

Concepts

Variables

Pressure - Normal force per unit area exerted on a surface due to the time rate of change of momentum of the gas particles impacing said surface.

$$P = \lim_{dA \rightarrow 0} \frac{dF_n}{dA}$$

Density - Mass per unit volume.

$$\rho = \lim_{dV \rightarrow 0} \frac{dm}{dV}$$

Temperature - Change in kinetic energy due to random molecular motion.

$$KE = \frac{3}{2}kT$$

Flow Velocity - Velocity due to organized motion.

$$\vec{v} = \frac{d\vec{x}}{dt}$$

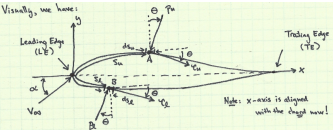
Forces and Moments

Causes of forces and moments on an aerodynamic body:

Pressure Distribution over the body surface.

Shear Stress Distribution over the surface:

$$\tau = \lim_{dA \rightarrow 0} \frac{dF_f}{dA} = \mu \frac{dV}{dy}$$



Lift and Drag per Unit Span:

$$L' = N' \cos \alpha - A' \sin \alpha$$

$$D' = N' \sin \alpha + A' \cos \alpha$$

Normal Force per Unit Span:

$$N' = \int_{LE}^{TE} (P_u \cos \theta + \tau_u \sin \theta) ds_u + \int_{LE}^{TE} (P_l \cos \theta - \tau_l \sin \theta) ds_l$$

Axial Force per Unit Span:

$$A' = \int_{LE}^{TE} (-P_u \sin \theta + \tau_u \cos \theta) ds_u + \int_{LE}^{TE} (P_l \sin \theta + \tau_l \cos \theta) ds_l$$

Moment per Unit Span:

$$M'_* = \int_{LE}^{TE} [(P_u \cos \theta + \tau_u \sin \theta)(x - x^*) - (P_u \sin \theta - \tau_u \cos \theta)(y - y^*)] ds_u + \int_{LE}^{TE} [(-P_l \cos \theta + \tau_l \sin \theta)(x - x^*) + (P_l \sin \theta + \tau_l \cos \theta)(y - y^*)] ds_l$$

When $x^* = y^* = 0$ we obtain the moment about the leading edge.

Center of Pressure:

$$x_{cp} = -\frac{M'_{LE}}{N'}$$

Force and Moment Coefficients

Dynamic Pressure: $q = \frac{1}{2} \rho_{\infty} v_{\infty}^2$

Reference Area: S

Reference Length: L or c

Lift Coefficient: $c_L = \frac{L}{q_{\infty} S}$

Drag Coefficient: $c_D = \frac{D}{q_{\infty} S}$

Moment Coefficient: $c_M = \frac{M}{q_{\infty} S L}$

Buckingham Pi Theorem

If we have a physically meaningful equation such as:

$$f(P_1, P_2, \dots, P_N) = 0$$

where P_i are physical variables in terms of K independent physical units (mass, length, time, temperature) then it can be re-stated as:

$$F(\Pi_1, \Pi_2, \dots, \Pi_{N-K}) = 0$$
 or

$$\Pi_{N-K} = G(\Pi_1, \Pi_2, \dots, \Pi_{N-K-1})$$

where Π_i are dimensionaless variables known as Pi Groups.

Basic Flow Equations

Fixed control volumes for basic flow equations.

Conservation of Mass

Net mass flow out of \mathcal{V} = Time rate of decrease of mass inside \mathcal{V} .

