### (1) Fruit drying

RÉPONSES INTÉGRÉES pénalité 0.10

A spherical fruit of diameter D, whose surface is wet, is dried by an airflow at temperature  $T_{\infty}$ , relative humidity  $\psi$ , and velocity  $U_{\infty}$ .

We want to compute the evaporation rate of the water film at the fruit surface.

You will use the following data

Diameter  $D = 4.0 \,\mathrm{cm}$ 

Temperature T = 34.0 °C

Relative humidity  $\psi = 35.\%$ 

Velocity  $U_{\infty} = 9.2 \,\mathrm{m\,s^{-1}}$ 

Atmospheric pressure  $p_{\text{atm}} = 101300$ . Pa

Water saturation pressure at given temperature  $p_{\rm sat}(T) = 5324.\,\mathrm{SI}$ 

Diffusion coefficient  $D_{AV} = 2.65 \, 10^{-5} \, \mathrm{m}^2 \, \mathrm{s}^{-1}$ 

Kinematic viscosity of air  $\nu = 1.63\,10^{-5}\,\mathrm{m^2\,s^{-1}}$ 

These data are personal

Compute the quantities below. The correlation used must involve the Schmidt number.

In your answers, use scientific notations if needed.  $(6.3410^{-5} \text{ writes } 6.34\text{e-}5 \text{ and } 10^3 \text{ writes } 1\text{e}3)$ .

Your answer is considered correct within a relative error of  $5.0\,\%$ 

Indicative ranges are proposed in front of each answer. This are orders of magnitude to help you to check your results.

Reynolds number : Re =

Numérique noté sur 1

 $2.2519226199e + 04 \pm 1.1259613099e + 03$   $\checkmark$ 

 $(22510. \rightarrow 41650.)$ 

Schmidt number : Sc =noté sur 1 Numérique  $6.1577028085e-01 \pm 3.0788514043e-02$   $\checkmark$  $(6.13\,10^{-1} \rightarrow 6.16\,10^{-1})$ Sherwood number : Sh =Numérique noté sur 2  $9.0854257730e + 01 \pm 4.5427128865e + 00$   $\checkmark$  $(90. \to 128.)$ Mass transfer coefficient :  $k_m =$ noté sur 1 Numérique  $6.0278290072e-02 \pm 3.0139145036e-03$   $\checkmark$  $m s^{-1}$   $(4.52 \, 10^{-2} \rightarrow 6.03 \, 10^{-2})$ Vapor concentration at the fruit surface :  $C_{V,\text{surface}} =$ Numérique noté sur 2  $2.0851412530e + 00 \pm 1.0425706265e - 01$  $mol \, m^{-3} \quad (2.08 \to 3.45)$ Incident vapor concentration :  $C_{V,\infty} =$ Numérique noté sur 2  $7.2979943855e-01 \pm 3.6489971927e-02 \checkmark$ 1.14 mol m<sup>-3</sup> (0.72  $\rightarrow$  1.14) Incident vapor concentration:

noté sur 2

 $mol m^{-3}$  (0.72  $\rightarrow$  1.14)

 $7.2979943855e-01 \pm 3.6489971927e-02$   $\checkmark$ 

Massic evaporation rate :  $\dot{m}_V =$ 

Numérique noté sur 1

# $7.3918325783e-06 \pm 3.6959162891e-07$ $\checkmark$

$$kg s^{-1}$$
  $(7.39 10^{-6} \rightarrow 3.79 10^{-5})$ 

The initial film thickness at the fruit surface is assumed to be  $e = 1.0 \,\mathrm{mm}$ 

Compute the total evaporation time:

Numérique noté sur 2

#### $6.8001381153e + 02 \pm 3.4000690576e + 01$ $\checkmark$

s 
$$(530. \rightarrow 680.)$$

#### (2) Fruit drying

RÉPONSES INTÉGRÉES pénalité 0.10

A spherical fruit of diameter D, whose surface is wet, is dried by an airflow at temperature  $T_{\infty}$ , relative humidity  $\psi$ , and velocity  $U_{\infty}$ .

