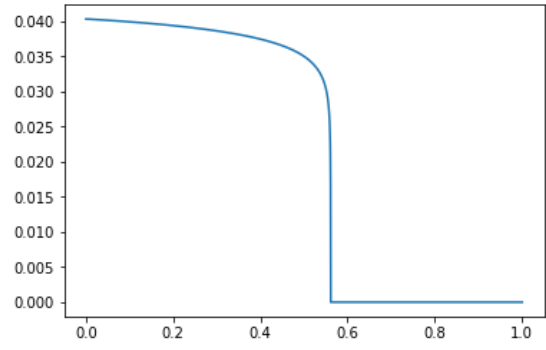


Figure 24: C_3H_8 mole fraction

3.3 T=1100K

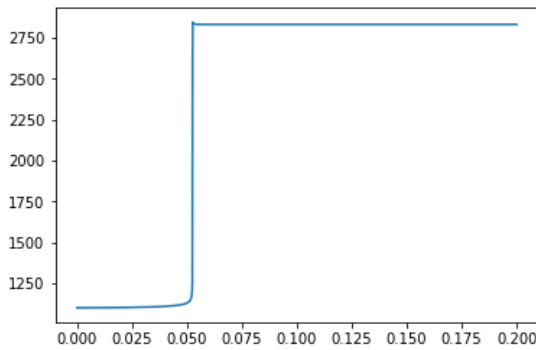


Figure 25: T [K]

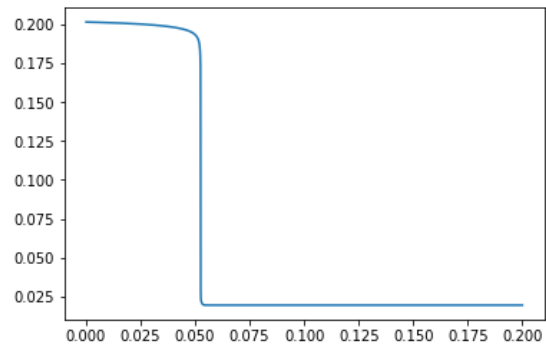


Figure 26: O_2 mole fraction

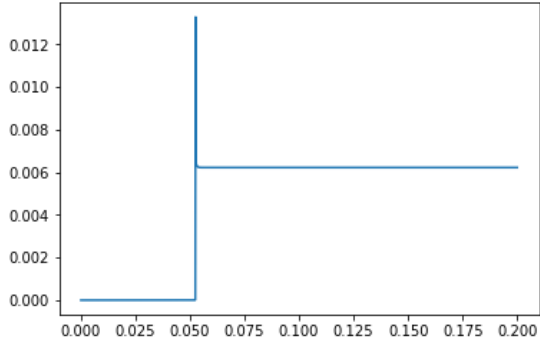


Figure 27: H mole fraction

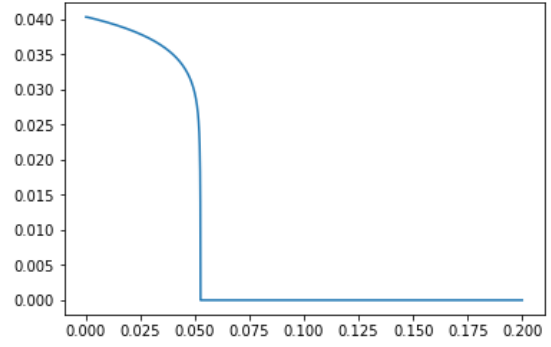


Figure 28: C_3H_8 mole fraction

3.4 T=1200K

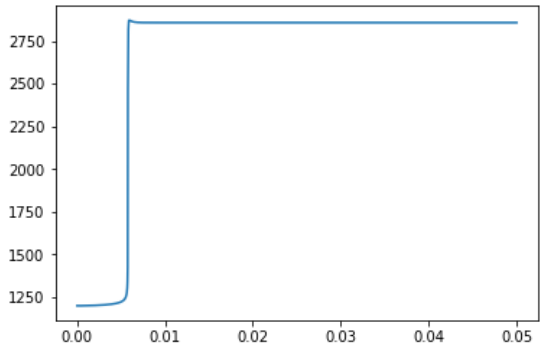


Figure 29: T [K]

