

Supplemental Material for:

“Mixture Rules and Falloff are Now Major Uncertainties in Experimentally Derived Rate Parameters for $\text{H} + \text{O}_2 (+\text{M}) \leftrightarrow \text{HO}_2 (+\text{M})$ ”

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S1 Dipole-Dipole Capture Rate Constants for HO₂ + H₂O

The dipole-dipole capture rate constants, Z_{d-d} , for HO₂+H₂O at various temperatures, are calculated according to Eq. (16) in [5],

$$Z_{d-d} = f_{rigid} \Gamma(1/3) (\mu_{D_1} \mu_{D_2})^{2/3} (k_B T)^{-1/6} (8\pi/\mu)^{1/2} \quad (S1)$$

where μ_{D_1} and μ_{D_2} are respectively the dipole moments for HO₂ and H₂O here; k_B is the Boltzmann constant; T is the temperature (K); μ is the reduced mass of the system; and the rigidity factor f_{rigid} is obtained from Eq. (2.21) in [9] as $f_{rigid} = k_{cap}/k_{cap}^{PST}$, where the thermal capture rate constants, k_{cap} , and the thermal capture rate constants from phase space theory (PST), k_{cap}^{PST} , are respectively obtained from Eqs. (2.13) and (2.24) in [9], which, for nonidentical dipoles, yields

$$\begin{aligned} f_{rigid} &= \frac{k_{cap}}{k_{cap}^{PST}} = \frac{f(\mu_{D_1} \mu_{D_2})^{1/3} C_6^{1/6} \sqrt{8\pi/\mu} \kappa(\theta, M)}{f \Gamma(1/3) (\mu_{D_1} \mu_{D_2})^{2/3} (k_B T)^{-1/6} \sqrt{8\pi/\mu}} \\ &= \frac{C_6^{1/6} \kappa(\theta, M)}{\Gamma(1/3) (\mu_{D_1} \mu_{D_2})^{1/3} (k_B T)^{-1/6}} \end{aligned} \quad (S2)$$

Thus, Eq.(S1) is further simplified as

$$Z_{d-d} = C_6^{1/6} \kappa(\theta, M) (\mu_{D_1} \mu_{D_2})^{1/3} \sqrt{8\pi/\mu} \quad (S3)$$

where C_6 is the constant of a $-C_6/r^6$ isotropic dispersion potential [9]; and $\kappa(\theta, M)$ is a dimensionless fitting function whose analytical form is reported in Fig. 2 of [9] as a function of the reduced dispersion constant $\theta = C_6 k_B T / (\mu_{D_1} \mu_{D_2})^2$ and dimensionless quantity describing degree of adiabaticity, M (not to be confused with the bath gas M).

Table S1: Molecular Parameters Used in the Current Calculations

	HO ₂	H ₂ O	HO ₂ -H ₂ O [†]
μ (g/mol)	33.006	18.015	11.654
ϵ/k_B (K)	365.56	535.21	442.32
σ (10 ⁻¹⁰ m)	3.433	2.673	3.053
μ_D (Debye)	2.090	1.847	
B_x (cm ⁻¹)	20.357	27.877	
B_y (cm ⁻¹)	1.118	14.512	
B_z (cm ⁻¹)	1.056	9.285	
B_{tot} (cm ⁻¹)	0.767	7.530	

[†] ϵ and σ for nonidentical molecule pair HO₂-H₂O are calculated from combination rules

