

1	Company Name Not Available Bedford, MA USA						Case Name:		GamVet From LEVULINIC ACID and ISOPROPANOL -Double Series R							
2							Unit Set:		SI							
3							Date/Time:		Sat Jul 22 12:30:17 2023							
4																
5																
6	HI Design Datasheet															
7																
8	APLUS_Import															
9	Scenario 1															
10	SimulationBaseCase															
11																
12	Performance															
13																
14																
15	Summary															
16																
17	NETWORK COST INDEXES															
18																
19			Cost Index						% of Target							
20	Heating (Cost/s)		6.049e-002 *						101.0 *							
21	Cooling (Cost/s)		-4.766e-004 *						-6696 *							
22	Operating Cost (Cost/s)		6.001e-002 *						100.2 *							
23	Capital Cost (Cost)		2.345e+006 *						112.0 *							
24	Total Cost (Cost/s)		7.963e-002 *						102.9 *							
25	NETWORK PERFORMANCE															
26																
27			HEN						% of Target							
28	Heating (kJ/h)		2.627e+007 *						103.5 *							
29	Cooling (kJ/h)		2.580e+007 *						103.6 *							
30	Number of Units		13.00 *						76.47 *							
31	Number of Shells		22.00 *						104.8 *							
32	Total Area (m2)		3582 *						100.8 *							
33	Heat Exchangers															
34																
35	Heat Exchanger		Cost Index (Cost)				Area (m2)		Shells		Load (kJ/h)					
36																
37	HE-102		1.062e+004 *				0.7219		1 *		3.420e+005					
38	Condenser@DC-103		5.837e+004 *				168.6		1 *		1.566e+006					
39	STHE-101		1.096e+004 *				0.8863		4 *		5.084e+004					
40	Reboiler@DC-101		1.212e+006 *				34.89		1 *		2.313e+007					
41	R-102_heat_Exchanger		1.099e+004 *				1.309		1 *		5.403e+004					
42	HE-101		1.055e+004 *				0.6196		1 *		1.807e+005					
43	STHE-102		1.058e+004 *				0.6662		1 *		3.245e+005					
44	Reboiler@DC-102		1.691e+005 *				1.085		1 *		7.178e+005					
45	R-101_heat_Exchanger		1.242e+004 *				3.982		1 *		1.644e+005					
46	Condenser@DC-101		7.789e+005 *				3290		7 *		2.344e+007					
47	Reboiler@DC-103		2.646e+004 *				43.81		1 *		1.687e+006					
48	Condenser@DC-102		2.373e+004 *				34.93		1 *		7.950e+005					
49	R-103_heat_Exchanger		1.028e+004 *				0.2689		1 *		1277					
50	Total		2.345e+006 *				3582 *		22 *		5.245e+007 *					
51	Utilities															
52																
53	Utility		Type		Cost Index (Cost/s)				Load (kJ/h)				% of Target			
54																
55	Air		COLD		6.945e-006 *				2.500e+007 *				100.4 *			
56	MP Steam Generation		COLD		-4.836e-004 *				7.950e+005 *				*** *			
57	Cooling Water		COLD		7.538e-008 *				1277 *				37.83 *			
58	HP Steam		HOT		5.146e-004 *				7.410e+005 *				*** *			
59	Very High Temperature		HOT		5.894e-002 *				2.384e+007 *				100.0 *			
60	MP Steam		HOT		1.031e-003 *				1.687e+006 *				109.7 *			
61	Total				6.001e-002 *				---				---			
62	WorkSheet															
63																
64																
65	Heat Exchanger	Cold Stream	Cold T in (C)	Tied	Cold T out (C)	Tied	Hot Stream	Hot T in (C)	Tied	Hot T out (C)	Tied	Load (kJ/h)	Area (m2)	Status	dT Min Hot	dT Min Cold
66																
67	HE-102	S7_To_S9	122.1	T	190.0	T	HP Steam	250.0		249.0		3.420e+005	0.7	OK	60.00	126.9
68	Condenser@DC-103	Air	30.00		35.00		Condenser@DC-103_TO_S20	56.25	T	55.75	T	1.566e+006	168.6	OK	21.25	25.75
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15	Heat Exchanger	Cold Stream	Cold T in (C)	Tied	Cold T out (C)	Tied	Hot Stream	Hot T in (C)	Tied	Hot T out (C)	Tied	Load (kJ/h)	Area (m2)	Status	dT Min Hot	dT Min Cold
16	STHE-101	S2_To_S4	28.13	T	63.68	T	S33_To_S34	210.9	T	30.00	T	5.084e+004	0.9	OK	147.3	1.867
17	Reboiler@DC-101	Reboiler@DC-101_TO_S24	419.8	T	420.3	T	Very High Temperature	3000		2999		2.313e+007	34.9	OK	2580	2579
18	102_heat_Exchanger	R-102_heat	190.0	T	190.5	T	HP Steam	250.0		249.0		5.403e+004	1.3	OK	59.50	59.00
