Lecture 9

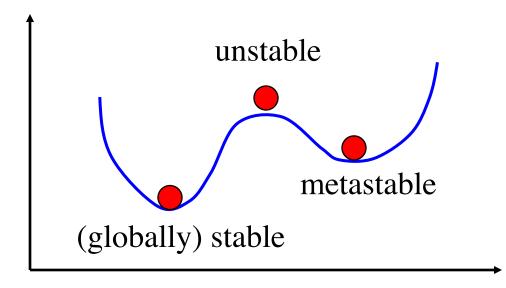
- Stability criteria
- Common stability criteria thermal, mechanical, diffusional
- Physical meaning of stability criteria
- Le Chatelier's principle
- Spinodal and Critical state
- The 3rd law

Objectives

- Aware of stability conditions
- Know the common stability conditions
- Know how to determine critical point for fluids from EOS
- Know the consequences of the 3rd law

Stable, Metastable and Unstable Equilibrium

- Equilibrium originally a mechanical concept vanishing of force
- Stability has to do with how system responds to perturbation



- Unstable: infinitesimal perturbation leads system away from its initial equilibrium state
- Metastable: system stable with respect to small local perturbations, but large perturbation will lead to transition to a more stable state
- (Globally) stable state: lowest energy state

Local stability determined by curvature

Entropy Maximization Principle

Like the equilibrium condition, stability condition comes from 2nd law

$$\left(\frac{\delta S}{\delta X}\right)_{V,U} = 0 \qquad \left(\frac{\delta^2 S}{\delta X^2}\right)_{V,U} < 0$$

For multiple variables

$$\left(\frac{\delta S}{\delta X_i}\right)_{V,U,X_{i\neq i}} = 0$$
 $\left(\frac{\delta^2 S}{\delta X_i \delta X_j}\right)_{V,U,X_{k\neq i,j}}$ is a matrix

In general need to look at eigenvalue of the matrix, and ensure that the largest eigenvalue remains negative.

Thermal Stability

$$U'$$
 $U-U'$ 1

$$\left(\frac{\delta S}{\delta U'}\right)_V = 0$$

$$\delta^{2}S = \delta^{2}S_{1} + \delta^{2}S_{2} = \left(\frac{\partial^{2}S_{1}}{\partial U_{1}^{2}}\right)(\delta U_{1})^{2} + \left(\frac{\partial^{2}S_{2}}{\partial U_{2}^{2}}\right)(\delta U_{2})^{2} < 0$$

$$\delta^{2}S = \delta^{2}S_{1} + \delta^{2}S_{2} = \left(\frac{\partial(1/T_{1})}{\partial U_{1}}\right)(\delta U_{1})^{2} + \left(\frac{\partial(1/T_{2})}{\partial U_{2}}\right)(\delta U_{2})^{2} < 0$$

$$\delta^{2}S = \delta^{2}S_{1} + \delta^{2}S_{2} = -\frac{1}{T^{2}}\left(\frac{1}{C_{V1}} + \frac{1}{C_{V2}}\right)(\delta U')^{2} < 0$$

$$\left(\frac{\partial 1/T}{\partial U}\right)_{V} = -\frac{1}{T^{2}}\left(\frac{\partial T}{\partial U}\right)_{V} = -\frac{1}{T^{2}C_{V}}$$

Thermal Stability

$$\left(\frac{1}{C_{V1}} + \frac{1}{C_{V2}}\right) < 0$$

True for any partitioning of the system

$$C_V > 0$$

$$C_V = T \left(\frac{\partial S}{\partial T} \right)_{N,V}$$

$$\left(\frac{\partial S}{\partial T}\right)_{N,V} > 0$$
 $T \Leftrightarrow S$, conjugates

$$T \Leftrightarrow S$$
, conjugates

Mechanical Stability

$$V'$$
 $V-V'$ 2

$$\left(\frac{\delta F}{\delta V'}\right)_T = 0$$

$$\delta^2 F = \delta^2 F_1 + \delta^2 F_2 = \left(\frac{\partial^2 F_1}{\partial V_1^2}\right) (\delta V_1)^2 + \left(\frac{\partial^2 F_2}{\partial V_2^2}\right) (\delta V_2)^2 > 0$$

$$\delta^2 F = \delta^2 F_1 + \delta^2 F_2 = -\left(\frac{\partial P_1}{\partial V_1}\right) (\delta V_1)^2 - \left(\frac{\partial P_2}{\partial V_2}\right) (\delta V_2)^2 > 0$$