Following [5], the optimized Lennard-Jones parameters and dipole moments from [11] are used for identical particle interactions (i.e. HO₂-HO₂ and H₂O-H₂O, see Table S1), from which the Lennard-Jones parameters for intermolecular dispersion potential between HO₂ and H₂O are estimated using Lorentz-Berthelot rules as $\epsilon_{12} = \sqrt{\epsilon_{11}\epsilon_{22}}$ and $\sigma_{12} = (\sigma_{11} + \sigma_{22})/2$. C_6 is therefore estimated from the Lennard-Jones parameters as $C_6 = 4\epsilon_{12}\sigma_{12}^6$ [5]. To get $\kappa(\theta, M)$, the dimensionless quantity M is first calculated from [9]

$$M = \frac{\mu(\mu_{D_1} \mu_{D_2})^{2/3} (B_1 + B_2)/2}{\hbar^2 (k_B T)^{2/3}} \quad (S4)$$

where B_i are the rotational constants for i^{th} particle in the system. Given that both involved particles are polyatomic with three distinct moments of inertia associated with x, y, z directions (Table S1), the rotational constant associated with the direction of dipole moments should be applied. However, if one simply calculates M using the total rotational constants (which are smaller than the appropriate rotational constant), then one could arrive at a lower limit for M (which turns out to be high enough for $\kappa(\theta, M)$ to be independent of M anyway for the present calculations).

Therefore, the results presented here should be relatively insensitive to the choice of rotational constants used in Eq.(S4). Using NIST’s Computational Chemistry Comparison and Benchmark DataBase (CCCBDB) [13] for molecular weights and directional rotational constants of HO₂ and H₂O, M is calculated from Eq. (S4). Together with $\theta = C_6 k_B T / (\mu_{D_1} \mu_{D_2})^2$, the values of $\kappa(\theta, M)$ for a specific temperature are read from Fig. 2 of [9] (it can be equivalently calculated using Eqs. (2.14, 2.15, 2.20) in [9] with the parameters from Table I and II in [9]). The dipole-dipole capture rate constants Z_{d-d} are then calculated via Eq. (S3) and tabulated in Table S2 for temperatures of relevant to the current study. (Note that the values in Table S2 differ from those in [5] by up to 25% using apparently the same procedures, though recalculations by [14] yielded the same results as reported here.)

Table S2: Calculated Dipole-Dipole Capture Rate Constants for HO₂ + H₂O at Various Temperatures.

T (K)	Z_{d-d} (10^{-10} cm ³ molecule ⁻¹ s ⁻¹)
200	7.18
300	7.37
400	7.55
500	7.73
600	7.89
700	8.03
800	8.17
900	8.29
1000	8.41
1100	8.52
1200	8.62
1300	8.72
1400	8.81
1500	8.90
1600	8.98
1700	9.06
1800	9.14
1900	9.22
2000	9.29

S2 Deriving Exponential-Down Factors to be Consistent with Reported Experimental Data

Alternative versions of Tables 1 and 2 (which display the $\langle \Delta E_{d,i} \rangle$ values in the 1D-ME model yielding consistency with the reported data) in the main text are provided as Tables S3 and S4 across the full range of experimental pressures (instead of the single representative pressure shown in Tables 1 and 2 used to fit $\langle \Delta E_d \rangle$). These are provided to show the variation of the extent of falloff of the mixture, $k_{0\text{-eff}}(T, P, \underline{X})/k_0(T, \underline{X})$, across the experimental ranges of pressure (which, as mentioned in the main text, is sufficiently small relative to experimental precision to evade detection).

Equivalent versions of these two tables are presented for the 2D/ φ -ME model as Tables S5 and S6. As mentioned in the main text, the exponential-down factors are instead chosen such that the calculated $k_{i,0\text{-eff}}(T, P)$ match the reported $k_{i,0\text{-eff,LMR-P,exp}}(T, P, \underline{X})$ from the experiments (i.e. assuming experiments were conducted in only pure mixtures) – due to the lack of functionality to handle bath gas mixtures in Variflex, the code which implements the 2D/ φ -ME model. These tables indicate that the strong-collision limit rate constant from the 2D/ φ -ME model using the dipole-dipole collision frequency for HO₂-H₂O are $\sim 30\%$ to a factor of ~ 3 lower than the experimentally reported rate constants. The $\langle \Delta E_{d,i} \rangle$ parameters derived for the 2D/ φ -ME to match experimental data are provided in Table S7.