Integral Continuity Equation:

$$\frac{\partial}{\partial t} \iiint_{\mathcal{V}} \rho d\mathcal{V} + \iint_S \rho \vec{V} \cdot d\vec{S} = 0$$

Differential Continuity Equation:

$$\frac{\partial \rho}{\partial t} + \vec{\nabla} \cdot (\rho \vec{V}) = 0$$

Conservation of Momentum

Net force applied to \mathcal{V} = Time rate of change of momentum of fluid in \mathcal{V}

$$\frac{\partial}{\partial t} \iiint_{\mathcal{V}} \rho \vec{V} d\mathcal{V} + \iint_S (\rho \vec{V} \cdot d\vec{S}) \vec{V} = - \iint_S p d\vec{S} + \iiint_{\mathcal{V}} \rho \vec{f} d\mathcal{V} + \vec{F}_{viscous}$$

1. Body Forces (e.g. gravity) which act on the fluid inside \mathcal{V}
 $\iiint_{\mathcal{V}} \rho \vec{f} d\mathcal{V}$
2. Pressure and shear surface forces acting on S
 $- \iint_S p d\vec{S} + \vec{F}_{viscous}$
3. Net flow of momentum out of volume across S
 $\iint_S (\rho \vec{V} \cdot d\vec{S}) \vec{V}$
4. Time rate of change of momentum due to unsteadiness in volume
 $\frac{\partial}{\partial t} \iiint_{\mathcal{V}} \rho \vec{V} d\mathcal{V}$

Navier-Stokes Equations:

$$\frac{\partial}{\partial t}(\rho u) + \vec{\nabla} \cdot (\rho u \vec{V}) = -\frac{\partial p}{\partial x} + \rho f_x + (F_x)_{viscous}$$

$$\frac{\partial}{\partial t}(\rho v) + \vec{\nabla} \cdot (\rho v \vec{V}) = -\frac{\partial p}{\partial y} + \rho f_y + (F_y)_{viscous}$$

Conservation of Energy

$$\frac{\partial}{\partial t} \iiint_{\mathcal{V}} \rho \left(e + \frac{V^2}{2} \right) d\mathcal{V} + \iint_S \rho \left(e + \frac{V^2}{2} \right) \vec{V} \cdot d\vec{S} = \iiint_{\mathcal{V}} \dot{q} \rho d\mathcal{V} + \underbrace{\dot{Q}_{viscous}}_{\text{Heat Addition Due to Viscosity}} - \iint_S \rho \vec{V} \cdot d\vec{S} + \iint_S \rho \vec{F} \cdot \vec{V} d\mathcal{V}$$

Net Time Rate of Change of Total Energy Due to Unsteadiness in \mathcal{V}

Net Rate of Flow of Total Energy Out of \mathcal{V}

Rate of Volumetric Heating

Rate of Pressure Work

Rate of Work Done by Body Forces

Rate of Viscous Work

$$\frac{\partial}{\partial t} \left(\rho \left(e + \frac{V^2}{2} \right) \right) + \vec{\nabla} \cdot \left(\rho \left(e + \frac{V^2}{2} \right) \vec{V} \right) = \rho \dot{q} + \dot{Q}'_{viscous} - \vec{\nabla} \cdot (\rho \vec{V}) + \rho \vec{F} \cdot \vec{V} + \dot{W}'_{viscous}$$

Kinematics

$\vec{\nabla} \cdot \vec{V}$: time rate of change of volume of a fluid element per unit volume → **Dilation**

Stream Line: Curve everywhere tangent to the velocity.

$$\frac{v}{u} = \frac{dy}{dx}$$

Path Line: Trajectory of a particle released from a point in time.

Streak Line: Line connecting all particles that have passed through a given point.

For a steady flow the three lines coincide.

