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A Molten Salt Fast Thermal Reactor System with no Waste

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Abstract

A Power system of 1 GW(e) containing a fast breeder reactor (2GW(t)) with a molten chloride fuel and a thermal burner reactor (~ 0,5 GW(t)) with molten fluoride fuel resulting in a total breeding system with a doubling time of 30 years is described.

The fast breeder works on a U-238/Pu-239 cycle, the thermal burner on Pu-239. The thermal burner 'incinerates' (by neutron transformation) most of the long lived fission products. Kr-85, Sr-90, Tc-99, Cs-135 and other. The actinides (Np, Am, Cm) might be recovered from the molten salt with a high efficiency and then burnt up in the fast reactor. The entire system produces no long lived radioactive wastes with the exception of T and partially Cs-137.

The fast reactor has an inherent stability against power excursions, and loss of coolant accidents because of the two or more independent cooling circuits and in which the fertile material (molten uranium chloride) plays the role of coolant.

A very high efficiency aluminium-chloride secondary coolant and turbine working agent is proposed. Together with a district heating system practically no thermal pollution occurs.

A very low I-131 and Xe-133 and low Cs-137 concentration, and very low CsCl volability in the steady state core due to continuous gas extraction guarantees the high safety level of this system.

I. Why a new reactor system?

The present generation of power reactors both thermal and fast both liquid-cooled (water or sodium) and gas-cooled, use solid fuel. The single reactor type with positive experience of liquid fuel is the Molten Salt Breeder Reactor (thermal reactor with molten fluoride and with breeding ratio ~1.05) (Rosenthal, 1972). Some other molten salt fast reactors have also been discussed in the literature over several years (Taube, 1961, 1967, Nelson 1967).

The liquid fuel molten salt reactors have some specific characteristics which make them more attractive for future use, especially in form of a coupled system of two molten salt power reactors as is proposed here

- 1) a fast breeder reactor with molten chloride fuel
- 2) a thermal burner with molten fluoride fuel.

This system appears to have the following special features which results in a reactor unit much more fitted to the future pattern of energy production than are the present day solid fuel reactors:

- 1) high inherent stability
- 2) much smaller environmental hazard
- 3) elimination of long lived fission product wastes and other radioactive wastes
- 4) better suited to district heating systems with a relatively high thermal efficiency for electricity generation.

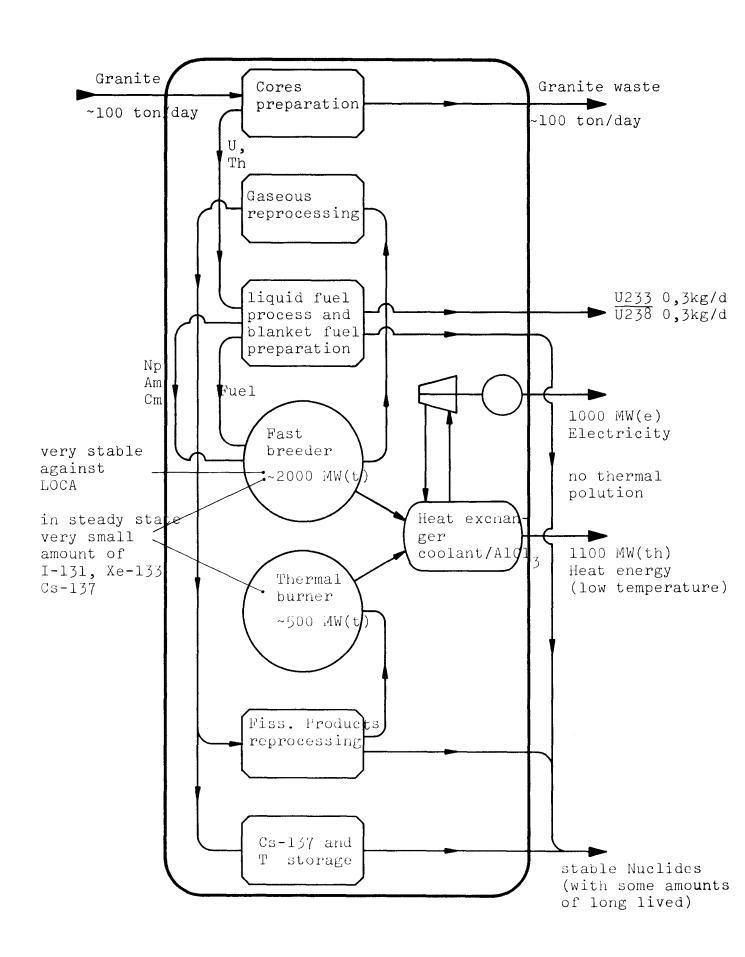
The "fast breeder - thermal burner" system proposed here has the following specific characteristics

- 1) inherent stability against power excursions which arise out of the following chain of events: criticality increase+ power excursion + temperature increase + density decrease + movement of part of the fuel out of the core + very strong negative influence on the criticality.
- 2) in the fast breeder reactor the loss of coolant is at the same time the loss of blanket which results in a very high negative coefficient of reactivity in this "Loss of Coolant Accident". The reactor thus shuts down without an engineered scram.
- of a hydrogen/helium stream for extraction of the volatile fission products especially the most hazardous I-131 and Xe-133 and also I-137, Xe-137, the volatile precursors of Cs-137 which have a large effect on the environmental impact in any reactor accident.
- 4) continuous reprocessing of liquid fuel with extraction of the long lived fission products (e.g. Kr-85, Sr-90, Zr-93 Tc-99, I-129, Cs-135) and the burning (neutron transformation) of them in a thermal reactor.
- 5) continuous reprocessing (with high yield) of the actinides (Np, Am, Cm) and continuous burning in the fast core.
- 6) the possibility of having a combined breeding ratio for both the fast and thermal reactors coupled together, greater than 1, achieving a doubling time of approx.

 30 years.

- 7) with the exception of tritium, virtually no nett rejection of radioactive wastes to the environment, if Cs-137 has been stored practically all the waste is transformed in the form of stable or semi-stable nuclides.
- 8) some of the corrosion processes of molybdenum (structural material) occuring in the core and blanket may be controlled by the continuous gas purging system.
- 9) the high thermal efficiency for electrical energy production of the total power system (55 % for only electrical, or 40 % for combined electrical and district heating system) results from the use of a chemically dissociating medium as secondary coolant and turbine working agent $(AlCl_3)$.
- 10) the system would seem to be suitable for an underground and fully automatic power plant of high safety.
- 11) this type of reactor gives, as do other molten salt systems, a complete independance from foreign supplies (no fuelelement manufacture, no external reprocessing plant) and has the ability to 'burn-rocks' i.e. low grade uranium "ores" from granites.

 (see Fig. 1)



II. The fast breeder - thermal burner coupled system

The total power system of approx 1 GW(e) contains:

- 1) fast breeder reactor with molten plutonium-chlorides fuel cooled in core by means of fertile material (uranium-238 chloride as fertile and coolant) The thermal power is approx 2000 MW.
 - In the coupled fuel cycle the breeder with a breeding ratio of ~ 1.4 form the basis of the breeding ratio of the entire system of 1.1 giving a doubling time of approx 30 years. In the fast reactor are also some of the long lived fission products being held under the neutron flux.
- thermal burner reactor with molten plutonium fluoride fuel, cooled externally (out of core). The thermal power is approx 500 MW. In the coupled fuel cycle the burner (with breeding ratio equal to zero; no fertile material) is responsible for the burning of the longest lived fission products coming from both reactors fast and thermal that is from total power of 2500 MW(t).
- 3) an appropriate power and heat generating system with the following circuits
 - reactor fuel in core cooling agent (molten uranium Salt)
 - secondary coolant out of core (aluminium trichloride)
 - tertiary coolant (e.g. nitrogen dioxide)
 - hot water for district heating.
- 4) multi-stage multicomponent reprocessing system with the following units.
 - reprocessing of the fast core fuel, including preparation of fresh fuel

- reprocessing of the blanket material from the blanket of the fast reactor
- preparation of uranium chloride from natural uranium oxide
- reprocessing of the thermal core fuel
- reprocessing of the irradiated solid or molten long lived fission products
- reprocessing of the in-core gas purge.

(see Fig. 2)

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Since the system contains both breeder and burner reactors and since a combined breeding ratio greater than 1 is required the relationship of the power of the fast breeder and thermal burner is the highest importance.

The problem of the achievement of the breeding ratio for the total system can be solved by the following simplified calculations concerning the ratio between the respective powers.

Fig. 2 Fast/Thermal Reactors System

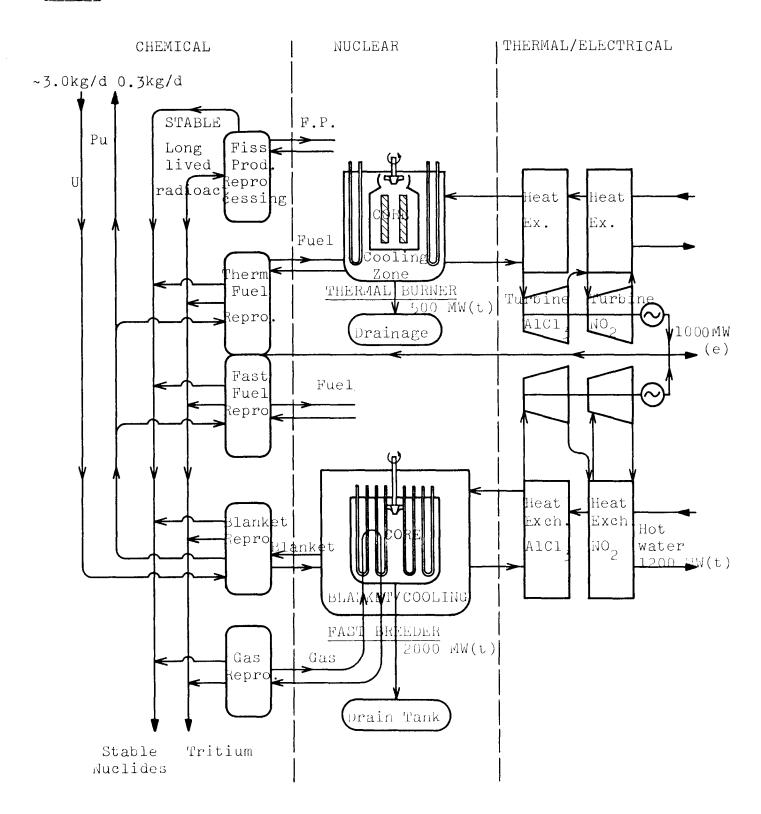


Table 1 Calculation of the fast breeder/thermal burner ratio

	<u>Unit</u>	Fast breeder	Thermal burner
Total power	MW(t)	Х	1
Specific power	gPu/MW(t)		
in core		P _f = 1000	P _t = 20
in total system including repro- cessing	gPu/MW(t)	P _f = 1100	P _t = 80
Plutonium burning	gPu/MWd(t)	F ≅ 1.1	F ≅ 1.1
Breeding ratio	gPu/MWd(t)	$B^{\mathbf{f}} = 1.35$	$B^{t} = 0$
Losses in the reprocessing system and uncertainties	gPu/MWd(t)	V = 0.05	V = 0.05
Breeding gain	gPu/MWd(t)		
G=F.(B-1-V)		F.(1.35-1.0-0.05)=	F.(0-1.0-0.05)=
:		= + F. 0.30	= -F. 1.05
Postulated doubling			
time: T ₂	years/days	≃ 30 years	~ 10 ⁴ days
Needed breeding gain		$g^{total} = X.P_f + P_t$	= 10 ³ ≅ 0.1

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Effective (total breeding gain for fast/thermal system:

$$G^{\text{tot}}$$
 = X·F·0.3 - F·1.05 = 0.1
The fast/thermal power ratio: $X = \frac{1.05 + 0.1}{0.3} = 3.9 \approx 4$

For a self-breeding system containing fast breeder and thermal burner the following power distribution is needed (B = breeding ratio)

- fast breeder reactor (
$$B^{fast} = 1.35$$
) 4 MW(t)

- total coupled system (
$$B^{syst} = 1.1$$
) 5 MW(t)

or for a total power of 2500 MW(t):

- fast breeder: 2000 MW(t)

- thermal burner: 500 MW(t)

A very rough estimation of the characteristics of both reactors is given in Table 2.

More details about the fast reactor are given in Chapter 3 and the thermal reactor in Chapter 4.