Table S3: 1D-ME Results at 296 K

M	P (Torr)	$k_{i,0\text{-eff,LMR-P,exp}}(T, P, \underline{X})^\top$	$k_{i,0\text{-eff,LMR-P}}(T, P, \underline{X})^\perp$	$k_{0\text{-eff}}(T, P, \underline{X})/k_0(T, \underline{X})$	$\langle \Delta E_d \rangle(T)^\dagger$
O ₂	25	3.1	3.20	0.99	35.03
	50		3.17	0.98	
	75		3.13	0.96	
	100		3.10	0.95	
	150		3.04	0.94	
	200		2.99	0.92	
Ar/O ₂ [‡]	25	2.2	2.26	0.99	30.71
	50		2.24	0.98	
	75		2.22	0.97	
	100		2.20	0.96	
	150		2.17	0.95	
	200		2.15	0.94	
N ₂ /O ₂ [‡]	25	4.3	4.48	0.98	40.13
	50		4.41	0.97	
	75		4.36	0.96	
	100		4.30	0.94	
	150		4.21	0.92	
	200		4.13	0.91	
H ₂ O/O ₂ [‡]	2.2	50	50.28	1.00	101.77
	2.5		50.17	1.00	
	3		50.04	1.00	
	4		49.93	1.00	
	5		49.69	1.00	
	6		49.52	0.99	
	7		49.43	0.99	

[‡] from [10], units: $10^{-32}\text{cm}^6\text{molecule}^{-2}\text{s}^{-1}$;

[⊥] calculated using PAPR-MESS, units: $10^{-32}\text{cm}^6\text{molecule}^{-2}\text{s}^{-1}$;

[‡] $X_i/X_{\text{O}_2} = 98.5\%/1.5\%$ for $i = \text{Ar}, \text{N}_2$; $X_i/X_{\text{O}_2} = 10\%/90\%$ for $i = \text{H}_2\text{O}$;

[†] the listed exponential-down factors in i/O_2 mixtures are for i , units: cm^{-1} .

Table S4: 1D-ME Results at 1200 K

M	P (atm)	$k_{i,0\text{-eff},\text{LMR-P,exp}}(T, P, \underline{X})^\top$	$k_{i,0\text{-eff},\text{LMR-P}}(T, P, \underline{X})^\perp$	$k_{0\text{-eff}}(T, P, \underline{X})/k_0(T, \underline{X})$	$\langle \Delta E_d \rangle(T)^\dagger$
Ar	12	4.93	5.04	0.78	162.85
	15		4.93	0.76	
	18		4.84	0.75	
	20		4.78	0.74	
	25		4.65	0.72	
	30		4.55	0.70	
N ₂	12	6.82	6.99	0.76	186.15
	15		6.82	0.74	
	18		6.68	0.72	
	20		6.59	0.71	
	25		6.40	0.69	
	30		6.24	0.68	
H ₂ O/Ar [‡]	12	113	117.01	0.73	862.33
	15		112.82	0.71	
	18		110.25	0.69	
	20		108.39	0.68	
	25		104.36	0.66	
	30		100.96	0.64	

[‡] from [12], units: $10^{-33}\text{cm}^6\text{molecule}^{-2}\text{s}^{-1}$;

[⊥] calculated using PAPR-MESS, units: $10^{-33}\text{cm}^6\text{molecule}^{-2}\text{s}^{-1}$;

[‡] $X_{\text{H}_2\text{O}}/X_{\text{Ar}} = 10\%/90\%$;

[†] the listed exponential-down factors in the i/Ar mixture are for i , units: cm^{-1} .