Substantial Derivative

Time rate of change of density of a given material fluid element as it moves through space and time.

$$\frac{D\rho}{Dt} = \frac{\partial \rho}{\partial t} + \vec{V} \cdot \vec{\nabla} \rho$$

Continuity Equation: $\frac{D\rho}{Dt} = -\rho \vec{\nabla} \cdot \vec{V}$

Material Acceleration: $\left(\frac{Du}{Dt}; \frac{Dv}{Dt}; \frac{Dz}{Dt} \right)$

Navier-Stokes:

$$\rho \frac{Du}{Dt} = -\frac{\partial p}{\partial x} + \rho f_x + (F_x)_{viscous} \rightarrow \text{applicable to } y \text{ and } z \text{ as well.}$$

Vorticity and Strain

$$\vec{\omega} = \frac{1}{2} \vec{\nabla} \times \vec{V} \rightarrow \text{angular velocity}$$

$$\vec{\xi} = \vec{\nabla} \times \vec{V} \rightarrow \text{Vorticity}$$

$$\epsilon_{xy} = \frac{\partial v}{\partial x} + \frac{\partial u}{\partial y} \rightarrow \text{Rate of Strain in } xy \text{ plane.}$$

$$\Gamma = -\oint_C \vec{V} \cdot d\vec{s} \rightarrow \text{Circulation}$$

$$\text{Relation between circulation and vorticity: } \vec{\omega} \cdot \vec{n} = \frac{d\Gamma}{dS}$$

Stream Functions and Velocity Potentials

Stream Function: For every incompressible, two-dimensional flow, there exists a scalar stream function such that:

$$u = \frac{\partial \psi}{\partial y}, v = -\frac{\partial \psi}{\partial x} \text{ DON'T FORGET } +C$$

$$\nabla^2 \psi = 0$$

Velocity Potential: For every irrotational flow, there exists a scalar velocity potential such that:

$$\vec{V} = \nabla \phi \rightarrow \frac{\partial \phi}{\partial x} = u, \frac{\partial \phi}{\partial y} = v$$

$$\nabla^2 \phi = 0$$

Laplace's Equation: 2nd order linear partial differential equation. Allows **superposition** if both ψ_1 and ψ_2 are solutions to

$\nabla^2 \phi = 0$, then $\psi_3 = \psi_1 + \psi_2$ is also a solution.

Finding Solutions:

1) Infinite Boundary Condition: far from the body, velocity is uniform and aligned with x-axis.

$$\phi(x, y) = v_\infty x \text{ and } \psi(x, y) = v_\infty y$$

2) Wall boundary: no flow of mass or momentum through solid boundaries.

$$\frac{\partial \phi}{\partial n} = 0 \text{ and } \frac{\partial \psi}{\partial n} = 0$$

To Find L, D, and M:

1) Solve Laplace's eq. for ϕ w/ boundary conditions.

2) Obtain velocity field: $\vec{V} = \nabla \phi$

3) Obtain P: Bernoulli's Equation **Euler's Equation:**

$$\frac{1}{2} d(V^2) = -\frac{1}{\rho} dp$$

If flow is barotropic, $\rho = \rho(p)$ is a function of pressure only and can integrate the equation. Occurs in incompressible flow, isothermal flow, or isentropic (frictionless) flow.

Bernoulli's Equation: $p + \frac{1}{2} \rho V^2 = \text{constant}$ - along a streamline for steady, inviscid, incompressible flow with no body forces.

$$c_P = 1 - \left(\frac{v}{v_\infty} \right)^2$$

Flow in a Duct

$\rho_1 A_1 V_1 = \rho_2 A_2 V_2 \rightarrow$ Steady, inviscid flow in a duct with no body forces. For incompressible flow remove ρ .

Elementary Flows & Combinations

Uniform Flow

$$\phi(x, y) = v_\infty x \text{ and } \psi(r, \theta) = v_\infty r \cos \theta$$

$$\psi(x, y) = v_\infty y \text{ and } \phi(r, \theta) = v_\infty r \sin \theta$$

$$\Gamma = 0$$

Source/Sink

$$\vec{V} = \left[\frac{\Lambda}{2\pi r} \right]$$

$$\phi(r, \theta) = \frac{\Lambda \ln(r)}{2\pi}$$

$$\psi(r, \theta) = \frac{\Lambda \theta}{2\pi}$$

$$\Gamma = 0$$

Superposition

Uniform Flow + Source

$$\psi(r, \theta) = v_\infty r \sin \theta + \frac{\Lambda \theta}{2\pi r}$$

$$\text{Equation for Body Shape: } r(\theta) = \frac{\Lambda(\pi - \theta)}{2\pi v_\infty \sin \theta} \text{ and } h = \frac{\Lambda}{v_\infty}$$

