

Module # 1.1.1

# INTRODUCTION

## Control: Why and How

*Lectures on*

**CHEMICAL PROCESS CONTROL**  
Theory and Practice

# Why do we need to control a system

- To stabilize an inherently unstable system
  - Examples:
    - Bicycle
    - Stick on palm
    - LCA Tejas (India's own fighter aircraft)
    - Unstable nonisothermal CSTR
- To deliver minimum performance guarantees for a system
  - Examples:
    - Petrol is octane number 92 or more
    - To produce X tph of commercial grade propylene
    - Missile strike accuracy guaranteed within 2 m radius
    - Driving a taxi in a manner that minimizes fuel consumption...

# Day-to-Day Control Examples

Tuning Guitar Strings



Balancing a Stick

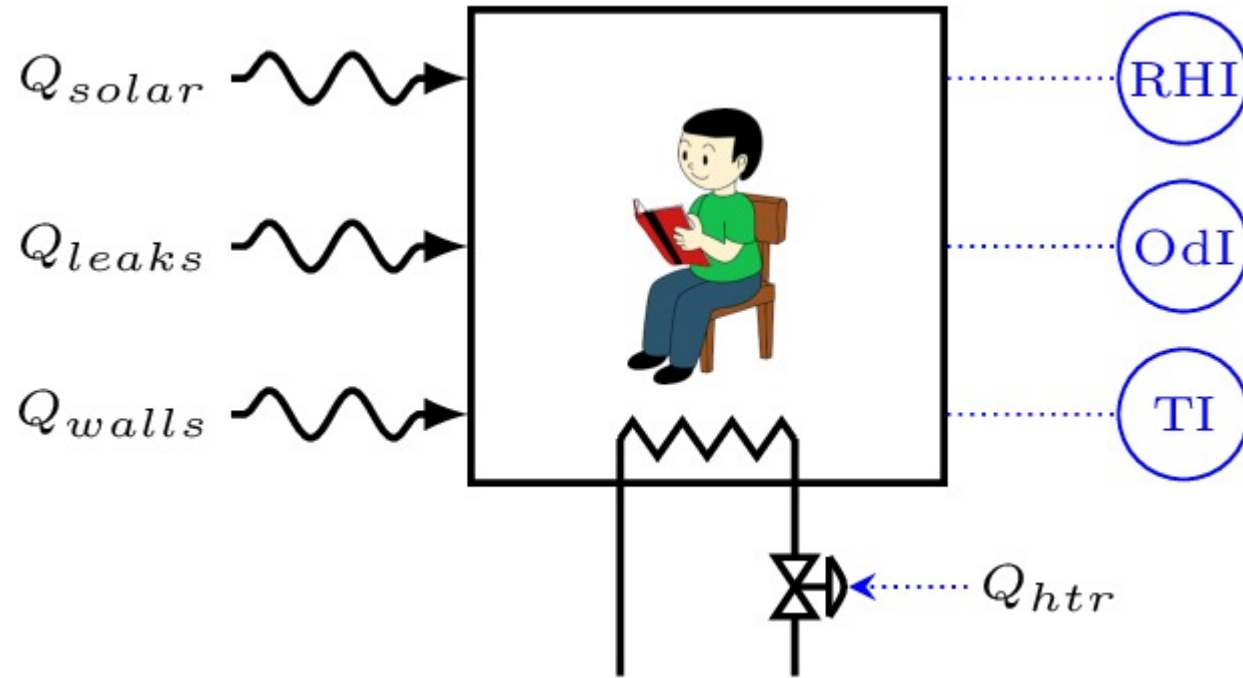


