



# Thermoelectric System Modelling and Design

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## Committee Members

Dr. Yanliang Zhang (Chair)  
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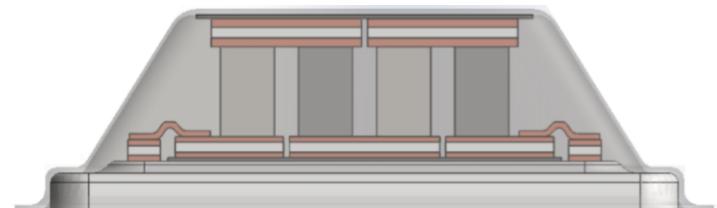
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# Introduction

# Why Thermoelectrics?

- Solid-state heat to electricity conversion or thermoelectric cooling with same device
- Environmentally friendly
- Easy implementation with other systems
- Compact design



Thermoelectric Module

# Thermoelectric Effect

- Seebeck Effect

$$-\alpha = -\frac{\Delta V}{\Delta T}$$

- Peltier Effect

$$-\pi = \frac{I}{q}$$

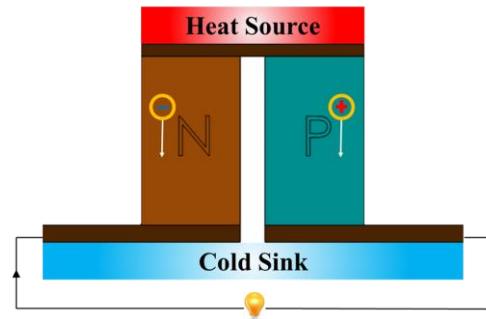
V: Voltage

T: Temperature

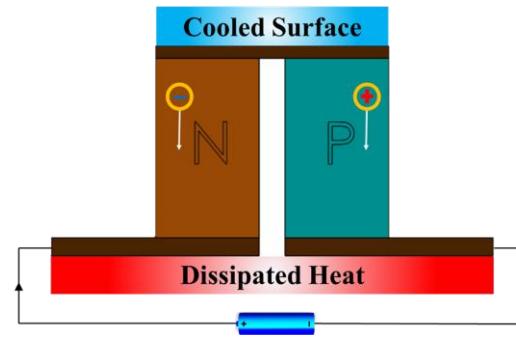
I: Electric Current

q: Heat Dissipated

Seebeck Effect



Peltier Effect



# Thermoelectric Figure of Merit (FOM)

$$Z = \frac{\sigma \alpha^2}{\kappa}$$

$\sigma$  : Electrical Conductivity  
 $\kappa$  : Thermal Conductivity  
 $\alpha$  : Seebeck Coefficient  
 $T$  : Absolute Temperature

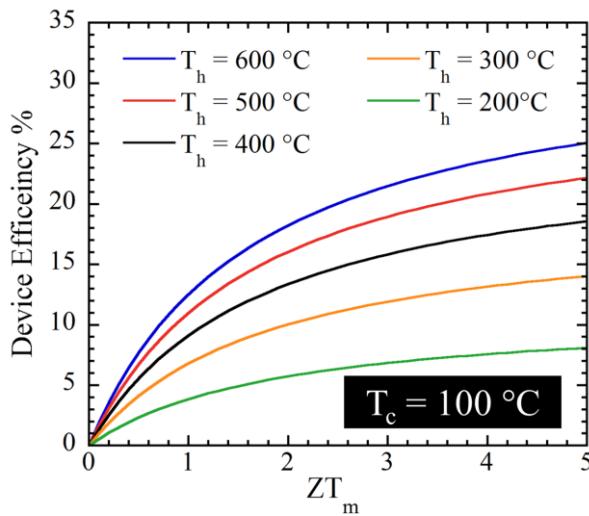
$$ZT = \frac{\sigma \alpha^2 T}{\kappa}$$

Dimensionless Figure of  
Merit

# ZT – Thermoelectric Generator (TEG) Efficiency

Max Efficiency Condition

Max Power Condition



$$\eta_{\max(E)} = \frac{\Delta T}{T_h} \frac{\sqrt{1 + Z \cdot T_m} - 1}{\sqrt{1 + Z \cdot T_m} + \frac{T_c}{T_h}}$$

$$\eta_{\max(P)} = \frac{\Delta T}{T_h} \frac{ZT_h}{ZT_m + ZT_h + 4}$$

**ΔT** : Temperature Difference Between Hot and Cold Side

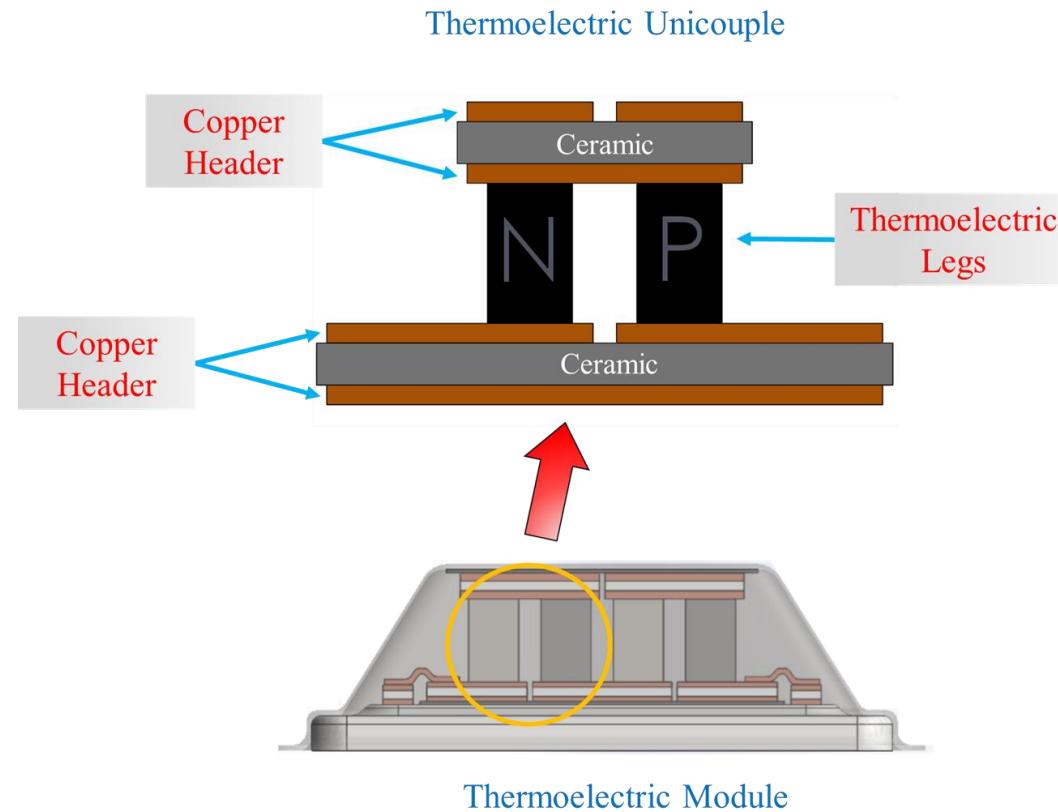
**Z** : Material FOM

**T<sub>m</sub>** : Average of Hot and Cold Side Temperatures

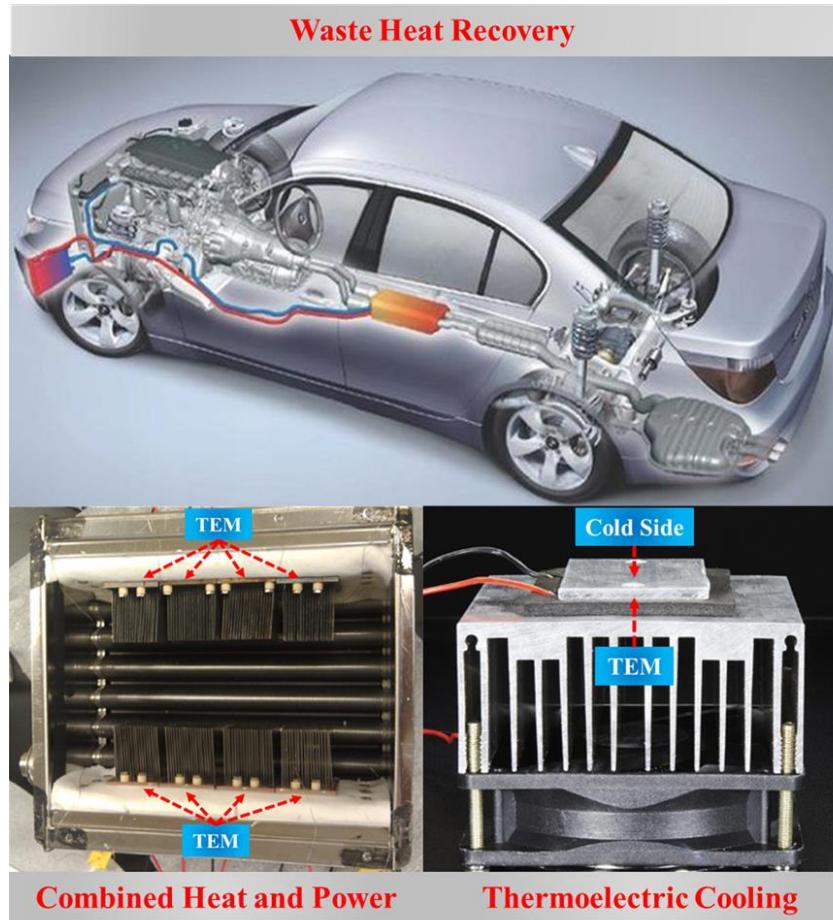
**T<sub>h</sub>** : Hot Side Temperature

**T<sub>c</sub>** : Cold Side Temperature

# Thermoelectric Module Components



# Thermoelectric Applications

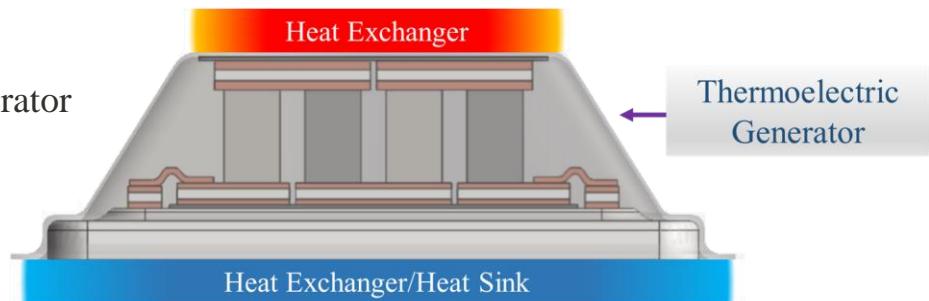


[1]G. Snyder, "Small Thermoelectric Generators", *The Electrochemical Society Interface*, pp. 54-56, 2008.

[2]Y. L. Zhang, X. W. Wang, M. Cleary, L. Schoensee, N. Kempf, and J. Richardson, "High-performance nanostructured thermoelectric generators for micro combined heat and power systems," *Applied Thermal Engineering*, vol. 96, pp. 83-87, Mar 5 2016.

# Organization of This Work

1. Temperature Dependent Finite Element Model for a Thermoelectric Generator (TEG)
  - I. Model Introduction
  - II. Model Validation
  - III. Improvements to a Thermoelectric Generator
    - a) Study of Ceramic Material
    - b) Segmented TEG
2. TEG – Heat Exchanger Model
  - I. Model Introduction
  - II. Model Validation
3. TEGs combined with Natural Convection Heat Sink
  - I. Heat Sink Model Introduction
  - II. Applications
    - a) Wireless Sensor Node powered by a TEG
    - b) Recovering Waste Heat from the Human Body
4. TEGs combined with Natural Convection Microwire Heat Sinks
  1. Microwire Heat Sink Model
  2. Recovering Waste Heat from the Human Body



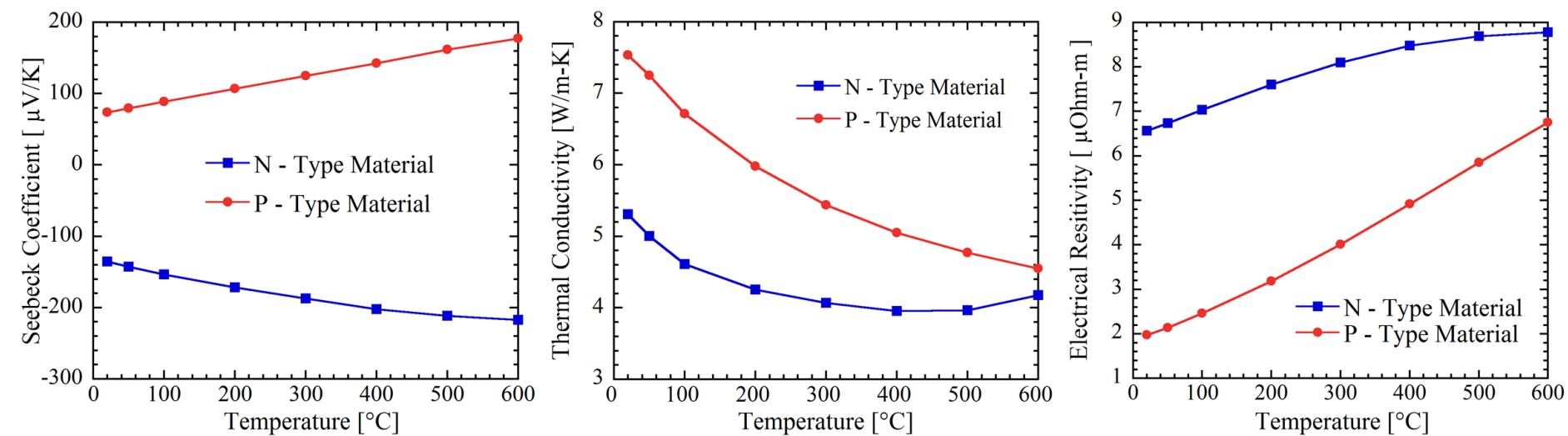


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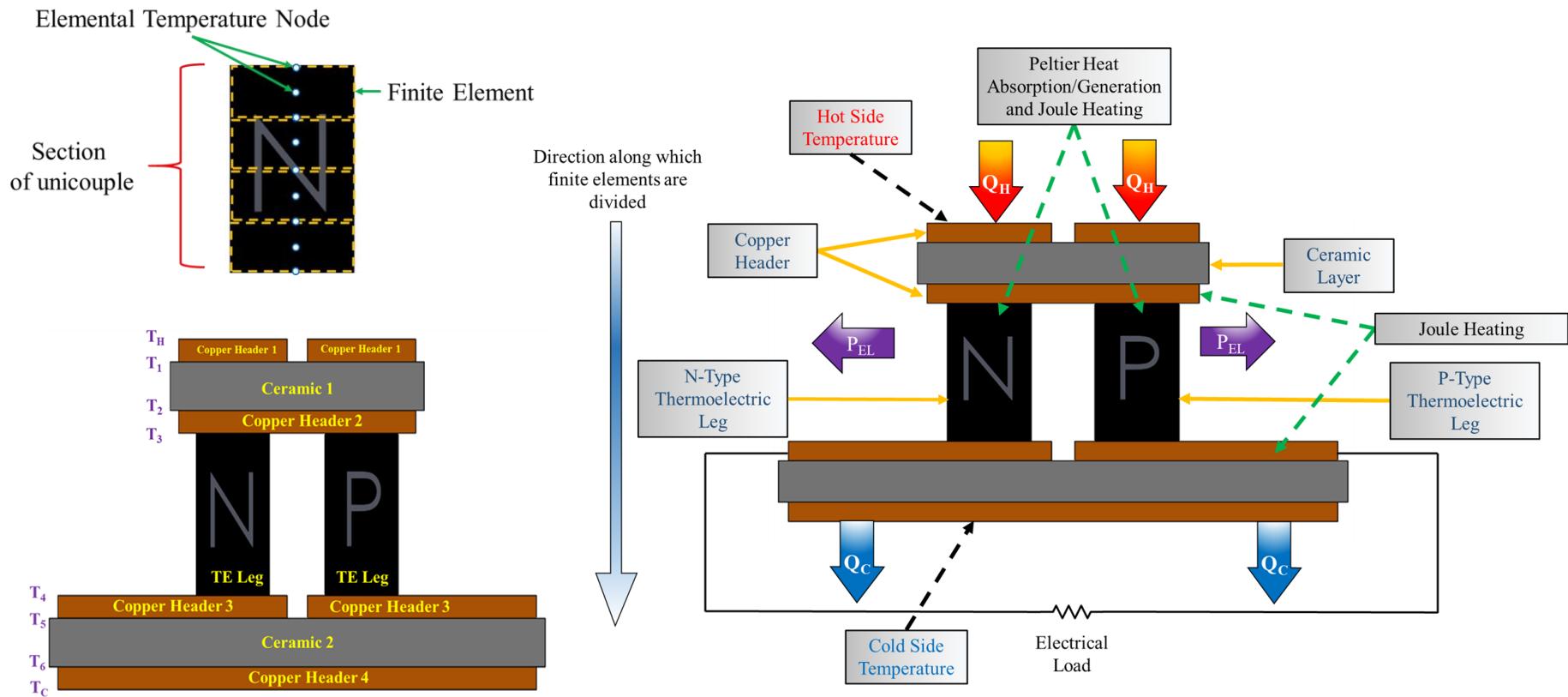
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# Why a Temperature Dependent Model is Needed?



