Simulations of Variable-Density Flows in the Low Mach Number Limit

Paul Bartholomew
Sylvain Laizet

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- Introduction
  - Motivation
  - The Low Mach Number (LMN) approximation
- `QuasIncompact3D`: the implementation of LMN in `Incompact3D`
  - Algorithm to solve LMN
  - Treatment of pressure equation
- Testcases
  - 2D mixing layer
  - Jet
- Conclusion

Introduction

What problem are we trying to solve?

- `Incompact3D` provides powerful capabilities for solving *incompressible* flows. . .
- or flows with small density variations

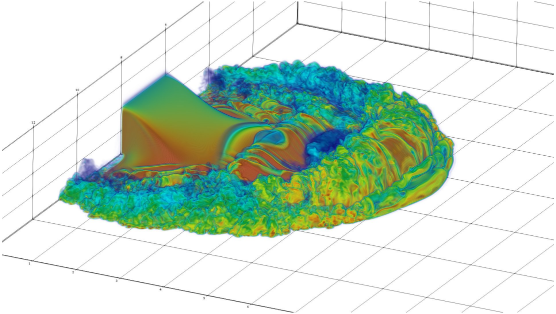


Figure: Gravity-driven flow simulated by `Incompact3D`[1]

[1] `https://twitter.com/incompact3d`

- If density variations are significant, needs to be treated as *compressible* flow
- Flow velocity may still be low ($\gamma M^2 \ll 1$)
- Results in ill-conditioned equations, *e.g.*

$$\gamma M^2 \rho \frac{D\boldsymbol{u}}{Dt} = -\boldsymbol{\nabla} p + \frac{\gamma M^2}{Re}\boldsymbol{\nabla}\cdot\boldsymbol{\tau}$$

- Numerically this leads to requirement for very small timesteps
  - Inefficient!

- Expand variables as power series using $\varepsilon = \gamma M^2$ as the small parameter and take lowest order terms (recall $\gamma M^2 \ll 1$)

$$\boldsymbol{u} = \boldsymbol{u}^{(0)} + \varepsilon \boldsymbol{u}^{(1)} + \varepsilon^2 \boldsymbol{u}^{(2)} + \ldots$$

$$\begin{aligned}
p^{(0)} &= \rho^{(0)} T^{(0)} \\
\frac{\partial \rho^{(0)}}{\partial t} + \boldsymbol{\nabla} \cdot \rho^{(0)} \boldsymbol{u}^{(0)} &= 0 \\
\boldsymbol{0} &= \boldsymbol{\nabla} p^{(0)} \\
\rho^{(0)} \frac{\partial T^{(0)}}{\partial t} + \rho^{(0)} \boldsymbol{u}^{(0)} \cdot \boldsymbol{\nabla} T^{(0)} &= \frac{\boldsymbol{\nabla} \cdot k \boldsymbol{\nabla} T^{(0)}}{RePrT^{(0)}} + \frac{dp^{(0)}}{dt} \\
\frac{\partial \rho^{(0)} \boldsymbol{u}^{(0)}}{\partial t} + \boldsymbol{\nabla} \cdot \rho^{(0)} \boldsymbol{u}^{(0)} \boldsymbol{u}^{(0)} &= -\boldsymbol{\nabla} p^{(1)} + \frac{\boldsymbol{\nabla} \cdot \boldsymbol{\tau}^{(0)}}{Re}
\end{aligned}$$

- Combining continuity and temperature equations yields velocity divergence constraint

$$\nabla \cdot \boldsymbol{u} = \frac{1}{p^{(0)}} \left(\frac{\nabla \cdot k \nabla T}{RePr} - \frac{dp^{(0)}}{dt} \right)$$

- Boundary condition follows

$$\int_{\partial\Omega} \boldsymbol{u} \cdot \widehat{\boldsymbol{n}} dS = \frac{1}{p^{(0)}} \left(\frac{1}{RePr} \int_{\partial\Omega} k \nabla T \cdot \widehat{\boldsymbol{n}} dS - \frac{dp^{(0)}}{dt} V_\Omega \right)$$

