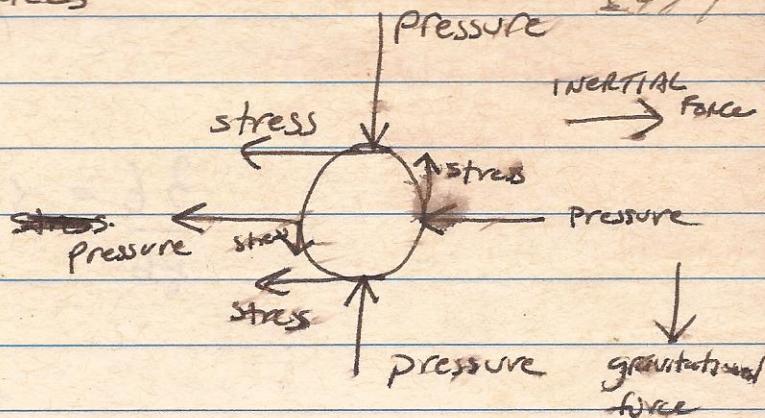
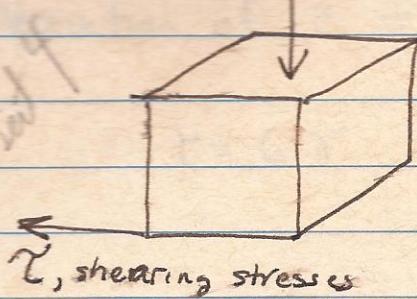


Encyclopedia of Physics
Science & Technology

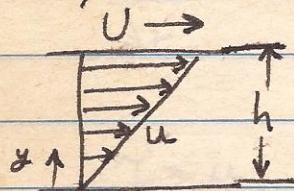
123
E497

Ref set P, pressure forces



$$F_{\text{RESULTANT}} = F_{\text{INERTIAL}} - F_{\text{PRESSURE}} - F_{\text{STRESS}} - F_{\text{GRAVITATIONAL}}$$

VELOCITY DISTRIBUTION:



$$u(y) = \frac{y}{h} U$$

u = fluid velocity in boundary layer
 U = free stream velocity

h = boundary layer thickness

rate of change of velocity with respect to position y .

$$\therefore \text{Frictional Force, } \tau = \mu \frac{du}{dy} = \frac{\mu U}{h} \quad \mu = \text{is the viscosity of the fluid}$$

τ units in $\frac{N}{m^2}$ μ units in $\frac{kg}{m \cdot sec}$

γ magnitude of the strain

$\frac{d\gamma}{dt}$ rate of change of strain

ϵ dilation $\frac{d\gamma}{dt}$

$$\text{Derivation of } \tau = \mu \frac{U}{h}$$

G = modulus of shear

ξ = displacement

$$\tau = G \gamma \quad \text{with} \quad \gamma = \frac{d\xi}{dy}$$

$$\text{and} \quad \xi = ut \quad \cancel{\text{and}} \quad \alpha \neq 0$$

$$\therefore \tau = \mu \frac{d\gamma}{dt} = \mu \frac{d}{dt} \left(\frac{d\xi}{dy} \right) = \mu \frac{d}{dy} \left(\frac{d\xi}{dt} \right)$$

$$\text{with} \quad \frac{d\xi}{dt} = u, \text{ then}$$

$$\tau = \mu \frac{du}{dy}$$

$$\text{with } u = \frac{y}{h} U \text{ and } \frac{du}{dy} = \frac{U}{h}$$

$$\therefore \boxed{\tau = \mu \frac{U}{h}} \quad \underline{\text{Proof!}}$$

IMP TO ACKNOWLEDGE KINEMATIC VISCOSITY WHEN TAKING INTO ACCOUNT THE FRICTIONAL + INERTIAL FORCES.

$$V = \frac{\mu}{\rho} \quad (\text{m}^2/\text{s})$$

V = Kinematic Viscosity, μ = Viscosity, ρ = density

$$\vec{r}_{\text{real}} = (91.37t - 48.41t^2)\hat{i} + (1.218 - 4.9t^2)\hat{j}$$

$$s = (91.37)(0.25) - 48.41(0.25)^2$$

$$= 22.84 - 3.026$$

$$= 19.81 \text{ m} \times 39.4 \text{ in} \times \frac{1}{12 \text{ in}} = \boxed{65.1 \text{ ft}}$$