Rankine Oval Flow

Uniform Flow + Source + Sink

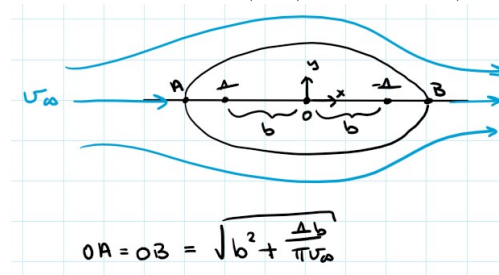
$$\psi(r, \theta) = v_\infty r \sin \theta + \frac{\Lambda \theta_1}{2\pi} + \frac{-\Lambda \theta_2}{2\pi}$$

$$\psi(x, y) = v_\infty y + \frac{\Lambda}{2\pi} \tan^{-1} \left(\frac{y}{x+b} \right) - \frac{\Lambda}{2\pi} \tan^{-1} \left(\frac{y}{x-b} \right)$$

$$\vec{V} = \left[\begin{array}{c} v_\infty + \frac{\Lambda}{2\pi} \frac{x+b}{(x+b)^2 + y^2} - \frac{\Lambda}{2\pi} \frac{x-b}{(x-b)^2 + y^2} \\ \frac{\Lambda}{2\pi} \frac{y}{(x+b)^2 + y^2} - \frac{\Lambda}{2\pi} \frac{y}{(x-b)^2 + y^2} \end{array} \right]$$

Equation of a Rankine Oval:

$$0 = v_\infty y + \frac{\Lambda}{2\pi} \tan^{-1} \left(\frac{y}{x+b} \right) - \frac{\Lambda}{2\pi} \tan^{-1} \left(\frac{y}{x-b} \right)$$



Doublet

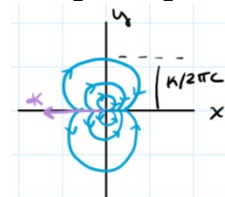
Source + Sink

Rankine Oval $b \rightarrow 0$

$$\psi(r, \theta) = \frac{-\kappa \sin \theta}{2\pi r}$$

$$\phi(r, \theta) = \frac{\kappa \cos \theta}{2\pi r}$$

$$\vec{V} = \left[\begin{array}{c} -\frac{\kappa \cos \theta}{2\pi r^2} \\ \frac{\kappa \sin \theta}{2\pi r^2} \end{array} \right]$$



Non-Lifting Flow over Cylinder

Uniform Flow + Doublet

$$\psi(r, \theta) = v_\infty r \sin \theta \left(1 - \frac{R^2}{r^2} \right)$$

$$\vec{V} = \left[\begin{array}{c} v_\infty \cos \theta \left(1 - \frac{R^2}{r^2} \right) \\ -v_\infty \sin \theta \left(1 + \frac{R^2}{r^2} \right) \end{array} \right]$$

Stagnation points at $v_r = v_\theta = 0$ or $(r, \theta) = (R, 0), (R, \pi)$

$L = D = 0$, when $D = 0$ it is called D'Alembert's Paradox

Vortex Flow

Rotation flow, but the fluid elements themselves do not rotate. They follow a streamline in a circle at a particular radius.