- Open domains

$$\frac{dp^{(0)}}{dt} = 0 \Rightarrow p^{(0)} = p_a$$

- Advance density in time

$$\rho^{k+1} = \rho^k + \Delta t \boldsymbol{\nabla} \cdot (\rho \boldsymbol{u})^k$$

- Update temperature via EOS and compute $\boldsymbol{\nabla} \cdot \boldsymbol{u}^{k+1}$

$$T^{k+1} = \frac{p^{(0)}}{\rho^{k+1}} \Rightarrow \boldsymbol{\nabla} \cdot \boldsymbol{u}^{k+1} = \frac{\boldsymbol{\nabla} \cdot k \boldsymbol{\nabla} T^{k+1}}{p^{(0)} Re Pr}$$

- Integrate momentum via fractional step method[2]

$$(\rho \boldsymbol{u})^\star = (\rho \boldsymbol{u})^k - \Delta t \left(\boldsymbol{\nabla} \cdot (\rho \boldsymbol{u} \boldsymbol{u})^k - \frac{\boldsymbol{\nabla} \cdot \boldsymbol{\tau}^k}{Re} \right)$$

$$(\rho \boldsymbol{u})^{k+1} = (\rho \boldsymbol{u})^\star - \Delta t \boldsymbol{\nabla} \widetilde{p^{(1)}}^{k+1} \Rightarrow \boldsymbol{u}^{k+1} = \frac{(\rho \boldsymbol{u})^{k+1}}{\rho^{k+1}}$$

[2] Chorin (1997)

- Like incompressible approach, take divergence of momentum directly

$$\nabla^2 \widetilde{p^{(1)}}^{k+1} = \frac{1}{\Delta t}\left(\boldsymbol{\nabla}\cdot(\rho\boldsymbol{u})^{\star} - \boldsymbol{\nabla}\cdot(\rho\boldsymbol{u})^{k+1}\right)$$

+ Constant coefficient Poisson equation: direct solution possible
− Need an approximation for $\boldsymbol{\nabla}\cdot(\rho\boldsymbol{u})^{k+1}$

$$\boldsymbol{\nabla}\cdot(\rho\boldsymbol{u})^{k+1} = -\left.\frac{\partial\rho}{\partial t}\right|^{k+1} \approx -\frac{\rho^{k+1}-\rho^{k}}{\Delta t}$$

- Alternatively, $\boldsymbol{\nabla} \cdot \boldsymbol{u}^{k+1}$ is available as a constraint[3]

$$\boldsymbol{\nabla} \cdot \frac{1}{\rho} \boldsymbol{\nabla} \widetilde{p^{(1)}}^{k+1} = \frac{1}{\Delta t} \left(\boldsymbol{\nabla} \cdot \boldsymbol{u}^{\star} - \boldsymbol{\nabla} \cdot \boldsymbol{u}^{k+1} \right)$$

- Cannot solve directly using FFT solver
- Iterative solver

$$\nabla^2 \widetilde{p^{(1)}}^{\nu+1} = \nabla^2 \widetilde{p^{(1)}}^{\nu} + \widetilde{\rho} \left[\frac{1}{\Delta t} \left(\boldsymbol{\nabla} \cdot \boldsymbol{u}^{\star} - \boldsymbol{\nabla} \cdot \boldsymbol{u}^{k+1} \right) - \boldsymbol{\nabla} \cdot \frac{1}{\rho} \boldsymbol{\nabla} \widetilde{p^{(1)}}^{\nu} \right]$$

$$\left|\left| \Delta \widetilde{p^{(1)}} \right|\right| \leq \texttt{tol}$$

[3] *c.f.* incompressible flow: $\boldsymbol{\nabla} \cdot \boldsymbol{u} = 0$

- Free choice of $\widetilde{\rho}$
- Choice of $\widetilde{\rho}$ will affect convergence
- Typical choices are an average or minimum value, $\widetilde{\rho} = \rho_0$
  - Stems from '*brute force*' derivation of iteration equation
- Chain-rule suggests $\widetilde{\rho}$ should vary in space

$$\begin{aligned}
\nabla \cdot \frac{1}{\rho} \nabla \widetilde{p^{(1)}} &= \frac{1}{\rho} \nabla^2 \widetilde{p^{(1)}} + \nabla \frac{1}{\rho} \cdot \nabla \widetilde{p^{(1)}} \\
&= \frac{1}{\rho} \nabla^2 \widetilde{p^{(1)}} + \left(\nabla \cdot \frac{1}{\rho} \nabla \widetilde{p^{(1)}} - \frac{1}{\rho} \nabla^2 \widetilde{p^{(1)}} \right) \\
\Rightarrow \widetilde{\rho} &= \left(\overline{1/\rho} \right)^{-1}
\end{aligned}$$