$$\delta^2 F = \delta^2 F_1 + \delta^2 F_2 = \left(\frac{1}{V_1 \kappa_{T1}} + \frac{1}{V_2 \kappa_{T2}}\right) (\delta V')^2 > 0$$

$$\kappa_T = -\frac{1}{V} \left(\frac{\partial V}{\partial P}\right)_T$$

Mechanical Stability

$$\left(\frac{1}{V_1\kappa_{T1}} + \frac{1}{V_2\kappa_{T2}}\right) > 0$$

True for any partitioning of the system

$$\kappa_T > 0$$

$$\kappa_T = -\frac{1}{V} \left(\frac{\partial V}{\partial P} \right)_T$$

$$-\left(\frac{\partial P}{\partial V}\right)_{N,T} > 0 \qquad -P \Leftrightarrow V, \text{ conjugates}$$

$$-P \Leftrightarrow V$$
, conjugates

Summary of Common Stability Conditions

$$C_p > C_V > 0$$

$$\kappa_T > \kappa_S > 0$$

Diffusional
$$\left(\frac{\partial \mu_i}{\partial n_i}\right)_{V,T,n_{j\neq i}} > \left(\frac{\partial \mu_i}{\partial n_i}\right)_{P,T,n_{j\neq i}} > 0$$

More generally

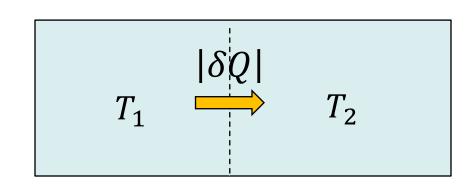
$$\left(\frac{\partial \xi_i}{\partial X_i}\right)_{Y,Z} > 0 \qquad \xi_i \iff X_i \quad \text{conjugates}$$

$$\xi_i \iff X_i$$

Physical Interpretation of Stability Condition

Take thermal stability as example

$$T_1 > T_2$$



Then, according to direction of change

$$Q_1 = -|\delta Q|$$
 $Q_2 = |\delta Q|$

Now,
$$C_V = \frac{\delta Q}{\delta T}$$
 \Longrightarrow $\delta T_1 = \frac{\delta Q_1}{C_{V1}} = -\frac{|\delta Q|}{C_{V1}}$ $\delta T_2 = \frac{\delta Q_2}{C_{V2}} = \frac{|\delta Q|}{C_{V2}}$

$$\delta T_2 = \frac{\delta Q_2}{C_{V2}} = \frac{|\delta Q|}{C_{V2}}$$

If
$$C_V < 0$$
 then $\delta T_1 > 0$ $\delta T_2 < 0$

$$\delta T_1 > 0$$

$$\delta T_2 < 0$$

Hotter side gets hotter Cooler side gets cooler



Le Chatelier's Principle

When a system at equilibrium is perturbed by the application of an <u>action</u>, the <u>reaction</u> of the system is such as to decrease the effect of the action.

Any change in <u>status quo</u> prompts an opposing reaction in the responding system

Spinodal

Susceptibility (response function) diverges

Spinodal: limit of local stability $\left(\frac{\partial^2 F}{\partial X^2}\right) = 0$

$$\left(\frac{\partial^2 F}{\partial X^2}\right) = 0$$

$$\left(\frac{\partial P}{\partial V}\right)_T = 0$$

For parameters

$$\kappa_T < 0$$

system spontaneously phase separate into a stable liquid and vapor with $\kappa_T > 0$ in each

Critical States

When
$$\left(\frac{\partial^2 F}{\partial X^2}\right) = 0$$
 need to go to higher order
$$\delta F = \delta F^{(1)} + \delta F^{(2)} + \delta F^{(3)} + \delta F^{(4)} \dots$$

Now
$$\delta F^{(3)} = \frac{1}{3!} \left(\frac{\partial^3 F}{\partial X^3} \right) (\delta X)^3$$
 Sign depends on δX

More generally

$$\left(\frac{\partial \xi_i}{\partial X_i}\right) = 0$$
 and $\left(\frac{\partial^2 \xi_i}{\partial X_i^2}\right) = 0$ ξ_i intensive conjugate to extensive X_i

Critical States

For fluid

$$\left(\frac{\partial P}{\partial V}\right)_T = 0$$
 and $\left(\frac{\partial^2 P}{\partial V^2}\right)_T = 0$

determined from EOS

Third Law

The entropy of a system at absolute zero Kevin is a finite constant.