Table 2

Brief characteristics of the "Fast breeder/thermal burner" system

Total electrical power = 1 GW(e)Total efficiency (arbitrary) = 40 % Total thermal power = 2.5 GW(t)

		Fast Breeder	Thermal Burner
Reactor, total power	MW(t)	2000	500
Specific power (per unit volume)			
in core	MW(t)/litre	1.22	2
in reactor with coo- ling region but with- out blanket		0.22	0.225
Core volume	litre	8750	250
Cooling region volume	litre	same as core	2000
Neutron flux	$n cm^{-2}s^{-1}$	7 x 10 ¹⁵ *	6 x 10 ¹⁵
Core volume composition	vol %		
Fuel-liquid	11	38.6	1.1
Moderator	11	none	homogeneous fuel; BeF ₂ as moderator
Coolant	11	55.5 (in this case the fertile material)	no coolant in the core; external cooling
Fission products	11	no special volume for F.P.	84 in the core
Tubes	11	5.9	5

Table 2

Blanket	m ³	47.85 (UCl ₃ as fer- tile ³ material)	no blanket
Role in fuel cycle		Breeding of Pu in U-238/Pu-239 cycle	Burning of long lived F.P.
Breeding ratio		~ 1.35	0
Fuel components fissionable		Molten chloride Pu-239 + other actinides (Am, Cm	Molten fluoride Pu-239)
diluent		NaCl	Zr F ₄
moderator		no	BeF ₂
Irradiation target (fission products)		Zr isotopes (?)	Kr-85, Cs-135, Sr-90, Tc-99. I-129
Literature		(Taube, Ligou 1973)	For thermal breeder reactor with molten fluorides fuel see (Rosenthal, 1972)

^{*} here for calculation purpose a neutron flux of 8 x 10^{15} is postulated, however a flux of 10^{16} n cm $^{-2}$ s $^{-1}$ seems realisable.

III. The Fast Breeder Reactor

In this study a 2000 MW(t) fast breeder molten chlorides reactor was used. (Fig. 3 and 4)

The detailed describtion of the reactor type was recently given (Taube, Ligou, 1973). The most important characteristics are summarised here: (Table 3 and 4)

- 1) the liquid fuel contains only plutonium chlorides diluted by other metal chlorides. The in core breeding ratio is realised by the presence of the uranium-238 chloride (diluted by other metal chlorides) which acts as the cooling agent flowing in the tubes.
- 2) the fertile material (238 UCl₃/NaCl) is at the same time the cooling material and the blanket material.

A very important and desirable feature of this fast reactor can be seen when the "maximal design accident" is discussed. This appears to be the Loss of Cooling Accident (LOCA) (Fig. 5)

The LOCA in fast reactor arises from two events.

the increase of criticality due to each coolant (even helium) being a neutron absorber and the loss of coolant results in an increase of neutron flux in the core (a trivial point is that in a thermal water cooled reactor "the Loss of Coolant" is also a "Loss of Moderator" which reduces the criticality); thus in a fast reactor the LOCA must be accompanied by an engineered shut-down device.

Fig. 3 CHLOROPHIL / EIR 2 GW(t)

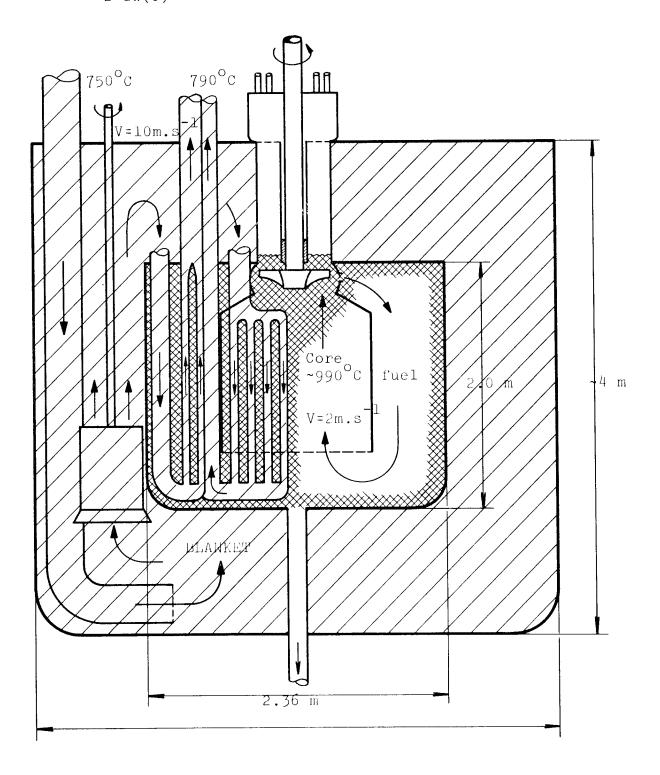
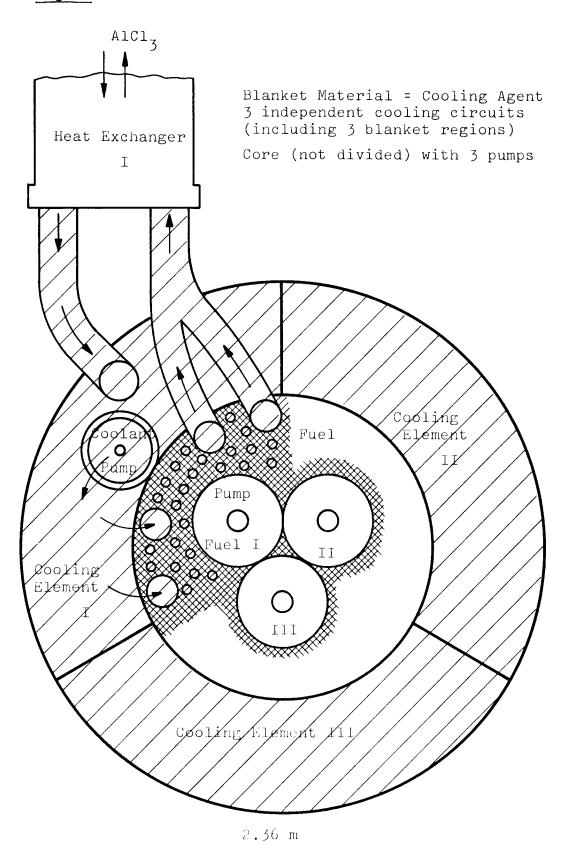


Fig. 4 CHLOROPHIL EIR



4.26 m

Table 3

Molten Chloride Fast Breeder Reactor (MCFBR) "CHLOROPHIL"

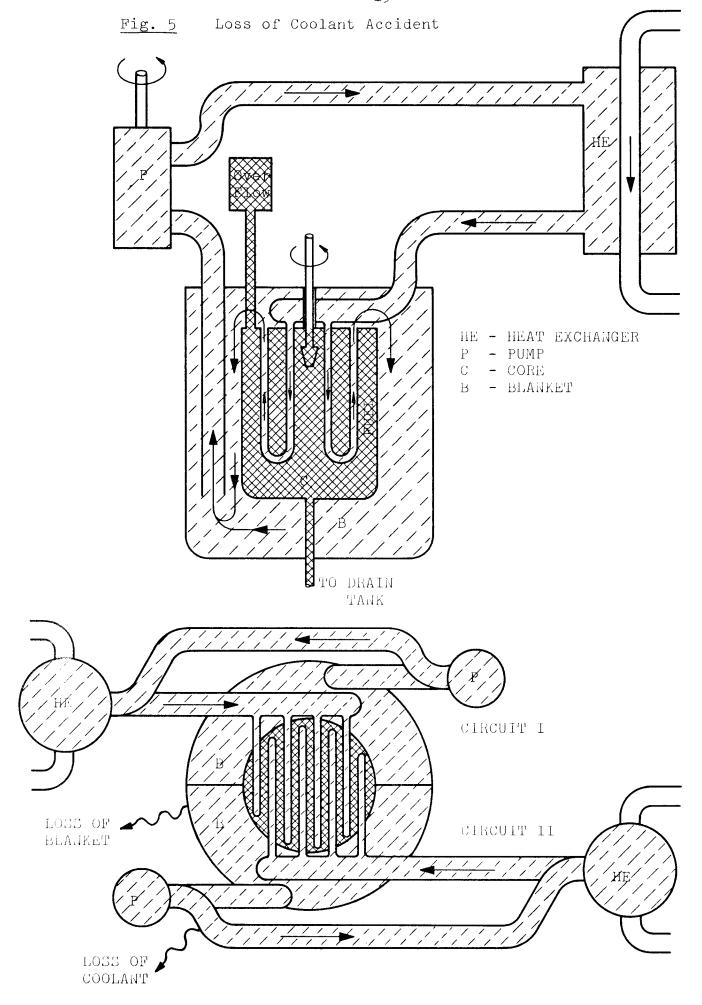
MW(e)	~ 800
MW(t)	2050/1940
3	8.75
MWm ⁻³	220
m	height 2.0/ 2.36 diameter
Mol%	16/18
,	~685/~1500 (approx)
°C	984
	0.386
	0.60/0.78
$n cm^{-2}s^{-1}$	$7 \cdot 10^{15}$
kg m ⁻³	2344
	0.95
$g cm^{-1}s^{-1}$	0.0217
$W cm^{-1}K^{-1}$	0.007
kg	7900
kg	2900/3150
weight %	36.4
MW(t)kg ⁻¹	0.67
	0.62
	MW(t) m ³ MWm ⁻³ m Mo1% oC oC oC c c w m Mo1% oC oC c c c c c c c c c c c c c c c c c

Table 3

Coolant liquid U-238 Cl ₃ /NaCl Liquidus / Boiling point Coolant temperature inlet/outlet Coolant volume fraction in the	Mol % OC OC	65/35 ~710/~1700 750/793
Coolant density Coolant salt in core/ in blanket	kg m ⁻³	0.555 4010 19'500/165'000
Thermohydraulics Fuel (shell side, pumped), velocity Coolant, velocity Number of coolant tubes Tubes inner/outer diameter	ms ⁻¹ ms ⁻¹	2 9 23'000 1.20/1.26
Breeding ratio, internal/ total Doubling time, load factor 1.0/0.8 years	cm	1.38 0.716/1.386 8.5/10.5

Table 4 Fast breeder neutron balance

Region		Atoms cm ³ ·10 ²¹	Absorption %	Leakage %	Production %
	U-238	3.5629	25.50 (n,γ) 22.51 (n,f) 2.99		8.23
	Pu-239	0.66796	34.56 (n,γ) 5.58 (n,f) 28.98		85.55
	Pu-240	0.16699	3.78(n, f) 2.24 (n, f) 1.54		4.72
	Na	6.3017	0.26		
CORE	Cl	19.495	3.16 in fuel 1.10 in cool.2.06		
	Fe	5.978	1.30		
	Мо	0.7386	2.04		
	F.P.	0.0679	0.50		
Total Core			71.10	27.40	98.50
	U-238	6.42	23.70(n,f) 23.15 (n,f) 0.55		-1.50
BLANKET	Na	3.457	0.08		
BLA	Cl	22.72	2.22		
Total Blanket			26.00	2.9	1.50



2) the radioactive decay heat of fission products is approx 7 % of the normal steady state power level and is high enough to melt the clad and in some cases the fuel in a few tens of seconds from the LOCA, especially in fast reactors with a high volumetric specific power.

The "Emergency Core Cooling Systems" are still under critical review.

Here in this type of fast reactor, both "negative" effects of LOCA could be virtually eliminated by means of the following design features (not shut-down devices):

- the cooling system is coupled with the blanket, that is the cooling agent plays the role of fertile blanket material.
- 2) the cooling system including the blanket region is divided into two or more fully independent circuits.
- 3) it is postulated here that a major accident will cause complete destruction of all but one of these independant circuit systems and one of the fuel pumps is intact.
- 4) the cooling system sub-divides into several if not all parts of the cooling region.

During an accident the loss of coolant accident thus brings about a corresponding loss of blanket in the region affected. The loss of blanket gives a very strong negative coefficient of reactivity which is clear from Table 4. The roughly estimated value is approw $(7 \pm 1\%)/N$ where N is the number of independant cooling/blanket circuits. In this reactor a failure in only one out of four circuits results in a reactivity decrease of $(7 \pm 1\%)/4$ which is equivalent to a full scram.

Thus the reactor stops without the use of any engineered devices. It seems that this is the only type of fast reactor with inherent negative criticality against the Loss of Coolant Accident.

The radioactive decay heat still has to be removed, if not, the vessel and cooling tubes may melt down. In this reactor the one remaining intact cooling circuit is able to remove this heat, because the molten fuel acts as the internal heat transport medium and assists the heat removal to the one intact system.

IV, The thermal burner reactor

As is shown in chapter VI the most effective neutron transformation of a large part of the long lived fission products is possible in a thermal neutron flux because the products of cross section and flux $(\sigma_j \cdot \emptyset_j)$ is often larger for thermal neutrons $(\emptyset_j = 16)$.

This is one of the reasons for using a thermal burner for the transformation.