Table S5: 2D/ φ -ME Results at 296 K

M	P (Torr)	$k_{i,0\text{-eff},\text{LMR-P,exp}}(T, P, \underline{X})^\top$	$k_{i,0\text{-eff}}(T, P)^\perp$	$k_{0\text{-eff}}(T, P)/k_0(T)$	$\langle \Delta E_d \rangle(T)^\dagger$
Ar	25	2.2	2.21	1.00	52.05
	50		2.21	1.00	
	75		2.20	1.00	
	100		2.20	1.00	
	150		2.19	0.99	
	200		2.19	0.99	
N ₂	25	4.3	4.30	1.00	102.02
	50		4.30	0.99	
	75		4.29	0.99	
	100		4.29	0.99	
	150		4.27	0.99	
	200		4.26	0.99	
H ₂ O	2.2	50	18.2		Strong-collision limit
	2.5		18.2		
	3		18.2		
	4		18.2		
	5		18.2		
	6		18.2		
	7		18.2		

[‡] from [10], units: $10^{-32}\text{cm}^6\text{molecule}^{-2}\text{s}^{-1}$;

[⊥] calculated using Variflex, units: $10^{-32}\text{cm}^6\text{molecule}^{-2}\text{s}^{-1}$;

[†] units: cm^{-1} .

Table S6: 2D/ φ -ME Results at 1200 K

M	P (atm)	$k_{i,0\text{-eff}, \text{LMR-P,exp}}(T, P, \underline{X})^{\dagger}$	$k_{i,0\text{-eff}}(T, P)^{\perp}$	$k_{0\text{-eff}}(T, P)/k_0(T)$	$\langle \Delta E_d \rangle(T)^{\dagger}$
Ar	12	4.93	4.97	0.95	204.71
	15		4.93	0.94	
	18		4.89	0.94	
	20		4.86	0.93	
	25		4.79	0.92	
	30		4.74	0.91	
N ₂	12	6.82	6.89	0.95	240.69
	15		6.82	0.94	
	18		6.76	0.93	
	20		6.70	0.92	
	25		6.61	0.91	
	30		6.54	0.90	
H ₂ O	12	113	83.9		Strong-collision limit
	15		81.4		
	18		79.4		
	20		77.9		
	25		74.6		
	30		72.5		

[†] from [12], units: $10^{-33}\text{cm}^6\text{molecule}^{-2}\text{s}^{-1}$;

[⊥] calculated using Variflex, units: $10^{-33}\text{cm}^6\text{molecule}^{-2}\text{s}^{-1}$;

[†] units: cm^{-1} .

Combining the results in Tables S3 and S4 for 1D-ME calculations and Tables S5 and S6 for 2D/ φ -ME calculations, the temperature-dependent exponential-down factors for M = Ar, N₂, and H₂O are derived as presented in Table 5 in the main text using 1D-ME model and in Table S7 using 2D/ φ -ME model. (Note that the calculated rate constants for H₂O from the 2D/ φ -ME could not be made to reproduce the experimental values even in the strong-collision limit.)

Table S7: Temperature-dependent energy-transfer parameters from 2D/ φ -ME model.

