Radiation-Driven Flame Extinction in Fires

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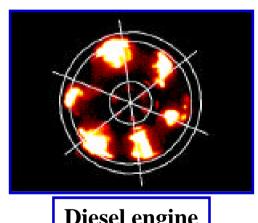


Motivation:

- Combustion science
 - Flame extinction has a significant impact on the performance of nonpremixed combustion systems. It determines in part the turbulent flame structure and the levels of pollutant emission (NOx, CO, soot).

> Engine applications

• Extinction due to high turbulence intensities in IC- or gas-turbine engines (momentumdriven, high-Reynolds number flames)



Diesel engine



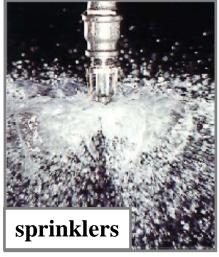
Motivation:

> Fire applications

• Extinction due to air vitiation in underventilated compartment fires or large-scale pool fires (buoyancy-driven, moderate-Reynolds number flames)

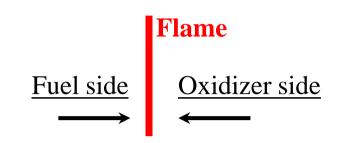


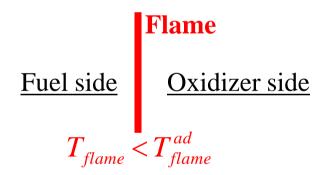
• Extinction due to inert gaseous agents or water sprays in fire suppression applications





- Different flame extinction phenomena:
 - Aerodynamic quenching: flame weakening due to flow-induced perturbations (i.e. decrease in flame residence time)
 - ➤ Thermal quenching: flame weakening due to heat losses (e.g. heat losses by convection/conduction to walls, by thermal radiation, by water evaporative cooling in fire suppression applications)
 - ➤ Quenching by dilution: flame weakening due to changes in fuel stream or oxidizer stream composition (e.g. air vitiation in under-ventilated fires)





Flame

Fuel side $Y_F < 1$ Oxidizer side $Y_{O_2} < Y_{O_{2,a}}$

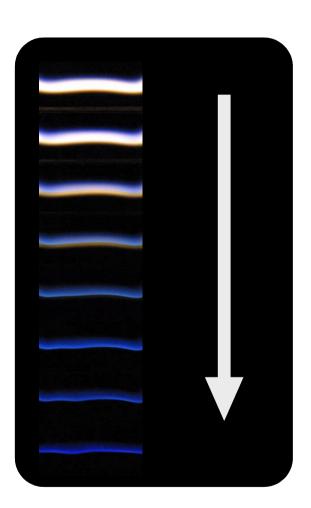


- Different flame extinction phenomena:
 - > Single criterion to predict extinction (laminar flame theory):

$$Da = \frac{\tau_{mixing}}{\tau_{chemical}} \le Da_{critical}$$

$$Da = \frac{\tau_{mixing}}{\tau_{chemical}} \sim \frac{(1/\chi_{st})}{\exp(T_a/T_{st})}$$

- > Two fundamental limits:
 - Fast mixing limit: Da is small because χ_{st} is large (e.g., aerodynamic quenching)
 - Slow mixing limit: Da is small because T_{st} is small (e.g., thermal or dilution quenching)

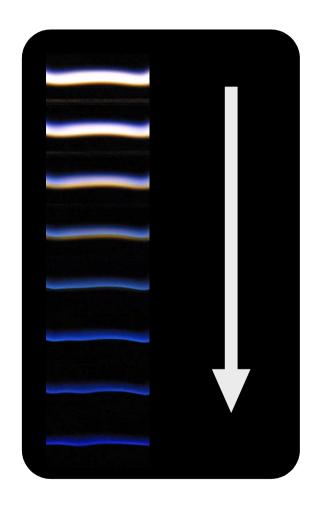




- Different flame extinction phenomena:
 - Fast mixing limit: also called kinetic extinction
 - Criterion for extinction:

$$\chi_{st} \geq \chi_{critical}$$

- **Sources**: aerodynamic quenching
 - Liñán (1974) Acta Astronautica
 - Williams (1985) "Combustion Theory"
 - Peters (2000) "Turbulent Combustion"



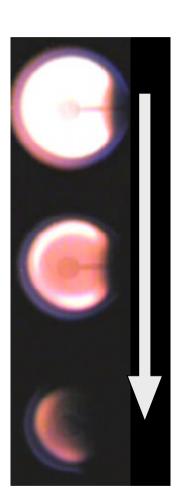


- Different flame extinction phenomena:
 - ➤ Slow mixing limit: also called *radiation* extinction
 - Criterion for extinction:

$$\Gamma_{rad} \ge \Gamma_{critical}$$

$$\chi_{st} \leq \chi_{critical}^*$$

- Sources: thermal quenching in microgravity combustion
 - Sohrab, Liñán & Williams (1982)
 Combustion Science and Technology
 - T'ien (1986) Combustion and Flame
 - Chao, Law & T'ien (1990) Proceedings Combustion Institute 23
 - Bedir & T'ien (1998) Combustion and Flame