$$Q_{\text{min}} = 1.57 \text{ in}^3 \quad \delta = 0.2 \text{ in}$$

$$Q_{\text{max}} = 3.48 \text{ in}^3 \quad \delta = 0.09 \text{ in}$$

$$0.18 \text{ ft/s}$$

$$C_g = \frac{V_0}{U} = \frac{0.18}{300} = 0.0006$$

$$C_g \cdot A \cdot U_b$$

$$\text{ft}^2 \text{ ft/s}$$

$$A = \pi r^2$$

$$(0.0006)(0.355866)(300) = 0.0640558 \text{ ft}^3/\text{s}$$

$$r = \frac{34}{12} = 0.0283$$

$$0.35587 \text{ ft}^2$$

$$Q = 0.0640558 \text{ ft}^3/\text{s} \times 1728 \frac{\text{in}^3}{\text{ft}^3} = 110.69 \text{ in}^3/\text{s}$$

For a front time of 0.29 s,

$$Q = 26.56522 \text{ in}^3$$

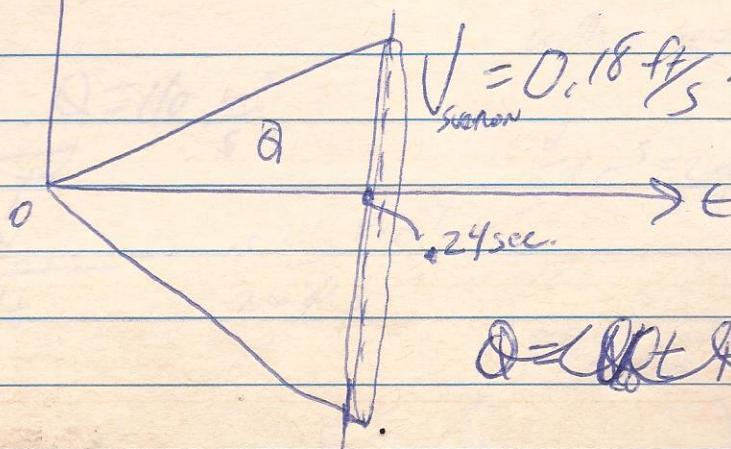
$$y(Q, t)$$

$$nV_{\text{Dimp}}$$

U_{Section}
 \bullet
Velocity
at section



$$U_{\text{Section}} = 0.18 \text{ ft/s} \times 12 \frac{\text{in}}{\text{ft}} = 2.16 \text{ in/s}$$



$$Q = C_d A t + \text{constant}$$

$$V = \frac{4}{3} \pi r^3$$

$$\frac{dV}{dt} = \frac{8}{3} \pi r = 110 \frac{\text{in}^3}{\text{s}}$$

SIZE OF
DIMPLE - experiment
OF CANNON FLUX

$$\frac{dV}{dr} = 4\pi r^2$$

$$\frac{dV}{dt} + P_0$$

$$\frac{4\pi r^3}{3} \cdot 2 \cdot \frac{9}{3} \pi r^2 =$$

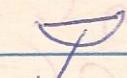
$$V = V_t + V_0 = 110t + \frac{4}{3} \pi r^3$$

$$\frac{d}{dr} \left(\frac{dV}{dt} \right) = 9\pi r^2$$

$$\frac{Q}{t_{cav}} = 26.57 \text{ m}^3$$

How does it take to
fill a dimple of Volume V_0
with a suction velocity of U_0 ?

$$Q = 110 \frac{\text{m}^3}{\text{s}}$$



$$\frac{dV_{\text{dimple}}}{dt}$$

$$= 0.26 \times 10^{-9}$$

$$26 \mu\text{s}$$

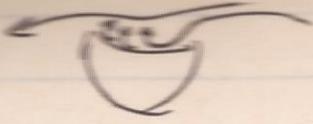
$$1.1125 \times 10^{-9}$$

$$\frac{d}{dr} \left(\frac{4}{3} \pi r^3 \right) = 3\pi r^2 \quad V = 0.882 \times 10^{-9}$$