+ Harmonic average is proportional to local minimum

- **Constant coefficient**
  - \+ Direct solver $\rightarrow$ fast solution
  - − Extrapolation is potential source of error
  - − Does not recover $\boldsymbol{\nabla} \cdot \boldsymbol{u}^{k+1} = 0$ in inviscid case[4]
- **Variable coefficient**
  - \+ Obeys $\boldsymbol{\nabla} \cdot \boldsymbol{u}^{k+1}$ constraint
  - − Iteration is potentially very expensive!

[4] Nicoud (2000)

Testcases

2D Non-Isothermal Mixing Layer - Initial & Boundary Conditions

- Hyperbolic tangent velocity profile

$$u\left(y\right) = \frac{u_1 + u_2}{2} + \frac{u_1 - u_2}{2} \tanh\left(\frac{2y}{\delta}\right)$$

$$u_c = \frac{u_1\sqrt{T_2} + u_2\sqrt{T_1}}{\sqrt{T_1} + \sqrt{T_2}} = 0$$

$$\frac{T_2}{T_1} = \frac{1}{2}\,,\ \frac{dp^{(0)}}{dt} = 0$$

- Initial perturbation applied to velocity field to promote transition
- Periodic in x no-slip on y

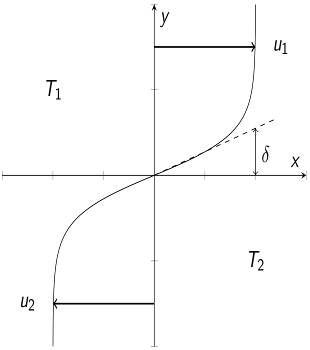
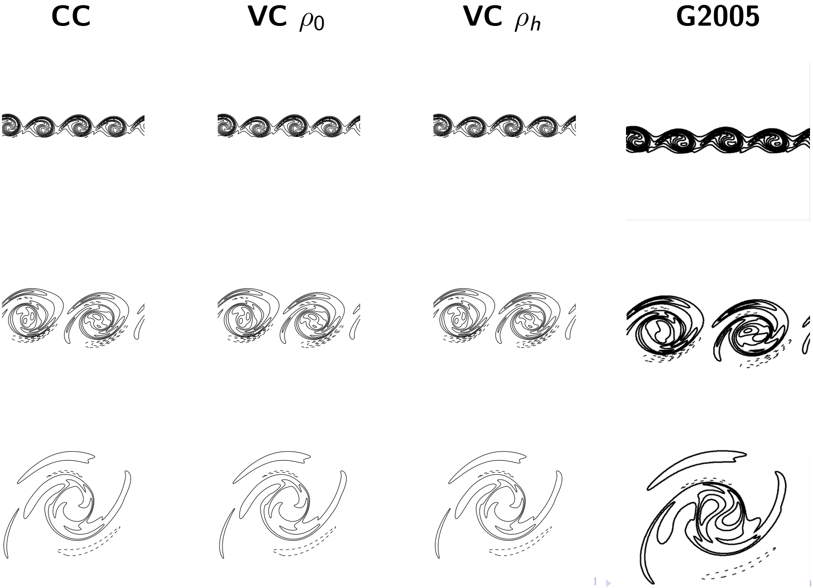