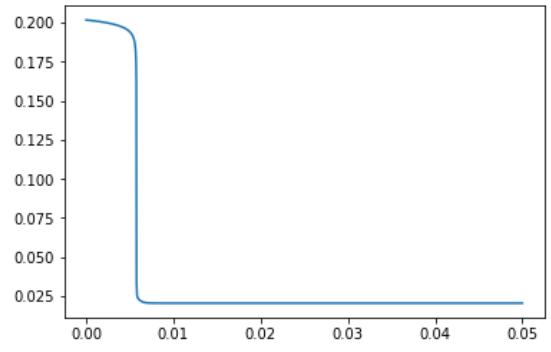


Figure 31: O_2 mole fraction

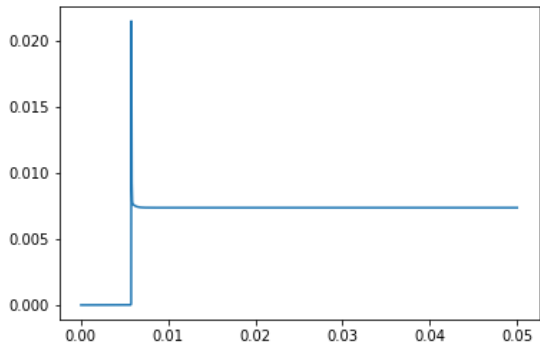


Figure 30: H mole fraction

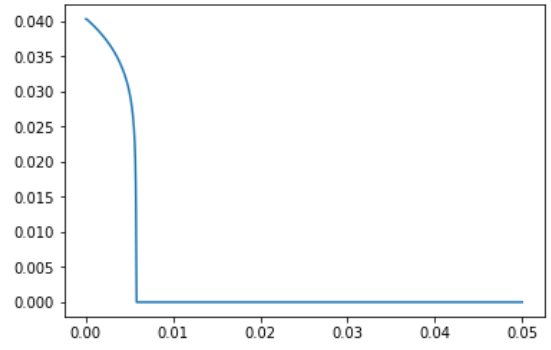


Figure 32: C_3H_8 mole fraction

As with the pressure, higher initial temperature causes faster combustion of the mixture. Temperature difference 300K causes delay to increase circa 100 times.

We can observe a minor differences in maximum temperature value caused by peaks or lack of them in the moment of combustion.

A major difference is visible on 'H mole fraction' graphs. The higher the initial temperature, the greater H mole fraction peak as well as const. value after combustion are.

In the first experiment there is no step change after combustion on any graph. We can assume that the process is more stable, when initial temperature is lower.

4 Variable equivalence ratio

In this section five experiments were run. The pressure and the temperature were constant and equal to:

$$p = 101325 \text{ Pa} = 1 \text{ atm}$$

$$T = 1000 \text{ K}$$

The equivalence ratio was different for each experiment.

The graphs for the same initial parameters ($T=1000\text{K}$, $p=1\text{atm}$) and stoichiometric mixture $\phi = 1$ were already presented in section Variable temperature (Figures 21-24).

