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Paul A. Iacomi

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Defended on JJ/MM/AAAA in front of the following jury:

Prénom NOM	Affiliation	Rapporteur
Prénom NOM	Affiliation	Rapporteur
Prénom NOM	Affiliation	Examinateur
Prénom NOM	Affiliation	Examinateur
Prénom NOM	Affiliation	Examinateur
Prénom NOM	Affiliation	Directeur de thèse

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Abstract

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1. Building a framework for adsorption data processing

1.1. Introduction

Historically, the processing of isotherms was done by hand, with large worksheets being used for the calculations. As an example, we point out that one of the initial limitations of the BJH method was that each point had to be determined with an approximation of critical pore radius, due to the tedious work involved in the calculation.⁽¹⁾

The advent of computers meant that the calculations could be performed quickly and reliably and led to the introduction of more complex methods for isotherm processing, such as the DFT method for pore size distribution.^(2,3) Commercial adsorption equipment which offers the users a complete software solution for any isotherm calculations is now commonplace and makes obtaining reports of desired properties for measured materials a matter of minutes.

Given the current ubiquitousness of adsorption as a characterisation method, particularly for investigating surfaces and porous compounds, there is a large pool of data published in the scientific community. Key performance indicators such as specific surface area, working capacity and pore volume are commonly reported in scientific literature and used as benchmarking tools for comparing performance.

Recent efforts have also focused on building a database of adsorption isotherms,⁽⁴⁾ to offer a searchable pool of standardised behaviours on different materials. This serves as both a useful reference for comparing synthesised compounds, as well as a method for quickly finding suitable materials which have the desired properties for a particular application.

In this chapter an open-source software package is presented, which is released under an MIT licence and written in Python, intended to be used for manipulation, storage, visualisation and processing of adsorption isotherms. Developed internally at the MADIREL Laboratory in Marseilles, the software is aimed to give users a powerful yet easy to use package that can perform the kind of processing usually offered by commercial software.

1.2. pyGAPS overview

1.2.1. Intended use cases

The software was imagined for use in two types of scenario. First, as a command line interface, in environments such as IPython and Jupyter. The typical user working in these environments is likely to be processing a small batch of results at one time, and is interested in obtaining the results in graphical form. For this type of application,

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the framework should provide an unobtrusive way of importing the user data, as well as present an API which does not require extensive knowledge of processing methods. Finally, a powerful graphing environment is required which will allow the user to visualise their original dataset and results.

The second envisaged application is related to bulk data processing. Requirements here shift towards parameter control, scripting and extensibility. The framework API should offer the option to change implicit parameters, select calculation limits and return the results in a numerical form for further processing. This type of application is also likely to require storage of isotherms in a database or under other types of data files.

1.2.2. Core structure

In order to offer a clear structuring of functionality, pyGAPS introduces several classes which abstract data and functionality for facile interaction. The classes are intuitively named: `Isotherm`, `Sample` and `Adsorbent`.

The Isotherm class

The `Isotherm` class is a representation of an adsorption isotherm i.e. a function of the amount adsorbed, or loading, with pressure at a fixed temperature. The class also contains other information relating to the isotherm, such as the material name and batch it describes, the adsorbate used and other user-defined properties.

Because the aforementioned relationship can be either a physical measurement defined by individual pressure-loading pairs or a model, describing the relationship as a function rather than discrete data, the `Isotherm` class is used as a parent class for two subclasses: `PointIsotherm`, describing datapoints and `ModelIsotherm` containing a model such as Henry, Langmuir etc., which encapsulate the respective functionality. The two classes are interchangeable as they share most methods and properties. Once an instance of an `Isotherm` class is created, it can then be used for the processing, conversion and graphing capabilities of pyGAPS.

The Sample class

The isotherm classes contain the name and batch of the sample they are measured on in a string format. The user might want to specify other information about the material, such as the date of synthesis or the material's density, as well as store this information in the database. For this case, pyGAPS provides the `Sample` class. The framework uses the string values in the isotherm to connect an `Isotherm` instance to a specific `Sample`.

The Adsorbate class

Finally, in order for many of the calculations included in pyGAPS to be performed, properties of the adsorbate used are needed e.g. liquid density, vapour pressure etc. The `Adsorbate` class is provided for this purpose, which is connected to an `Isotherm` class similarly to a `Sample`. The physical properties are either calculated in the background

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through an equation of state, either the open source CoolProp library⁽⁵⁾ or the NIST-made REFPROP.⁽⁶⁾ The properties can also be retrieved from the internal database or specified by the user.

1.2.3. Creation of an Isotherm

An Isotherm can be created either from the command line directly or through an import from a supported format. For the direct creation, the code takes two kinds of inputs: the data itself, in the form of a `pandas.DataFrame`, and the isotherm parameters describing it. Only four parameters are strictly required: the material name, the material batch, the adsorbate used and the experimental temperature. Other parameters can be passed as well and will be stored in the isotherm class.

Listing 1.1: Creating the `DataFrame`

```
1 isotherm_data = pandas.DataFrame({  
2     'pressure' : [1, 2, 3, 4, 5, 3, 2],  
3     'loading' : [1, 2, 3, 4, 5, 3, 2],  
4     'enthalpy' : [15, 15, 15, 15, 15, 15, 15],  
5     'xrd_peak_1' : [0, 0, 1, 2, 2, 1, 0],  
6 })
```

The `DataFrame` must contain a column containing the pressure points and one containing the corresponding loading points of the isotherm. Other columns can also be passed, when secondary data such as enthalpy of adsorption is present at each measurement point. These columns will be saved in the case of the `PointIsotherm` class and can be plotted afterwards.

If no unit data is specified in the constructor, the framework will assume that the isotherm is in units of mmol g^{-1} loading as a function of bar. Both the units and the basis can be specified, as it is explained in a latter section.

Finally, the data is saved in the newly created class or used to generate parameters for a model such as BET, Langmuir, etc., in the case of a `PointIsotherm` and `ModelIsotherm` respectively. It should be noted that the creation of `Sample` and `Adsorbate` instances is similar.

Alternatively, the isotherm can be imported from a file containing a format that is recognised by pyGAPS. Parsing from suitably structured JSON, CSV and Excel files is supported.

1.2.4. Workflow

Once an isotherm object is created, it will be used for all further processing. The class contains methods which can be used to inspect the data visually, or retrieve parts of the isotherm such as the adsorption or desorption branches with user-chosen limits or units. Singular values of pressure or loading can be calculated, either through interpolation in the case of a `PointIsotherm` or by evaluation of the internal model in the `ModelIsotherm`. For an isotherm with datapoints, these can also be converted into different units or modes.

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Listing 1.2: Creating the PointIsotherm

```
1 point_isotherm = pygaps.PointIsotherm(
2
3     # First the pandas.DataFrame with the points
4     # and the keys to what the columns represent.
5
6     isotherm_data,
7
8     loading_key='loading',           # The loading column
9     pressure_key='pressure',        # The pressure column
10    other_keys=['enthalpy',
11                'xrd_peak_1'],       # The columns containing other data
12
13    # Some of the unit parameters can be
14    # specified if desired.
15
16    pressure_mode='absolute',       # absolute pressure
17    pressure_unit='bar',            # with units of bar
18    adsorbent_basis='mass',         # adsorbent mass basis
19    adsorbent_unit='kg',            # with units of kg
20    loading_basis='mass',           # loading mass basis
21    loading_unit='g',              # with units of g
22
23    # Finally the isotherm description
24    # parameters are passed.
25
26    'sample_name' : 'carbon',       # Required
27    'sample_batch' : 'X1',           # Required
28    'adsorbate' : 'nitrogen',       # Required
29    't_exp' : 77,                  # Required
30    't_act' : 150,                 # Recognised / named
31    'user' : 'Username',           # Recognised / named
32    'DOI' : '10.000/mydoi',        # Unknown / user specific
33 )
```

Characterisation functions take a single isotherm object as their first parameter. This is the case for the BET area, Langmuir area, t-plot, α_s plot, and pore size distribution methods. These characterisation functions attempt to automate as much of the process as possible. For example, the BET area limits are automatically calculated using the Rouquerol⁽⁷⁾ method, with all the checks implemented into the code. In another example the straight line sections of the t-plot are determined automatically through a calculation of the second derivative of the transformed isotherm. For detailed control, there is an option to specify options for each individual method, such as manual BET limits, different thickness functions for the t-plot or Kelvin-based mesoporous pore distribution methods, custom parameters for the Horvath-Kawazoe microporous pore distribution, custom DFT or NLDFT kernels and more. The results are returned in a dictionary or can be directly graphed if the `verbose` parameter is passed.

1.2.5. Units

When computers work with physical data, units are often a matter that introduces confusion. Here we explain how pyGAPS handles units and other physical world concepts such as relative pressure and mass or volume basis.

The following dimensions can be specified for an Isotherm: the measurement *pressure*, the quantity of guest adsorbed or *loading* and the amount of adsorbent material the loading is reported on, or *adsorbent*.

Pressure can be reported either in an absolute value, in several common units such as bar, torr, Pa, or as *relative pressure*, the pressure divided by the saturation vapour pressure of the adsorbate at the respective measurement temperature. Conversions between the two modes are automatic and handled internally.

Both the *loading* and *adsorbent* can be reported in three different bases: a molar basis, a mass basis or a volume basis. Within each basis different units are recognised and can be easily converted. The conversions between bases can also easily performed if the required conversion factors (i.e. molar mass and density) are available. For *loading*, these factors are automatically calculated internally, while for the *adsorbent* they should be provided by the user in the respective `Sample` class.

1.3. Isotherm characterisation and fitting

1.3.1. Mathematical descriptions of isotherms

A lot of effort was put into attempting to describe the phenomenon of adsorption using a simple model. Through a mathematical understanding, the underlying mechanisms of adsorption can be understood. Unfortunately, the plethora of isotherm features and shapes can only be truly recreated by molecular simulation, which requires an exact knowledge of the adsorbent structure and its interaction with the adsorbed gas. Nevertheless, great strides have been taken to obtain several models which can be useful when fitted to measured isotherms for obtaining simple parameters which are representative of physical factors such as guest-host interaction, surface area, pore size, total pore volume and others. More importantly, it allows us to numerically compare measured isotherms.

A page of figures for different models with several values of their parameter can be seen in [Figure 1.1](#).

The Henry model

The simplest method of describing adsorption on a surface is Henry's law. It assumes only interactions with the adsorbate surface and is described by a linear dependence of adsorbed amount with increasing pressure.

$$n_a(p) = K_H p \tag{1.1}$$

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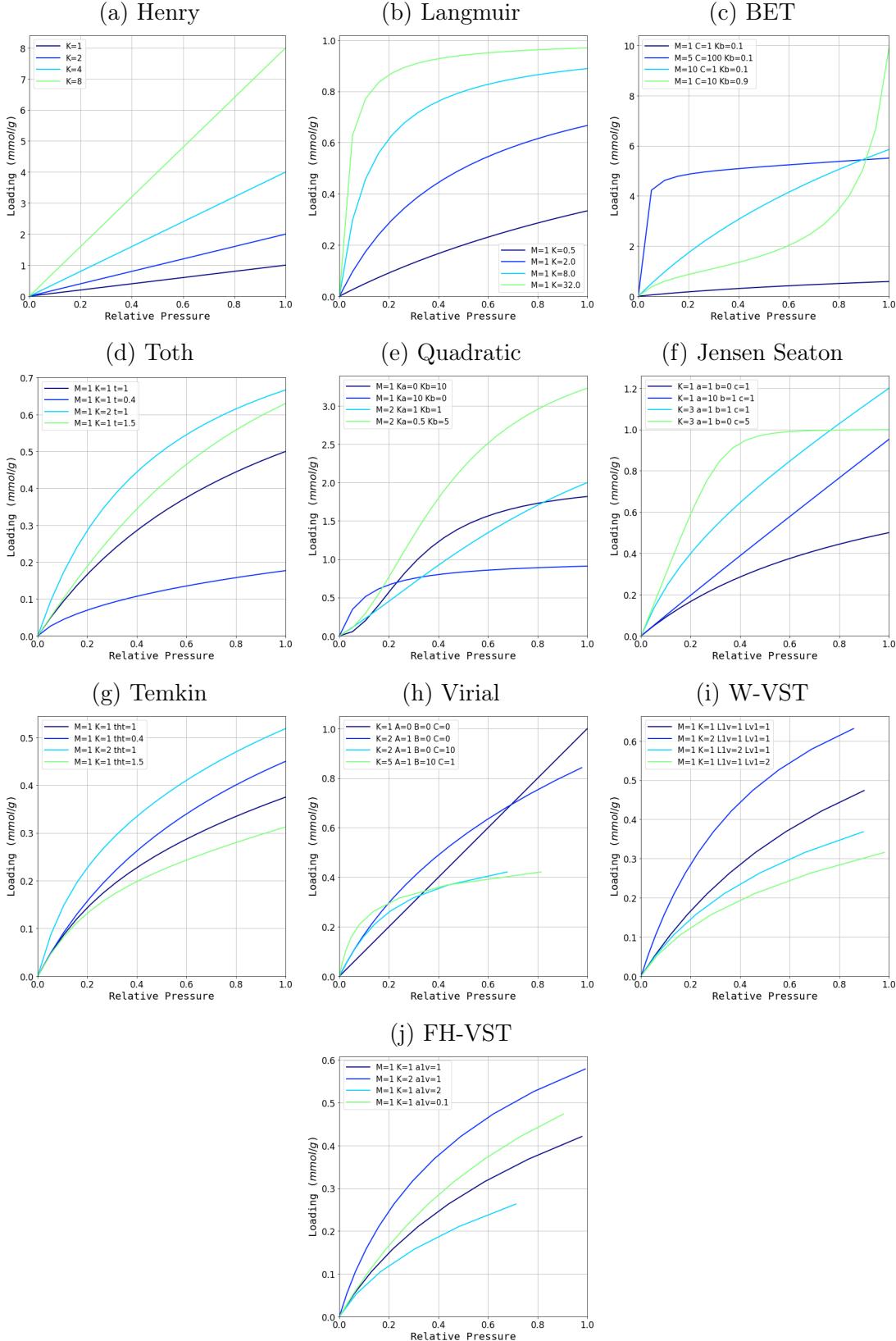


Figure 1.1.: Examples of models

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It is derived from the Gibbs equation, by substituting a two dimensional analogue to the ideal gas law. From a physical standpoint, Henry's law is unrealistic as adsorption sites will saturate at higher pressures. However, the constant K_H , or Henry's constant, can be thought of as a measure of the strength of the interaction of the probe gas with the surface. At very low concentrations of gas there is a theoretical requirement for the applicability of Henry's law. Therefore, most models reduce to [Equation 1.1](#) as $\lim_{p \rightarrow 0} n(p)$.

Langmuir and multi-site Langmuir model

The Langmuir theory,⁽⁸⁾ proposed at the start of the 20th century, states that adsorption takes place on specific sites on a surface, until all sites are occupied. It is derived from a kinetic model of gas adsorption and is based on several assumptions:

- All sites are equivalent and have the same chance of being occupied.
- Each adsorbate molecule can occupy one adsorption site.
- There are no interactions between adsorbed molecules.
- The rates of adsorption and desorption are proportional to the number of sites currently free and currently occupied, respectively.
- Adsorption is complete when all sites are filled.

Using these assumptions we can define rates for both adsorption and desorption. The adsorption rate ([Equation 1.2](#)) will be proportional to the number of sites available on the surface, as well as the number of molecules in the gas, which is given by pressure. The desorption rate, on the other hand, will be proportional to the number of occupied sites and the energy of adsorption ([Equation 1.3](#)). It is also useful to define $\theta = n_a/n_a^m$ as the surface coverage, the number of sites occupied divided by the total sites. At equilibrium, the rate of adsorption and the rate of desorption are equal, therefore the two equations can be combined. The equation can then be arranged to obtain an expression for the loading called the Langmuir model ([Equation 1.6](#)).

$$v_a = k_a p (1 - \theta) \quad (1.2)$$

$$v_d = k_d \theta \exp\left(-\frac{E}{RT}\right) \quad (1.3)$$

$$v_a = v_d \quad (1.4)$$

$$k_a p (1 - \theta) = k_d \theta \exp\left(-\frac{E}{RT}\right) \quad (1.5)$$

$$n_a(p) = n_a^m \frac{Kp}{1 + Kp} \quad (1.6)$$

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The Langmuir constant K is the product of the individual desorption and adsorption constants k_a and k_d and exponentially related to the energy of adsorption $\exp(-E/RT)$.

A common extension to the Langmuir model is to consider the experimental isotherm to be the sum of several Langmuir-type isotherms, each with specific maximum coverage and affinities. The underlying assumption is that the adsorbent has several distinct types of homogeneous adsorption sites and a Langmuir equation is used for each. This is particularly applicable in cases where the structure of the adsorbent suggests that different types of sites are present, such as in crystalline materials of variable chemistry like zeolites and MOFs. The resulting isotherm equation is:

$$n_a(p) = \sum_i n_{a,i}^m \frac{K_i p}{1 + K_i p} \quad (1.7)$$

In practice, only up to three adsorption sites are usually considered.

BET model

The BET model⁽⁹⁾ assumes that adsorption takes place on the surface of the material in incremental layers according to several assumptions:

- The adsorption sites are equivalent, and therefore the surface is heterogeneous.
- There are no lateral interactions between adsorbed molecules.
- The adsorption takes place in layers, with adsorbed molecules acting as sites for the next layer.

A particular surface percentage θ_x is occupied with x layers. For each layer at equilibrium, the adsorption and desorption rates must be equal. We can then apply the Langmuir theory for each layer as presented in Table [Table 1.1](#). We can assume that the adsorption energy of a molecule on the second and higher layers is just the condensation energy of the adsorbent $E_{i>1} = E_L$. Since we are assuming that all layers beside the first have the same properties, we can also define $g = k_{d_2} k_{a_2} = k_{d_3} k_{a_3} = \dots$.

The coverage for each layer θ can now be expressed in terms of θ_0 .

$$\theta_i = \left[p \frac{k_{a_1}}{k_{d_1}} \exp\left(-\frac{E_1}{RT}\right) \right] x^{i-1} \theta_0 \quad (1.8)$$

where

$$x = \frac{p}{g} \exp\left(-\frac{E_L}{RT}\right) \quad (1.9)$$

A constant C may be defined such that:

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Table 1.1.: Derivation of the BET method applied for, each adsorbed layer

All layers	Re-arranged
$k_{a_1}p\theta_0 = k_{d_1}\theta_1 \exp\left(-\frac{E_1}{RT}\right)$	$p\theta_0 = \frac{k_{d_1}}{k_{a_1}}\theta_1 \exp\left(-\frac{E_1}{RT}\right)$
$k_{a_2}p\theta_1 = k_{d_2}\theta_2 \exp\left(-\frac{E_2}{RT}\right)$	$p\theta_1 = g\theta_2 \exp\left(-\frac{E_L}{RT}\right)$
$k_{a_3}p\theta_2 = k_{d_3}\theta_3 \exp\left(-\frac{E_3}{RT}\right)$	$p\theta_2 = g\theta_3 \exp\left(-\frac{E_L}{RT}\right)$
\vdots	\vdots
$k_{a_i}p\theta_{i-1} = k_{d_i}\theta_i \exp\left(-\frac{E_i}{RT}\right)$	$p\theta_{i-1} = g\theta_i \exp\left(-\frac{E_L}{RT}\right)$

$$C = \frac{k_{a_1}}{k_{d_1}}g \exp\left(\frac{E_1 - E_L}{RT}\right) \quad (1.10)$$

$$\theta_i = Cx^i\theta_0 \quad (1.11)$$

For all the layers, the equations can be summed:

$$\frac{n}{n_m} = \sum_{i=1}^{\infty} i\theta^i = C \sum_{i=1}^{\infty} ix^i\theta_0 \quad (1.12)$$

and since

$$\theta_0 = 1 - \sum_1^{\infty} \theta_i \sum_{i=1}^{\infty} ix^i = \frac{x}{(1-x)^2} \quad (1.13)$$

Then we obtain the BET equation:

$$n_a(p) = n_a^m \frac{C(p/p_0)}{(1-p/p_0)[1-(p/p_0)+C(p/p_0)]} \quad (1.14)$$

The BET constant C is a measure of the interaction with the adsorption surface and can be seen to influence the “knee” a BET-type isotherm has at low pressure, before the statistical monolayer formation.

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Toth model

The Toth model is an empirical modification to the Langmuir equation ([Equation 1.6](#)) which introduces a power parameter for the denominator leading to the following formula:

$$n_a(p) = n_a^m \frac{Kp}{[1 + (Kp)^t]^{1/t}} \quad (1.15)$$

The parameter t is a measure of the system heterogeneity. Thanks to this additional parameter, the Toth equation can accurately describe a large number of adsorbent/adsorbate systems and, due to its correct behaviour in both the low and high pressure limits, is recommended as the fitting isotherms of many adsorbents such as hydrocarbons, carbon oxides, hydrogen sulphide and alcohols on activated carbons and zeolites.

Temkin model

The Temkin adsorption isotherm, ⁽¹⁰⁾ like the Langmuir model, considers a surface with n_a^m identical adsorption sites, but takes into account adsorbate- adsorbate interactions by assuming that the heat of adsorption is a linear function of the coverage. This expression for the Temkin isotherm is derived using a mean-field argument and uses an asymptotic approximation to obtain an explicit equation for the loading. ⁽¹¹⁾

$$n_a(p) = n_a^m \frac{Kp}{1 + Kp} + n_a^m \theta \left(\frac{Kp}{1 + Kp} \right)^2 \left(\frac{Kp}{1 + Kp} - 1 \right) \quad (1.16)$$

Here, n_a^m and K have the same physical meaning as in the Langmuir model. The additional parameter θ describes the strength of the adsorbate-adsorbate interactions ($\theta < 0$ for attractions).

