

# Lecture # 13 CHE331A

Introduction and  
Design equations for  
Ideal reactors  
(BR, CSTR, PFR, PBR)

Basic Concepts in  
Chemical kinetics  
(types of reactions,  
rate and equilibrium  
constants)

Isothermal Reactor  
Design (CSTR, PFR,  
PBR), Constant volume  
and Variable volume,  
EG production

Collection and  
Analysis of Data  
(Differential, Integral,  
Non-linear regression,  
Differential reactor)

**Design of Multiple  
Reactions in  
Isothermal Reactors**

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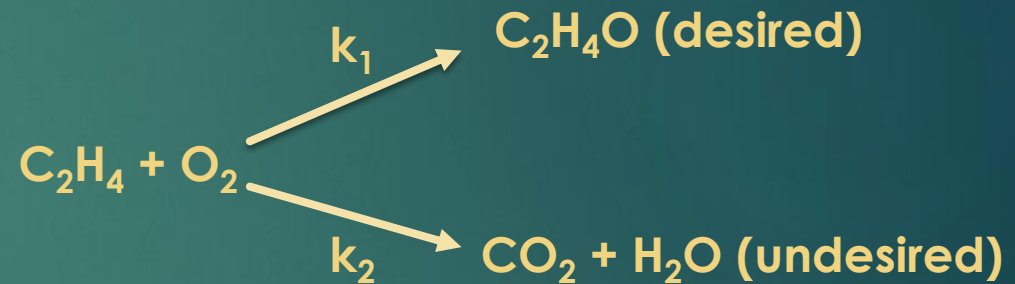
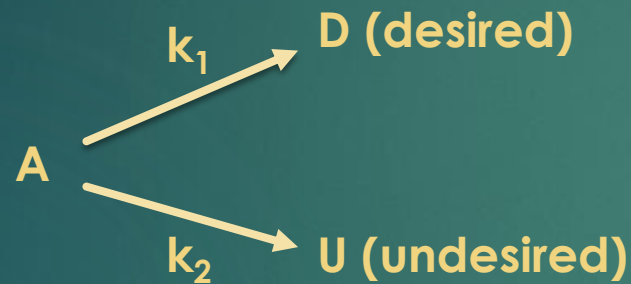
# Often Multiple reactions occur in Reactors in the Chemical Industry

- ▶ Some reactions are desirable and others undesirable
- ▶ There is a need to minimize undesirable reactions to enhance the profitability of a process
- ▶ Reactions can be classified into four basic reactions
  - Parallel
  - Series
  - Complex
  - Independent

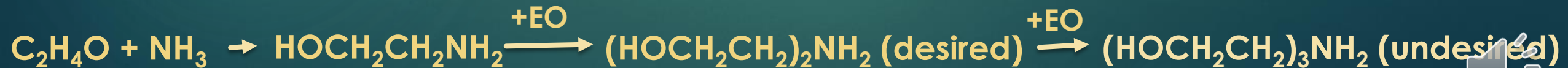
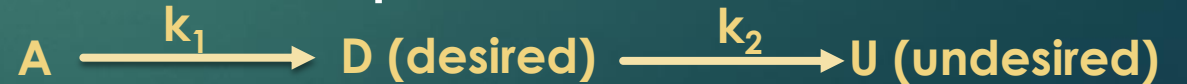


# Parallel and Series Reactions differ in the way the reactants are consumed

- ▶ In parallel reactions the reactant is consumed in different reaction pathways



- ▶ In series reactions an intermediate desirable product is formed, which reacts to form another product



# Independent reactions involve different reactants reacting at the same time

- ▶ Reactants nor products react with each other



- ▶ Example,

Cracking of crude oil to form petrol



# Complex reactions involve the combination of series, parallel and independent reactions



- Combination of series and parallel reactions is seen in the formation of butadiene from ethanol