Some general remarks about the criteria for this thermal burner are given below:

the thermal neutron flux must be as high as possible but as will be show there is an upper limit. It appears that a flux of $3 - 6 \times 10^{15} \text{n cm}^{-2} \text{s}^{-1}$ is most suitable (e.g. for $\sigma_{\text{th}} = 5 \text{ barns}$; $\sigma \cdot \emptyset = (5 \times 10^{-24}) \times (6 \times 10^{15}) = 2 \times 10^{-8} \text{s}^{-1}$ which corresponds to an effective half life of 2.25 years).

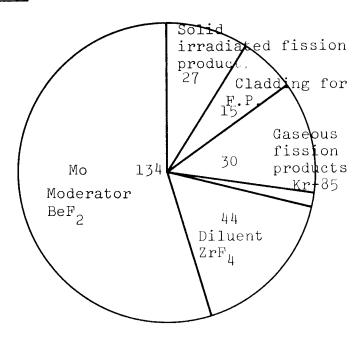
- 2) the specific volumetric power should not be too high because the thermal core volume and the neutron balance has to be kept to a size to accommodate the appropriate amounts of neutron absorbing fission products (e.g. specific power 1-2 MW/litre) (for 1 MW/l the core volume is 500 l, for 2 MW/l the volume is ~250 l).
- 3) the specific power per unit volume must not be too high to keep the total power down. The thermal core is intended as a burner only, that is with breeding ratio zero.
- 4) the core containing only fissionable nuclide, moderator and appropriate fission products must give the best possible neutron balance. The following two postulates are added.
- 5) no fertile material in the core
- 6) no coolant in the core except for the fuel itself which is cooled by means of out of core heat exchangers. The fuel is also in liquid form to permit continuous reprocessing.

As will be seen from the following discussions the apropriate specific volume power for this core is choosen to be as high as possible: 2 MW/1.

(HFIR Reactor in Oak Ridge, USA; 100 MW(t): 100 litre core; 1 MW/1) CM-2 Reactor in Mellekes, Soviet Union 50 MW(t); litre; MW/1 both with mean neutron fluxes of 6×10^{15} n cm⁻²s⁻¹. It must be stressed that a more conservative figure of 1 MW/1 and flux of 3×10^{15} n cm⁻²s⁻¹ would also meet the requirements but of course with lower effectiveness (higher steady state concentration of fission products). Fig. 6 and 7 give some details concerning the thermal high flux burner. Some datas concerning the neutron balance of the thermal burner reactor are given on the Table 5.

It is worh mentioning the possibility of a neutron coupled fast/ thermal system which would help to solve the problem should the thermal burner reactor have too small a k_{∞} due to the large amounts of neutron absorbing fission products present. In reducing the leakage from the thermal reactor it could be that neutron coupling will improve the entire neutron balance raising the system breeding ratio over 1.1. (Fig. 8)

Fig. 6 Core Volume Composition (Vol%)



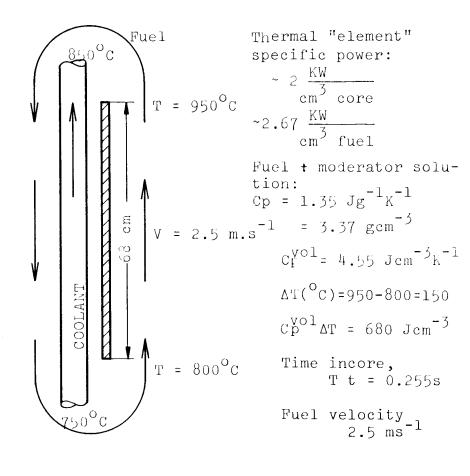
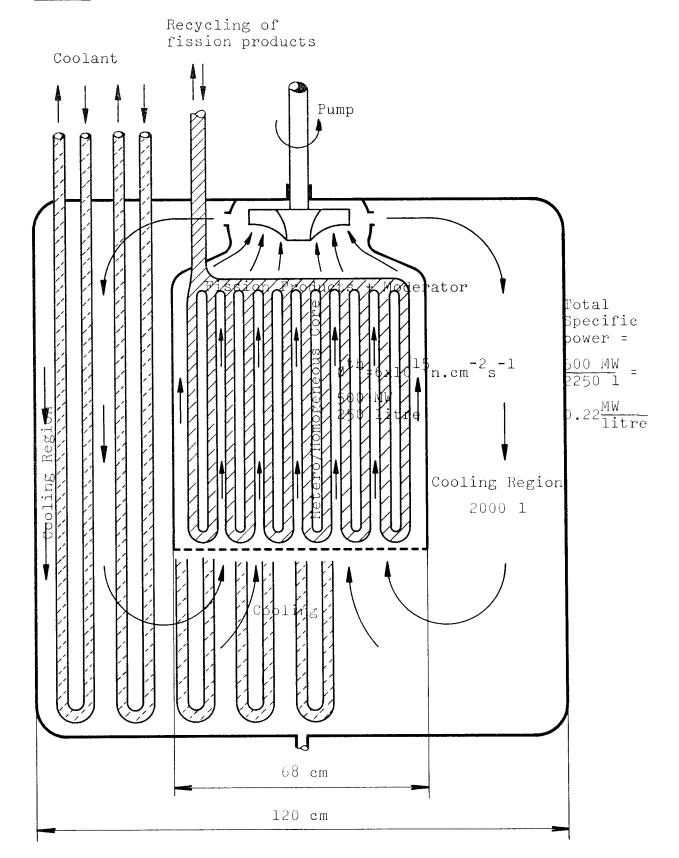


Fig. 7 Thermal Reactor Burner



Not to scale

Table 5

First approximations of the thermal burner reactor neutron balance

Total power: 500 MW

Specific power: MW/l Volume: 250 litre

Thermal neutron flux: $\emptyset_{th} = 6 \times 10^{15} \text{ n cm}^{-2} \text{s}^{-1}$

2 MW/l gives $\sim \frac{2 \times 10^6}{10^{-3}}$ = 2 x 10³ W/cm³

Fission rate $2 \times 10^3 \times 3.1 \times 10^{10} \text{ fiss/W} = 6.2 \times 10^{13} \text{ fiss/cm}^3$

Plutonium atoms: $N_{cm}^{Pu-239} = \frac{6.2 \times 10^{13}}{(7.2 \times 10^{-22}) \times (6 \times 10^{15})} = \frac{6.2 \times 10^{13}}{4.3 \times .0^{-6}} =$

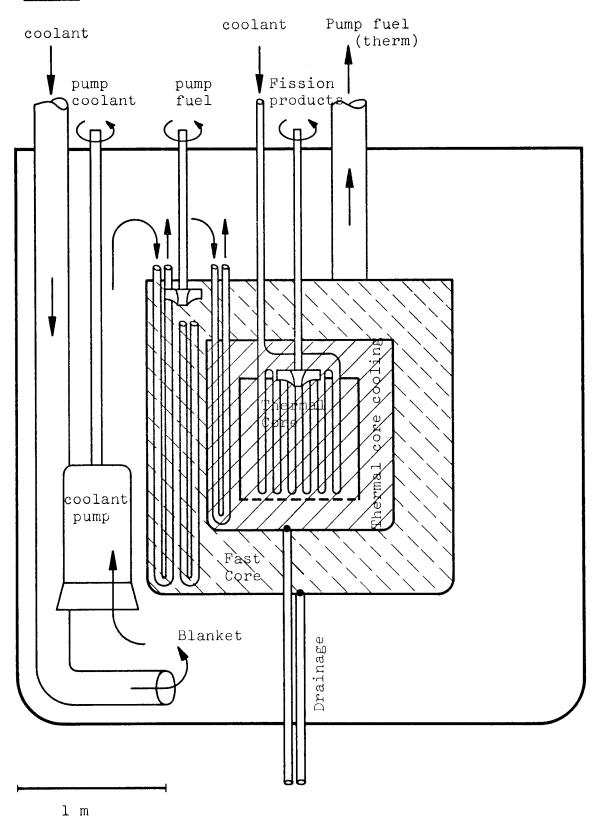
= $1.45 \times 10^{19} \text{ Atom Pu/cm}^3$

For 250 litres: N^{Pu-239} = (1.45 x 10^{19})x(2.5 x 10^{5}) = 3.6 x 10^{24} = tot = 6 Mol Pu-239

Table 5

Volume	Fuel	Amount in steady state	Cross Section	Neutron Balance		i i
(litre)		(mol/in core)	(otherm,barn)	Absorption Pro		Production
1	Pu-239/241	6 Mol (80%)	σ _f = 720 σ _c = 250	4320 1500	36 12.5	100
	Pu-240/242	1.2 Mol (20%)	σ _c = 250	300	2.5	
	Irradiated Fiss	sion products				
11	Sr-90	350 Mol	1.20	420	3.5	
2.3	Tc-99	57 Mol	22.0	1260	10.5	
7	Cs-135	185 Mol	8.7	1600	13.3	
	I - 129	7 Mol	35.0	245	2.0	
0.5	I-127	14 Mol	6.0	85	0.7	
30	Kr-85	68 Mol	1.8	120	1.0	
	Diluent/Mc	oderator —				
	BeF ₂	5100 Mol	0.01	150	1.25	
	ZrF ₄	ll00 Mol	0.03	100	0.8	
15	Structure (tubes Zr)	1100 Mol	0.3	300	2.5	
250 litr	e <u>Leakage</u>			1600	13.3	
	Totals			1200 0	100%	100

Fig. 8 Fast/thermal system



V. The in-core continuous gas purging

V.a) General remarks

In this reactor an in-core continuous gas purging of the molten fuel is postulated which significantly improves the safety of this reactor in an in-core accident.

A mixture of hydrogen-helium gas is continously bubbled through the liquid fuel in the core. The mean dwell time of the gas-bubbles needs to be controlled and the mean transport time of the molten components to these bubbles must also be controlled (e.g. if speed-up is desired-intensive mixing, if delay-local addition of a further gas stream).

The aim of the gas stripping is as follows:

- 1) to remove the volatile fission products which in the case of an accident control the environmental hazard. (I-131, Xe-133, Kr-85 and precusors of Cs-137 and at the same time for the thermal reactor, removal of the I-135, precursor of Xe-135, improves the neutron balance.
- 2) to control the production of delayed neutrons since most of the precursors and nuclides of this group are very volatile, e.g.: Br-I-isotopes.
- 3) removal of oxygen and sulphur, continously (see Chapter VIII)
- 4) in situ control of corrosion problems on structural materials (see Chapter VIII).

For the sake of a first approximation a gas flux of 30 cm 3 per sec. (normal state) of $\rm H_2/He$ is arbitrarily assumed. At 20 bar pressure

and with a dwelling time in core of 20 seconds, the gas bubbles will only occupy a fraction of the core equal to 10^{-5} of its volume and has little influence on the criticality, (but the collapsing of bubbles results in a positiv criticality coefficient).

The system proposed for continuous removal of the volatile fission product from the core itself has a retention time of some hundreds of seconds only. Each reprocessing mechanism which operates out of core is limited by the amount of molten fuel being pumped from the core to the reprocessing plant. This amount, due to the high capital cost of the fuel and high operation costs cannot be greater than that which gives a fuel in-core dwell time of about one week. Even with a 1 day dwell time, that is, if a after one day the fuel goes through the reprocessing plant, no acceptable solution to the I-131 problem is obtained since the activity of this nuclide is only diminished by one order of magnitude (see Fig. 9).

Only a direct in-core removal gives the dwell time in core as low as some hindreds of seconds.

V.b) Delayed neutrons emitters

The principal question arise out of the fact that some of the short lived iodine and bromine (perhaps also arsenic, tellurium) isotopes are the precursors of the delayed neutrons.

Table 6 Precursors of delayed neutrons for Pu-239 fast fission

Group	<u>Half life</u> t 1/2 (seconds)	Fraction %	<u>Probable</u> <u>Nuclide</u>
1	52.75	3.8	Br-87
2	22.79	28.0	I-137, Br-86
3	5.19	21.6	I-138, Br-89
4	2.09	32.8	I-139, Br-90
5	0.549	10.3	
6	0.216	3. 5	

As other possible nuclides the following can be considered: As-85; Kr-92,-93; Rb-92,-93,-94; Sr-97,-98; Te-136,-137; Cs-142,-143. The removal of these delayed-neutron precursors from the core reduces the value of β , which is lower for Pu-239 than U-235.

Thus we have a problem of reaching a compromise between a removal as rapid as possible of the hazardous I-131, and as long a dwell time in the core for the delayed neutron precursors: I-140, I-139, I-138, I-137 and the appropriate bromine isotopes.

The compromise is given by a quasi-steady state regime in the core in which the amounts of isotopes present are given as an example in Fig. 10.