$$\lim_{T\to 0} S = S_0$$

Planck: The entropy of a perfect crystal at T=0 K is zero

With Boltzmann's statistical definition, 3rd is automatically satisfied.

$$S = k \ln \Omega$$

Consequences of Third Law

Calculating absolute entropy

$$S(T) = \int_0^T \frac{C_P}{T} dT$$

If there are phase transitions, including latent heat. Example gas

$$S(T) = \int_0^{T_m} \frac{C_{P,S}}{T} dT + \frac{\Delta_{fus}H}{T_m} + \int_{T_m}^{T_b} \frac{C_{P,l}}{T} dT + \frac{\Delta_{vap}H}{T_b} + \int_{T_b}^{T} \frac{C_{P,g}}{T} dT$$

Consequences of Third Law

$$\lim_{T\to 0} C_{x} = 0$$

X can be anything, P, V, E, etc.

Proof:

$$S(0) = S(T) + \left(\frac{\partial S}{\partial T}\right)(0 - T) + O(T^2)$$

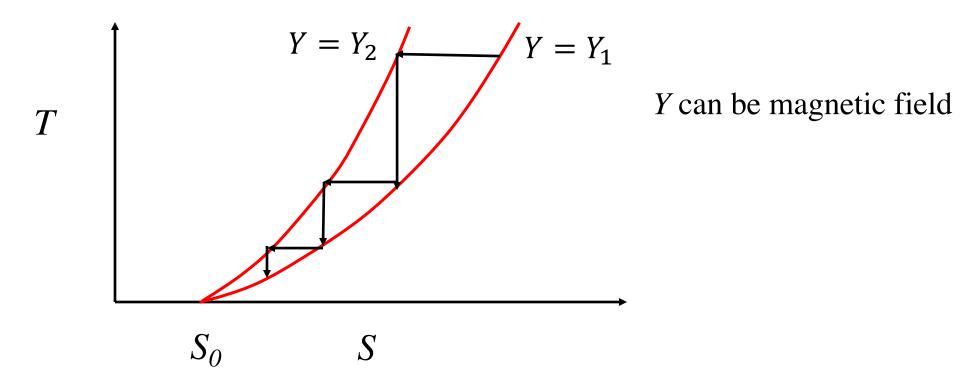
$$S(0) = S(T) - T\left(\frac{\partial S}{\partial T}\right) + O(T^2)$$

Since
$$\lim_{T\to 0} S(T) = S(0)$$
 \Longrightarrow $\lim_{T\to 0} T\left(\frac{\partial S}{\partial T}\right) = 0$

i.e.
$$C_X(0) = 0$$

Consequences of Third Law

It is impossible to reach absolute zero K by a finite number of isothermal-adiabatic steps



T-S diagram: useful for analyzing reversible heat (analogue of P-V diagram for work

$$Q_{rev} = \int T dS$$

Questions to Think about

- Think physically why $C_p > C_V \quad \kappa_T > \kappa_S$
- Repeat the physical interpretation for mechanical and diffusional stability
- Is it necessary to know the absolute value of entropy?

Lecture 11

- Ideal gas
 - fundamental equation perspective
 - entropic origin of EOS
 - chemical potential
 - properties
- Real gas
 - virial EOS
 - van der Waals
 - hard sphere (Carnahan-Starling)
 - Redlich-Kwong, Peng-Robinson
 - properties

Read Ch. 7 Sandler, Chs. 9 and 11 Callen

Objectives

- Know *everything* about ideal gas
- *Memorize* vdW EOS
- Be able to calculate property and property changes for vdW EOS and virial EOS

Ideal Gas

Defined by IG EOS

$$PV = nRT$$
 $Pv = RT$

Fundamental equation

$$s = s_0 + f(u) + R\ln(\nu/\nu_0)$$

$$S = ns_0 + nf(U/n) + nR\ln(V/N\nu_0)$$

$$dS = \frac{1}{T}dU + \frac{P}{T}dV - \frac{\mu}{T}dn$$

$$\frac{1}{T} = \left(\frac{\partial S}{\partial U}\right)_{n,V} = f_u'$$

$$\left(\frac{\partial^2 S}{\partial U^2}\right)_{n,V} = \left(\frac{\partial \left(\frac{1}{T}\right)}{\partial U}\right)_{n,V} = -\frac{1}{T^2 C_V} = -\frac{1}{n} f_{uu}^{"} \qquad \text{so} \qquad C_V = -\frac{n}{T^2 f_{uu}^{"}}$$