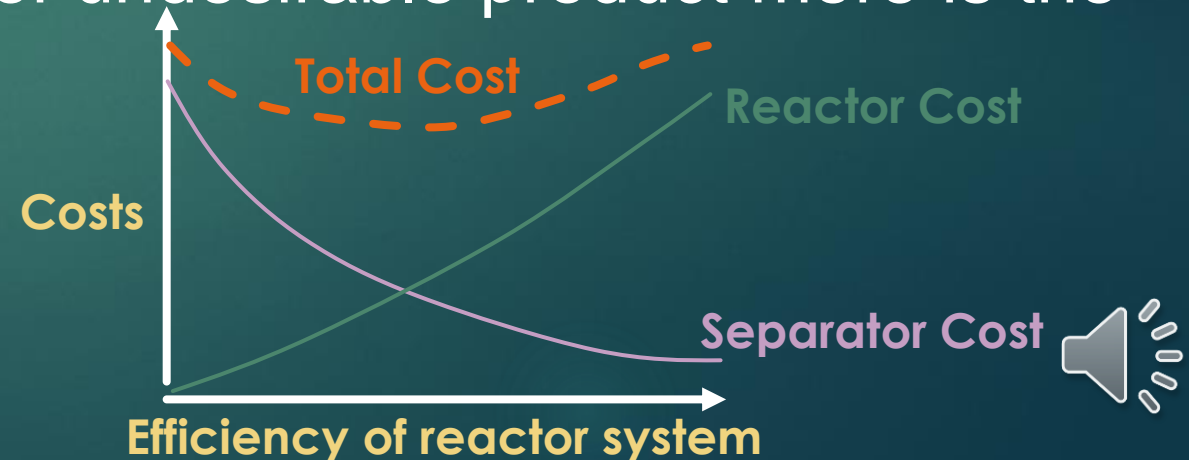
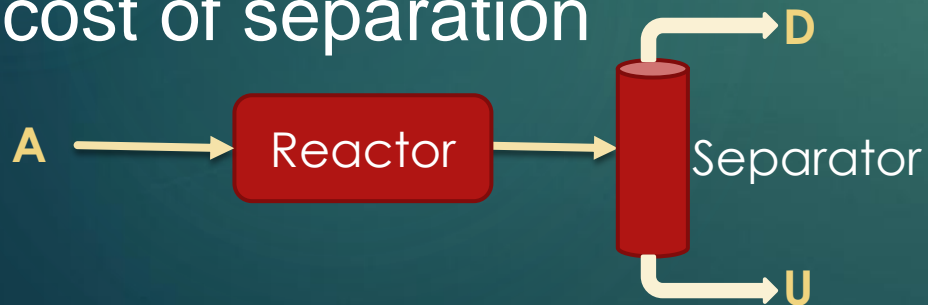


# Desired and Undesired Reactions and decisions to make

- Focus is to maximize the desired product formed and minimize the amount of undesired formed



Usually, the greater the amount of undesirable product more is the cost of separation





# Selectivity and yield are useful parameters that are required to describe Multiple reactions

- ▶ Selectivity: Provides information about the formation of one product over another – two types of selectivity defined in literature

- Instantaneous selectivity:  $S_{D/U} = \frac{r_D}{r_U} = \frac{\text{rate of formation of } D}{\text{rate of formation of } U}$

- Overall selectivity:  $\bar{S}_{D/U} = \frac{F_D}{F_U} = \frac{\text{exit molar flow rate of } D}{\text{exit molar flow rate of } U}$  (Flow reactor)

(Batch reactor)  $\bar{S}_{D/U} = \frac{N_D}{N_U} = \frac{\text{Number of moles of } D \text{ at the end of reaction}}{\text{Number of moles of } U \text{ at the end of reaction}}$

- ▶ For CSTR:  $A \xrightarrow{k_D} D$  and  $A \xrightarrow{k_U} U \Rightarrow \bar{S}_{D/U} = \frac{F_D}{F_U} = \frac{r_D V}{r_U V} = \frac{r_D}{r_U} = S_{D/U}$

- ▶ Thus, for a CSTR:  $\bar{S}_{D/U} = S_{D/U}$  (try this for a series reaction)



# Similar to selectivity, the yield also has two definitions

► Instantaneous Yield,  $Y_D$  : 
$$Y_D = \frac{r_D}{-r_A} = \frac{\text{rate of formation of } D}{\text{rate of disappearance of } A}$$

► Overall selectivity,  $\bar{Y}_D$ :

○ (Flow reactor) 
$$\bar{Y}_D = \frac{F_D}{F_{A0} - F_A} = \frac{\text{exit molar flow rate of } D}{\text{moles of } A \text{ converted}}$$

○ (Batch reactor) 
$$\bar{Y}_D = \frac{N_D}{N_{A0} - N_A} = \frac{\text{Number of moles of } D \text{ formed at the end of reaction}}{\text{Number of moles of } A \text{ consumed at the end of reaction}}$$

► Similar to selectivity, for a CSTR:  $Y_D = \bar{Y}_D$

► Overall selectivities and yields are important for determining profits, whereas rate-based parameters help in reactor selection and reactor scheme