$$\left(\frac{1.1125 \times 10^{-9}}{0.26 \times 10^{-9}} \right)^3 = 0.445$$

$$\delta = 0.0223$$

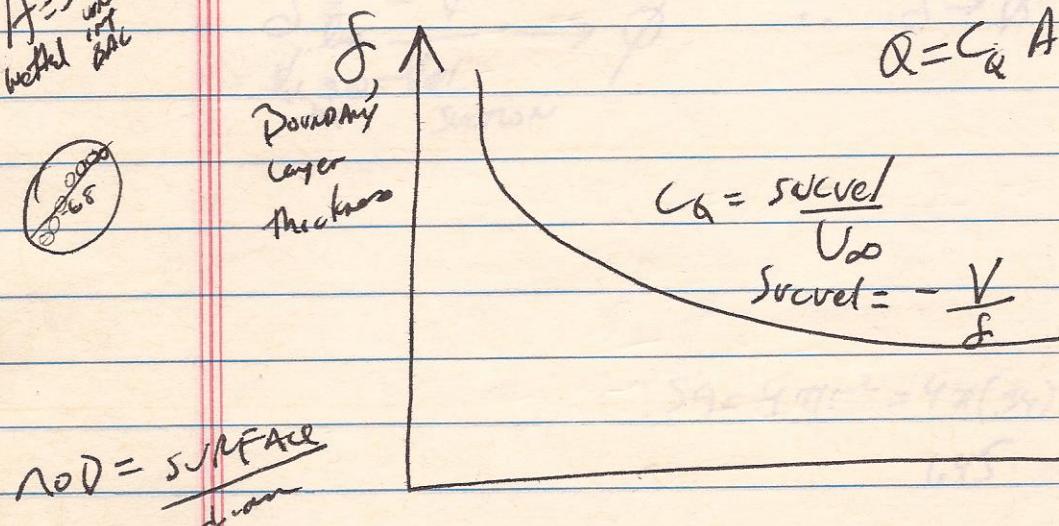
$$F = 0.0011125$$



- 1) Choose ARBITRARY Dimple size.
 - 2) Compute # of dimples meets optimum dimple size.
 - 3) Compute VOLUME OF DIMPLES (TOTAL)
 - 4) From MAX & MIN SUCTION RECORDS OBTAIN

From other sources, compute total MAX + MIN
SUGAR VOLUME

- 5) Compute C_d & boundary-layer thickness.
 - 6) Compute New Reynolds Number & compare with upstream
surface (e.g. smooth hill to hills + valleys).
 - 7) Compute ~~local coefficient of drag~~ to get drag equation.
 - 8) Plot improved-ball trajectory.



$$Q = C_A A \cup \infty \quad \frac{Q}{A \cup \infty} = C_Q$$

$$\begin{array}{r}
 & 1 \\
 & .34 \\
 & .34 \\
 \hline
 & 136 \\
 102 \overline{)1156} & 4624 \\
 & 34 \quad \cancel{156} \\
 & \cancel{34} \quad 68 \\
 & \hline
 \end{array}$$

Q

Sutton volume.

$$\begin{array}{r}
 2137 \\
 \cdot 362789
 \end{array}$$

$$\begin{array}{r} \overline{12.0} \\ \times 121n^3 \\ \hline 36278 \end{array}$$

$$\frac{n \text{ Volumen}}{\cancel{35}} = \cancel{42 \text{ m}^3} \cdot 3, \text{ m}^3$$

$$C_Q = \lim_{A \rightarrow \phi} \frac{Q}{A U_\infty} = \frac{C_a}{U_\infty} \rightarrow \infty$$

$$V_{el.} = \lim_{\substack{\text{SUCTION} \\ C_a \rightarrow 0}} C_Q U_\infty \rightarrow \infty$$

$$\int \bar{t}_{\text{kin}} - V \rightarrow \phi \quad \therefore \int \rightarrow \phi$$

~~$t_{el} \rightarrow \infty$~~

~~$t_{el} \rightarrow \infty$~~

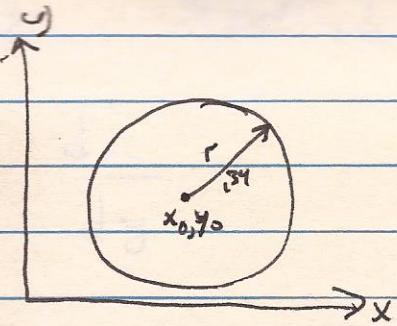
SUCTION

$$SA = 4\pi r^2 = 4\pi(34)^2$$

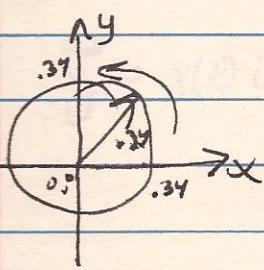
1.45

$$\frac{34}{6}$$

$$\frac{1156}{214}$$



$$\int_C x^2 + y^2 - r^2$$



$$\int_C x^2 dy + y^2 dx$$

$$\iint_R \left(\frac{\partial g}{\partial x} - \frac{\partial f}{\partial y} \right) dA =$$