High Temperature Thermoelectric Material : Half – Heusler Alloy

# Model Overview





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# Thermoelectric Power Generation

**Heat Flow into Element**

$$Q_{h,p,n} = \text{abs}(\alpha_{p,n}(T)) \cdot (T_{no,p,n}) \cdot I + K_{p,n}(T_{no,p,n} - T_{no+2,p,n}) - \frac{1}{2}I^2 \cdot R_{el,p,n}$$

**Heat Flow leaving Element**

$$Q_{c,p,n} = \text{abs}(\alpha_{p,n}(T)) \cdot (T_{no+2,p,n}) \cdot I + K_{p,n}(T_{no,p,n} - T_{no+2,p,n}) + \frac{1}{2}I^2 \cdot R_{el,p,n}$$

**Power generated**

$$P_{p,n} = Q_{h,p,n} - Q_{c,p,n}$$

**Thermal Conductance**

$$K_{p,n} = \frac{\kappa_{p,n}(T) \cdot A_{p,n}}{l_{p,n}}$$

**Electrical Resistance**

$$R_{el,p,n} = \frac{\rho_{p,n}(T) \cdot l_{p,n}}{A_{p,n}}$$

**Open Circuit Voltage**

$$V_{oc} = \sum_{i=1}^{N} (\alpha_p - \alpha_n)(T_{no} - T_{no+2})$$

**Electric Current**

$$I = \frac{V_{oc}}{R_{el,TEC} + R_{el,L}}$$

 **$\alpha$**  : Seebeck Coefficient **$\kappa$**  : Thermal Conductivity **$\rho$**  : Electrical Resistivity**A** : Element Area**I** : Element length **$R_{el,L}$**  : Load Resistance**T** : Temperature**no** : Node**p** : P - Leg**n** : N - Leg**N** : Number of elements **$R_{el,TEC}$**  : Electrical Resistance  
of Unicouple

# Temperature Profile Along Unicouple

Temperature Profile

$$T = K^{-1}F$$

Elemental Stiffness Matrix

$$K_e = \int_l [B]^T [D] [B] A_e dx$$

Elemental Stiffness Matrix  
Simplified for a quadratic  
element

$$K_e = \frac{A_e \kappa_e(T)}{l_e} \begin{bmatrix} 14 & -16 & 2 \\ -16 & 32 & -16 \\ 2 & -16 & 14 \end{bmatrix}$$

Elemental Loading Vector

$$F_e = \int_l G[N]^T A dx$$

Elemental loading vector  
simplified for a quadratic  
element

$$F_e = \frac{G_e A_e l_e}{6} \begin{bmatrix} 1 \\ 4 \\ 1 \end{bmatrix}$$

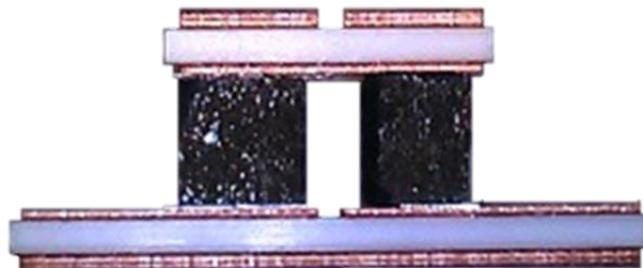
T : Temperature Profile  
K : Global Stiffness Matrix  
F : Global Loading Vector  
B : Strain Displacement Matrix  
D : Thermal Conductivity Terms  
N : Shape Function  
A<sub>e</sub> : Elemental Area  
l<sub>e</sub> : Elemental Length  
κ<sub>e</sub> : Element Thermal Conductivity  
G<sub>e</sub> : Volumetric Energy Generation

# Model Assumptions

1. Temperature variation is assumed 1-D.
2. Constant energy generation or absorption throughout element
3. Convection and radiation from external surfaces ignored
4. The complete top and bottom surfaces are assumed to have a constant temperature
5. Material properties within an element is constant
6. Module power obtained by the product of power output per unicouple and number of unicouples. Similarly, for device voltage.



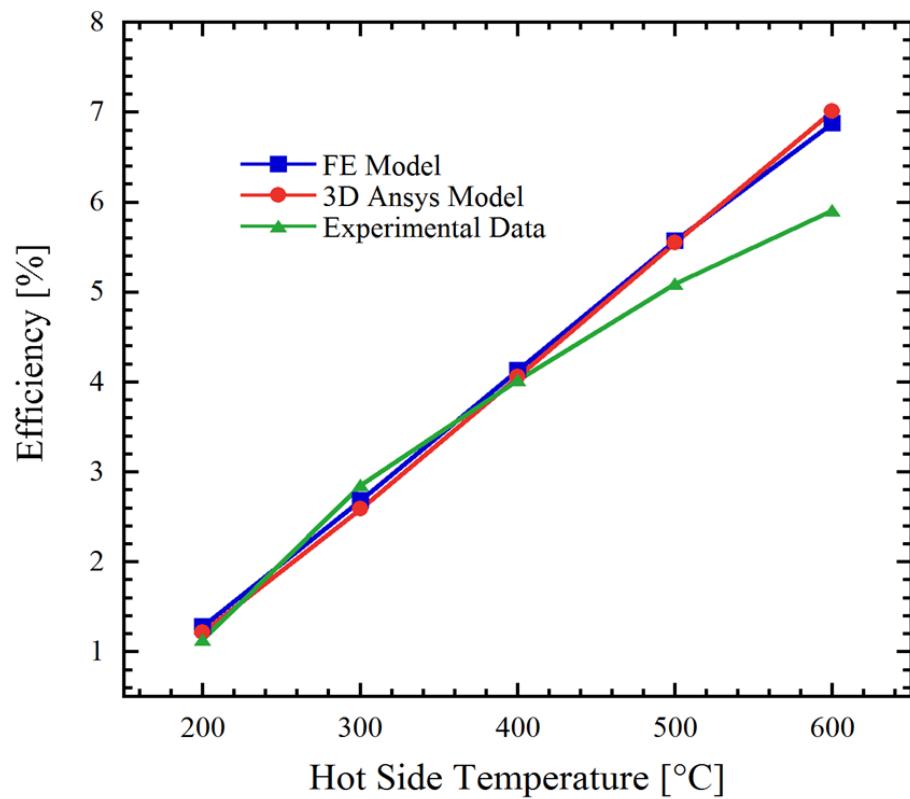
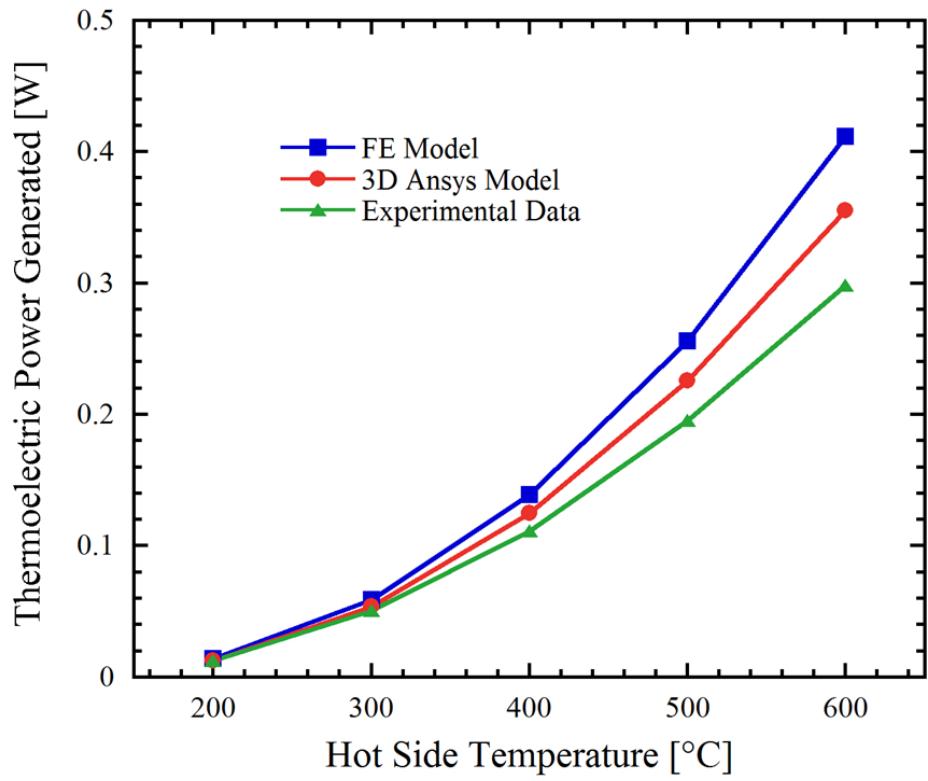
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# Geometric Input

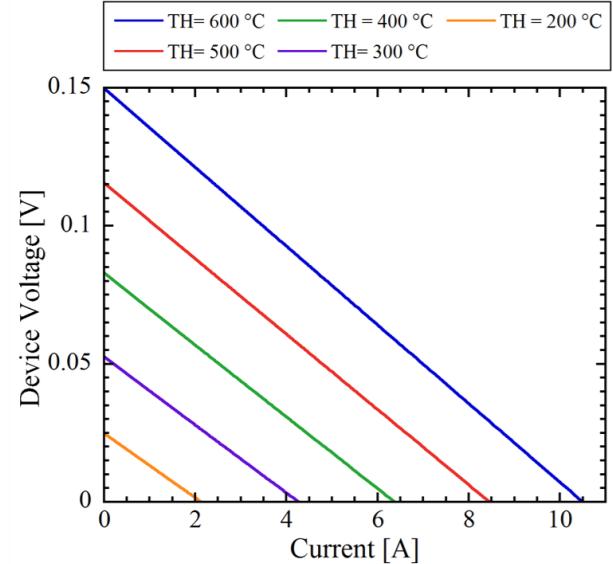
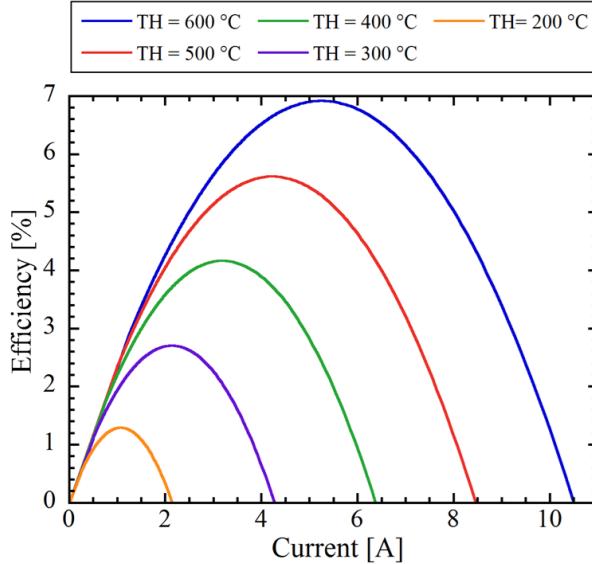
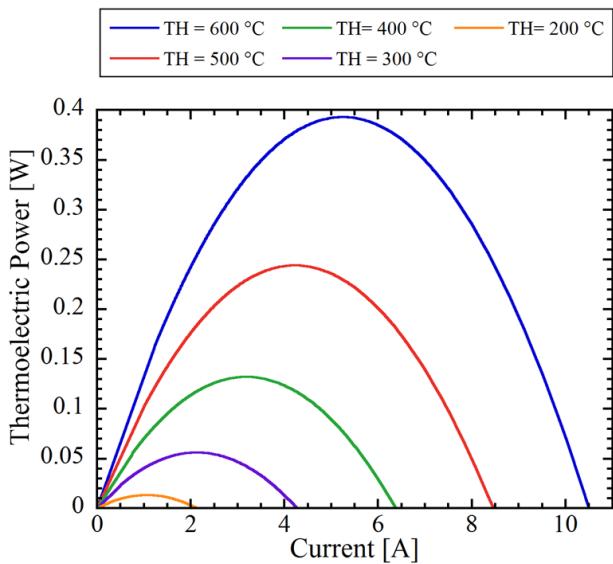
Component	Thickness/Height [mm]	Area [mm x mm]
Copper Header 1	0.203	[1.93 x 1.96]*2
Ceramic 1	0.635	2.26 x 4.51
Copper Header 2	0.203	1.96 x 4.21
P-Leg	2.400	1.50 x 1.50
N-Leg	2.400	1.50 x 1.50
Copper Header 3	0.203	[1.96 x 4.07]*2
Ceramic 2	0.635	2.26 x 8.81
Copper Header 4	0.203	[1.96 x 8.50]*2

# Half-Heusler Alloy Unicouple TEG Power and Efficiency



$$T_c = 100 \text{ } ^\circ\text{C}$$

# Half-Heusler Alloy Unicouple Power-Current, Efficiency-Current and Voltage-Current Curves



$$T_c = 100 \text{ } ^\circ\text{C}$$

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### III. Improvements to a Thermoelectric Generator