Grocery Weighing



Pictures from google images

# Room Example



## PROCESS VARIABLES

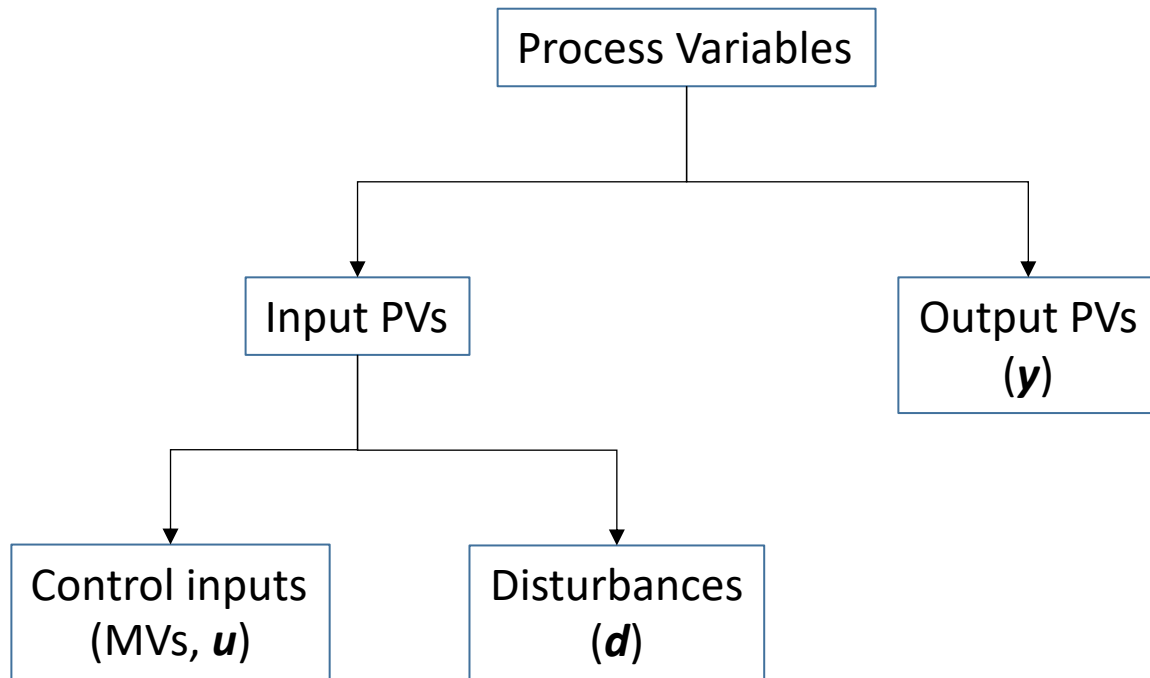
|                     |             |
|---------------------|-------------|
| Temperature         | T           |
| Odor                | Od          |
| Relative Humidity   | RH          |
| Heater Duty         | $Q_{htr}$   |
| Solar heating rate  | $Q_{solar}$ |
| Heat leak rate      | $Q_{leaks}$ |
| Wall heat loss rate | $Q_{walls}$ |

$Q_{htr}$   
 Manipulated Variable  
 Control dof  
 Control Input

$Q_{solar}, Q_{walls}, Q_{leaks}$   
 Disturbances

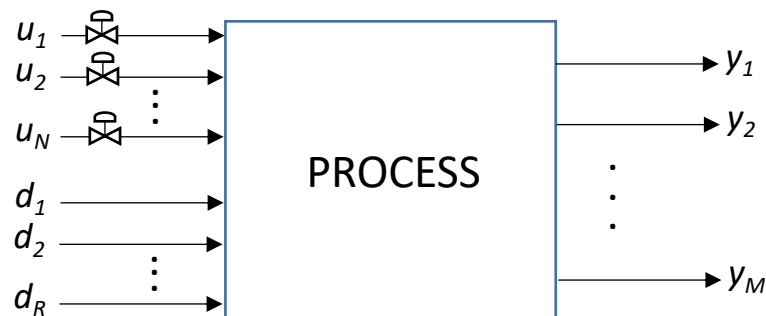
$Q_{htr}, Q_{solar}, Q_{leaks}, Q_{walls}$  Input PVs  
 T, RH, Od Output PVs

