

## Predictive Equations for the Gas-phase diffusivity

Empirical equation: Fuller, Schettler & Giddings (1966)

$$D_{AB} = \frac{1.0133 \times 10^{-7} T^{1.75}}{P [(\sum v_A)^{1/3} + (\sum v_B)^{1/3}]^2} \left[ \frac{1}{M_A} + \frac{1}{M_B} \right]^{1/2} \text{ m}^2/\text{s}$$

• Fick's law for liquids

$\sum v_A$  = Diffusion volume of component A [Ex:

$M_A, M_B$  = Molecular weights of A & B, resp.

$P$  = total pressure, in bar

$T$  = temp in K

## Molecular diffusion in liquids:

- Liquids are closely packed than gases & hence diffuse slowly.  $D \sim (0.5 - 2) \times 10^{-5} \text{ cm}^2/\text{s}$

- Fick's law of diffusion is applicable for liquids as well

For liquids:  $N_A = (N_A + N_B) x_A - D_{AB} \left( \frac{\rho}{m} \right)_{av} \frac{dx_A}{dz}$ ;  $x_A = C_A/C$

$(\rho/m)_{av}$  = Average molar conc. of the liquid  
 $\rho$  = Density  
 $m$  = molecular weight

For gas:  
 $N_A = (N_A + N_B) \frac{C_A}{C} - D_{AB} C \frac{dx_A}{dz}$

Fluxes for the following cases, discussed earlier, can be derived similarly: for liquids also.

(a) Diffusion of A through non-diffusing B:

(b) Equimolar counter diffusion of A & B:

$$N_A = \frac{D_{AB} (\rho/m)_{av} (x_{A0} - x_{A1})}{l x_{Bm}}$$

$$N_A = \frac{D_{AB} (\rho/m)_{av} (x_{A0} - x_{A1})}{l}$$

$$x_{Bm} = \frac{x_{B0} - x_{B1}}{\ln(x_{B0}/x_{B1})}$$

## Liquid-phase diffusivity:

Empirical correlation: Wilke-Chang equation (1955)

$$D_{AB}^0 = \frac{1.173 \times 10^{-16} (\phi M_B)^{1/2} T}{\mu V_A^{0.6}}$$

$D_{AB}^0$  = Diffusivity of A in B @ infinite dilution

$M_B$  = molecular weight of B

$\phi$  = Association factor for the solvent

$T$  = temp, K

$\mu$  = Solution viscosity

$V_A$  = Solute molar volume @ normal boiling point.

$D_{AB} \propto \frac{1}{\mu}$   
 $\propto \frac{1}{V_A^{0.6}}$  (larger molecules have lower diffusion)  
 $\propto T$