Fig. 9 I-131 in CHLOROPHIL

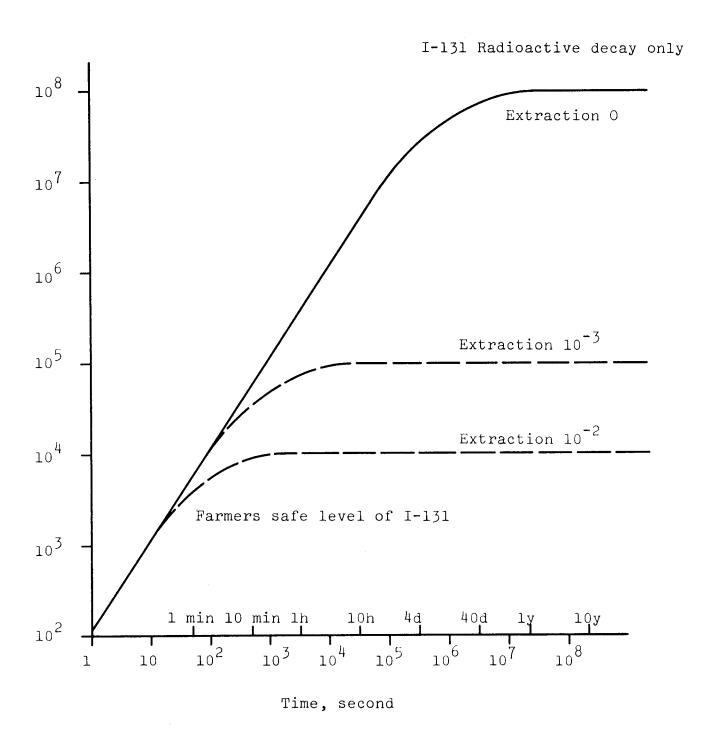
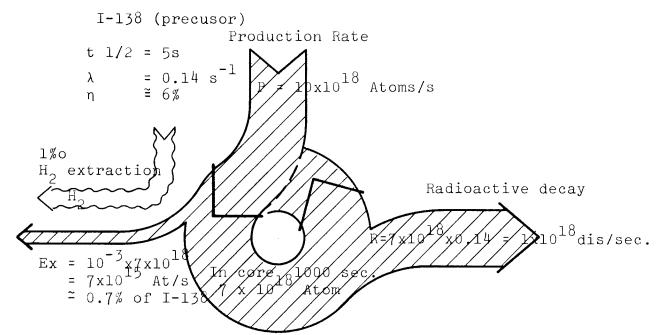
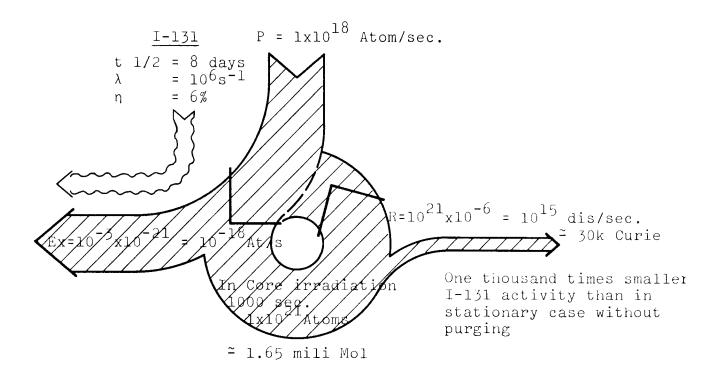


Fig. 10 Removal of I-131 in CHLOROPHIL I and the problem of the precursors of the delayed Neutrons $2 \text{ GW} = 6.2 \times 10^{19} \text{ fiss/sec.}$



Neutron loss = 0.7%



Without extraction: after approx 2 months \sim 30 Mega curies I-131 (1×10^{18} dis/sec)

In this case the mean dwell time of iodine in the steady state reactor is about 100 seconds. From the curve in Fig. 9 it can be seen that the activity of iodine for a 2.5 GW(t) reactor is of the order of only 10 k curies (for 100 seconds) instead of $\sim 100 \text{ M}$ curies in the steady state, a decrease of activity of approx. 10^4 (or 10^3 for 1000 second extraction rate).

V. c) Gas-extraction and other fission products

The gas-extraction also influence the other volatile nuclides. From a very rough estimation for these molten salts (with a small excess of free hydrogen) the following fission products and their associated precursors of iodine and bromine can be volatile at $\sim 1000^{\circ}$ C.

In elementary form: Xe, Kr, Te (?)

In simple volatile hydrides: BrH, IH

In simple volatile chlorides: SnCl₂, SbCl₃, NbCl₃, CdCl₂.

This amount of finally volatile components including I, Br, Xe, Kr amounts to approximately half the total fission products (i.e. 100 micromoles per second). In addition there is the corresponding amount of tritium (from ternary fission). This amount of all fission products corresponds to a gas volume ratio of about 2 cm³/s or 10 times smaller than the postulated amount of hydrogen flow at 30 cm³/s. For volatile fission products release: see (Farmer, 1973; Beattie, 1973).

The extraction removes all short lived fission products which are volatile under these conditions. Thus not only is the removal of the iodine isotopes and the consequent reduction in production of xenon (e.g. for the atom number: A = 135, 136, 137, 138, 139) achieved but it slows down the in-core production of Cs-137, Cs-138, Cs-139 and then also Barium-139 (Fig. 11).

The gas extraction will also cause the vaporization of the higher components of the liquid fuel: $PuCl_3$ and NaCl.

The fuel consists of:

- 15 mol% PuCl₃; boiling point 2040°K
- 85 mol% NaCl; boiling point 1738 K

(see Fig. 12).

One can as a first approximation say that it would have to following composition in the vapour phase: 5 mol% PuCl $_3$ - 95 mol% NaCl.

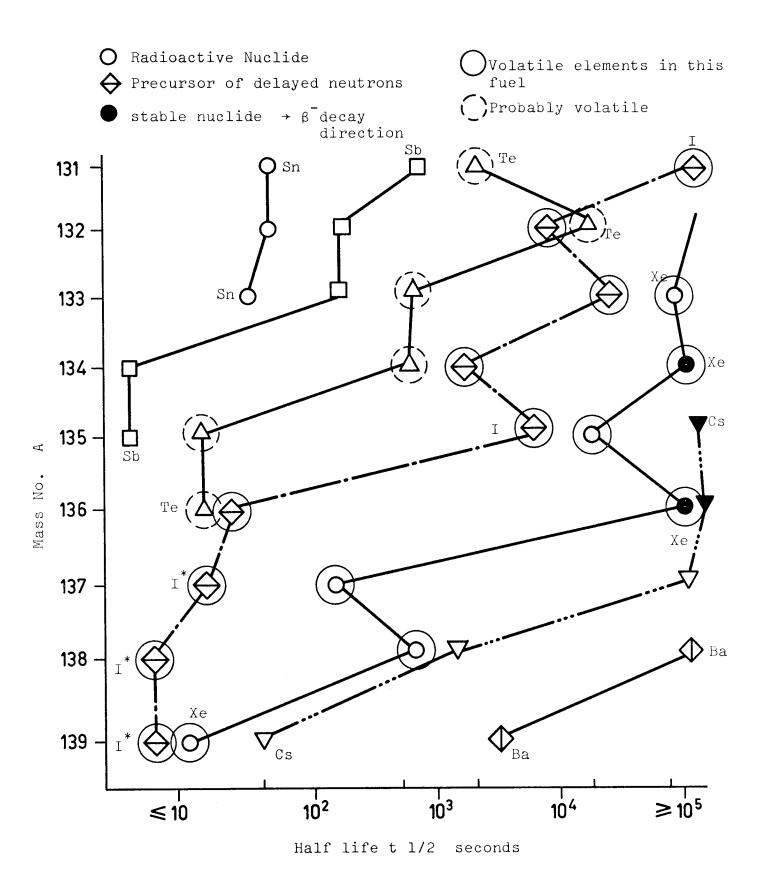
The order of magnitude of vapour for pure components at a temperature of about 1250 K is

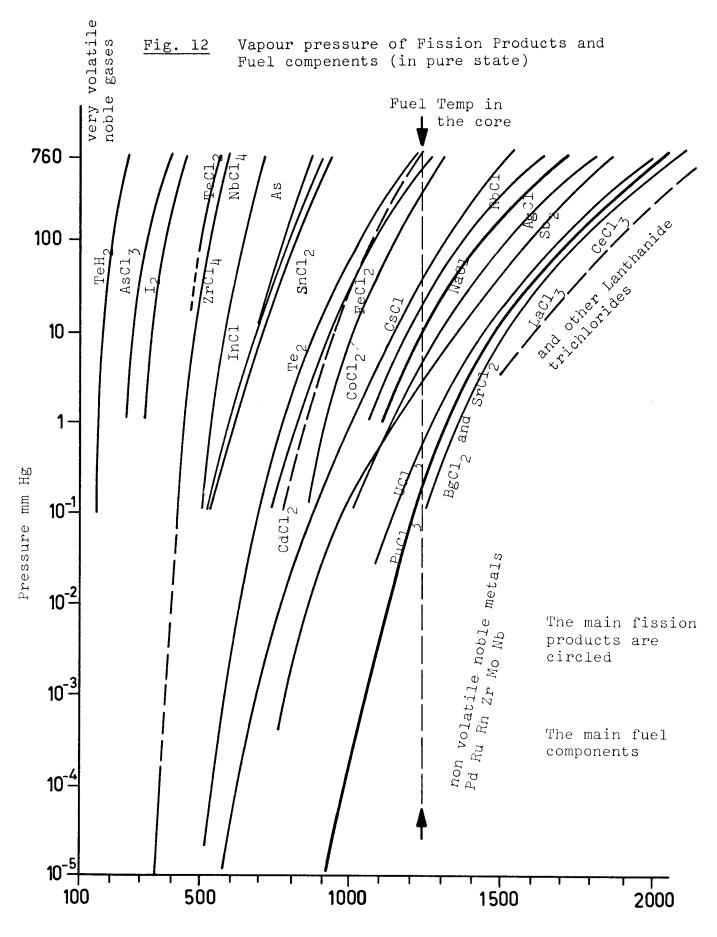
NaCl
$$\sim 5 \times 10^{-2} \text{ bar}$$
; PuCl₃ $\sim 10^{-4} \text{ bar}$

For the PuCl₃-NaCl system one assumes here a lowering of the vapour pressure (thermodynamic activity coefficient approx 0.1). At the postulated volumetric flow rate of $30~{\rm cm}^3~{\rm H}_2$ normal) per second, the vapourized amount of plutonium is given by:

$$\frac{30 \text{ cm}^3}{22000 \text{ cm}^3/\text{mol}} \cdot 10^{-4} \text{ bar} \cdot 10^{-1} = 10^{-8} \text{ mol Pu/s}$$

Fig. 11 Precursors of delayed neutrons





Temperature K

This amount of plutonium is of the order of 10^{-4} relative to the amount of plutonium fissioned in the same time (approx 10^{-4} mol Pu/s). However, it still has to be recovered which makes the reprocessing unfortunately more complicated.

Last but not least is the in-core gas extraction of two other elements

- oxygen in the form of H_2^0 : oxygen from impurities (i.e. Pu0C1)
- sulphur in the form of H_2S : sulphur from the nuclear reaction:

35
Cl (n,p) 35 S (see chapter VII)

VI. The neutron transformation of the fission products

VI. Principle of neutron transformations

Some of long lived radioactive nuclides are shown in Fig. 13 and 14.

The aim of this part of the paper is firstly to discuss the possibility of the steady state nuclear transformation (steady state burning) in the thermal neutron region, of the larger part of the long lived fission products. A first approximation for the solutions of this problem is given here and a further discussion initiated.

Mega Curies for USA ☐ Burning in CHLOROPHIL I/EIR Mega Curies for Europe ***** Burning in CHLOROPHIL II/EIR 104 Nuclide which cannot be burnt here Qs-137 Sr-90 10³-Kr-85 Activity - Mega Curies 10²-Pu-238 Am-241 Cm-244 10 1 Tc-99 1 -Pu-239 Zr-93 Gm-245 0,1-Cs-135 * 200 300 100 400

Fig. 13 Long lived radioactive wastes

Time from unloading from Reactor (at the year 2000)

Postulated hazard index for long lived fission Fig. 14 products and actinides 10¹⁸ Ingestion 10¹⁷ Sr-90 10¹⁶ Pu-239 Am-241 242 10¹⁵ -Cs-137 Pu-238 1014 Potential Hazard Index 10¹³ -100 10 200 0 Pu-239 10¹⁹ Am 241, 242 Inhalation Pu-288 10¹⁸ 10¹⁷ Sr-90 10¹⁶ Cs-137 10¹⁵ 1014 10 100 200

According to

The idea of destroying the beta-active long lived radionuclides is based on the following:

In Fig. 15 are given the nuclide transformations under a high flux discussed here.