$$\iint_R \left(\frac{\partial (x^2)}{\partial x} - \frac{\partial (y^2)}{\partial y} \right) dA$$

$$\int_{0}^{0.34} \int_{0}^{0.34} \left[\frac{2x^2}{2} - \frac{2y^2}{2} \right] dy dx$$

$$\int_0^{0.34} (2xy - 2y^2) \Big|_0^{\sqrt{r^2 - x^2}} dx$$

$$\int_0^{0.34} (2x\sqrt{r^2 - x^2} - (r^2 - x^2)) dx$$

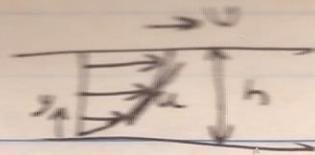
$$\int 2x(r^2 - x^2)^{1/2} - (r^2 - x^2) dx$$

$$u = r^2 - x^2$$

$$du = -2x dx$$

$$-\int \frac{du}{u^{1/2}} - \left(x r^2 + \frac{x^3}{3} \right)$$

$$-\frac{2}{3} u^{-1/2} = -\frac{2}{3} (r^2 - x^2)^{1/2} - x r^2 - \frac{x^3}{3}$$



$$W = \mathbf{F} \cdot \mathbf{s} = m a s$$

$$\frac{du}{dy}$$

$$\frac{d\vec{u}}{d\vec{y}}$$

$$t^3 t_i^2 + (t - t^2) j$$

$$t^5 i + (t - t^2) j$$

$$\vec{y} = x(t) i + y(t) j$$

Partial Derivatives

A function of two variables where the derivative of the function with respect to one variable.

Ex. $f(x,y) = 2x^3y^2 + 2y + 4x$

Find $f_x(1,2)$, $f_y(1,2)$

$$f_x(1,2) = 6x^2y^2 + 4 = 6(1)(2)^2 + 4 = 24 + 4 = 28$$

$$f_y(1,2) = 4x^3y + 2 = 4(1)(2) + 2 = 8 + 2 = 10$$

Other notation.

$$f_x = \frac{\partial f}{\partial x} \quad f_y = \frac{\partial f}{\partial y}$$

Ex.

$$z = x^4 \sin(xy^3)$$

$$\text{find } \frac{\partial z}{\partial x}, \frac{\partial z}{\partial y}$$

$$\frac{\partial z}{\partial x} = 4x^3 \sin(xy^3) + x^4 \cos(xy^3) y^3$$

$$\frac{\partial z}{\partial y} = x^4 \cos(xy^3) 3xy^2 = 3x^5 y^2 \cos(xy^3)$$

Ex. of Diff. Eq.

1) $\frac{dy}{dx} + y = x+1$ - 1st order Linear O.D.E.

2) $\frac{d^2y}{dx^2} + xy^2 \left(\frac{dy}{dx} \right)^3 = 0$ - 2nd order because 1st NO derivative is raised to 3rd power & in the form it is not raise.

3) $\frac{d^5y}{dx^5} + \frac{dy}{dx} = x^2y \Rightarrow$ 5th order Linear O.D.E.
also written $\frac{d^5y}{dx^5} + \frac{dy}{dx} - x^2y = 0$ where x^2 is $a_2(x)$ of the form

4) $\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} = 0$ - 2nd order NO

5) $\frac{\partial u}{\partial x} + \frac{\partial u}{\partial y} + \frac{\partial u}{\partial z} = 0$ - 1st order. NO

Differential equation = is an equation containing derivatives

Ordinary Diff. Eq (O.D.E) = NO PARTIAL DERIVATIVES

Partial Diff. Eq (P.D.E) = CONTAINING ONLY PARTIAL DERIVATIVES

Order of Diff. Eq. determined by order of derivative

Linear O.D.E of order n in the dependent variable y & independent variable x is a Diff. Eq. of the form

$$a_n(x) \frac{d^n y}{dx^n} + a_{n-1}(x) \frac{d^{n-1} y}{dx^{n-1}} + \dots + a_1(x) \frac{dy}{dx} + a_0(x)y = b(x)$$

If $a_n(x)$ is constant, then the above D.E. is a D.E. with constant coefficients

$$\frac{d^2y}{dx^2} + 5 \frac{dy}{dx} + 6y = 0$$

is a D.E. w/ constant coefficients

Solution of D.E.

1) $y = x + 3e^{-x}$ is a solution of $\frac{dy}{dx} + y = x + 1$

$$\frac{dy}{dx} = 1 - 3e^{-x}$$

An explicit solution
of the D.E.

$$\frac{dy}{dx} + y = 1 - x$$

OBJECTIVE:

Given the D.E., and determine the solution.