Air to fuel ratio for stoichiometric mixture:

$$(A/F)_{\text{stoich}} = \frac{5 \cdot 2 \cdot 16 + 5 \cdot 2 \cdot 3,76 \cdot 14}{3 \cdot 12 + 8 \cdot 1} = 15,6$$

According to literature flammability limits for propane in air are:

$$\text{LFL} = 2,1\%$$

$$\text{UFL} = 9,5\%$$

Air to fuel ratio for LFL and UFL mixtures

$$(A/F)_{\text{LFL}} = \frac{1-0,021}{0,021} \cdot 0,59 = 27,05$$

$$(A/F)_{\text{UFL}} = \frac{1-0,095}{0,095} \cdot 0,59 = 5,62$$

Equivalence ratios for 2,1% and 9,5% mixtures:

$$\phi_{\text{LFL}} = 0,577$$

$$\phi_{\text{UFL}} = 2,78$$

That means that theoretically propane-air mixture is flammable for ϕ greater than 0,577 but not greater than 2,78.

4.1 $\phi = 0.1$

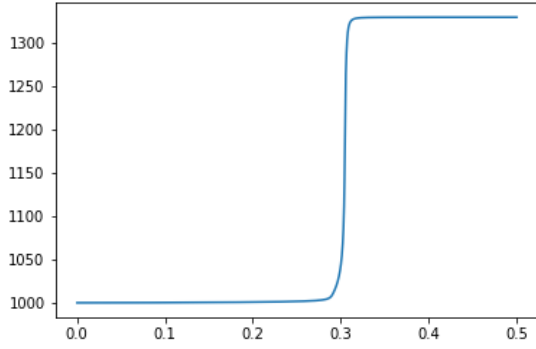


Figure 33: T [K]

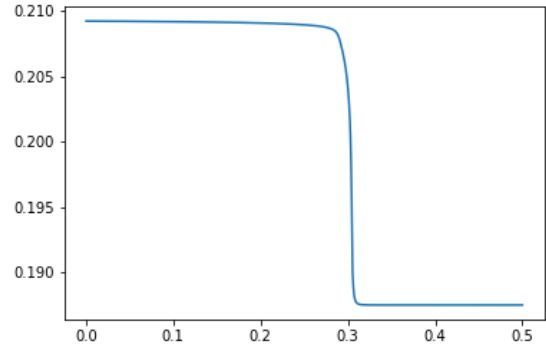


Figure 35: O_2 mole fraction

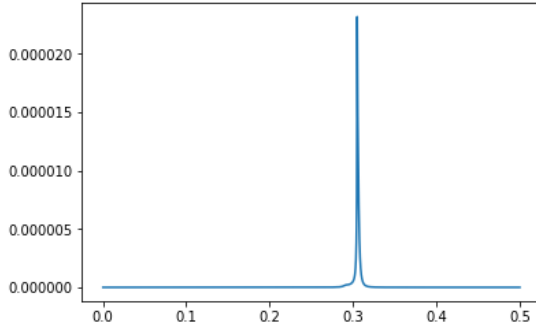


Figure 34: H mole fraction

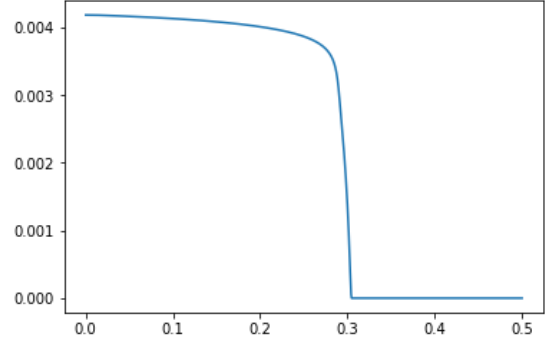


Figure 36: C_3H_8 mole fraction

4.2 $\phi = 0.75$

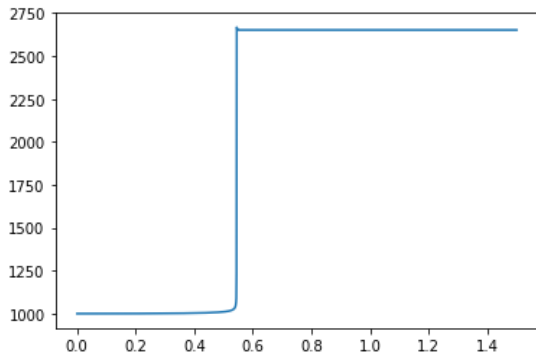


Figure 37: T [K]

