

## Concepts

### Variables

**Pressure** - Normal force per unit area exerted on a surface due to the time rate of change of momentum of the gas particles impacting said surface.

$$P = \lim_{dA \rightarrow 0} \frac{dF_n}{dA}$$

**Density** - Mass per unit volume.

$$\rho = \lim_{dV \rightarrow 0} \frac{dm}{dV}$$

**Temperature** - Change in kinetic energy due to random molecular motion.

$$KE = \frac{3}{2}kT$$

**Flow Velocity** - Velocity due to organized motion.

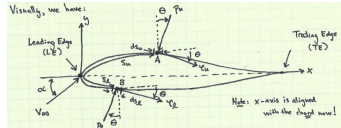
$$\vec{v} = \frac{d}{dt}\vec{x}$$

### Forces and Moments

**Causes of forces and moments on an aerodynamic body:**

Pressure Distribution over the body surface.

Shear Stress Distribution over the surface.



**Lift and Drag per Unit Span:**

$$L' = N' \cos \alpha - A' \sin \alpha$$

$$D' = N' \sin \alpha + A' \cos \alpha$$

**Normal Force per Unit Span:**

$$N' = \int_{LE}^{TE} (P_u \cos \theta + \tau_u \sin \theta) ds_u + \int_{LE}^{TE} (P_l \cos \theta - \tau_l \sin \theta) ds_l$$

**Axial Force per Unit Span:**

$$A' = \int_{LE}^{TE} (-P_u \sin \theta + \tau_u \cos \theta) ds_u + \int_{LE}^{TE} (P_l \sin \theta + \tau_l \cos \theta) ds_l$$

**Moment per Unit Span:**

$$M'_* = \int_{LE}^{TE} [(P_u \cos \theta + \tau_u \sin \theta)(x - x^*) - (P_u \sin \theta - \tau_u \cos \theta)(y - y^*)] ds_u + \int_{LE}^{TE} [(-P_l \cos \theta + \tau_l \sin \theta)(x - x^*) + (P_l \sin \theta + \tau_l \cos \theta)(y - y^*)] ds_l$$

When  $x^* = y^* = 0$  we obtain the moment about the leading edge.

**Center of Pressure:**

$$x_{cp} = -\frac{M'_{LE}}{N'}$$

### Force and Moment Coefficients

**Dynamic Pressure:**  $q = \frac{1}{2} \rho_{\infty} v_{\infty}^2$  **Reference Area:**  $S$

**Reference Length:**  $L$  or  $c$

**Lift Coefficient:**  $c_L = \frac{L}{q_{\infty} S}$

**Drag Coefficient:**  $c_D = \frac{D}{q_{\infty} S}$

**Moment Coefficient:**  $c_M = \frac{M}{q_{\infty} S L}$

### Buckingham Pi Theorem

If we have a physically meaningful equation such as:

$$f(P_1, P_2, \dots, P_N) = 0$$

where  $P_i$  are physical variables in terms of  $K$  independent physical units (mass, length, time, temperature) then it can be re-stated as:

$$F(\Pi_1, \Pi_2, \dots, \Pi_{N-K}) = 0 \text{ or}$$

$$\Pi_{N-K} = G(\Pi_1, \Pi_2, \dots, \Pi_{N-K-1})$$

where  $\Pi_i$  are dimensionless variables known as Pi Groups.

## Calculus Review

### Vector Calculus

$$\text{Magnitude: } |\vec{A}| = \sqrt{A_1^2 + A_2^2 + A_3^2}$$

$$\text{Dot Product: } \vec{A} \cdot \vec{B} = A_x B_x + A_y B_y + A_z B_z = |\vec{A}| |\vec{B}| \cos \theta$$

$$\text{Cross Product: } \vec{A} \times \vec{B} = (A_y B_z - A_z B_y) \hat{i} + (A_z B_x - A_x B_z) \hat{j} + (A_x B_y - A_y B_x) \hat{k}$$

$$|\vec{A} \times \vec{B}| = |\vec{A}| |\vec{B}| \sin \theta$$

$$\text{Gradient of Scalar Field: } \vec{\nabla} p = \frac{\partial p}{\partial x} \hat{i} + \frac{\partial p}{\partial y} \hat{j} + \frac{\partial p}{\partial z} \hat{k} \text{ vector field}$$