This problem of nuclear transformation of fission and non-fissionable actinides, being the irradiation products, has been discussed for many years. The most recent remarks and calculations concerning this problem made the following claim: "It is not practical to burn fission product wastes in power reactors because the neutron fluxes are too low. Developing special burner reactors with the required (thermal) neutron flux of the order of 10^{17} n cm⁻²s⁻¹ or burning in the blankets of thermonuclear reactors is beyond the limits of current technology. It seems reasonable to extract three actinides (Np, Am, Cm, (M.T.)) for separate storage or for recycling through the reactors that produce them" (Claiborne, 1972).

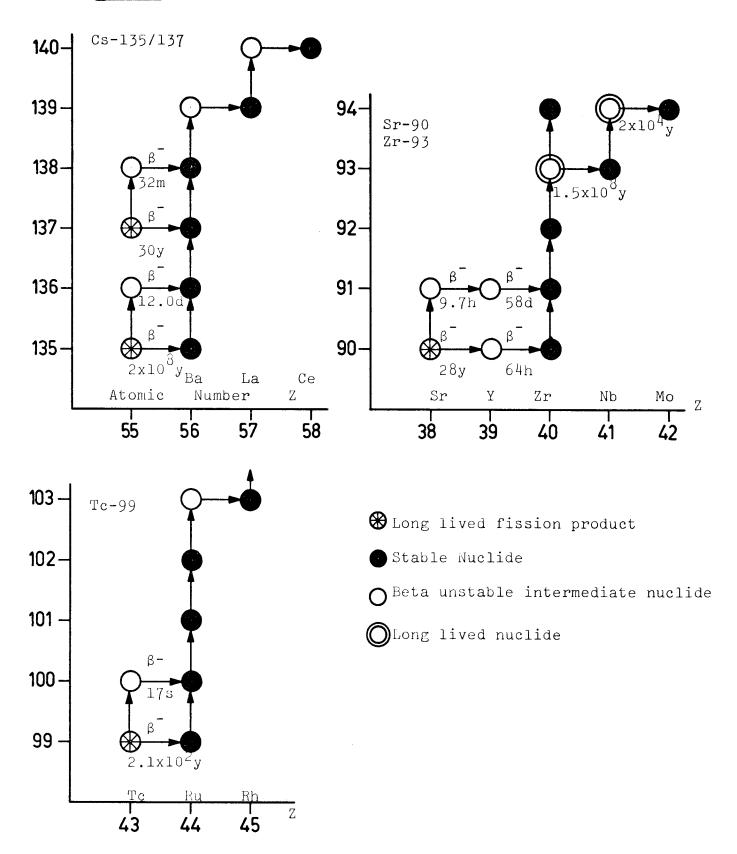
Also a controlled thermonuclear reactor CTR was used for calculation of neutron transformations. In those calculations a neutron flux of 5×10^{15} n cm⁻²s⁻¹ was used with remark that this flux level is somewhat higher than that usually associated with CTR power plants (Wolkenhauer, 1972, 1973). A three year irradiation was proposed but it would seem that for the most important fission products the neutron build-up in relation to the radioactive decay plays a relatively small role; e.g. for Strontium-90 after 3 years irradiation all neutron reaction products from (n,γ) and (n, 2n) are lower than 10% of those from the radioactive decay products Sr-90 and for Cs-137 only (n, 2n) products result in ~ 40% of the radioactive decay products. But (n, 2n) reactions need a rather hard neutron spectrum (Gore, Leonard, 1973).

VI. b Cross sections and neutron fluxes for nuclear transformations

In this system the following simple evaluations are made

- 1) the amount of fission pr-ducts coming from both the fast breeder (2000 MW) and the thermal burner (500 MW)
- 2) the cores are purged by means of gas (He + H_2 stream) for evacuation of some volatile nuclides (Kr, Xe, Br, I)
- 3) the fuels and blanket materials are continually reprocessed
- 4) the irradiated fission products are continuously (or periodically) separated for the sake of eliminating the daughter stable nuclides (e.g. Zr-90 and Zr-91 from the decay and burning of Sr-90)
- 5) the amounts C in steady state (ss) burning are calculated by the obvious relationship for the i-th nuclide.

Fig. 15 Burning of selected Nuclides



$$i_{ss} = \frac{px(3.1 \times 10^{10}) \text{ fiss.s}^{-1}w^{-1} \times \eta i}{(\lambda_{R}^{i} + \sigma_{j}^{i}\Phi_{j}) \times (6 \times 10^{23})}$$
 (mol)

P = thermal power (watts)

 η = yield (relative amount per 100 fissioned Pu-239/241 atoms)

 $\lambda_{\rm p}$ = radioactive decay constant (s⁻¹)

 σ = cross section (cm⁻²)

 Φ = mean neutron flux (n cm⁻²s⁻¹)

j = appropriate neutron spectrum (j = fast or thermal)

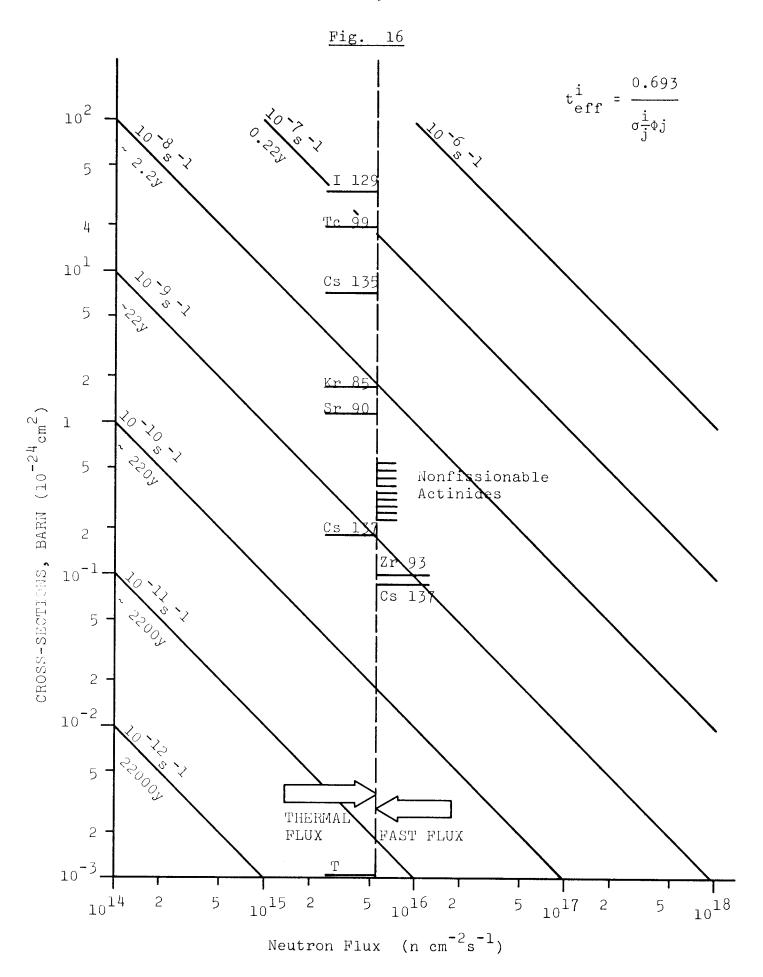
The most critical values $\sigma_j^i \sigma_j^i$ are given in Fig. 16 for some selected nuclides for thermal and fast neutron fluxes.

The calculation given above results in the following:

Burning in a thermal high flux power reactor $\emptyset = 6 \times 10^{15} \text{ n cm}^{-2} \text{s}^{-1}$

I - 129/127 (Fig. 18)

Burning in fast power breeder reactor: $\emptyset = 10^{16} \text{ n.cm}^{-2} \text{ s}^{-1}$



A more complicated problem is the need for the separation of the two caesium isotopes Cs-135 for thermal burning and Cs-137 for fast burning or out of core storage. From Fig. 11 it can be seen that the in-core gas extraction takes out the precursors of Cs-135, that is the long lived volatile I-135 and Xe-135, but the short lived precursors of Cs-137 remain in the fuel, so the separation of these isotopes is possible (see Chapter VII).

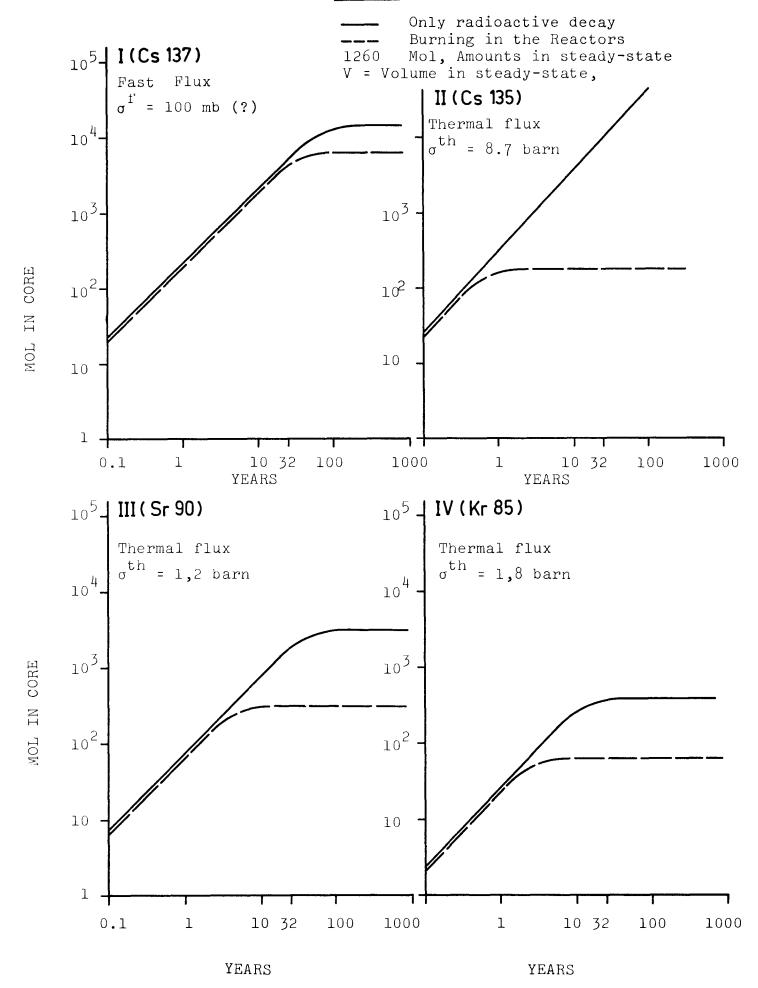
Among the most dangerous long lived radioactive wastes are some of the actinides (see Fig. 13, 14).

The problem of the "destruction" of these nuclides: Np-237, Pu-238, Am-241, Am-243, Cm-244, Cm-245, is simple. In any high flux fast or thermal reactor because of the relatively large cross sections these actinides are burned up, the problem is only limited by the present state of the reprocessing technology of irradiated fuel. In the most obvious aqueous processes e.g. the aqueous phase - organic phase extraction, these elements: Np, Am, Cm being hydrolysed, because of a relatively low concentration, and in the hydrolysed form are not extractable by many organic extractants. Of course a more refined aqueous process could give a significant improvement in the recovery of these actinides making it possible to recycle in the fuel and eventually to burn-up (Fig. 20 and 21).

In the fused salt fast-thermal system proposed here the recovery of the actinides seems much easier and simpler due to the fact that

1) the reprocessing occurs not in an aqueous but in a molten salt medium; the hydrolysis of the low concentration actinides is not possible; the recovery is very high.