Must make $rv_\theta = c$ in order to prevent going to $r = 0$ where flow is not irrotational.

$$\vec{V} = \left[\begin{array}{c} 0 \\ \frac{c}{r} = \frac{-\Gamma}{2\pi r} \end{array} \right]$$

$$\phi(r, \theta) = \frac{-\Gamma \theta}{2\pi}$$

$$\psi(r, \theta) = \frac{\Gamma \ln r}{2\pi}$$

Calculus Review

Vector Calculus

$$\text{Magnitude: } |\vec{A}| = \sqrt{A_1^2 + A_2^2 + A_3^2}$$

$$\text{Dot Product: } \vec{A} \cdot \vec{B} = A_x B_x + A_y B_y + A_z B_z = |\vec{A}| |\vec{B}| \cos \theta$$

$$\text{Cross Product: } \vec{A} \times \vec{B} = (A_y B_z - A_z B_y) \hat{i} + (A_z B_x - A_x B_z) \hat{j} + (A_x B_y - A_y B_x) \hat{k}$$

$$|\vec{A} \times \vec{B}| = |\vec{A}| |\vec{B}| \sin \theta$$

Gradient of Scalar Field: Vector Field

$$\text{Cart.: } \vec{\nabla} p = \frac{\partial p}{\partial x} \hat{i} + \frac{\partial p}{\partial y} \hat{j} + \frac{\partial p}{\partial z} \hat{k}$$

$$\text{Cyl.: } \vec{\nabla} p = \frac{\partial p}{\partial r} \hat{r} + \frac{1}{r} \frac{\partial p}{\partial \theta} \hat{\theta} + \frac{\partial p}{\partial z} \hat{z}$$

Directional Derivative: $\frac{dp}{ds} = \vec{\nabla} p \cdot \vec{s} \rightarrow$ unit vector in \vec{s} direction.

Divergence of a Vector Field: Scalar Field

$$\text{Cart.: } \text{div} \vec{V} = \vec{\nabla} \cdot \vec{V} = \frac{\partial V_x}{\partial x} + \frac{\partial V_y}{\partial y} + \frac{\partial V_z}{\partial z}$$

$$\text{Cyl.: } \text{div} \vec{V} = \vec{\nabla} \cdot \vec{V} = \frac{1}{r} \frac{\partial(r V_r)}{\partial r} + \frac{1}{r} \frac{\partial V_\theta}{\partial \theta} + \frac{\partial V_z}{\partial z}$$

Curl of a Vector Field: $\text{curl} \vec{V} = \vec{\nabla} \times \vec{V}$

$$\text{Cart.: } = \left(\frac{\partial V_z}{\partial y} - \frac{\partial V_y}{\partial z} \right) \hat{i} + \left(\frac{\partial V_x}{\partial z} - \frac{\partial V_z}{\partial x} \right) \hat{j} + \left(\frac{\partial V_y}{\partial x} - \frac{\partial V_x}{\partial y} \right) \hat{k}$$

$$\text{Cyl.: } = \left(\frac{1}{r} \frac{\partial V_z}{\partial \theta} - \frac{\partial V_\theta}{\partial z} \right) \hat{r} + \left(\frac{\partial V_r}{\partial z} - \frac{\partial V_z}{\partial r} \right) \hat{\theta} + \left(\frac{1}{r} \frac{\partial}{\partial r}(r V_\theta) - \frac{1}{r} \frac{\partial V_r}{\partial \theta} \right) \hat{z}$$

Laplacian: ∇^2

$$\text{Cart.: } = \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2} + \frac{\partial^2}{\partial z^2}$$

$$\text{Cyl.: } = \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2}{\partial \theta^2} + \frac{\partial^2}{\partial z^2}$$

Integrals

$$\text{Stokes' Theorem: } \oint_C \vec{A} \cdot d\vec{s} = \iint_S (\vec{\nabla} \times \vec{A}) \cdot d\vec{S}$$

$$\text{Divergence Theorem: } \oint_S \vec{A} \cdot d\vec{S} = \iiint_V (\vec{\nabla} \cdot \vec{A}) dV$$

$$\text{Gradient Theorem: } \oint_S p d\vec{S} = \iiint_V \vec{\nabla} p dV$$