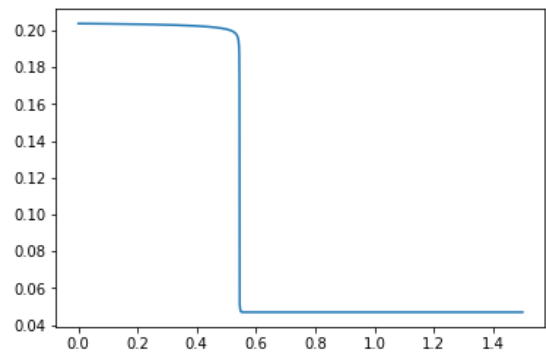


Figure 38: O_2 mole fraction

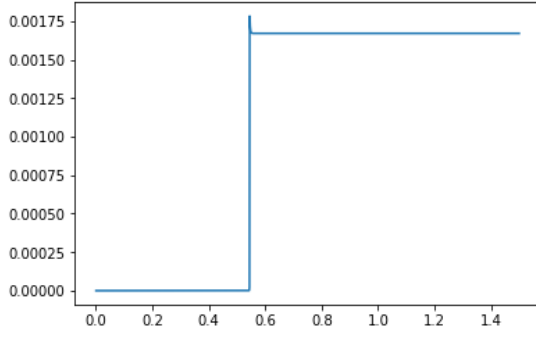


Figure 39: H mole fraction

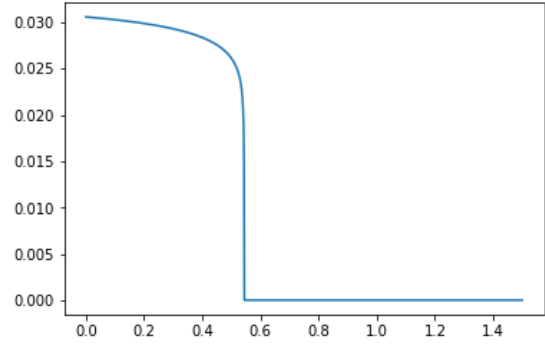


Figure 40: C_3H_8 mole fraction

4.3 $\phi = 1.5$

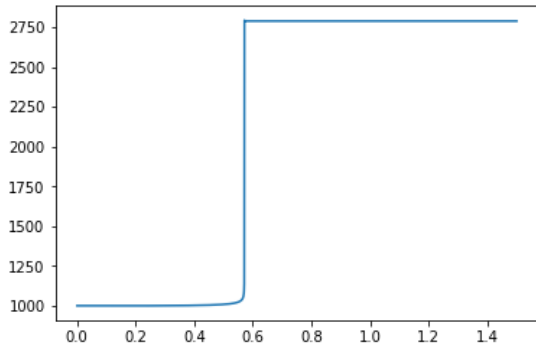


Figure 41: T [K]