# PV Classification



Input PVs affect output PVs through cause-and-effect relationships

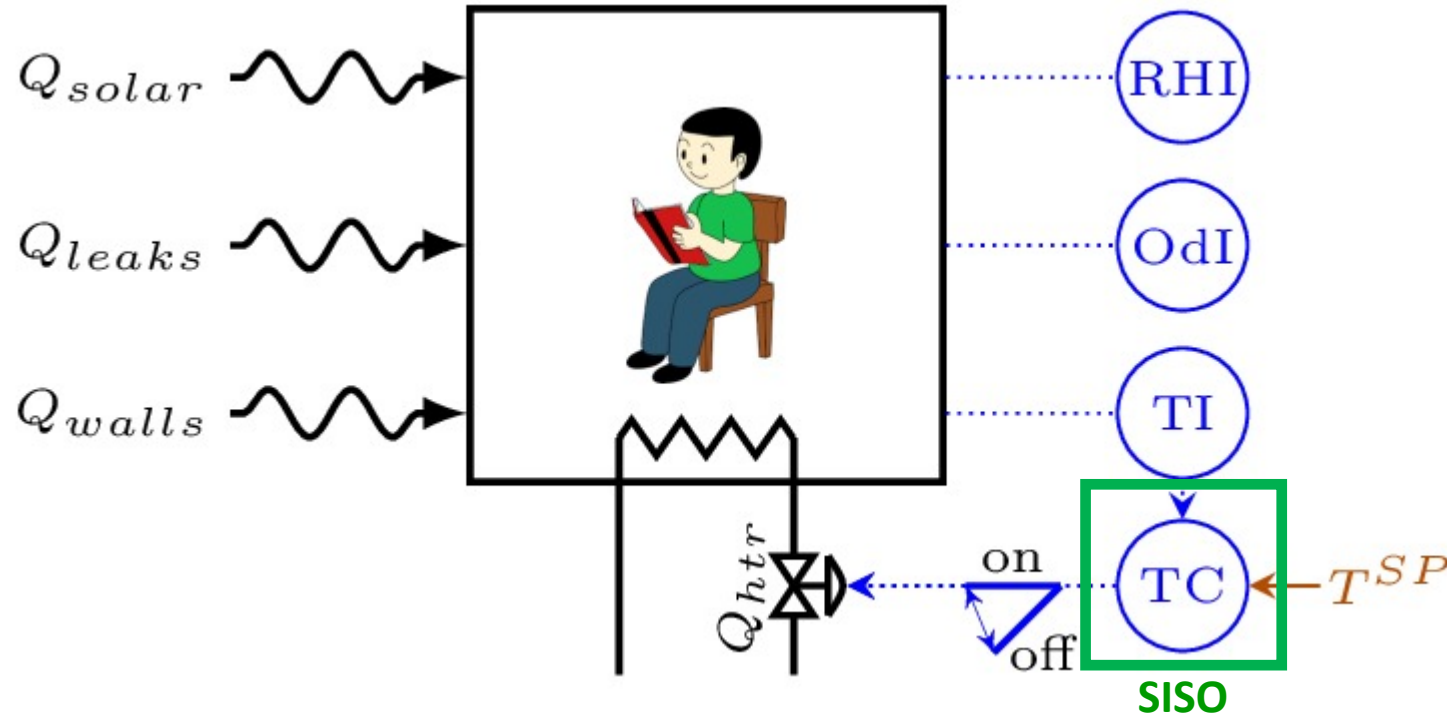
An MV with 'strong' effect on a PV can be adjusted to control the PV



$$M \gg N$$

|             |                                  |
|-------------|----------------------------------|
| Output PVs: | Several. May be designed         |
| MVs:        | Limited. Fixed by process design |