Jensen-Seaton model

When modelling adsorption in micropores, a requirement was highlighted by Jensen and Seaton in 1996⁽¹²⁾ that at sufficiently high pressures the adsorption isotherm should not reach a horizontal plateau corresponding to saturation but that this asymptote should continue to rise due to the compression of the adsorbate in the pores. They developed a semi-empirical equation to describe this phenomenon based on a function that interpolates between two asymptotes: the Henry's law asymptote at low pressure and an asymptote reflecting the compressibility of the adsorbate at high pressure.

$$n(p) = K_H p \left(1 + \frac{K_H p}{[a(1+bp)]^c} \right)^{(-1/c)} \quad (1.17)$$

Here K_H is the Henry constant, b is the compressibility of the adsorbed phase and c an empirical constant.

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The equation can be used to model both absolute and excess adsorption as the pore volume can be incorporated into the definition of b , although this can lead to negative adsorption slopes for the compressibility asymptote. This equation has been found to provide a better fit for experimental data from microporous solids than the Langmuir or Toth equation, in particular for adsorbent/adsorbate systems with high Henry's constants where the amount adsorbed increases rapidly at relatively low pressures and then slows down dramatically.

Quadratic model

The quadratic adsorption isotherm⁽¹³⁾ exhibits an inflection point. The loading is convex at low pressures but changes concavity as it saturates, yielding an S-shape. The S-shape can be explained by adsorbate-adsorbate attractive forces; the initial convexity is due to a cooperative effect of adsorbate-adsorbate attractions aiding in the recruitment of additional adsorbate molecules.

$$n(p) = n_a^m \frac{(K_a + 2K_bp)p}{1 + K_{ap} + K_{bp}^2} \quad (1.18)$$

The parameter K_a can be interpreted as the Langmuir constant; the strength of the adsorbate-adsorbate attractive forces is embedded in K_b .

Virial model

A virial isotherm model attempts to fit the measured data to a factorized exponent relationship between loading and pressure.⁽¹⁴⁾

$$p = n \exp(K_1 n^0 + K_2 n^1 + K_3 n^2 + K_4 n^3 + \dots + K_i n^{i-1}) \quad (1.19)$$

It has been applied with success to describe the behaviour of standard as well as supercritical isotherms. The factors are usually empirical, although some relationship with physical properties can be determined: the first constant is related to the Henry constant at zero loading, while the second constant is a measure of the interaction strength with the surface.

$$K_1 = -\ln K_{H,0} \quad (1.20)$$

In practice, besides the first constant, only 2-3 factors are used.

Vacancy solution theory models

As a part of the Vacancy Solution Theory (VST) family of models, it is based on concept of a "vacancy" species, denoted v , and assumes that the system consists of a mixture of these vacancies and the adsorbate.

The VST model is defined as follows:

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- A vacancy is an imaginary entity defined as a vacuum space which acts as the solvent in both the gas and adsorbed phases.
- The properties of the adsorbed phase are defined as excess properties in relation to a dividing surface.
- The entire system including the adsorbent are in thermal equilibrium however only the gas and adsorbed phases are in thermodynamic equilibrium.
- The equilibrium of the system is maintained by the spreading pressure which arises from a potential field at the surface

It is possible to derive expressions for the vacancy chemical potential in both the adsorbed phase and the gas phase, which when equated give the following equation of state for the adsorbed phase:

$$\pi = -\frac{R_g T}{\sigma_v} \ln y_v x_v \quad (1.21)$$

where y_v is the activity coefficient and x_v is the mole fraction of the vacancy in the adsorbed phase. This can then be introduced into the Gibbs equation to give a general isotherm equation for the Vacancy Solution Theory where K_H is the Henry's constant and $f(\theta)$ is a function that describes the non-ideality of the system based on activity coefficients:

$$p = \frac{n_{ads}}{K_H} \frac{\theta}{1-\theta} f(\theta) \quad (1.22)$$

The general VST equation requires an expression for the activity coefficients. The Wilson⁽¹⁵⁾ equation can be used, which expresses the activity coefficient in terms of the mole fractions of the two species (adsorbate and vacancy) and two constants Λ_{1v} and Λ_{1v} . The equation becomes:

$$p = \left(\frac{n_{ads}}{K_H} \frac{\theta}{1-\theta} \right) \left(\Lambda_{1v} \frac{1 - (1 - \Lambda_{1v})\theta}{\Lambda_{1v} + (1 - \Lambda_{1v})\theta} \right) \exp \left(- \frac{\Lambda_{1v}(1 - \Lambda_{1v})\theta}{1 - (1 - \Lambda_{1v})\theta} - \frac{(1 - \Lambda_{1v})\theta}{\Lambda_{1v} + (1 - \Lambda_{1v})\theta} \right) \quad (1.23)$$

Cochran⁽¹⁶⁾ developed a simpler, three parameter equation based on the Flory–Huggins equation for the activity coefficient. The equation for then becomes:

$$p = \left(\frac{n_{ads}}{K_H} \frac{\theta}{1-\theta} \right) \exp \frac{\alpha_{1v}^2 \theta}{1 + \alpha_{1v} \theta} \quad \text{where} \quad \alpha_{1v} = \frac{\alpha_1}{\alpha_v} - 1 \quad (1.24)$$

Here α_1 and α_v are the molar areas of the adsorbate and the vacancy respectively.

1.3.2. Specific surface area and pore volume calculations

As adsorption takes place on the surface, isotherms measured on porous materials are uniquely suited for the determination of the accessible area of the void space present inside the material structure or external area of fine powders. pyGAPS comes with several common methods used to determine surface area, some with theoretical basis like the IUPAC-recommended BET method and some empirical, such as the t-plot method.

BET surface area

The BET method⁽⁹⁾ for determining surface area is the recommended IUPAC method⁽¹⁷⁾ to calculate the surface area of a porous material. It is generally applied on isotherms obtained through N₂ adsorption at 77 K, although other adsorbates (Ar at 77 K or 87 K, Kr at 77 K, CO₂ at 293 K) have been used. In principle, any probe with an adsorption behaviour which can be described through the BET equation in the low pressure regime can be used.

As previously mentioned, the method assumes that adsorption takes place in incremental layers according to the BET model (section 1.3.1). Even if the adsorbent is porous, the initial amount adsorbed (usually between 0.05–0.4 p/p_0) can be described through the equation written in its linear form:

$$\frac{p/p_0}{n_{ads}(1 - p/p_0)} = \frac{1}{n_m C} + \frac{C - 1}{n_m C} (p/p_0) \quad (1.25)$$

If we plot the isotherm points as $(p/p_0)/n_{ads}(1 - p/p_0)$ versus p/p_0 , a linear region can usually be found. The slope and intercept of this line can then be used to calculate n_m , the amount adsorbed at the statistical monolayer, as well as C , the BET constant.

$$n_m = \frac{1}{s + i} \quad C = \frac{s}{i} + 1 \quad (1.26)$$

From the BET monolayer capacity, the specific surface area can be calculated if the area taken up by one of the adsorbate molecules on the surface is known. The calculation uses the following equation together with Avogadro's number:

$$a_{BET} = n_m A_N \sigma \quad (1.27)$$

While commonly used for surface area determination, the BET area should be used with care, as the assumptions made in its calculation may not hold. To augment the validity of the BET method, Rouquerol⁽⁷⁾ proposed several checks to ensure that the selected BET region is valid:

- The BET (C) obtained should be positive;

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- In the corresponding Rouquerol plot where $n_{ads}(1 - p/p_0)$ is plotted with respect to p/p_0 , the points chosen for BET analysis should be strictly increasing;
- The loading at the statistical monolayer should be situated within the limits of the BET region.

All these checks are implemented in pyGAPS. Regardless, the BET surface area should still be interpreted carefully. Since adsorption takes place on the pore surface, microporous materials which have pores of similar or smaller size as the probe molecule used will not give a realistic surface area since in the micropore range it is difficult to separate pore condensation behaviour from multilayer adsorption. Furthermore, the cross-sectional area of the molecule on the surface cannot be guaranteed. For example, nitrogen has been known to adopt a different conformation on the surface of some materials due to inter-molecular forces, which effectively lowers its cross-sectional area.⁽⁷⁾

In pyGAPS, starting from an isotherm object, it is easy to calculate the BET area by using the code in Listing 1.3. The framework automatically applies the Rouquerol rules to find the optimum pressure range and returns the results as a dictionary. The `verbose =True` option prints a short text with all the calculation variables as well as graphing the BET and Rouquerol plots (Figure 1.2). The user can override automatic pressure range selection by using the range parameter (`limits=(0.05, 0.3)`).

Listing 1.3: Calculating a BET area

```
1 area_dict = pygaps.area_BET(isotherm, verbose=True)
```

```
BET surface area: a = 1277 m2/g
Minimum pressure point chosen is 0.005 and maximum is 0.034
The slope of the BET fit: s = 76.344
The intercept of the BET fit: i = 0.052
BET constant: C = 1463
Amount for a monolayer: n = 0.01309 mol/g
```

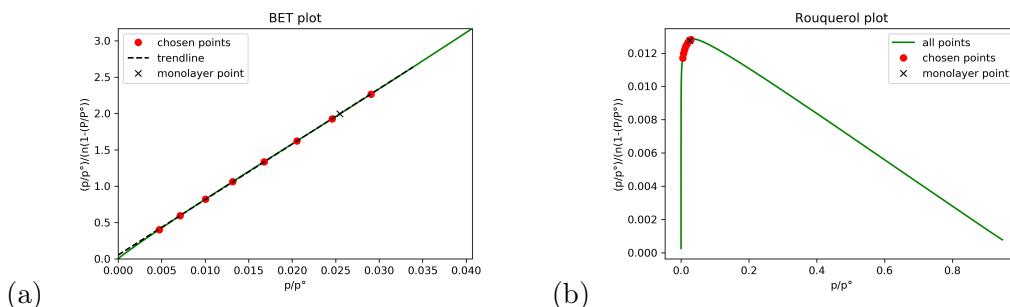


Figure 1.2.: Output from the BET area function (a) the BET plot showing the selected points for fitting the equation, as well as the location of the statistical monolayer and (b) the Rouquerol plot for this calculation.

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Langmuir surface area

The Langmuir equation ([Equation 1.6](#)) can be also be expressed in a linear form by rearranging it as:

$$\frac{p}{n} = \frac{1}{Kn_m} + \frac{p}{n_m} \quad (1.28)$$

Assuming the data can be fitted with a Langmuir model, by plotting p/n against pressure, a straight line will be obtained. The slope and intercept of this line can then be used to calculate n_m , the amount adsorbed at the monolayer, as well as K , the Langmuir constant.

$$n_m = \frac{1}{s} \quad K = \frac{1}{i * n_m} \quad (1.29)$$

The surface area can then be calculated by using the monolayer capacity in a manner analogous to the BET surface area method.

$$a_{Langmuir} = n_m A_N \sigma \quad (1.30)$$

The Langmuir method for determining surface area assumes that adsorption takes place until all active sites on the material surface are occupied, or until monolayer formation in the case of complete surface coverage. As most adsorption processes (except chemisorption) don't follow this behaviour, it is important to regard the Langmuir surface area as an estimate.

As with the BET area, the Langmuir area is calculated by using the code in [Listing 1.4](#). The framework will alert the user if the correlation is not linear in the selected range. Here the `verbose=True` option prints a short text with all the calculation variables and the graphs the Langmuir plot as seen in [Figure 1.3a](#). If desired the user can override automatic pressure range selection as seen in the second example in [Listing 1.4](#).

Listing 1.4: Calculating a Langmuir area

```
1 area_dict = pygaps.area_langmuir(isotherm, verbose=True)
```

```
| WARINING The correlation is not linear!
```

```
1 area_dict = pygaps.area_langmuir(isotherm,
2                               limits=(0.05, 0.3),
3                               verbose=True)
```

```
| Langmuir surface area: a = 415 m2/g
| Minimum pressure point chosen is 0.0 and maximum is 0.194
| The slope of the Langmuir line: s = 234.968
| The intercept of the Langmuir line: i = 1.607
| The Langmuir constant is: K = 146
| Amount for a monolayer: n = 0.00426 mol/g
```

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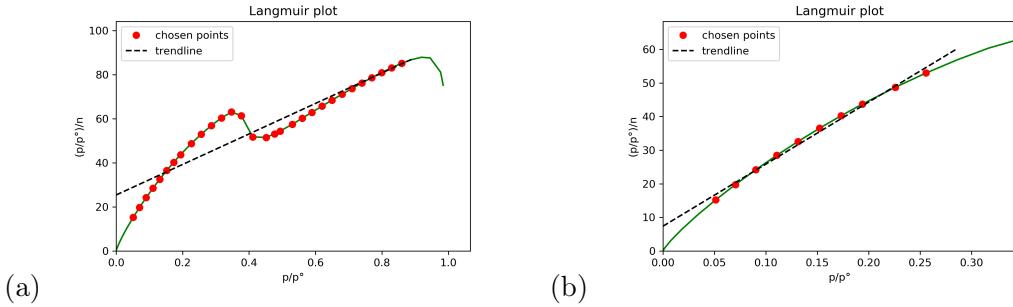


Figure 1.3.: Output from the Langmuir area function (a) the Langmuir plot showing the automatic fitting attempt which generates a warning and (b) a manually selected pressure range for the Langmuir plot.

Ideal isotherms or thickness functions

The initial part of an isotherm (the Henry regime) can be seen to be very dependent on the interactions between the adsorbate and the surface. However, the subsequent layers are less influenced by the material and can often be assumed, like in the BET model, to have an energy of adsorption identical to the enthalpy of liquefaction of the bulk liquid and therefore, their formation depends essentially only on the partial pressure.

With this assumption, several studies have been focused on obtaining an “ideal” isotherm of adsorption on a non-porous material which can then, if the cross-sectional area of the molecule is known, be transformed in a function capable of predicting the multilayer thickness as a function of pressure. This kind of empirical function, also referred to as a *thickness function* or *t-curve*, can then be used as an alternative method for surface area determination, as explained in the next section. These curves are also used in the classical methods for calculating mesoporous size distributions. It is important to clarify that the function is only applicable for a single adsorbent and a single temperature.

Several common thickness functions have been implemented in pyGAPS, applicable for nitrogen at 77K such as the Halsey⁽¹⁸⁾ (Equation 1.31) and the Harkins and Jura⁽¹⁹⁾ (Equation 1.32) curve.

$$t_{Halsey} = 0.354 \left(\frac{-5}{\log(p/p_0)} \right)^{1/3} \quad (1.31)$$

$$t_{Harkins\&Jura} = \left(\frac{0.1399}{0.034 - \log_{10}(p/p_0)} \right)^{1/2} \quad (1.32)$$

check
equations

These t-curves are selected by name as parameters in the functions that use them. The user can also define their own t-curve as a function and pass it as a parameter. An example is shown in Listing 1.5 in the t-plot section.

t-plot Method

The t-plot method is an empirical method, developed as a tool to determine the surface area of porous materials, which can also be used for other calculations, such as external pore area and micropore volume calculations.⁽²⁰⁾ A plot is constructed, where the isotherm loading data is plotted versus the ideal thickness of the adsorbate layer, obtained through the a t-curve ([section 1.3.2](#)). It stands to reason that, in the case when the experimentally measured loading follows the model, a straight line will be obtained with its intercept through the origin. However, since in most cases there are differences between adsorption in the pores and ideal surface adsorption, the t-plot will deviate and form features which can be analysed to describe the material characteristics.

- A sharp vertical deviation will indicate condensation in a type of mesopore structure.
- A gradual slope will indicate adsorption on a specific surface.

The slope of the linear section can be used to calculate the area where adsorption is taking place. If the linear region occurs at low loadings, it will represent the total surface area of the material. If at the end of the curve, it will instead represent adsorption on the external surface area of the sample. The formula to calculate the area is presented in [Equation 1.33](#), where ρ_l is the liquid density of the adsorbate at experimental conditions.

$$a_{surface} = \frac{sM_m}{\rho_l} \quad (1.33)$$

If the region selected is after a vertical deviation, the intercept of the line will no longer pass through the origin. This intercept can be used to calculate the volume of the filled pore through the following equation:

$$V_{ads} = \frac{iM_m}{\rho_l} \quad (1.34)$$

Since the t-plot method is comparing the experimental isotherm with an ideal model, care must be taken to ensure that the t-curve is an accurate representation of the thickness of the adsorbate multilayers on the surface of the adsorbent. Since there is no such thing as a universal thickness curve, care must be taken when selecting a thickness model to ensure that it is applicable to both the material and the adsorbate. Also, features on the t-plot found at loadings lower than the monolayer thickness do not have any physical meaning.

In pyGAPS, when the function is called without any parameters except an isotherm, the framework will attempt to find plateaus in the data and automatically fit them with a straight line, returning a dictionary with the slope, intercept and calculated pore volume and specific area for each linear region found. As an example, the first function

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Listing 1.5: Generating a t-plot

```

1 # using automatic region detection
2 pygaps.t_plot(isotherm, verbose=True)
3
4 # specifying a manual region
5 pygaps.t_plot(isotherm, limits=(0.3,0.44), verbose=True)
6
7 # using the Halsey thickness curve
8 pygaps.t_plot(isotherm, thickness_model='Halsey', verbose=True)
9
10 # defining a custom t-curve to use in the t-plot
11 def carbon_model(relative_p):
12     return 0.88*(relative_p**2) + 6.45*relative_p + 2.98
13
14 pygaps.t_plot(isotherm, thickness_model=carbon_model, verbose=True)

```

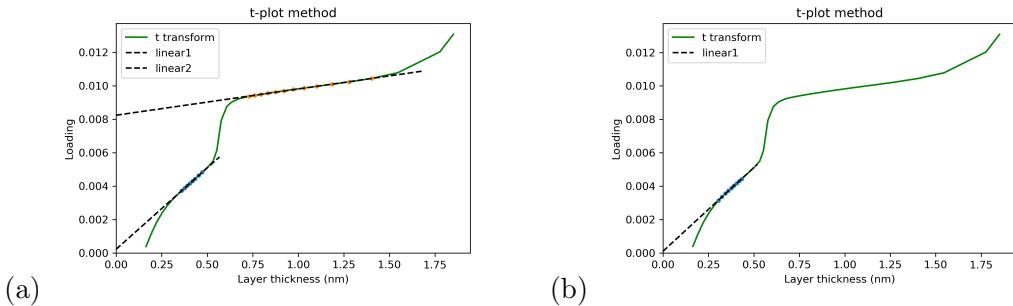


Figure 1.4.: Output from the t-plot method function (a) an automatically obtained t-plot with the calculated fit regions and (b) a manually selected range for the t-plot.

in Listing 1.5 will generate the graph in Figure 1.4a. The isotherm in this example is measured on a sample of MCM-41.

The first linear region in Figure 1.4a can be attributed to adsorption on the mesopore surface, while the second one represents adsorption on the available surface after mesopore filling. Therefore, the surface area values calculated for the first and second region correspond to the area of the mesopores and the external particle area, respectively. As only one pore filling event occurs, the pore volume calculated for the second region gives us the mesopore volume. We can obtain a more accurate result for the surface area by fitting the first linear region to a zero intercept through manual region selection, as shown in the second example in Listing 1.5.

Finally, the framework allows for the thickness model to be substituted with an user-provided function which will be used for the t-plot, as mentioned before in section 1.3.2. Usage of a carbon black-type thickness curve is presented in the last example in Listing 1.5.

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α_s Method

In order to extend the t-plot analysis with other adsorbents and non-standard thickness curves, the α_s method was devised.⁽²¹⁾ Instead of attempting to find an ideal isotherm that describes the thickness of the adsorbed layer, a reference isotherm is used. This isotherm is measured on a non-porous version of the same material, assumed to have identical surface characteristics. The dimensionless α_s values are obtained from this isotherm by dividing the loading values by the amount adsorbed at a specific relative pressure, usually taken as $p/p_0 = 0.4$ since nitrogen hysteresis loops theoretically close at this point.

$$\alpha_s = \frac{n_a}{n_{0.4}} \quad (1.35)$$

The analysis then proceeds as in the t-plot method, with the same explanation for observed features. The only difference is that the surface area calculation from linear regions observed uses the known specific area of the reference material.

$$A = \frac{sA_{ref}}{(n_{ref})_{0.4}} \quad (1.36)$$

The reference isotherm chosen for the α_s method must be a description of the adsorption on a completely non-porous sample of the same material. It is often impossible to obtain such non-porous versions, therefore care must be taken how the reference isotherm is measured.

To generate an α_s -plot in pyGAPS, both an analysis isotherm and a reference isotherm must be supplied as shown in [Listing 1.6](#). In this example, the reference isotherm is measured on non-porous silica. The reference material area can be specified by using the `reference_area` parameter. If not specified, it is automatically calculated by applying the BET method on the reference isotherm.

Listing 1.6: Generating an α_s -plot

```
1 pygaps.alpha_s(isotherm,
2                  reference_isotherm=isotherm_r,
3                  verbose=True)
```

1.3.3. Assessing porosity

Characterization of pore sizes and their distribution in porous materials is often the main goal when performing adsorption experiments. It is therefore important that pyGAPS includes several robust methods for determining pore distribution from isotherm data.

When it comes to porous materials, three kinds of pore sizes have been defined, based on their lengthscales: micropores ($<2\text{ nm}$), mesopores (2 nm to 50 nm), and macropores ($>50\text{ nm}$).

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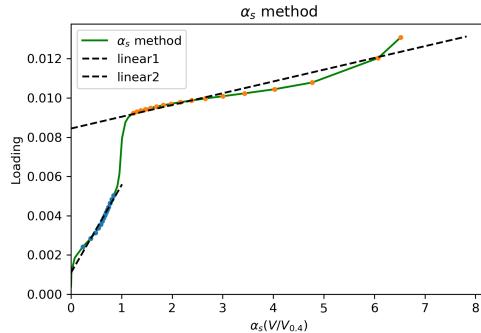


Figure 1.5.: Output from the α_s -plot function showing two automatically fit regions.