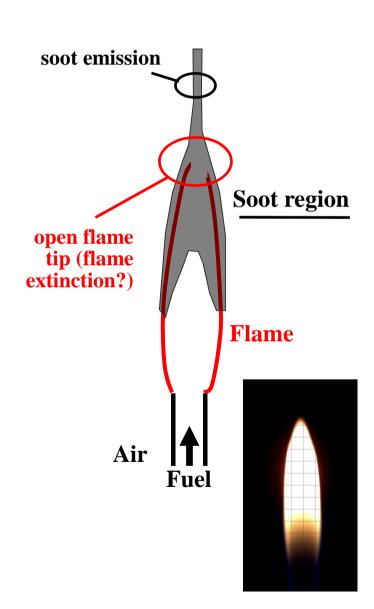




- Relation between radiation extinction and soot emission/smoke point studies:
 - ➤ Unclear: many recent studies of radiation extinction correspond to one-dimensional flames that are soot-free at the extinction limit
 - ➤ But: past studies of the smoke point (SP) of laminar jet diffusion flames suggest that SP is controlled by the flame luminosity; hence, SP may be interpreted as a radiation extinction event

Source:

• Markstein, de Ris (1984) *Proceedings* Combustion Symposium



Objectives



- Study mechanisms responsible for diffusion flame extinction in laminar and turbulent flames (focus on conditions relevant to fire applications)
 - > Establish flame extinction criterion; construct flammability map(s)
- Tools:
 - Asymptotic analysis of extinction limits of laminar counter-flow diffusion flames exposed to different levels of radiant losses
 - ➤ Direct Numerical Simulations (DNS) of laminar counter-flow and coflow diffusion flames, and of turbulent diffusion flames

Explore relationship between flame extinction and soo emission





Numerical approach



- Use direct numerical simulation (DNS)
 - ➤ Leverage DOE-sponsored SciDAC collaboration on DNS solver called S3D Sandia Ntl. Laboratories (J.H. Chen), Univ. Michigan (H.G. Im)
- DNS solver S3D
 - ➤ Navier-Stokes solver; fully compressible flow formulation
 - ➤ High-order methods: 8th order finite difference; 4th order explicit Runge-Kutta time integrator
 - Characteristic-based boundary condition treatment (NSCBC)
 - Structured Cartesian grids
 - Parallel (MPI-based, excellent scalability)
 - Flame modeling: detailed fuel-air chemistry (CHEMKIN-compatible); simplified soot formation model; thermal radiation model (Discrete Ordinate/Discrete Transfer Methods); Lagrangian particle model to describe dilute liquid sprays

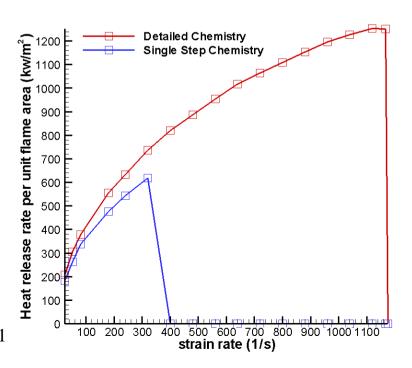
Flame Modeling

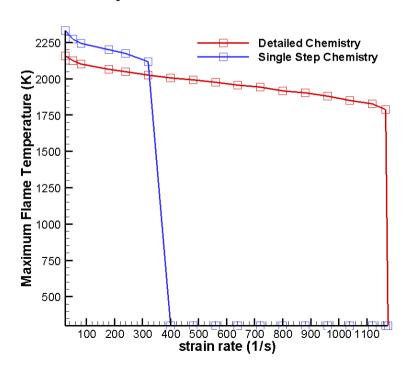


• Combustion model: single-step chemistry, ethylene-air combustion (Westbrook & Dryer, 1981)

$$\dot{\omega}_F = B_{RR} \left(\frac{\rho Y_F}{M_F}\right)^p \left(\frac{\rho Y_{O_2}}{M_F}\right)^q \exp(-\frac{T_a}{T})$$

➤ Counter-flow flame: comparison of laminar flame response to changes in strain rate for single-step and detailed chemistry





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Flame Modeling



- **Soot formation model:** a phenomenological approach (Moss *et al.*, Lindstedt *et al.*)
 - Two-variable model; empirical description of fundamental soot formation processes (nucleation, surface growth, coagulation, oxidation)
 - Model parameters are fuel-dependent
 - ➤ No PAH chemistry
 - Monodispersed soot particle size distribution

$$\frac{\partial}{\partial t}(\rho Y_{soot}) + \frac{\partial}{\partial x_{i}}(\rho u_{i}Y_{soot}) = -\frac{\partial}{\partial x_{i}}(\rho Y_{soot}V_{t,i}) + \frac{\partial}{\partial x_{j}}(\frac{\mu}{Sc}\frac{\partial Y_{soot}}{\partial x_{j}}) + \frac{\dot{\omega}'''_{s,nucleation}}{\dot{\omega}_{s,nucleation}} + \frac{\dot{\omega}'''_{s,surface}}{\dot{\omega}_{s,oxidation}} - \frac{\dot{\omega}'''_{s,oxidation}}{\dot{\omega}_{s,oxidation}}$$