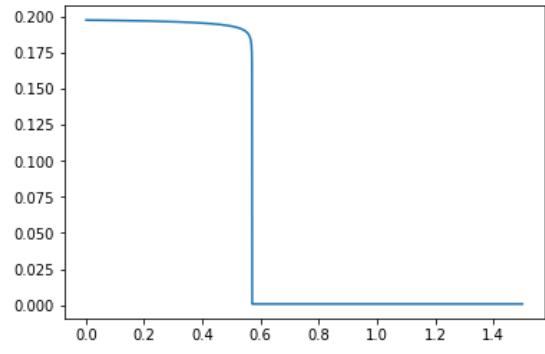


Figure 43: O_2 mole fraction

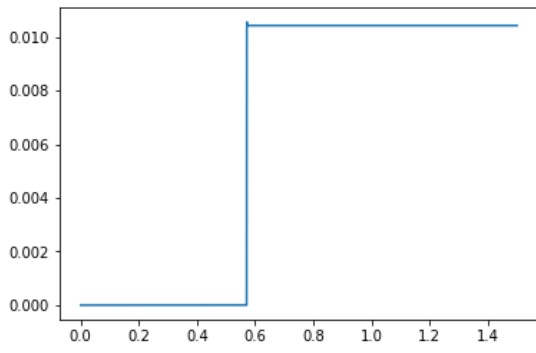


Figure 42: H mole fraction

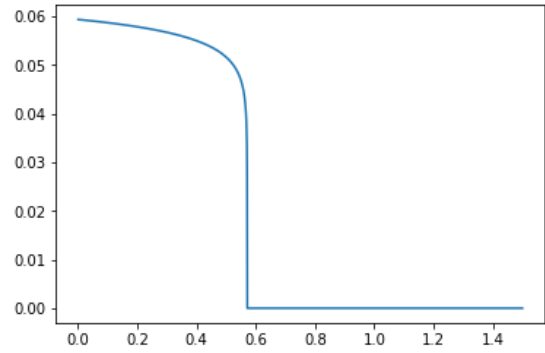


Figure 44: C_3H_8 mole fraction

4.4 $\phi = 3$

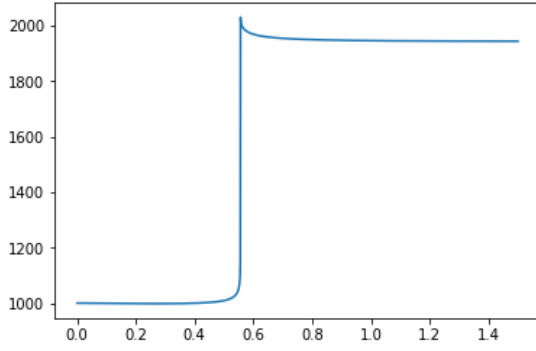


Figure 45: T [K]