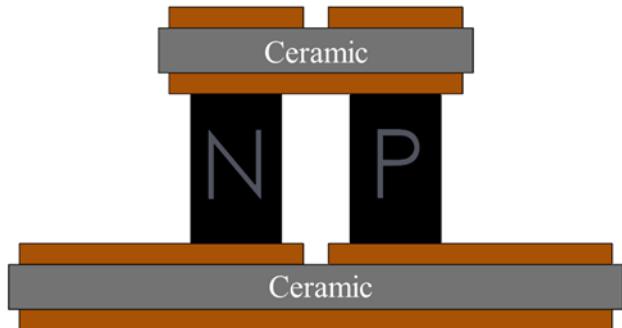
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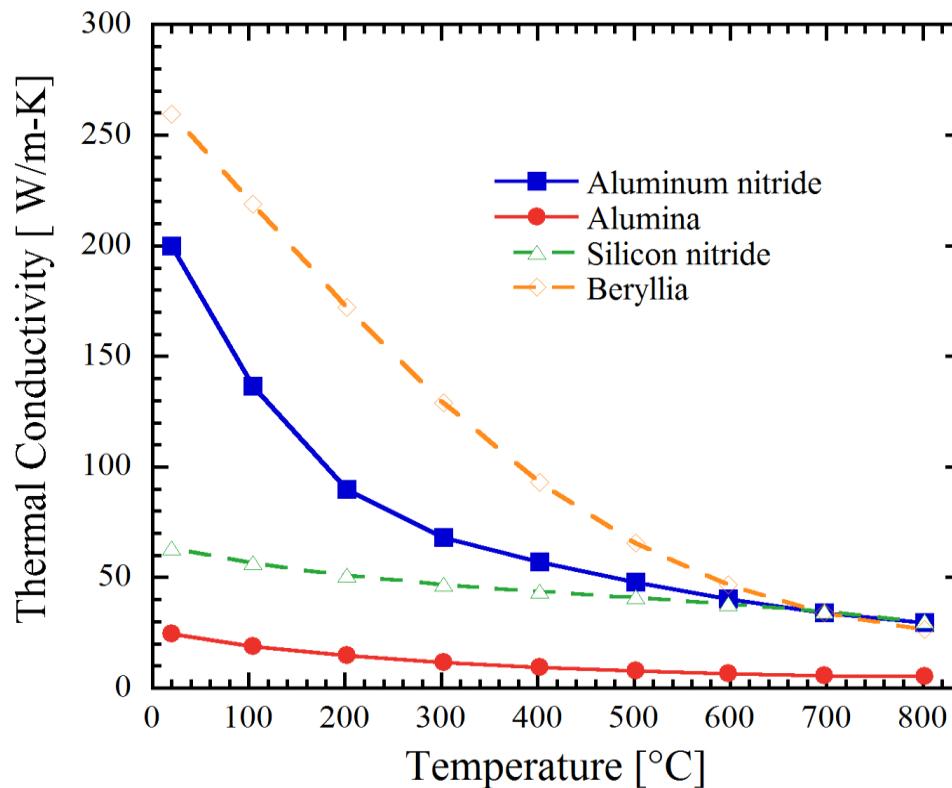
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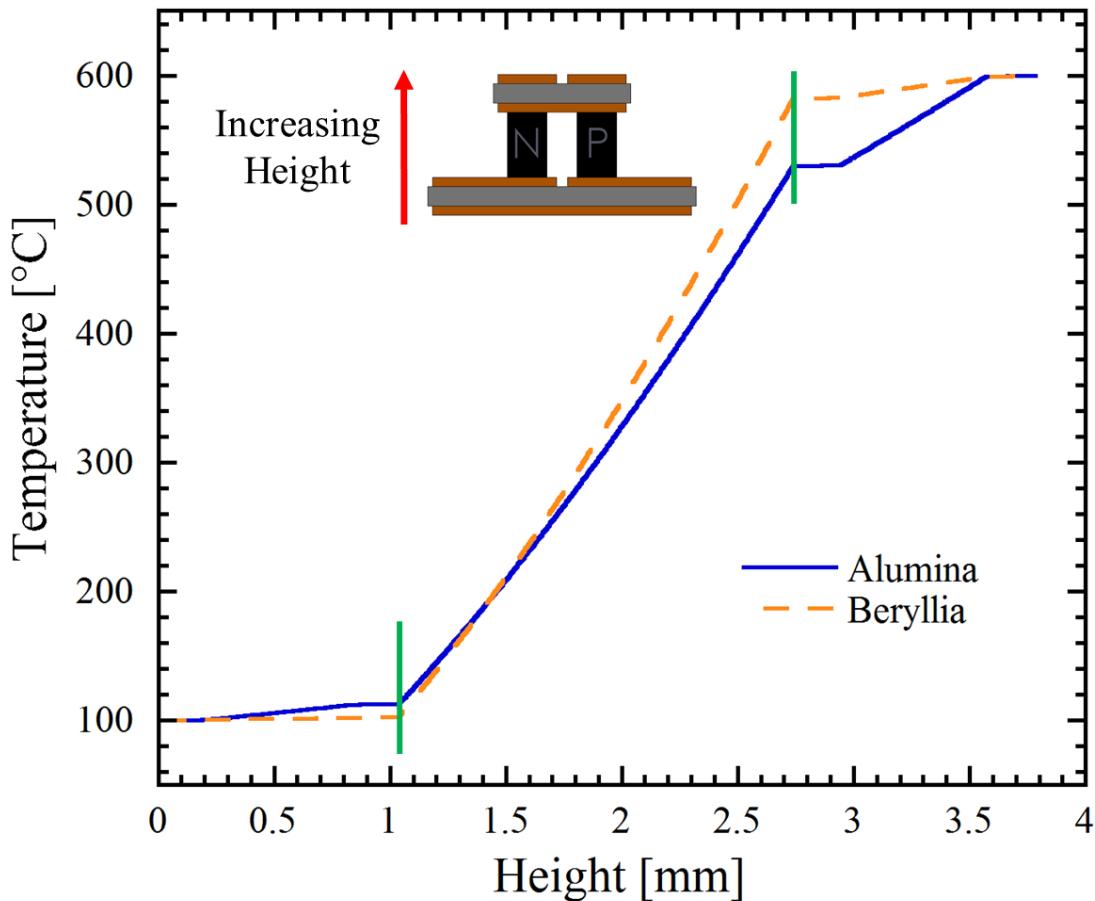
- 1. Microwire Heat Sink Model
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## Thermal Conductivity of Various Ceramic Materials with Varied Temperature



[4] D. de Faoite, D. J. Browne, F. R. Chang-Diaz, and K. T. Stanton, "A review of the processing, composition, and temperature-dependent mechanical and thermal properties of dielectric technical ceramics," *Journal of Materials Science*, vol. 47, pp. 4211-4235, May 2012.

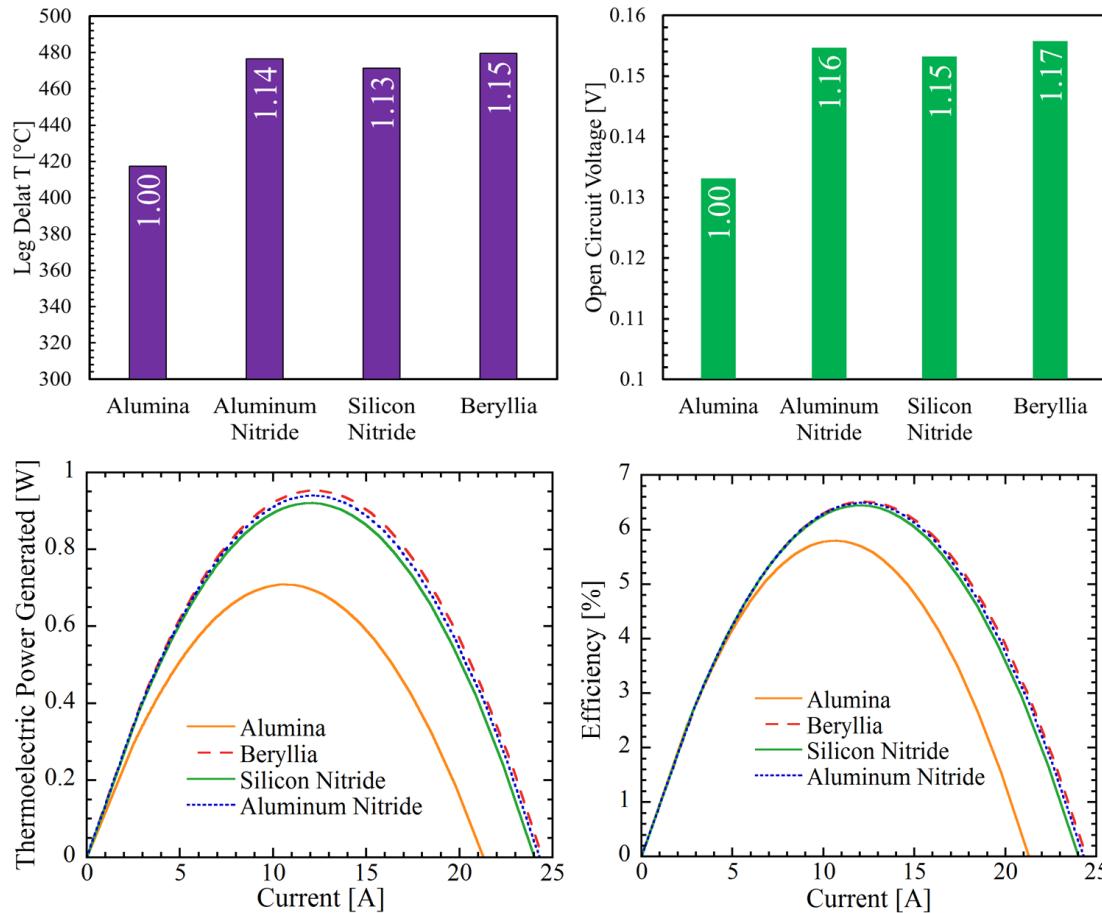
# Temperature Profile of Unicouple with Two Different Ceramics



Component	Thickness/Height [mm]	Area [mm x mm]
Copper Header 1	0.203	[1.93 x 1.96]*2
Ceramic 1	0.635	2.26 x 4.51
Copper Header 2	0.203	1.96 x 4.21
P-Leg	1.700	2.00 x 2.00
N-Leg	1.700	2.00 x 2.00
Copper Header 3	0.203	[1.96 x 4.07]*2
Ceramic 2	0.635	2.26 x 8.81
Copper Header 4	0.203	[1.96 x 8.50]*2

Updated Unicouple  
Dimensions

# Performance Comparison with Different Ceramic Materials





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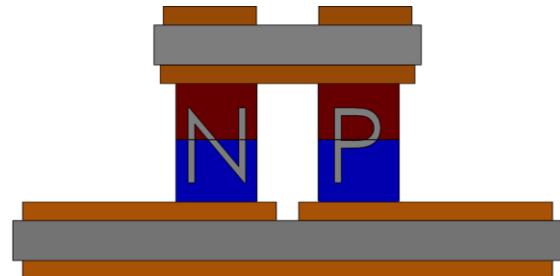
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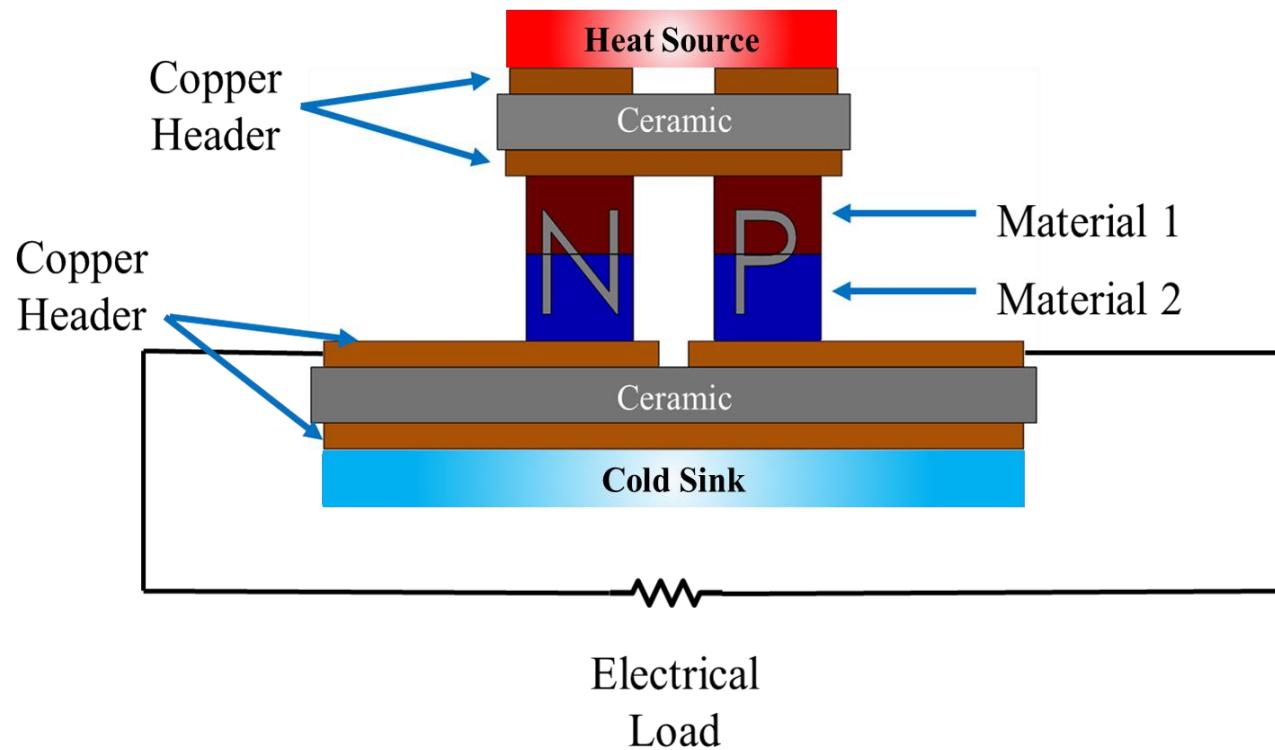
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# Segmented TEGs