$$\frac{\partial}{\partial t}(\frac{n_{soot}}{N_{A}}) + \frac{\partial}{\partial x_{i}}(u_{i}\frac{n_{soot}}{N_{A}}) = -\frac{\partial}{\partial x_{i}}(\frac{n_{soot}}{N_{A}}V_{t,i}) + \frac{\partial}{\partial x_{j}}(\frac{\mu}{\rho Sc}\frac{\partial}{\partial x_{j}}(\frac{n_{soot}}{N_{A}})) + \frac{\dot{\omega}'''_{n,nucleation}}{\dot{\omega}_{n,nucleation}} - \frac{\dot{\omega}'''_{n,nucleation}}{\dot{\omega}_{n,nucleation}}$$

Flame Modeling

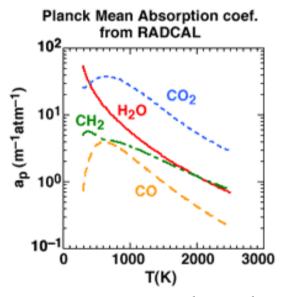


- Thermal radiation transport model: non-scattering, gray gas assumption; Discrete Transfer Method (Lockwood & Shah, 1981)
 - ➤ Radiative transfer equation

$$\frac{dI}{ds} = \underbrace{\kappa(\sigma T^4/\pi)}_{\text{Emission}} - \underbrace{\kappa I}_{\text{Absorption}}$$

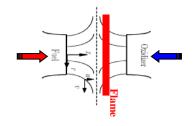
Mean absorption coefficient [m⁻¹]

$$\kappa = p(x_{H_2O}a_{H_2O} + x_{CO_2}a_{CO_2}) + \kappa_{soot}$$



- $a_{p,i}$ is the Planck mean absorption coefficient for species i [m⁻¹ atm⁻¹] and is obtained from tabulated data (TNF Workshop web site)
- κ_{soot} is the soot mean absorption coefficient [m⁻¹]

$$\kappa_{soot} = C_{soot} \times f_v T = C_{soot} \times (\rho Y_{soot} / \rho_{soot}) T \rightarrow C_{soot} = 1817 \,\mathrm{m}^{-1} \mathrm{K}^{-1}$$





- Classical activation energy asymptotic (AEA) analysis
 - Mass density variations handled with Howarth transformation $\xi = \int_0^x (\rho/\rho_2) dx$
 - \triangleright Mixture fraction equation and solution (α is strain rate)

$$-\alpha \xi \frac{dZ}{d\xi} = D_2 \frac{d^2 Z}{d\xi^2}$$

$$\Rightarrow Z = \frac{1}{2} - \frac{1}{2} \operatorname{erf}\left(\frac{\xi}{\sqrt{2D_2/\alpha}}\right)$$

> Flame structure given by flamelet equations (in mixture fraction space)

$$-\frac{\chi_{st}}{2}\frac{d^2T}{dZ^2} = \left(\frac{\Delta H_F}{c_p}\right)\frac{\dot{\omega}_F}{\rho_{st}}$$



- Classical decomposition into inner/outer layers
 - \triangleright Perform asymptotic expansion in terms of small parameter ε

$$\varepsilon = \frac{1}{Ze} = \frac{(T_{st})^2}{T_a} (\frac{c_p}{\Delta H_F Y_{F,1}})$$

> Inner layer problem

$$T = T_{st} - \varepsilon \theta \left(\frac{\Delta H_F Y_{F,1}}{c_p}\right) + O(\varepsilon^2) \; ; \; Z = Z_{st} + \varepsilon \zeta + O(\varepsilon^2)$$

$$\frac{d^2 \theta}{d\zeta^2} = \delta [\theta + \zeta]^p \left[\theta - \frac{Z_{st} \zeta}{(1 - Z_{st})}\right]^q \exp(-\theta) \qquad (\delta \text{ is a reduced Damkohler number})$$

$$(d\theta / d\zeta)_{\zeta \to -\infty} = -1 \; ; \; (d\theta / d\zeta)_{\zeta \to +\infty} = Z_{st} / (1 - Z_{st})$$



- AEA flame structure with thermal radiation
 - > Temperature decomposition (outer layer problem)

$$T = T_{BS}^{ad} - \Delta T$$

➤ Governing equation for temperature deficit due to radiant cooling

$$\alpha \xi \frac{d}{d\xi} (\Delta T) = -D_2 \frac{d^2}{d\xi^2} (\Delta T) - \frac{\dot{q}_{rad}}{\rho c_p}$$

Green's function solution

$$\Delta T(\xi) = \int_{-\infty}^{+\infty} \frac{\dot{q}_{rad}}{\rho c_p} (\xi^*) g(\xi, \xi^*) d\xi^*$$

Consider that chemical reaction zone is thin compared to characteristic radiation length scale ($\kappa \delta_{reaction}$) << 1): inner layer problem is essentially unchanged