Macropores are generally unable to be characterised through adsorption, with methods such as mercury intrusion porosimetry as the standard for pore size distributions at this lengthscale, although other alternatives have been suggested⁽²²⁾ due to the high toxicity of mercury. These methods are therefore outside the scope of this framework.

In the mesopore range, the “classical” methods are usually applied, which are based on the application of Kelvin’s equation pertaining to capillary condensation. This equation calculates the critical pressure at which the fluid completely files a pore of a specific diameter. This equation, applicable to a range of geometries is used in multiple approaches such as the Barrett-Joyner-Halenda (BJH) method or the Dollimore-Heal (DH) method.

For microporous materials, the Kelvin equation, with its assumption of continuous fluid properties and comparable density of the adsorbed state to bulk liquid density breaks down. An atomistic approach is required here, to address the interaction between solid-fluid and fluid-fluid through potential functions. The Horvath-Kawazoe or HK method is often used, and it is implemented in pyGAPS.

Finally, methods based on density functional theory (DFT) and derivations such as non-local DFT (NLDFT) and quenched solid state DFT (QSDFT) should be mentioned, as they can be used for multiscale (micropore and mesopore) characterisation. These methods rely on *in-silico* simulation of isotherms on a range of pore sizes, which can then be collated in a so-called *DFT kernel*, able to be used in decomposition of a experimental isotherm to obtain a pore size distribution. While the generation of DFT kernels is outside the scope of the pyGAPS framework, it is able to use user-provided kernels to fit adsorption isotherms, and comes with a basic kernel for N₂ adsorption at 77 K on carbon slit pores.

It should be noted that all methods here described require knowledge of the pore geometry and depend on the material having pores which conform to a well-defined shape. Real adsorbents usually have interconnected networks of irregular pores, which the ideal pores used in these models merely approximate.

Mesoporous size distribution

The Kelvin equation Since the Kelvin equation is the basis of both the BJH and DH methods its theory and its implementation will be described here. The original

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form of the equation ([Equation 1.37](#)) gives the dependence of pressure on the radius of curvature of a meniscus in a pore r by means of surface tension γ , molar liquid volume, here expressed as $v_l = M_m/\rho_l$ and the fluid contact angle with the surface θ . The fluid is often assumed to be fully wetting, with $\theta = 0$ and $\cos \theta = 1$.

$$\ln\left(\frac{p}{p_0}\right) = -\frac{\gamma M_m}{\rho_l RT} \frac{2 \cos \theta}{r} \quad (1.37)$$

To apply the Kelvin equation to different types of pore systems, the generalized form presented in [Equation 1.38](#) is used. It replaces the meniscus radius by a mean radius of curvature r_m .

$$\ln\left(\frac{p}{p_0}\right) = -\frac{\gamma M_m}{\rho_l RT} \frac{2}{r_m} \quad (1.38)$$

The mean radius of curvature is defined through the two principal radii of the curved interface.

$$\frac{1}{r_m} = \frac{1}{2} \left(\frac{1}{r_1} + \frac{1}{r_2} \right) \quad (1.39)$$

The relationship of the kelvin radius r_m to the actual pore radius is more subtle, as it depends on pore geometry and the filling state of the pore.⁽²³⁾ If considering a cylindrical pore open at both ends, the radius reduces to the original Kelvin equation during the desorption phase, and takes other values with different combinations of parameters as can be seen in [Table 1.2](#).

Table 1.2.: Relationship between pore geometry, pore filling and meniscus geometry

Pore geometry	Pore filling	
	Adsorption	Desorption
slit	cylindrical	concave
cylinder	cylindrical	spherical
sphere	spherical	spherical

According to Rouquerol,⁽⁷⁾ in adopting this approach, it is assumed that:

- The Kelvin equation is applicable over the pore range (mesopores). Therefore in pores which are below a certain size (around 2.5 nm), the granularity of the liquid-vapour interface becomes too large for classical bulk methods to be applied.
- The meniscus curvature is controlled by the pore size and shape. Ideal shapes for the curvature are assumed.

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- Pores are rigid and of well defined shape. Their geometry considered to be invariant across the entire adsorbate.
- The filling/emptying of each pore does not depend on its location.
- Adsorption on the pore walls is not different from surface adsorption.

The Barrett, Joyner and Halenda (BJH) method The BJH method for calculating pore size distribution is based on a classical description of the adsorbate behaviour in the adsorbent pores.⁽¹⁾ Under this method, the adsorbate is adsorbing on the pore walls in a predictable way, and decreasing the apparent pore volume until condensation takes place, filling the entire pore. The critical radius is a sum of two radii, the adsorbed layer thickness, which can be modelled by a thickness model (such as Halsey, Harkins & Jura or similar as presented in section 1.3.2) and a critical radius model for condensation/evaporation, based on a form of the Kelvin equation.

$$r_p = t + r_k \quad (1.40)$$

The original model uses the desorption curve as a basis for calculating pore size distribution. Between two points of the curve, the volume desorbed can be described as the volume contribution from pore evaporation and the volume from layer thickness decrease as per Equation 1.40. The computation is done cumulatively, starting from the filled pores and calculating for each point the volume adsorbed in a pore from the following equation:

$$V_p = \left(\frac{\bar{r}_p}{\bar{r}_k + \Delta t_n} \right)^2 \left(\Delta V_n - \Delta t_n \sum_{i=1}^{n-1} \Delta A_p + \Delta t_n \bar{t}_n \sum_{i=1}^{n-1} \frac{\Delta A_p}{\bar{r}_p} \right) \quad (1.41)$$

where

$$A = 2\Delta V_p / r_p \quad (1.42)$$

here

- ΔA_p is the area of the pores
- ΔV_p is the adsorbed volume change between two points
- \bar{r}_p is the average pore radius calculated as a sum of the kelvin radius and layer thickness of the pores at pressure p between two measurement points
- \bar{r}_k is the average kelvin radius between two measurement points
- \bar{t}_n is the average layer thickness between two measurement points

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- Δt_n is the average change in layer thickness between two measurement points

Then, by plotting $\Delta V/(2 * \Delta r_p)$ versus the width of the pores calculated for each point, the pore size distribution can be obtained.

In order to calculate the

Listing 1.7: PSD using the BJH method

```

1 result_dict = pygaps.mesopore_size_distribution(
2     charact_iso,
3     psd_model='BJH',
4     verbose=True
5 )

```

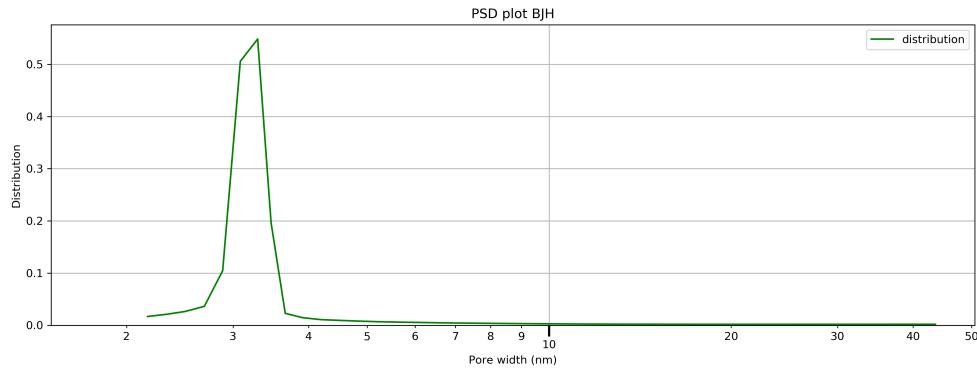


Figure 1.6.: BJH pore size distribution

The Dollimore-Heal (DH) method The DH or Dollimore-Heal method⁽²⁴⁾ of calculating pore size distribution is an extension of the BJH method which takes into account the geometry of the pores by introducing a length component.

Like the BJH method, it is based on a classical description of the adsorbate behaviour in the adsorbent pores.

$$V_p = \left(\frac{\bar{r}_p}{\bar{r}_k + \Delta t_n} \right)^2 \left(\Delta V_n - \Delta t_n \sum_{i=1}^{n-1} \Delta A_p + 2\pi \Delta t_n \bar{t}_n \sum_{i=1}^{n-1} L_p \right) \quad (1.43)$$

$$A = 2\Delta V_p / r_p \quad (1.44)$$

$$L = \Delta A_p / 2\pi r_p \quad (1.45)$$

Where:

- ΔA_p is the area of the pores
- ΔV_p is the adsorbed volume change between two points

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- \bar{r}_p is the average pore radius calculated as a sum of the kelvin radius and layer thickness of the pores at pressure p between two measurement points
- \bar{r}_k is the average kelvin radius between two measurement points
- \bar{t}_n is the average layer thickness between two measurement points
- Δt_n is the average change in layer thickness between two measurement points

Then, by plotting $\Delta V/(2 * \Delta r_p)$ versus the width of the pores calculated for each point, the pore size distribution can be obtained.

Microporous size distribution

When it comes to micropores (width <2 nm), classical fluid methods stop being viable. Adsorption of molecules in these pores of comparable scale is highly dependent on the surface properties and on guest-host interaction and leads to adsorbate densities often very different than those in the bulk liquid state. In order to model adsorption in such pores, a good description of both solid-fluid and fluid-fluid potential functions is required.

The Horvath-Kawazoe (HK) method The H-K method attempts to describe the adsorption within pores by calculation of the average potential energy for a pore.⁽²⁵⁾ The method starts by assuming the relationship between the gas phase as being:

$$R_g T \ln\left(\frac{p}{p_0}\right) = U_0 + P_a \quad (1.46)$$

Here U_0 is the potential function describing the surface to adsorbent interactions and P_a is the potential function describing the adsorbate-adsorbate interactions. This equation is derived from the equation of the free energy of adsorption at constant temperature where the term $T\Delta S^{tr}(w/w_\infty)$ is assumed to be negligible.

If it is assumed that a Lennard-Jones potential function can describe the interactions between adsorbate and surface molecules, then the two contributions to the total potential can be replaced by the extended function in [Equation 1.47](#).

$$\begin{aligned} RT \ln(p/p_0) &= N_A \frac{n_a A_a + n_A A_A}{2\sigma^4(l-d)} \\ &\times \int_{d/2}^{1-d/2} \left[-\left(\frac{\sigma}{r}\right)^4 + \left(\frac{\sigma}{r}\right)^{10} - \left(\frac{\sigma}{l-r}\right)^4 + \left(\frac{\sigma}{l-r}\right)^4 \right] dx \quad (1.47) \end{aligned}$$

where l is the width of the pore, d defined as $d = d_a + d_A$ is the sum of the diameters of the adsorbate and adsorbent molecules, n_a is number of molecules of adsorbent and A_a and A_A the Lennard-Jones potential constant of the fluid molecule and solid molecule respectively which are defined as

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$$A_a = \frac{6mc^2\alpha_a\alpha_A}{\alpha_a/\varkappa_a + \alpha_A/\varkappa_A} \quad (1.48)$$

and

$$A_a = \frac{3mc^2\alpha_A\varkappa_A}{2} \quad (1.49)$$

Here m is the mass of an electron, α_a and α_A are the polarizability of the adsorbate and adsorbate molecule and \varkappa_a and \varkappa_A the magnetic susceptibility of the adsorbate molecule and adsorbent molecule, respectively.

The HK method is applicable to slit pores, and it can be modified to be extended to cylindrical and spherical pores. It is worth noting that there are several assumptions which limit its applicability:

- The HK method is reliant on knowledge of the properties of the surface atoms. This assumption is true only if the material surface is homogenous. Furthermore, longer range interactions with multiple surface layers are not considered.
- Each pore is modelled as uniform and of infinite length. Materials with varying pore shapes or highly interconnected networks may not give realistic results.
- Only dispersive forces are accounted for. If the adsorbate-adsorbent interactions have other specific contributions, the Lennard-Jones potential function will not be an accurate description of pore environment.
- It does not have a description of capillary condensation. This means that the pore size distribution can only be considered accurate up to a maximum of 5 nm.

The pyGAPS framework contains the required physical properties for the most commonly used adsorbates in its database, as well as properties from literature for several materials: the original parameters developed by Horvath and Kawazoe for a carbon surface ⁽²⁵⁾ and the oxide surface parameters published by Saito and Foley. ⁽²⁶⁾ The user can provide custom dictionary of these parameters when calling the function as can be seen in the second example in [Listing 1.8](#).

Multiscale computational methods

DFT theory emerged as a rigorous description of molecular adsorption in pores. ⁽²⁾ It calculates the properties of the fluid directly from the forces acting between constituent molecules through a statistical mechanical approach. Latter developments, like non-local DFT (NLDFT), ⁽³⁾ which makes an account for short range molecule correlation and therefore for the changes in the density profile around the pore walls, and quenched solid state DFT (QSDFT), ⁽²⁷⁾ which allows for heterogeneity of pore walls to be incorporated in the model, have improved the accuracy of the method.

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Listing 1.8: Using the HK method for PSD

```

1 # Calling the HK micropore method with the
2 # Saito-Foley oxide surface parameters
3 result_dict = pygaps.micropore_size_distribution(
4     isotherm,
5     psd_model='HK',
6     adsorbent_model='OxideIon(SF)',
7     verbose=True
8 )
9 # Defining a custom adsorbate parameter dictionary
10 # and using it in the HK method
11 adsorbate_params = {
12     'magnetic_susceptibility': 3.6e-35,
13     'molecular_diameter': 0.3,
14     'polarizability': 1.76e-30,
15     'surface_density': 6.71e+18
16 }
17 result_dict = pygaps.micropore_size_distribution(
18     isotherm,
19     psd_model='HK',
20     adsorbent_model='OxideIon(SF)',
21     adsorbate_model=adsorbate_params,
22     verbose=True
23 )

```

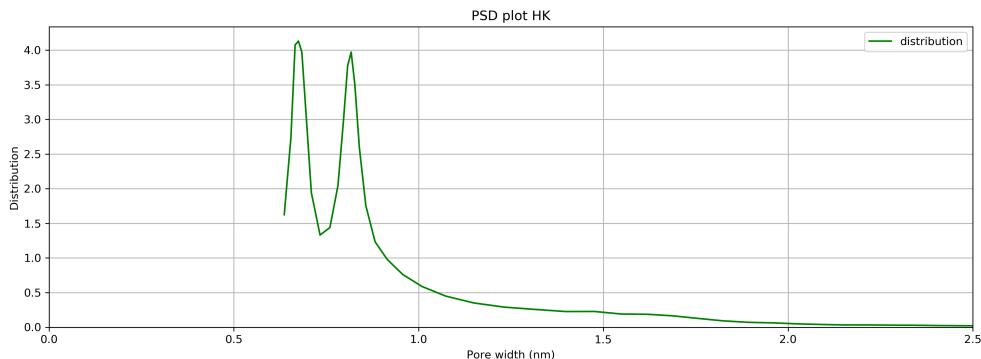


Figure 1.7.: Pore size distribution calculated through the Horvath-Kawazoe method on the UIO-66(Zr) sample

The density functional theory approach can therefore simulate adsorption isotherms on pores of different geometries and sizes. By defining a pore geometry and running the simulation with a range of pore radii, a collection of isotherms is obtained. If an experimental isotherm is through of as a sum of adsorption isotherms in different material pores, then it stands to reason that the preponderence of those pores can be calculated through deconvolution.

As the DFT method can model adsorbate condensation behaviour, as well as micropore

1. Building a framework for adsorption data processing

filling and multilayer adsorption, it can be used for multiscale pore size distribution. The downside is that DFT kernels are temperature, probe, pore-geometry and adsorbent specific and as such are not universally applicable.

The pyGAPS framework can perform isotherm fitting to DFT kernels through the `dft_size_distribution` function. The function takes an `Isotherm` object, then then load the DFT kernel either from disk or from memory and apply a minimization function on the sum of squared differences of the sum of all individual kernel isotherms to generate the contribution of each as per the following equation:

$$f(x) = \sum_{p=p_0}^{p=p_x} \left(n_{p,\text{exp}} - \sum_{w=w_0}^{w=w_y} n_{p,\text{kernel}} X_w \right)^2 \quad (1.50)$$

The user can specify their own kernel in a CSV format, which will be used for the isotherm fitting. Alternatively, a common DFT kernel is included with the framework, which is applicable on nitrogen adsorption on a carbon slit-like pores in the range of 0.4 nm to 10 nm.

Listing 1.9: DFT size distribution in pyGAPS

```
1 result_dict = pygaps.dft_size_distribution(
2     charact_iso,
3     'internal',
4     verbose=True
5 )
```

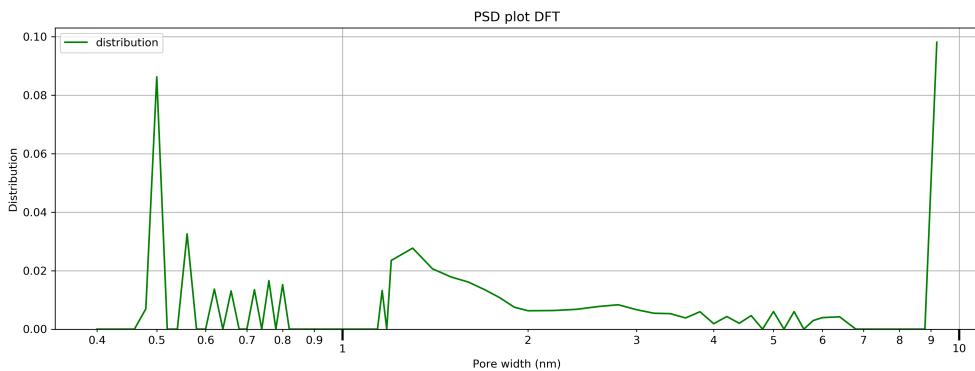


Figure 1.8.: Pore size distribution calculated through the DFT fitting on the Takeda 5A carbon

1.3.4. Predicting multicomponent adsorption

Until now, we have only referred to isotherms pertaining to the adsorption of a single adsorbate. However, besides gas storage, most if not all industrial applications of

1. Building a framework for adsorption data processing

adsorbents involve multiple chemical species undergoing competitive adsorption. Experiments involving several adsorbents are generally difficult and time consuming. There is therefore a requirement to predict such multicomponent systems in order to rapidly screen for potentially interesting separations starting from pure component data.

To this end, the several methods have been devised, with perhaps the most common approach as considering the adsorbed phase as an analogue to a fluid mixture. This method, also known as the ideal adsorbed solution theory (IAST), has been implemented in pyGAPS and will be presented here. Other multicomponent theories such as real adsorbed solution theory (RAST) or the Nitta model exist but usually require more information about specific surface binary activity coefficients to be well suited to a general high throughput approach.

Ideal adsorbed solution theory

The pyGAPS framework includes a modified version of the pyIAST code⁽²⁸⁾ which has been adapted to work with the Isotherm classes. Both model isotherms and real data can be used for IAST, with spreading pressure being calculated through the underlying isotherm model or through interpolation, respectively.

In this case, we fit the experimental data to the available models in pyGAPS which have been presented in [subsection 1.3.1](#), then use the resulting model isotherms for IAST simulations. In order to get a ‘best-fit’ model isotherm, we use the function in [Listing 1.10](#), which fits all available models and selects the one with the lowest residuals between the fitted function and the real data. The isotherms and their best-fitting model is displayed in [Figure 1.9a](#) for the CO₂-N₂ pair and in [Figure 1.10a](#) for the C₃H₈-C₃H₆ pair.

Listing 1.10: Guessing the best model

```
1 model = pygaps.ModelIsotherm.from_pointisotherm(iso, guess_model=True)

Attempting to model using Henry
Model Henry success, rmse is 7.42
Attempting to model using Jensen-Seaton
Modelling using Jensen-Seaton failed
.....
Best model fit is Quadratic
```

For the carbon dioxide separation, we simulate all equilibrium points for the adsorbed and gaseous phases at different concentrations of the two gases at 1 bar. To do this we use the `pygaps.iast_vle()` function which produces an analogue of a vapour-liquid equilibrium at a specified pressure for a binary mixture. The resulting graph of this function can be seen in [Figure 1.10b](#). As expected, the predicted adsorbed mixture is rich in carbon dioxide. Selectivity can also be calculated in a single point, with the value at 15% CO₂ and 1 bar being 16.5.

For the propane-propylene separation, we simulate the selectivity for propane within a pressure range for a 50% mixture of the two gases. It can be seen that there is little

1. Building a framework for adsorption data processing

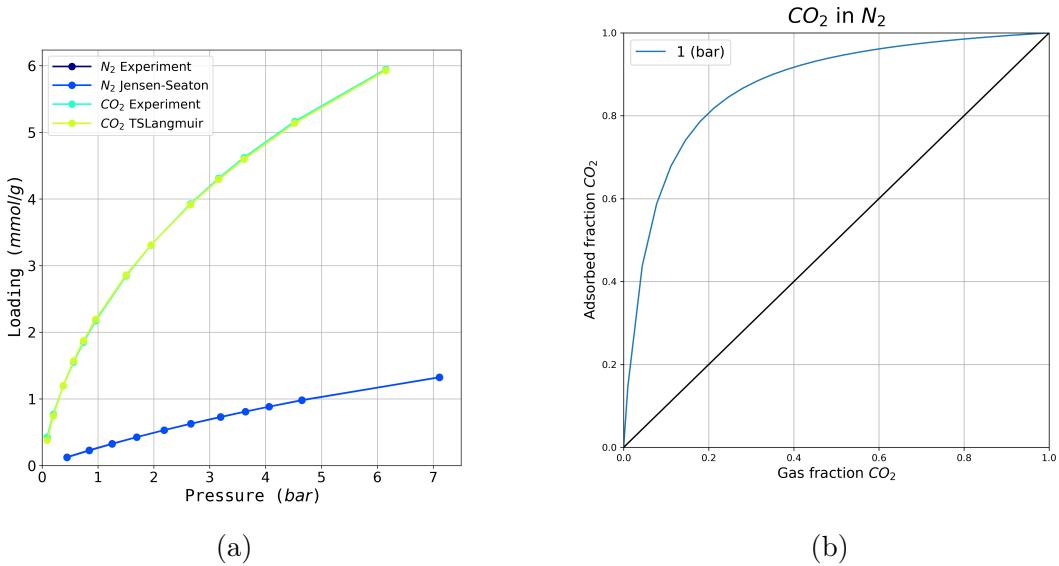


Figure 1.9.: Modelling binary adsorption of CO₂ and N₂: (a) the pure component isotherms and their best fit models and (b) the predicted composition of the gaseous and adsorbed phase for different fractions of CO₂ at 1 bar

or no preference for the unsaturated molecule, though the selectivity increases slightly at pressures above 1 bar.