$$\text{Directional Derivative: } \frac{dp}{ds} = \vec{\nabla} p \cdot \vec{s} \rightarrow \text{unit vector in } \vec{s} \text{ direction.}$$

$$\text{Divergence of a Vector Field: } \text{div } \vec{V} = \vec{\nabla} \cdot \vec{V} = \frac{\partial V_x}{\partial x} + \frac{\partial V_y}{\partial y} + \frac{\partial V_z}{\partial z} \text{ scalar field}$$

$$\text{Curl of a Vector Field: } \text{curl } \vec{V} = \vec{\nabla} \times \vec{V} = \left( \frac{\partial V_z}{\partial y} - \frac{\partial V_y}{\partial z} \right) \hat{i} + \left( \frac{\partial V_x}{\partial z} - \frac{\partial V_z}{\partial x} \right) \hat{j} + \left( \frac{\partial V_y}{\partial x} - \frac{\partial V_x}{\partial y} \right) \hat{k}$$

### Integrals

$$\text{Stokes' Theorem: } \oint_C \vec{A} \cdot d\vec{s} = \iint_S (\vec{\nabla} \times \vec{A}) \cdot d\vec{S}$$

$$\text{Divergence Theorem: } \oint_S \vec{A} \cdot d\vec{S} = \iiint_V (\vec{\nabla} \cdot \vec{A}) dV$$

$$\text{Gradient Theorem: } \oint_S p d\vec{S} = \iiint_V \vec{\nabla} p dV$$

## Basic Flow Equations

Fixed control volumes for basic flow equations.

### Conservation of Mass

Net mass flow out of  $\mathcal{V}$  = Time rate of decrease of mass inside  $\mathcal{V}$ .

**Integral Continuity Equation:**

$$\frac{\partial}{\partial t} \iiint_V \rho dV + \oint_S \rho \vec{V} \cdot d\vec{S} = 0$$

**Differential Continuity Equation:**

$$\frac{\partial \rho}{\partial t} + \vec{\nabla} \cdot (\rho \vec{V}) = 0$$

### Conservation of Momentum

Net force applied to  $\mathcal{V}$  = Time rate of change of momentum of fluid in  $\mathcal{V}$

$$\frac{\partial}{\partial t} \iiint_V \rho \vec{V} dV + \oint_S (\rho \vec{V} \cdot d\vec{S}) \vec{V} = - \oint_S p d\vec{S} + \iiint_V \rho \vec{f} dV + \vec{F}_{viscous}$$

1. Body Forces (e.g. gravity) which act on the fluid inside  $\mathcal{V}$

$$\iiint_V \rho \vec{f} dV$$

2. Pressure and shear surface forces acting on S

$$- \oint_S p d\vec{S} + \vec{F}_{viscous}$$

3. Net flow of momentum out of volume across S

$$\oint_S (\rho \vec{V} \cdot d\vec{S}) \vec{V}$$

4. Time rate of change of momentum due to unsteadiness in volume

$$\frac{\partial}{\partial t} \iiint_V \rho \vec{V} dV$$

**Navier-Stokes Equations:**

$$\frac{\partial}{\partial t} (\rho u) + \vec{\nabla} \cdot (\rho u \vec{V}) = - \frac{\partial p}{\partial x} + \rho f_x + (\mathcal{F}_x)_{viscous}$$

$$\frac{\partial}{\partial t} (\rho v) + \vec{\nabla} \cdot (\rho v \vec{V}) = - \frac{\partial p}{\partial y} + \rho f_y + (\mathcal{F}_y)_{viscous}$$

### Conservation of Energy

$$\frac{\partial}{\partial t} \iiint_V \rho \left( e + \frac{V^2}{2} \right) dV + \oint_S \rho \left( e + \frac{V^2}{2} \right) \vec{V} \cdot d\vec{S} =$$