# Thermoelectric Compatibility

Optimum relative current density

$$u = \frac{J}{\kappa \nabla T}$$

J : Current Density

$\kappa$  : Thermal Conductivity

$\nabla T$  : Temperature Gradient

$zT$  : Dimensionless FOM

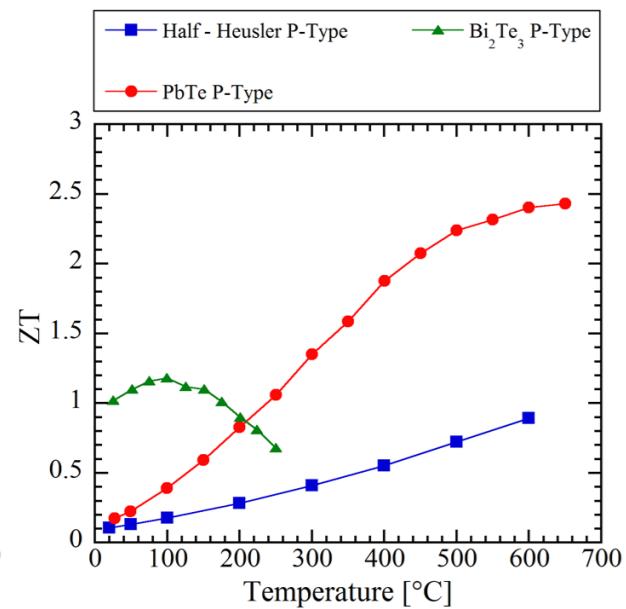
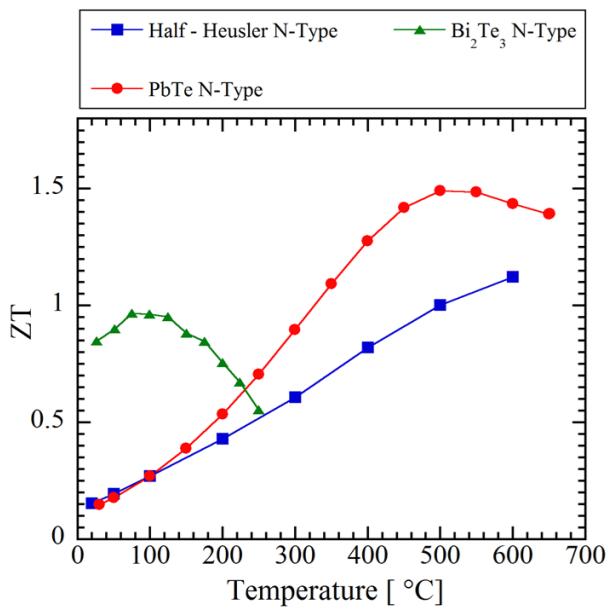
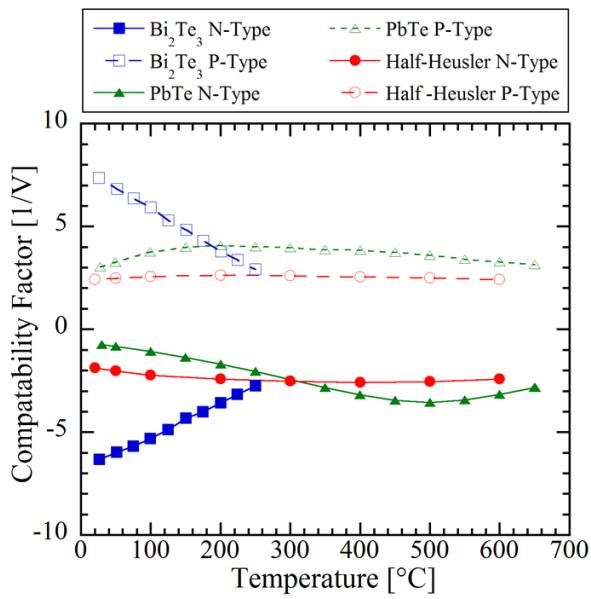
$\alpha$  : Seebeck Coefficient

T : Absolute Temperature

Compatibility Factor

$$s = \frac{\sqrt{1 + zT} - 1}{\alpha T}$$

# Material Compatibility and ZT



# Leg Height Ratios

P – Leg Ratio

$$\frac{l_{p1}}{l_{p2}} = \frac{\int_{T_{\text{int}}}^{T_h} \kappa_{p1}(T) dT}{\int_{T_c}^{T_{\text{int}}} \kappa_{p2}(T) dT}$$

N – Leg Ratio

$$\frac{l_{n1}}{l_{n2}} = \frac{\int_{T_{\text{int}}}^{T_h} \kappa_{n1}(T) dT}{\int_{T_c}^{T_{\text{int}}} \kappa_{n2}(T) dT}$$

**I** : Leg Height

**p** : p-leg

**n** : n-leg

**T<sub>h</sub>** : Temperature at Intercept of Top Copper Header and Top Material

**T<sub>int</sub>** : Temperature at Interface Between the Two Materials

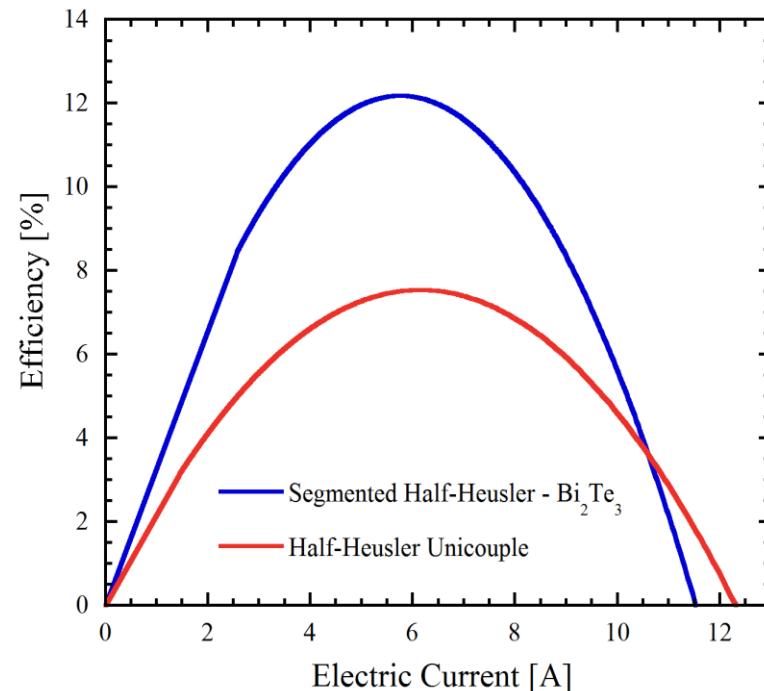
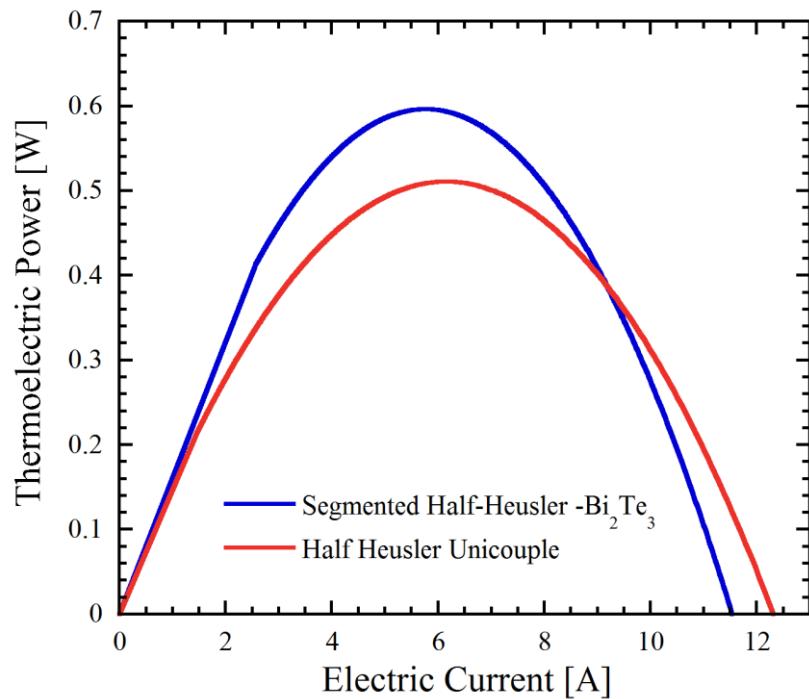
**T<sub>c</sub>** : Temperature at Interface Between Bottom Copper Header and Bottom Material

**κ** : Thermal Conductivity

Segment	Unicouple A	Unicouple B
Half-Heusler alloy segment	2.106 mm	-
PbTe segment	-	1.618 mm
Bi <sub>2</sub> Te <sub>3</sub> segment	0.294 mm	0.782 mm
Total Height	2.4 mm	2.4 mm

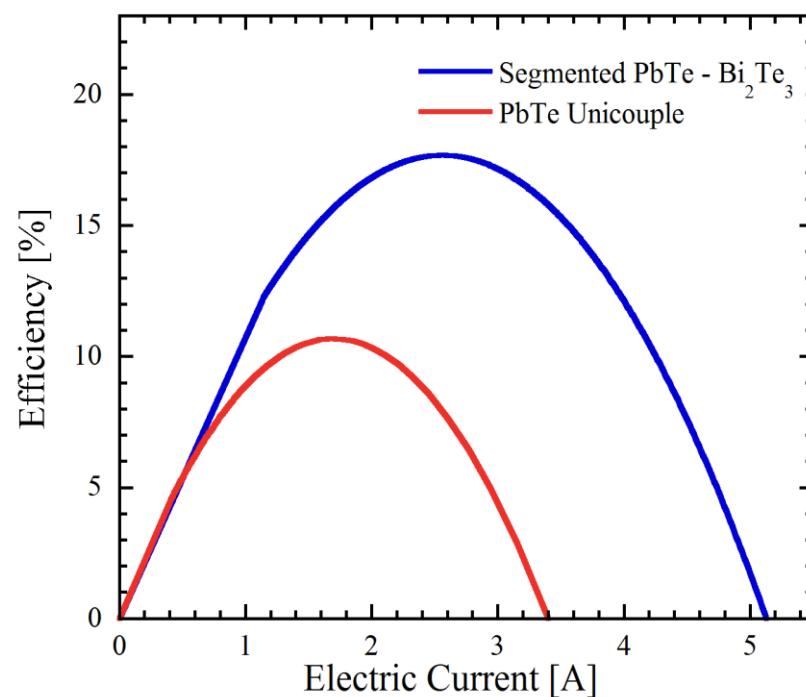
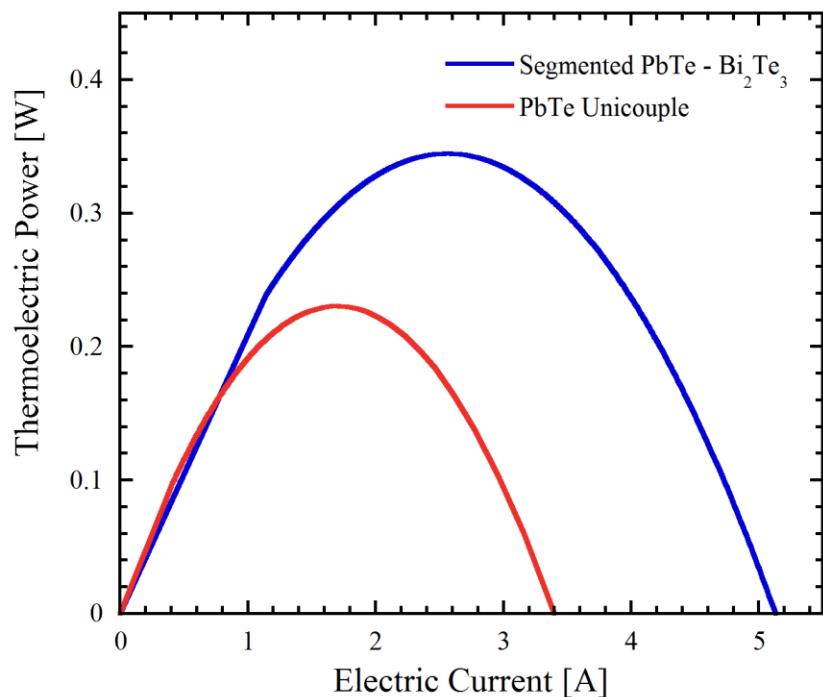
## Leg Dimensions

# Segmented HH – $\text{Bi}_2\text{Te}_3$ Unicouple



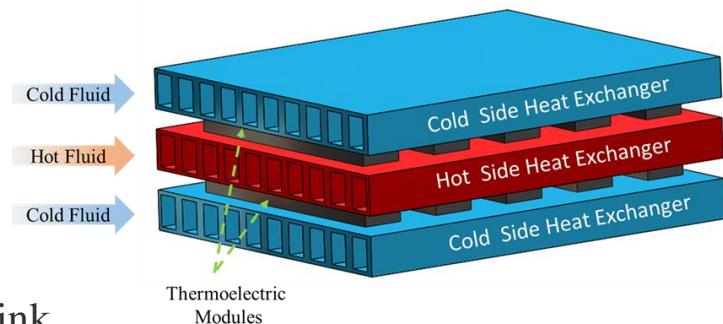
Delta T = 580 °C

# Segmented PbTe – $\text{Bi}_2\text{Te}_3$ Unicouple

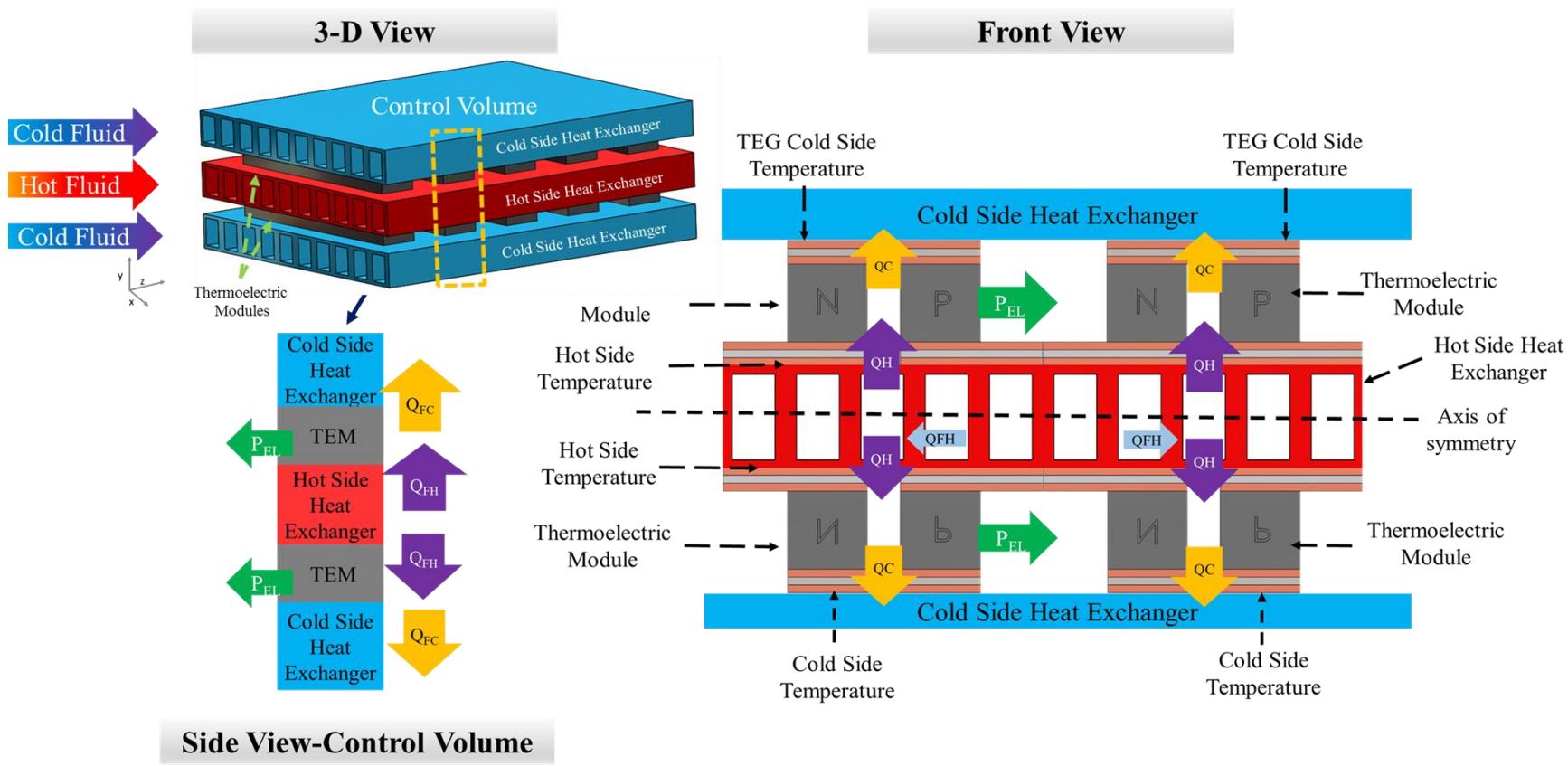


Delta T = 580 °C

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# Model Overview



# Model Assumptions

1. Heat exchanger divided into number of individual channels
  - I. Mass flowrate is identical in each channel
  - II. Heat transfer coefficient constant for each section of channel
2. Lateral variations in heat exchanger ignored
3. Assumes fully developed flow enters heat exchanger
4. Constant base temperature in each control volume
5. Lateral sides are assumed perfectly insulated