1.4. Case studies

1.5. Conclusion

1. Building a framework for adsorption data processing

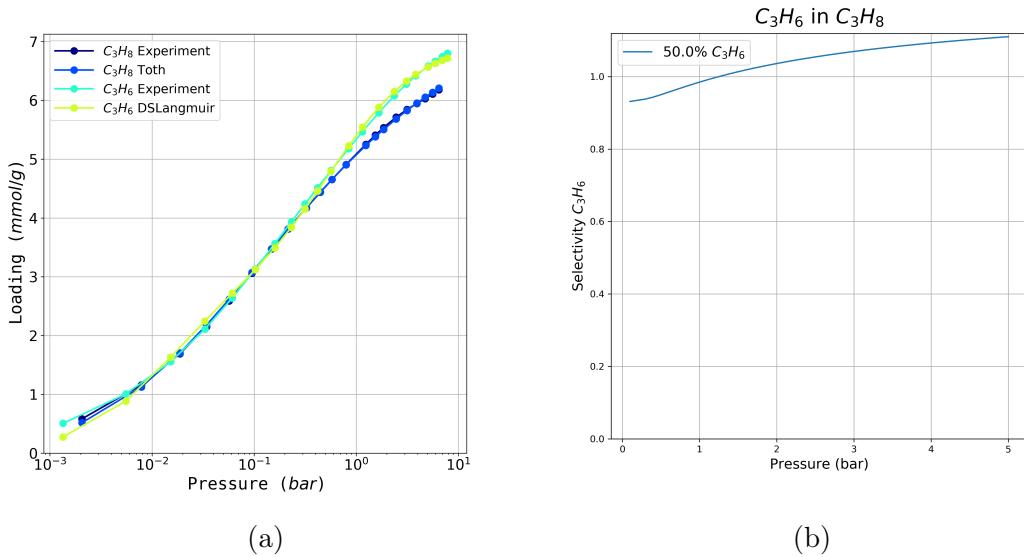


Figure 1.10.: Modelling binary adsorption of a propane-propylene mixture: (a) the pure-component isotherms and their best fit models and (b) the predicted selectivity of propane adsorption of a 50-50% mixture in a range of pressure from 0.1 to 7 bar

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2. Extending bulk analysis of porous compounds through calorimetry

2.1. Introduction

2.2. Literature

Isosteric heat

The isosteric heats are calculated from experimental data using the Clausius-Clapeyron equation as the starting point:

$$\left(\frac{\partial \ln P}{\partial T}\right)_{n_a} = -\frac{\Delta H_{ads}}{RT^2} \quad (2.1)$$

Where ΔH_{ads} is the enthalpy of adsorption. In order to approximate the partial differential, two or more isotherms are measured at different temperatures. The assumption made is that the heat of adsorption does not vary in the temperature range chosen. Therefore, the isosteric heat of adsorption can be calculated by using the pressures at which the loading is identical using the following equation for each point:

$$\Delta H_{ads} = -R \frac{\partial \ln P}{\partial 1/T} \quad (2.2)$$

and plotting the values of $\ln P$ against $1/T$ we should obtain a straight line with a slope of $-\Delta H_{ads}/R$.

The isosteric heat is sensitive to the differences in pressure between the two isotherms. If the isotherms measured are too close together, the error margin will increase. The method also assumes that enthalpy of adsorption does not vary with temperature. If the variation is large for the system in question, the isosteric heat calculation will give unrealistic values.

Even with carefully measured experimental data, there are two assumptions used in deriving the Clausius-Clapeyron equation: an ideal bulk gas phase and a negligible adsorbed phase molar volume. These have a significant effect on the calculated isosteric heats of adsorption, especially at high relative pressures and for heavy adsorbates.

2.3. Method

Gas adsorption isotherms and enthalpies were measured experimentally using a Tian-Calvet type microcalorimeter coupled with a home-made manometric gas dosing system.⁽¹⁾ This apparatus allows the simultaneous measurement of the adsorption isotherm

2. Extending bulk analysis of porous compounds through calorimetry

and the corresponding differential enthalpies. Gas is introduced into the system using a step-by-step method and each dose is allowed to stabilize in a reference volume before being brought into contact with the adsorbent located in the microcalorimeter. The introduction of the adsorbate to the sample is accompanied by an exothermic thermal signal, measured by the thermopiles of the microcalorimeter. The peak in the calorimetric signal is integrated over time to give the total energy released during this adsorption step. At low coverage the error in the signal can be estimated to around $\pm 0.2 \text{ kJ mol}^{-1}$. Around 0.4 g of sample is used in each experiment. For each injection of gas, equilibrium was assumed to have been reached after 90 minutes. This was confirmed by the return of the calorimetric signal to its baseline ($<5 \mu\text{W}$). The gases used for the adsorption were obtained from Air Liquide and were of minimum N47 quality (99.997 % purity).

2.4. Results and discussion

2.4.1. Routine characterization of a MOF sample

When a newly synthesised sample is available, an initial characterisation is often performed to compare the material with previous batches. Adsorption of nitrogen at 77 K is commonly used to verify if predictors such as specific surface area and pore size distribution are consistent with other samples or literature values.

The nitrogen isotherm is first imported in pyGAPS. To obtain the BET area, the `pygaps.area_BET()` method is used with the isotherm object as the parameter and the verbose option, with Figure ?? as the output. It can be seen that the framework has automatically selected the points within the applicable BET region using the checks devised by Rouquerol et al.^(?) to assert method validity. The statistical BET monolayer point is within the selected region, which is one of the checks implemented for method validity. The calculated surface area is $1277 \text{ m}^2/\text{g}$, which is similar to literature values.^(? ?)

The same isotherm is used to calculate the pore size distribution of the UiO-66(Zr) sample. This MOF has octahedral cages surrounded by eight corner tetrahedral cages of 11 and 8 Å respectively. The structure is therefore expected to have only micropores. Two methods are available in pyGAPS for micropore size distributions: a ‘classical’ Horvath-Kawazoe (HK) method,^(?) as well as a DFT fitting routine. The HK method is called by using the function in Listing ???. Here, the surface characteristic parameters determined by Saito and Foley^(?) are to be used, with the framework automatically supplying the parameters for the adsorbed gas.

The DFT fitting is done using the internal kernel which is applicable for N_2 on carbon slit pores and included with pyGAPS. Results are shown in Figure ???. We can see that whilst both methods produce a bimodal size distribution, neither is accurate in describing the crystallographic pore widths. This is to be expected, since neither method is applicable to the UiO-66(Zr) system. However, when comparing two samples of the same MOF, these methods can still highlight differences in the quality of the two batches. For example, it can be seen that the DFT method shows wide peaks at $>1 \text{ nm}$ which can

2. Extending bulk analysis of porous compounds through calorimetry

be an indication of the presence of defects in the UiO-66(Zr) structure. Indeed, TGA analysis of the pristine sample shows a linker ratio (11.8 linkers per cluster) that is lower than it would be in a perfect sample (see figure in supplemental information.)

New materials are often screened for their ability to act as a CO₂ capture material. A good predictor of performance in this application are the enthalpies of adsorption, which are an indication of host-guest interactions. Here, we first measure the differential heats of adsorption directly through the use of adsorption microcalorimetry at 303 K. Then, to determine the isosteric heats of adsorption, two isotherms have been measured at 303 K and 323 K respectively. The complete set of isotherms is loaded into pyGAPS and plotted by the `pygaps.plot_iso()` function as seen in Figure 2.1a. To calculate the isosteric heat of adsorption, the two isotherms measured for this purpose are passed through the `pygaps.isosteric_heat()` function. The results from the calculation are overlaid on top of the measured calorimetric data in Figure 2.1b. The two datasets are overlap for the most part but diverge at low loadings and near complete coverage. At low loading the small changes in pressure amount introduce large errors in the Clausius-Clapeyron equation. This, together with the breakdown of the assumption of equilibrium due to active sites in the MOF lead to the calorimetric measurement providing more valid results. At higher loadings, where the isotherm reaches a plateau and the change in adsorbed amount is small from point to point, errors are introduced in the direct calculation of the heat of adsorption. The two techniques are thus complementary.

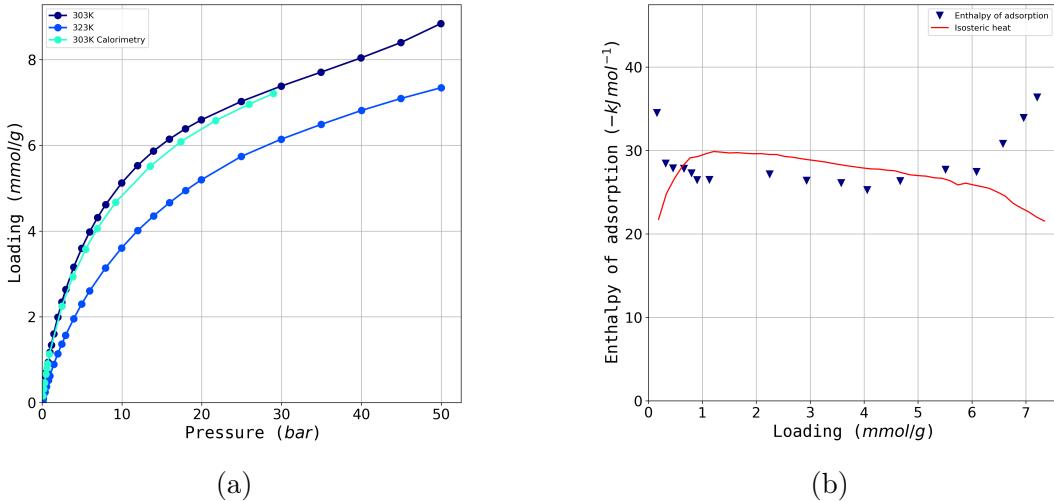


Figure 2.1.: Calculation of enthalpy of adsorption: (a) the dataset of isotherms used and (b) the calculated isosteric heat (red line) together with the measured differential enthalpy of adsorption (blue triangles)

2.4.2. Analysis of a carbon sample for gas separation applications

A sample of reference carbon Takeda 5A is to be investigated for an in-depth characterisation of the adsorption behaviour of pure gases, with a focus on describing the pore environment. Afterwards, the performance of different binary separations is evaluated, such as CO₂/N₂ and propane/propylene.

Pure gas adsorption data has been recorded at 303 K in conjunction with microcalorimetry on N₂, CO, CO₂, CH₄, C₂H₆, C₃H₆ and C₃H₈. The complete dataset is plotted with the pygaps.plot_iso() function and can be seen in Figure 2.2a.

Nitrogen and carbon monoxide are similar in their adsorption behaviour, with a nearly linear isotherm and low capacities. Hydrocarbons are adsorbed with higher loadings, with both propane and propylene reaching a plateau at low pressures. Propylene is seen to have a higher capacity than propane, with packing effects as a likely cause. Carbon dioxide has the highest loading capacity of the entire dataset.

Two parameters can be useful in characterising the local pore environment before guest-guest interactions come into effect: the Henry constant at low loadings as well as the initial enthalpy of adsorption. Both can be calculated with pyGAPS, with several options in regard to the methodology. Here, Henry's constant is calculated using the pygaps.initial_henry_virial() function, which fits a virial model to the isotherm and then takes the limit at loading approaching zero. The initial enthalpy of adsorption is obtained through the pygaps.initial_enthalpy_comp() function. This fits the enthalpy curve to a compound contribution from guest-host interaction, defects, guest-guest attraction and repulsion using a minimization algorithm. The results of the calculations are plotted versus the polarizability of the gas used, which can be obtained from the respective `Adsorbate` class. Figure 2.2b shows that both the parameters fall on a linear trend, which suggests that the interactions between those guests and the pore walls are mostly due to Lennard-Jones interactions. Carbon dioxide has a higher enthalpy of adsorption than the baseline due to the contribution from its quadrupole moment. There is almost a complete overlap between propane and propylene, which leads to the conclusion that the unsaturated double bond does not interact in a specific way with the carbon surface. The difference between the two isotherms is due exclusively to steric and packing effects.

2.5. Conclusion

2. Extending bulk analysis of porous compounds through calorimetry

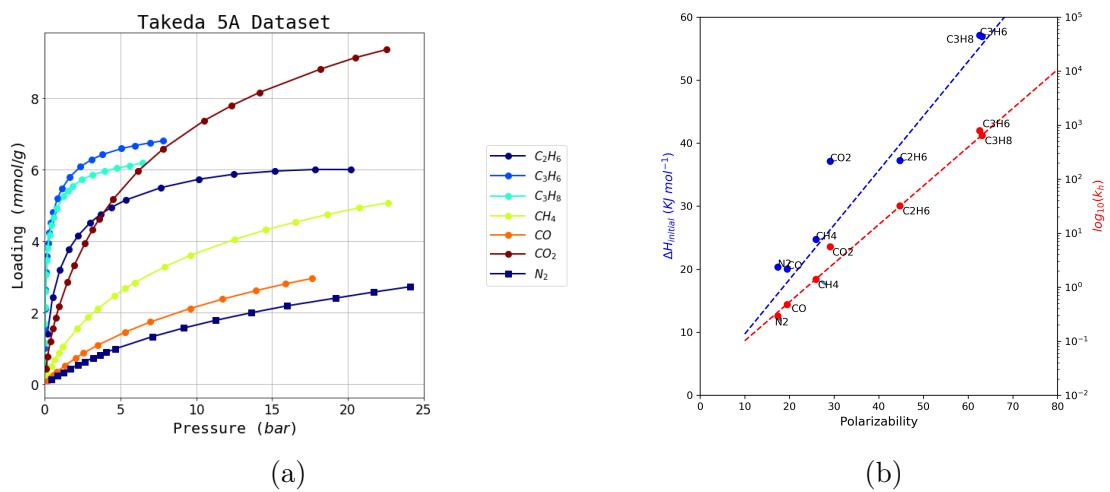


Figure 2.2.: Takeda 5A dataset processing: (a) the experimental dataset all recorded gases and (b) the calculated trends of initial heat of adsorption and Henry's constant

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3.Exploring the impact of synthesis and defects on adsorption measurements

3.1. Introduction

The UiO-66(Zr) MOF and its derivatives are well known due to their thermal and chemical stability.^(?) It is composed of $[\text{Zr}_6\text{O}_4(\text{OH})_4]^{12+}$ clusters which are connected with benzene dicarboxilate (BDC) linkers to form a face-centered cubic framework. It has shown promise^(?) in use for gas adsorption and catalytic applications.

3.2. Literature

3.3. Method

3.4. Results and discussion

3.5. Conclusion

Bibliography

4. Exploring the impact of material form on adsorption measurements

4.1. Introduction

An adsorbent cannot be used in an industrial process in its raw powder form. The small crystals which are normally the synthesis product of such a material would not be suited for direct use and need to be transformed into hierarchically porous structures.

Therefore, adsorbents are usually shaped into pellets, a process which introduces a range of benefits, such as improved flow regimes, better thermal management and material containment. The shaping process is needed not just for stabilising the small particles, but also to impart the resulting pellet with a high enough mechanical resistance to withstand the stresses imposed by the high flow encountered in an industrial bed.

The shaping process is therefore a crucial step towards the large-scale use of an adsorbent material. Even for commonplace adsorbents such as carbons and zeolites, the optimum binding compound and the shaping process itself are the subject of extensive research. Often, the procedure is tailored for individual material and application.

In an ideal setting, the process has limited effects on the properties of the material. However, this is often not the case, as shaping can degrade or improve adsorption performance. After a short introduction to shaping, this chapter explores the variability introduced by the binder in three topical MOFs: UiO-66(Zr), MIL-100(Fe) and MIL-127(Fe), which have been selected for their good stability and well-studied adsorption behaviour. The alumina shaped variant of these MOFs is compared to the original powder material, with regard to the adsorption of a series of common gasses and vapours. Microcalorimetry in conjunction with 8 gas probes has been used to get an in-depth picture of the change in surface energetics, with a separate study of adsorption of water and methanol vapour to examine changes in hydrophobicity. Particular behaviours are then highlighted and discussed.

Finally, a previous study on the same materials shaped with a poly-vinyl alcohol (PVA) binder is extended to vapour adsorption and the entire dataset is processed to obtain an overview of the impact of a hydrophobic and a hydrophilic binder on adsorption performance.

4.2. Shaping in context

In order to use an adsorbent in an industrial setting such as the beds and columns common in PSA (pressure swing adsorption) and TSA (temperature swing adsorption) processes, a pelletized form of the material is required.⁽¹⁾

The kinetics of the adsorption process are generally improved by the multi-scale pore size distribution afforded through shaping. Capacity per mass of pellet is expected to

4. Exploring the impact of material form on adsorption measurements

decrease due to the addition of a non-porous component, but the difference should be small and should not arise due to effects such as pore blocking or pore filling with the binder material. Furthermore, the densification effect is expected to lead to better performance on a volume basis. Finally, binder addition should not influence the chemical properties of the adsorbent, and preserve the original interactions with the adsorbate. With a judicious choice of binding material, the resulting pellet should outperform the powder.

For carbons, binders such as pitch, polymers (CMC, PVA) or even non-porous carbon black are commonly used.⁽²⁾ Often, a combination of binders is used, each with a different task during the pelletization process.⁽³⁾ The process itself consists of extrusion of the particle-binder slurry and then hardening either through temperature, cross-linking or chemical treatment. Other methods, such as spray-drying or granulation can similarly be used.⁽⁴⁾

shaping
meth-
ods

For zeolites, inorganic binders are more prevalent, with silica, alumina and clay binders commonly used in industry. It has been shown^(5,6) that the choice of binder can introduce large property variations, ranging from loss of porosity and structure to the enhancement of the desired reactivity and selectivity through changes in the acid site density or ion migration.

The shaping of MOFs has been attempted with a wide range of binders and methods. Methods such as granulation, spray-drying or extrusion have all been successfully employed to create MOF pellets.⁽⁷⁾ Monoliths have also been shown to be an effective way for shaping purposes, either through impregnation⁽⁸⁾ or through support on alumina.⁽⁹⁾ Surprisingly, compression⁽¹⁰⁾ or even simple air drying of MOF slurries⁽¹¹⁾ have also shown good results. Note that the ZIF-8 monolith prepared through the latter method had a three times larger volumetric specific surface area than the conventional powder.

The connection between MOF and binder is also of crucial importance for membranes. The MOF-polymer interface has been shown⁽¹²⁾ to be subject to a complex interplay of interactions between the organic chains and the crystal surfaces. These effects can be striking enough to warrant further research into MOF-polymer hybrids,⁽¹³⁾ with the aim of combining the unique attributes of both materials.

Previous work from this group⁽¹⁴⁾ has analysed the impact of PVA shaping on a series of MOFs. It was shown that the binder did introduce some specific effects, such as a protection effect on the reduction of Fe^{3+} to Fe^{2+} in MIL-127(Fe), as well as a curious gating effect seen on butane adsorption on MIL-100(Fe), likely due to polymer chains covering pore entrances. Otherwise, the shaping imparted good performance to the shaped samples, with almost no capacity loss on a mass basis. Unfortunately, the use of a polymer limited the activation temperature of the samples to a maximum of 150 °C.

In this work we have selected the same series of “topical” MOFs and have investigated the influence of a different shaping method, namely the use of alumina binder, on their adsorption properties.

The UiO-66(Zr) MOF and its derivatives are well known due to their stability, both in regards to temperature and chemical compounds.⁽¹⁵⁾ It is composed of Zr6-oxo clusters which are connected with benzene dicarboxilate (BDC) linkers to form a face-centered

4. Exploring the impact of material form on adsorption measurements

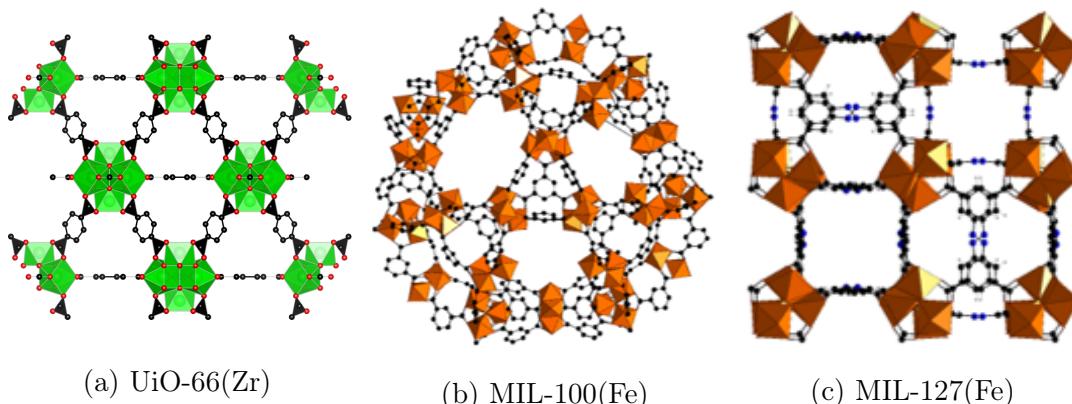


Figure 4.1.: The unit structures of the investigated MOFs. The colour coding is as follows: Zr polyhedra in green, Fe octahedra in brown, C in black, O in red, N in blue. Hydrogen atoms are omitted for clarity.

cubic framework. It has shown promise⁽¹⁶⁾ in use for gas adsorption applications.