19	HE-101	S2_To_S4	63.68	T	190.0	T	HP Steam	250.0		249.0		1.807e+005	0.6	OK	60.00	185.3
20	STHE-102	S7_To_S9	28.60	T	122.1	T	S28_To_S29	425.7	T	190.0	T	3.245e+005	0.7	OK	303.6	161.4
21	Reboiler@DC-102	Reboiler@DC-102_TO_S26	425.1	T	425.6	T	Very High Temperature	3000		2999		7.178e+005	1.1	OK	2574	2574
22	101_heat_Exchanger	R-101_heat	190.0	T	190.5	T	HP Steam	250.0		249.0		1.644e+005	4.0	OK	59.50	59.00
23	Condenser@DC-101	Air	30.00		35.00		Condenser@DC-101_TO_S17	60.55	T	60.05	T	2.344e+007	3289.9	OK	25.55	30.05
24	Reboiler@DC-103	Reboiler@DC-103_TO_S22	119.0	T	119.5	T	MP Steam	175.0		174.0		1.687e+006	43.8	OK	55.52	55.02
25	Condenser@DC-102	MP Steam Generation	174.0		175.0		Condenser@DC-102_TO_S31	207.4	T	206.9	T	7.950e+005	34.9	OK	32.42	32.92
26	103_heat_Exchanger	Cooling Water	20.00		25.00		R-103_heat	30.00	T	29.50	T	1277	0.3	OK	5.000	9.500
27																
28	Heat Exchangers															
29																
30																
31	Summary															
32																
33	ALL HEAT EXCHANGERS															
34																
35	Heat Exchanger	Load (kJ/h)	Cost	Area (m2)	Shells	LMTD (C)	HTC (kJ/h-m2-C)	F Factor	Fouling							
36	HE-102	3.420e+005	1.062e+004 *	0.7219	1 *	89.30	5419	0.9985	0.0000 *							
37	Condenser@DC-103	1.566e+006	5.837e+004 *	168.6	1 *	23.43	396.8	0.9992	0.0000 *							
38	STHE-101	5.084e+004	1.096e+004 *	0.8863	4 *	33.29	1805	0.8914	0.0000 *							
39	Reboiler@DC-101	2.313e+007	1.212e+006 *	34.89	1 *	2579	257.0	1.000	0.0000 *							
40	R-102_heat_Exchanger	5.403e+004	1.099e+004 *	1.309	1 *	59.25	696.8	1.000	0.0000 *							
41	HE-101	1.807e+005	1.055e+004 *	0.6196	1 *	111.1	2629	0.9982	0.0000 *							
42	STHE-102	3.245e+005	1.058e+004 *	0.6662	1 *	225.1	2261	0.9209	0.0000 *							
43	Reboiler@DC-102	7.178e+005	1.691e+005 *	1.085	1 *	2574	257.0	1.000	0.0000 *							
44	R-101_heat_Exchanger	1.644e+005	1.242e+004 *	3.982	1 *	59.25	696.8	1.000	0.0000 *							
45	Condenser@DC-101	2.344e+007	7.789e+005 *	3290	7 *	27.74	257.0	0.9995	0.0000 *							
46	Reboiler@DC-103	1.687e+006	2.646e+004 *	43.81	1 *	55.27	696.8	1.000	0.0000 *							
47	Condenser@DC-102	7.950e+005	2.373e+004 *	34.93	1 *	32.67	696.8	0.9999	0.0000 *							
48	R-103_heat_Exchanger	1277	1.028e+004 *	0.2689	1 *	7.011	683.5	0.9913	0.0000 *							
49	All Heat Exchangers (Continued)															
50	Heat Exchanger	Hot Stream	Hot T in (C)	Hot T out (C)	Cold Stream	Cold T in (C)	Cold T out (C)	dT Min Hot (C)	dT Min Cold (C)							
51	HE-102	HP Steam	250.0	249.0	S7_To_S9	122.1	190.0	60.00	126.9							
52	Condenser@DC-103	To Condenser@DC-103_TO_S20	56.25	55.75	Air	30.00	35.00	21.25	25.75							
53	STHE-101	S33_To_S34	210.9	30.00	S2_To_S4	28.13	63.68	147.3	1.867							
54	Reboiler@DC-101	Very High Temperature	3000	2999	To Reboiler@DC-101_TO_S24	419.8	420.3	2580	2579							
55	R-102_heat_Exchanger	HP Steam	250.0	249.0	R-102_heat	190.0	190.5	59.50	59.00							
56	HE-101	HP Steam	250.0	249.0	S2_To_S4	63.68	190.0	60.00	185.3							
57	STHE-102	S28_To_S29	425.7	190.0	S7_To_S9	28.60	122.1	303.6	161.4							
58	Reboiler@DC-102	Very High Temperature	3000	2999	To Reboiler@DC-102_TO_S26	425.1	425.6	2574	2574							
59	R-101_heat_Exchanger	HP Steam	250.0	249.0	R-101_heat	190.0	190.5	59.50	59.00							
60	Condenser@DC-101	To Condenser@DC-101_TO_S17	60.55	60.05	Air	30.00	35.00	25.55	30.05							
61	Reboiler@DC-103	MP Steam	175.0	174.0	To Reboiler@DC-103_TO_S22	119.0	119.5	55.52	55.02							
62	Condenser@DC-102	To Condenser@DC-102_TO_S31	207.4	206.9	MP Steam Generation	174.0	175.0	32.42	32.92							
63	R-103_heat_Exchanger	R-103_heat	30.00	29.50	Cooling Water	20.00	25.00	5.000	9.500							
64																
65																
66																
67																
68																
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Company Name Not Available