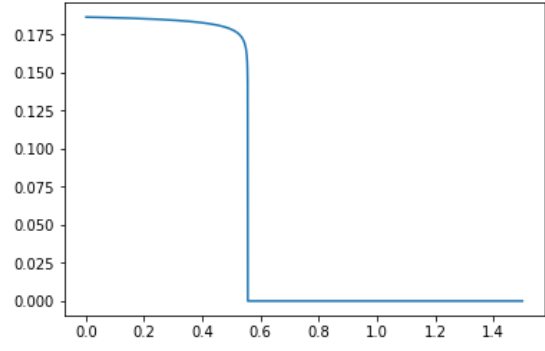


Figure 47: O_2 mole fraction

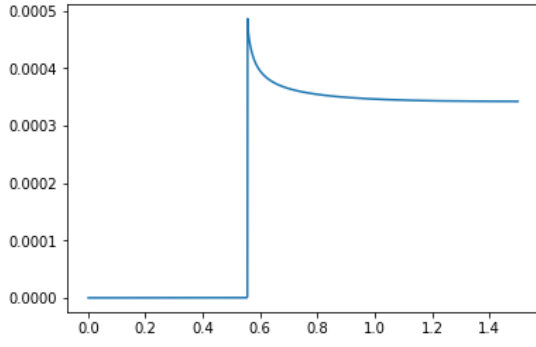


Figure 46: H mole fraction

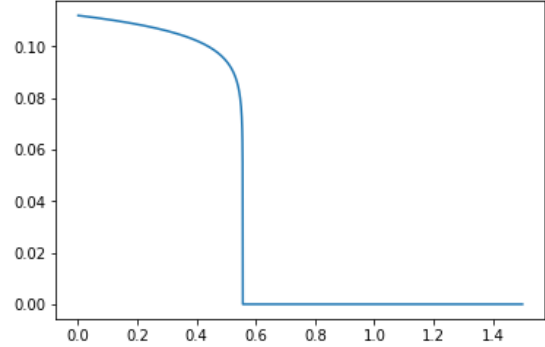


Figure 48: C_3H_8 mole fraction

4.5 $\phi = 5$

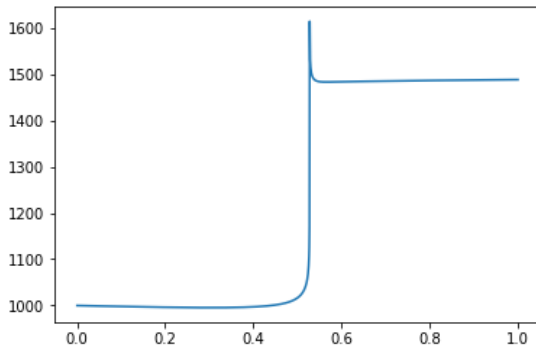


Figure 49: T [K]

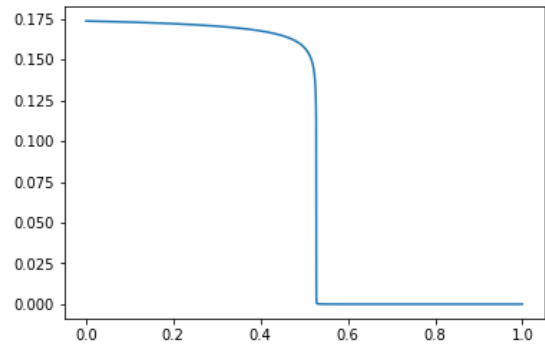


Figure 50: O_2 mole fraction

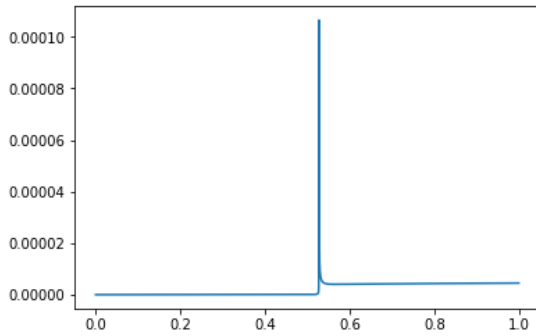


Figure 51: H mole fraction

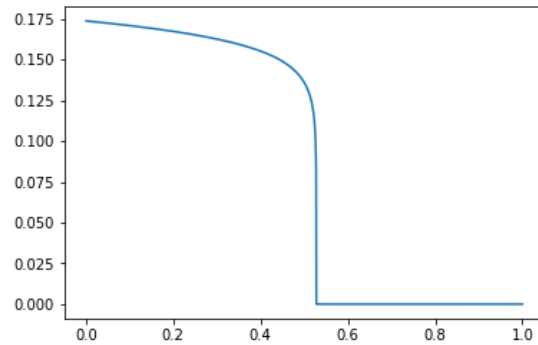


Figure 52: C_3H_8 mole fraction

In the first and the two last experiments where equivalence ratios are smaller or greater than flammability limits a full combustion process does not occur. $T[K]$ and H mole fraction characteristics differ from the others.

Within flammability limits equivalence ratio doesn't have a significant influence on maximum temperature or combustion delay time.

5 Summary

Conclusions

- Influencing the time after which the combustion occurs is possible by changing initial temperature or pressure.
- Combustion is more stable for lower initial temperatures.
- Combustion is possible only within flammability limits. Outside limits we can observe a process in which temperature rises but it is not a combustion.
- Changes in initial parameters don't have a significant influence on C_3H_8 or O_2 mole fraction characteristics.

6 Bibliography

http://fluid.wme.pwr.wroc.pl/~spalanie/dydaktyka/spalanie_instrukcje/spalanie_labor_instr_stezeniowe_granice_palnosci_gazow.pdf