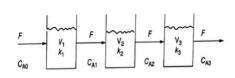
## **Experiment No 8** Rate Study in Cascade CSTR

**Aim:** Rate study in a cascade CSTR (CSTR in series)

Description: The Cascade CSTR consist 3 identical CSTRs in series where product stream



of the first CSTR enters 2nd one as feed, product stream of the 2<sup>nd</sup> CSTR enters 3<sup>rd</sup> as feed and product of the system flows out from the 3<sup>rd</sup> CSTR. The reactant streams N/20 NaOH Solution (A) and N/10 CH<sub>3</sub>COOC<sub>2</sub>H<sub>5</sub> Solution (B) flows to the 1st CSTR from respective storage tanks via rotameters to control flow rates. Reactor volume = 1.135 L

## **Procedure:**

- Reactants of prescribed concentration are already prepared and fed in the designated storage tanks.
- Record the ambient temperature of reaction mixture.8. 2.
- 3. Calibrate each rotameter with respective liquid.
- 4. Allow the two reactants streams [NaOH(A) and CH<sub>3</sub>COOC<sub>2</sub>H<sub>5</sub> (B)] to enter the first CSTR at equal feed rate so that in the reactor  $C_{A0} = C_{B0}$ . Start the mixer and wait till the product flows out from the 3<sup>rd</sup> CSTR. Give 5-10 min for steady state.
- Fix and record the flow rates  $F_A = F_B$ 5.
- Collect 10 ml sample from each 3 reactor outlets and and titrate with N/50 Succinic 6. Acid Solution to estimate unreacted NaOH
- 7. Repeat steps 4-6 for different flow rate sets.
- Record Volume of each reactor  $(V_1 = V_2 = V_3)$ 8.

## Calculations:

 $-r_A = -\frac{dC_A}{dt} = kC_A^2$ Feed conditions are such that  $C_{A0} = C_{B0}$ ,

= Volumetric flow rate through the reactor system (constant)

= Volume of reaction mass in the nth reactor

 $(C_A)_n$  = molar conc. Of reactant A in the nth reactor

 $(C_A)_{n-1}$  = molar conc. Of reactant A in the(n-1)th reactor

= V<sub>n</sub>/F = normal holding time in the nth reactor

A steady flow material balance over nth reactor is

$$F(C_A)_{n-1} + V_n \frac{dC_A}{dt} = F(C_A)_n ---- (1)$$

$$(C_A)_n = \text{molar conc. Of reactant A in the nth reactor} \\ (C_A)_{n-1} = \text{molar conc. Of reactant A in the (n-1)th reactor} \\ \theta_n = V_n/F = \text{normal holding time in the nth reactor} \\ A \text{ steady flow material balance over nth reactor is} \\ F(C_A)_{n-1} + V_n \frac{dC_A}{dt} = F(C_A)_n & ---- (1)_n \\ \text{or,} & \frac{(C_A)_{n-1}}{(C_A)_n} = 1 - \frac{\theta_n}{(C_A)_n} \left(\frac{dC_A}{dt}\right)_n & ---- (2)_n \\ \text{For second order reaction,} & -\frac{dC_A}{dt} = kC_A^2 \\ \text{And from Eq. (2)} & \frac{(C_A)_{n-1}}{(C_A)_n} = 1 + k\theta_n(C_A)_n & ---- (3)_n \\ \text{For the conditions, equal volume of tanks V}_1 = V_2 = V_3 = V \text{ and } \theta_1 = \theta_2 = \theta_3 \\ & (C_A)_{n-1} - (C_A)_n = k\theta_n(C_A)_n^2 \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] = ln(k\theta_n) + 2ln(C_A)_n & ---- (4)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] = ln(k\theta_n) + 2ln(C_A)_n & ---- (4)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] = ln(k\theta_n) + 2ln(C_A)_n & ---- (4)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] = ln(k\theta_n) + 2ln(C_A)_n & ---- (4)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] = ln(k\theta_n) + 2ln(C_A)_n & ---- (4)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] = ln(k\theta_n) + 2ln(C_A)_n & ---- (4)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] = ln(k\theta_n) + 2ln(C_A)_n & ---- (4)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] = ln(k\theta_n) + 2ln(C_A)_n & ---- (4)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] & ---- (4)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] = ln(k\theta_n) + 2ln(C_A)_n & ---- (4)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] = ln(k\theta_n) + 2ln(C_A)_n & ---- (4)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] & ---- (C_A)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] = ln(k\theta_n) + 2ln(C_A)_n & ---- (L_A)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] & ---- (C_A)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] & ---- (C_A)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] & ---- (C_A)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] & ---- (C_A)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] & ---- (C_A)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] & ---- (C_A)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] & ---- (C_A)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] & ---- (C_A)_n \\ \text{or} & ln[(C_A)_{n-1} - (C_A)_n] & ---- (C_A)_n \\ \text{or} & ln[(C_A)_{n-1}$$

For second order reaction,

And from Eq. (2) 
$$\frac{(C_A)_{n-1}}{(C_A)_n} = 1 + k\theta_n(C_A)_n \qquad --- (3)$$

For the conditions, equal volume of tanks  $V_1 = V_2 = V_3 = V$  and  $\theta_1 = \theta_2 = \theta_3 = \theta$ ,

or 
$$(C_A)_{n-1} - (C_A)_n = k\theta_n (C_A)_n^2$$
  
or  $ln[(C_A)_{n-1} - (C_A)_n] = ln(k\theta_n) + 2ln(C_A)_n$  --- (4)

Performance Chart to be obtained by plotting  $(C_A)_{n-1}$  vs  $(C_A)_n$  using Eq. (3)

Rate constant to be obtained from Eq (4) as 
$$k = \frac{[(C_A)_{n-1}/(C_A)_n] - 1}{\theta_n(C_A)_n}$$