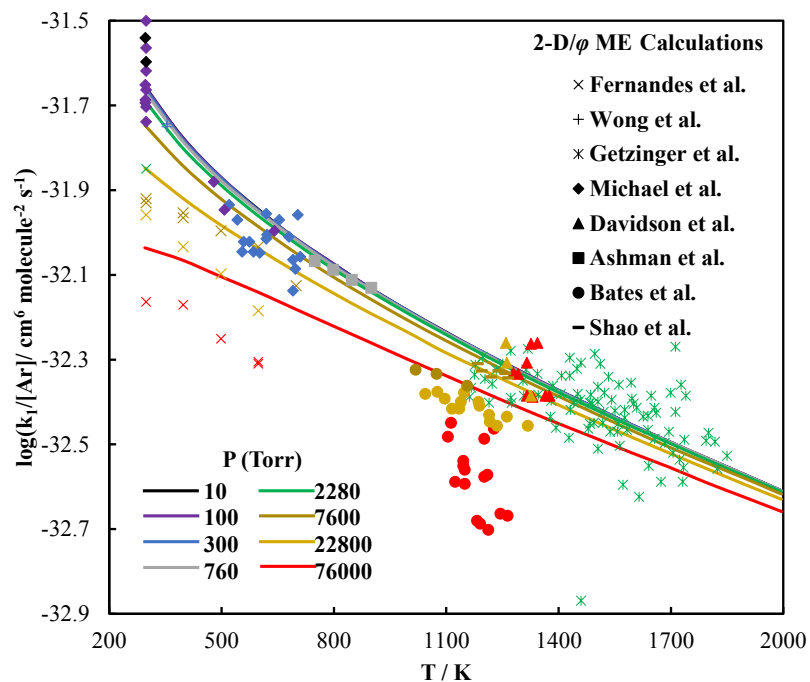
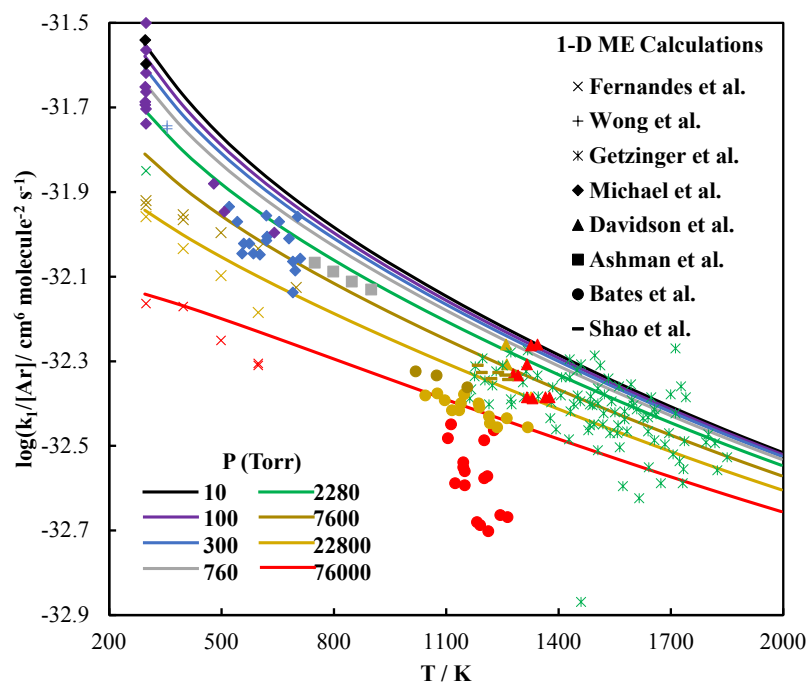
Ar	$\langle \Delta E_d \rangle_{\text{Ar}} = 52.40 \times (T/298)^{0.978}$
N ₂	$\langle \Delta E_d \rangle_{\text{N}_2} = 102.45 \times (T/298)^{0.613}$
H ₂ O	—

S3 Comparisons of Calculations and Other Experiments

Results from 1D-ME and 2D/ φ -ME calculations using the exponential-down factors from Table S7 and a priori 2D-ME calculations for Ar [8] with comparisons to reported experimental determinations [1, 2, 3, 4, 5, 6, 10, 12, 15] are shown in Figures S1–S4.

All three master equation models show reasonable agreement with experimental data (given the scatter in the experimental data) as shown in Figs. S1, S3, and S4. The a priori 2D-ME calculations, which are expected to be accurate within $\sim 20\text{--}30\%$ [7, 8], unsurprisingly appear to yield the best agreement with the experimental data. The 1D-ME and 2D/ φ -ME calculations, while different, show similar agreement with experimental data – at a level that still appears reasonable given the large scatter in most experimental datasets.

As shown in Fig. S2, the three master equation models yield similar results – with some slight differences on the order of $\sim 30\%$ – which provides an indication of the sensitivity of the calculation to different treatments of angular momentum.