MIL-100(Fe) is a MOF which uses the benzene tricarboxilate (BTC) linker in conjunction with trimeric iron (III) octahedral clusters.⁽¹⁷⁾ The framework assembles in hybrid supertetrahedra which leads to very large pore sizes. The iron trimers are coordinated with anions and have shown a propensity to partially reduce to a divalent Fe^{2+} state, exposing a naked metal site in the process.⁽¹⁸⁾

The last material, MIL-127(Fe), originally reported by Liu et al. is a MOF built from the same metal (III) octahedra trimers as MIL-100(Fe), but using the 3,3',5,5'-azobzenenetetracarboxylate (TazBz) linker, to produce a framework with the (soc) topology. This material has shown promise⁽²⁰⁾ for large scale synthesis. Furthermore, due to its alternating hydrophobic/hydrophilic microporous systems, it has been shown to be of interest for multiple applications such as catalysis or CO_2 capture.⁽²¹⁾

The structures of the three materials can be seen in Figure 4.1.

4.3. Synthesis, shaping and characterisation

4.3.1. Material Synthesis

The synthesis of these MOFs is well described in literature, as it has been previously reported for UiO-66(Zr)⁽¹⁵⁾ and MIL-100(Fe).⁽²²⁾

The UiO-66(Zr) and MIL-100(Fe) powders have been synthesised at the Korea Research Institute of Chemical Technology (KRICT) according to the methods previously referenced. Complete details of the synthesis method can be found in the related publication⁽²³⁾ and in Appendix B.

4.3.2. Shaping Procedure

The shaping of the samples also took place at KRICT and was done using a wet granulation method. In the case of the alumina binder, the MOF powder was mixed with the previously prepared mesoporous ρ -alumina with water added as the dispersing medium. For the PVA binder, the MOF powder was instead added to a solution of ethanol solution containing a polymer mixture of polyvinyl groups such as polyvinyl alcohol and polyvinyl butyral. The resulting mixture was shaped into beads using a hand-made pan granulator. During the process, the spheres were sprayed with the respective solvent in order to achieve desired size. The beads were then sieved and rolled using a roller machine to enhance their spherical shape. Finally, the prepared samples were dried at 303 K for 12 h to remove all residual solvent. The resulting beads were near spherical in shape, with a diameter between 2 mm to 2.5 mm.

4.3.3. Characterisation of powders and pellets

The primary interest of the study was observing differences in adsorption properties between the powder and the shaped materials.

Thermogravimetric analysis was used to verify that the binder did not change the thermal stability of the materials and, in the case of the PVA variant, to ensure that the activation temperature chosen did not induce polymer decomposition. The TGA method is described in detail in Appendix A.1.

The bulk and skeletal density of the powder and pellets were measured to allow isotherms to be presented on a volume basis, as well as to check the level of densification afforded through the shaping process. The procedure is described in Appendix A.2 and Appendix A.3.

Specific surface area and pore volume were determined through nitrogen adsorption at 77 K. These measurements were recorded according to the method in Appendix A.4. For inspecting changes in surface hydrophobicity, water and methanol adsorption isotherms were measured according to the method presented in Appendix A.5.

Finally, all calorimetry data was recorded using the high sensitivity Tian-Calvet calorimeter coupled with adsorption volumetry, as introduced in chapter 2.

4.3.4. Sample activation for adsorption

The materials were pre-treated before all adsorption experiments by activation at high temperature under secondary vacuum for 16 hours. The activation temperature was specific to each solid: 200 °C for UiO-66(Zr), 150 °C for MIL-100(Fe) and 150 °C for MIL-127(Fe).

4.4. Results and discussion

4.4.1. Thermal stability

In order to check if the shaped samples have not undergone bulk structural changes, as well as find a suitable activation temperature, the powder and shaped samples underwent thermogravimetric analysis under an argon atmosphere.

The process of shaping did not have any impact on the thermal stability of the investigated MOFs, as evidenced by the TGA curves in [Figure 4.2](#). The primary mass loss occurs in a 10 °C range for all powder-pellet pairs. Shaped samples are also seen to have a smaller mass loss at high temperatures. This is expected, as after the addition of temperature inert alumina, the MOF makes up a lower percentage of the material.

4.4.2. Adsorption isotherms at 77K and room temperature

Nitrogen sorption isotherms measured at 77 K have been measured on both powder and ρ -alumina pellets, with the isotherms presented in [Figure 4.3](#). Observation of the physisorption curves sheds light on the impact of the alumina binder on the materials chosen. The shapes of all isotherms are visually similar, with the pellet curves shifted downwards due to the aforementioned structure degradation. In both powders and pellets, the increased uptake after $0.9 p/p^0$ is a sign of condensation in very large pores or voids, which can be attributed to intra-pellet spaces and crystal agglomeration. In the MIL-127(Fe) pellets, a narrow hysteresis curve is seen, which closes at a p/p^0 of 0.5. This curve corresponds to capillary condensation in a pore size of around 4 nm. This pore width is too small to be a sign of inter-pellet voids and therefore must be a consequence of the shaping process.

While no other significant features are visible on the isotherms themselves, we use pyGAPS to further process them and obtain properties such as specific surface area, calculated through the BET method and pore volume, calculated as the volume of nitrogen adsorbed at a p/p^0 of 0.2. As the surface area of the binder is lower than the one of the MOF, a drop in both these properties is expected. The calculated values are shown in [Table 4.1](#).

Table 4.1.: Properties of the studied powders and pellets

MOF	form	BET surface area	Pore volume	Bulk density
UiO-66(Zr)	powder	903	0.38	0.3192
	ρ -alumina	619	0.24	0.4724
MIL-100(Fe)	powder	1928	0.78	0.2165
	ρ -alumina	1451	0.6	0.3512
MIL-127(Fe)	powder	1400	x	0.412
	ρ -alumina	1266	0.49	0.526

As predicted, the specific surface area of the shaped samples is decreased compared to

4. Exploring the impact of material form on adsorption measurements

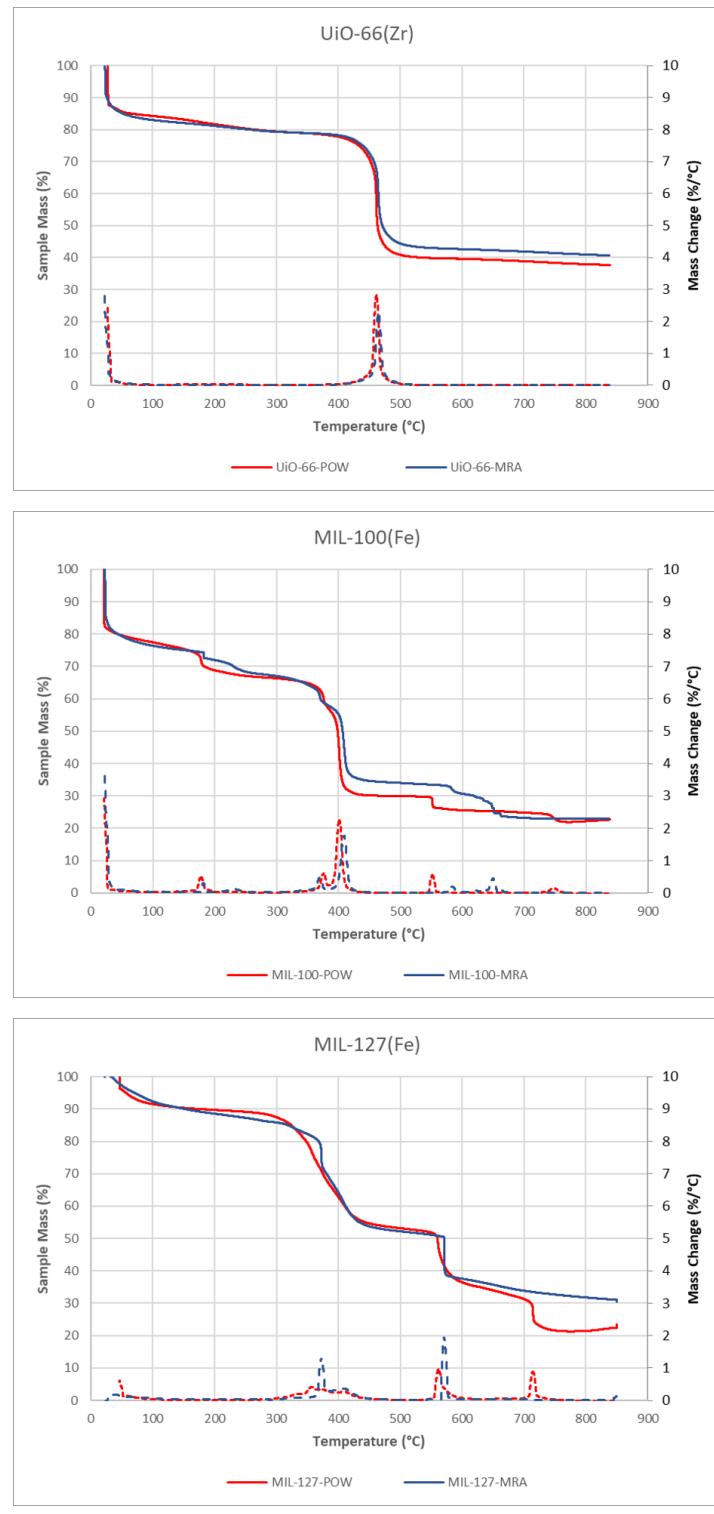


Figure 4.2.: High resolution TGA curves recorded under argon on (a) $\text{UiO-66}(\text{Zr})$, (b) $\text{MIL-100}(\text{Fe})$ and (c) $\text{MIL-127}(\text{Fe})$. The original powders are depicted in red and the shaped material in blue.

4. Exploring the impact of material form on adsorption measurements

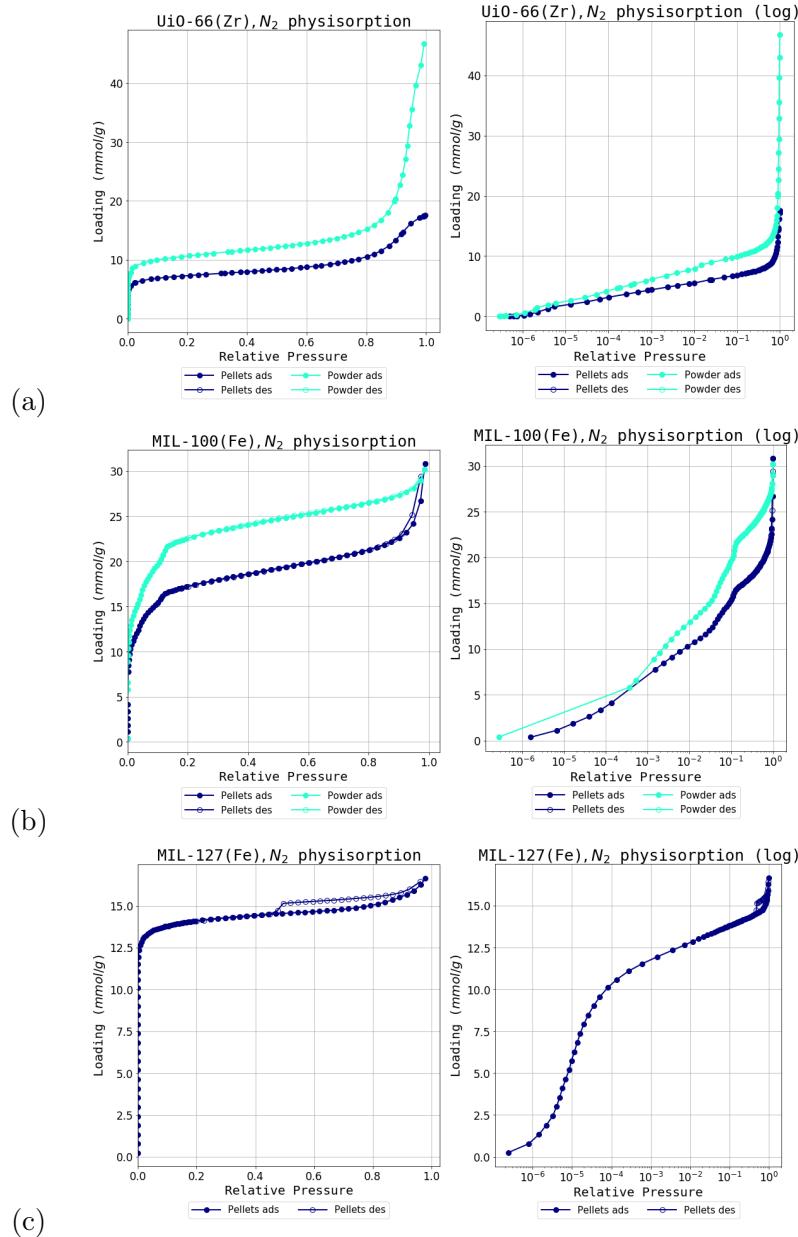


Figure 4.3.: Nitrogen isotherms at 77K for (a) $\text{UiO-66}(\text{Zr})$, (b) $\text{MIL-100}(\text{Fe})$ and (c) $\text{MIL-127}(\text{Fe})$. The powder sample is in light blue while the ρ -alumina sample in dark blue. Logarithmic graphs of the isotherms are on the right for clarity of the low pressure region.

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the corresponding powder. While in the case of MIL-127(Fe) the BET area is only 10% lower, for the MIL-100(Fe) and UiO-66(Zr) materials a larger drop is seen, of 25% and 31%, respectively. A similar decrease can be seen in pore volume, with a 36%, 23% and x% loss seen in UiO-66(Zr), MIL-100(Fe) and MIL-127(Fe) respectively. The decrease in both surface area and micropore volume is too large for it to be a consequence of the presence of non-porous binder. It is therefore theorised that some structure degradation must have occurred during the pelletisation process. Despite a loss in surface area, the bulk density of the material has increased, due to crystal aggregation.

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4.4.3. Room temperature gas adsorption and microcalorimetry

As previously shown, combining microcalorimetry with adsorption manometry can give an insight into the energetics of the adsorption process by directly measuring differential heat. Even though the different contributions to the overall enthalpy curve cannot be decoupled from the individual sources, such as guest-host interactions or fluid-fluid interactions, it can be successfully applied to observing the effect of a process or treatment such as shaping on the properties of a MOF.

Eight probe gasses have been chosen for adsorption at 303 K: N₂, CO, CO₂, CH₄, C₂H₆, C₃H₆, C₃H₈ and C₄H₁₀. The range of adsorbates chosen allows different effects to be investigated. The adsorption of saturated hydrocarbons with an increasing carbon number (C1-C4) can be assumed to be driven strictly by Van-der-Waals forces, due to the shielding effects of the hydrogen atoms. Differences in the maximum uptakes of these gasses will point to loss of porosity or crystallinity. A capacity loss with an increasing carbon number will point to size exclusion effects induced by the binder, such as particle coating, pore filling or pore obstruction. The other probes have been chosen for their properties which can shine light on other specific interaction types present during the adsorption. Carbon monoxide is a slightly dipolar molecule which has the ability to act as an with other charges in the pores. It also can highlight CUS (coordinatively unsaturated sites) generated through defects, reduction or open metal sites due to its propensity for π backbonding coordination. This electron transfer process can also result in complexation with molecular orbitals in systems with π bonds such as alkenes and alkynes. Propylene is used as an unsaturated hydrocarbon probe gas for this purpose. Carbon dioxide is a highly quadrupolar molecule which will be strongly adsorbed in polar pore environments. Changes in the adsorption behaviour of CO₂ will shed light on such surface changes and can even be used as a predictor of hydrophobicity.⁽²¹⁾ Finally, N₂ is a staple adsorbent for material characterisation when used at 77 K. The molecule is a slight quadrupole and has also been shown to chelate to some transitional metals in an analogue fashion to CO.

To eliminate the influence of kinetic and diffusion effects on the experiments, care has been taken to allow time for complete equilibration of both pressure and calorimeter signal. The complete dataset of adsorption isotherms, in the basis of both mass and volume can be found in Appendix C.

After collecting the combined isotherm and enthalpy data, three indicators have been chosen to best represent the effects of shaping: initial enthalpy of adsorption, initial

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Henry constant and maximum capacity. These numeric performance indicators have been calculated using the available functionality in pyGAPS.

The initial enthalpy of adsorption extrapolated at zero coverage is a measure of the interaction with highest energetic sites on the MOF surface. Conversely, the initial Henry constant ($K_H i$), here obtained through fitting the virial adsorption model through the method in ??, is also an indication of adsorption in the pores before any layering or adsorbate-adsorbate interaction comes into effect. The last indicator, maximum capacity, was taken as the loading attained when the isotherm reached a plateau. In the case of probes where the plateau was outside the range of pressure of the instrumentation (>50 bar), the loading at the highest available pressure was considered as a suitable approximation. The three key performance indicators (KPIs) have then been compared side by side on both the powder and shaped samples.

UiO-66(Zr)

A visual inspection of the enthalpy curves on as-synthesised UiO-66(Zr) show it to be relatively homogenous, with flat profiles being common. This is typical of this MOF, which has a pore environment without high energy adsorption sites.⁽¹⁶⁾ Both CO₂ and CO show a higher enthalpy of adsorption at low loadings, as seen in Figure 4.4, which is likely due to their quadrupole and dipole interaction, respectively.

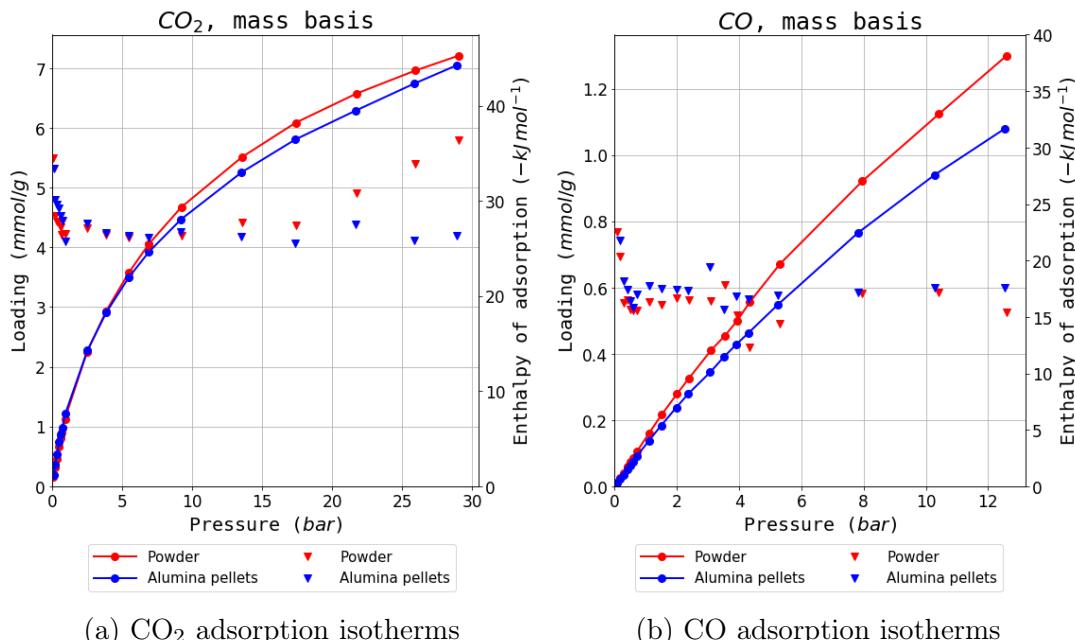


Figure 4.4.: Selected isotherms from the UiO-66(Zr) dataset

The KPI graphs in Figure 4.5 show very similar values for both Henry's constant and initial enthalpy of adsorption. It is therefore apparent that the shaping process did not change the interaction of the adsorbate with the MOF surface.

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The maximum capacity graphs show a more interesting trend. When using small adsorbates such as N₂, CO₂ and CH₄, the shaped samples have a similar performance on a mass basis and, due to the densification process, better capacities on a volume basis. Starting with ethane, the maximum capacity difference starts to increase, with lower performance as molecule size increases. On hydrocarbons with a carbon number of 3 and 4, both mass basis and volume basis capacity is decreased compared to the original powder. This size exclusion effect could be explained by the coating of crystal surfaces with the alumina binder.

It could also be argued that instead of size exclusion, the effect is due to an overall decrease in pore volume, and that the isotherms of the low molecular weight gasses will diverge at higher pressures as the pores are filled. A counterargument for this hypothesis is that in the case of CO₂, the plateau is reached with no differences between the powder and the pellet as seen in [Figure 4.4a](#).

Carbon monoxide is an apparent outlier to this trend, with a decreased maximum capacity and a small molecular size. However, when looking at the isotherms directly ([Figure 4.4b](#)) it is obvious that the effect is likely to be due to experimental errors, considering the low amount adsorbed and the good overlap in the enthalpy curves.

Overall, the shaping performance of UiO-66(Zr) is reasonable, as long as only small adsorbates are used.

MIL-100(Fe)

The enthalpy profiles on the MIL-100(Fe) powder are less homogenous than the ones on UiO-66(Zr). Some effects can be seen with probes which can interact with the partially reduced Fe(II) atom, such as carbon monoxide and propylene ([Figure 4.6](#)). Indeed, when comparing both the initial Henry constants and enthalpy of adsorption, for CO and C₃H₆, these are higher than the values obtained on UiO-66(Zr). With initial enthalpy of adsorption for CO of around 45 kJ mol⁻¹, the value falls into the range of previous⁽¹⁸⁾ results for interactions with such Fe(II) CUS.