- AEA flame structure with thermal radiation
 - > Green's function solution

$$\Delta T(\xi) = \int_{-\infty}^{+\infty} \frac{\dot{q}_{rad}}{\rho c_p}(\xi^*) g(\xi, \xi^*) d\xi^*$$

Emitting/absorbing medium (spectrally-averaged gray)

$$\dot{q}_{rad} = \kappa (4\sigma T^4 - G)$$

Planck mean aborption coefficient:

$$\kappa = p(x_{CO_2}a_{CO_2} + x_{H_2O}a_{H_2O}) + C_{soot} \times f_v T$$

Analytical expression for G (as a function of optical depth τ):

$$\begin{split} G &= 2\pi [I_{b,1} E_2(\tau) + I_{b,2} E_2(\tau_R - \tau) \\ &+ \int_0^\tau I_b(\tau') E_1(\tau - \tau') d\tau' + \int_\tau^{\tau_R} I_b(\tau') E_1(\tau' - \tau) d\tau'] \end{split}$$



- AEA flame structure with soot
 - Two-equations model for ssot mass fraction and soot number density (Moss *et al.*, Lindstedt *et al.*)

$$(-\alpha\xi + \overline{V_t}) \frac{dY_{soot}}{d\xi} + \frac{d\overline{V_t}}{d\xi} Y_{soot} = \frac{\dot{\omega}_{Y_{soot}}}{\rho}$$

$$(-\alpha\xi + \overline{V_t}) \frac{d}{d\xi} (\frac{n_{soot}}{\rho N_A}) + \frac{d\overline{V_t}}{d\xi} (\frac{n_{soot}}{\rho N_A}) = \frac{\dot{\omega}_{n_{soot}}}{\rho}$$

 \triangleright Soot formation and oxidation rates (C_2H_2 -air combustion)

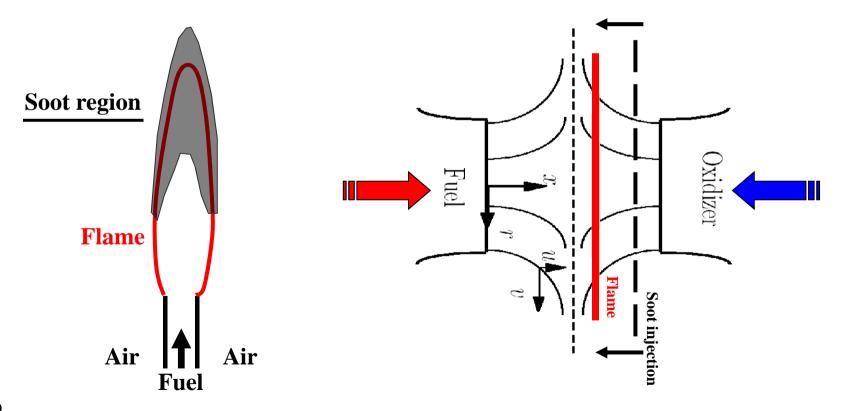
$$\dot{\omega}_{Y_{soot}} = c_{\alpha}(\rho^{2}\sqrt{T}X_{F})\exp(-\frac{T_{\alpha}}{T}) + c_{\gamma}(\rho\sqrt{T}X_{F})\exp(-\frac{T_{\gamma}}{T}) \times n_{soot}$$

$$-c_{o}(\frac{X_{O_{2}}}{\sqrt{T}})\exp(-\frac{T_{o}}{T}) \times (\rho Y_{soot})^{2/3}n_{soot}^{1/3}$$

$$\dot{\omega}_{n_{soot}} = c_{\delta}c_{\alpha}(\rho^{2}\sqrt{T}X_{F})\exp(-\frac{T_{\alpha}}{T}) - c_{\beta}\sqrt{T} \times (\frac{n_{soot}}{N_{A}})^{2}$$

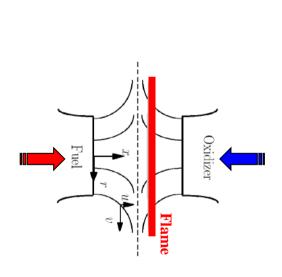


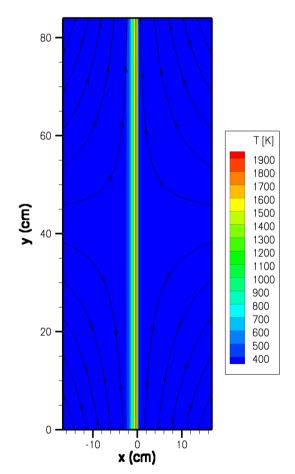
- AEA flame structure with soot
 - External soot loading: a mechanism to simulate non-local effects observed in multi-dimensional flames in a one-dimensional framework
 - > Soot loading from the flame air side





- Reference counter-flow diffusion flame configuration
 - Flamelet perspective: steady flame structure obtained as a function of flame stretch, ranging from ultra-high to ultra-low values