We want to compute the evaporation rate of the water film at the fruit surface.

You will use the following data

Diameter  $D = 8.0 \,\mathrm{cm}$ 

Temperature  $T = 44.0 \,^{\circ}\text{C}$ 

Relative humidity  $\psi = 33.\%$ 

Velocity  $U_{\infty} = 9.0 \,\mathrm{m\,s^{-1}}$ 

Atmospheric pressure  $p_{\rm atm}=101300.\,{\rm Pa}$ 

Water saturation pressure at given temperature  $p_{\text{sat}}(T) = 9111.\,\text{SI}$ 

Diffusion coefficient  $D_{AV} = 2.82 \, 10^{-5} \, \mathrm{m}^2 \, \mathrm{s}^{-1}$ 

Kinematic viscosity of air  $\nu = 1.73 \, 10^{-5} \, \mathrm{m^2 \, s^{-1}}$ 

These data are personal

Compute the quantities below. The correlation used must involve the Schmidt number.

In your answers, use scientific notations if needed.  $(6.3410^{-5} \text{ writes } 6.34\text{e-}5 \text{ and } 10^3 \text{ writes } 1\text{e3})$ .

Your answer is considered correct within a relative error of  $5.0\,\%$ 

Indicative ranges are proposed in front of each answer. This are orders of magnitude to help you to check your results.

Reynolds number : Re =

Numérique noté sur 1

## $4.1654043359e + 04 \pm 2.0827021680e + 03$ $\checkmark$

 $(22510. \rightarrow 41650.)$ 

Schmidt number : Sc =

Numérique noté sur 1

## $6.1330096894e-01 \pm 3.0665048447e-02$ $\checkmark$

 $(6.13\,10^{-1} \rightarrow 6.16\,10^{-1})$ 

Sherwood number : Sh =

Numérique noté sur 2

# $1.2842785885e + 02 \pm 6.4213929423e + 00$ $\checkmark$

 $(90. \to 128.)$ 

Mass transfer coefficient :  $k_m =$ 

Numérique noté sur 1

## $4.5245035769e-02 \pm 2.2622517885e-03$ $\checkmark$

$$m \, s^{-1} \quad (4.52 \, 10^{-2} \, \to \, 6.03 \, 10^{-2})$$

Vapor concentration at the fruit surface :  $C_{V,\text{surface}} =$ 

Numérique noté sur 2

$$3.4556189867e + 00 \pm 1.7278094934e - 01$$
  $\checkmark$ 

 $mol \, m^{-3} \quad (2.08 \to 3.45)$ 

Incident vapor concentration :  $C_{V,\infty} =$ 

Numérique noté sur 2

# $1.1403542656e + 00 \pm 5.7017713281e - 02$ $\checkmark$

 $mol \, m^{-3} \quad (0.72 \, \to \, 1.14)$ 

Incident vapor concentration:

Numérique

noté sur 2

### $1.1403542656e + 00 \pm 5.7017713281e - 02$ $\checkmark$

 $mol \, m^{-3} \quad (0.72 \, \to \, 1.14)$ 

Massic evaporation rate :  $\dot{m}_V =$ 

Numérique noté sur 1

 $3.7911759608e-05 \pm 1.8955879804e-06$   $\checkmark$ 

 $kg s^{-1}$   $(7.39 10^{-6} \rightarrow 3.79 10^{-5})$ 

The initial film thickness at the fruit surface is assumed to be  $e = 1.0 \,\mathrm{mm}$ 

Compute the total evaporation time:

Numérique noté sur 2

 $5.3034185674e + 02 \pm 2.6517092837e + 01$   $\checkmark$ 

s  $(530. \rightarrow 680.)$ 

Total des points : 28