Fig. 17



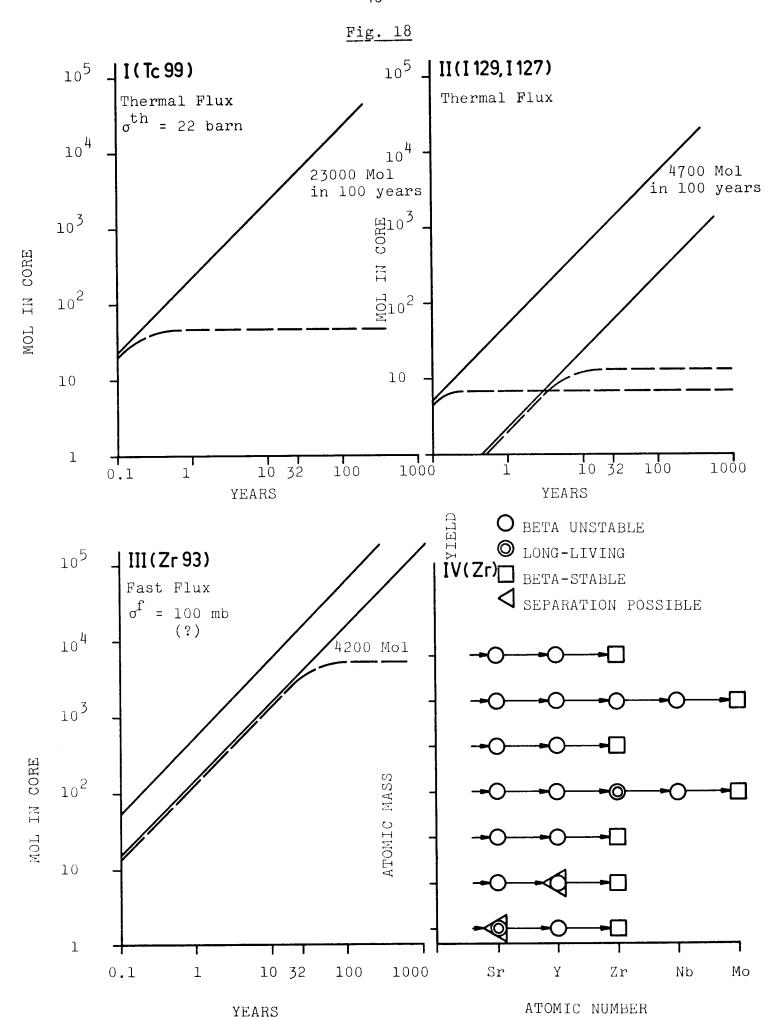
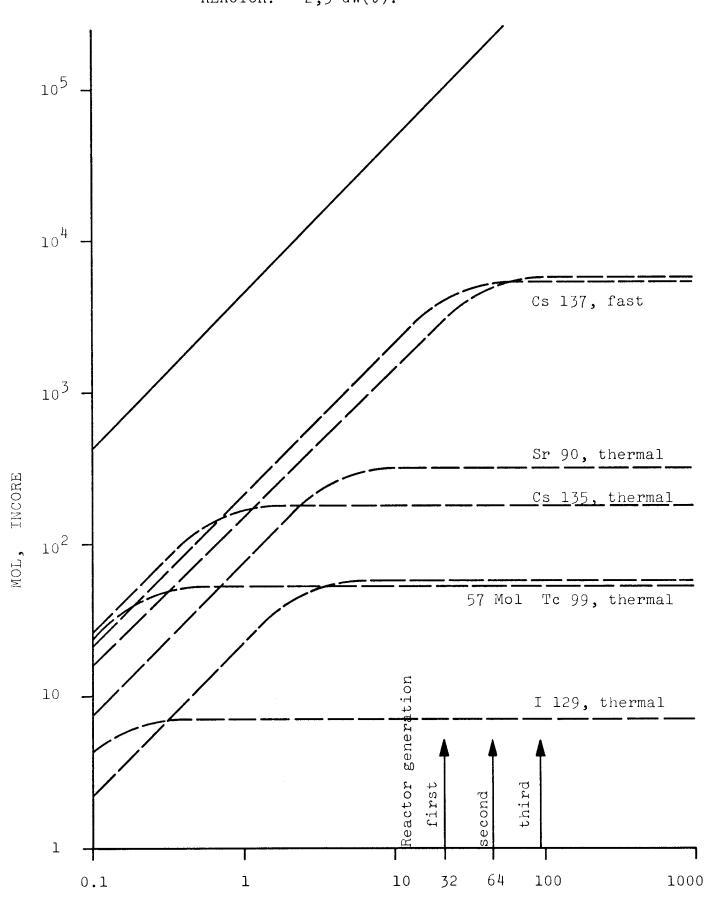


Fig. 19 FISSION-PRODUCTS IN STEADY-STATE POWER REACTOR: 2,5 GW(t).



TIME OF IRRADIATION (YEARS)

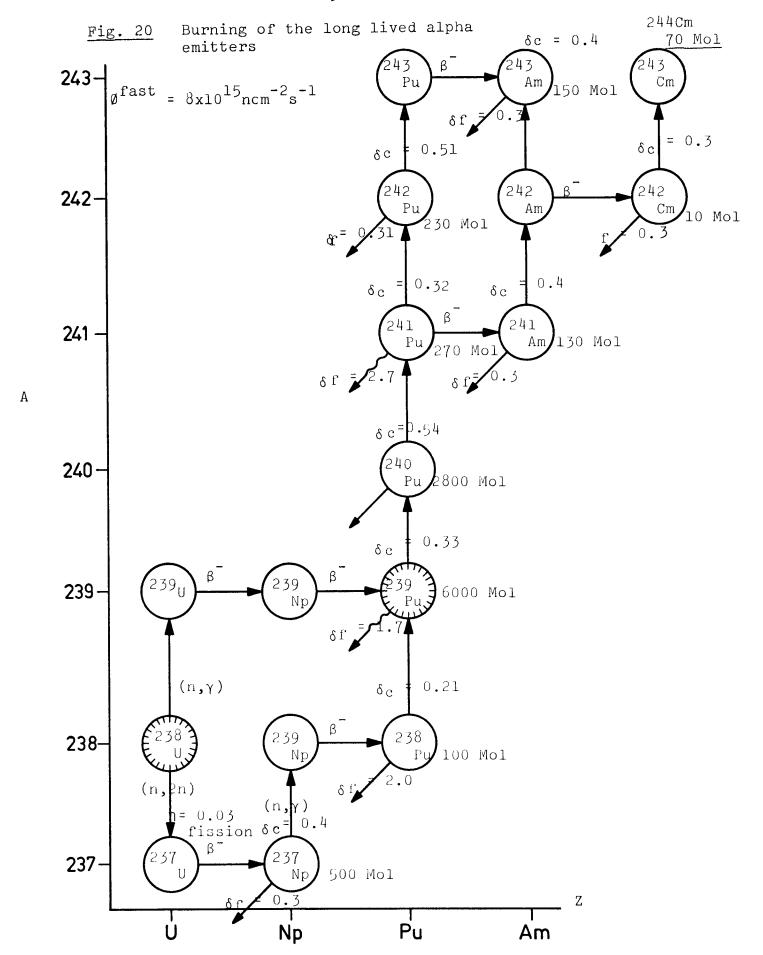
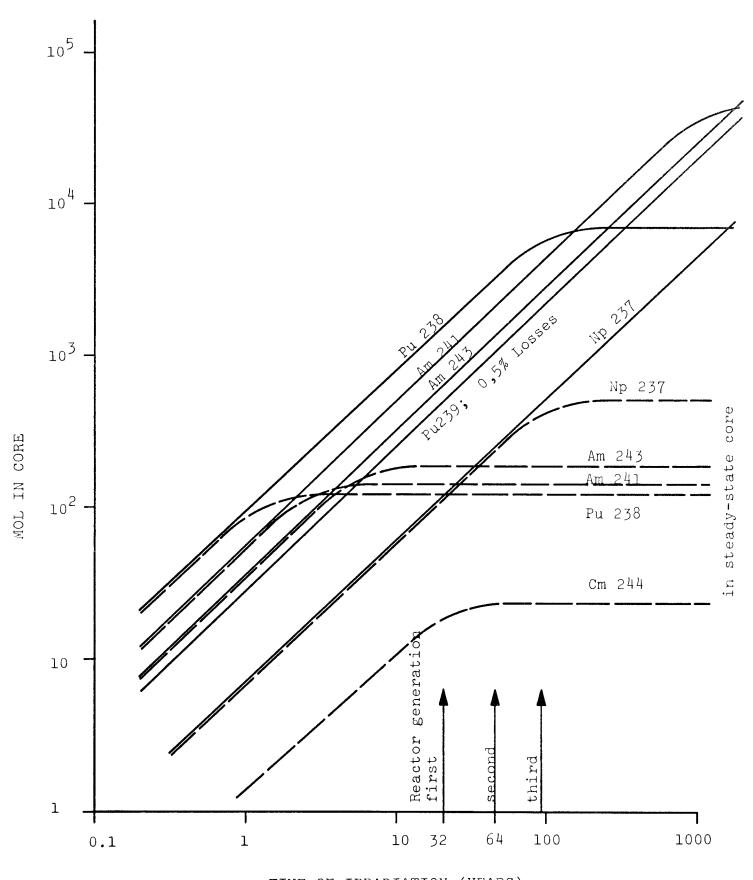


Fig. 21



TIME OF IRRADIATION (YEARS)

2) the continuous remotely operated extraction processes and preparation of the liquid fuel, and the absence of fuel elements etc. make this recycling of the actinides (very hazardous alpha and partly neutron emitters) possible and desirable.

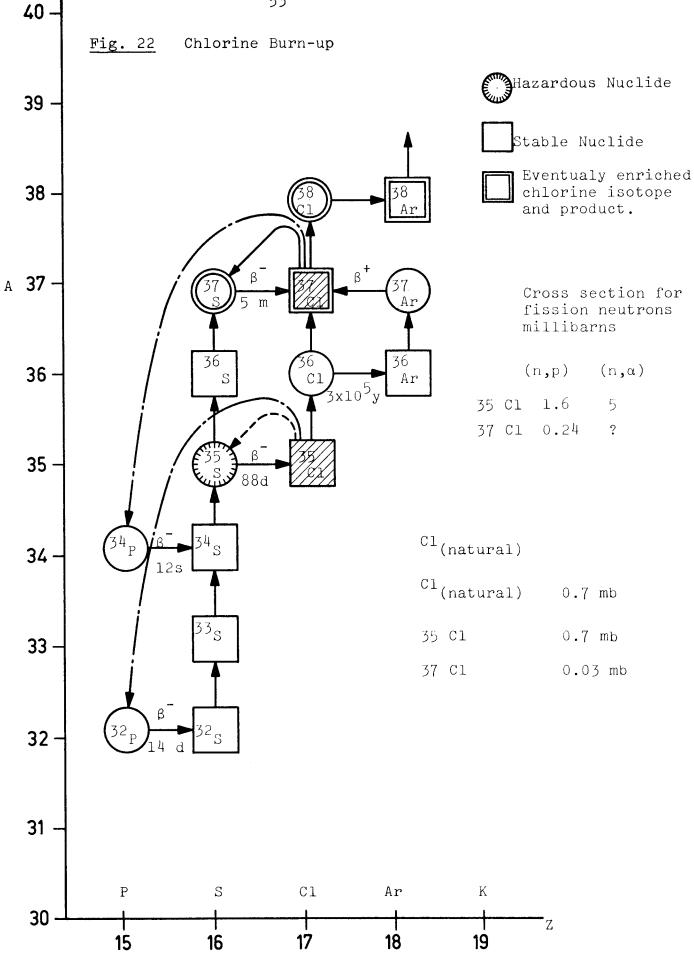
The high grade recovery of the actinides postulated here gives the steady state results for the fast reactor shown in Fig. 20 and 21. The reason for burning in the fast and not in the thermal reactor is based on the fact that the relation $\delta_{\rm c}^{\rm f}/\delta_{\rm c}^{\rm th}$ is greater in the fast reactor than in the thermal.

It must be remembered that the relatively high neutron flux results not only in the irradiation of the non desirable radio-active nuclides but also the stable fission products, not to mention the stable components of the fuel and the structural material. A very short review of these partial processes is given here

1) chlorine contains two stable isotopes (underlined) (see Fig. 22).

but not only (n,γ) reactions are important here. Much more important is the following reaction:

$$\frac{35}{17}$$
 (n,p) $\frac{35}{16}$ $\frac{\beta}{8.7 \text{ days}}$ $\frac{35}{17}$



The presence of sulphur influences the chemistry of the molten fuel.

2) Sodium has only one stable isotope

This chain seems to result in increasing amounts of stable magnesium and in longer time also stable aluminium.

A short summary of the "history" of the long lived radioactive nuclides proposed in this paper is given in Table 7.

Table 7 Problems in fission-products management

Nuclide	<u>Separation</u>	Transformation	
Т	from in core gas purging diluted with H	not possible, waste only	
Kr-85	from in core gas purging after decay of other Kr isotopes:	burning in thermal reactor (under pressure or as fluoride compend)	
Sr-90	from fuel reprocessing: separation Sr/Ba needed	burning in thermal reactor	
Zr-93	from fuel reprocessing: the preliminary separation of Y-91, precursor of Zr-91 is needed	burning in fast reactor; not possible in thermal reactor due to too large a volume. The radioactive Zr-93 is diluted by Zr-94,	
	Mixture of Zr-93, 94, 95	partially used as a dilutent for the thermal reactor ZrF_{4} or as structural material & fission products cladding in thermal reactor.	
Tc-99	from fuel reprocessing	burned in thermal reactor	
I-129	from gas purging, after decay time of I-131, that is ~ 160 days	burning in thermal reactor	
Cs-135	from gas purging, after the decay of Xe-135, that is after ~ 5 days	burning in thermal reactor	
Cs-137	from fuel reprocessing: separa- tion of Cs/Rb is needed	quasi-burning (storage) in fast breeder core- (in solid form) or out of core	
Actinides	from fuel reprocessing together with plutonium; very high efficiency of separation processes is needed.	fissioning in fast reactor	

VII. Reprocessing

The system proposed here is a rather complicated and sophisticated 'chemical machine' and not only a nuclear energy thermal energy transformer as are other classical reactors.