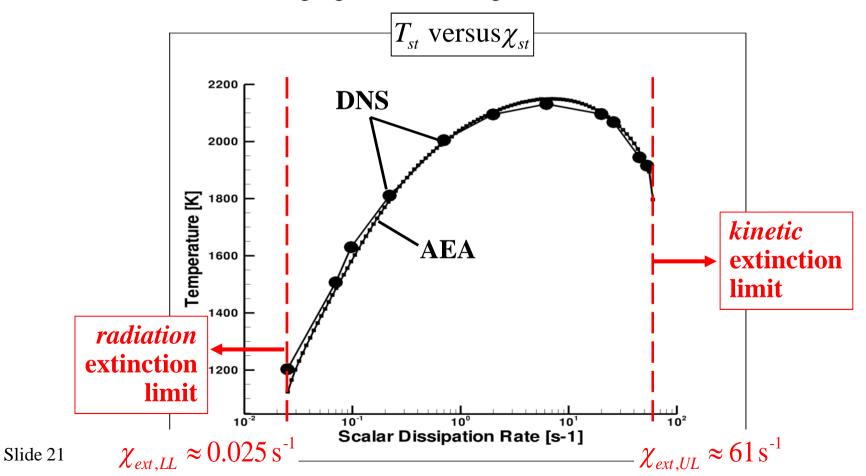




 $\Delta x = 60 \ \mu \text{m}$ variable Δy

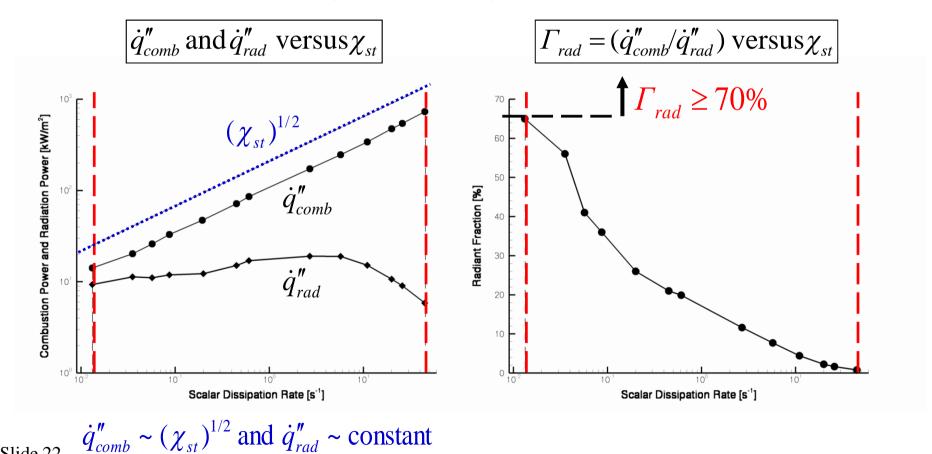


- Reference counter-flow flame configuration
 - Flamelet database: steady flame structure obtained as a function of flame stretch, ranging from ultra-high to ultra-low values





- Reference counter-flow flame configuration
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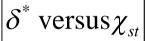
• Extinction limits: correspond to critical value of Damköhler number

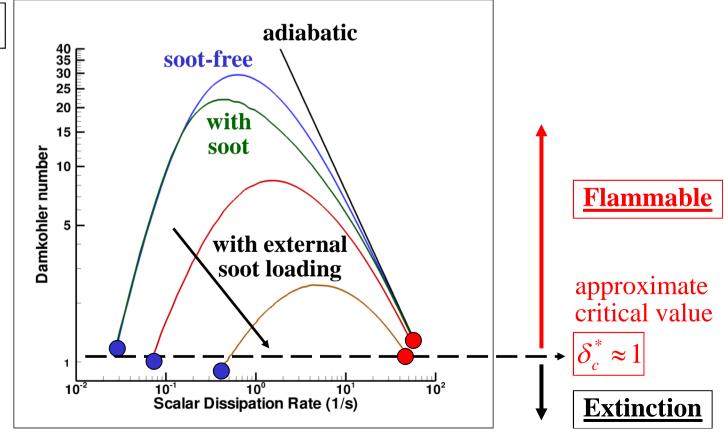
$$\delta^* = \frac{8\rho_{st}^{(p+q-1)}Y_{F,1}^{(p+q-1)}r_s^q A \exp(-T_a/T_{st})}{(1+b)^2(10^6)^{p+q-1}M_F^{(p-1)}M_{O_2}^q \chi_{st} Ze^{(p+q+1)}} \le \delta_c^*$$



Extinction limits: correspond to critical value of Damköhler number

$$\delta^* = \frac{8\rho_{st}^{(p+q-1)}Y_{F,1}^{(p+q-1)}r_s^q A \exp(-T_a/T_{st})}{(1+b)^2(10^6)^{p+q-1}M_F^{(p-1)}M_{O_2}^q \chi_{st} Ze^{(p+q+1)}} \le \delta_c^*$$