Special Case of Constant Cv

$$dU = C_V dT \qquad U = C_V T \qquad dS = \frac{1}{T} dU + \frac{P}{T} dV - \frac{\mu}{T} dn$$

$$\frac{1}{T} = \left(\frac{\partial S}{\partial U}\right)_{n,V} = f'_u \qquad \longrightarrow \qquad f(u) = aR\ln(u/u_0)$$

$$\longrightarrow$$
 $u = aRT$

$$C_V = naR$$

PVT Equation of State

from
$$S = ns_0 + nf(U/n) + nR\ln(V/N\nu_0)$$

$$S = ns_0 + nf(U/n) + nR\ln(V/N\nu_0) \qquad dS = \frac{1}{T}dU + \frac{P}{T}dV - \frac{\mu}{T}dn$$

$$\frac{P}{T} = \left(\frac{\partial S}{\partial V}\right)_{n,U} = \left(\frac{\partial S}{\partial V}\right)_{n,u} = \frac{nR}{V}$$

$$\longrightarrow$$
 $PV = nRT$

Pressure of IG is entropic in origin

$$P = -\left(\frac{\partial F}{\partial V}\right)_{T} = -\left(\frac{\partial V}{\partial V}\right)_{T}^{0} + T\left(\frac{\partial S}{\partial V}\right)_{T}^{0}$$

Chemical Potential of Ideal Gas

$$-\frac{\mu}{T} = \left(\frac{\partial S}{\partial n}\right)_{U,V} = s_0 + f(u) - \frac{u}{T} + R \ln \frac{v}{v_0} - R \qquad dS = \frac{1}{T}dU + \frac{P}{T}dV - \frac{\mu}{T}dn$$

For special case $f=aR\ln(u/u_0)$

$$\mu = -Ts_0 - aR \ln \frac{aRT}{u_0} + R \ln \frac{Pv_0}{RT} + (a+1)R$$

From Euler equation
$$U = TS - PV + \mu n$$
 \longrightarrow $G = U - TS + PV = \mu n$

 $\mu(T, P)$ is molar Gibbs free energy

Knowing $\mu(T, P)$ we obtain $G(n, T, P) = n\mu(T, P)$

Fundamental equation!

Chemical Potential of Ideal Gas

Alternatively, since m is molar Gibbs free energy, we have

$$d\mu = -sdT + vdP$$

Integrating at constant T

$$\mu(P,T) = \mu(P_0,T) + RT \ln \frac{P}{P_0}$$

Often choose P_0 as standard pressure P^{Θ} (1 bar)

$$\mu(P,T) = \mu^{\Theta}(T) + RT \ln \frac{P}{P^{\Theta}}$$

Reference chemical potential is given by fundamental equation (we derive it in stat. mech.)

Properties of Ideal Gas

- U and H are functions of temperature only and independent of density or pressure
- Joule coefficient

$$\left(\frac{\partial T}{\partial V}\right)_{N,U} = 0$$

• Joule-Thomson coefficient

$$\left(\frac{\partial T}{\partial P}\right)_{N,H} = 0$$

• Chemical potential

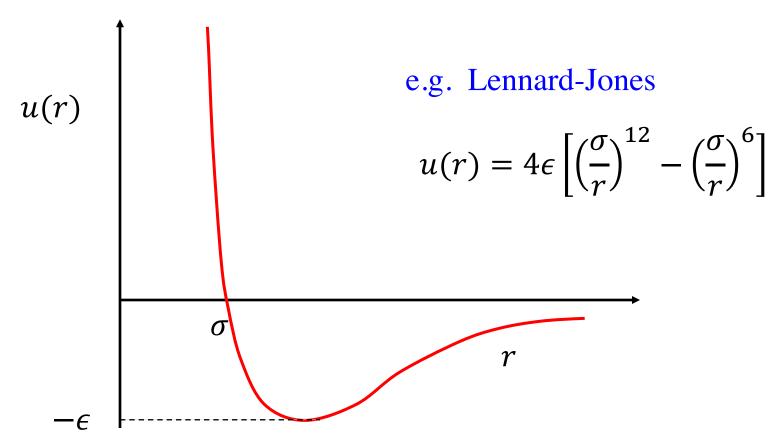
$$\mu = \mu^{(0)}(T) + RT \ln(p / p^{(0)})$$

a fundamental equation

Real Gases

Interactions

- Short-range hard repulsion (excluded volume)
- Long-range attraction (dispersion interaction)