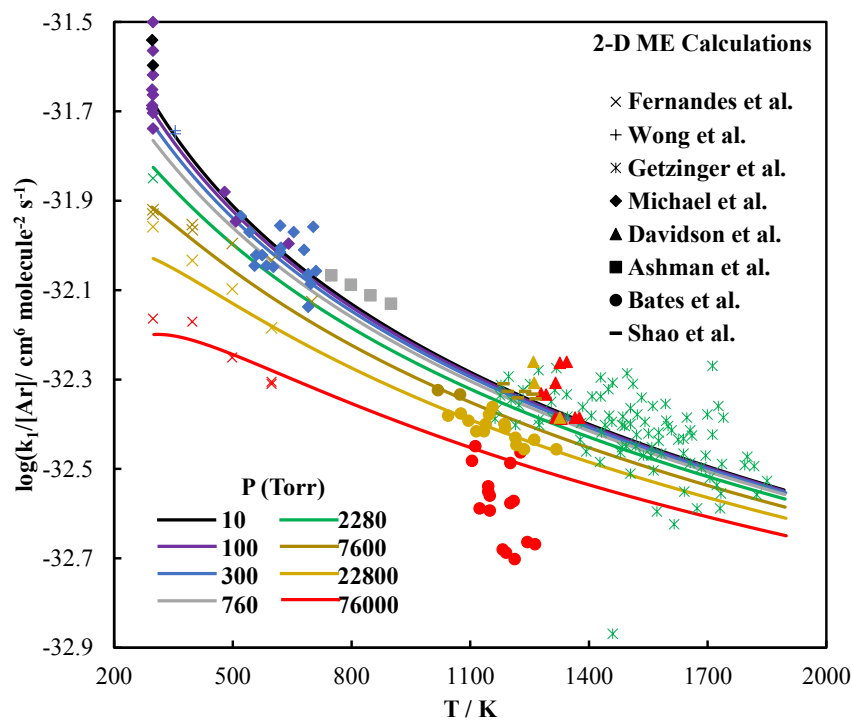


Figure S1: Ab initio master equation (ME) calculated temperature- and pressure-dependent rate constants for $\text{H} + \text{O}_2 + \text{Ar} \rightarrow \text{HO}_2 + \text{Ar}$ versus experimental determinations. The experimental data points [1, 2, 4, 5, 6, 10, 12, 15] are color coded according to the closest pressure from the theoretical calculations. Results are shown from a 1D-ME (E -resolved model) (top), a 2D/ φ -ME (approximate E, J -resolved model) (middle), and an a priori 2D-ME (E, J -resolved model) [8] (bottom).