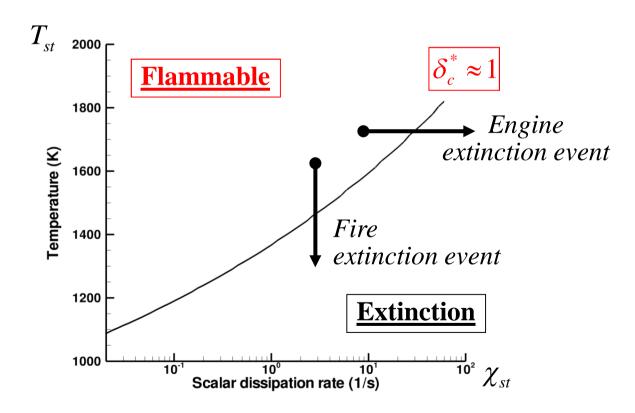






Extinction limits

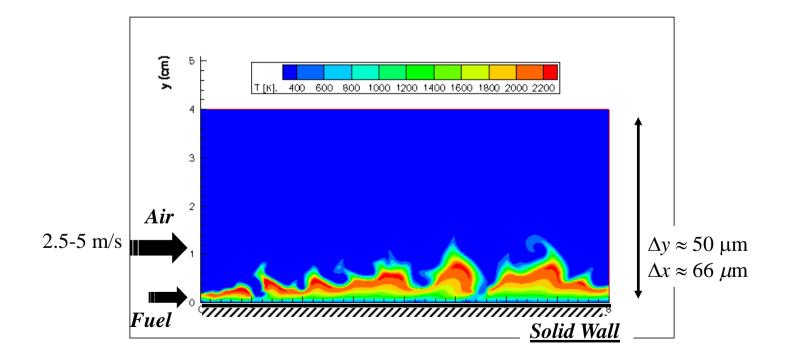
Flammability map with mixing rate and fuel-air flame temperature as coordinates



Turbulent Wall-Jet Flames



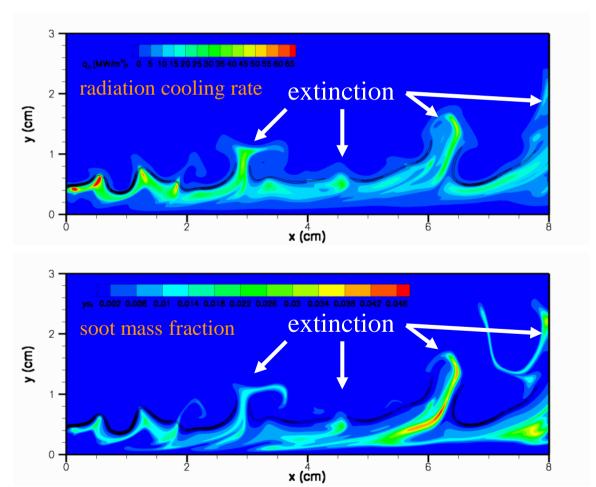
- Simplified turbulent flame configuration
 - > Two-dimensional (8×4 cm²); grid size: 1216×376 (uniform×stretched); prescribed inflow turbulent fluctuations (u'=1-2.5 m/s; $L_t=1.7 \text{ mm}$)



Turbulent Wall-Jet Flames



• Analysis of flame structure (case: $T_w = 300$ K; $\delta = 0.5$ cm; with soot/radiation; $C_{soot} = 7000$ m⁻¹K⁻¹)



Observations:

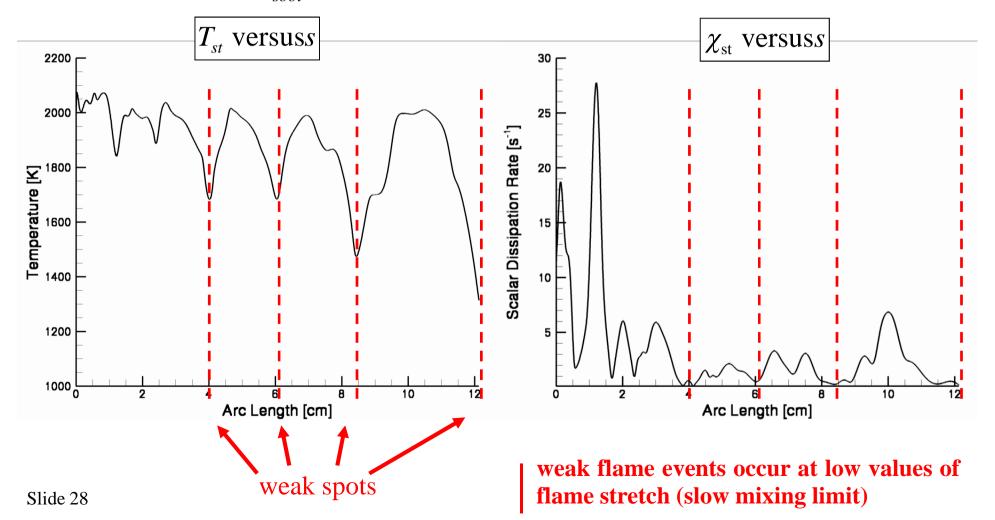
- radiative cooling region is not thin
- soot region is not thin
- Weak flame events correlated with soot mass leakage across the flame