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# Primary Equations

Heat transferred  
through HX in  
Control Volume

$$Q_f = M \cdot \tanh\left(m \cdot \frac{f_h}{2}\right) \cdot (N_f - 1) + A_{uf} \cdot (h) \cdot (T_b - T_f)$$

Fin Parameter

$$M = \sqrt{h \cdot P \cdot k \cdot A_c} \cdot (T_b - T_f)$$

Fin Parameter

$$m = \sqrt{\frac{h \cdot P}{k \cdot A_c}}$$

Fluid Temperature  
in control volume

$$T_{f,out} = T_{f,in} - \frac{Q_f}{\dot{m} \cdot C_p}$$

- $f_h$  : Fin Height  
 $N_f$  : Number of Fins  
 $h$ : Convection Coefficient  
 $T_b$  : Base Temperature  
 $T_f$  : Fluid Temperature  
 $A_{uf}$  : Unfinned Area  
 $k$  : Fin Thermal Conductivity  
 $P$  : Fin Perimeter  
 $A_c$  : Fin Cross-sectional Area  
 $T_{f,in,out}$  : Inlet and Outlet Temperature of the Fluid in Control Volume  
 $C_p$  : Specific Heat Capacity of Fluid

# Channel Convection Coefficient - Duct

Reynolds Number

$$Re_{dh} = \frac{v_{ch} \cdot d_h}{v_f}$$

$v_{ch}$  : Channel Velocity

$v_f$  : Fluid Kinematic Viscosity

$A$  : Channel Cross Sectional Area

$P$ : Wetting Perimeter

$Pr$  : Prandtl Number

$k_f$  : Fluid Thermal Conductivity

Hydraulic Diameter

$$d_h = \frac{4 \cdot A}{P}$$

$$\alpha = \frac{s}{f_h}$$

Spacing Ratio

Nusselt Number

$$Nu = 0.026 \cdot Re_{dh}^{0.8} Pr^{0.3}$$

$$Re_{dh} \geq 2500 \quad (T_s > T_f)$$

$$Nu = 0.024 \cdot Re_{dh}^{0.8} Pr^{0.4}$$

$$Re_{dh} \geq 2500 \quad (T_f > T_s)$$

$$Nu = 7.541 \cdot (1 - 2.61\alpha + 4.970\alpha^2 - 5.199\alpha^3 + 2.702\alpha^4 - 0.548\alpha^5) \quad Re_{dh} \leq 2500$$

Convection Coefficient

$$h = \frac{Nu \cdot k_f}{d_h}$$

# Channel Convection Coefficient – Compact HX

Colburn Factor

$$j = 0.483 \cdot \left(\frac{hxl}{d_h}\right)^{-0.162} \cdot \alpha^{-0.184} \cdot Re_{dh}^{-0.536} \quad Re \leq 1000$$

$$j = 0.242 \cdot \left(\frac{hxl}{d_h}\right)^{-0.322} \cdot \left(\frac{t_f}{d_h}\right)^{-0.089} \cdot Re_{dh}^{-0.368} \quad Re > 1000$$

Convection Coefficient

$$h = j \cdot Re_{dh} \cdot Pr^{1/3} \cdot \frac{k_f}{d_h}$$

$Re_{dh}$  : Reynolds Number  
 $\alpha$  : Spacing Ratio

$hxl$  : Heat Exchanger Length

$d_h$  : Hydraulic Diameter

$t_f$  : Fin Thickness

$Pr$  : Prandtl Number

$k_f$  : Fluid Thermal Conductivity

[8] A. R. Wieting, "Empirical Correlations for Heat-Transfer and Flow Friction Characteristics of Rectangular Offset-Fin Plate-Fin Heat-Exchangers," *Journal of Heat Transfer-Transactions of the Asme*, vol. 97, pp. 488-490, 1975.

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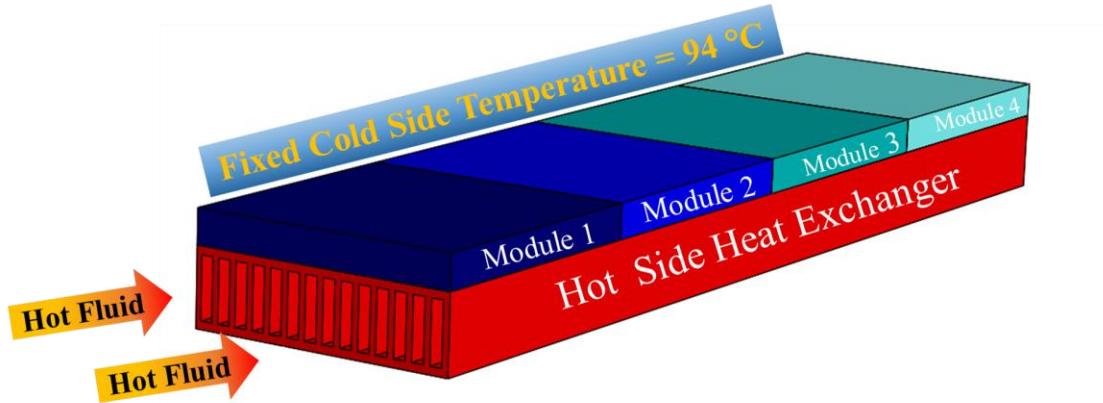


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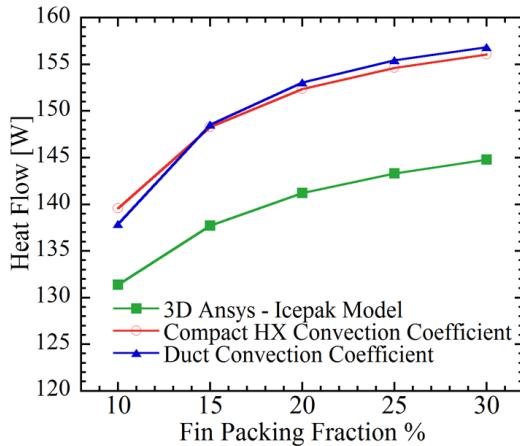
# Model Input

Input	Value
Exhaust Inlet Temperature	558 °C
Hot Side Fluid	Exhaust gas (Air)
Number of Modules	4
Module Size	40mm x 40 mm x 4.9 mm
TEM Cold Side Temperature	94 °C
Heat Exchanger Width	40 mm
Heat Exchanger Length	160 mm
Heat Exchanger Height	20 mm
Heat Exchanger Material	Nickel

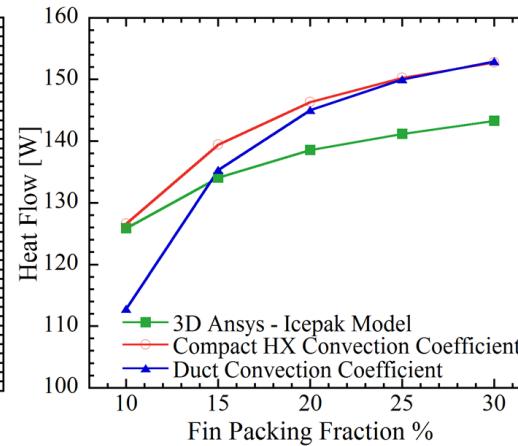


# Average Heat Flow Through TEG Comparison

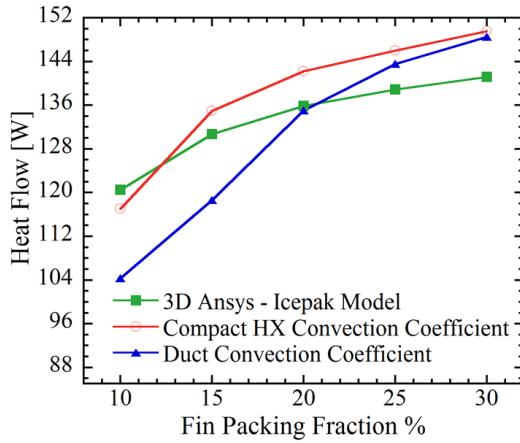
Fin Thickness  
of 0.1mm



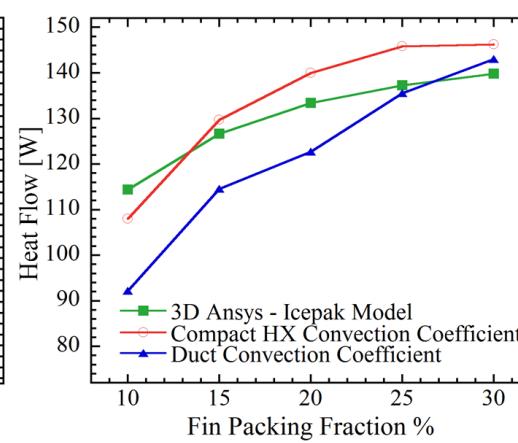
Fin Thickness  
of 0.2mm



Fin Thickness  
of 0.3mm



Fin Thickness  
of 0.4mm





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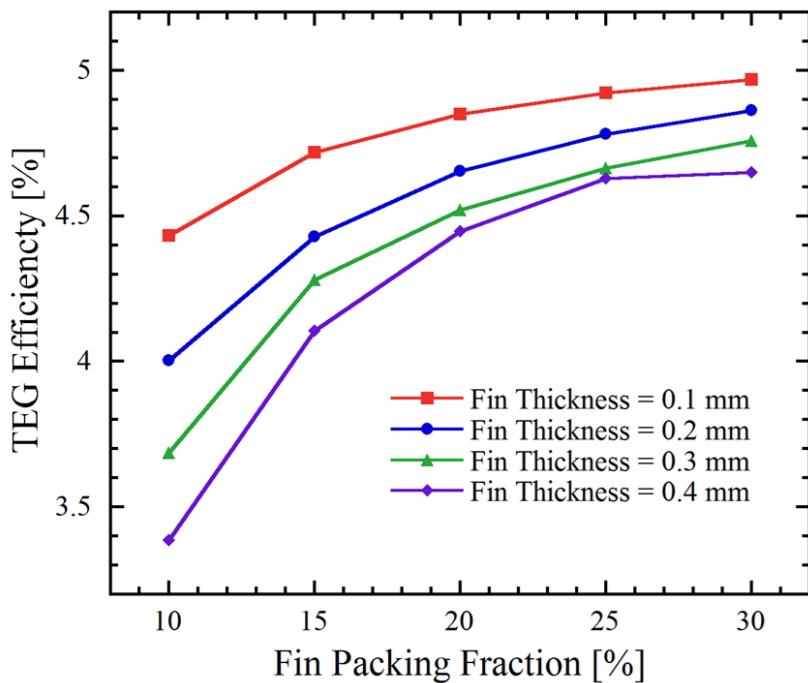
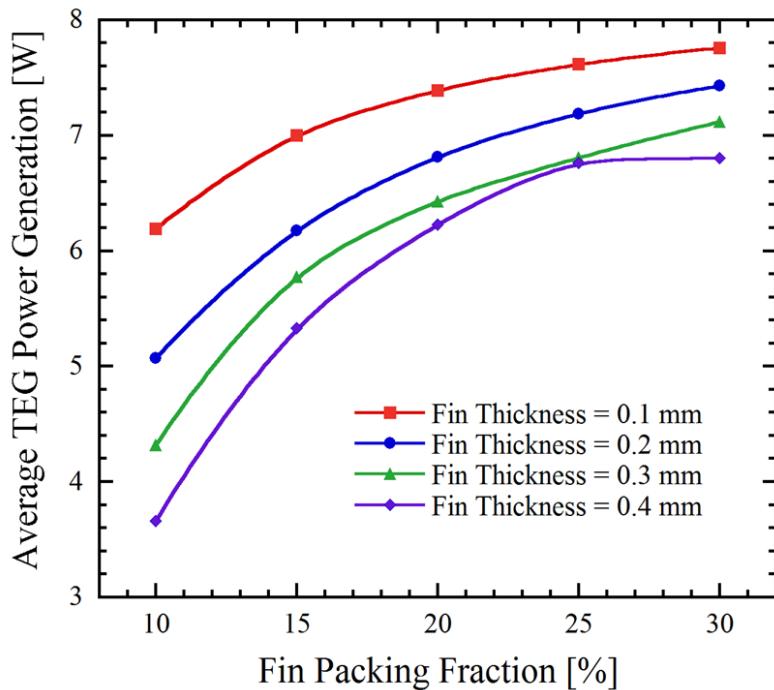
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# Average Percent Comparison

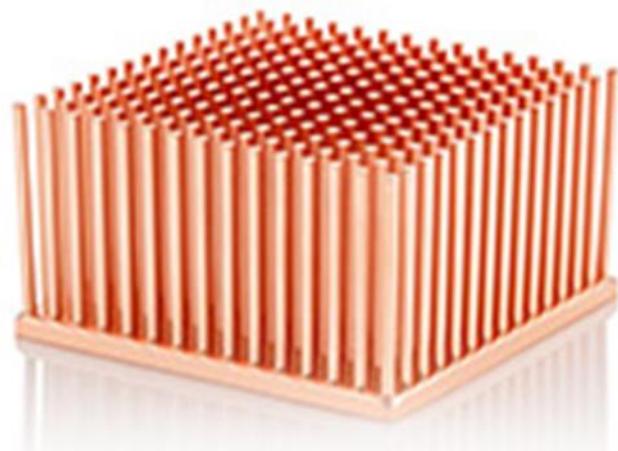
Fin Thickness	Duct Convection Coefficient Model	Compact Heat-Exchanger Convection Coefficient Model
0.1 mm	7.60 %	7.50 %
0.2 mm	5.79 %	4.63 %
0.3 mm	6.37 %	4.36 %
0.4 mm	8.13 %	4.76 %

- Compact HX convection coefficient more accurate
  - Geometry of heat exchanger used
- Produces less erratic results

# TEG Power and Efficiency



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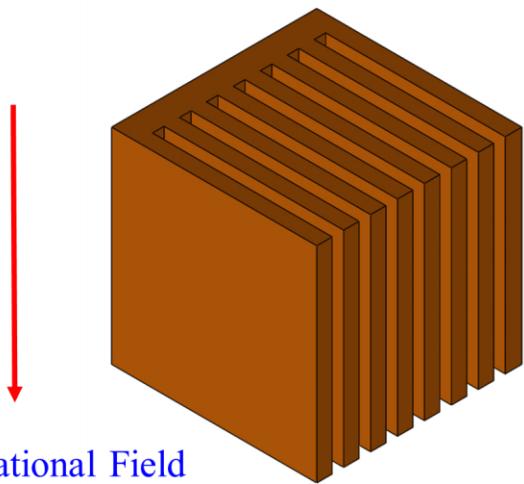


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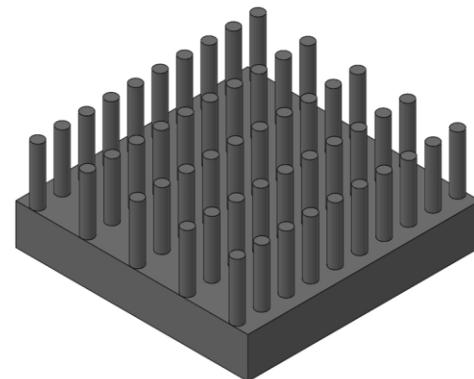
# Heat Sinks Examined