Figure: Diagram of non-isothermal mixing layer

Testcases

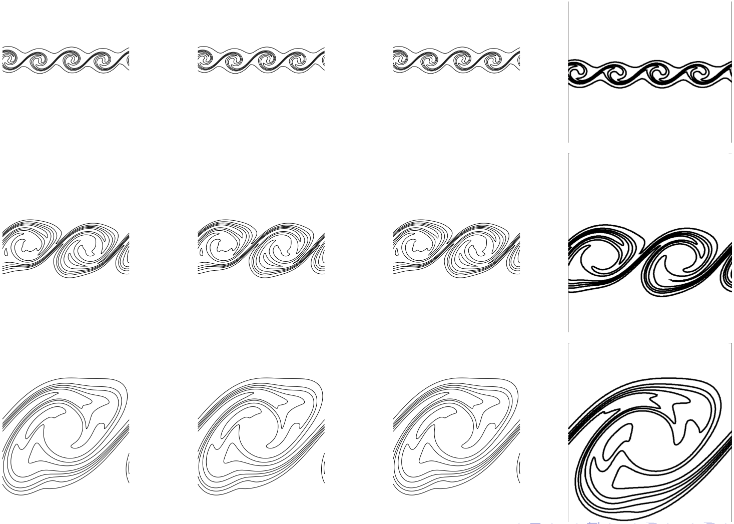
2D Non-Isothermal Mixing Layer - Results (Vorticity)



Testcases

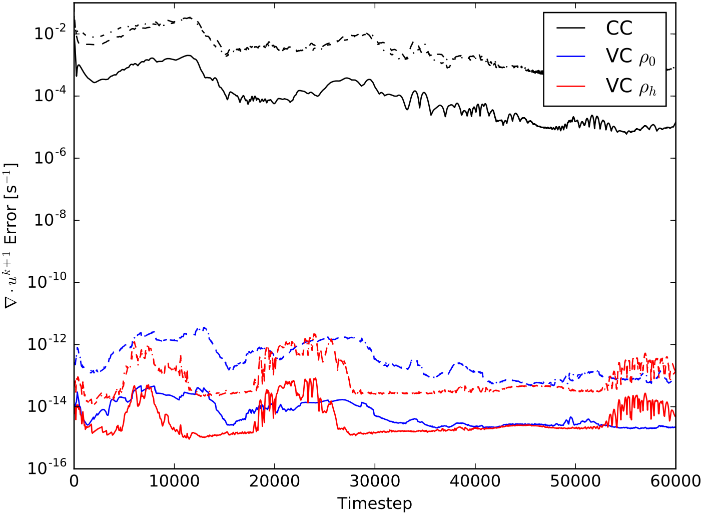
2D Non-Isothermal Mixing Layer - Results (Density)

CC **VC ρ_0** **VC ρ_h** **G2005**



Testcases

2D Non-Isothermal Mixing Layer - Results (Error in $\nabla \cdot \boldsymbol{u}^{k+1}$)



Testcases

2D Non-Isothermal Mixing Layer - Results (Performance Comparison)

Poisson Eq.	CPU / Δt [s]
CC	4.48×10^{-2}
VC ρ_0	6.16×10^{-1}
VC ρ_h	3.53×10^{-1}
	Cost (normalised)
CC	1
VC ρ_0	13.75
VC ρ_h	7.88
	Time in Poisson [%]
CC	23.4 (1)
VC ρ_0	94.2 (34.1)
VC ρ_h	89.9 (18.8)

- Jet is heated above ambient ($T_j = 568\ K,\ \ T_a = 300\ K$)
- Convective outflow boundary condition, convecting velocity chosen to satisfy

$$\frac{dp^{(0)}}{dt} = 0$$

$$\Rightarrow \int_{\partial\Omega} \boldsymbol{u} \cdot \widehat{\boldsymbol{n}} dS = \frac{\int_{\partial\Omega} k \boldsymbol{\nabla} T \cdot \widehat{\boldsymbol{n}} dS}{p^{(0)} RePr}$$

- Free-slip applied at lateral boundaries

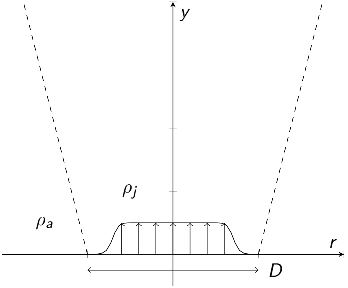


Figure: Diagram of jet

Testcases

Jet - Results

Conclusion and Future Work

- LMN implemented in `Incompact3D`
- Implemented constant and variable coefficient Poisson solvers
- Proposed new formulation for variable coefficient Poisson solver

- Complete simulation of buoyant, turbulent jets
- Multicomponent flows

Thanks for listening!