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Turbulent Wall-Jet Flames



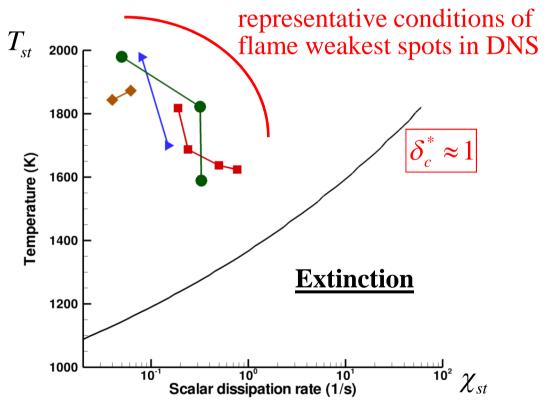
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Extinction limits

Flammability map with mixing rate and fuel-air flame temperature as coordinates

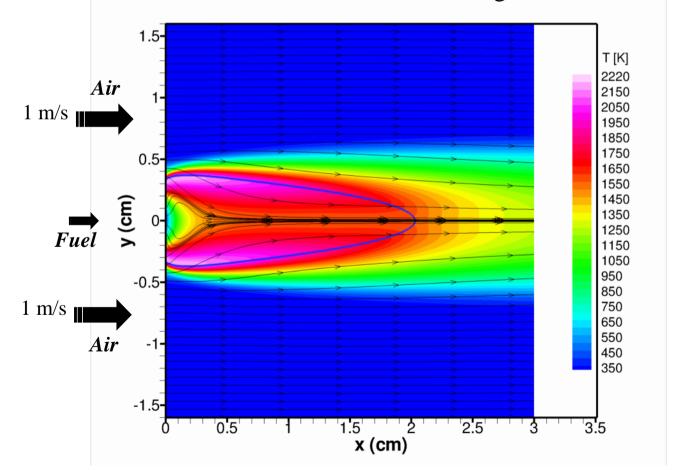


Flame weakest spots (e.g., locations that show soot mass leakage) correspond to weak burning conditions, not flame extinction

Laminar Co-Flow Flames



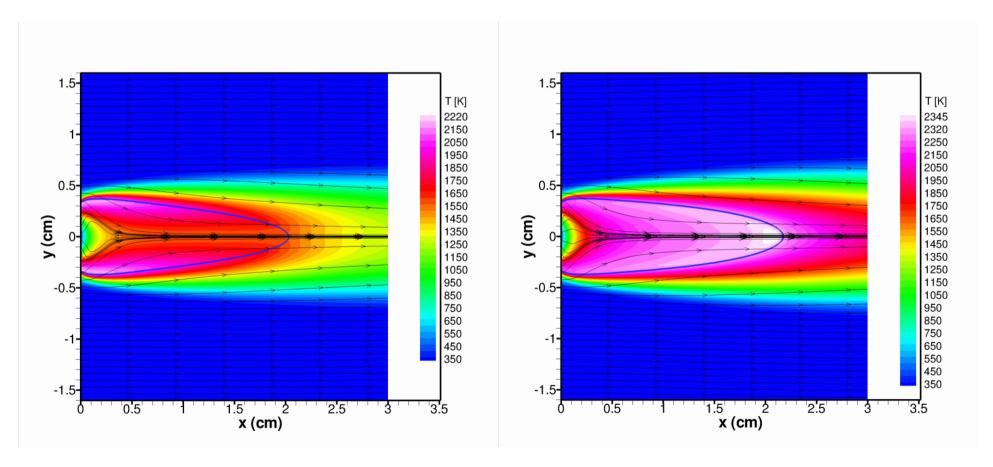
- Simplified laminar flame configuration
 - ➤ High air co-flow velocity, diffusive-driven incoming fuel stream, zero-g
 - ➤ Recirculation zone close to fuel surface, long residence times



Laminar Co-Flow Flames



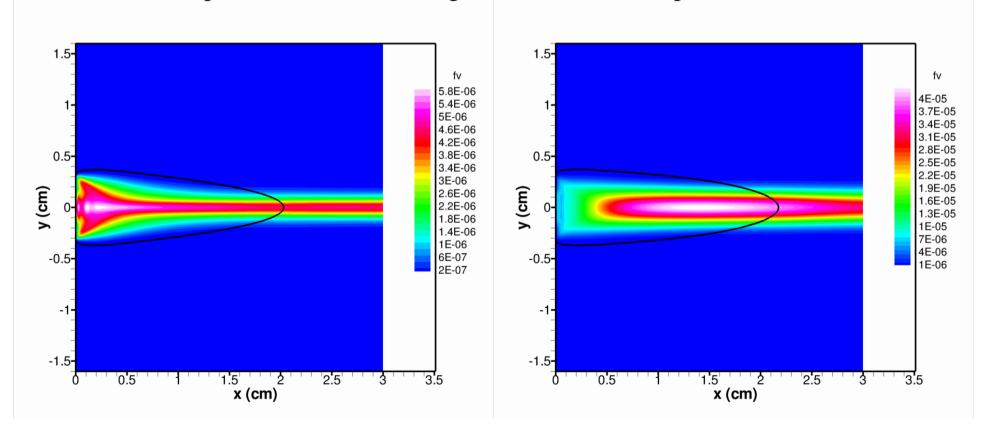
- Simplified laminar flame configuration
 - Comparison between solutions with (left) and without radiation (right)
 - > Flame tip temperatures differ by more than 700 K