The entire reprocessing scheme includes: (Fig. 23)

Table 8 Scheme of entire reprocessing system

Continuous Process	Short description	Principle action Secondary
Gas extraction	Hydrogen-helium gas stream	removal of I-131 and Xe
Fast chloride fuel reprocessing	Reprocessing of the 2 GW(t) fast breeder Remark: only plutonium!	separation of Cs-135/Cs-137
Thermal fluoride fuel reprocessing	Reprocessing of the 0.5 GW(t) thermal only plutonium! No uranium!	
Fertile chloride, material reprocessing	Reprocessing of the fast breeder blanket material Mostly uranium, small amounts of plutonium.	
Fission products, mostly fluoride reprocessing	Reprocessing of the long lived fission products, irradiated in in the thermal high-flux.	removal of stable nuclides *rom Zr

The effective burning of the most important long lived nuclides needs a rather complicated reprocessing plant with high temperature pyrochemical separation methods, both in gaseous and liquid salt or/and metallic phases. In some cases also a retention volume is necessary (for spontaneus decay of short-lived nuclides).

This reprocessing philosophy arises from the following assumptions: The caesium nuclides are very hazardous but there are at least two isotopes Cs-135 (t $1/2 = 2 \times 10^6 a$) and Cs-137 (t 1/2 = 30 a). The first one has a reasonable cross section from the point of view of neutron transformation ($\sigma_{th} = 8 \text{ barn}$), the second a very small cross section in both fast and thermal reactors $\sigma^f = 100 \text{ mb}$ or less, $\sigma^{th} = 110 \text{ mb}$). The separation of two flows e.g. Cs-135 for thermal burning and Cs-137 for quasi burning (rather selfdecaying) could help solve this problem.

In this system the continuous in core gas purging system is expected to extract some of the volatile fission products especially those with longer half life period. In the case of caesium the separation of both isotopes is possible due to the different time chains

The extractable volatile and relatively long lived nuclides in short time gas purging are underlined. The Cs-135 could be extracted in the form of the precursors. Cs-137 is retained in the fuel and must be separated by more conventional (but not so simple) methods.

Another similar problem arises in the case of zirconium isotopes (see Fig. 18/IV) and iodine (Fig. 18/II). Part of the zirconium could be used as a diluent of the homogenous fuel for the thermal core (e.g. 20 mol% $\rm ZrF_4$ + 80 mol% $\rm FeF_2$) part as component of the molten fuel for the fast core (?) and part in metallic form as structural (but radioactive) material when in the final period of fast reactor development when the $\rm Zr-93$ will be reduced to less than 1 mass % of the total zirconium

Some further similar questions will have to be discussed, in some a separation of isotopes is possible by means of rapid in core gas extraction or slow out of core (liquid phase) separation process.

A preliminary draft of the possible reprocessing scheme is given in Fig. 23.

VIII. Molybdenum and corrosion processes

The corrosion processes in this type of reactor are of crucial importance. In the cores of these reactors are approx 950 kg molybdenum or approx 10'000 mol.

We postulate here, arbitrarily, a relatively high corrosion rate equivalent to a full or 100% corrosion of the complete amount of molybdenum in approx 10 years. This means a corrosion rate of:

$$\frac{10.000 \text{ mol molybdenum}}{10 \text{ years x } (3.1 \text{ x } 10^7 \text{s/year})} = 3 \text{ x } 10^{-5} \text{ mol/s} = 30 \text{ } \mu\text{m/s}$$

Fig. 23

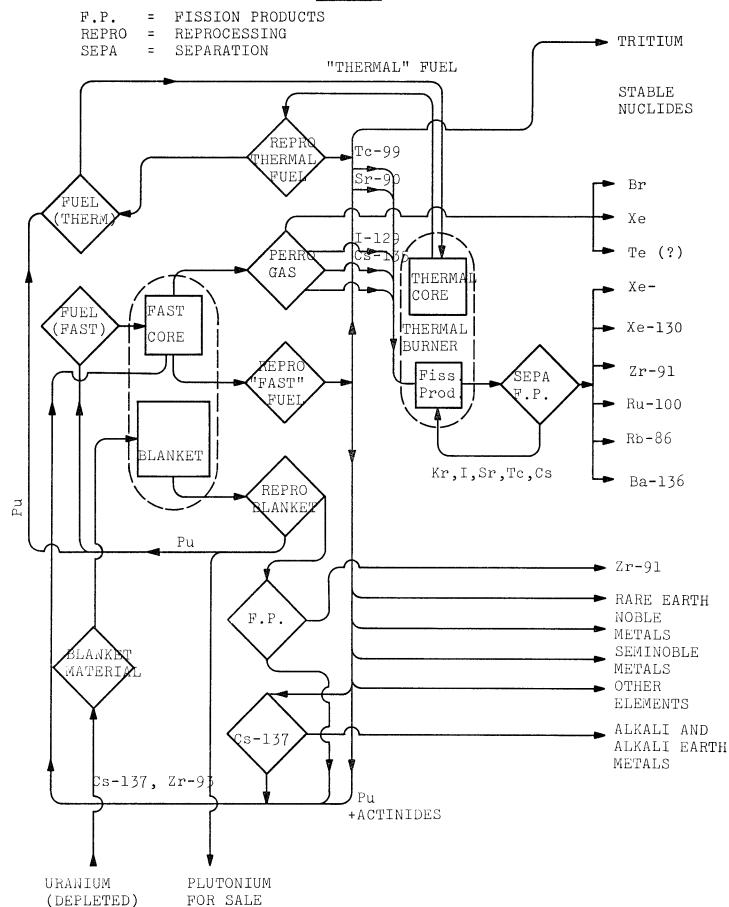
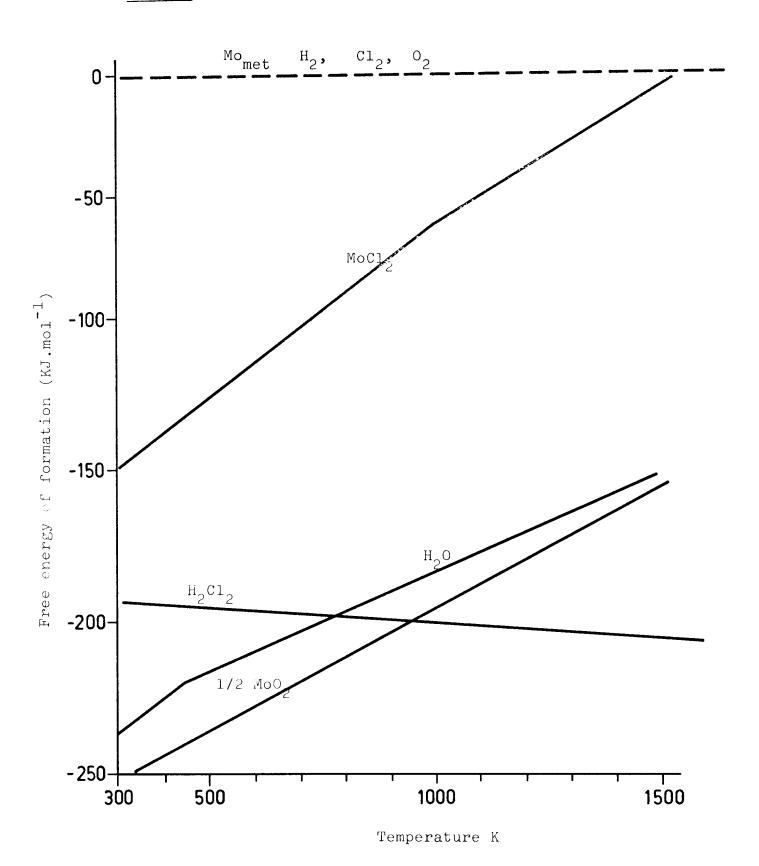


Fig. 24



Thus 30 micromoles molybdenum per second (or approx 3 mg Mo/s). In addition to this we have molybdenum as fission product. In the 2000 MW(t) fast reactor the amount of fissioned plutonium equals:

2000 MW(t) x l day x (1.06 g Pu/MWd(t)) \approx 2150 g Pu/day or: 25 mg Pu/s: that is; 100 μ mol Pu/s.

The production side of fission products equals 200 μ mol/s. Molybdenum is present at about 18 mol% of fission products which means a 36 μ mol/s, or almost half the amount of corroding material. From both sources, corrosion and fissioning the amount of molybdenum is about 50 μ mol/s. The corrosion processes can go in three directions

- 1) Chloride reaction Mo_{met} + 2 Cl + Me + → MoCl₂ + Me_{met}
- 2) Oxygen reaction $Mo_{met} + O_2 \rightarrow MoO_2$
- 3) Tellurium reaction $Mo_{met} + Te_2 \rightarrow MoTe_2$

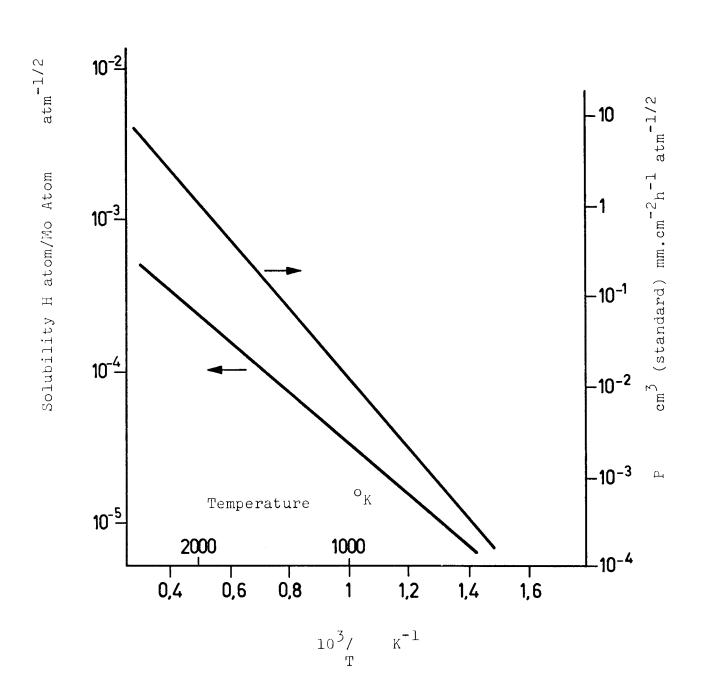
These and eventually other molybdenum corrosion processes are potentially dangerous and should when possible be prevented in the core itself. This possibility exists due to the reaction with the gaseous hydrogen (see also Chapter IV).

- 1) $MoCl_2$ + H_2 Mo_{met} + 2HCl
- 2) MoO_2 + H_2 Mo_{met} + $2H_2O$
- 3) $MoTe_2$ + $2H_2$ \rightarrow Mo_{met} + $2TeH_2$ \rightarrow Te_2 + $2H_2$

(see Fig. 24)

Fig. 26 Solubility and Penneability

Momet - H2
gas



In the extreme case the molar amount of hydrogen is twice as big as that of molybdenum giving 120 μ mol H $_2$ /s.