Comparing the powder and shaped variants, there are no apparent differences between the two. The only discrepancy, which can be seen on the nitrogen initial K_H follows as a result of an ill-fitting virial parameter, and can be assumed an error after observing the isotherm overlap directly. It could be theorised that by activation at a higher temperature (250 °C), the percentage of iron trimers which would undergo reduction will increase and a further interaction could be observed. However, the activation temperature was chosen to allow comparisons with the PVA study,⁽¹⁴⁾ where temperatures over 180 °C would lead to the burn-off of the polymer binder.

The maximum loading differences ([Figure 4.7c](#)) of MIL-100(Fe) show a very similar behaviour. On all probes tested, a fixed capacity loss of between 10-20% can be seen on a mass basis. However, the increase in density afforded by the compression during pelletisation leads to a compensation in performance as can be seen directly when looking at isotherms on mass and volume material basis in [Figure 4.6a](#) and [Figure 4.6b](#) respectively.

We can conclude that MIL-100(Fe) is almost unaffected by alumina shaping. A slight

4. Exploring the impact of material form on adsorption measurements

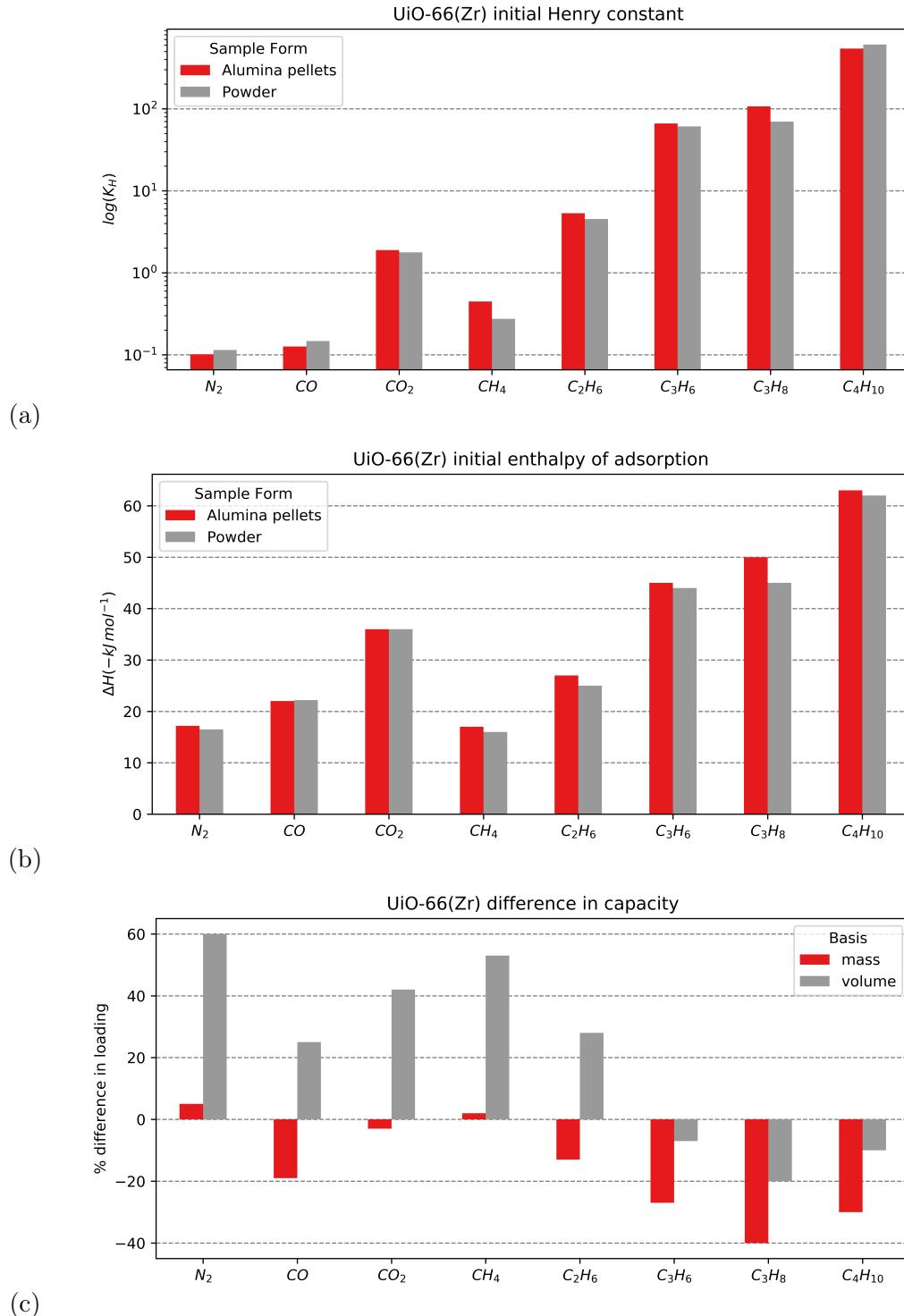


Figure 4.5.: KPIs extracted from the Uio-66(Zr) adsorption dataset with (a) logarithmic initial Henry constant (b) initial enthalpy of adsorption and (c) change in adsorption maximum capacity from the powder to the alumina shaped version on a mass and volume basis in red and grey respectively

4. Exploring the impact of material form on adsorption measurements

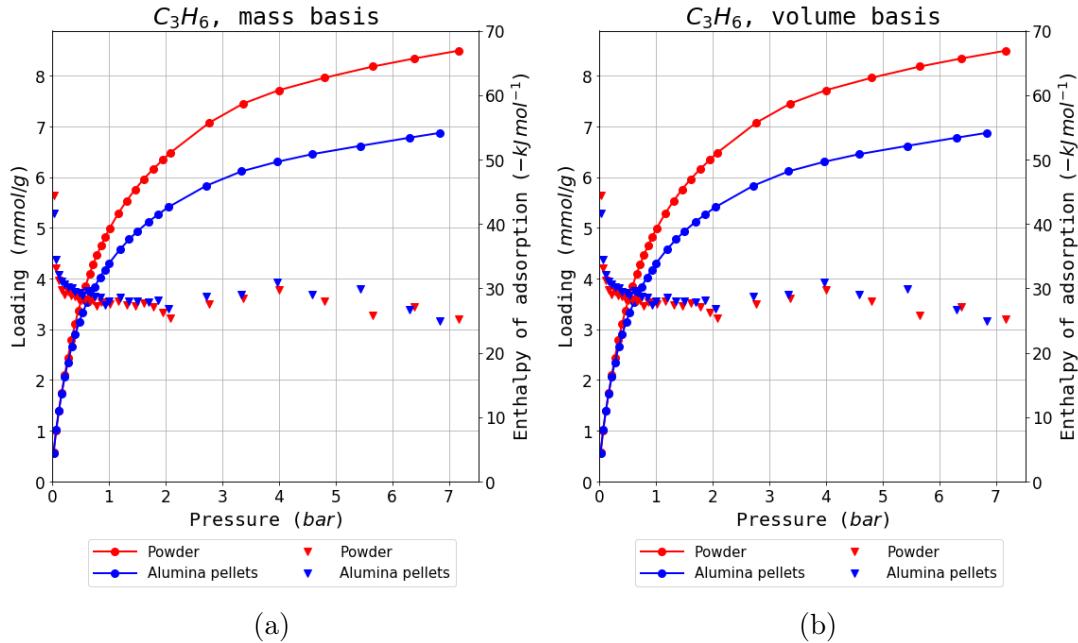


Figure 4.6.: Propylene isotherms on MIL-100(Fe) on a (a) mass and (b) volume adsorbent basis.

loss in maximum capacity on a mass basis is compensated by a pronounced densification, which is desirable in an industrial setting.

MIL-127(Fe)

The isotherms on the original powder form of MIL-127(Fe) should show similar behaviour as on MIL-100(Fe), due to the presence of the same iron trimesate moieties, although with a sharper uptake as a result of the smaller pores. Enthalpy profiles are also influenced by the similar interactions with the iron CUS leading to higher initial heats of adsorption on CO and C₃H₆. An overall increase in the heat of adsorption at higher loadings is seen throughout the probe series, as seen for example on butane in Figure 4.8a. Due to the bimodal pore distribution in the MIL-127(Fe) structure, it is likely that adsorption first commences in the small ($\sim 6 \text{ \AA}$) channels and then, at higher pressures, intrusion into the larger cage-type pores is possible through the $\sim 3 \text{ \AA}$ narrow apertures. The confined cages have an increased interaction with the molecule which leads to the higher enthalpy values.

When comparing the powder and the pellet variant with respect to initial Henry's constant, a large difference in K_H on CO stands out. The value of the initial enthalpy of adsorption does not follow the same pattern. However, visual inspection of the enthalpy curve in Figure 4.8b shows that the energy of adsorption corresponding to interactions with the more active sites is maintained for a larger percentage of the total coverage. This points to the higher preponderence of such sites in the powder variant. A similar offset can be seen in the propylene enthalpy at very low pressures, but this is not reflected

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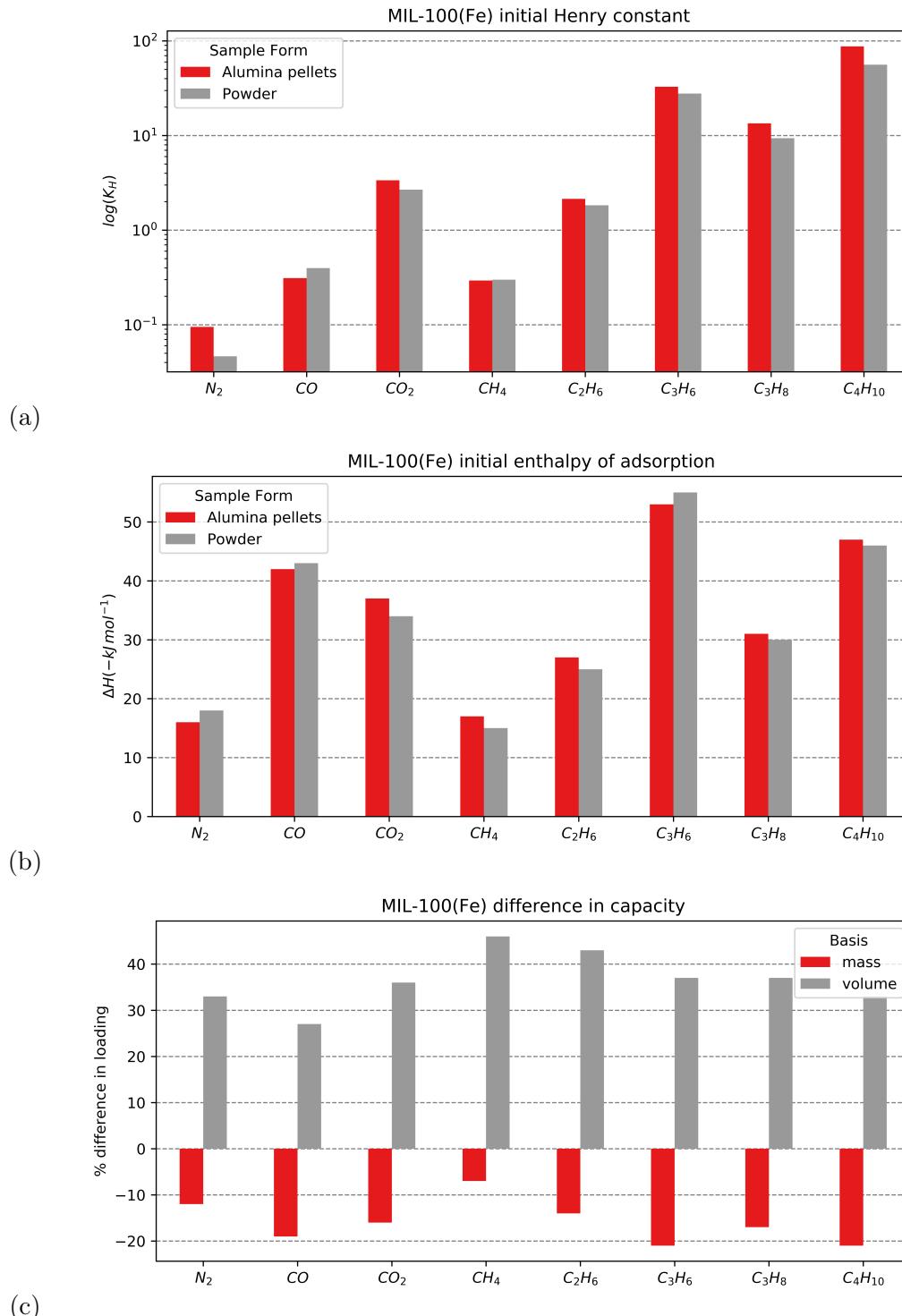


Figure 4.7.: KPIs extracted from the MIL-100(Fe) adsorption dataset with (a) logarithmic initial Henry constant (b) initial enthalpy of adsorption and (c) change in adsorption maximum capacity from the powder to the alumina shaped version on a mass and volume basis in red and grey respectively

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in the shape of the isotherm. The weaker complexation strength and the larger size of the molecule likely limits the effect seen in the carbon monoxide isotherm. As for the underlying reason behind the isotherm divergence, it could be that the alumina binder acts as protection against the generation of iron(II) during thermal activation. No other differences are seen between the two forms on either Henry constant and initial enthalpy of adsorption.

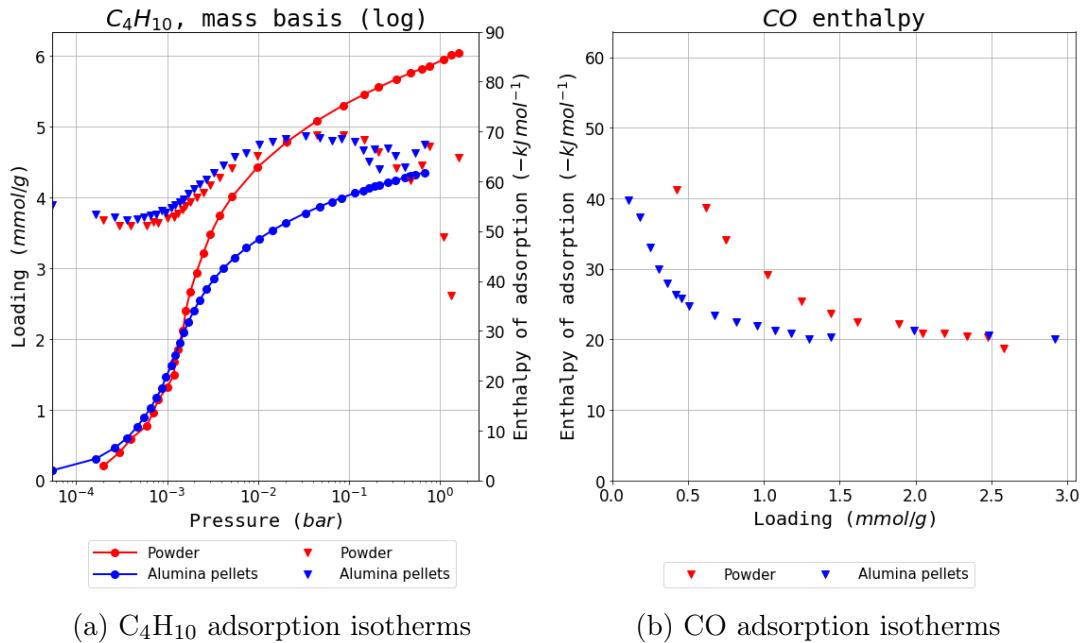


Figure 4.8.: Selected isotherms from the MIL-127(Fe) dataset

The capacity comparison in Figure 4.9c paints an interesting picture. For most probes there is no change in maximum loading showing that there is no structure degradation or pore filling. Two outliers are apparent: carbon monoxide and butane. The decrease in capacity on CO can be explained through the aforementioned changes in active site prevalence. The drop in butane cannot be a consequence of the same effect as there is a perfect overlap in the enthalpy curves as seen in Figure 4.8a. Therefore it likely better explained through a size exclusion effect as seen on UiO-66(Zr).

Overall, MIL-127(Fe) shows excellent performance when undergoing alumina shaping, with almost no capacity loss, as long as carbon monoxide or butane adsorption are required, where specific effects come into play.

4.4.4. Vapour adsorption

The effects of shaping with ρ -alumina are so far more subtle than the changes encountered when using PVA, as shown in the corresponding study.⁽¹⁴⁾ The influence of the binder on hydrophobic character of the material may be of interest for tuning the properties of the beads. Adsorption of water and methanol vapour can serve as a probe for

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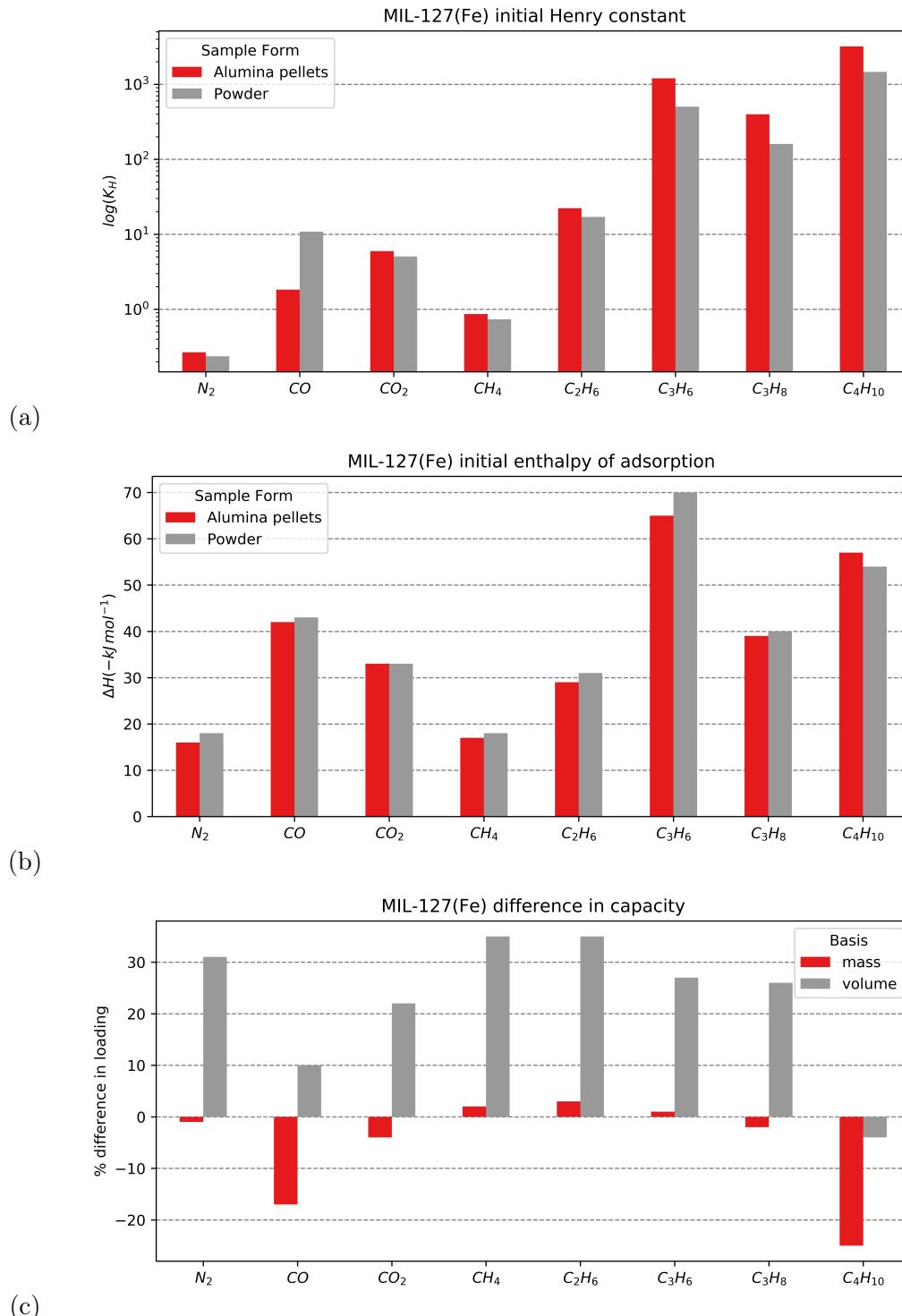


Figure 4.9.: KPIs extracted from the MIL-127(Fe) adsorption dataset with (a) logarithmic initial Henry constant (b) initial enthalpy of adsorption and (c) change in adsorption maximum capacity from the powder to the alumina shaped version on a mass and volume basis in red and grey respectively

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small changes is surface properties. To this end, the same PVA samples which were studied in the previous study were studied alongside the MRA-shaped MOF.

Due to its surface charges, alumina is a hydrophilic substance, with a contact angle of 10°. It is expected that its addition will therefore increase the affinity of the resulting pellet towards water. On the other hand, the PVA binder is more hydrophilic, with a water contact angle of 51°. The medium affinity for water is due to the surface hydroxyl functionalizations, which can lead to hydrogen bonding.

Two indicators may highlight changes in material hydrophilicity: adsorption in the low relative pressure region ($p/p^0 < 0.3$) and condensation steps in the isotherm. The adsorption at low pressures is representative of the first interactions with the surface, as explained in the previous sections. The pressure at which condensation occurs in the pores of the material, or where a sharp isotherm increase is seen depends on the size of the pore, but also on the pore environment and guest-guest interactions.

The measured isotherms on water and methanol can be found in [Figure 4.10](#) and [Figure 4.11](#) respectively. The isotherms measured on the original powder materials show the normal adsorption behaviour which can then be compared with the MRA and PVA shaped samples.