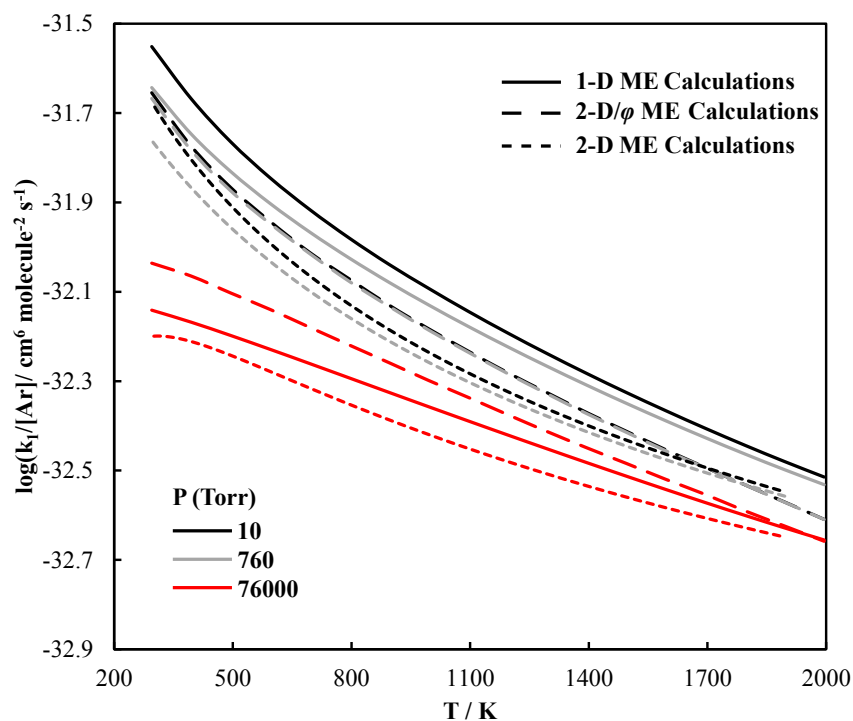


Figure S2: Ab initio master equation (ME) calculated temperature- and pressure-dependent rate constants for $\text{H} + \text{O}_2 + \text{Ar} \rightarrow \text{HO}_2 + \text{Ar}$ versus experimental determinations. Results are shown from a 1D-ME (E -resolved model) (solid lines), a 2D/ ϕ -ME (approximate E, J -resolved model) (long dashed lines), and an a priori 2D-ME (E, J -resolved model) [8] (short dashed lines).