Under normal conditions (1 bar, 0° C) this amount of hydrogen is acceptable:

~120
$$\mu$$
mol x (2.2 x 10⁴ cm³/mol) x 10⁻⁶ \approx 3.0 cm³ H₂/s

For further calculations we arbitrarily assume ten times more, approx 30 ${\rm cm}^3{\rm H}_2/{\rm s}$. (see also Chapter V)

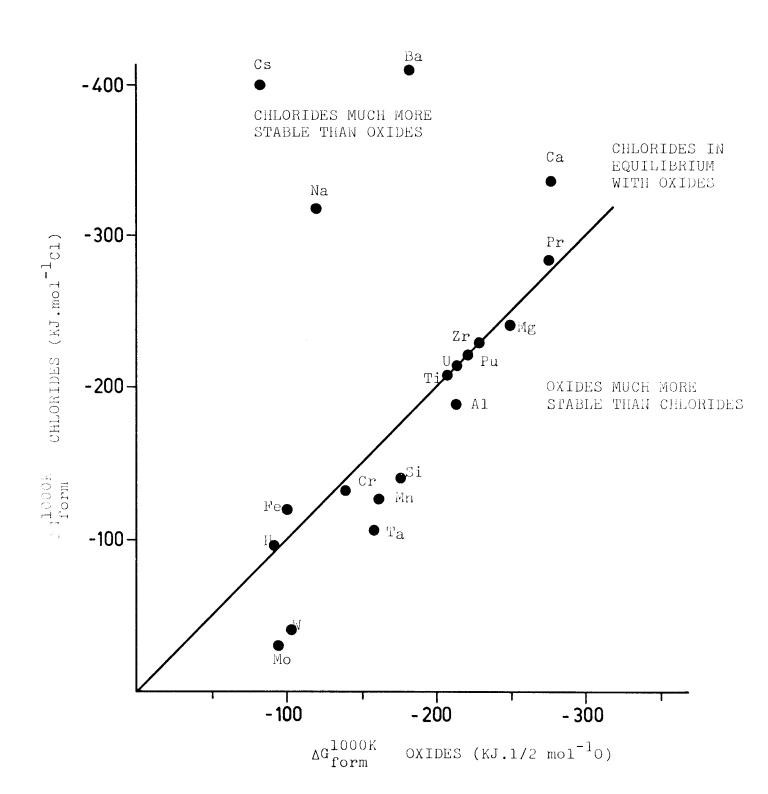
Here is a major question concerning the reaction of metallic molybdenum with hydrogen. From about 100 elements there are only twelve elements which form no chemical binding with hydrogen.

	d ⁴	d ⁵	a ⁶	d^7	d ⁸
3d - Electrons		Mn	Fe	Со	
4d - Electrons	Мо	Тс	Ru	Rh	
5d - Electrons	W	Re	Os	Ir	Pt

Thus molybdenum fulfills the minimum requirements: it has no reaction with hydrogen. Also manganese-cobalt alloys are suitable for this reactor (chromium and nickel not!).

In addition the solubility of hydrogen in molybdenum is relatively small. The dependence of the solubility of $\rm H_2$ in Mo-metal on temperature and pressure is known since molybdenum is a possible constructional material for containing plasma (hydrogen) in fusion reactors. Also the diffusion of hydrogen through metallic molybdenum is relatively very small (see Fig. 26).

Fig. 25 CHLORIDES-OXIDES EQUILIBRIUM DIAGRAM AT 1000K



The diffusion rate of hydrogen from the melted fuel to coolant and blanket (here also UCl₃ - NaCl) needs to be discussed.

One can assume, however, that also this melt with hydrogen is saturated so that the porosity of the wall (molybdenum) will play a minor role. The most important: the variation in mechanical properties of the molybdenum caused by the dissolved hydrogen.

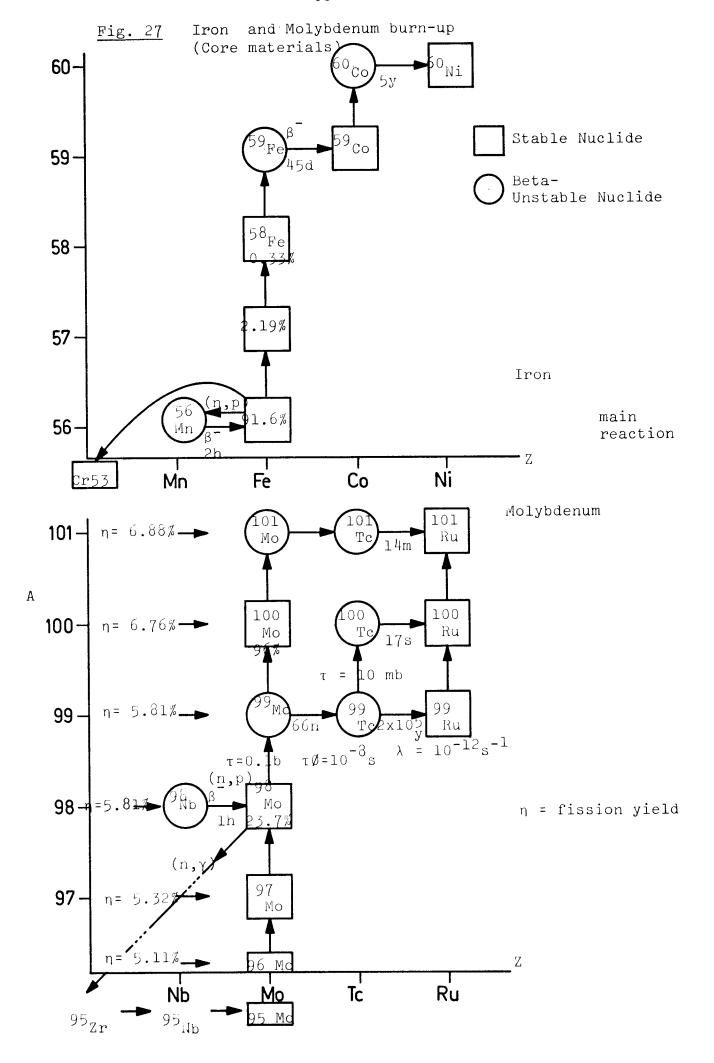
The problem of the corrosion of molybdenum in chlorine containing media is particularly complicated by the numerous molybdenum chlorides: $MoCl_2$, $MoCl_3$, $MoCl_4$, $MoCl_5$.

Also the oxygen chlorine systems for molybdenum and some selected fuel components including hydrogen are rather complex (Fig. 24).

In the region of the external heat exchanger the main corrosion process results from the action of gaseous aluminium chloride (the secondary working agent)

$$AlCl_{3(g)} + \frac{1}{x} Mo \rightarrow \frac{1}{x} MoCl_{2x(g)} + AlCl_{(g)}$$

This reaction has been discussed in earlier publications (Blander 1957) but unfortunately not all the thermodynamic data is known. The stability of the molybdenum chlorines is of course strongly influenced by the concentration of free chlorine and also by the temperature.



A more detailed calculation of metallic molybdenum corrosion in the aluminium trichloride is needed. These calculations are very sensitive to the vapour pressure of chlorides. More detailed calculations of the corrosion in this system have been given earlier (Taube, Schumacher 1969).

IX. Molybdenum and iron irradiated in a fast high flux reactor IX a) Nuclear effects

The high neutron flux irradiation causes physical and chemical changes in structural materials.

Molybdenum is a mixture of stable isotopes (Fig. 27). The most important by-product of neutron irradiation is the Tc-99 beta-emitter with t $1/2 \cong 2.1 \times 10^5$ year and which belongs to the chain (stable nuclides underlined)

$$\frac{\text{Mo-98}}{23\%} \text{ (n,}\gamma) \quad \text{Mo-99} \qquad \frac{\beta}{66 \text{ h}} \qquad \text{Tc-99} \qquad \frac{\beta}{2.1 \times 10^5 \text{ a}}$$

$$\text{Tc-100} \qquad \frac{\beta}{17 \text{ s}} \quad \text{Ru-100}$$

for approx 1000 kg. Mo in core or about 10'000 moles the Mo-98 gives 2300 mol. The irradiation rate equals:

$$N^{\text{Mo-99}}$$
 = (2.3 x 10³) x (6 x 10²³) x (10 x 10⁻²⁷) x 10¹⁶ Atom/s = 1.2 x 10¹⁷ Atom/s

turbine cycle with various working fluids 75-70 Total Power Plant thermodynamic efficiency Two circuits with dissociating fluids in 65gas turbine 90 bar 60-(N₂O₄/NO₂)+(Al₂Cl₆/AlCl₃) 55-50-One dissocia ting fluid in gasture 45-(N₂O₄/ Heliu gas-turbin 40 35-(°C) 30-600 500 700 400 900 800 Temperature

Fig. 28 Approximate thermal efficiency using a

After 700 hrs the steady state concentration of Mo-99 (t $1/2 = 66 \text{ hrs} \cong 2.4 \times 10^5 \text{s} \colon \lambda = 3 \times 10^{-5} \text{ s}^{-1}$) equals:

$$C_{\text{steady}}^{\text{Mo-99}} = \frac{1.2 \times 10^{17}}{3 \times 10^{-5}} = 3 \times 10^{21} \text{ Atom}$$

The activity of the Tc-99 (t $1/2 = 2.1 \times 10^5 a = 6.2 \times 10^{12} s$: $\lambda \approx 10^{-13} s^{-1}$) after 3 years irradiation of 100 kg of molybdenum in the fast reactor core:

Activity
$$^{\text{Tc-99}}_{(3 \text{ year})} = 1.2 \times 10^{17} \text{ Atom/s } \times (3 \times 3.1 \times 10^7 \text{ s/year})$$

$$\times \frac{10^{-13}}{3.7 \times 10^{10}} \cong 3 \text{ Curie/l tonne of Mo}$$

IX b) Radiolysis of molten chlorides in very high flux of fast neutron

The high flux of neutrons and especially of the fission fragments results in a high damage in the fuel material and cladding. In the type of reactor under discussion this problem seems to be much easier to solve because

- 1) the molten chlorides are fluids with structure that is with a very low activation energy for recombination of the radiolysis product and therefore with a very high recombination velocity.
- 2) in core there are no structural materials (tube, cladding etc.)

X. Aluminium trichloride as a secondary coolant and working agent

In this consideration for the power production a non conventional gas-turbine cycle is postulated: we have chosen aluminium tri-chloride, AlCl₃.

It is now clear that this chosen secondary coolant-working fluid substance has specific additional properties, which make it particularly intersting in the present application. The reason is the following: it is well known that real progress in improvement of the thermal efficiency of turbines is limited by two parameters:

- 1) for steam turbines, corrosion effects with non austenic steel above 580°C on the one hand, and on the other hand the dramatic increase of costs when an austenic steel is used.
- 2) for gas turbines (e.g. helium), the operation of the gascompressor consumes more than half of the energy produced
 by the power turbines. A number of methods are available
 for overcoming these limitations, one of these proceeds
 as follows: the working agent in the turbine, when the
 temperature decreases undergoes a chemical reaction which
 decreases the volume. This result is most conveniently
 obtained when the working substance polymerises at the
 lower temperature. Of course, this polymersiation must
 be completely reversible, that is to say that, at the
 higher temperature, the depolymerisation process is
 effectively complete. One of the most promising working
 agent is aluminium trichloride, which, at the lower

temperature dimerises by the following mechanism:

(2 AlCl₃)
$$\frac{\text{gas}}{\text{monomer}}$$
 (Al₂Cl₆) $\frac{\text{gas}}{\text{dimer}}$ (Al₂Cl₆) $\frac{\text{liq.}}{\text{dimer}}$ higher temp. lower temp.

When the temperature increases a monomerisation process takes place. Already in 1959 Blander and co-workers discussed the problem of AlCl₃ as working agent. They wrote: "A number of typical application (including a gas turbine cycle employing AlCl₃ as the working fluid and a binary vapour cycle employing water vapour for the lower temperature: M.T.) have been considered but in none of these has the aluminium chloride shown outstanding advantages over more conventional media. However, it is believed that for some special applications it may well prove to have outstanding advantages, where the characteristics of the other system components are such as to make it possible to exploit to the fullest the unique characteristics of aluminium chloride" (Blander, 1959).

Much more optimistic conclusions could be seen in the papers of Krasin and Nesterenko (1972). These authors maintain that the overall thermal efficiency of a dual cycle with aluminium chloride as working fluid in the high temperature cycle and NO_2 in the low temperature cycle promises to increase up to 60% for 800 °C and 90 ata (see also: Krasin, 1971).

But with aluminium chloride and with nitrogen dioxide the chemical industry has considerable experience, including experience with corrosion problems, in the high-temperature region. Unfortunately there seems to be a lack of data concerning the erosion and corrosion behaviour of these substances in turbines and on their behaviour under neutron irradiation in reactor conditions.

Aluminium chloride as a working fluid in a condensation turbine has the following advantages:

- 1) the efficiency of the power generation is about 30-50% higher than for the "classical" working fluids; helium or steam. The quantity of fuel used is correspondingly smaller. For a country in which the sources of uranium an and plutonium are limited this advantage may be decisive.
- 2) the waste heat is smaller an the temperature of the heating water is lower. In a country in which the only sources of cooling water are the rivers, such an advantage is of importance.
- than for a steam turbine is approximately 5 times smaller than for a steam turbine of the same power. For a direct cycle (when the reactor coolant agent is the working fluid in the turbine) when the circuit is radioactive the small size of turbine is an important factor.
- 4) all these properties of an aluminium chloride circuit have a significant influence in reducing the capital cost of a power station.

Let us repeat the advantageous properties: decreased fuel consumption, reduction of waste heat, decrease of turbine size. All these trends promise to give a significant reduction in power generating costs.

The crucial problem of possible corrosion processes caused by ${\rm AlCl}_3$ may be controlled by the small addition of hydrogen.

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