On UiO-66(Zr), the water isotherm shows a slow uptake at the start, corresponding to a hydrophobic material and then shows a small step at $p/p^0 = 0.3$. Complete pore filling happens at $p/p^0 = 0.8$.

Water isotherms on MIL-100(Fe) show a more hydrophilic environment, with a higher initial uptake, and two condensation steps at $p/p^0 = 0.3$ and $p/p^0 = 0.5$. There is pronounced hysteresis on the desorption branch. The methanol adsorption isotherms also show a two step adsorption isotherm, but without any hysteresis present. The shaped samples also show a lower

It can be therefore concluded that overall, the addition of either binder has not influenced the behaviour towards water or methanol for the materials studied. The full water adsorption isotherms can be found in [Figure 4.10](#).

4.5. Conclusion

It can be concluded that the process of alumina shaping does not, in general, have an impact on the surface chemistry of the three MOF materials. Interestingly, in regards to the changes in maximum capacity, each material has its own particular behaviour: UiO-66(Zr) has a higher loss in capacity with larger molecular probes, MIL-100(Fe) has a decrease of 10-20% across all gasses and MIL-127(Fe) matches loading on a mass basis except on CO and C₄H₁₀.

The shaping also induces a densification which, in almost all cases, leads to a better performance on a volumetric basis. However, the influence on the mass transport effects of the alumina binder is not known and should be investigated further.

Overall, the process of alumina shaping is a promising method of preparing MOFs for gas-related applications in separation and storage, but care should be taken to not generalise the effects present on one material to another.

4. Exploring the impact of material form on adsorption measurements

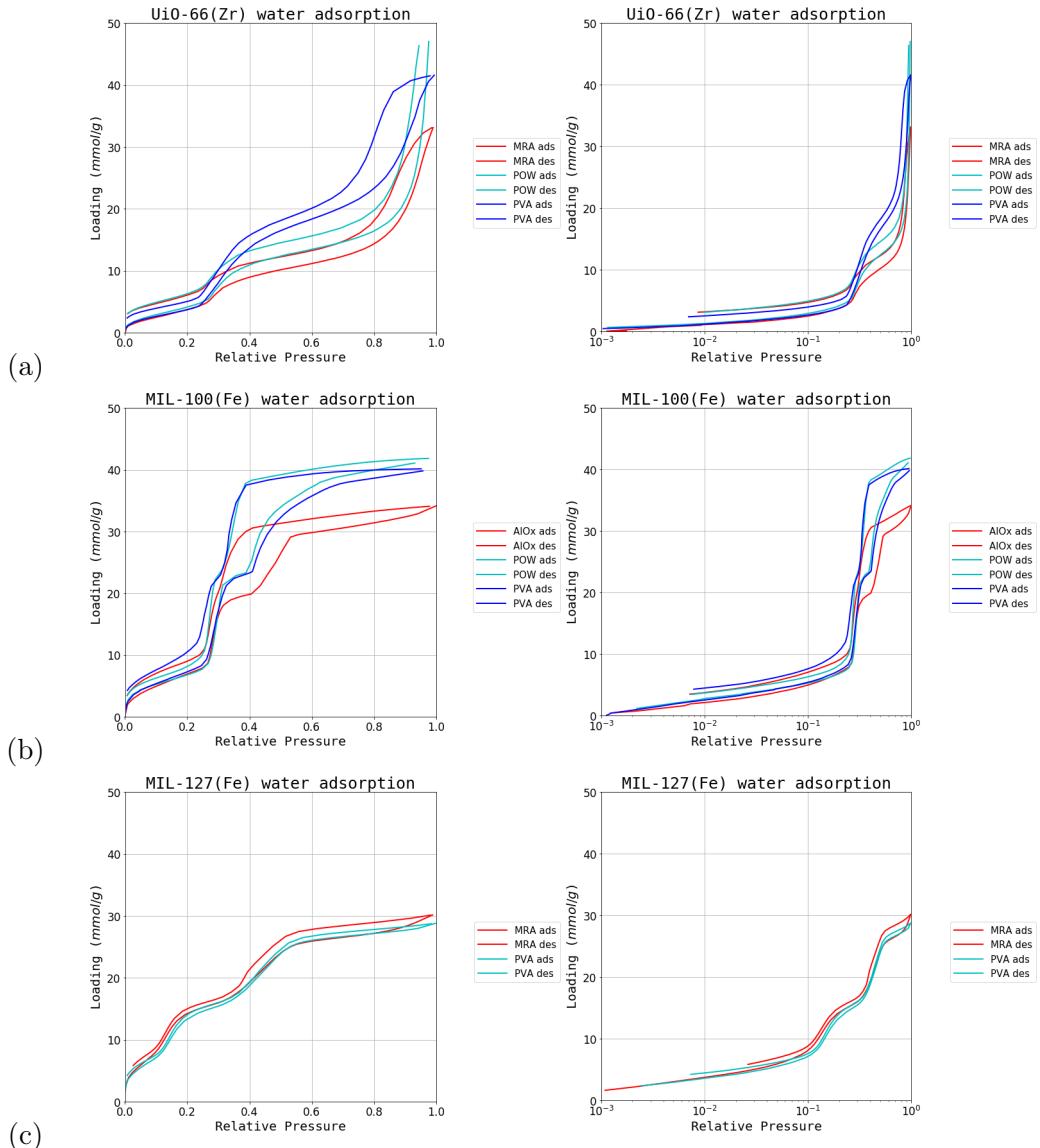


Figure 4.10.: Water adsorption isotherms (a) *UiO-66(Zr)*, (b) *MIL-100(Fe)* and (c) *MIL-127(Fe)*. The powder samples are in light blue, while the ρ -alumina and poly-vinyl alcohol samples are in red and dark blue respectively. Logarithmic graphs of the isotherms are on the right for clarity of the low pressure region.

4. Exploring the impact of material form on adsorption measurements

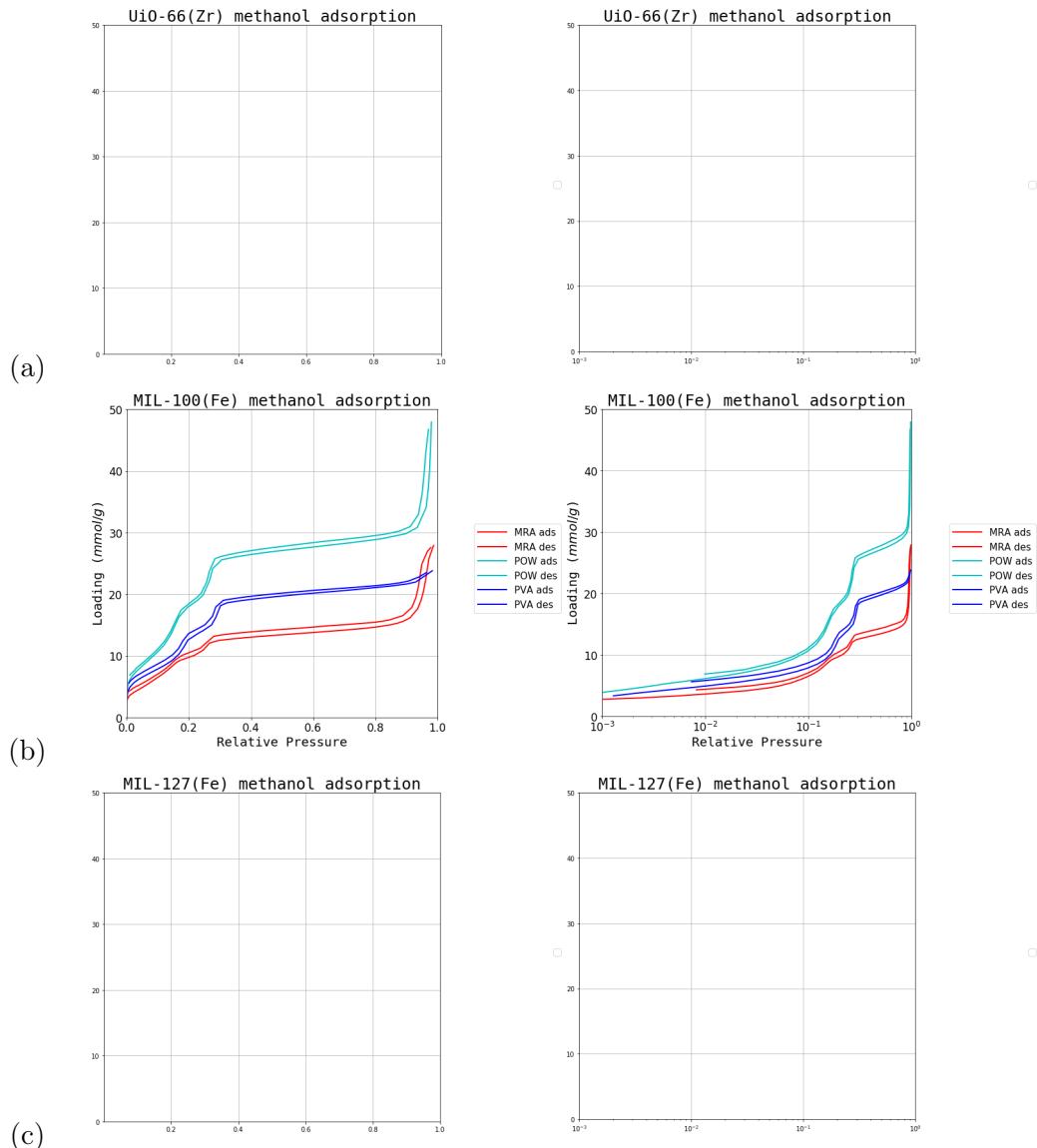


Figure 4.11.: Methanol adsorption isotherms (a) $\text{UiO-66}(\text{Zr})$, (b) $\text{MIL-100}(\text{Fe})$ and (c) $\text{MIL-127}(\text{Fe})$. The powder samples are in light blue, while the ρ -alumina and poly-vinyl alcohol samples are in red and dark blue respectively. Logarithmic graphs of the isotherms are on the right for clarity of the low pressure region.

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5.Exploring novel behaviours

5.1. Introduction

5.2. Literature

5.3. Method

5.4. Results and discussion

5.5. Conclusion

Bibliography

A. Common characterisation techniques

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A.1. Thermogravimetry

Thermogravimetry (TGA) is a standard laboratory technique where the weight of a sample is monitored while ambient temperature is controlled. Changes in sample mass can be correlated to physical events, such as adsorption, desorption, sample decomposition or oxidation, depending on temperature and its rate of change.

TGA experiments are carried out on approximately 15 mg of sample with a TA Instruments Q500 up to 800 °C. The sample is placed on a platinum crucible and sealed in a temperature controlled oven, under gas flow of $40 \text{ cm}^3 \text{ min}^{-1}$. Experiments can use a blanket of either air or argon. The temperature ramp can be specified directly and should be chosen to ensure that the sample is in equilibrium with the oven temperature and no thermal conductivity effects come into play. Alternatively, a dynamic “Hi-Res” mode can be used which allows for automatic cessation of heating rate while the sample undergoes mass loss.

The main purpose of thermogravimetry as used in this thesis is the determination of sample decomposition temperature, to ensure that thermal activation prior to adsorption is complete and that all guest molecules have been removed without loss of structure. To this end, experiments are performed under an inert atmosphere (argon), and the sample activation temperature is chosen as 50 °C to 100 °C lower than the sample decomposition temperature.

A.2. Bulk density determination

Bulk density is a useful metric for the industrial use of adsorbent materials, as their volume plays a critical role in equipment sizing.

Bulk density is determined by weighing 1.5 ml empty glass vessels and settling the MOFs inside. Powder materials are then added in small increments and settled through vibration between each addition. The full vessel is finally weighed, which allowed the bulk density to be determined. The same cell is used in all experiments, with cleaning through sonication between each experiment.

A. Common characterisation techniques

A.3. Skeletal density determination

True density or skeletal density is determined through gas pycnometry in a Microtrac-BEL BELSORP-max apparatus. Helium is chosen as the fluid of choice as it is assumed to be non-adsorbing.

The volume of a glass sample cell (V_c) is precisely measured through dosing of the reference volume with helium up to (p_1), then opening the valve connecting the two and allowing the gas to expand up to (p_2). Afterwards approximately 50 mg of sample are weighed and inserted in a glass sample cell. After sample activation using the supplied electric heater to ensure no solvent residue is left in the pores, the same procedure is repeated to determine the volume of the cell and the adsorbent. With the volume of the sample determined, the density can be calculated by.

$$V_s = V_c + \frac{V_r}{1 - \frac{p_1}{p_2}} \quad (\text{A.1})$$

A.4. Nitrogen physisorption at 77 K

Nitrogen adsorption experiments are carried out on a Micromeritics Triflex apparatus. Approximately 60 mg of sample are used for each measurement. Empty glass cells are weighed and filled with the samples, which are then activated in a Micromeritics Smart VacPrep up to their respective activation temperature under vacuum and then back-filled with an inert atmosphere. After sample activation, the cells are re-weighed to determine the precise sample mass. The cells are covered with a porous mantle which allows for a constant temperature gradient during measurement by wicking liquid nitrogen around the cell. Finally, the cells are immersed in a liquid nitrogen bath and the adsorption isotherm is recorded using the volumetric method. A separate cell is used to condense the adsorptive throughout the measurement for accurate determination of its saturation pressure.

A.5. Vapour physisorption at 298 K

Vapour adsorption isotherms throughout this work are measured using a MicrotracBEL BELSORP-max apparatus in vapour mode. Glass cells are first weighed and then filled with about 50 mg of sample. The vials are then heated under vacuum up to the activation temperature of the material and re-weighed in order to measure the exact sample mass without adsorbed guests. The cells are then immersed in a mineral oil bath kept at 298 K. To ensure that the cold point of the system occurs in the material and to prevent condensation on cell walls, the reference volume, dead space and vapour source are temperature controlled through an insulated enclosure.

A.6. Gravimetric isotherms

The gravimetric isotherms in this thesis are obtained using a commercial Rubotherm GmbH balance. Approximately 1 g of dried sample is used for these experiments. Samples are activated *in situ* by heating under vacuum. The gas is introduced using a step-by-step method, and equilibrium is assumed to have been reached when the variation of weight remained below 30 µg over a 15 min interval. The volume of the sample is determined from a blank experiment with helium as the non-adsorbing gas and used in combination with the gas density measured by the Rubotherm balance to compensate for buoyancy.

B.Synthesis method of referenced materials

B.1. Takeda 5A reference carbon

The Takeda 5A carbon was purchased directly from the Takeda corporation. The sample was activated at 250 °C under secondary vacuum (5 mbar) before any measurements.

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B.2. MCM-41 controlled pore glass

MCM-41 (Mobil Composition of Matter No. 41) is a mesoporous silica (SiO_2) material with a narrow pore distribution. First synthesised by the Mobil Oil Corporation, it is produced through templated synthesis using mycelle-forming surfactants. The material referenced in this thesis was purchased from Sigma-Aldrich. The activation procedure consists of heating at 250 °C under secondary vacuum (5 mbar).

B.3. Zr fumarate MOF

The synthesis of the Zr fumarate was performed in Peter Behren's group in Hannover, through modulated synthesis. This MOF can only be synthesised through the addition of a modulator, in this case fumaric acid, to the ongoing reactor, as detailed in the original publication.^(?)

The procedure goes as follows: ZrCl_4 (0.517 mmol, 1 eq) and fumaric acid (1.550 mmol, 3 eq) are dissolved in 20 mL N,N-dimethylformamide (DMF) and placed in a 100 mL glass flask at room temperature. 20 equivalents of formic acid were added. The glass flasks were Teflon-capped and heated in an oven at 120 °C for 24 h. After cooling, the white precipitate was washed with 10 mL DMF and 10 mL ethanol, respectively. The washing process was carried out by centrifugation and redispersion of the white powder, which was then dried at room temperature over night

B.4. UiO-66(Zr) for defect study

The UiO-66(Zr) sample preparation was adapted from Shearer et al. ^(?) as follows: ZrCl_4 (1.55 g, 6.65 mmol), an excess of terephthalic acid (BDC) (1.68 g, 10.11 mmol), HCl 37 % solution (0.2 mL, 3.25 mmol) and N,N'-dimethylformamide (DMF) (200 mL, 2.58 mol) were added to a 250 mL pressure resistant Schott bottle. The mixture was stirred for 10 min, followed by incubation in a convection oven at 130 °C for 24 h. The resulting white precipitate was washed with fresh DMF (3× 50 mL) followed by ethanol (3× 50 mL) over the course of 48 h and dried at 60 °C. After drying, the sample was

B. Synthesis method of referenced materials

activated on a vacuum oven by heating at 200 °C under vacuum for 12 h. The yield was 78 % white microcrystalline powder. Before the experiment, the sample was calcined at 200 °C under vacuum (5 mbar) to remove any residual solvents from the framework.

B.5. UiO-66(Zr) for shaping study

The scaled-up synthesis of UiO-66(Zr) was carried out in a 5 L glass reactor (Reactor Master, Syrris, equipped with a reflux condenser and a Teflon-lined mechanical stirrer) according to a previously reported method.^(?) In short, 462 g (2.8 mol) of H₂BDC (98%) was initially dissolved in 2.5 L of dimethyl formamide (DMF, 2.36 kg, 32.3 mol) at room temperature. Then, 896 g (2.8 mol) of ZrOCl₂ · 8H₂O (98%) and 465 mL of 37% HCl (548 g, 15 mol) were added to the mixture. The molar ratio of the final ZrOCl₂ · 8H₂O/H₂BDC/DMF/HCl mixture was 1 : 1 : 11.6 : 5.4. The reaction mixture was vigorously stirred to obtain a homogeneous gel. The mixture was then heated to 423 K at a rate of 1 K min⁻¹ and maintained at this temperature for 6 h in the reactor without stirring, leading to a crystalline UiO-66(Zr) solid. The resulting product (510 g) was recovered from the slurry by filtration, redispersed in 7 L of DMF at 333 K for 6 h under stirring, and recovered by filtration. The same procedure was repeated twice, using methanol (MeOH) instead of DMF. The solid product was finally dried at 373 K overnight.

B.6. MIL-100(Fe) for shaping study

The synthesis of the MOF for the shaping study was done at the KRICT institute using a previously published method.^(?) To synthesise the MIL-100(Fe) material Fe(NO₃)₃ was completely dissolved in water. Then, trimesic acid (BTC) was added to the solution; the resulting mixture was stirred at room temperature for 1 h. The final composition was Fe(NO₃)₃ · 9 H₂O : 0.67 BTC : n H₂O (x = 55–280). The reactant mixture was heated at 433 K for 12 h using a Teflon-lined pressure vessel. The synthesized solid was filtered and washed with deionized (DI) water. Further washing was carried out with DI water and ethanol at 343 K for 3 h and purified with a 38 mM NH₄F solution at 343 K for 3 h. The solid was finally dried overnight at less than 373 K in air.

B.7. MIL-127(Fe) for shaping study

MIL-127(Fe) was synthesized by reaction of Fe(ClO₄)₃ · 6 H₂O (3.27 g, 9.2 mmol) and C₁₆N₂O₈H₆ (3.3 g) in DMF (415 mL) and hydrofluoric acid (5 M, 2.7 mL) at 423 K in a Teflon flask. The obtained orange crystals were placed in DMF (100 mL) and stirred at ambient temperature for 5 h. The final product was kept at 375 K overnight. MIL-127(Fe) was synthesized by reaction of Fe(ClO₄)₃ · 6 H₂O (3.27 g, 9.2 mmol) and C₁₆N₂O₈H₆ (3.3 g) in DMF (415 mL) and hydrofluoric acid (5 M, 2.7 mL) at 423 K in a Teflon flask.

B. Synthesis method of referenced materials

The obtained orange crystals were placed in DMF (100 mL) and stirred at ambient temperature for 5 h. The final product was kept at 375 K overnight.