Bedford, MA

USA

Case Name: GamVet From LEVULINIC ACID and ISOPROPANOL -Double Series R4

Unit Set: SI

Date/Time: Sat Jul 22 12:30:17 2023

HI Design Datasheet

APLUS_Import

Scenario 1

SimulationBaseCase

Heat Exchangers

Summary

HEAT EXCHANGERS FOR STREAM: R-102_heat

Heat Exchanger	Load (kJ/h)	Cost Index (Cost)	Area (m2)	Shells	LMTD (C)	HTC (kJ/h-m2-C)	T in (C)	T out (C)	Matched With
R-102_heat_Exchanger	5.403e+004 *	1.099e+004 *	1.309 *	1 *	59.25 *	696.8 *	190.0 *	190.5 *	HP Steam

DRIVING FORCE PLOT

Driving Force Plot

Targets

Heating	2.538e+007 kJ/h *	Operating Cost Index	5.989e-002 Cost/s *
Cooling	2.491e+007 kJ/h *	Capital Cost Index	2.093e+006 Cost *
Number of Units	16 *	Total Cost Index	7.740e-002 Cost/s *
Total Area	3553 m2 *		

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Licensed to: Company Name Not Available

Specified by user.

1	Company Name Not Available Bedford, MA USA			Case Name:		GamVet From LEVULINIC ACID and ISOPROPANOL -Double Series R	
2				Unit Set:		SI	
3				Date/Time:		Sat Jul 22 12:30:17 2023	
4							
5							
6	HI Design Datasheet						
7							
8	APLUS_Import						
9	Scenario 1						
10	SimulationBaseCase						
11							
12	Topology Data						
13							
14							
15	Sub-Networks						
16							
17	Number of Sub-Networks		11		*		
18	Network Number		Streams in Network				
19	1	*	S7_To_S9				
20			S28_To_S29				
21	2	*	S2_To_S4				
22			S33_To_S34				
23	3	*	To Condenser@DC-101_TO_S17				
24	4	*	To Condenser@DC-102_TO_S31				
25	5	*	To Condenser@DC-103_TO_S20				
26	6	*	R-102_heat				
27	7	*	R-103_heat				
28	8	*	R-101_heat				
29	9	*	To Reboiler@DC-102_TO_S26				
30	10	*	To Reboiler@DC-103_TO_S22				
31	11	*	To Reboiler@DC-101_TO_S24				
32	Loops						
33							
34	Independant Loops:		0		*		Dependant Loops: 0 *
35	Loop Number		Exchangers in Loop				
36							
37	Paths						
38							
39	Path Number	Hot Utility		Heat Exchangers in Path			Cold Utility
40							
41	Utilities						
42							
43	Utilities in Design				Utility Included in Searches for Sub-Nets, Loops and Paths		
44	Air				Not Included		
45	MP Steam Generation				Not Included		
46	Cooling Water				Not Included		
47	HP Steam				Not Included		
48	Very High Temperature				Not Included		
49	MP Steam				Not Included		
50	Notes						
51							
52							
53	Design Notes						
54							
55							
56							
57	Modification Log						
58							
59	Heat exchanger STHE-101 is added by data extraction module;Heat exchanger STHE-102 is added by data extraction module;Cooler Condenser@DC-103 is added by data extraction module;Cooler Condenser@DC-101 is added by data extraction module;Cooler Condenser@DC-						