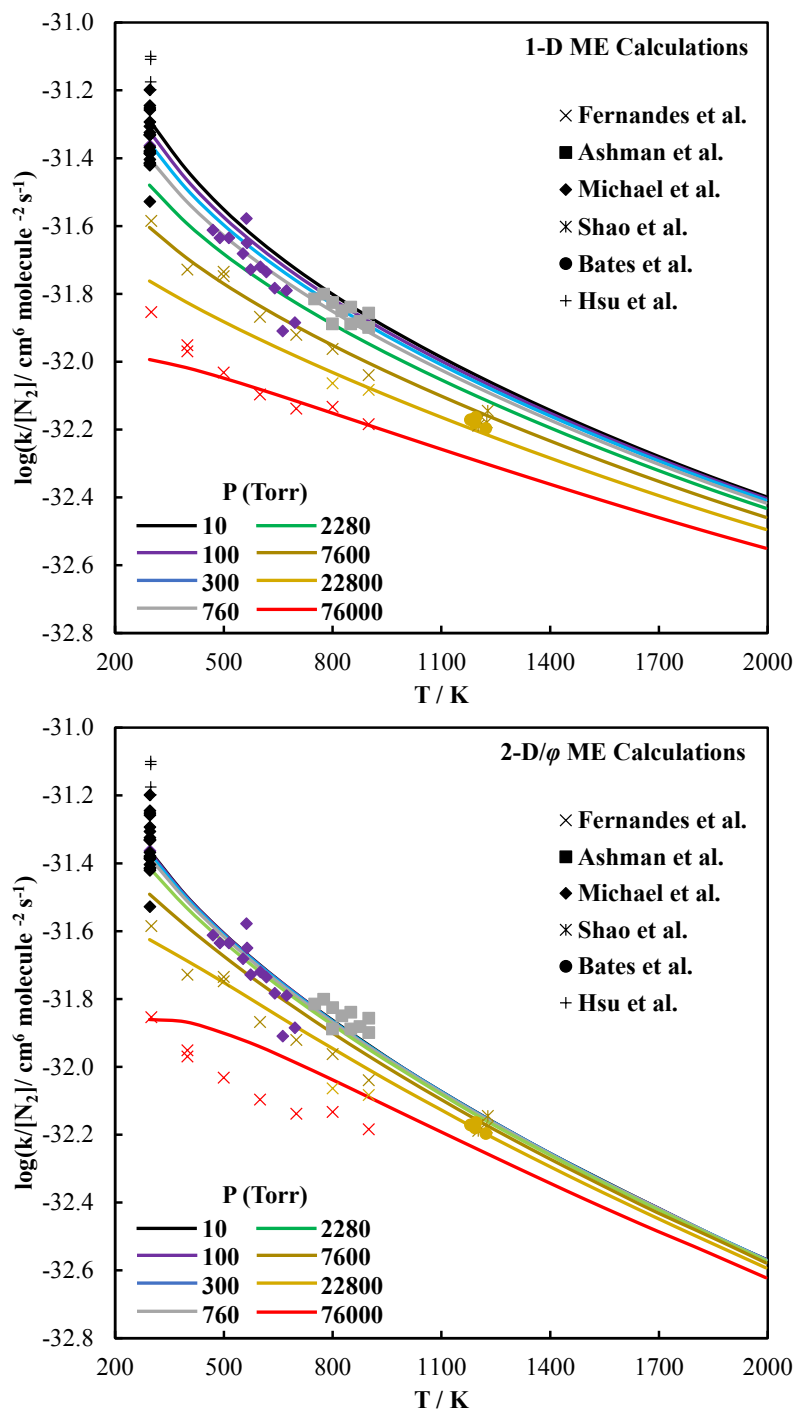


Figure S3: Ab initio master equation (ME) calculated temperature- and pressure-dependent rate constants for $\text{H} + \text{O}_2 + \text{N}_2 \rightarrow \text{HO}_2 + \text{N}_2$ versus experimental determinations. The experimental data points [1, 2, 5, 10, 12] are color coded according to the closest pressure from the theoretical calculations. Results are shown from a 1D-ME (E -resolved model) (top) and a 2D/ ϕ -ME (approximate E, J -resolved model) (bottom).

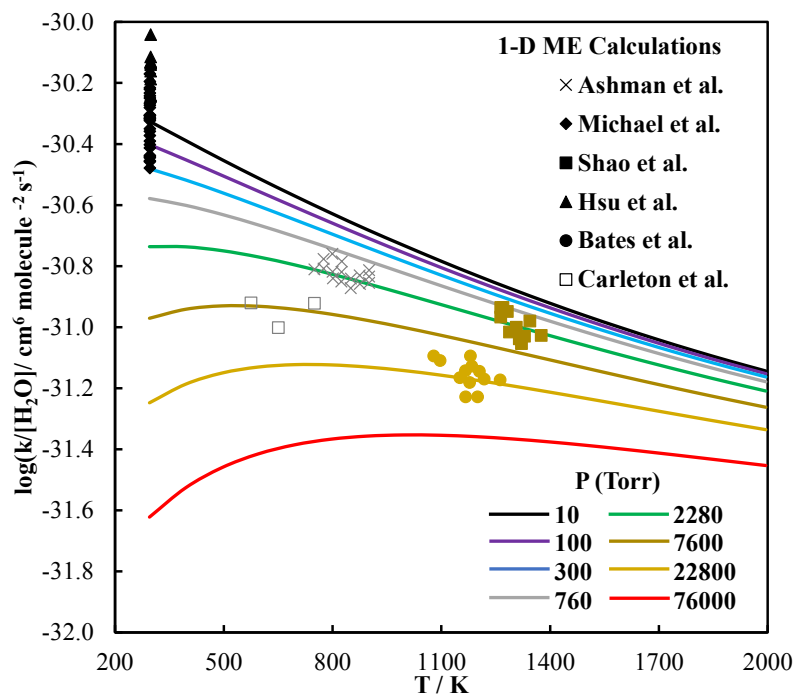


Figure S4: Ab initio master equation (ME) calculated temperature- and pressure-dependent rate constants for $\text{H} + \text{O}_2 + \text{H}_2\text{O} \rightarrow \text{HO}_2 + \text{H}_2\text{O}$ versus experimental determinations. The experimental data points [1, 2, 3, 10, 12] are color coded according to the closest pressure from the theoretical calculations. Results are shown from a 1D-ME (E -resolved model). Note that the calculated results plotted were obtained for pure H_2O , whereas the experimental determinations plotted were obtained in mixtures of various H_2O mole fractions using the linear mixture rule.

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