Vertical Flat Plate  
Heat Sink



Gravitational Field

Horizontal Base  
Pin Fin Heat Sink



Gravitational Field

# Heat Sink Model

Heat Flow from  
Heat Sink

$$Q_{HS} = n_{fin} \cdot q_{fin} + h_{base} \cdot A_{uf} \cdot (T_b - T_{amb})$$

Heat Flow from  
Fin

$$q_{fin} = M \cdot \tan h(m \cdot H)$$

Fin Parameter

$$M = \sqrt{h \cdot P \cdot k \cdot A_c} \cdot (T_b - T_{amb})$$

Fin Parameter

$$m = \sqrt{(h \cdot P) / (k \cdot A_c)}$$

**$n_{fin}$**  : Number of Fins  
 **$h_{base}$**  : Base Convection Coefficient  
 **$T_b$**  : Base Temperature  
 **$T_{amb}$**  : Fluid Ambient Temperature  
 **$A_{uf}$**  : Unfinned Area  
 **$H$**  : Fin Height  
 **$k$**  : Fin Thermal Conductivity  
 **$P$**  : Fin Perimeter  
 **$A_c$**  : Fin Cross-sectional Area  
 **$h$**  : Fin Convection Coefficient

# Vertical Flat Plate Heat Sink Convection Coefficient

Base Convection  
Coefficient

$$h_{\text{base}} = 0.59 \cdot Ra_L^{1/4} \cdot k_f / L$$

Rayleigh Number

$$Ra_L = g \cdot \beta \cdot \theta_b \cdot Pr \cdot L^3 / v^2$$

Fin Convection  
Coefficient

$$h_{\text{fin}} = \frac{k_f}{s} \cdot \left( \frac{576}{(\eta_{\text{fin}} \cdot El)^2} + \frac{2.873}{(\eta_{\text{fin}} \cdot El)^{\frac{1}{2}}} \right)^{1/2}$$

Elenbaas Number

$$El = (g \cdot \beta \cdot \theta_b \cdot Pr \cdot s^4) / Lv^2$$

L : Heat Sink Length Parallel to Gravity

**d<sub>h</sub>** : Hydraulic Diameter

t<sub>f</sub> : Fin Thickness

Pr : Prandtl Number

k<sub>f</sub> : Fluid Thermal Conductivity

g : Gravity

β : Coefficient of Thermal Expansion

θ<sub>b</sub> : Temperature Difference Between Base and Ambient

v : Kinematic Viscosity

s : Fin Spacing

η<sub>fin</sub> : Fin Efficiency

# Horizontal Base Vertical Square Pins

**Fin Spacing Dependent  
Nusselt Number**

$$Nu_s = 0.0285 \left\{ 1 - \exp \left( -\frac{H}{W} \right) \right\} \dots$$

$$\dots \left\{ 1 + 1.50 \exp \left( -0.07 \frac{L}{H} \right) \right\} Ra_s^{1/2} \left\{ 1 - \exp \left[ -\frac{7000}{Ra_s} \right] \right\}^{1/3}$$

**Fin Spacing Dependent  
Rayleigh Number**

$$Ra_s = \frac{g \beta \theta_b S^3 Pr}{v^2}$$

**Fin Spacing**

$$S = P - W$$

**Mean Convection  
Coefficient**

$$h_c = \frac{k_f \cdot Nu_s}{S}$$

**H** : Pin Height

**W** : Pin Width

**L** : Heat Sink Length

**Pr** : Prandtl Number

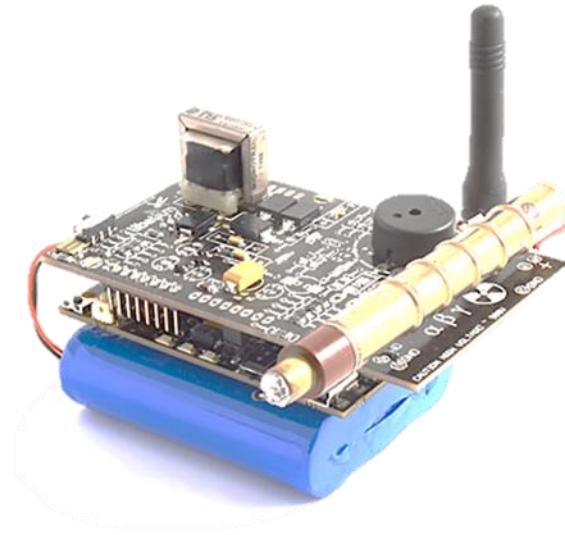
**g** : Gravity

**β** : Coefficient of Thermal Expansion

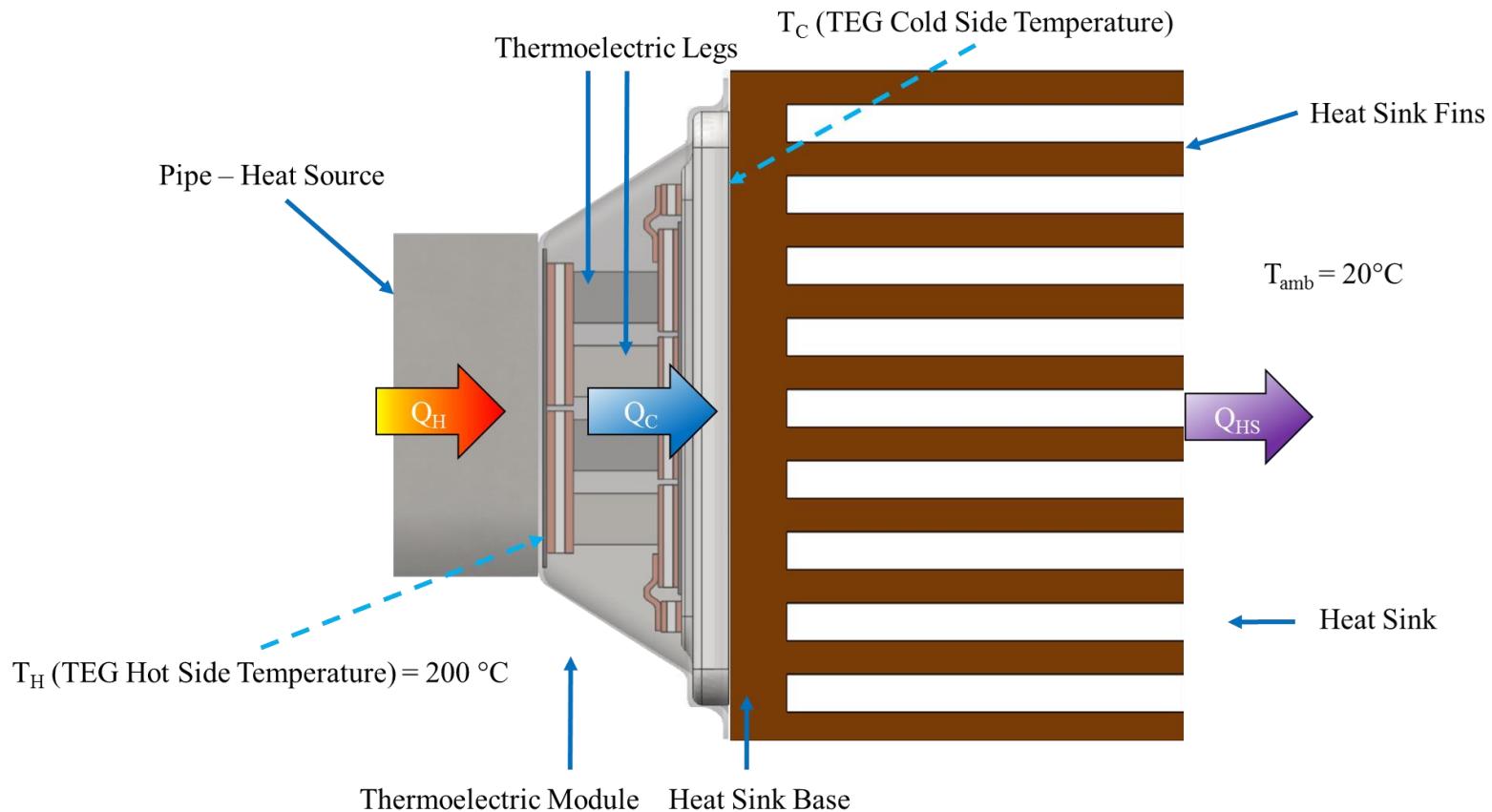
**θ<sub>b</sub>** : Temperature Difference Between Base and Ambient

**v** : Kinematic Viscosity

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# Model Overview

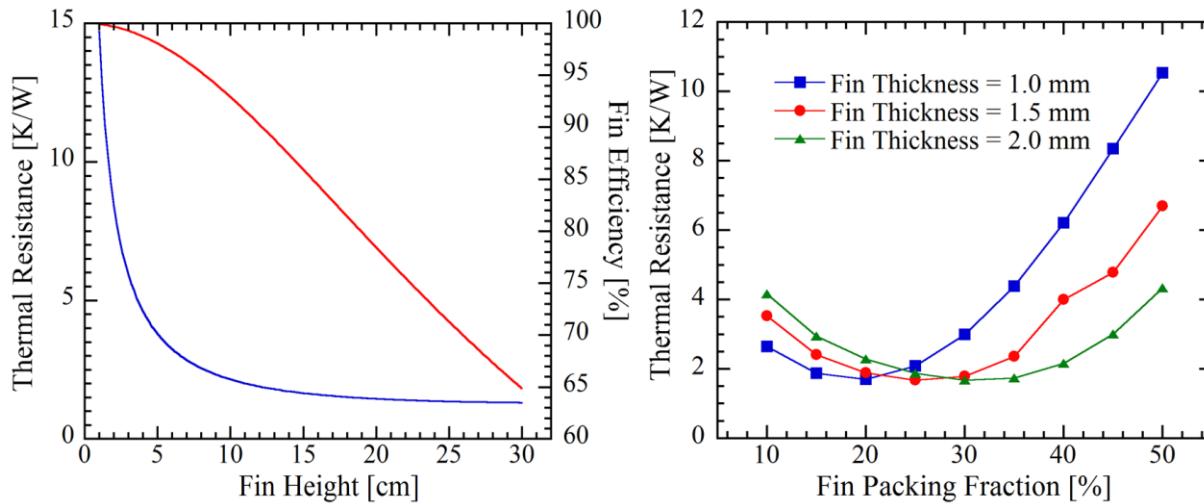


# Heat Sink Optimization

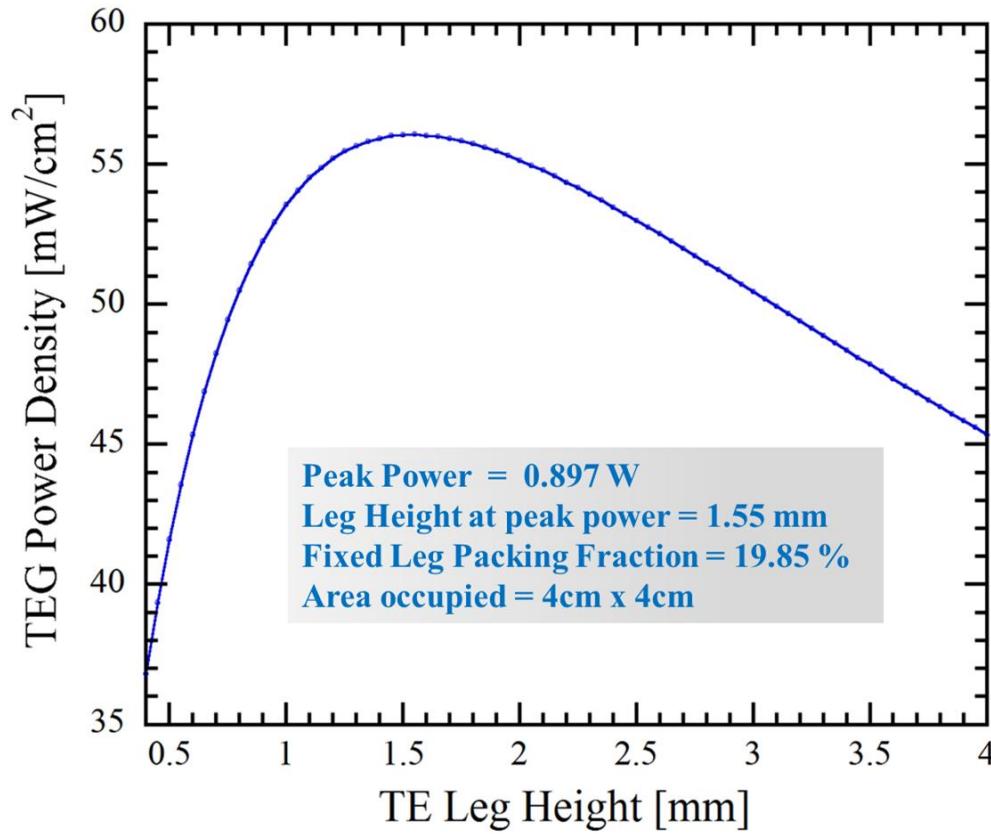
## Optimization Parameters

Parameter	Value
Fin Thickness	1mm – 10 mm with 0.5 mm increments
Fin Height	1cm – 30 cm with 1 cm increments
Fin Packing Fraction	10% - 50 %

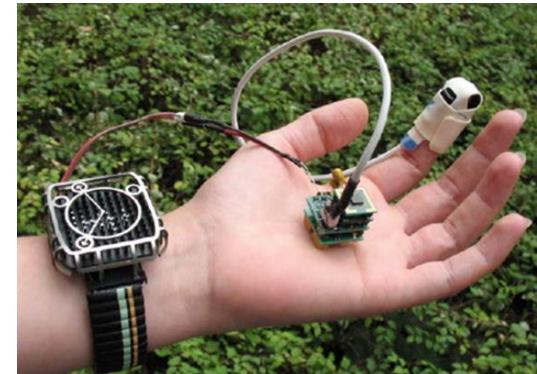
## Optimization Results



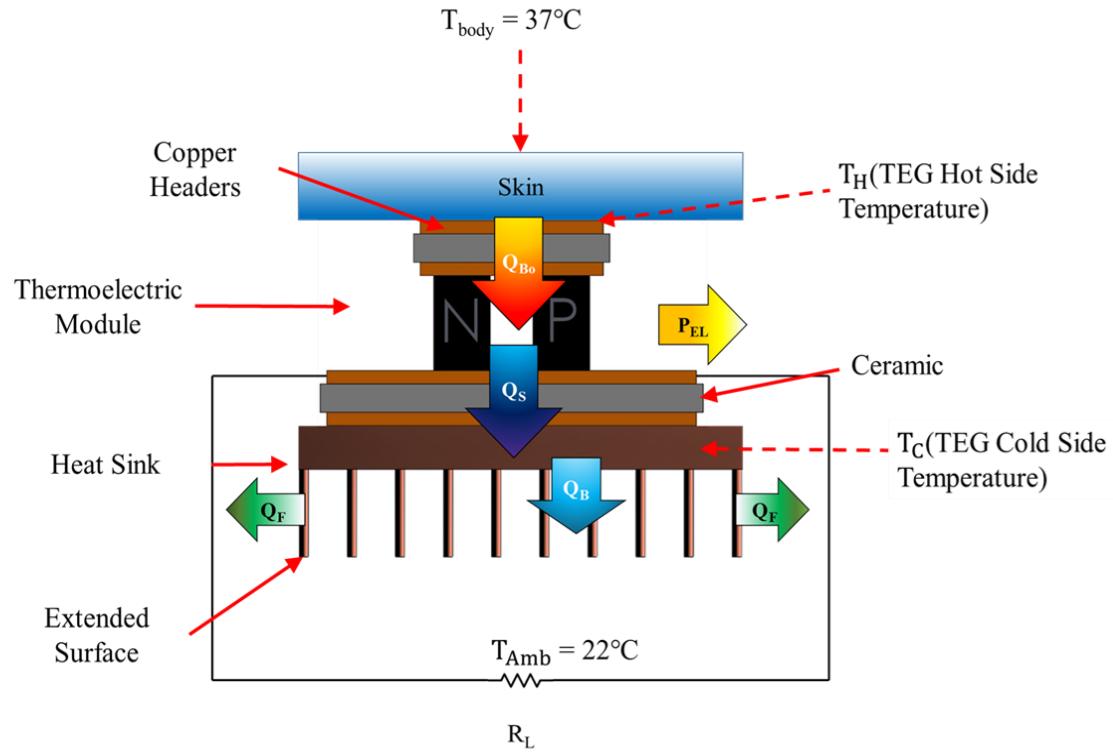
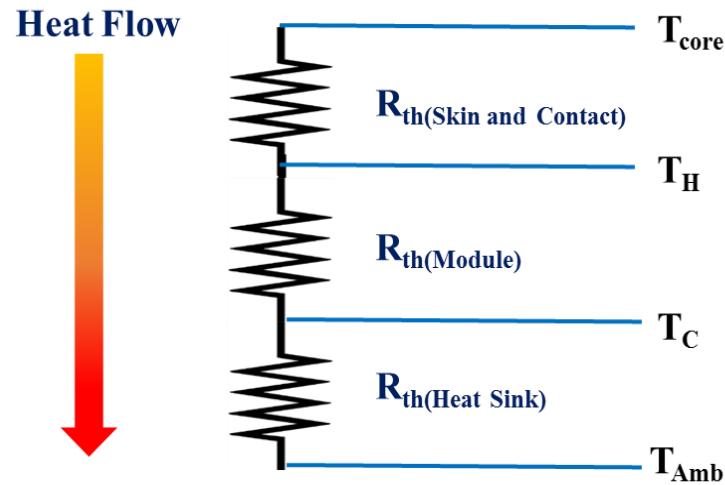
# TEG Optimization