60							
61	Grid Design						
62							
63							
64	Infeasible HX: 0, HX Not Calculated: 0Unsatisfied Streams: 0						
65	Cross Pinch						
66							
67	Pinch		429.80 C / 419.80 C		425.73 C / 415.73 C		60.55 C / 50.55 C 38.13 C / 28.13 C
68	Network Cross Pinch Load (kJ/h)		0.0000 *		0.0000 *		8.898e+005 * 7.929e+005 *
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5							
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7							
8	APLUS_Import						
9	Scenario 1						
10	SimulationBaseCase						
11							
12	Grid Design						
13							
14							
15	Cross Pinch						
16							
17	HE-102	(kJ/h)	0.0000 *	0.0000 *	0.0000 *	0.0000 *	
18	Condenser@DC-103	(kJ/h)	0.0000 *	0.0000 *	0.0000 *	0.0000 *	
19	STHE-101	(kJ/h)	0.0000 *	0.0000 *	2.417e+004 *	-2100 *	
20	Reboiler@DC-101	(kJ/h)	0.0000 *	0.0000 *	0.0000 *	0.0000 *	
21	R-102_heat_Exchanger	(kJ/h)	0.0000 *	0.0000 *	0.0000 *	0.0000 *	
22	HE-101	(kJ/h)	0.0000 *	0.0000 *	0.0000 *	0.0000 *	
23	STHE-102	(kJ/h)	0.0000 *	0.0000 *	7.061e+004 *	0.0000 *	
24	Reboiler@DC-102	(kJ/h)	0.0000 *	0.0000 *	0.0000 *	0.0000 *	
25	R-101_heat_Exchanger	(kJ/h)	0.0000 *	0.0000 *	0.0000 *	0.0000 *	
26	Condenser@DC-101	(kJ/h)	0.0000 *	0.0000 *	0.0000 *	0.0000 *	
27	Reboiler@DC-103	(kJ/h)	0.0000 *	0.0000 *	0.0000 *	0.0000 *	
28	Condenser@DC-102	(kJ/h)	0.0000 *	0.0000 *	7.950e+005 *	7.950e+005 *	
29	R-103_heat_Exchanger	(kJ/h)	0.0000 *	0.0000 *	0.0000 *	0.0000 *	
30	Heat Exchanger Status						
31							
32	Degrees of Freedom: 0						
33	Heat Exchangers			Status			
34							
35							
36							
37							
38							
39							
40							
41							
42							
43							
44							
45							
46							
47	Stream Load Status						
48							
49	Streams		Type	Unsatisfied	% of Total	Total	
50							
51	Network Heating						
52							
53	Utility	Type	Cost Index	Load	% of Target		
54			(Cost/s)	(kJ/h)			
55	HP Steam	HOT	5.146e-004 *	7.410e+005 *	*** *		
56	MP Steam	HOT	1.031e-003 *	1.687e+006 *	109.7 *		
57	Very High Temperature	HOT	5.894e-002 *	2.384e+007 *	100.0 *		
58	Total		6.049e-002 *	2.627e+007 *	103.5 *		
59	Network Cooling						
60							
61	Utility	Type	Cost Index	Load	% of Target		
62			(Cost/s)	(kJ/h)			
63	MP Steam Generation	COLD	-4.836e-004 *	7.950e+005 *	*** *		
64	Cooling Water	COLD	7.538e-008 *	1277 *	37.83 *		
65	Air	COLD	6.945e-006 *	2.500e+007 *	100.4 *		
66	Total		-4.766e-004 *	2.580e+007 *	103.6 *		
67							
68							
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