Laminar Co-Flow Flames



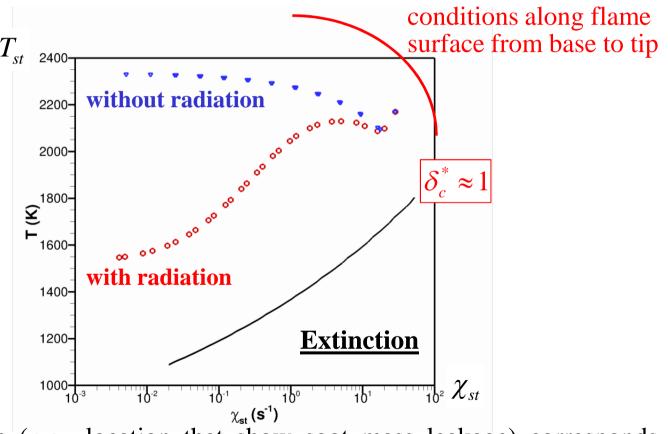
- Simplified laminar flame configuration
 - Comparison between solutions with (left) and without radiation (right)
 - ➤ Both flames feature both large amounts of soot within the flame envelope and soot mass leakage across the flame tip





Extinction limits

> Flammability map with flame temperature and mixing rate as coordinates



Flame tip (e.g., location that show soot mass leakage) corresponds to weak burning conditions, not flame extinction

Conclusions

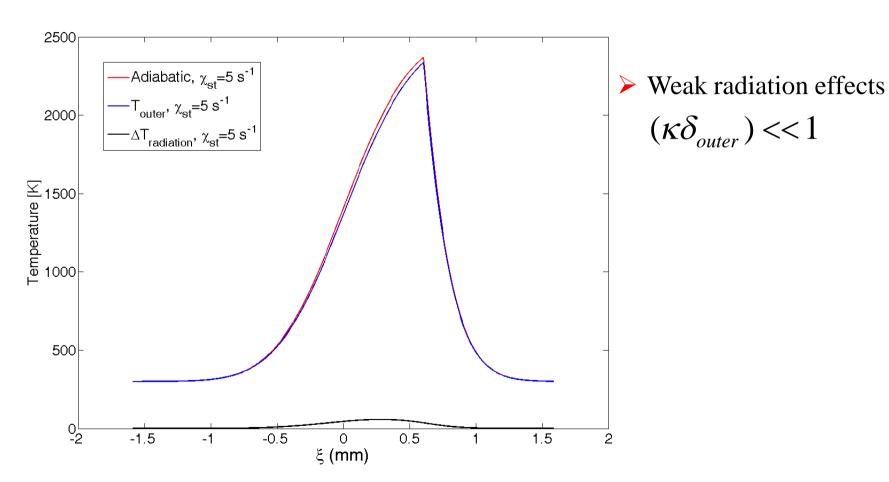


- AEA theory and DNS are used to make fundamental observations of extinction phenomena in non-adiabatic turbulent diffusion flames
- In laminar counter-flow flames, two different sets of flame extinction conditions are observed:
 - Kinetic extinction occurring under fast mixing conditions
 - > Radiation extinction occurring under slow mixing conditions
- These 2 different modes correspond to the same extinction limit:
 - AEA analysis suggests that all extinction limits may be described by a single criterion corresponding to a critical value of the Damköhler number
 - > Soot has a significant impact on the extinction limit
- In laminar co-flow flames and in turbulent flames, it is found that soot mass leakage events do not correspond to radiation extinction events



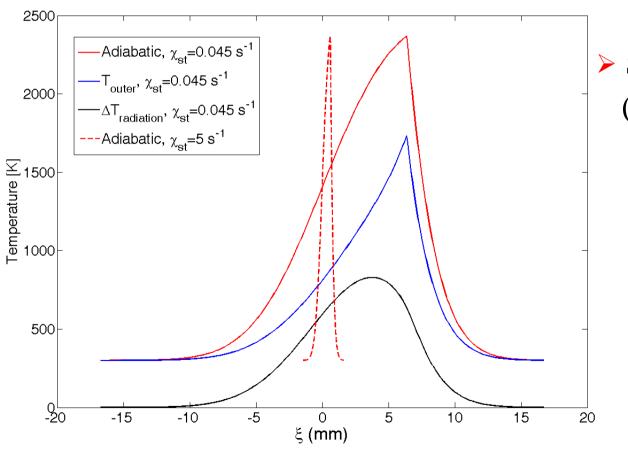


- Intermediate stretch rate: $\chi_{st} = 5 \text{ s}^{-1}$
 - > Flame temperature versus distance normal to the flame





- Low stretch rate: $\chi_{\rm st} = 0.045 \, {\rm s}^{-1}$
 - > Flame temperature versus distance normal to the flame



> Strong radiation effects

$$(\kappa \delta_{outer}) = O(1)$$