C. Complete adsorption dataset for shaping study

C.1. Calorimetry dataset UiO-66(Zr)

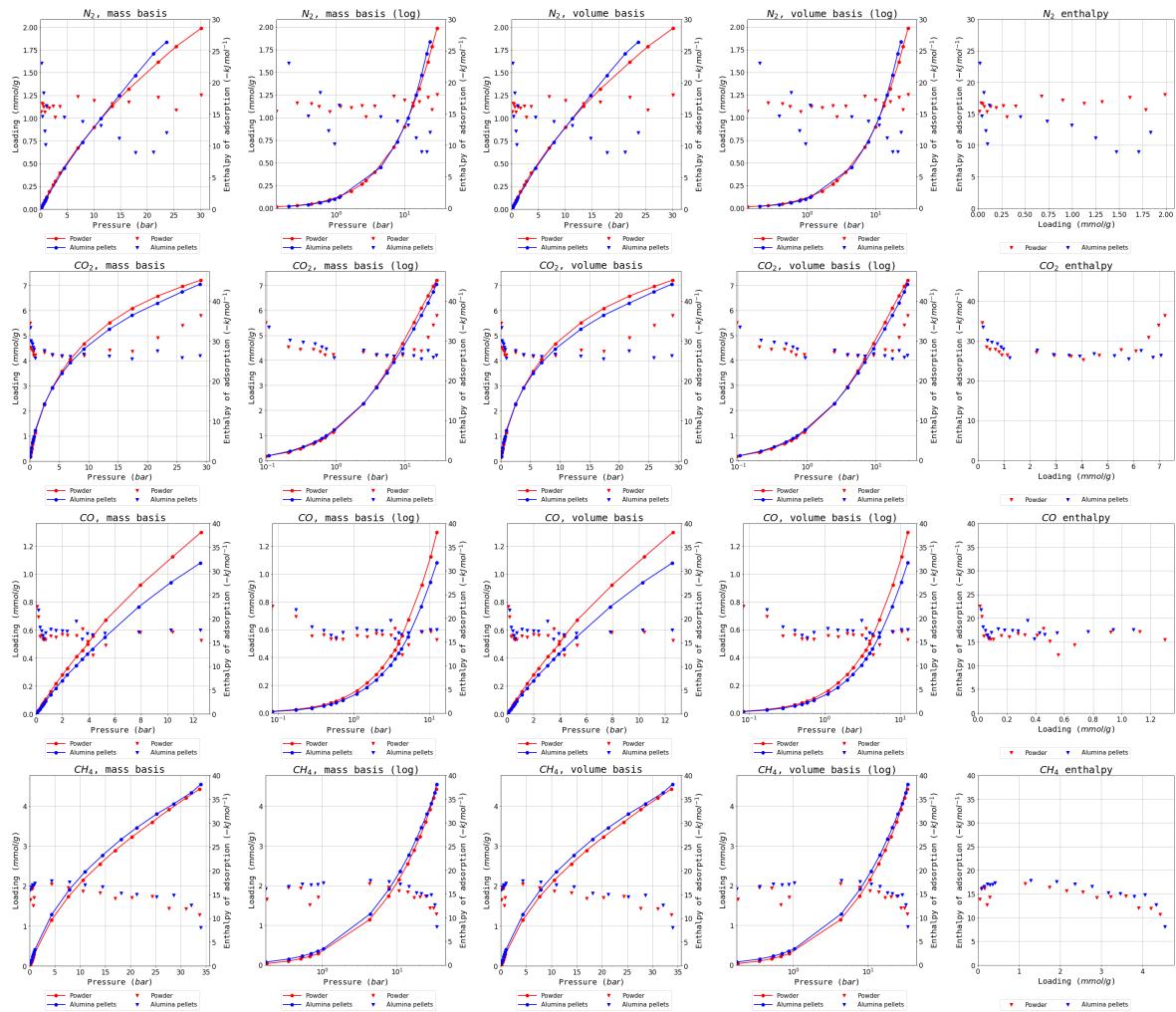


Figure C.1.: Complete isotherm and enthalpy dataset for UiO-66(Zr)

C. Complete adsorption dataset for shaping study

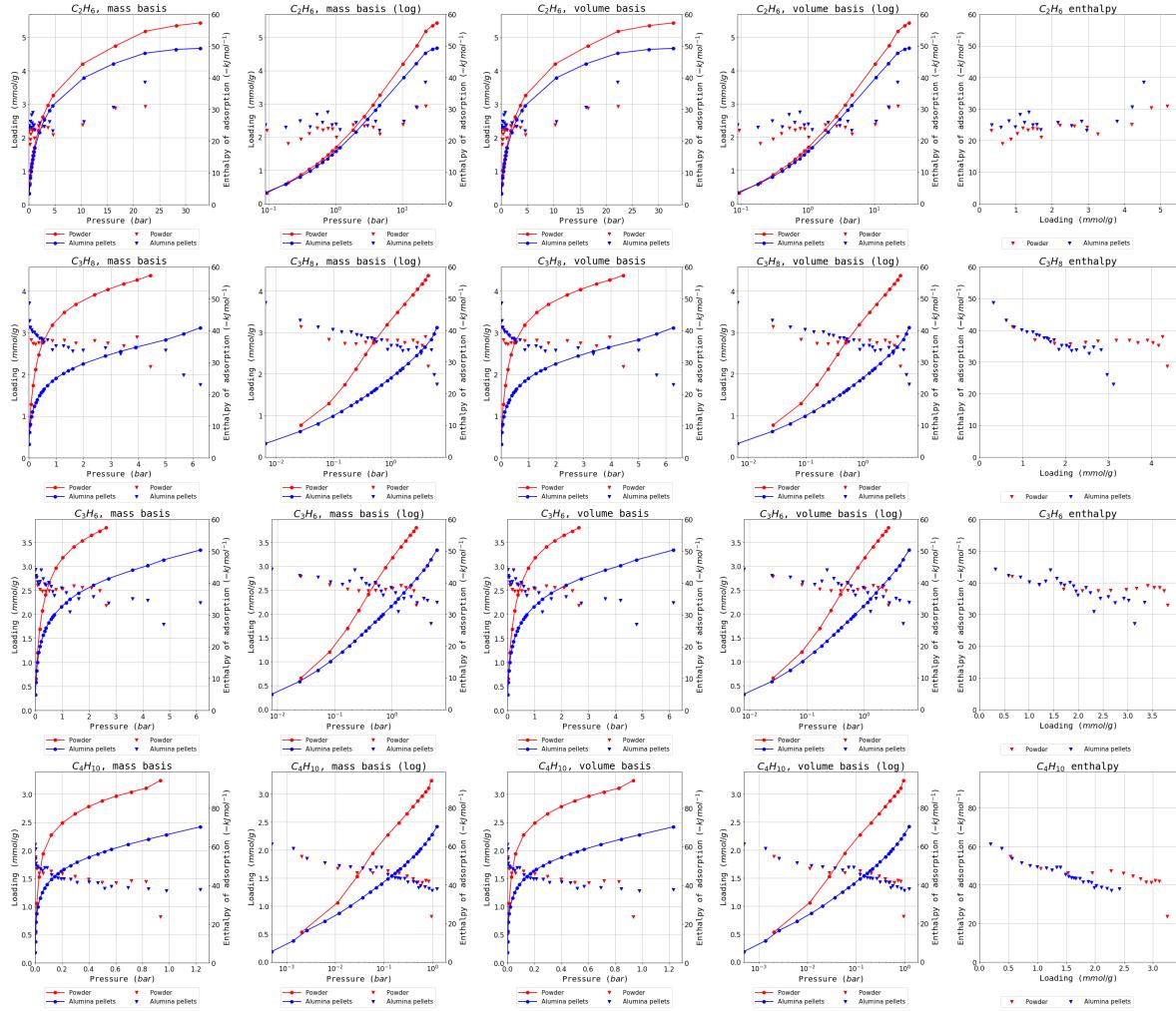


Figure C.1.: Complete isotherm and enthalpy dataset for UiO-66(Zr)

C.2. Calorimetry MIL-100(Fe)

C. Complete adsorption dataset for shaping study

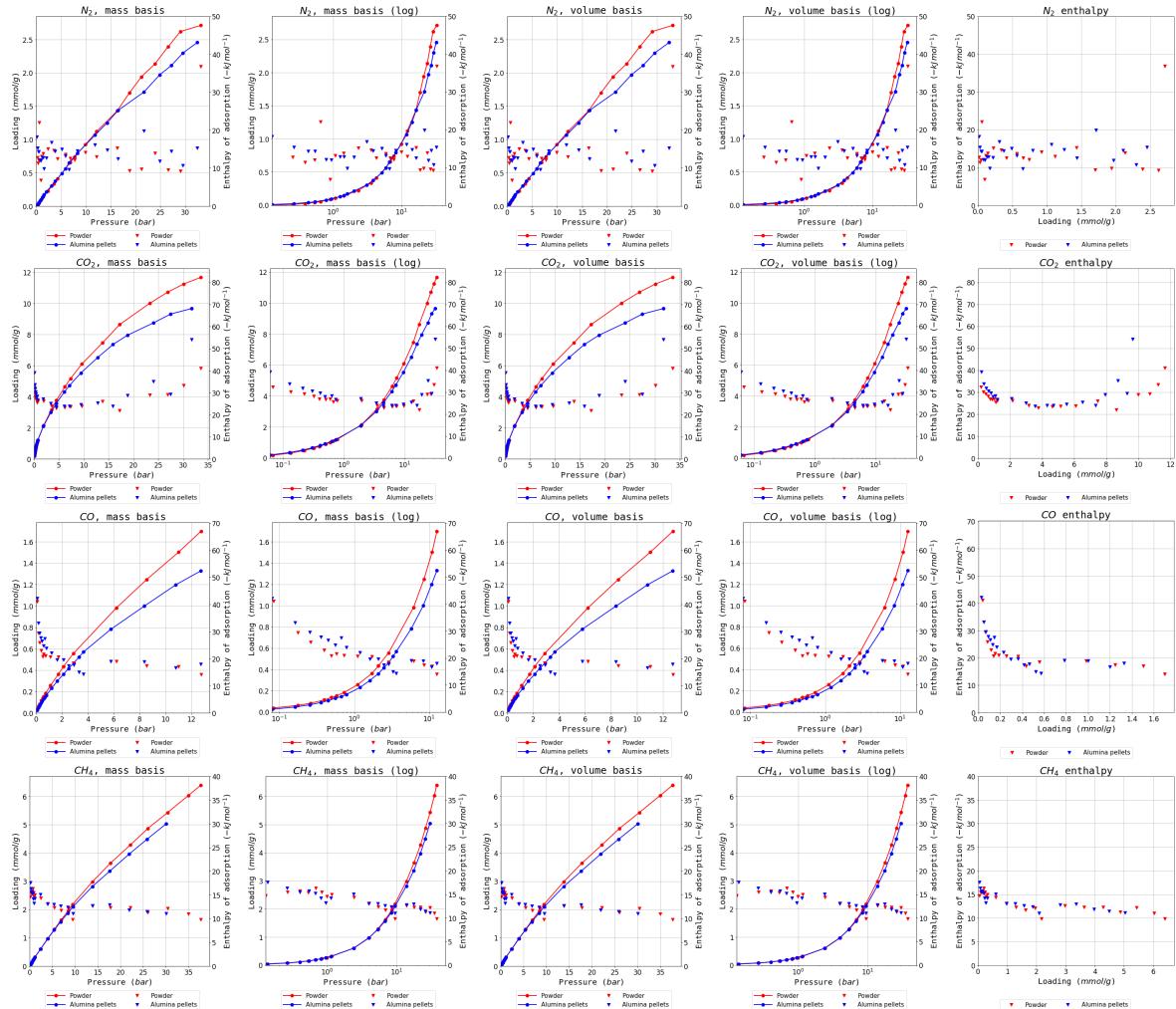


Figure C.2.: Complete isotherm and enthalpy dataset for MIL-100(Fe)

C. Complete adsorption dataset for shaping study

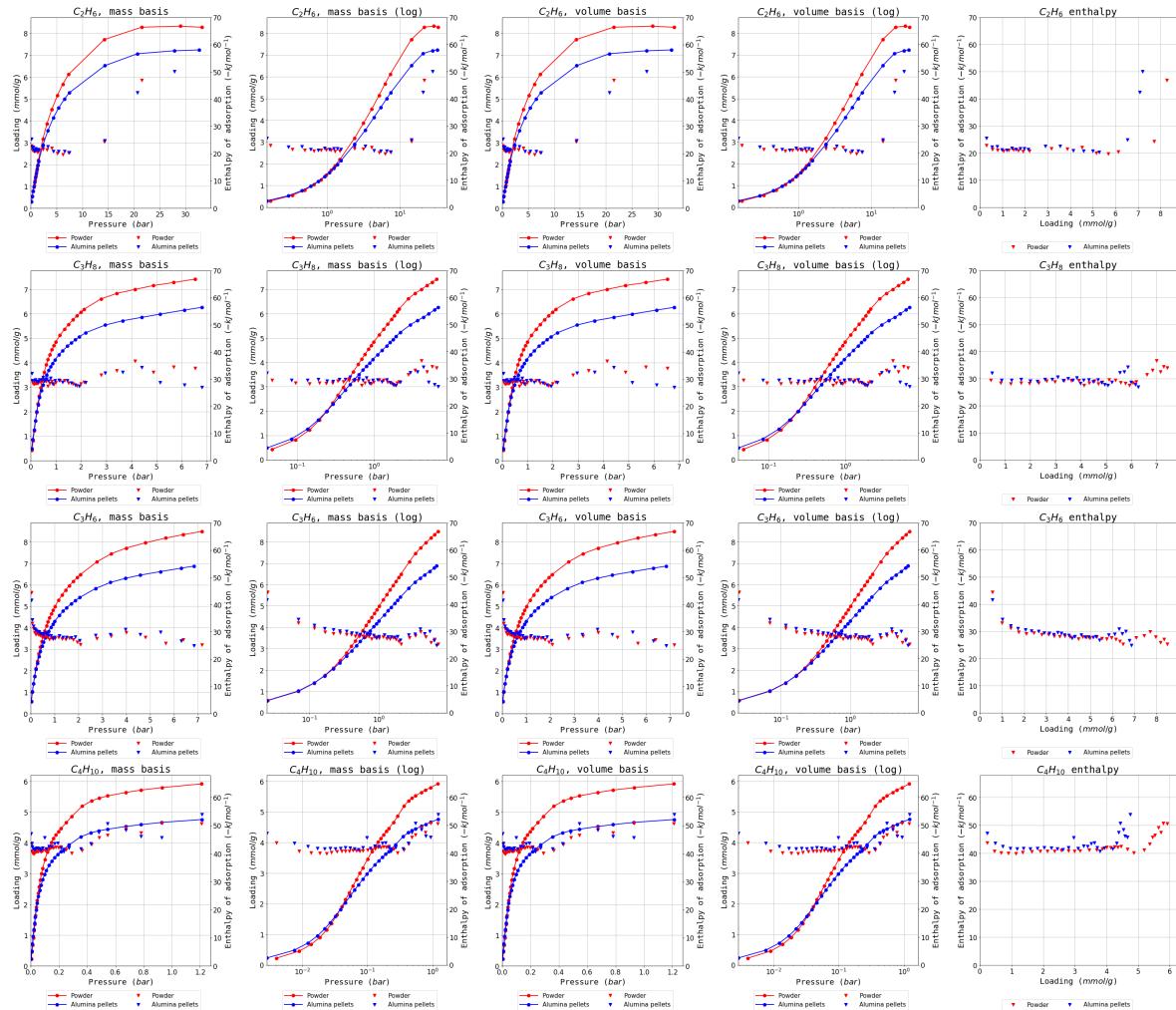


Figure C.2.: Complete isotherm and enthalpy dataset for MIL-100(Fe)

C. Complete adsorption dataset for shaping study

C.3. Calorimetry MIL-127(Fe)

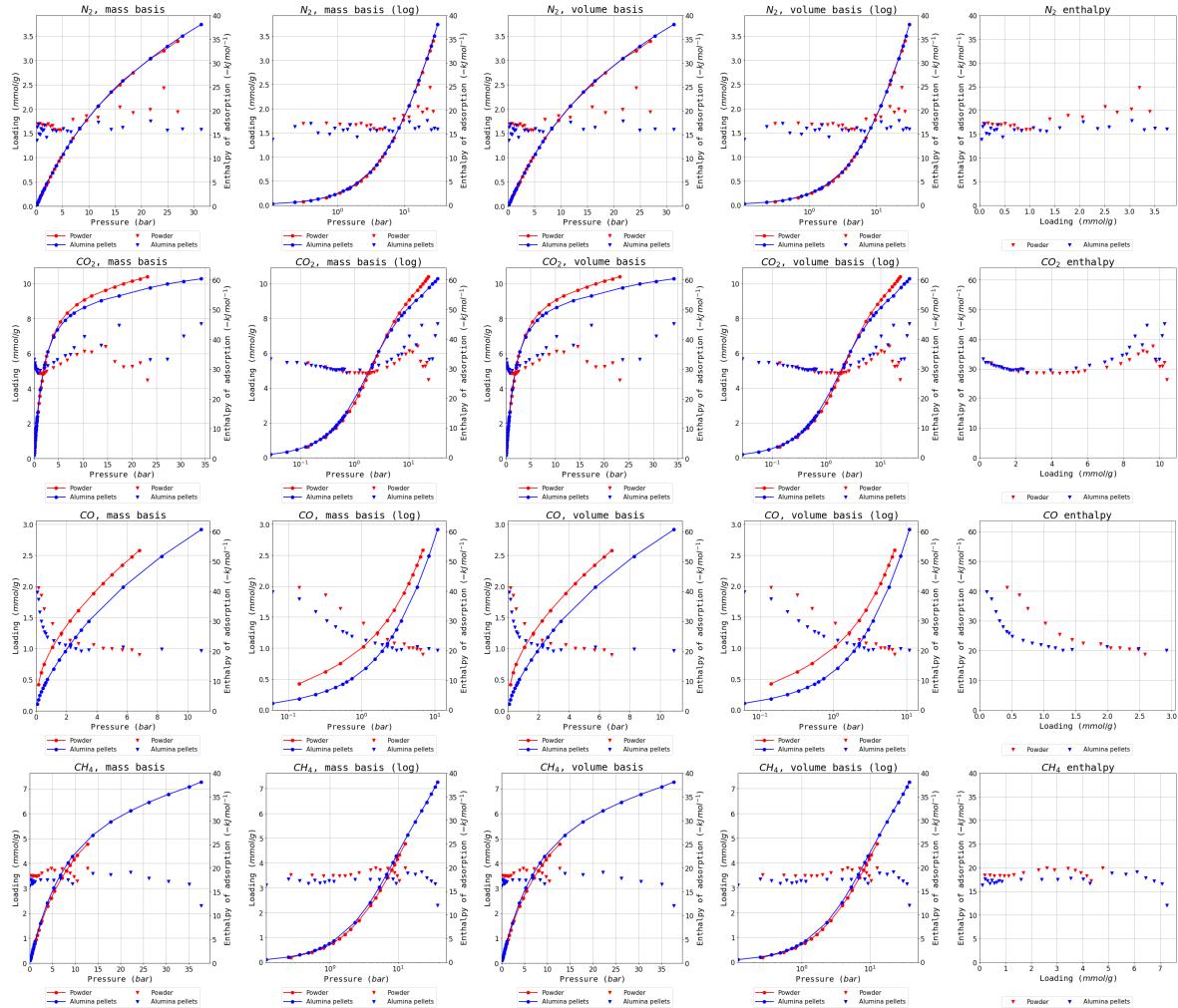


Figure C.3.: Complete isotherm and enthalpy dataset for MIL-127(Fe)

C. Complete adsorption dataset for shaping study

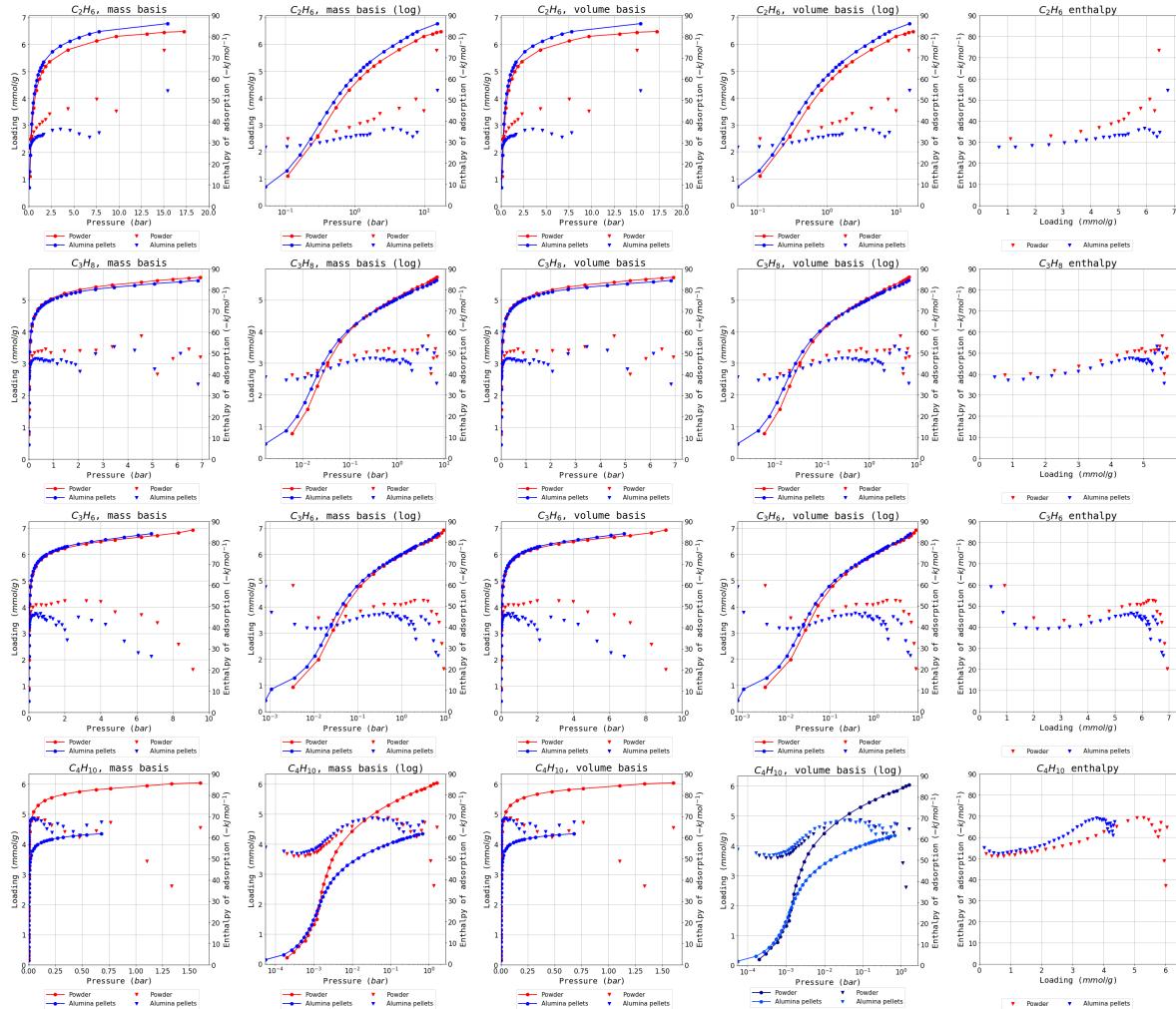


Figure C.3.: Complete isotherm and enthalpy dataset for MIL-127(Fe)