Real Gases

Virial EOS

$$P = \rho RT[1 + B\rho + C\rho^2 + \cdots] = \rho RTZ$$
 Z: compressibility factor
$$Z = 1 + B'P + C'P^2 + \cdots$$

$$B' = \frac{B}{RT}, C' = \frac{C - B^2}{(RT)^2}$$

• Hard-spheres (Carnahan-Starling) $b_0 = N_a(\pi/6)\sigma^3$

$$P = \frac{RT}{\nu} \left[\frac{\nu^3 + b_0 \nu^2 + b_0^2 \nu - b_0^3}{(\nu - b_0)^3} \right]$$

• Hard-spheres + attraction

$$P = \frac{RT}{\nu} \left[\frac{\nu^3 + b_0 \nu^2 + b_0^2 \nu - b_0^3}{(\nu - b_0)^3} \right] - \frac{a}{\nu^2}$$

Real Gases

Van der Waals

$$P = \frac{RT}{v - b} - \frac{a}{v^2}$$

a: two-body attraction

b: excluded volume

Redlich-Kwong

$$P = \frac{RT}{\nu - b} - \frac{a}{T^{1/2}\nu(\nu + b)}$$

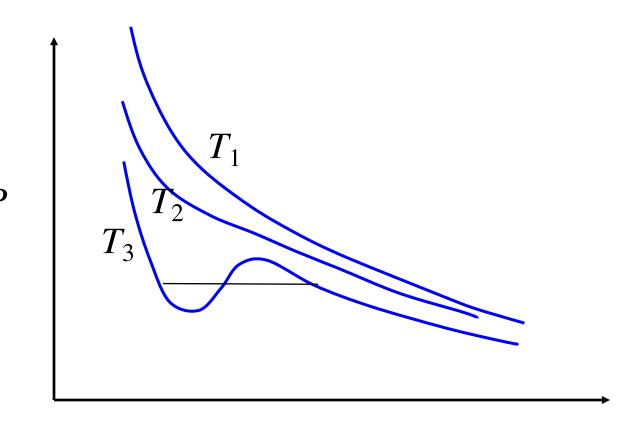
• Peng-Robinson

$$P = \frac{RT}{\nu - b} - \frac{a}{\nu(\nu + b) + b(\nu - b)}$$

accurate up to high pressures widely used in industrial modeling

P-V Isotherm

- Pressure increases with T and decreases with v
- At sufficiently low *T*, can have nonmonotonic behavior, signaling vapor-liquid transition
- Some portion violates stability condition
- Use Maxwell construct to get rid of unphysical region



 ν

Properties of Real Gases

- U, H, functions of T and P (or V)
- Nonzero Joule and Joule-Thompson coefficients
- Can condense into liquid phase at sufficiently low temperature and/or high pressure

usually
$$\left(\frac{\partial T}{\partial V}\right)_U < 0$$

but
$$\left(\frac{\partial T}{\partial P}\right)_H$$
 can change sign

Joule Coefficient for vdW Gas

$$\left(\frac{\partial T}{\partial V}\right)_{U} = -\left(\frac{\partial T}{\partial U}\right)_{V} \left(\frac{\partial U}{\partial V}\right)_{T} = -\frac{1}{C_{V}} \left[T\left(\frac{\partial P}{\partial T}\right)_{V} - P\right]$$

For vdW gas
$$P = \frac{RT}{v - b} - \frac{a}{v^2}$$

$$\left[T\left(\frac{\partial P}{\partial T}\right)_{V} - P\right] = \frac{a}{v^2}$$

$$\left(\frac{\partial T}{\partial v}\right)_u = -\frac{a}{v^2 c_V}$$
 Joule coefficient usually negative

Joule-Thomson Coefficient for vdW Gas

$$\left(\frac{\partial T}{\partial P}\right)_{H} = \left[\frac{2a}{RT}\left(\frac{v-b}{v}\right)^{2} - b\right] \left[\frac{5R}{2} - \frac{3a}{vT}\left(\frac{v-b}{v}\right)^{2}\right]^{-1}$$

low density $\nu \to \infty$

$$\left(\frac{\partial T}{\partial P}\right)_{H} = \frac{2}{5R} \left(\frac{2a}{RT} - b\right)$$

inversion temperature

$$T_{inv} = \frac{2a}{Rb}$$

 $T < T_{inv}$ cooling upon throttling (liquefaction)

 $T > T_{inv}$ heating upon throttling

Questions to Think about

- What's the physical reason that the Joule coefficient is negative?
- Why the Joule coefficient of the vdW gas doesn't depend on the parameter *b*?
- How does the chemical potential behave as the pressure or density approaches zero?