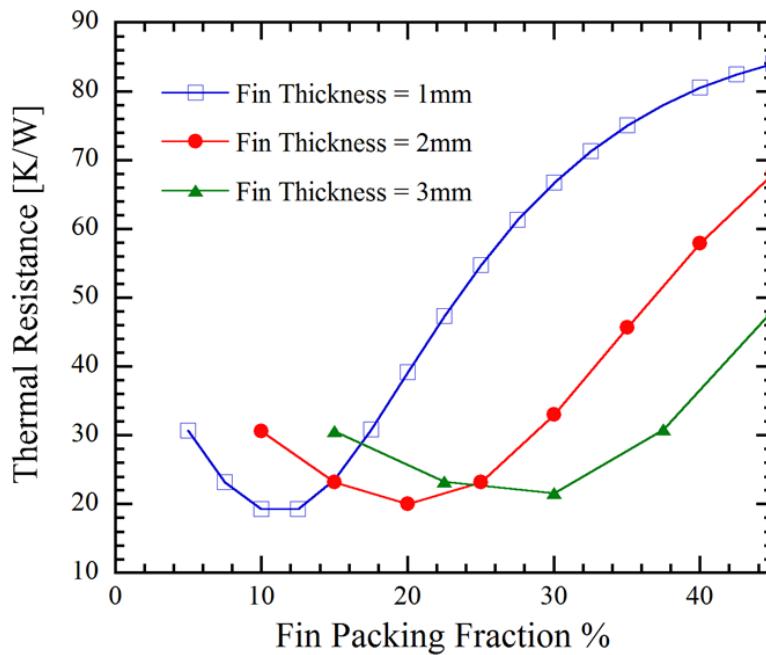
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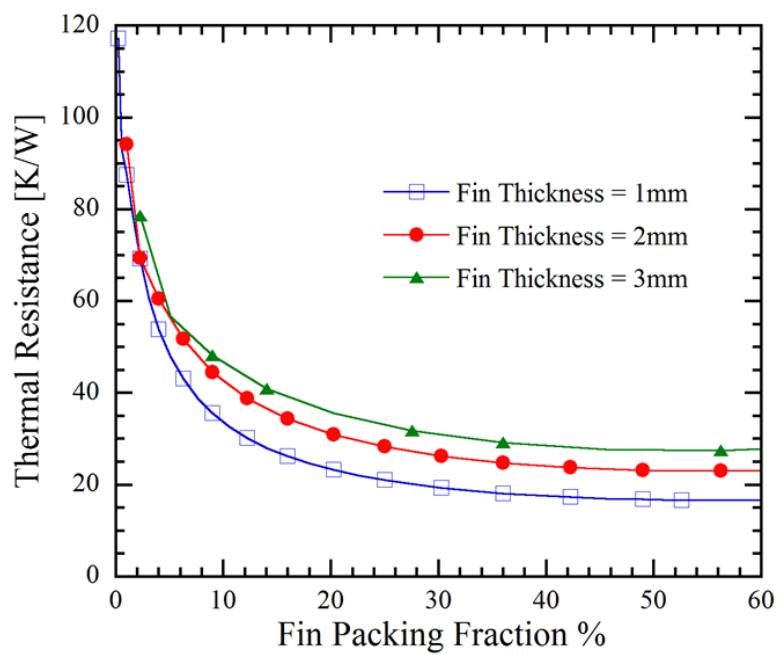
# Model Overview



# Heat Sink Optimization for a Fin Height of 3 cm

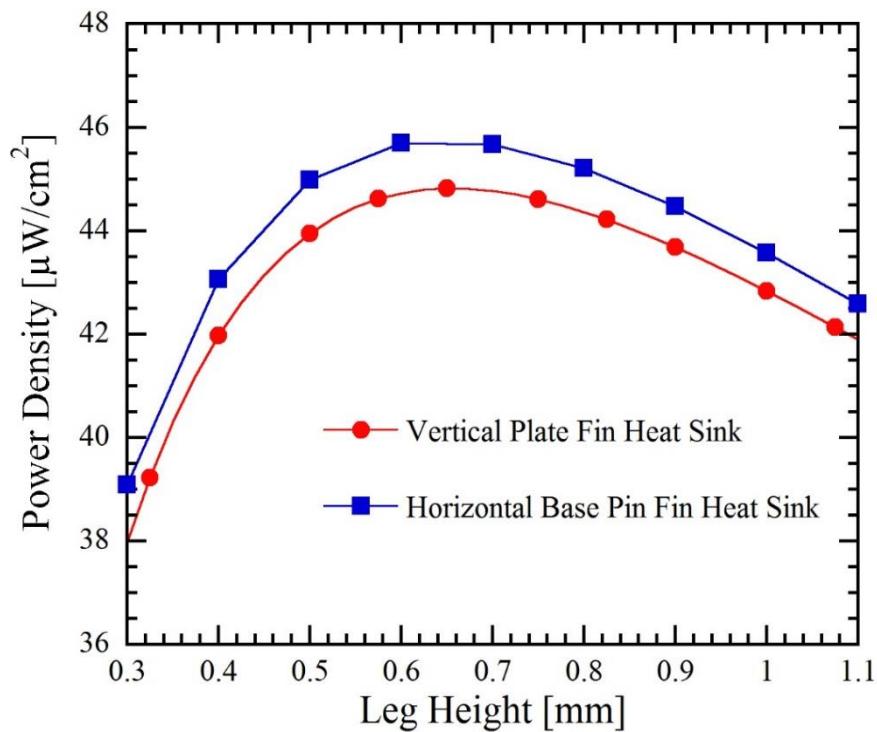


Flat Plate Natural  
Convection Heat Sink



Horizontal Base Square Pin Fin  
Natural Convection Heat Sink

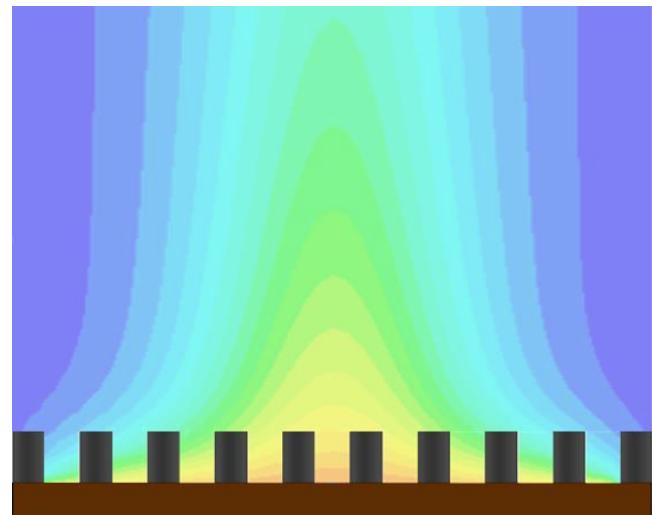
# TEG Optimization Results



Leg Packing Fraction = 0.638 %

Parameter	Flat Plate HS	Horizontal Base HS
Max Power	0.717 mW	0.731 mW
Max Heat Flow	8.074 $\text{mW}/\text{cm}^2$	8.231 $\text{mW}/\text{cm}^2$
TE Leg Height	0.65 mm	0.60 mm

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# Microwire Convection Coefficient

Empirical Convection  
Coefficient From Ref [12]

$$h = \frac{k_a}{1 + K_n} \left( \frac{1}{d} \right) \left[ \frac{1}{16} \ln^2 \left( \frac{\alpha_a}{d^2} \right) - 0.292 \ln \left( \frac{\alpha_a}{d^2} \right) + 0.958 \right]^{-1/2}$$

Nusselt Number From Ref [13]

$$Nu = 1.03 \cdot (Gr \cdot Pr)^{0.035}$$

Grashof Number From Ref [13]

$$Gr = \frac{g \cdot \beta \cdot (T_s - T_\infty) d^3}{\nu^2}$$

Empirical Convection  
Coefficient From Ref [13]

$$h = \frac{k_a \cdot Nu}{d}$$

**k<sub>a</sub>** : Fluid Thermal Conductivity

**α<sub>a</sub>** : Fluid Thermal Diffusivity

**d** : Fin Diameter

**Pr** : Prandtl Number

**g** : Gravity

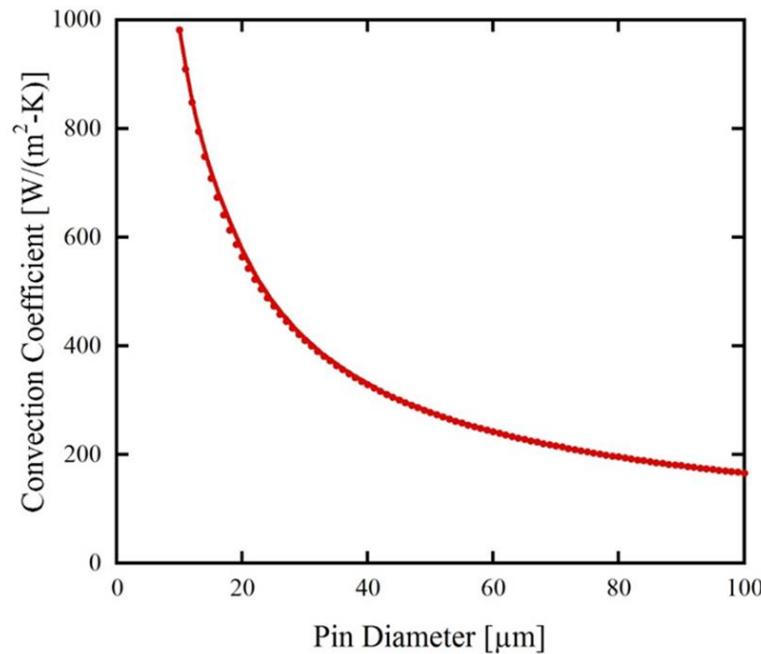
**β** : Coefficient of Thermal Expansion

**T<sub>s</sub>** : Temperature of Microwire Surface

**T<sub>∞</sub>** : Ambient Temperature

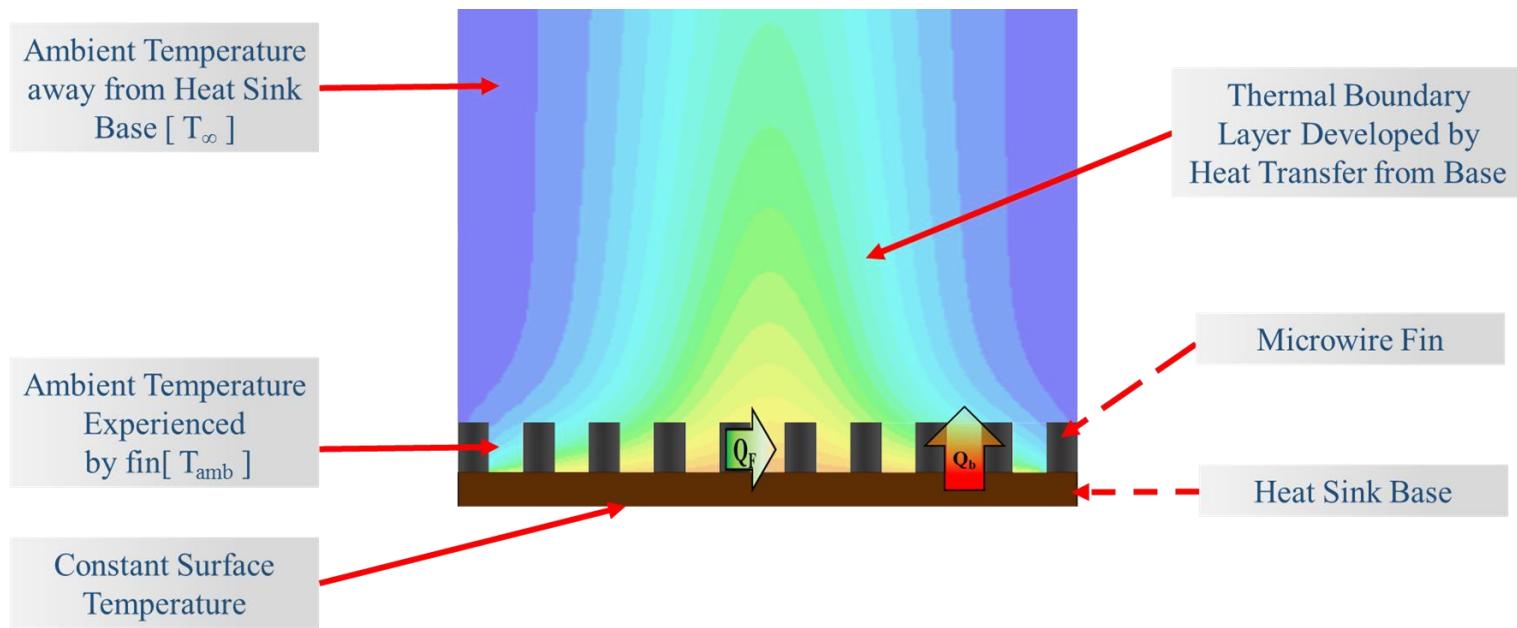
**ν** : Kinematic Viscosity of Air

# Microwire Convection Coefficient



Empirical Convection  
Coefficient From Ref<sup>[12]</sup>

# Model Overview



# Model Assumptions

1. Heat Source is a thermal reservoir
2. Microwire boundary layer thickness has little influence on heat transfer from adjacent fin
3. Each fin treated as an individual fin based on spacing limitation
4. Microwire convection coefficient used as fin convection coefficient