Given the relation

cannot find y in terms of x , therefore must use implicit differentiation to find the D.E.,

$$2xy \left(\frac{dy}{dx} \right) + x^2 + y^2 = 0$$

Remember (x_1) is an example of an implicit solution of the D.E.)

Def

A function $f(x)$ defined for all x in some interval I and having an n th derivative for all $x \in I$ is called an explicit solution of the D.E. $F[x, y, \frac{dy}{dx}, \frac{d^2y}{dx^2}, \dots, \frac{d^ny}{dx^n}] = 0$

F.

- 1) $F[x, F(x), F'(x), F''(x), \dots, F^{(n)}(x)]$ is defined for all $x \in I$
- 2) $F[x, f(x), f'(x), \dots, f^{(n)}(x)] = \emptyset$ for all $x \in I$,

Def

$g(x, y) = 0$ is a implicit solution of the D.E. if
 $f(x)$ is an explicit solution of the D.E.

Ex

$5x^2y^2 - 2x^3y^2 = 1$ is an implicit solution of the D.E.

$$x \frac{dy}{dx} + y = x^3y^3$$

$$G_{\text{max}} = \frac{1}{4} C_{\text{eff}}^2 \left(40.12 + 4.22 \times 10^{-7} V^3 A_s^2 \right)$$

432 VCH

$$6.334 \pm \sqrt{40.12 + (4.031 \times 10^2)} V^3 A_s^2$$

$$r_{0,1} = \frac{C\pi}{432V}$$

$$C = INT \left(\frac{A_0}{\pi r^2} \right)$$

$$216V_{AS} = 216 \left(As / \pi r^2 \right) [216 V_F - 6.354]$$

$$INT \left(-0.369 \right) \\ \pi r^2$$

$$\therefore S = 216 \text{ VAs} = \frac{A_S}{F} [216 V_F - 6.334]$$

INT(.0112)

$$\text{INT} \left(\frac{E_2}{2} \right) = 2 \quad 216 \text{ VAsr} = \underline{216 \text{ AsV}} - 6.334 \text{ As}$$

$$F = 0.01852 \times 10^{-5}$$

$$(40.31 \times 10^7) (0.0004895 \times 10^{-12})$$

$$4.031 \times 10^7 \quad 3.375 \times 10^{-9} \quad 7.001362 \times 10^3$$

$$INT\left(\frac{3}{8}\right) = \frac{61334 + \sqrt{4012 + (4031 \times 10^7)(0.00050)^2(0.0362)^2}}{2} \text{ and } C(3,14)$$

432 (1,060/150)

$$\lim_{r \rightarrow 0} \sqrt{wt\left(\frac{f^2}{g}\right)}$$

$$(150 \times 10^{-6})^3$$

40.12/3.140

$$\underline{3375000 \times 10^{-7}}$$

$$6,334 \pm \sqrt{12,777} / C$$

$$\frac{0.648}{61339 + 3,6745,7(C^{-1})^{1/2}}$$

44-0369

$$\frac{1,451,936 \text{ cu. ft.}}{12 \text{ in.}} = 121 \text{ ft. m}$$

$$r^2 - 51,21c^{-1} = 0$$

$$(r^2 - 51,21c^{-1})^2 = (90,75)^2$$

$$r^2 - 51,21c^{-1} = r^2 - 51,21c^{-1}$$

$$r^2 - 102,42c^{1/2} + 2622,46c^{-1} = 8235,56$$

$$\frac{r^2 - 102,42}{c^{1/2}} + \frac{2622,46}{c} = 8235,56$$

$$c^{1/2}r^2 - 102,42c^{1/2} + 2622,46 = 8235,56c$$

$$8235,56c - c^{1/2} + 102,42\sqrt{c} - 2622,46 = 0$$

$$f(c, r) = 8235,56c - c^{1/2} + 102,42c^{1/2} - 2622,46 = 0$$

$$\frac{\partial f}{\partial c} = 8235,56 - \frac{1}{2}c^{-1/2} + 102,42c^{1/2} \quad \frac{\partial f}{\partial r} = 2rc = 0$$

$$c = \phi$$

$$8235,56 - r^2 = 0$$

$$r^2 = 8235,56$$

$$D = \sqrt{c} \cdot$$

$$r = 90,75$$

$$(8235,56 - r^2) D^2 + 102,42 D - 2622,46 = 0$$

$$D =$$

$$C =$$