Net Time Rate of Change of Total Energy Due to Unsteadiness in  $\mathcal{V}$       Net Rate of Flow of Total Energy Out of  $\mathcal{V}$

$$\underbrace{\iiint_V \dot{q} \rho dV}_{\text{Rate of Volumetric Heating}} + \underbrace{\dot{Q}_{viscous}}_{\text{Heat Addition Due to Viscosity}}$$

$$- \underbrace{\oint_S p \vec{V} \cdot d\vec{S}}_{\text{Rate of Pressure Work}} + \underbrace{\oint_S \rho \vec{f} \cdot \vec{V} dV}_{\text{Rate of Work Done by Body Forces}}$$

$$+ \underbrace{\dot{W}_{viscous}}_{\text{Rate of Viscous Work}}$$

$$\frac{\partial}{\partial t} \left( \rho \left( e + \frac{V^2}{2} \right) \right) + \vec{\nabla} \cdot \left( \rho \left( e + \frac{V^2}{2} \right) \vec{V} \right) =$$

$$\rho \dot{q} + \dot{Q}'_{viscous} - \vec{\nabla} \cdot (p \vec{V}) + \rho \vec{f} \cdot \vec{V} + \dot{W}'_{viscous}$$

### Kinematics

$\vec{\nabla} \cdot \vec{V}$ : time rate of change of volume of a fluid element per unit volume  $\rightarrow$  **Dilation**

**Stream Line:** Curve everywhere tangent to the velocity.

$$\frac{v}{u} = \frac{dy}{dx}$$

**Path Line:** Trajectory of a particle released from a point in time.

**Streak Line:** Line connecting all particles that have passed through a given point.

For a steady flow the three lines coincide.

## Substantial Derivative

Time rate of change of density of a given material fluid element as it moves through space and time.

$$\frac{D\rho}{Dt} = \frac{\partial\rho}{\partial t} + \vec{V} \cdot \vec{\nabla}\rho$$

Continuity Equation:  $\frac{D\rho}{Dt} = -\rho\vec{\nabla} \cdot \vec{V}$

Material Acceleration:  $(\frac{Du}{Dt}; \frac{Dv}{Dt}; \frac{Dz}{Dt})$

Navier-Stokes:

$$\rho \frac{Du}{Dt} = -\frac{\partial p}{\partial x} + \rho f_x + (\mathcal{F}_x)_{viscous} \rightarrow \text{applicable to y and z as well.}$$

## Vorticity and Strain

$$\vec{\omega} = \frac{1}{2}\vec{\nabla} \times \vec{V} \rightarrow \text{angular velocity}$$

$$\vec{\xi} = \vec{\nabla} \times \vec{V} \rightarrow \text{Vorticity}$$

$$\epsilon_{xy} = \frac{\partial v}{\partial x} + \frac{\partial u}{\partial y} \rightarrow \text{Rate of Strain in xy plane.}$$

$$\Gamma = -\oint_C \vec{V} \cdot d\vec{s} \rightarrow \text{Circulation}$$

Relation between circulation and vorticity:  $\vec{x}i \cdot \vec{n} = \frac{d\Gamma}{dS}$

## Stream Functions and Velocity Potentials

**Stream Function:** For every incompressible, two-dimensional flow, there exists a scalar stream function such that:  $u = \frac{\partial\psi}{\partial y}$ ,

$$v = -\frac{\partial\psi}{\partial x} \text{ DON'T FORGET +C}$$

**Velocity Potential:** For every irrotational flow, there exists a scalar velocity potential such that:  $\vec{V} = \vec{\nabla}\phi / \rightarrow \frac{\partial\phi}{\partial x} = u, \frac{\partial\phi}{\partial y} = v$

**Euler's Equation:**  $\frac{1}{2}d(V^2) = -\frac{1}{\rho}dp$

If flow is barotropic,  $\rho = \rho(p)$  is a function of pressure only and can integrate the equation. Occurs in incompressible flow, isothermal flow, or isentropic (frictionless) flow.

**Bernoulli's Equation:**  $p + \frac{1}{2}\rho V^2 = \text{constant}$  - along a stream-line for steady, inviscid, incompressible flow with no body forces.

## Flow in a Duct

$\rho_1 A_1 V_1 = \rho_2 A_2 V_2 \rightarrow \text{Steady, inviscid flow in a duct with no body forces. For incompressible flow remove rho.}$