# Fin Heat Transfer

Fin Temperature Profile

$$T = K^{-1}F$$

Elemental Stiffness Matrix

$$K_e = \int_l [B]^T [D] [B] A dx + \int_l h P [N]^T [N] dx$$

Elemental Stiffness Matrix  
Simplified for a linear element

$$K_e = \frac{A_e k_e}{l_e} \begin{bmatrix} 1 & -1 \\ -1 & 1 \end{bmatrix} + \frac{h P}{l_e} \begin{bmatrix} 2 & 1 \\ 1 & 2 \end{bmatrix}$$

$$F_e = \int_S h T_{amb} [N]^T dS = \frac{h P T_{amb} l_e}{2} \begin{bmatrix} 1 \\ 1 \end{bmatrix}$$

$$Q_{T\_Fin} = \sum_{i=1}^{\text{elems}} h \cdot A_{e\_s} \cdot \left( \frac{T_n + T_{n+1}}{2} - T_{amb(n)} \right)$$

$$Q_{HeatSink} = \sum_{i=1}^{Nf} Q_{T\_Fin} + h_{hp} \cdot A_{uf} \cdot (T_b - T_\infty)$$

Heat Transferred from an individual fin

Total Heat Transferred from Heat Sink

**T** : Temperature Profile  
**K** : Global Stiffness Matrix  
**F** : Global Loading Vector  
**B** : Strain Displacement Matrix  
**D** : Thermal Conductivity Terms  
**N** : Shape Function  
**h** : Convection Coefficient  
**P** : Fin Perimeter  
**A<sub>e</sub>** : Elemental Cross-sectional Area  
**l<sub>e</sub>** : Element Length  
**T<sub>amb</sub>** : Ambient Temperature  
**elems** : Number of elements  
**A<sub>e-s</sub>** : Elemental Fin Surface Area  
**T** : Temperature  
**n** : Node  
**N** : Number of Elements  
**h<sub>hp</sub>** : Convection Coefficient of a Hot Plate  
**A<sub>uf</sub>** : Unfinned Area  
**T<sub>∞</sub>** : Ambient Temperature Away from Base  
**Nf** : Number of fins

# Ambient Temperature Above Base

Temperature Profile

$$\frac{T_{x,y} - T_{\infty}}{T_s - T_{\infty}} = (1 - y/\delta)^2$$

Boundary Layer  
Thickness

$$\delta = 4.317x \left[ \frac{\text{Pr} + (16/21)}{\text{Pr} \cdot \text{Gr}_x} \right]^{1/5}$$

Local Grashof Number

$$\text{Gr}_x = \frac{g\beta x^3(T_s - T_{\infty})}{v^2}$$

$T_{\infty}$  : Ambient Temperature

$T_s$  : Surface Temperature

$y$ : Vertical Distance

$x$  : Horizontal Distance

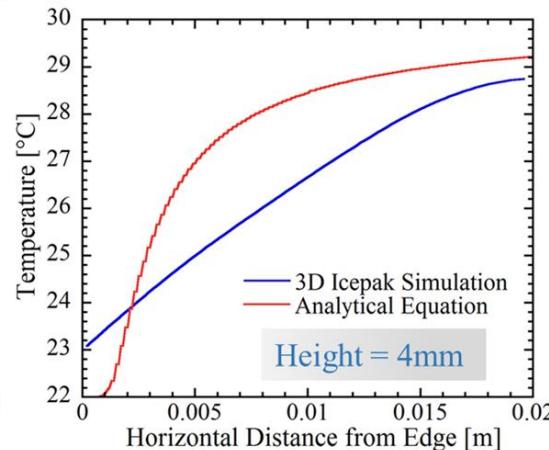
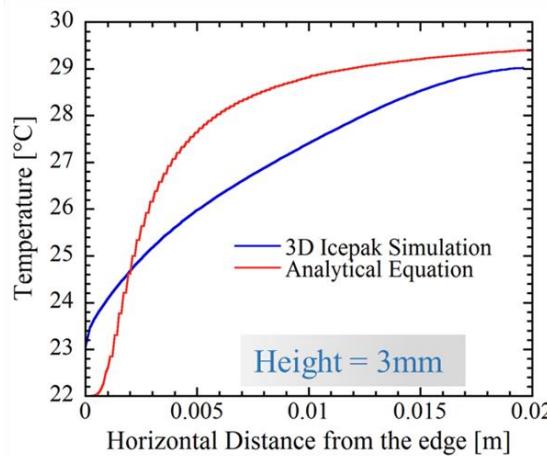
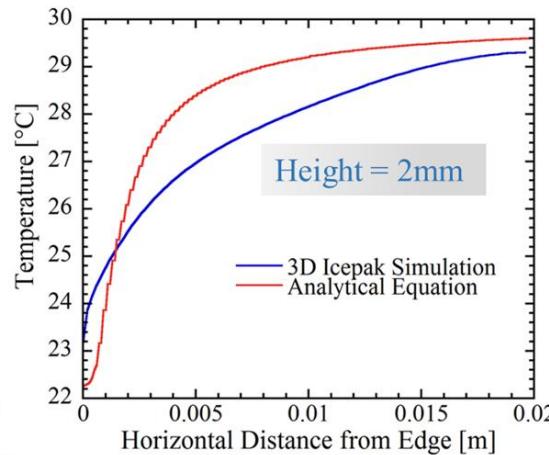
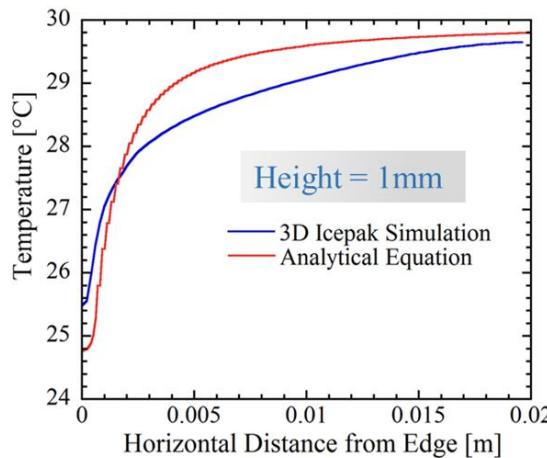
$\text{Pr}$  : Prandtl Number

$g$  : Gravity

$\beta$  : Coefficient of Thermal Expansion

$v$  : Kinematic Viscosity of Air

# Temperature Profile Comparison





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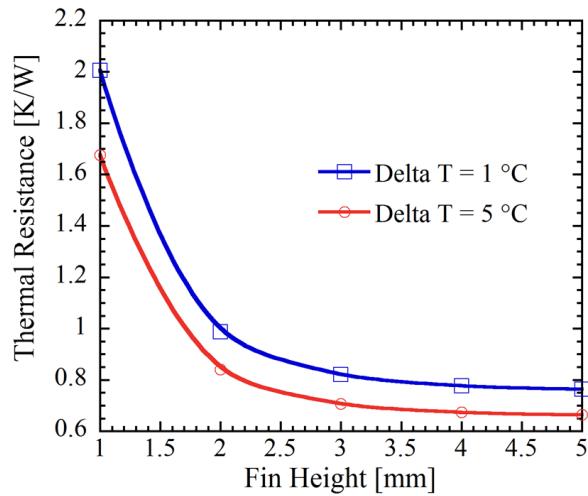
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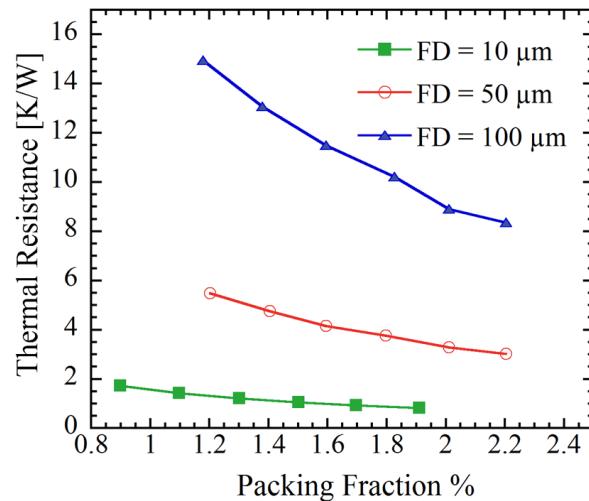
# Heat Sink Optimization Input

Parameter	Value
Fin Diameter	10 $\mu\text{m}$ , 50 $\mu\text{m}$ , 100 $\mu\text{m}$
Fin Height	1 mm , 2 mm, 3 mm, 4 mm, 5 mm
Fin Packing Fraction [10 $\mu\text{m}$ , 50 $\mu\text{m}$ and 100 $\mu\text{m}$ ]	0.9 % - 1.9 %, 1.2%, 2.2%

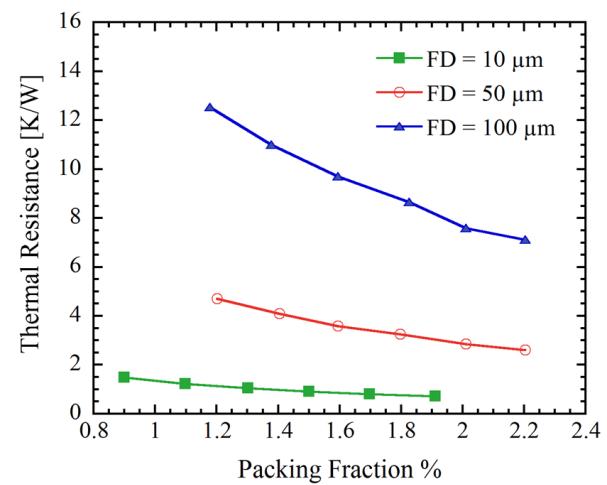
# Heat Sink Optimization Results



Fin Height  
Optimization



Delta T = 1°C



Delta T = 5°C

# Optimized Results and Comparison

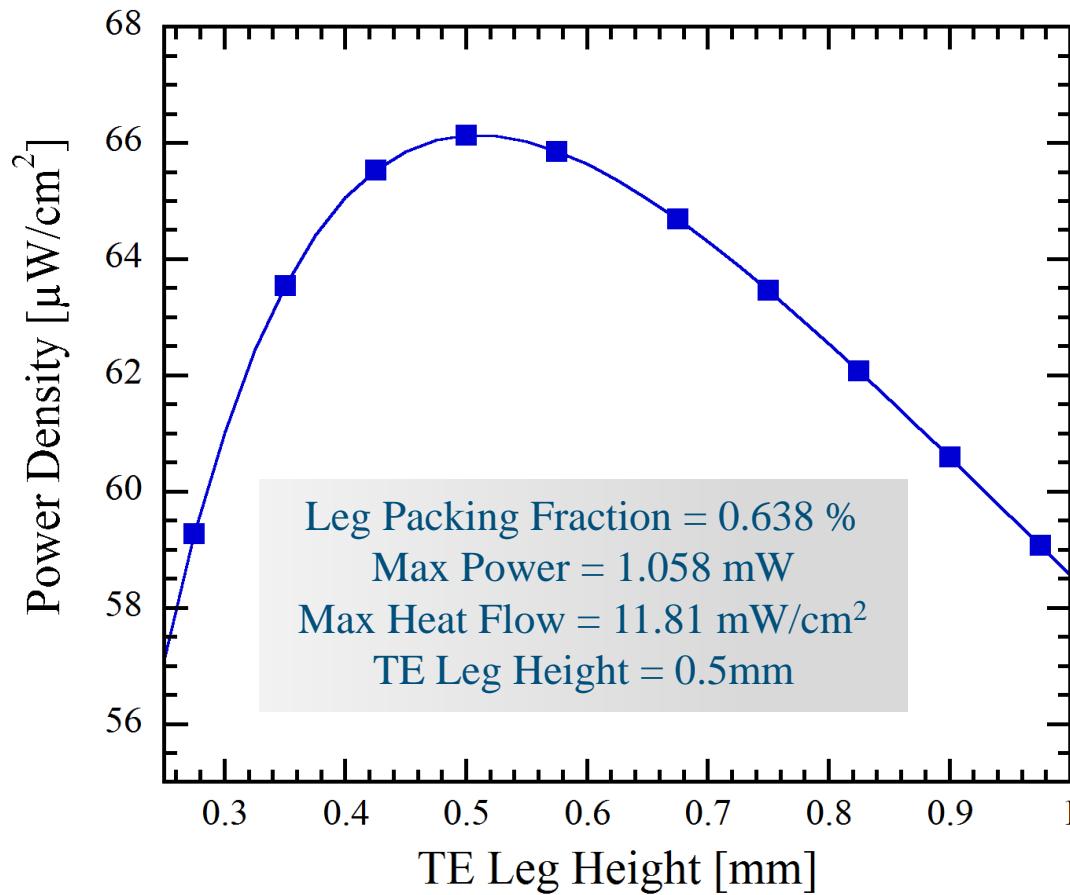
Optimized Heat Sink  
Parameter

Comparison with a  
Macro-scale Heat Sink  
with height 3 cm

Parameter	Value
Heat Exchanger Base Area	40 mm x 40 mm
Heat Exchanger Base Thickness	0.5 mm
Fin Diameter	10 $\mu\text{m}$
Fin Height	3 mm
Fin Packing Fraction	1.9 %

Heat Sink Type	Thermal Resistance $\Delta T = 1^\circ\text{C}$	Adjusted Thermal Resistance $\Delta T = 1^\circ\text{C}$	Thermal Resistance $\Delta T = 5^\circ\text{C}$	Adjusted Thermal Resistance $\Delta T = 5^\circ\text{C}$
Macro-scale	28.68 K/W	77.05 K-cm/W	12.90 K/W	38.70 K-cm/W
Micro-scale	0.820 K/W	0.246 K-cm/W	0.706 K/W	0.212 K-cm/W

# TEG Optimization





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# Conclusion and Future Work

# Conclusion

## 1. TEG Model

- Can be used as initial step in TEG design
- Validated with 3-D Model
- Improvement to TEG design suggested
  - Ceramic layer
  - Segmented TEGs

## 2. TEG- HX Model

- Compact HX model developed
- Two convection coefficients implemented
- Validated with 3-D Model

## 3. TEG – Heat Sink Model

- Heat sink model developed for two different heat sink types
- Optimized heat sink applied with TEG to power wireless sensor node and harvest waste heat from the human body.

## 4. TEG- Microwire Heat Sink Model

- Microwire heat sink model developed
- Optimized design used with TEG to harvest waste heat from the human body.

# Improvements to Models

1. TEG Model
  - I. Capture heat spreading effects in TEG model
  - II. Incorporate radiation losses from outer surfaces of unicouple
2. Heat Exchanger Model
  1. Obtain pressure drop values for heat exchanger
  2. Obtain net power using pressure drop values

## 3. Natural Convection microwire heat sink

- I. Model for varied base temperature
- II. Consider vertical base for heat sink and related heat transfer
- III. Obtain a global convection coefficient correlation for the heat sink based on fin height and fin diameter using data for various heat sink designs.

# Acknowledgments

I would like to thank my advisor and committee chair Dr. Yanliang Zhang and the rest of the thesis committee, Dr. John Gardner and Dr. Inanc Senocak. I would also like to thank my colleagues at the Advanced Energy Lab. Finally, I would like to thank my parents Asoka and Bandula.



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**THANK YOU**