# SISO Feedback Control



## Feedback Loop Open

Operator specifies MV ( $Q_{htr}$ )  
CV ( $T$ ) floats

## Feedback Loop Closed

Operator specifies CV setpoint ( $T^{SP}$ )  
MV ( $Q_{htr}$ ) floats

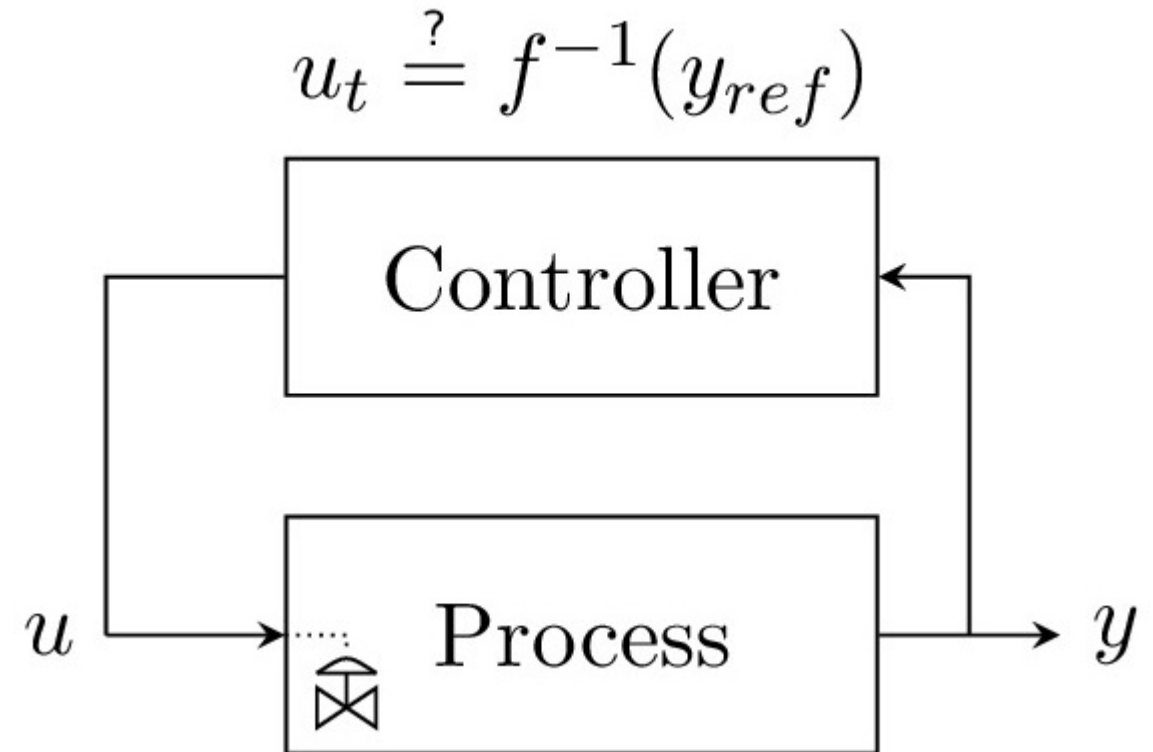
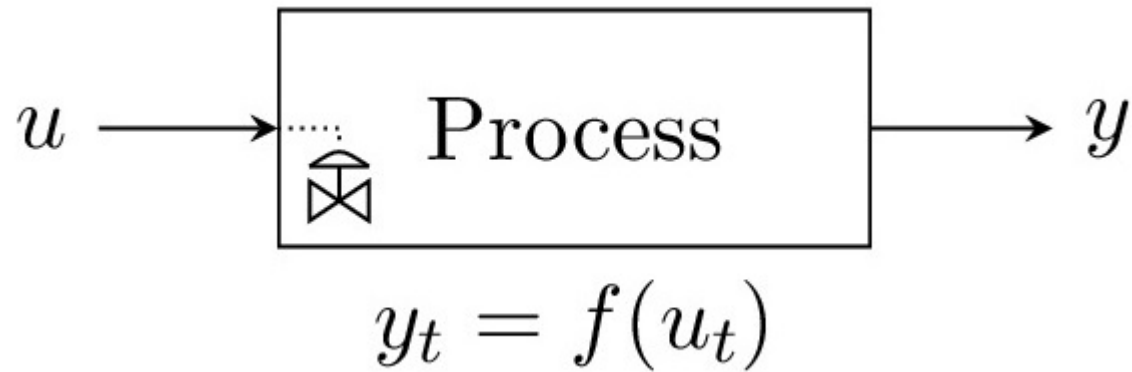
## FEEDBACK

Adjust MV based only on CV values (current and past)  
to drive CV to CV setpoint (desired value)

## SINGLE-INPUT-SINGLE-OUTPUT (SISO)

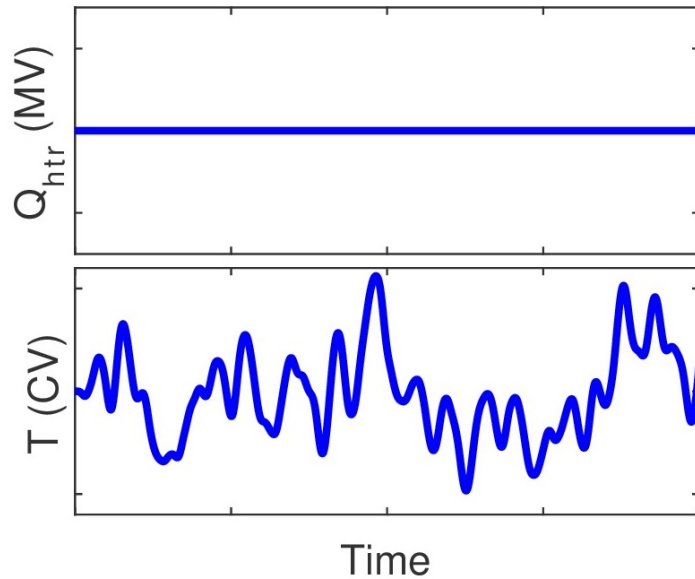
**Controller Input:** Single PV measurement  
**Controller Output:** Single MV signal

# Control Inverts MV-CV Relation

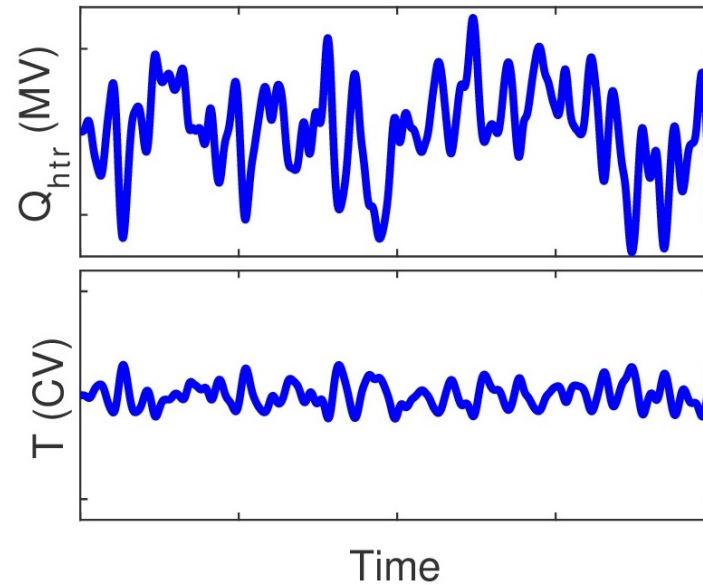


# Control as Transformation of Variability

No T Control



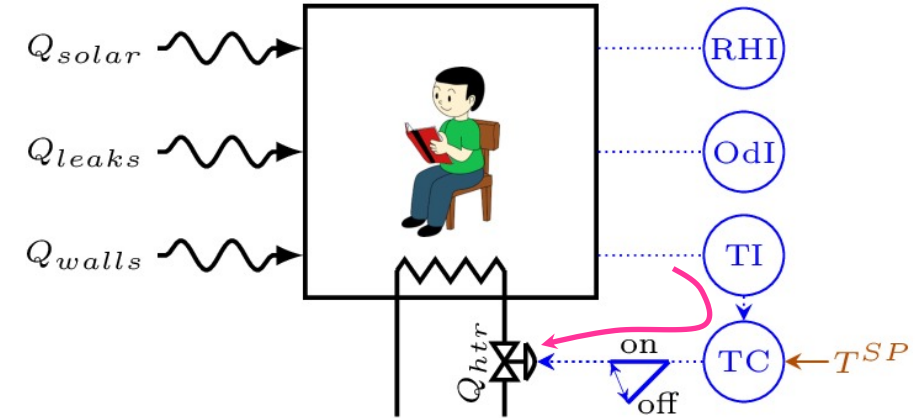
Feedback T Control



**CV**  
Variability



**MV**  
Variability



Alters dynamic characteristics of the process to more desirable



# PVs of Interest?



# PVs of Interest?



# Process Control

- Alters dynamic characteristics of a process
  - Transforms variability from CVs to MVs
  - Altered characteristics are 'desirable'
    - Safety, stability, economics, performance guarantees
- PV feedback a powerful mechanism for control
  - Inverts MV-CV relation
- Several available PV measurements
- What PV to control and how tightly to control it is a key decision
  - Requires process understanding